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pH-Responsive nanofiltration membranes based on porphyrin supramolecular self-assembly by layer-by-layer technique†

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A novel pH-responsive nanofiltration membrane was fabricated by means of layer-by-layer (LbL) technique based on porphyrin supramolecular self-assembly. The multilayer membrane was prepared on a hydrolyzed poly(acrylonitrile) (PAN) support membrane, and was composed of poly(allylamine hydrochloride) (PAH) as a polycation and poly(styrene sulfonate) (PSS) as a polyanion and 5,10,15,20-tetrakis-(4-sulfonatophenyl)-porphyrin (TPPS) as the pH-responsive functional supramolecular. Aggregation of TPPS and the shielding effect of salt in solution affected the adsorption of TPPS onto the membrane, while the higher ionization degree of the oppositely charged membrane with PAH favored the adsorption of TPPS. A coil structure of polyelectrolytes caused by the lower ionization degree of PAH or by the shielding effect of salt led to higher adsorption of polyelectrolytes on the membrane. The LbL assembly membrane showed higher and pH-responsive water flux and salt rejection compared with that without TPPS. At pH 1.0, TPPS assembled into J-aggregates on the membrane surface, and the membrane showed relatively lower water flux and higher rejection. When the pH value was increased above 2.0, TPPS transformed into H-aggregates and monomers, and the membrane showed relatively higher water flux and lower salt rejection.

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1. Introduction

Nanofiltration (NF) membranes with separation characteristics falling in the range between reverse osmosis (RO) and ultrafiltration (UF) membranes have gained lots of attention due to their utility in various industrial fields for selective separation processes at low applied pressures.^{1–3} Currently, most commercial NF membranes are prepared by phase inversion,^{4,5} interfacial polymerization,^{6–9} and post-treatment of a more porous support (surface coatings, grafting, *etc.*).^{10,11} However, these technical controls are often more complicated, and there are many factors that can effect the structures and properties of the membranes.

The layer-by-layer (LbL) approach based on self-assembly of charged polyelectrolytes on an oppositely charged porous support to fabricate NF membranes has attracted great attention recently.^{12–16} Polyelectrolytes assembly is driven by electrostatic interactions and by entropic considerations related to

the liberation of counterions during assembly. LbL approach to fabricating NF membranes can provide number of advantages. It can provide the potential to accurately control membrane thickness on the nanometer-scale, and there is a degree of self-healing from the fabrication process, and the separation properties of membrane can be readily controlled *via* the types of the polyelectrolyte used, numbers of applied layers, polymer compositions, concentration, pH and ionic strength during coating.¹ In particular, the materials can be low-cost, water soluble and commercially available polymers.

Stimuli responsive membranes can alter their physicochemical properties when subjected to specific external environmental conditions such as pH, temperature, ionic strength, and so forth.^{2,15–22} These physicochemical changes can lead to changes in their permeability and selectivity. Since pH is a crucial parameter and easy to be adjusted in membrane separations, pH-responsive membranes have attracted great attention. Most of pH-responsive membranes composed of porous membrane substrates and surface-tethered pH-responsive polymer chains are fabricated by surface graft or phase inversion method.^{23–27} Qian *et al.* proposed pH-responsive membranes for sugar separations based on surface modified by grafting poly(acrylic acid) (PAA) nano-chains using a UV initiated free radical polymerization method, and pH dramatically affected the membrane performance and selectivity that be used to separate monosaccharides, disaccharides, and their mixtures.²³ Chu *et al.* prepared pH-responsive membranes by

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other chemicals were analytical reagents and used as received. Deionized water purified with a Milli-Q system (Millipore) was used in this study.

The charged PAN support was prepared using a procedure reported earlier with slightly modified.¹³ PAN membrane was hydrolyzed by immersing in a NaOH solution (1.5 M) at 40 °C for 1.5 h, and then neutralized by rinsing with deionized water. After the process, the -CN groups on PAN membrane were transformed to -COOH groups, which could benefit assembling the first positively charged PAH layer. The original PAN membrane and PAN-COOH membrane were characterized by attenuated total reflectance Fourier transform infrared spectroscopy (ATR-FTIR) (Bruker Vector 22).

The polyelectrolyte layers were cross-linked by glutaraldehyde (GA) to improve the stability of LbL assembly membrane. The PAN-[PAH/(PSS-TPPS)]_n membrane was added into 0.1 wt% GA solution for different time (0, 60, 100, 120, and 150 min), and then rinsing with deionized water for 30 min to remove the residual GA.

2.3.1 Influence of solution pH on LbL assembly membrane. To study the influence of polyelectrolyte solution pH on LbL assembly membrane, PAH buffer solutions (1.0 g L^{-1}) with different pH values (pH 2.0, pH 3.5, pH 4.5, pH 6.0, pH 8.0 and pH 9.0) and PSS-TPPS buffer solution (1.0 g L^{-1} and $65 \text{ }\mu\text{M}$) at a fixed pH 6.5 were prepared as the feeding solutions. Also PSS-TPPS buffer solutions (1.0 g L^{-1} and $65 \text{ }\mu\text{M}$) with different pH values (pH 2.0, pH 3.5, pH 4.5, pH 6.5 and pH 8.0) and PAH buffer solution (1.0 g L^{-1}) at a fixed pH 6.5 were prepared as another set of feeding solutions.

2.1 Materials

PSS ($M_w = 70\,000$ Da), PAH ($M_w = 15\,000$ Da) and 5,10,15,20-tetrakis-(4-sulfonatophenyl)-porphyrin (TPPS, >95%) were obtained from J&K Chemicals and used without further purification. PAN ($M_w = 150\,000$ Da) was purchased from Tianjin Kemiou Chemical Reagent Co., Ltd and used as received. All the

2.3.2 Influence of ionic strength on LbL assembly membrane. Different membranes were prepared with similar method except adding 0 M, 0.3 M, 0.8 M, and 1.2 M of NaCl in PAH and PSS–TPPS solutions to study the influence of ionic strength.

2.4 Characterization

The water contact angle of membrane was measured *via* a sessile drop method using a contact angle measurement apparatus (CM3250, KRUS GmbH, Germany) equipped with video capture. The membranes were dried under nitrogen gas and then dried overnight at room temperature prior to the contact angle measurements. For each membrane, average of 6–8 measurements was taken to minimize the experimental error.

Ultraviolet-visible (UV-vis) absorption and solid-state diffuse reflectance UV-vis (DRUV) spectra were measured on a TU-1901 UV-vis spectrophotometer (Purkinje General, China).

The surface and cross-section morphology of membranes were characterized by field emission electron microscopy (FESEM, Hitachi S-4800, Japan) under high vacuum conditions.

The surface morphology and roughness of dry membranes were measured by atomic force microscopy (AFM) recorded using a Multimode IIIA scanning probes. Imaging was done in tapping mode at ambient condition using a silicon RTESPA probe.

The outer surface zeta potential of the membrane was measured using the Sur Pass Electrophoretic Analyzer (Anton-Paar GmbH, Austria) in 0.001 M KCl solution. Each data point represents an average of five measurements for each membrane. The outer surface zeta potential was estimated using the Helmholtz–Smoluchowski equation as given below:^{38,39}

$$\zeta = \frac{U}{\Delta P} \frac{\eta}{\varepsilon \varepsilon_0} \kappa_B$$

where U was the steam potential, ΔP was the operation pressure, η was the viscosity of the electrolyte solution, ε was the dielectric constant of electrolyte, ε_0 was the vacuum permittivity and κ_B was the electrolyte conductivity.

2.5 Nanofiltration experiments

The separation performance of the membrane was determined using a home-made stainless steel disc with an effective filtration area of 22.9 cm². Before test, the membranes were equilibrated with buffer solutions at each pH for 10 h, and the system was first pressurized at 0.2 MPa for 30 min until the flux reach a steady state. The concentration of MgSO₄ was 2.0 g L⁻¹. The water flux (J) was calculated using the following equation:

$$J = \frac{V}{A \times t}$$

where J is the water flux (L m⁻² h⁻¹); V is the permeate volume (L); A is the effective membrane area (m²); t is the filtration time (h).

The salt rejection (R) was calculated as following:

$$R = \left(1 - \frac{C_p}{C_f}\right) \times 100\%$$

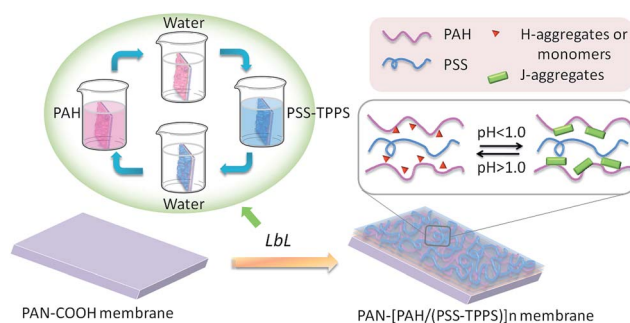
where C_f and C_p are the salt concentrations in the feed and permeate, respectively.

3. Results and discussion

3.1 Preparation of LbL membrane

ATR-FTIR was used to confirm the hydrolysis of the PAN support (Fig. S1†). The peaks at 2243 cm⁻¹ and 1451 cm⁻¹ are due to stretching vibrations of the CN moiety of the PAN membrane.⁴⁰ After hydrolysis of PAN membrane, a peak reduction at 2243 cm⁻¹ and the emergence of new peaks at 1560 cm⁻¹ and 1405 cm⁻¹ corresponding to the C=O bond in the COOH groups proved that most of the CN groups on the membrane surface converted to COOH groups.⁴¹

Multilayer of PAH/(PSS–TPPS) was assembled on PAN–COOH membrane surfaces by layer-by-layer method due to electrostatic interaction (Scheme 1). The pH and ionic strength of PAH and PSS–TPPS solutions may influence the structure and properties of the multilayer. PAH is a weak base, and the pK_a is about 9.0. The charge and extension of PAH chain change with pH value. The DRUV was used to investigate the adsorption capacity of TPPS and PSS at different pH values of PAH solution (Fig. 1). At pH 2.0 of PAH solution, B bands and Q bands of TPPS were red shifted to 490 nm and 705 nm (Fig. 1a), which indicated that TPPS molecules self-assembled into J-aggregates on the membrane surface. When pH value of PAH solution was increased above 3.5, the bands at about 405 nm and 422 nm can be observed, which suggested that H-aggregates and monomers of TPPS coexisted on the membrane surface. In addition, the absorption intensity of TPPS on the membrane was higher at pH 2.0 than at pH above 3.5, and the absorption intensity at 422 nm was decreased with increased pH value (Fig. 1a). This is because the charge of PAH was reduced with increased pH value and the electrostatic interaction between PAH and TPPS was weakened leading to lower adsorption capacity of TPPS. At pH 9.0, the shoulder at 405 nm presenting H-aggregates of TPPS disappeared, which means TPPS existed as only monomer on the membrane because of quite low adsorption capacity. Then the absorption intensity at 405 nm was used to evaluate the



Scheme 1 Schematic model of LbL assembly membrane fabrication and pH-responsive structure of the TPPS assembly.



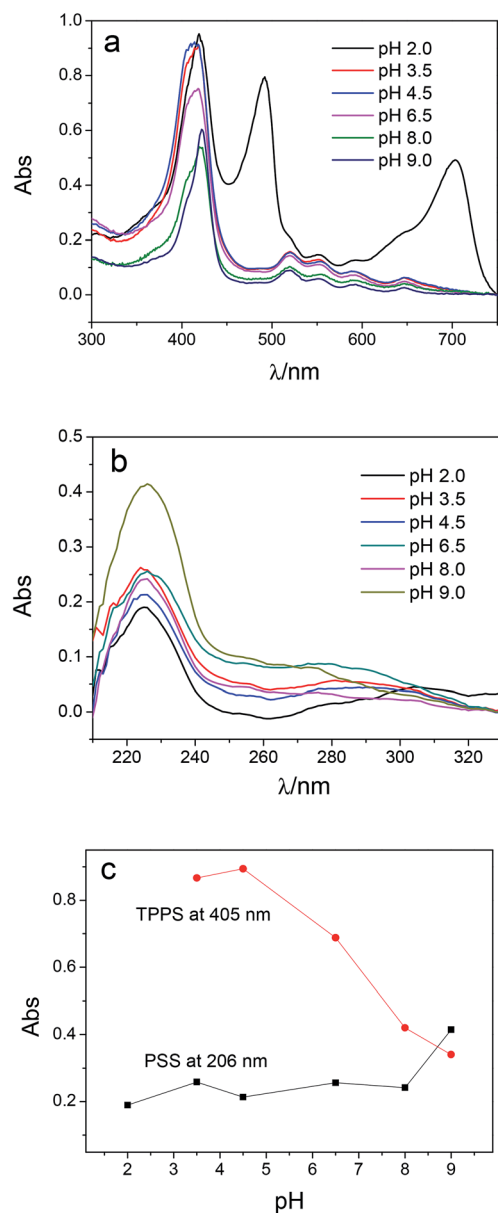


Fig. 1 DRUV spectra of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared from PSS-TPPS solution at pH 6.5 and PAH solutions at different pH values (a, TPPS; b, PSS), and absorbance at 405 and 206 nm at different pH values of PAH (c). The absorbance at 405 nm at pH 2.0 of PAH was not displayed because TPPS formed J-aggregates here.

amount of TPPS adsorbed on membrane. The trend of decreasing adsorption capacity of TPPS can be obviously observed in Fig. 1c. By contrast, larger adsorption capacity of

polyelectrolytes on the membrane was obtained at higher pH value of PAH solution. The band at 226 nm attributing to the benzene of PSS showed an increased intensity when pH value of PAH solution was increased to 9.0 (Fig. 1b and c). Because, at pH above pK_a of PAH, the electrostatic repulsion between positively charged groups on PAH was weakened and the extended chain changed to a coil structure, which allowed more PAH chains to attach to the membrane and favored the adsorption of PSS consequently.

The top surface morphologies and roughness of the PAN-[PAH/(PSS-TPPS)]₆ membranes prepared with different pH value of PAH solutions were investigated by AFM. As shown in Fig. 2, the surface of PAN support membrane was smooth, and the root-mean-square (RMS) which was used to evaluate the surface roughness was about 19.6 nm. The RMS of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared with PAH pH values of 2.0, 4.5, and 9.0 were 23.2 nm, 36.3 nm, and 46.0 nm, respectively. The roughness increased with increased pH value of PAH solution because of the increasing adsorption capacity of PSS and PAH.⁴²

PSS is a strong polyelectrolyte, and the charge and the configuration of PSS are not pH-dependent. Thus adsorption capacity of PSS on membrane is supposed to be unchanged as the pH of PSS-TPPS changes. However, the pH value of PSS-TPPS solution could influence the ionization degree of PAH on the membrane and the aggregation of TPPS in solution. Fig. 3 shows the DRUV spectra of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared at different pH values of PSS-TPPS. The absorption intensity of TPPS increased first and then decreased with increased pH value of PSS/TPPS solution (Fig. 3a and c). The lower adsorption capacity of TPPS at lower pH was due to the J-aggregation of TPPS formed in solution at pH 2.0 which affected the adsorption of TPPS on membrane. At pH above 8.0, the decreased adsorption capacity of TPPS may be caused by the decreased ionization degree of PAH adsorbed on the membrane. The increased concentration of OH⁻ may also play a role in shielding the interaction between TPPS and PAH. The decrease in adsorption capacity of PSS at higher pH was not significant (Fig. 3b and c), because the multiple-point cooperative binding of polyelectrolytes allowed considerable amounts of PSS to interact with PAH.

As shown in Fig. 4, the RMS of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared with PSS-TPPS solutions at pH values of 2.0, 4.5, and 8.0 were 42.4 nm, 44 nm, and 44.8 nm, respectively. The nearly unchanged roughness also indicated little changes in the adsorption capacity of polyelectrolytes when different pH values of PSS/TPPS solutions were applied.

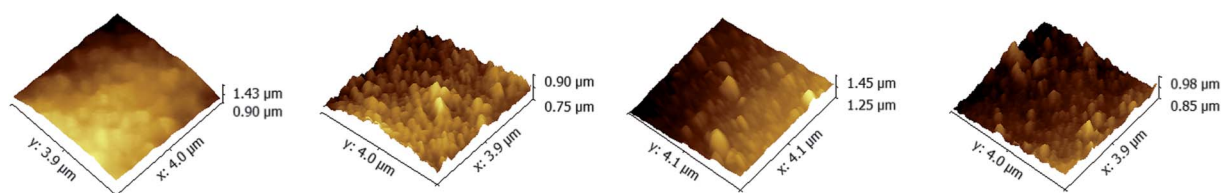


Fig. 2 AFM images of PAN support membrane (A); and PAN-[PAH/(PSS-TPPS)]₆ membranes prepared from PSS-TPPS solutions at pH 6.5 and PAH solutions at pH values of 2.0 (B), 4.5 (C), and 9.0 (D).



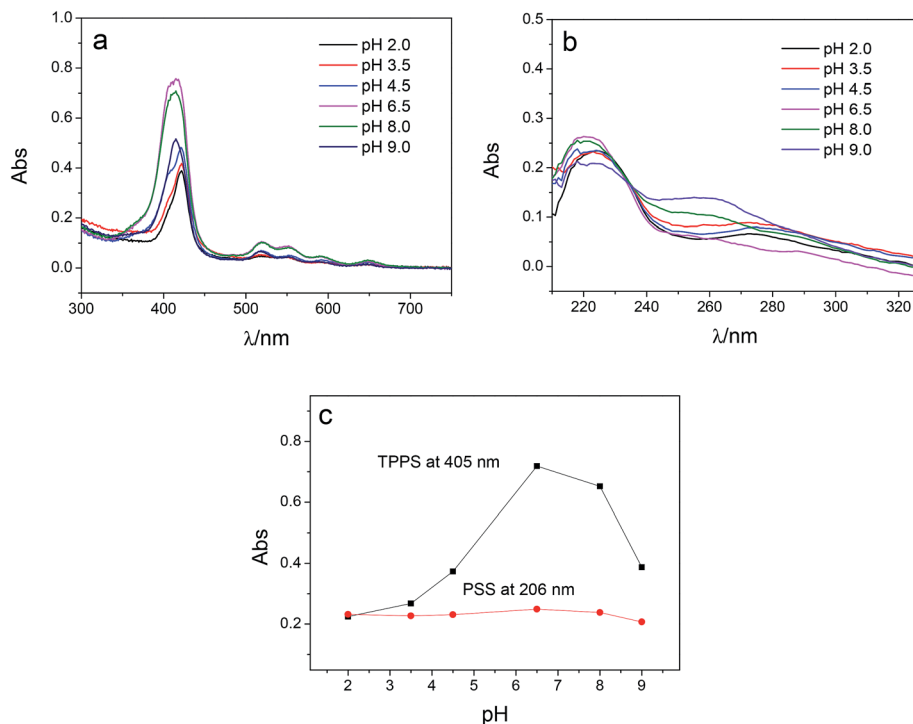


Fig. 3 DRUV spectra of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared from PAH solutions at pH 6.5 and PSS-TPPS solutions at different pH values (a, TPPS; b, PSS), and absorbance at 405 and 206 nm at different pH values of PSS (c).

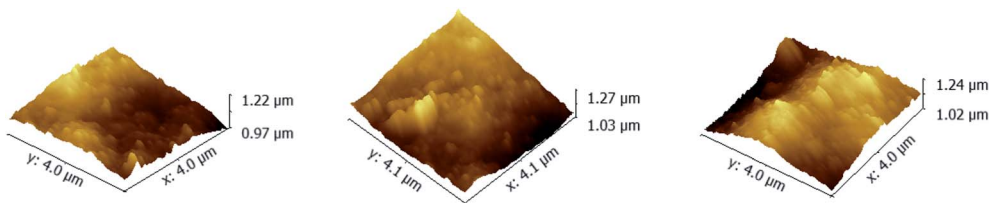


Fig. 4 AFM images of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared from PAH solutions at pH 6.5 and PSS-TPPS solutions at pH values of 2.0 (A), 4.5 (B), and 8.0 (C).

To investigate the influence of the ionic strength on polyelectrolyte multilayer forming, LbL assembly experiments were conducted in buffers with variable salt concentrations. A set of DRUV spectra of PAN-[PAH/(PSS-TPPS)]₆ membranes obtained

at different ionic strengths varied from 0 to 1.2 M is depicted in Fig. 5. It is clearly seen that the adsorption capacity of TPPS decreased (Fig. 5a) and that of PSS increased (Fig. 5b) when ionic strength increased. It is clear that ions of high

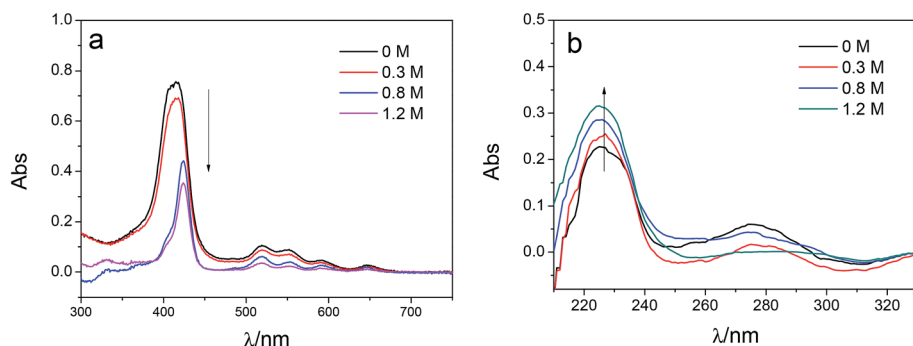


Fig. 5 DRUV spectra of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared at different ionic strengths (TPPS (a) and PSS (b)).



Fig. 6 AFM images of PAN-[PAH/(PSS-TPPS)]₆ membranes prepared at different ionic strengths (0 (A), 0.3 (B), 0.8 (C), and 1.2 (D)).

concentration shielded the interaction between TPPS and polyelectrolytes. As for polyelectrolyte, at low ionic concentration, polyelectrolyte chains normally present an extended conformation, while at higher ionic strength, they tend to coil because salt ions shield the electrostatic repulsion between charged groups of polyelectrolytes.^{43,44} That is the reason why more PSS were loaded on membrane surface at higher ionic strength. As shown in Fig. 6, the surface of PAN-[PAH/(PSS-TPPS)]₆ membrane became rougher as ionic strength increased. The RMS were 25.6 nm, 47.4 nm, 53.6 nm, and 71.4 nm for PAN-[PAH/(PSS-TPPS)]₆ membranes prepared at ionic concentration of 0 M, 0.3 M, 0.8 M, and 1.2 M because of more polyelectrolytes adsorbed onto the membrane. All these results above showed that the adsorption of TPPS onto the membrane was determined only by electric attraction, while the assembly of polyelectrolytes depended on chain configuration as well as electrostatic interaction.

3.2 Surface properties of LbL membrane

The adsorption capacity of TPPS and polyelectrolytes on the membrane grew as depositing more polymer/TPPS films. Fig. 7 shows the DRUV spectra of PAN-[PAH/(PSS-TPPS)]_n membranes with different number of bilayer prepared at pH 6.5 and 0.5 M of ionic strength. It is obviously seen that the absorption of TPPS (Fig. 7a) and PSS (Fig. 7b) increased with increasing bilayer number. Further, the surface properties of the layers were of particular importance to the transport processes occurring at the interface between the electrolyte solutions and the multilayer. Herein, we prepared PSS-TPPS-terminated (T-PSS-TPPS) layers ($n = 1.0, 2.0, 3.0...$) and PAH-terminated (T-PAH) layers ($n = 0.5, 1.5, 2.5, 3.5...$) to

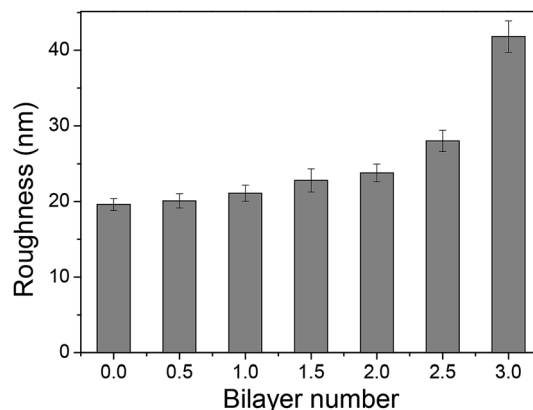


Fig. 8 Surface roughness of PAN-[PAH/(PSS-TPPS)]_n membranes with different bilayer numbers prepared at 0.5 M ionic strength and pH 6.5. For example, $n = 2$ means the membrane had 2 PAH/(PSS-TPPS) bilayers and the outmost layer (terminating layer) is PSS-TPPS; $n = 2.5$ means the membrane had one more PAH coating (*i.e.*, half of a bilayer) in addition to the 2 PAH/(PSS-TPPS) bilayers, with PAH being the terminating layer.

investigate the surface properties of the layers. The experimental results for the PAN-COOH substrate were also displayed as a reference for comparative study.

Membrane surface roughness increased with the increased number of polyelectrolyte layers (Fig. 8), which could be attributed to the random adsorption of the polyelectrolytes.³¹ As increasing bilayer number, the roughness had an increasing tendency for both T-PSS-TPPS and T-PAH layers.

The values of the zeta potential reflected the surface electric properties because they were the electric potential difference

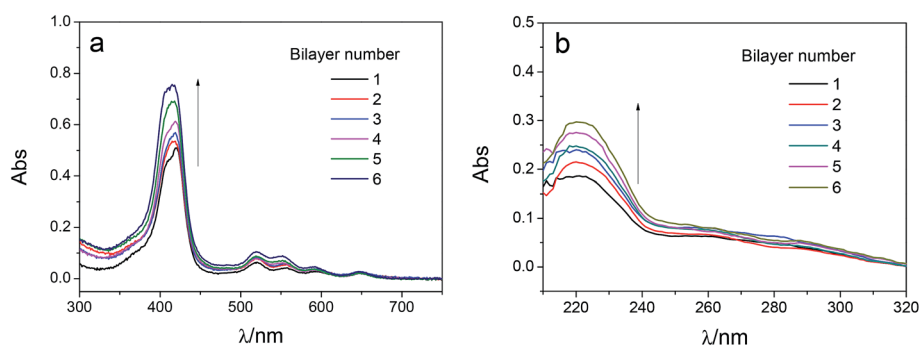


Fig. 7 DRUV spectra of PAN-[PAH/(PSS-TPPS)]_n membranes with different number of bilayer (TPPS (a) and PSS (b)). The concentration of PAH, PSS, and TPPS were 1.0 g L⁻¹, 1.0 g L⁻¹, and 65 μM, respectively. The pH value of solutions was 6.5 and ionic strength was 0.5 M.



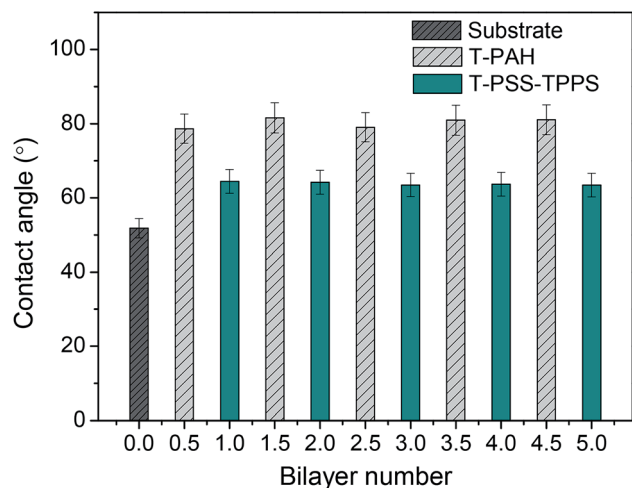


Fig. 9 Water contact angles of PAN-[PAH/(PSS-TPPS)]₆ membranes with different layers prepared at 0.5 M of salt and pH 6.5.

between the mobile diffusion layer on the charged surface and the bulk solution. The sign of the surface charge was reversed. For PAN-(PAH/PSS) $_n$ membrane without TPPS, and a positive value of +25 mV was yielded when the first PAH layer was deposited on the negatively charged PAN-COOH substrate ($n = 0.5$) (Fig. S2†). After depositing the next negatively charged PSS, the zeta potential of layer was reversed to -40 mV. As depositing more layers of the polyelectrolyte film, oscillatory changes of the surface potential were displayed with amplitudes about 60 mV. PSS-terminated layers gave rise to a higher potential absolute

value compared to PAH-terminated layers because of the strong polyelectrolyte PSS. It is also noted that, as for PAN-[PAH/(PSS-TPPS)]_n membrane, TPPS enhanced the amplitudes, especially increased the potential absolute value of PSS-TPPS-terminated layers. This made it possible to enhance membrane salt rejection that was strongly influenced by electrostatic repulsion.

The contact angle measurement is a useful method to observe changes in the surface hydrophilicity of the membranes. As shown in Fig. 9, contact angle of PAN-COOH support membrane is about 52° . The coating of polyelectrolytes on the membrane support in all cases led to higher contact angles. As increasing the number of bilayer, little difference in contact angle value of the same type of terminating layer was observed. However, contact angle values of T-PSS-TPPS layer were lower than those of T-PAH layers. That is to say, the PSS-TPPS-terminated membrane is more hydrophilic as compared to the PAH-terminated membrane, because sulfonic acid groups are more easily to form hydrogen bond with water.

The morphology of PAN-COOH substrate membrane and PAN-[PAH/(PSS-TPPS)]₆ membrane was studied by field emission scanning electron microscopy (FESEM) as shown in Fig. 10. It can be seen that the top surface image of the PAN-COOH membrane (Fig. 10A) was quite smooth and the bottom surface (Fig. 10B) had an open pore structure. The immobilization of PAH/(PSS-TPPS) multilayer destroyed the top surface smoothness (Fig. 10D). However, almost no change was observed on the bottom surface after LbL assembly, indicating that the deposition of polyelectrolytes and TPPS mainly occurred on the top surface due to its high functional group density. The cross-section FESEM images of PAN-COOH membrane (Fig. 10C)

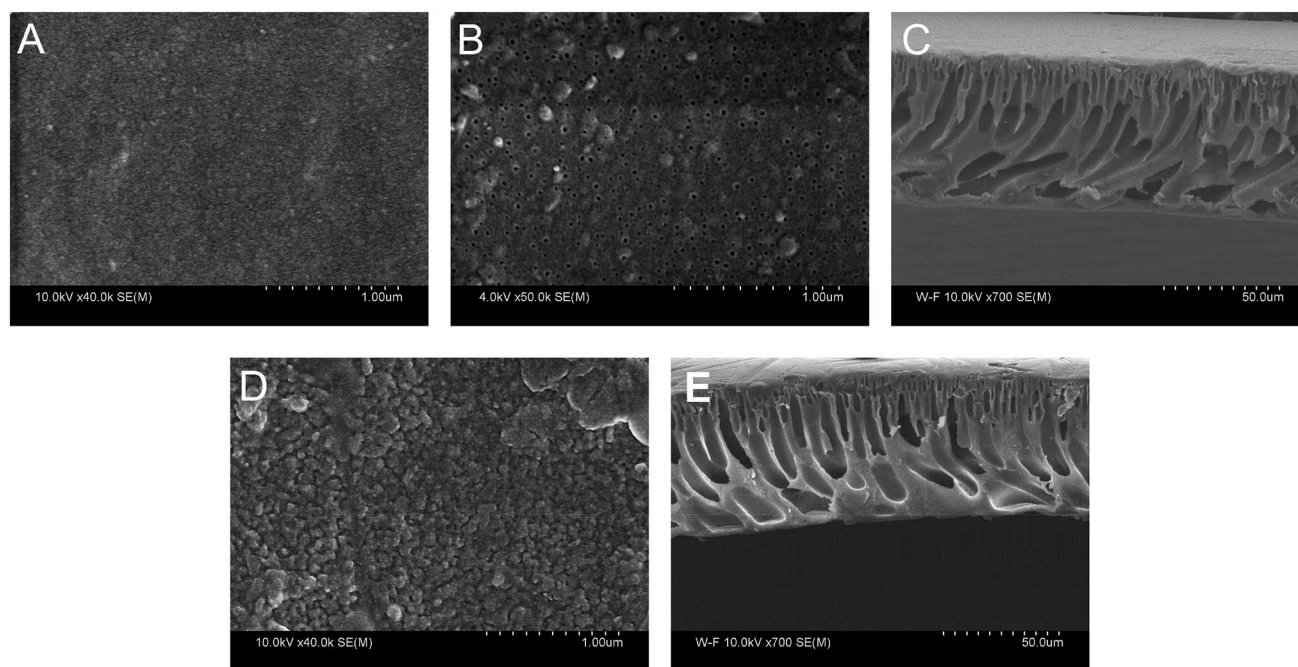
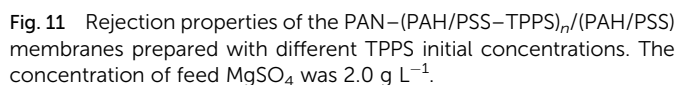
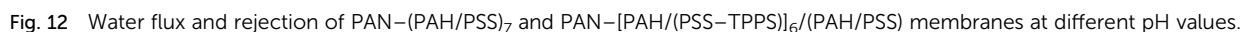


Fig. 10 Surface FE-SEM images of top surface (A), bottom surface (B), and cross-section (C) of PAN-COOH membrane, top surface (D), and cross-section (E) of PAN-[PAH/(PSS-TPPS)]₆ membrane (the bottom surface image of PAN-[PAH/(PSS-TPPS)]₆ membrane was not shown because no distinction compared with the substrate was observed).



The introduction of TPPS increased the charge amount of the assembly layer, and may also change the compact degree of the assembly layer,³⁶ thus affecting the permeability and rejection of the membrane. Fig. 11 shows the water flux and MgSO_4 rejection of $\text{PAN-}[\text{PAH}/(\text{PSS}/\text{TPPS})]_n(\text{PAH}/\text{PSS})$. Obviously, with the increase of bilayer number, the water flux was reduced and the rejection was increased due to the more compact assembly layers. When the bilayer number reached 6, the rejection rate was no longer increased. It is important that, at the same bilayer

It has been proved that J-aggregates attached to grafted polymer chains has a large size which can block the pore of the separating membrane layer and then influence the permeability and rejection properties of membrane.²⁹ The supramolecular aggregates of small amount immobilized in LbL assembly layers may be used in the fine structure adjustment and separation property controlling of nanofiltration membranes. As shown in Fig. 12, both water flux and rejection of the membrane PAN-[PAH/(PSS-TPPS)]₆/(PAH/PSS) with TPPS were higher than those of PAN-(PAH/PSS)₇ without TPPS. More importantly, the water flux and rejection of the membrane without TPPS hardly changed within the pH range; by contrast, a prominent change in the water flux and rejection of PAN-[PAH/(PSS-TPPS)]₆/(PAH/PSS) occurred within the pH range of 1.0–2.0. It is the assembly structure of the TPPS aggregates in response to pH on the



membrane surface that caused the pH-dependent change in the pore size and the resultant permeability and rejection. At flux pH 1.0, TPPS J-aggregates of larger size blocked the membrane surface pores. On the contrary, at a feed pH above 2.0, J-aggregates transformed to small-sized H-aggregates and monomers and resulted in a larger membrane pore size and higher water permeation rate and lower salt rejection (Scheme 1).

4. Conclusions

In this paper, pH-responsive nanofiltration membrane was fabricated by means of the LbL technique based on TPPS supramolecular self-assembly with hydrolyzed PAN as support membrane and PAH and PSS as the polyelectrolytes. The self-assembly of TPPS and polyelectrolytes onto membrane was influenced by pH and ionic strength of the feed solution. At lower pH of PAH solution, TPPS formed J-aggregates on the membrane and had a higher adsorption capacity, while at higher pH of PAH solution, higher adsorption capacity of polyelectrolytes was obtained due to the coil structure of polymers. Lower pH of PSS and TPPS mixed solution affected the adsorption of TPPS due to J-aggregates of the dye formed in solution. The shielding effect of increased ionic strength resulted in a lower TPPS adsorption but higher polyelectrolyte adsorption. PSS–TPPS-terminated layer showed larger zeta-potential absolute values and better wettability than PAH-terminated layer. The LbL assembly membrane with TPPS showed higher and pH-responsive water flux and MgSO_4 rejection compared with that without TPPS. At pH 1.0, TPPS assembled into J-aggregate on the membrane surface, and the membrane showed relatively lower water flux and higher rejection. At a feed pH above 2.0, the membrane showed higher water permeation rate and lower salt rejection due to small-sized H-aggregates and monomers of TPPS. The present systems provide valuable insights into the smart nanofiltration membrane and expand types of smart membrane.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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References

- 1 M. Paul and S. D. Jons, *Polymer*, 2016, **103**, 417–456.
- 2 Z. Dang, L. Liu, Y. Li, Y. Xiang and G. Guo, *ACS Appl. Mater. Interfaces*, 2016, **8**, 31281–31288.
- 3 F. Y. Zhao, Q. F. An, Y. L. Ji and C. J. Cao, *J. Membr. Sci.*, 2015, **492**, 412–421.

- 4 G. R. Guillen, G. Z. Ramon, H. P. Kavehpour, R. B. Kaner and E. M. V. Hoek, *J. Membr. Sci.*, 2013, **431**, 212–220.
- 5 M. Sadrzadeh and S. Bhattacharjee, *J. Membr. Sci.*, 2013, **441**, 31–44.
- 6 J. Cheng, W. X. Shi, L. H. Zhang and R. J. Zhang, *Appl. Surf. Sci.*, 2017, **416**, 152–159.
- 7 Q. Zhang, L. Fan, Z. Yang, R. N. Zhang, Y. N. Liu, M. R. He, Y. L. Su and Z. Y. Jiang, *Appl. Surf. Sci.*, 2017, **410**, 494–504.
- 8 K. P. Lee, G. Bargeman, R. de Rooij, A. J. B. Kemperman and N. E. Benes, *J. Membr. Sci.*, 2017, **523**, 487–496.
- 9 K. Yoon, B. S. Hsiao and B. Chu, *J. Membr. Sci.*, 2009, **326**, 484–492.
- 10 D. Menne, C. Uzum, A. Koppelman, J. E. Wong, C. V. Foeken, F. Borre, L. Dahne, T. Laakso, A. Pihlajamaki and M. Wessling, *J. Membr. Sci.*, 2016, **520**, 924–932.
- 11 G. Cocchi, M. G. De Angelies and F. Doghieri, *J. Membr. Sci.*, 2015, **492**, 612–619.
- 12 N. Joseph and P. Ahmadianmini, *Polym. Chem.*, 2014, **5**, 1817–1831.
- 13 S. Ilyas, N. Joseph, A. Szymczyk, A. Volodin, K. Nijmeijer, W. M. de Vos and I. F. J. Vankelecom, *J. Membr. Sci.*, 2016, **514**, 322–331.
- 14 D. Menne, C. Uzum, A. Koppelman, J. E. Wong, C. van Foeken, F. Borre, L. Dahne, T. Laakso, A. Pihlajamaki and M. Wessling, *J. Membr. Sci.*, 2016, **520**, 924–932.
- 15 Q. Nan, P. Li and B. Cao, *Appl. Surf. Sci.*, 2016, **387**, 521–528.
- 16 X. Hu, E. McIntosh, M. G. Simon, C. Staii and S. W. Thomas, *Adv. Mater.*, 2016, **28**, 715–721.
- 17 R. Shevate, M. Karunakaran, M. Kumar and K. V. Peinemann, *J. Membr. Sci.*, 2016, **501**, 161–168.
- 18 B. Ma, X. J. Ju, F. Luo, Y. Q. Liu, Y. Wang, Z. Liu, W. Wang, R. Xie and L. Y. Chu, *ACS Appl. Mater. Interfaces*, 2017, **9**, 14409–14421.
- 19 T. Ito and T. Yamaguchi, *Langmuir*, 2006, **22**, 3945–3949.
- 20 F. P. Nicoletta, D. Cupelli, P. Formoso, G. D. Filpo, V. Colella and A. Gugliuzza, *Membranes*, 2012, **2**, 134–197.
- 21 S. Singh, A. Junghans, J. Tian, M. Dubey, S. Gnanakaran, J. Chlistunoff and J. Majewski, *Soft Matter*, 2013, **9**, 8938–8948.
- 22 J. Irigoyen, L. Han, I. Llaena, Z. Mao, C. Gao and S. E. Moya, *Macromol. Rapid Commun.*, 2012, **33**, 1964–1969.
- 23 H. H. Himstedt, H. Du, K. M. Marshall, S. R. Wickramasinghe and X. Qian, *Ind. Eng. Chem. Res.*, 2013, **52**, 9259–9269.
- 24 Y. C. Chen, R. Xie and L. Y. Chu, *J. Membr. Sci.*, 2013, **442**, 206–215.
- 25 X. Chen, B. W. Zhao, L. Z. Zhao, S. Y. Bi, P. Han, X. Feng and L. Chen, *RSC Adv.*, 2014, **4**, 29933–29945.
- 26 T. Luo, S. Lin, R. Xie, X. J. Ju, Z. Liu, W. Wang, C. L. Mou, C. Zhao, Q. Chen and L. Y. Chu, *J. Membr. Sci.*, 2014, **450**, 162–173.
- 27 J. I. Clodt, V. Filiz, S. Rangou, K. Buhr, C. Abetz, D. Hoeche, J. Hahn, A. Jung and V. Abetz, *Adv. Funct. Mater.*, 2013, **23**, 731–738.
- 28 M. Wang, F. Yan, L. Zhao, Y. Zhang and M. Sorci, *RSC Adv.*, 2017, **7**, 1687–1696.



- 29 H. Ye, L. Chen, A. Li, L. Huang, Y. Zhang, Y. Li and H. Li, *J. Appl. Polym. Sci.*, 2015, **132**, 41775.
- 30 Y. Egawa, R. Hayashida and J.-I. Anzai, *Langmuir*, 2007, **23**, 13146–13150.
- 31 Z. El-Hachemi, C. Escudero, F. Acosta-Reyes, M. T. Casas, V. Altoe, S. Aloni, G. Oncins, A. Sorrenti, J. Crusats, J. L. Campos and J. M. Ribo, *J. Mater. Chem. C*, 2013, **1**, 3337–3346.
- 32 A. D. Schwab, D. E. Smith, C. S. Rich, E. R. Young, W. F. Smith and J. C. de Paula, *J. Phys. Chem. B*, 2003, **107**, 11339–11345.
- 33 P. Kubat, K. Lang, P. Janda and P. Anzenbacher, *Langmuir*, 2005, **21**, 9714–9720.
- 34 P. Dambruoso, M. Ballestri, C. Ferroni, A. Guerrini, G. Sotgiu, G. Varchi and A. Massi, *Green Chem.*, 2015, **17**, 1907–1917.
- 35 F. Tantussi, F. Fuso, M. Allegrini, N. Micali, I. G. Occhiuto, L. M. Scolaro and S. Patane, *Nanoscale*, 2014, **6**, 10874–10878.
- 36 V. V. Serra, N. G. B. Neto, S. M. Andrade and S. M. B. Costa, *Langmuir*, 2017, **33**, 7680–7691.
- 37 M. Liu, L. Zhao, S. Li, H. Ye, H. An and Y. Zhang, *RSC Adv.*, 2016, **6**, 10704–10712.
- 38 Y. Liao, T. P. Farrell, G. R. Guillen, M. Li, J. A. T. Temple, X. G. Li, E. M. V. Hoek and R. B. Koner, *Mater. Horiz.*, 2014, **1**, 58–64.
- 39 M. Kumar and M. Ulbricht, *Polymer*, 2014, **55**, 354–365.
- 40 G. Zhang, H. Meng and S. Li, *Desalination*, 2009, **242**, 313–324.
- 41 G. Zhang, H. Yan, S. Ji and Z. Liu, *J. Membr. Sci.*, 2007, **292**, 1–8.
- 42 T. Ogawa, B. Ding, Y. Sone and S. Shiratori, *Nanotechnology*, 2007, **18**, 695–700.
- 43 J. Zhang, R. Kou and G. Liu, *Langmuir*, 2017, **33**, 6838–6845.
- 44 S. M. R. Shaikh, M. S. Nasser, I. A. Hussein and A. Benamor, *Chem. Eng. J.*, 2017, **311**, 265–276.

