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# ***In situ* hierarchical self-assembly of NiFeHCF nanoparticles on nickel foam: highly active and ultra-stable bifunctional electrocatalysts for water splitting and their environmental assessment towards green energy†**

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A 3D hierarchical nickel–iron hexacyanoferrate electrocatalyst was successfully grown on nickel foam using an energy-efficient *in situ* self-assembly method. The as-prepared NiFeHCF@NF electrode has good morphology and intimate contact with the NF compared to electrodes from the co-precipitation method. The well-designed NiFeHCF@NF nanostructure delivers prominent performances that require overpotentials as low as 210 and 125 mV@10 mA cm<sup>−2</sup> for the OER and HER in 1 M KOH, respectively. Tafel slope and electrochemical impedance studies further revealed favourable kinetics during electrolysis. Hence, an NiFeHCF@NF||NiFeHCF@NF water electrolyser only required 1.56 V@10 mA cm<sup>−2</sup> with an ~2.5% potential loss. Furthermore, the synergistic effect of iron and nickel with ferrocyanide improved the structural stability and promoted the generation of active phases during the OER/HER, resulting in outstanding durability for 150 h. Moreover, the novel all-in-one strategy can be used to explore other bifunctional and cost-efficient electrocatalysts for various applications. The solar-based water electrolysis and environmental assessment confirmed the practical use of NiFeHCF@NF for eco-friendly industrial hydrogen production.

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## 1. Introduction

Hydrogen production *via* electrocatalytic water splitting (EWS) is being extensively observed as a potential method for addressing the world's energy crisis and related environmental problems. EWS comprises two half-reactions: the cathodic hydrogen evolution reaction (HER) and the anodic oxygen evolution reaction (OER); both are sluggish even while using effective benchmark catalysts of RuO<sub>2</sub> and IrO<sub>2</sub> (OER) and Pt/C (HER). However, high price, low abundance and instability limit the

global scalability of sustainable energy technologies.<sup>1–6</sup> Therefore, efficient, stable, abundant and cost-effective bifunctional electrocatalysts are essential for water splitting. Although numerous studies throughout the past few years have concentrated on transition metal-based chalcogenides, nitrides, oxides and phosphides, more emphasis has been paid to the use of materials derived from metal–organic frameworks (MOFs), which are well-known potential electrocatalysts.<sup>7–12</sup> Recently, NiFe-LDH has been demonstrated as the best OER catalyst in alkaline electrolytes.<sup>13–15</sup> However, its preparation process requires a high cost chain reaction, which makes it difficult to use in practice, hence, the need for a green synthetic method required to produce non-noble metal electrocatalysts without using additional energy, improving the number of catalytic sites by modifying their shape and structure, and enhancing the reactivity of catalytic sites by including additional components are now the essential approaches for enlightening catalytic performance.<sup>16,17</sup>

Prussian blue analogues (PBAs), a form of perovskite-type MOF with high porosity, large surface area and variable metal catalytic sites have emerged in recent years as catalytic materials for EWS, rechargeable batteries, sensors

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and hydrogen storage applications.<sup>18–24</sup> Andronescu *et al.* reported  $\text{NiFeNO}_3$  with excellent electrocatalytic activity ( $270 \text{ mV}@10 \text{ mA cm}^{-2}$ ) for the OER. Poor adhesion of the catalyst powder to the electrode surface is a significant challenge in the use of powder materials as electrocatalysts for energy conversion. Additionally, binder materials (Nafion) do not have adequate electrical conductivity, which prevents rapid electron transport between the catalyst particles and between particles and electrodes. Consequently, the possible current density becomes significantly reduced.<sup>25</sup> Zhang *et al.* synthesized *in situ* grown iron–nickel nitride nanoparticles on nickel ( $\text{FeNi}_3\text{N}/\text{NF}$ ), which display low overpotentials of 75 and 202 mV for the HER and OER@ $10 \text{ mA cm}^{-2}$ , respectively.<sup>18</sup> Zhang *et al.* synthesized  $\text{NiFeLDH}/\text{NiCoP}/\text{NF}$  electrodes with low overpotentials of 220/120  $\text{mV}@10 \text{ mA cm}^{-2}$  for the OER/HER, respectively.<sup>26</sup> Lu *et al.* synthesized 3D- $\text{NiFeLDH}$  film for the OER, which exhibited a small overpotential of 1.46 V.<sup>27</sup> The aforementioned methods required extra energy supply and were costly, and hence are unsuitable for green energy production.

To overcome all these issues, we synthesised nickel–iron hexacyanoferrate ( $\text{NiFeHCF}/\text{NF}$ ) on NF electrocatalysts by using an all-in-one strategy that includes (i) a binder-free *in situ* growth method; (ii) modifying their shape and structure; (iii) increasing the active sites by adding metal components; and (iv)  $\text{NiFeHCF}/\text{NF}$  being prepared *via* a complete green synthetic method. The advantages gained through the synthetic procedure have been thoroughly discussed in the results and discussion. The as-prepared  $\text{NiFeHCF}/\text{NF}$  was used as a bifunctional electrocatalyst and displayed outstanding catalytic performance for the HER ( $125 \text{ mV}@10 \text{ mA cm}^{-2}$ ) and OER ( $210 \text{ mV}@10 \text{ mA cm}^{-2}$ ). Notably, an  $\text{NiFeHCF}/\text{NF}$  electrolyser showed excellent bifunctional activity of 1.56 V in 1 M KOH@ $10 \text{ mA cm}^{-2}$ . The current findings provide a novel path for the development of economical and productive catalysts for electrocatalytic water splitting. Moreover, the easy

accessibility of  $\text{NiFeHCF}/\text{NF}$  should facilitate commercial hydrogen production.

## 2. Results and discussion

Nickel–iron hexacyanoferrate ( $\text{NiFeHCF}$ ) on NF was fabricated as a 3D self-supported electrode with bifunctional activity using an *in situ* hierarchical self-assembly method for electrocatalytic water splitting. Fig. 1 displays the step-wise synthetic procedure of  $\text{NiFeHCF}/\text{NF}$  (details are given in the ESI†). When utilised as an electrocatalyst for overall water splitting, the 3D hierarchical nanostructure of  $\text{NiFeHCF}/\text{NF}$  has several benefits. The porous 3D structure of NF is beneficial for releasing the  $\text{H}_2$  and  $\text{O}_2$  gas bubbles and is employed as the collector of current. The *in situ* hierarchical self-assembly eliminates the requirement for polymer binders (increased resistance) and creates a smooth channel for electron transport over the whole electrode.<sup>11,25,27</sup> The successful *in situ* growth of  $\text{NiFeHCF}$  on NF was evidenced by the apparent difference in nickel foam colour (Fig. S1a†). The digital photographs of pure Ni foam, as-prepared samples and post-use materials are presented in Fig. S1b.† After water splitting treatment, the shape of the Ni foam remains unchanged but the colour and surface morphology of the electrocatalyst had changed.

The morphology and microstructure of bare NF,  $\text{NiFeHCF}/\text{NF}$  and post-use materials were established by the FESEM technique (Fig. S2†). The surface of bare NF is smooth and free of impurities with a 3D porous structure that offers an abundant surface area to grow active material as a scaffold (Fig. S2a†).<sup>28</sup> The FESEM images (Fig. S2b–d†) at high magnification show that the  $\text{NiFeHCF}/\text{NF}$  has a hierarchical rugged surface and that it was changed after its electrocatalytic performance. Numerous interconnected ultrathin nanosheets are vertically grown on  $\text{NiFeHCF}/\text{NF}$  after the HER and the rugged layers of the electrocatalyst become smooth after the

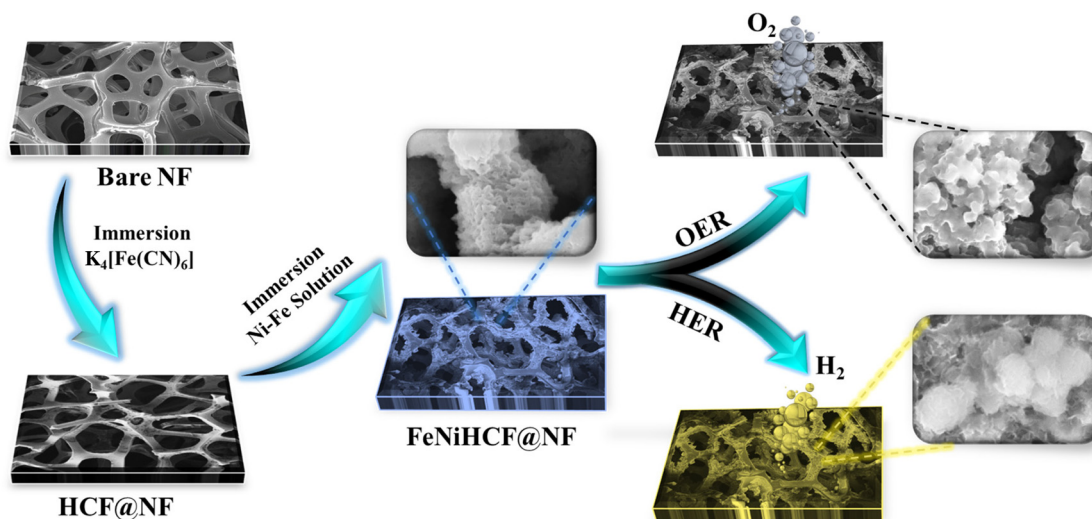


Fig. 1 Synthetic scheme of  $\text{NiFeHCF}/\text{NF}$ .

OER owing to the generation of active sites during the process. Fig. 1 shows the colour and morphological changes of NiFeHCF@NF during the OER/HER and that the catalysts are well adhered to the nickel foam surface.

The crystalline nature and plane values of the prepared catalyst were confirmed by using XRD (Fig. 2a). NiFeHCF@NF has peaks at  $2\theta$  of  $15.1^\circ$  (111),  $17.6^\circ$  (200),  $25^\circ$  (220),  $29.6^\circ$  (311),  $35.6^\circ$  (400),  $39.9^\circ$  (420),  $44.3^\circ$  (422),  $51.6^\circ$  (440),  $54.7^\circ$  (600),  $58.2^\circ$  (620) and  $74.9^\circ$  (800). These peaks lie between the  $\text{Fe}_4[\text{Fe}(\text{CN})_6]_3$  [JCPDS: 73-0687] and  $\text{Ni}_2[\text{Fe}(\text{CN})_6]$  [JCPDS: 75-0037] peaks, which may be due to the presence of nickel- and iron-coordinated cyanides in NiFeHCF@NF.<sup>20,29</sup> According to the XRD of bare NF (JCPDS No. 87-0712), the peaks at  $44.3^\circ$ ,

$51.6^\circ$  and  $76.5^\circ$  have been produced due to the nickel foam substrate (Fig. S3†). The aforementioned results confirmed the successful formation of NiFeHCF in the nickel foam. The functional groups of NiFeHCF@NF were identified using FT-IR (Fig. 2b). The peak at  $2087\text{ cm}^{-1}$  is attributed to the stretching frequency of  $\text{Fe}^{2+}\text{-CN-Ni}^{2+}$ . The bands at  $1610$  and  $3400\text{ cm}^{-1}$  belong to the distortion vibrations and stretching modes of O-H in  $\text{H}_2\text{O}$ , respectively. The peak at  $597\text{ cm}^{-1}$  belongs to the in-plane deformation of Fe-C.<sup>30</sup>

The morphology of NiFeHCF@NF was examined by FESEM at different magnifications. Fig. 3a-d shows the formation of hierarchical coral-like NiFeHCF on the nickel foam. The hierarchical coral-like electrode consists of nanosized units that

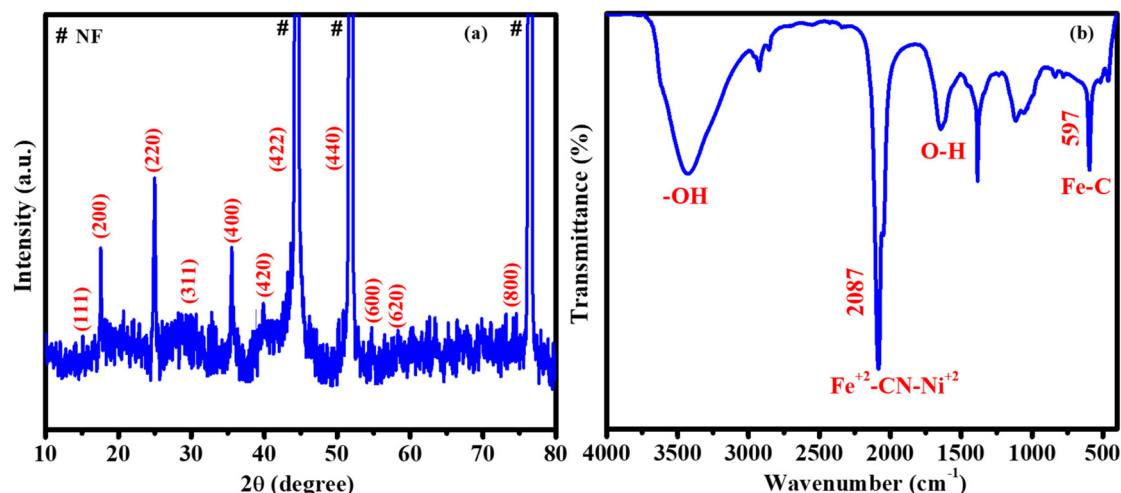


Fig. 2 XRD pattern (a) and the FT-IR spectrum (b) of NiFeHCF@NF.

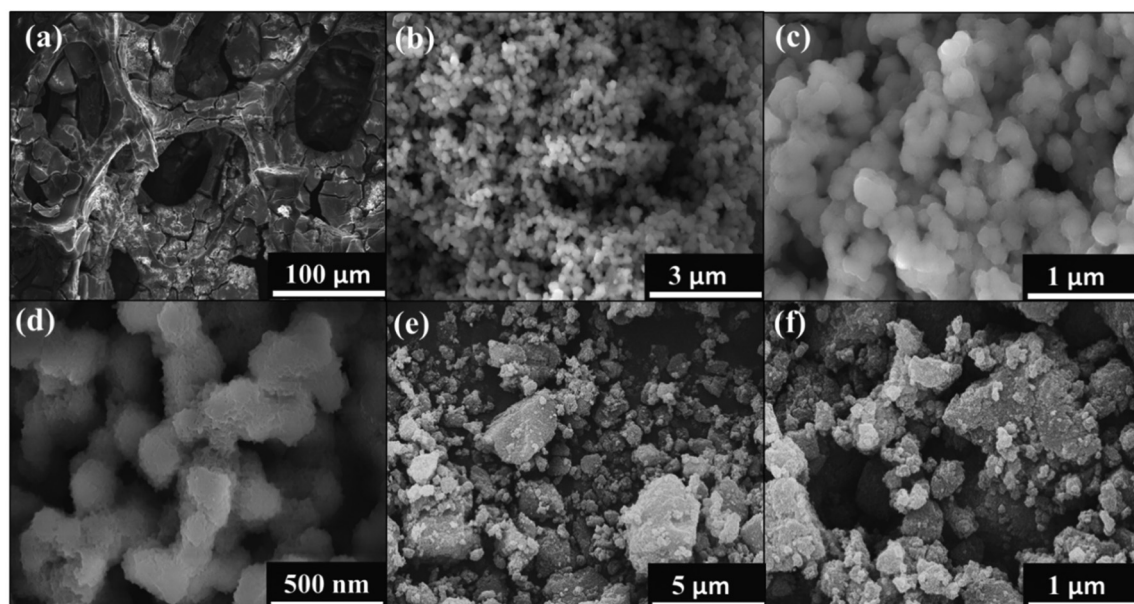


Fig. 3 FE-SEM of NiFeHCF@NF; (a–d) the *in situ* self-assembly method and (e and f) coprecipitation method.



form a system of nanopores; it generates copious catalytic sites leading to improvement of the catalytic performance per geometric area and enables close contact with electrolytes, thus allowing more efficient utilization of active sites.<sup>27</sup> The highly open hierarchical structure facilitates gas release during the HER and OER, and accordingly, this electrode showed high current density ( $\sim 500 \text{ mA cm}^{-2}$ ). The SEM images of NiFeHCF nanoparticles prepared through a co-precipitation method show that they have agglomerated morphology (Fig. 3e and f). Agglomeration of nanoparticles has many disadvantages including reduced surface area, resistance and low catalyst-electrolyte interaction. The SEM images clearly show the morphological improvement of the *in situ* self-assembly method over the co-precipitation method.<sup>31–35</sup> EDX elemental mapping confirmed the homogeneous distribution of component elements and the presence of constituent elements (Fig. S4†). The absence of other elements shows the purity of NiFeHCF@NF, which has the atomic percentages of 28.43% (C), 10.73% (N), 46.21% (O), 11.09% (Ni) and 3.51% (Fe) (Fig. S4g†). The successful *in situ* growth of NiFeHCF@NF without binder was confirmed by the FESEM images.

The crystalline structure and morphology of NiFeHCF@NF were further examined by using HRTEM and EDS. The catalysts were scraped from the NF owing to the tight contact of the catalyst with NF. Consequently, it was difficult to retain the original morphology and hence, the hierarchically grown coral-like morphology is inevitably separated.<sup>31</sup> Fig. 4a and b reveals that together they had a neat shape and smooth coral-like

interconnected morphology. Higher magnification HRTEM images show lattice fringes with *d* spacings of 2.23 Å and 2.5 Å, which are assigned to the FCC (420) and (400) planes, respectively (Fig. 4c). The corresponding SAED (selected area electron diffraction) pattern exhibits concentric circles, which are assigned to the (220), (400), (422) and (440) planes, indicating the crystalline nature of NiFeHCF@NF and this was corroborated by XRD findings (Fig. 4d). The EDX spectrum confirms the existence of constituent elements and the absence of other elements, which shows the purity of the electrocatalyst (Fig. 4e). The atomic percentages of NiFeHCF@NF were determined to be 3.89% (Ni), 2.88% (Fe), 6.79% (O), 9.78% (N) and 76.66% (C). Additionally, inductively coupled plasma optical emission spectroscopy (ICP-OES) was used to analyse the elemental composition of NiFeHCF@NF and the results are shown in Table S1.†

The composition and valence state of NiFeHCF@NF were identified by using XPS. The survey spectrum confirmed the presence of Ni, Fe, O, N and C elements in the electrocatalyst (Fig. 5a). The spectrum of C 1s shows peaks at  $\sim 284.8$  and  $\sim 285.5$  eV attributed to C–C and C–N fragments, respectively (Fig. 5b). Fig. 5c displays the N 1s spectrum corroborating the existence of cyanide content in the catalyst; the peaks at  $\sim 398.1$  and  $\sim 398.6$  eV are attributed to pristine ferrocyanide (C≡N) and metal–N of the ferrocyanide, respectively.<sup>36</sup> The O 1s spectrum revealed signals at  $\sim 531.0$  and  $\sim 533.1$  eV attributed to coordinated water and adsorbed water, respectively (Fig. 5d). The Fe 2p spectrum has peaks at 708.8, 710.1 and

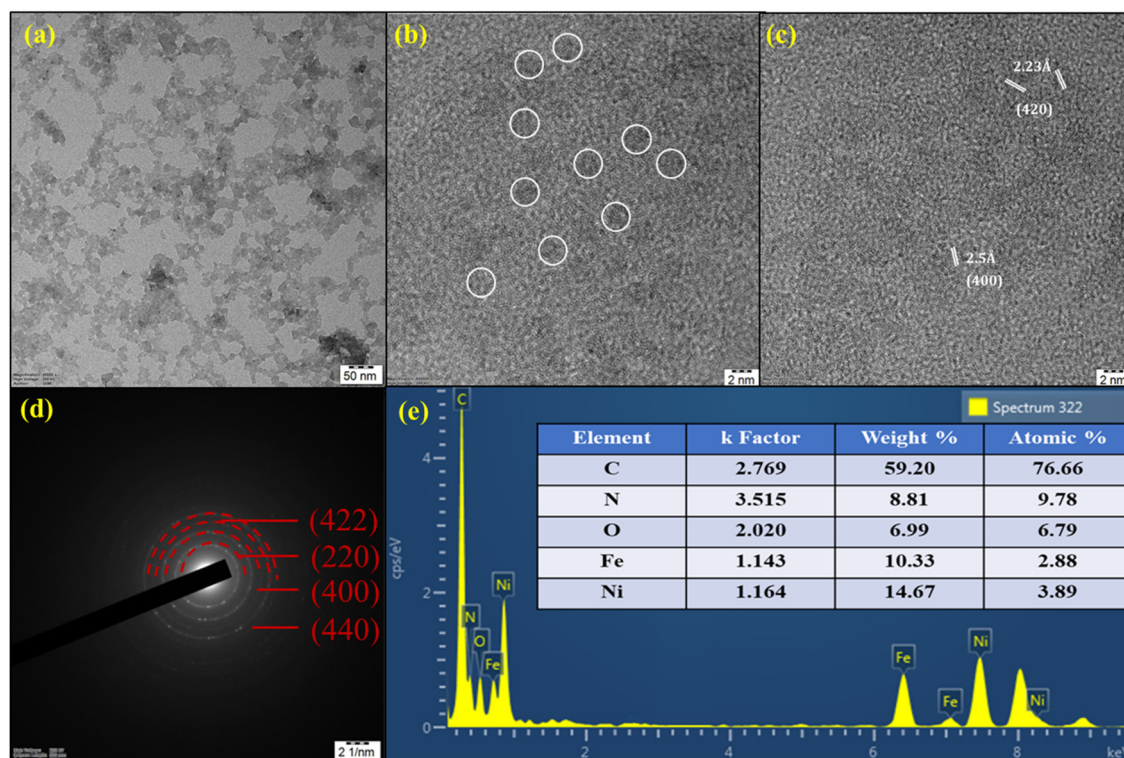


Fig. 4 HR-TEM images of NiFeHCF@NF (a and b); lattice fringes (c); SAED pattern (d) and EDX spectrum (e).

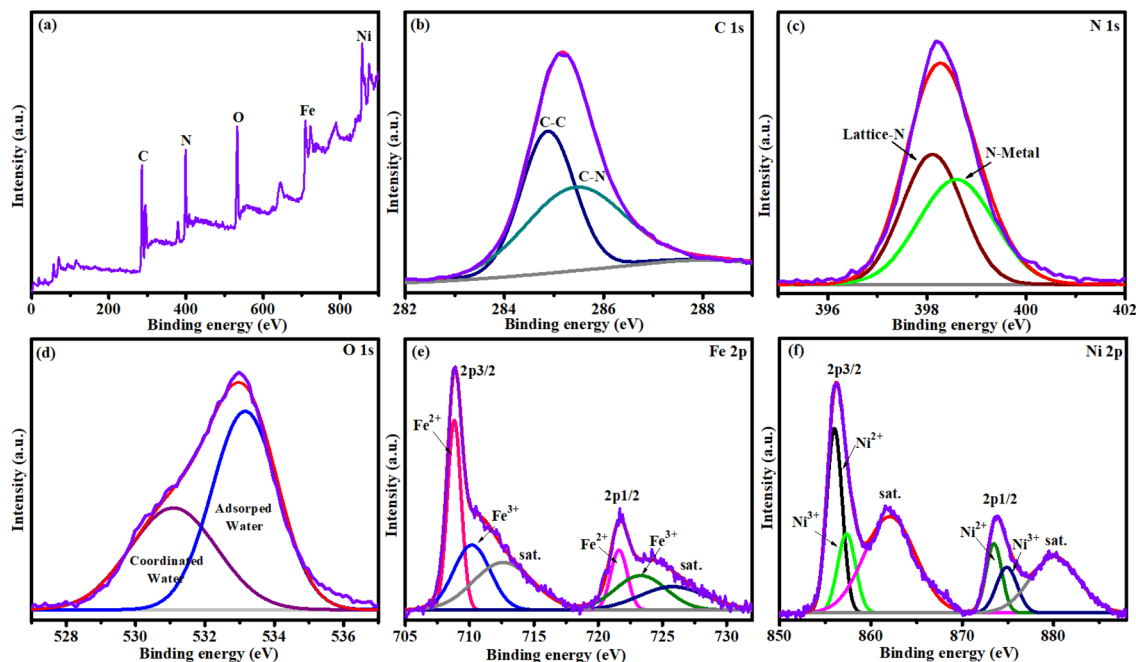


Fig. 5 XPS of NiFeHCF@NF: (a) XPS survey; (b) carbon; (c) nitrogen; (d) oxygen; (e) iron; and (f) nickel.

712.5 eV attributed to  $\text{Fe}^{2+}$ ,  $\text{Fe}^{3+}$  and satellite peaks of  $\text{Fe } 2p_{3/2}$  signals, respectively, and peaks at 721.6, 723.3 and 725.8 eV assigned to  $\text{Fe}^{2+}$ ,  $\text{Fe}^{3+}$  and satellite peaks of  $\text{Fe } 2p_{1/2}$  signals, respectively (Fig. 5e).<sup>37</sup> High-resolution spectra of  $\text{Ni } 2p$  (Fig. 5f) having peaks at  $\sim 856.0$  eV ( $\text{Ni } 2p_{3/2}$ ) and  $\sim 873.9$  eV ( $\text{Ni } 2p_{1/2}$ ) and the coexistence of  $\text{Ni}^{3+}$  and  $\text{Ni}^{2+}$  were confirmed by the binding energy (17.9 eV) difference between the two peaks. Furthermore, it can be fitted into shakeup satellites and spin-orbit doublets using the Gaussian fitting method. The peaks at  $\sim 855.9$ ,  $\sim 873.4$  and the satellite at  $\sim 862.1$  eV corresponded to  $\text{Ni}^{2+}$  and those at  $\sim 857.4$ ,  $\sim 874.8$  and the satellite at  $\sim 879.9$  eV were assigned to  $\text{Ni}^{3+}$ .<sup>38</sup> Thus, the XPS conclusion further confirmed the formation of NiFeHCF@NF.

### 3.1. Electrochemical characterization

The exact half-cell potential of NiFeHCF@NF was investigated by using a three-electrode setup in 1.0 M KOH. The overpotential of electrocatalysts was calculated by LSV in the potential range of 1.1–1.8 V. The overpotentials of FeNiLDH@NF,  $\text{IrO}_2$ , NiFeHCF@NF, NiHCF@NF, FeHCF@NF, HCF@NF and bare NF@10  $\text{mA cm}^{-2}$  are of 230, 341, 210, 290, 330, 370 and 481 mV, respectively (Fig. 6a and b). Compared to FeNiLDH@NF (64  $\text{mV dec}^{-1}$ ),  $\text{IrO}_2$  (98  $\text{mV dec}^{-1}$ ), NiHCF@NF (85  $\text{mV dec}^{-1}$ ), FeHCF@NF (93  $\text{mV dec}^{-1}$ ), HCF@NF (128  $\text{mV dec}^{-1}$ ) and bare NF (150  $\text{mV dec}^{-1}$ ), NiFeHCF@NF showed the smallest Tafel slope (56  $\text{mV dec}^{-1}$ ) (Fig. 6c). The long-term durability of a catalytic electrode is another crucial issue for industrial purposes, particularly for these types of porous nanostructured electrocatalysts. The stability of NiFeHCF@NF shows negligible degradation (<2 and <3.5%)@10 and 100  $\text{mA cm}^{-2}$ , respectively, after 150 h of testing, revealing its excellent

stability (Fig. 6d and S5a†). The OER efficiencies of NiFeHCF@NF electrocatalysts prepared *via in situ* self-assembly and co-precipitation have been compared with that of bare NF and required overpotential values of 210, 270 and 481 mV, respectively, to attain 10  $\text{mA cm}^{-2}$  (Fig. S6a†). This was ascribed to the tight binding between the active material and the substrate, evidence for which was revealed by movie S1† and post-use OER FESEM (Fig. 10a–c). The turnover frequency (TOF) of NiFeLDH@NF (0.1183  $\text{s}^{-1}$ ),  $\text{IrO}_2$  (0.0236  $\text{s}^{-1}$ ), NiFeHCF@NF (0.2738  $\text{s}^{-1}$ ), NiHCF@NF (0.0578  $\text{s}^{-1}$ ), FeHCF@NF (0.0324  $\text{s}^{-1}$ ), HCF@NF (0.0135  $\text{s}^{-1}$ ) and NF (0.0029  $\text{s}^{-1}$ ) was measured at 1.6 V. The benefits afforded by the 3D architecture were confirmed by the high performance and durability of NiFeHCF@NF. Combining the above merits, the 3D NiFeHCF@NF electrode was the most active non-precious 3D metal electrocatalyst (Table S2†).

The general OER mechanism followed by the electrocatalyst (NiFeHCF@NF) is:  $\text{M}^* + \text{OH}^- \rightarrow \text{M-OH}^* + \text{e}^-$ ;  $\text{M-OH}^* + \text{OH}^- \rightarrow \text{M-O}^* + \text{H}_2\text{O} + \text{e}^-$ ;  $\text{M-O}^* + \text{OH}^- \rightarrow \text{M-OOH}^* + \text{e}^-$ ;  $\text{M-OOH}^* + \text{OH}^- \rightarrow \text{O}_2 + \text{H}_2\text{O} + \text{e}^-$ . The excellent activity of NiFeHCF@NF was mainly derived from nickel in comparison with iron. During the OER process, Fe ions present as  $\text{Fe}^{2+}/\text{Fe}^{3+}$  [ $\text{Fe}(\text{OH})_2/\text{FeOOH}$ ] and Ni ions present as  $\text{Ni}^{2+}/\text{Ni}^{3+}$  [ $\text{Ni}(\text{OH})_2/\text{NiOOH}$ ] oxidation states were confirmed by post-use XPS results. The formed FeOOH optimized the electrons of nickel and assisted the development of active  $\text{Ni}(\text{OH})_2/\text{NiOOH}$  species, which are the active sites for the OER process. The outstanding durability and active sites during the OER of NiFeHCF@NF were also established by *ex situ* IR, XRD, SEM and XPS analyses. Both XRD and XPS results changed after the durability test, which confirmed the establishment of  $\text{Ni}(\text{Fe})\text{OOH}$  and  $\text{Ni}(\text{Fe})(\text{OH})_2$

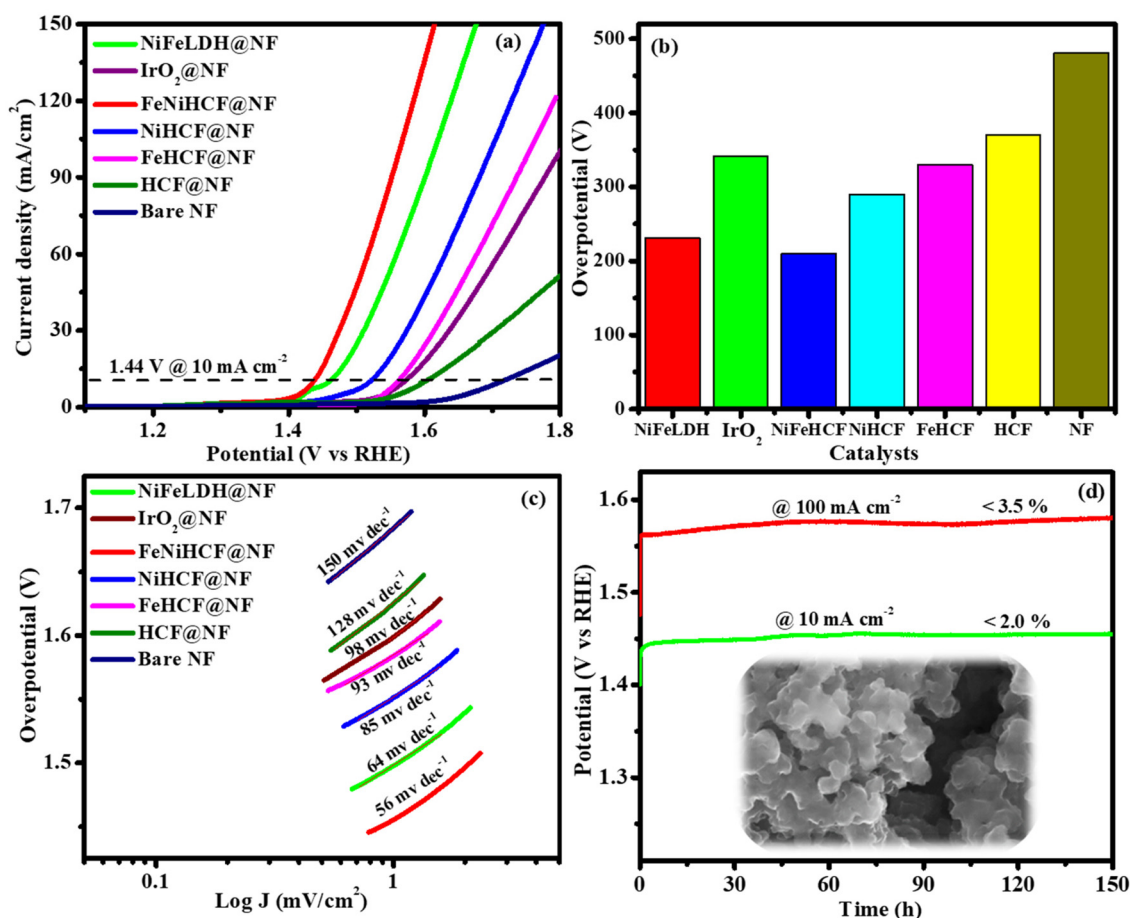


Fig. 6 OER polarization curves (without *iR*-correction) of electrocatalysts: (a) LSV curve; (b) overpotential@10 mA cm<sup>-2</sup>; (c) Tafel slopes; and (d) the chronopotentiometry durability test (inset: post-use OER image).

as catalytic sites. Similarly, the SEM images revealed the well-preserved morphology with an amorphous layer after the OER.<sup>26,39–42</sup>

The half-cell potential of Pt/C, NiFeHCF@NF, NiHCF@NF, FeHCF@NF, HCF@NF and bare NF for the HER activity was studied by LSV (without *iR* correction) in a three-electrode system. The LSV was spotted in the potential range of  $-0.4$ – $0.1$  V in 1 M KOH. The LSV and Tafel slope revealed that NiFeHCF@NF has lower overpotential (125 mV) and Tafel value (80 mV dec<sup>-1</sup>) than those of NiHCF@NF (200 mV; 99 mV dec<sup>-1</sup>), FeHCF@NF (265 mV; 117 mV dec<sup>-1</sup>), HCF@NF (295 mV; 126 mV dec<sup>-1</sup>) and bare NF (318 mV; 150 mV dec<sup>-1</sup>). Although Pt/C has lower overpotential (51 mV) and Tafel slope (62 mV dec<sup>-1</sup>) than NiFeHCF@NF, NiFeHCF@NF shows outstanding activity@ $-10$  mA cm<sup>-2</sup> compared to the recently stated non-precious metal electrocatalysts (Table S2†). The lower overpotential and Tafel value reveal the fabulous activity and fast kinetics of NiFeHCF@NF (Fig. 7a–c). The calculated TOFs at  $-0.2$  V of 0.1206 s<sup>-1</sup> (NiFeHCF@NF), 0.0259 s<sup>-1</sup> (NiHCF@NF), 0.0097 s<sup>-1</sup> (FeHCF@NF), 0.0071 s<sup>-1</sup> (HCF@NF), 0.1496 s<sup>-1</sup> (Pt/C) and 0.0067 s<sup>-1</sup> (NF) show the extraordinary HER activity of NiFeHCF@NF over a definite period. The

NiFeHCF@NF shows constant activity and outstanding stability over 150 h@10 and 100 mA cm<sup>-2</sup> with 2.2% and 4.6% potential loss, respectively (Fig. 7d and S5b†).

In alkaline electrolytes, the overall HER mechanism followed by the NiFeHCF@NF electrocatalyst may be Volmer–Heyrovsky:  $[M_{\text{cat}} + e^- + H_2O \rightleftharpoons OH^- + M_{\text{cat}}H_{\text{chem}}$  (Volmer);  $M_{\text{cat}}H_{\text{chem}} + e^- + H_2O \rightleftharpoons H_2\uparrow + OH^- + M_{\text{cat}}$  (Heyrovsky)].<sup>40</sup> The HER efficiencies of NiFeHCF@NF electrocatalysts prepared *via in situ* self-assembly and co-precipitation have been compared with bare NF and required overpotentials of 125, 162 and 318 mV, respectively to attain  $-10$  mA cm<sup>-2</sup> (Fig. S6b†). The establishment of Ni(Fe)(OH)<sub>2</sub> on the surface of NiFeHCF@NF may serve as the catalytic site for the HER, which was supported by the post-use analysis (Fig. 10 and 11).<sup>26,33,43–45</sup>

The comparison of OER/HER activity of NiFeHCF@NF, NiHCF@NF, FeHCF@NF and HCF@NF confirms that the excellent activity of NiFeHCF@NF may be due to the synergism of Ni and Fe in the composite. Specifically, the electron redistribution between iron, nickel and ferrocyanide was regulated and optimized the adsorption energy of OER/HER reaction intermediates. Owing to the merits of higher electrical conductivity, more surface-active sites and higher oxidation states of

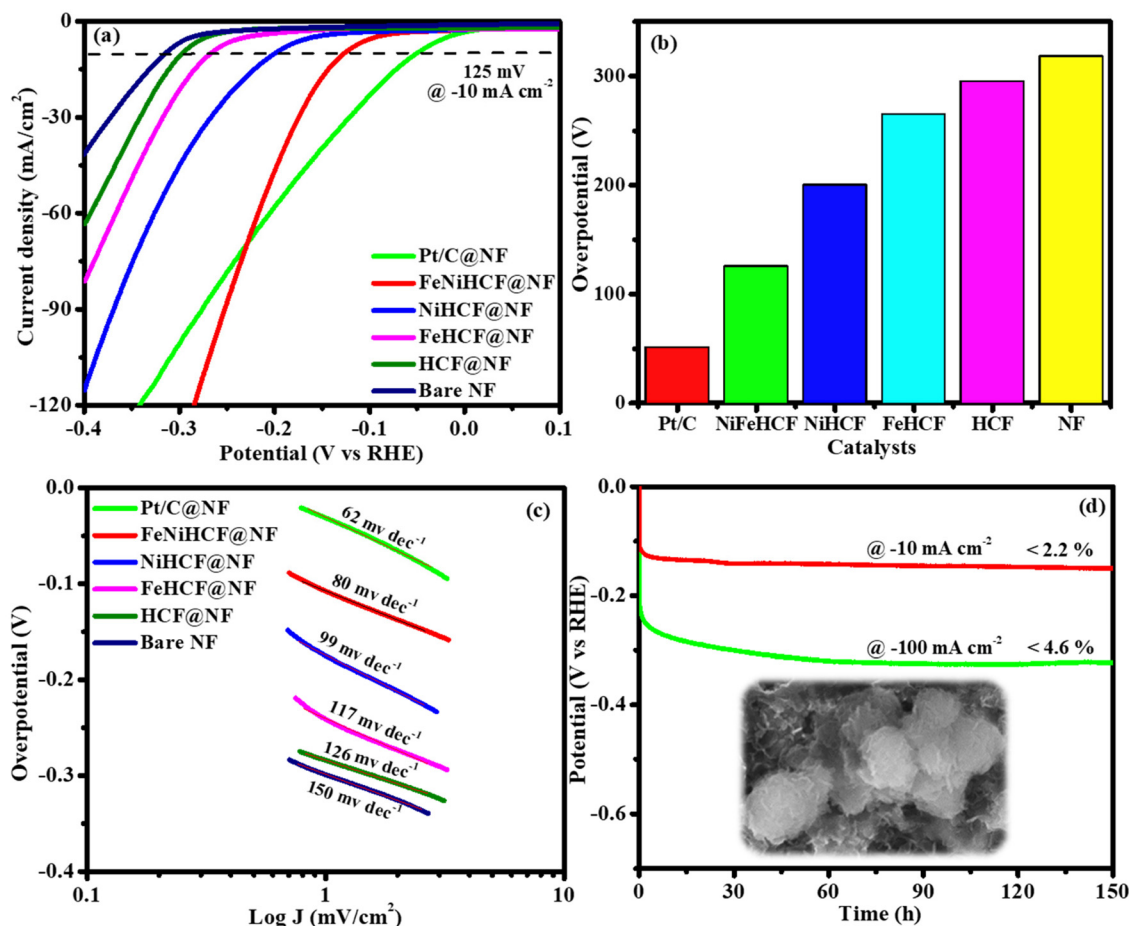


Fig. 7 HER polarization curves (without  $iR$ -correction) of electrocatalysts: (a) LSV curve; (b) overpotential@ $-10 \text{ mA}/\text{cm}^2$ ; (c) Tafel slopes; and (d) the chronopotentiometry durability test (inset: post-use HER image).

ions, NiFeHCF@NF exhibited excellent OER/HER catalytic performance. Specifically, ultralow overpotential within the large current density region, small Tafel value and consistent stability were included. Current research exposed the observations that iron addition not only caused optimal adsorption energy of intermediates but also induced the partial charge transfer to Ni sites to provide improved electrocatalytic performance.<sup>11,31,45–49</sup>

Additionally, to reveal the influence of the electrochemically active surface area (EASA) and structure–activity relationship, we calculated the double-layer capacitance by conducting cyclic voltammogram (CV) tests on the electrodes. CV curves have been produced at various scan rates of  $10\text{--}60 \text{ mV s}^{-1}$  within a range of  $1.20\text{--}1.30 \text{ V}$  vs. RHE, regardless of evident faradaic activities. NiFeHCF@NF exhibits significantly larger linear slope when the current density difference ( $\Delta j$ ) at  $1.25 \text{ V}$  vs. RHE is plotted *versus* the scan rate (Fig. 8a); a greater  $C_{dl}$  of  $5.745 \text{ mF cm}^{-2}$  was observed as related to that of the bare NF substrate ( $1.617 \text{ mF cm}^{-2}$ ). NiFeHCF@NF has 3.5 times greater capacitance than bare NF, which may be ascribed to its porous nanostructure.<sup>21</sup> The larger capacitance of NiFeHCF@NF compared to Ni foam indicates the large surface area of the

catalyst. The large EASA ( $143.6$ ) and RF ( $574.5$ ) values of NiFeHCF@NF over those of bare NF (EASA -  $40.4$  and RF -  $161.7$ ) confirmed the large electrochemical surface area of NiFeHCF@NF. To ensure the intrinsic activity of the NiFeHCF@NF catalyst, its EASA-normalized LSV curve was analysed (Fig. S7†). The overpotential needed for a current density of  $0.1 \text{ mA}/\text{cm}^2$  was  $227 \text{ mV}$  for NiFeHCF@NF, confirming its higher intrinsic activity. The higher OER activity of NiFeHCF@NF is not only due to the larger EASA but also due to the enhanced intrinsic activity of the catalyst as a result of the optimised electronic structure.<sup>13,50</sup> The hierarchical nature offered copious catalytic sites, which facilitated electrolyte infiltration and assisted fast charge and mass transportation and contributed to the extraordinary activity for the OER and HER.<sup>18,19</sup>

Electrochemical impedance results are depicted in Fig. 8b accompanied by circuit model fitting analysis (inset: Randles equivalent circuit diagram, where  $Q_1$  and  $Q_2$  denote the double-layer capacitance;  $R_1$  and  $R_2$  denote the charge transfer resistance and  $R_s$  denotes the electrolyte resistance). The smaller  $R_{ct}$  of NiFeHCF@NF ( $2.5 \Omega$ ) than that of NiHCF@NF ( $3.9 \Omega$ ), FeHCF@NF ( $4.2 \Omega$ ), HCF@NF ( $4.6 \Omega$ ) and bare NF



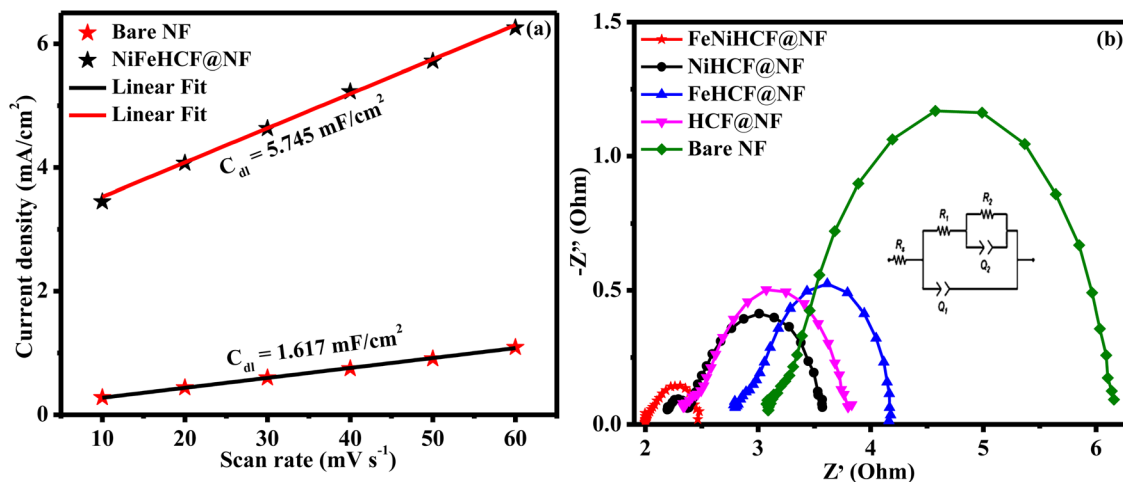


Fig. 8 The double-layer capacitance (a) and the Nyquist plot (b) of different electrocatalysts.

( $6.4 \Omega$ ) may be due to the strong contact between NiFeHCF and conductive nickel foam substrate, which offers a very active network for electron transfer throughout the electrode, resulting in rapid reaction kinetics. The different starting points of each electrocatalyst indicate internal resistance between the catalyst/electrolyte interfaces, and we observe that NiFeHCF has very low internal resistance compared to other electrocatalysts due to its intimate contact with the current collector.<sup>51,52</sup> The successful hierarchical self-assembly of NiFeHCF on the NF substrate further enables the synergism of various elements, which boosted both electron and mass transportation, promoted the conductivity and substantially assisted the electrochemical activity.<sup>49,53</sup>

Encouraged by the easy fabrication, high efficiency and durability of the NiFeHCF@NF electrode toward the OER and HER, we tested the possibility of utilizing it as the cathode and anode (NiFeHCF@NF||NiFeHCF@NF) in a two-electrode system. It was very clear to observe the evolution of  $\text{H}_2$  and  $\text{O}_2$

from the cathode and anode, respectively (Movie S1†). Fig. 9a shows the polarization curve of the NiFeHCF@NF||NiFeHCF@NF electrolyser in 1.0 M KOH. A cell voltage of only 1.56 V is needed for achieving  $10 \text{ mA cm}^{-2}$ , lower than the voltage required for benchmark electrolyzers, Pt/C/NF|| $\text{IrO}_2$ /NF (1.62 V) and bare NF||bare NF (1.81 V). The smaller cell voltage reveals that the 3D nano-structured NiFeHCF@NF utilized the advantage of iron, nickel and ferrocyanide components and produced excellent activity for overall water splitting.<sup>31</sup> The as-prepared NiFeHCF@NF electrodes achieved excellent bifunctional activity in 1 M KOH compared to that of recently reported Earth-abundant electrocatalysts (Table S2†). Additionally, we investigated the prolonged stability of the fabricated electrolyser, which was extremely excellent. A steady voltage had been preserved for over 150 h@ $10 \text{ mA cm}^{-2}$  and @ $100 \text{ mA cm}^{-2}$  (Fig. 9b and S5c†).

To further gain insights into the reaction mechanism, the NiFeHCF@NF electrode after the HER and OER was character-

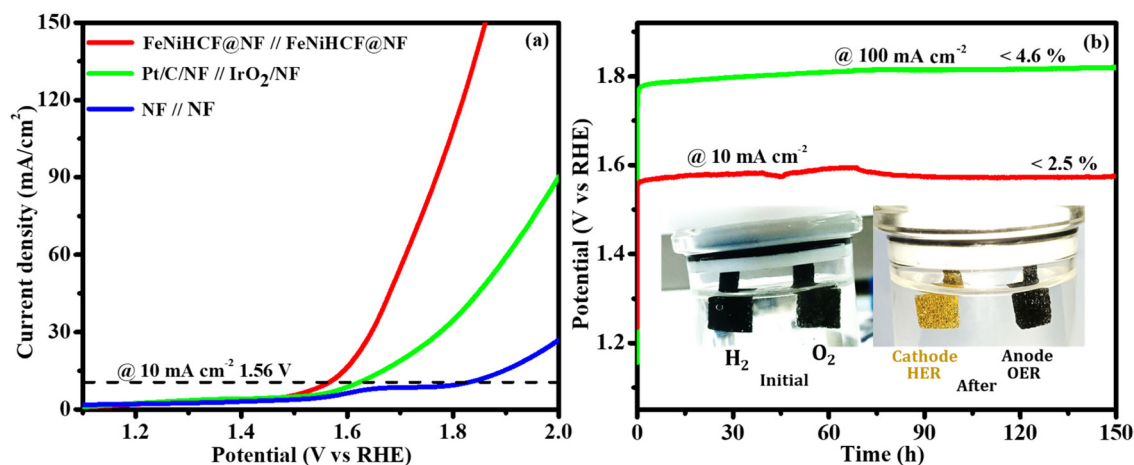


Fig. 9 (a) LSV polarization curve (without  $iR$ -correction) of NiFeHCF@NF for overall water splitting. (b) Chronopotentiometry durability test (inset: optical photograph of the electrodes).



ized by using FESEM, XRD, FT-IR and XPS analyses. Fig. S8a† presents the post-use XRD of NiFeHCF@NF after the HER process. The crystalline character of the catalyst remained constant and the additional peaks at  $19^\circ$ ,  $23^\circ$ ,  $34^\circ$ ,  $59^\circ$  and  $71^\circ$  are attributable to nickel hydroxide (JCPDS No. 14-0117). Fig. S8b† demonstrates an amorphous nature after the OER analysis with peaks marked “#” denoting the nickel foam substrate (JCPDS No. 87-0712). This may be related to the development of amorphous FeOOH and NiOOH during the OER.  $\text{Fe}^{3+}$  and  $\text{Ni}^{3+}$  boosted the electrophilicity of adsorbed oxygen, which is predominantly beneficial for the OER. The results are consistent with post-use XPS findings (Fig. 11).<sup>43,48,54</sup>

The post-use HER-IR spectra of NiFeHCF@NF showed new peaks at  $\sim 890\text{ cm}^{-1}$  (M–OH) and  $\sim 1278.76\text{ cm}^{-1}$  belonging to NiFe(OH), which support the formation of metal hydroxides after the HER (Fig. S9a†). The  $\text{Fe}^{2+}$ –CN– $\text{Ni}^{2+}$  peak at  $2087\text{ cm}^{-1}$  was retained after the HER. The peaks at  $\sim 1356$ ,  $\sim 1635$  and  $\sim 3000\text{--}3500\text{ cm}^{-1}$  are attributed to bending, stretching and scissoring of OH, respectively. The post-use OER-IR spectra of NiFeHCF@NF showed a new peak at  $677.36\text{ cm}^{-1}$  ascribed to FeOOH (Fig. S9b†). The peak intensity at  $2087\text{ cm}^{-1}$  was greatly reduced after the OER process. According to post-use IR analyses, the surface of NiFeHCF@NF was enriched with hydroxides (during the HER) and hydroxides/oxyhydroxides (during the OER), these being the electrocatalytically active phases, which is corroborated by the post-use XPS and XRD results.<sup>55–57</sup>

The post-use FESEM images of NiFeHCF@NF show that the surface of the coral-like structure becomes smooth after the OER process, and it is this that supports the formation of metal oxyhydroxide during the OER process (Fig. 10a–c).<sup>58</sup> This agrees with both post-use XRD and post-use XPS findings.

EDX elemental mapping confirmed the homogeneous distribution of component elements and the presence of constituent elements after 150 h of stability testing (Fig. S10 and S11†). The absence of other elements shows the purity of NiFeHCF@NF, which has atomic percentages of 27.13% (C), 2.80% (N), 52.14% (O), 16.61% (Ni) and 1.32% (Fe) after the OER (Fig. S10g†). The increment of oxygen in the EDX mapping and the smooth surface confirm the formation of oxyhydroxide during the OER process. Fig. 10d–f shows the morphology change from coral to nanosheet after the HER process, which supports the formation of metal hydroxides during the HER process. After the HER process, NiFeHCF@NF has the atomic percentages of 23.92% (C), 3.61% (N), 50.91% (O), 19.73% (Ni) and 1.83% (Fe) (Fig. S11g†). Movie S1† confirmed the good adhesion of electrocatalyst on the nickel foam surface. The higher stability even after 150 h with vigorous  $\text{H}_2/\text{O}_2$  gas evolution shows the ultra-sustainability of NiFeHCF@NF. Detachment of the catalyst from the electrode could be the major cause of its faster activity loss. Hence, post-use FESEM analysis and movie S1† confirmed the good adhesion of the electrocatalyst with NF. Comparison of morphology and colour changes of electrocatalyst before and after the OER and HER processes confirmed the development of hydroxides and oxyhydroxides after the HER and OER, respectively (Fig. S1 and S2†). The surface of NiFeHCF@NF was enriched with hydroxides (during the HER) and hydroxides/oxyhydroxides (during the OER), which were transformed from pristine NiFeHCF@NF.<sup>25,26,43</sup>

Post-use XPS was carried out to validate the change of oxidation state and composition after the electrocatalytic performance. However, the surface oxidation state and composition of NiFeHCF@NF were changed substantially after long-

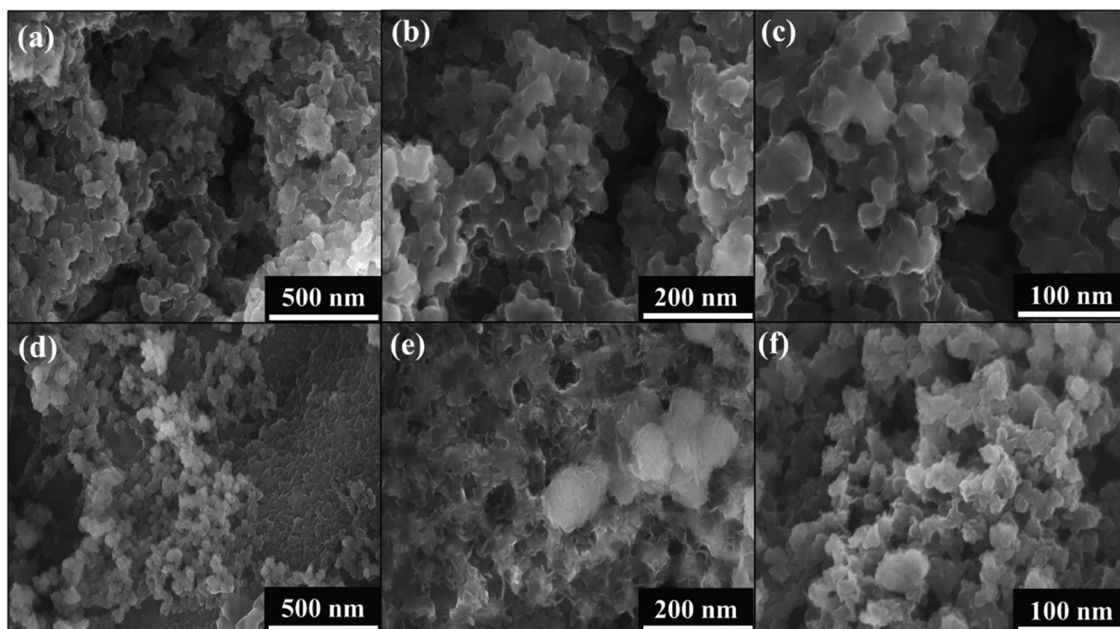


Fig. 10 Post-use FE-SEM image of NiFeHCF@NF; after the OER (a–c) and after the HER (d–f).

term electrocatalytic performance. Compared with the HER operating in a reducing potential environment, the strong anodic oxidation in the OER potential range leads to an evident and irreversible phase transformation of metal ferrocyanide to metal oxide/oxyhydroxide. Here, post-use XRD and FESEM characterization also suggested that the main crystalline phase and morphology of NiFeHCF@NF were changed after long-term OER/HER measurement.

For better understanding, XPS results of post-use OER and HER have together been compared. The post-use OER and HER Ni 2p spectrum revealed that the peak position was the same as that of the pristine electrocatalyst but the domination of peak intensity played an important role (Fig. 11c and f). The peaks at  $\sim 855.9$ ,  $\sim 873.4$  eV and the satellite peak at  $\sim 862.1$  eV corresponded to  $\text{Ni}^{2+}$  and those at  $\sim 857.4$ ,  $\sim 874.8$  eV and the satellite peak at  $\sim 879.9$  eV were attributed to  $\text{Ni}^{3+}$ . An evident shape change was found on the nickel spectrum in which the main peak of  $\text{Ni}^{3+}/\text{Ni}^{2+}$  accounted for 89% due to surface oxidation/reduction during the OER/HER process, which confirms the formation of  $\text{NiOOH}$  and  $\text{Ni}(\text{OH})_2$  layers during the OER/HER process.<sup>38</sup> Fig. 11a and d shows the post-use oxygen XPS spectrum, where new peaks at 529.4, 530.7 and 531.7 eV are ascribed to M-OOH, Ni(Fe)-O and M-OH, respectively, while the new peak at 531.7 eV belongs to M-OH after the OER. The peak intensity of absorbed water at 533.0 eV was reduced after the HER process.<sup>26</sup> As shown in the Fe 2p spectrum, two resolved peaks at  $2p_{3/2}$  (713.5 eV) and  $2p_{1/2}$  (725.7 eV) and the satellite peak of  $2p_{3/2}$  at 719.9 eV indicated the presence of iron as  $\text{Fe}^{3+}$  after the OER process (Fig. 11b).<sup>53</sup> The signal that disappeared at 708.8 eV indicates the conversion of iron to a higher oxidation state

after the OER process. The post-use HER Fe 2p spectrum showed two peaks at 708.5 and 721.6 eV for  $2p_{3/2}$  and  $2p_{1/2}$  of  $\text{Fe}^{2+}$  with satellite peaks at 712.5 and 725.8 eV, respectively (Fig. 11e), which is well consistent with the as-prepared catalyst and demonstrates the existence of  $\text{Fe}^{2+}$  after the HER process. These findings demonstrated that the surface of NiFeHCF@NF was enriched by the newly formed  $\text{Ni}(\text{Fe})\text{OOH}$  and  $\text{Ni}(\text{Fe})(\text{OH})_2$  layers after the OER/HER process, which have been regarded as the electrocatalytically active phases during the OER/HER process.<sup>26,56</sup>

The hierarchical NiFeHCF electrode displays highly efficient bifunctional catalytic activity for overall water splitting. The superior catalytic activity of NiFeHCF@NF is due to the following features: (1) close interaction of coral-like nanoparticles directly formed on a highly conductive 3D NF substrate not only enables full utilisation of the electrocatalyst active sites and efficient electron and mass transfer, but also avoids the need for polymer binders, which impart extra resistance;<sup>59</sup> (2) synergistic effect of two active metal sites *via* charge transfer;<sup>31</sup> (3) complete coverage of the pristine NF surface by NiFeHCF, which prevents corrosion and enhances the durability of the 3D structure;<sup>11</sup> (4) owing to the aggregation-free vertically grown coral nanostructure, the 3D electrode has a larger surface area compared to that of the bare current collector, suggesting a high density of active sites for the OER/HER;<sup>18</sup> (5) *in situ* growth on the metal foam substrate improved the structural stability and provided faster charge transfer as well as hydrogen/oxygen bubbles release;<sup>31</sup> and (6) the proposed synthetic procedure provides high reproducibility in terms of both catalytic activity and operational stability of the resulting material.

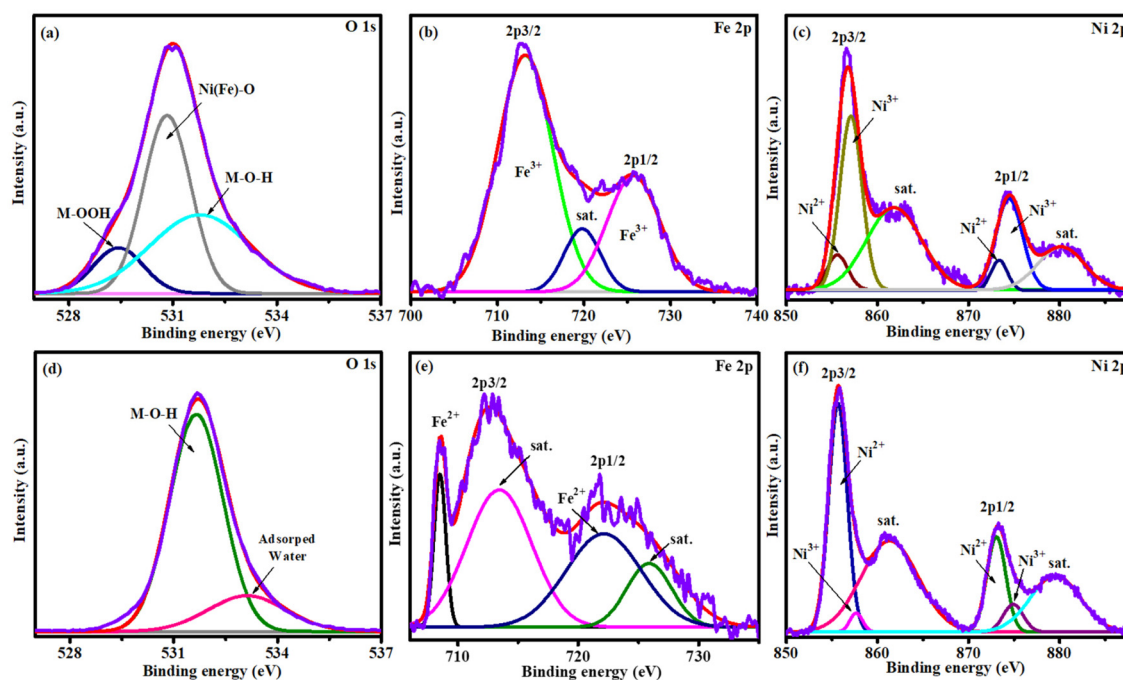


Fig. 11 Post-use OER-XPS spectra of (a) oxygen, (b) iron, (c) nickel, and post-use HER-XPS spectra of (d) oxygen, (e) iron, and (f) nickel.

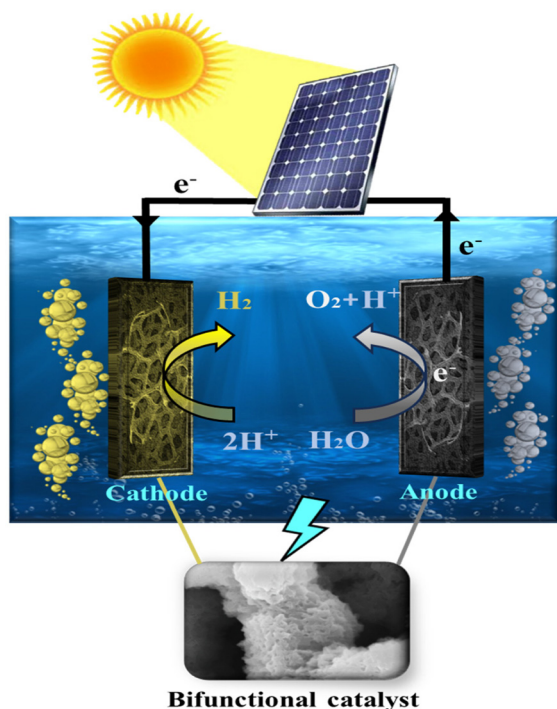


Fig. 12 Schematic diagram of solar-assisted water splitting.

### 3.2. Solar-assisted water splitting

The production of hydrogen by solar-assisted water electrolysis has become an economical and sustainable method. Fig. 12 shows a schematic diagram of solar-assisted water splitting using the NiFeHCF@NF||NiFeHCF@NF water electrolyser. Solar energy is fed into the NiFeHCF@NF||NiFeHCF@NF water electrolyser to generate electricity. The electrodes, present in 1 M KOH, and the solar panel (5.63 V) are connected by using crocodile clips. The voltage of the water electrolyser is measured and adjusted using a voltmeter. The solar-based water electrolyser only requires 1.56 V to attain 10 mA cm<sup>-2</sup> with continuous evolution of H<sub>2</sub> and O<sub>2</sub> bubbles at the cathode and anode showing the effectiveness toward H<sub>2</sub> production (Fig. S12; Movie S2†). The amount of O<sub>2</sub> and H<sub>2</sub> generated by using NiFeHCF@NF||NiFeHCF@NF was 1.52 and 3.12 μmol min<sup>-1</sup>, respectively, which is equal to ~96.5% faradaic efficiency (Fig. S13†).<sup>60</sup> Therefore, the solar-based water electrolyser developed in the present work is highly advised for inexpensive large-scale H<sub>2</sub> generation.

### 3.3. Environmental impact assessment

The level of the greenness of NiFeHCF@NF and its synthetic process were evaluated quantitatively and qualitatively, utilising presently suggested technological development based on mass-relevant sustainability and socioeconomic elements are compared the environmental effect to past efforts (Table S3†). The corresponding calculations were performed by applying the equations specified in the ESI (SI-S5†).

**3.3.1. Raw materials.** NiFeHCF@NF was synthesised using the smallest quantities of Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, Fe(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O and K<sub>4</sub>[Fe(CN)<sub>6</sub>], then washed with water and ethanol, yielding a water intensity of 93.5 (minimum amount of water used). With a reaction mass efficiency (RME) of 74%, the mass intensity (excluding water) was determined to be 1.35 kg kg<sup>-1</sup>. The RME was enhanced by increasing the reactant mass and reducing the utilisation of excess reagents.

**3.3.2. Energy consumption.** The electrocatalysts were synthesised without using any electricity and dried in sunlight. In laboratory-scale synthesis, the energy intensity was calculated to be 0.00 kW h per kg of NiFeHCF@NF; however, it is possible to drastically reduce the energy intensity by increasing the manufacturing level.

**3.3.3. Resulting emission.** There are no dangerous byproducts identified in NiFeHCF@NF characterization. Since a minimal amount of H<sub>2</sub>O was utilised for washing, the determined environmental factor (0.5) indicates that almost no emission was produced and the unreacted salts collected after several washings may be recycled.

**3.3.4. Toxicity potential.** According to NFPA 704: standard system for the identification of hazards materials for emergency response guidelines, iron nitrates and potassium ferrocyanide are non-toxic while nickel nitrate is toxic to both humans and aquatic organisms. Potassium ferrocyanide is available on the market and used as a food additive (E 536) approved by the European Food Safety Authority (EFSA). The laboratory and industrialized process should be executed using quite basic preventative measures.<sup>61–66</sup>

**3.3.5. Disposal of waste.** The used nickel foam was ultimately cleaned off by a reputable waste disposal company. The nickel foam with used catalyst was dispersed in a combustible solvent and burned in a scrubber and afterburner-equipped chemical incinerator.

**3.3.6. Affordability.** Due to the environmentally friendly green synthesis of the sustainable NiFeHCF@NF electrocatalyst, the demonstration of the solar-assisted water-splitting set-up in the current study provided the opportunity to push it for hydrogen production in the water-splitting company, which is both economical and effective.

**3.3.7. Social acceptability.** The current sustainable method for producing NiFeHCF@NF is affordable, easy to use, acceptable as a consumer product and generates clean H<sub>2</sub> with substantial positive social effects. Because the proposed set-up does not need highly skilled employees for both installation and maintenance, it is very suitable for the water-splitting industry. Here, we synthesised nickel-iron hexacyanoferrate on NF (NiFeHCF@NF) using a simple *in situ* self-assembly approach at room temperature without the use of additional energy.

## 4. Conclusion

In summary, a binder-free bifunctional electrocatalyst with a 3D hierarchical nanostructure of NiFeHCF on NF has been syn-



thesised *via* a simple *in situ* growth strategy. The results showed that the NiFeHCF@NF was effectively coupled with robust electronic interaction leading to facilitated charge transfer as well as enhanced reaction kinetics. The enhanced activity of the bifunctional NiFeHCF@NF electrocatalyst was determined by its low overpotential of 210/125 mV@10 mA cm<sup>-2</sup> without *iR* correction for the OER/HER, respectively. An NiFeHCF@NF couple as a water electrolyzer requires 1.56 V to attain 10 mA cm<sup>-2</sup> with a durability of 150 h. The solar-based water electrolyser requires 1.56 V@10 mA cm<sup>-2</sup>. The environmental impact assessments and solar-based water electrolysis respectively confirmed the greenness and effectiveness of NiFeHCF@NF. Hence, NiFeHCF@NF is a potential electrode for industrial hydrogen production.

## Conflicts of interest

The authors have no conflicts of interest to declare.

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