

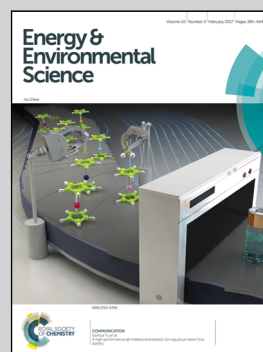


Showcasing research from Dr Pierre Ceccaldi and Prof. Sean Elliott at Boston University, U.S.A., and the group of Prof. Volker Müller at Johann Wolfgang Goethe University, Germany.

The hydrogen dependent CO₂ reductase: the first completely CO tolerant FeFe-hydrogenase

The hydrogen dependent CO₂ reductase (HDCR) enzyme complex found in *Acetobacterium woodii* reversibly couples hydrogen oxidation and the reduction of carbon dioxide. We found that HDCR rapidly and robustly recovers its activity after exposure to the inhibitor carbon monoxide, making HDCR the first 'syngas-friendly' hydrogenase catalyst.

As featured in:



See Sean J. Elliott et al.,
Energy Environ. Sci., 2017, 10, 503.



Cite this: *Energy Environ. Sci.*,
2017, 10, 503

Received 26th August 2016,
Accepted 24th October 2016

DOI: 10.1039/c6ee02494g

www.rsc.org/ees

The Hydrogen Dependent Carbon dioxide Reductase (HDCR) from *Acetobacterium woodii* presents a promising solution to the issue of H₂ storage by reversibly coupling H₂ oxidation to CO₂ reduction. We here report on the electrocatalytic properties of the hydrogenase (Hase) module in the intact complex, including (an)aerobic oxidation, CO inhibition and the first systematic analysis of the catalytic bias (CB) of a Hase. CB depends on pH, regardless of the H₂ concentration, despite a higher affinity for H₂ than other FeFe-Hases. Remarkably, CO inhibition is fully reversible under all oxidation states of the active site, making HDCR the first “syngas-friendly” FeFe-Hase.

The consideration of dihydrogen (H₂) as a potential new energy vector requires balancing the issue of gas storage and the possibility of an explosive hazard. Carbon dioxide (CO₂) has been considered as an H₂ storage unit through formic acid or formate:¹ a concept used by acetogenic bacteria that can grow on H₂ and CO₂ only, thus using H₂ and CO₂ as energy and carbon source, respectively, through the Wood–Ljungdahl pathway (WLP) in *Acetobacterium woodii* (ref. 2, 3 and references therein). The methyl branch of WLP starts with the four-subunit Hydrogen Dependent Carbon dioxide Reductase (HDCR),² the object of the present study (Fig. 1). Two subunits contain one catalytic site each: FdhF2 houses a Mo-bisPGD cofactor⁴ that reduces CO₂ to formate, while the H₂-oxidizing H-cluster characteristic of FeFe-Hases⁵ is bound by HydA2. These two active sites are connected to one another *via* eleven predicted FeS clusters distributed between all four subunits. This direct and reversible intramolecular coupling of H₂ activation to

Broader context

Molecular hydrogen (H₂) has been considered as a clean energy source for several decades, yet a number of critical obstacles must be overcome to allow hydrogen to be widely usable. In particular, the extreme explosive hazard of H₂ prevents safe storage of large quantities, and one way chemists have sought to overcome this restriction is to transform H₂ into another chemical that would serve as a storage unit, such as formate. Here, we report on the mechanistic traits of the Hydrogen Dependent Carbon dioxide Reductase from *Acetobacterium woodii* (HDCR), an enzymatic system recently reported by our co-authors, that is capable of the direct interface between a FeFe hydrogenase and a CO₂ reductase.

CO₂ reduction in a soluble enzyme is, to the better of our knowledge, unique in nature (see ref. 6 for a more complex example that *a priori* catalyses the reverse reaction only). HDCR catalysis is currently enigmatic, as it is unclear how the two enzymatic activities are coupled to one another, and how each catalytic component can serve as a standalone, monofunctional enzyme. In solution, HDCR turns over H₂ 10² times faster than CO₂, thus accurate characterization of the HDCR Hase properties constitutes a required first-step to understand the electrochemical coupling between the two activities. Here, we use the lens of catalytic protein film electrochemistry (PFE) to examine HDCR for the

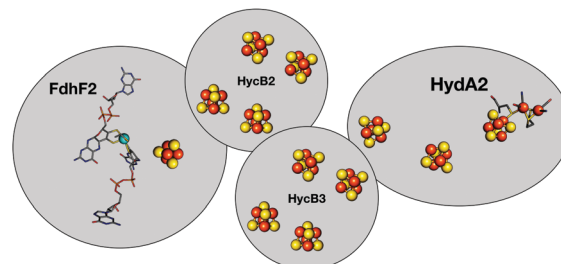


Fig. 1 Schematic representation of HDCR.² The formate dehydrogenase unit FdhF2 belongs to the bisPGD superfamily,⁴ and the HydA2 subunit is a typical FeFe-hydrogenase, with two FeS clusters besides the active site. Depicted cluster numbers and stoichiometries are predicted on the basis of amino acid sequence.

^a Department of Chemistry, Boston University, 590 Commonwealth Avenue, Massachusetts 02215, USA. E-mail: elliott@bu.edu

^b Molecular Microbiology and Bioenergetics, Institute of Molecular Biosciences, Johann Wolfgang Goethe University Frankfurt/Main, Max-von-Laue-Strasse 9, 60438 Frankfurt, Germany

† Electronic supplementary information (ESI) available: Methods. Comment on pH dependence of catalytic bias. Measure of H₂ concentration by chronopotentiometry. Supplementary figures. See DOI: 10.1039/c6ee02494g

‡ Present address: Center for Biomolecular Sciences, University of Nottingham, Nottingham, UK.



first time. PFE has been extensively used for examining complex activity features of Hases, such as catalytic bias,⁷ inhibition by the small molecules CO^{8,9} and O₂,^{10–12} as well as (in)activation processes.^{13–17} Here, we present the first electrochemical characterization of the intact HDCR complex, focusing on its Hase activity. We find that HDCR possesses the canonical properties of FeFe-Hases in terms of catalytic bias and oxidative inactivation, but reveals an unprecedented fully reversible inhibition by carbon monoxide.

Hases are reversible enzymes that catalyze H₂ oxidation as well as proton reduction,¹⁸ yet FeFe-Hases are typically biased for proton reduction, which manifests itself by displaying low affinity for H₂ ($K_M \sim 0.6$ atm and $K_i = 5\text{--}30$ atm)¹⁹ compared to NiFe-Hases that favor H₂ oxidation.^{8,20} We initially examined the Hase activity of HDCR, as it was unclear if the complex may be *a priori* biased toward H₂ evolution or oxidation. To do so, we defined the catalytic bias as the ratio of proton reduction and H₂ oxidation activity under given conditions of pH and H₂ pressure. Fig. 2 shows cyclic voltammograms (CVs) of a HDCR-coated rotating electrode, under 1 atm of H₂ between pH 5 and 8. The electrode potential was swept at 0.1 V s^{-1} to prevent any redox (in)activation process^{15,16} and to limit film-loss during the experiment. All CVs cross the zero current axis at the value of the $E_{\text{H}^+/\text{H}_2}^0$, as do all reversible hydrogenases. At pH 5 under 1 atm of H₂ and an overpotential of 0.25 V, HDCR reduces protons 10 times faster than it oxidizes H₂, thus revealing its bias towards proton reduction. That a FeFe-Hase favors proton reduction under acidic conditions is of no surprise (*e.g.* see Fig. 3 in ref. 8),

but as pH increases, the ratio between reductive and oxidative activity decreases.

To analyse the pH dependence of the bias of HDCR-Hase, we built on the conclusions from Léger and coworkers (see eqn (9) and Fig. 5 in ref. 21) that showed the proportionality between the maximum turn-over rate k_2 and the shape of the steady-state voltammogram.²² We thus consider the catalytic bias β as the ratio of the slopes for H₂ formation or oxidation at high driving-force (Fig. 2 inset). Values of β distribute along the black dash lines, of which the slope is 0.5. This suggests that the catalytic bias is directly proportional to $[\text{H}^+]^{0.5}$, with no apparent effect of $[\text{H}_2]$ on this behaviour. Lowering H₂ pressure at a given pH does increase β (*i.e.* the circles plot above the squares in the figure inset), but has no effect on its pH dependence (see ESI,† Section S2). We hope this first systematic study of catalytic bias under different thermodynamic conditions (pH and $[\text{H}_2]$) will inspire other groups to run comparable studies to thus arrive at an universal “fingerprint” of the catalytic bias of Hases.

H₂ either acts as a substrate or an inhibitor whether one considers the H₂ oxidation or evolution. Consequently, lowering H₂ pressure directly increases proton reduction and lowers H₂ oxidation activity. Because the electrochemical setup allows for measurement of the hydrogenase activity while varying the H₂ concentration in the cell, we measured the apparent affinity for H₂ in the case of H₂ oxidation (K_M) or evolution (K_i), using multi-step chronoamperometry. This consists of monitoring the activity over time at a fixed electrode potential on each potential step (Fig. 3). The H₂ pressure is varied by subsequently turning on and off its flow, thus inducing an exponential relaxation of $[\text{H}_2]$ in the electrochemical cell (panel A), which further results in a transient catalytic response (panel B, black trace). Under reductive conditions, the decrease of $[\text{H}_2]$ reversibly increases proton reduction current, and conversely decreases H₂ oxidation current. The H₂ oxidation current does not drop to zero when the H₂ stream is stopped, due to the presence of some H₂ remaining in the cell (black trace at $t \approx 1600$ s in Fig. 3B). This residual H₂ concentration can be measured independently through the monitoring of the open circuit potential, which shifts in accord with $[\text{H}_2]$ (Fig. S1 and Section S3, ESI†). To measure parameters K_i and K_M , we analysed the data using QSoas, an open-source program that permits quantitative analysis of one-dimensional signals.²³ We fitted the experimental data to the following equations:

$$i_{\text{H}_2 \text{ production}} = i([\text{H}_2] = 0)/(1 + [\text{H}_2]/K_i) \quad (1)$$

$$i_{\text{H}_2 \text{ oxidation}} = i([\text{H}_2] = \infty)/(1 + K_M/[\text{H}_2]) \quad (2)$$

respectively for the product inhibition of proton reduction, and for the Michaelis constant for H₂; the terms $i([\text{H}_2] = 0)$ and $i([\text{H}_2] = \infty)$ correspond to the maximum current for either proton reduction (inhibitor concentration is null) or H₂ oxidation activity (infinite substrate concentration), hence an equivalent of the catalytic constant k_{cat} . K_i (6.4 ± 1.3 atm) compares to the value of 7 atm reported for *Chlamydomonas reinhardtii* (Cr) FeFe-Hase, and is five times lower than the 26 atm value for

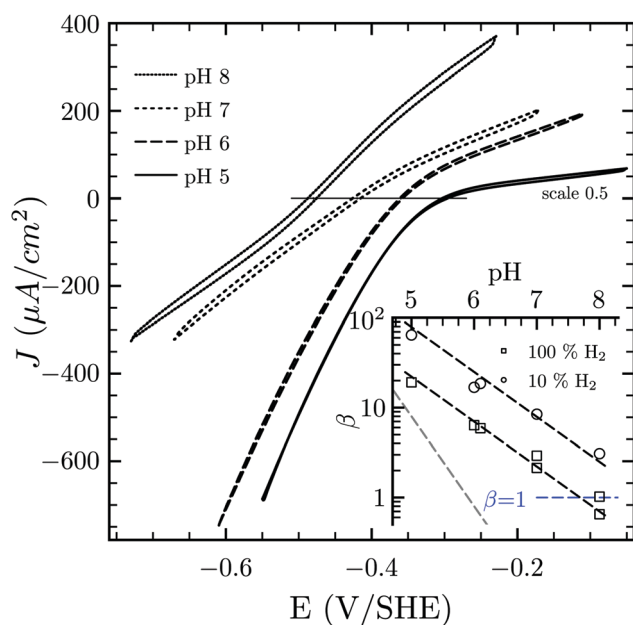


Fig. 2 Catalytic bias of the hydrogenase activity of HDCR. Cyclic voltammogram of HDCR adsorbed on pyrolytic graphite disk electrode ($\approx 3.1\text{ mm}^2$) at 30°C , pH 5, 6, 7 and 8 under 1 atm of H₂. Scan rate, 0.1 V s^{-1} ; $\omega = 3\text{ k rpm}$. The inset shows the pH dependence of β calculated as the ratio of the slopes of the voltammogram at high driving force^{21,22} (the dash lines follow the eqn (S1) (ESI†) with the slope $[\text{H}^+]^{0.5}$ in black and $[\text{H}^+]^1$ in grey for comparison).





Fig. 3 Measurement of K_I and K_M for H_2 at -560 and -160 mV per SHE, respectively. (A) H_2 concentration against time. (B) Current corrected for non-faradic contribution (black, note the small but constant decay in current in absolute values, due to film-loss), best fit to eqn (1) and (2) (red) and electrode potential (blue) against time. (C) Difference between the fit and the data. Best fit parameters to the eqn (1) and (2) returned $K_I = 6.1$ atm (the average of 3 measurements returned $K_I = 6.4 \pm 1.3$ atm) and $K_M = 0.26$ atm ($N = 3$, $K_M = 0.24 \pm 0.02$ atm), respectively. Experimental conditions: 30°C , pH 7, $\omega = 3\text{ k rpm}$.

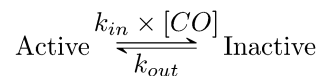
the *Clostridium acetobutylicum* (*Ca*) enzyme (Fig. 3 in ref. 19). The K_M for H_2 is 0.24 ± 0.02 atm, three times lower than the reported values for both *Cr* and *Ca* Hases.¹⁹ Overall, HDCR shows the highest apparent affinity for H_2 ever reported for a FeFe-Hase. Using the H_2 affinity as a proofreading of the catalytic bias, this could induce a lower bias to proton reduction than other FeFe-Hases, but it is not the case here. Given that H_2 diffuses to or from the active site during turnover,¹⁹ higher affinity for H_2 displayed by HDCR might be due to the shape of its substrate tunnel, albeit amino acid sequences of FeFe-Hases are strictly conserved along the putative gas tunnel (Fig. S2 and S3, ESI†).^{24–26} Moreover, even though the electron transfer relays in HycB are thought to be far away from the active site, this specificity of HDCR might be at play in its reactivity towards H_2 standing out of the dogma “proton bias/low H_2 affinity”.

FeFe-Hases are inhibited by carbon monoxide (CO), and HDCR is no exception. Schuchmann and Müller reported that CO inhibits HDCR hydrogenase activity: 50% of inhibition is observed at $0.2\ \mu\text{M}$ CO in the assay (see Figure S8 in ref. 2). Here, we examined the kinetics of CO inhibition of HDCR by monitoring its change in activity upon transient CO exposure (Fig. 4). The experiment consists in injecting a small volume of a CO-saturated buffer solution in the electrochemical cell, after which the inhibitor is flushed away by the constant H_2 flow (panel A).

Using QSoas²³ and the procedure introduced by Leroux and coworkers and since developed by our first author and



Fig. 4 CO and O_2 inhibition of H_2 oxidation activity of *A. woodii* HDCR at $+40$ mV per SHE. (A) CO (green) and O_2 (red) concentration against time. (B) Resulting current (black trace) and best fit of model 1 and 2 (green and red dashes, respectively). The best parameters of eqn (3) in ref. 27 to the CO inhibition (green trace) returned $k_{in} = 0.18 \pm 0.01\ \text{s}^{-1}\ \mu\text{M}^{-1}$ and $k_{out} = 0.02 \pm 0.001\ \text{s}^{-1}$; fitting the parameters of scheme to the aerobic inactivation returned $k_{in} = 4.8 \pm 0.4\ \text{s}^{-1}\ \text{mM}^{-1}$, $k_{out} = 5.5 \pm 1 \times 10^{-3}\ \text{s}^{-1}$ and $k_3 = 7 \pm 1.4 \times 10^{-3}\ \text{s}^{-1}$. (C) Difference between the fit and the data. Experimental conditions: pH 7, 1 atm H_2 , $T = 30^\circ\text{C}$, $\omega = 3\text{ k rpm}$.



Scheme 1 Kinetic model of CO inhibition of HDCR. CO binds with the bimolecular rate constant k_{in} and unbinds with the unimolecular rate constant k_{out} . Here, k_{in} is not corrected for protection by H_2 , thus should be considered an apparent rate constant.

others,^{9,27–29} we fitted the transients of CO exposure with the parameters of Scheme 1, which considers reversible CO binding to HDCR in a single rate limiting step. Fitting parameters are the maximal current, the two rate constants of CO binding and release, the time-constant at which CO is flushed out of the cell and film-loss (see ESI† text). As noted previously, K_I for CO will depend upon $[H_2]$ (here 1 atm), and thus k_{in} is an apparent rate constant. The best fit returned $k_{in} = 0.18 \pm 0.01\ \text{s}^{-1}\ \mu\text{M}^{-1}$ and $k_{out} = 0.02 \pm 0.005\ \text{s}^{-1}$, giving the inhibition constant $K_I^{\text{CO}} = 0.11 \pm 0.01\ \mu\text{M}$, thus three and ten times smaller than the reported values for the *Cr* and *Ca* FeFe-Hases⁹ obtained under the same conditions (pH 7, 1 atm H_2 , 30°C). This larger inhibition by CO of HDCR might appear as a disadvantage for use of HDCR-based catalysts to process CO-containing syngas, nonetheless this is counterbalanced, and we think overcome by the full reversibility of the inhibition (see below).

Three distinct redox states of the H-cluster have been identified by FTIR and EPR spectroscopy: H_{ox} and H_{red} differ by one electron and convert to one another at $E^{0'} = -0.4$ V per SHE at pH 8, as observed with *Cr* HydA1.^{30,31} Under turn-over conditions, CO reversibly binds to the H_{ox} and H_{red} states, the latter leading to the disruption of the active site.⁹ The “super-reduced”



state of the H-cluster (H_{sred}), one electron more reduced than H_{red} , appears at $E^{0'} = -0.47$ V per SHE³⁰ and seems less sensitive to CO than H_{red} , as it is generated upon reduction of the H_{red} -CO state.³¹ Here we used CO as a probe of the oxidation state of the HDCR H-cluster, attempting to detect the three intermediate states through their differential sensitivity to CO. We repeated experiments similar to the one presented in Fig. 4 with different values of E across a ≈ 600 mV potential range, and with sequential injections of varying CO concentrations in order to extend CO exposure of the HDCR film and detect a possible slow irreversible step following CO binding on H_{red} state^{9,32} (Fig. S4, ESI†).

The kinetic parameters of CO inhibition as a function of electrode potential are plotted in Fig. 5 (note the log scale on the y axis). Starting from the high potential values, the inactivation slows down when approaching $E_{H^+/H_2}^{0'}$, then accelerates upon further reduction. This trend is similar to *Ca* and *Cr* HydA⁹ and appears as indirect evidence of redox changes within the H-cluster. Fitting the redox dependences of k_{in}^{CO} and k_{out}^{CO} returned $E_{H_{ox/red}}^{0'} = -0.33$ V per SHE, and $E_{H_{red/sred}}^{0'} = -0.45$ V per SHE, similar to reported values.³¹

The most original feature of CO inhibition of HDCR is that the enzyme fully reactivates upon CO escape from the cell in all three oxidation states of the H-cluster. This observation is contrary to all PFE-based CO inhibition studies of FeFe-Hases to date, where CO binding to the H-cluster in the stability range of the H_{red} state provokes irreversible damage, assigned to the disruption of the bridge between the Fe_2 subcluster and the adjacent cubane.^{8,9,32} In the case of HDCR, we took great care to expose the enzyme to high concentrations of inhibitor (up to $50 \mu M \approx 500 \times K_i^{CO}$) so as to not miss an irreversible reaction of the CO-bound states (Fig. S4, ESI†). In the time scale of our experiments we only detected fully reversible inhibition, which could be simulated using the parameters of Scheme 1.



Fig. 5 Redox dependence of rate constants k_{in} and k_{out} from Scheme 1. The vertical lines mark the positions of the reduction potential of H^+/H_2 couple at pH 7 (red) and the redox transitions undergoing at the H-cluster according to ref. 31 (we assume $\Delta E_{H_{ox}/H_{red}}^0 = -60$ mV per pH unit).

In contrast, for *Ca* HydA1 the irreversible inhibition by CO is pronounced for concentrations much lower than the ones used here (see first transient in Fig. 1D and E in ref. 9), even though CO binds to the active site ≈ 75 times slower than in HDCR. Therefore if CO caused irreversible damage to HDCR, we would detect it.

Besides favoring proton reduction and being (up to the present work) sensitive to CO damage under certain conditions, FeFe-Hases also undergo oxidative (in)activation, with or without implication of O_2 . Fourmond and coworkers demonstrated that *Ca* and *Cr* FeFe-Hases produce three inactive species through anaerobic oxidation, two of which reactivate upon reduction.¹⁵ Such reactivatable oxidized states can be detected in CV experiments through the “ E_{switch} ” inflection point on the reductive scan, which corresponds to the potential at which reactivation becomes faster than scan rate.^{12,14,17} The CVs presented in Fig. 6 display one or two E_{switch} features depending on scan rate and temperature (Fig. S5, ESI†): HDCR anaerobic oxidation produces at least two species that reactivate upon reduction at different rates. The third, irreversibly inactivated species detected in previous studies¹⁵ could not be assigned here as this process combines with film-loss. Notably, these rates are approximately 100 times slower than in the case of previously reported enzymes.¹⁵

Finally Orain and coworkers demonstrated the partial reversibility of O_2 attack on the H-cluster,^{12,33} a mechanism firstly suggested by two groups^{8,11} that we here test and validate for HDCR. We studied the aerobic inactivation of HDCR by measuring the H_2 oxidation activity upon transient exposure to O_2 (Fig. 4 red traces). We chose to perform this study at $30^\circ C$ rather than at $12^\circ C$ as in ref. 12, in order to best report on the determination of the rates of the underlying anaerobic processes. When exposed to O_2 , HDCR inactivates more slowly

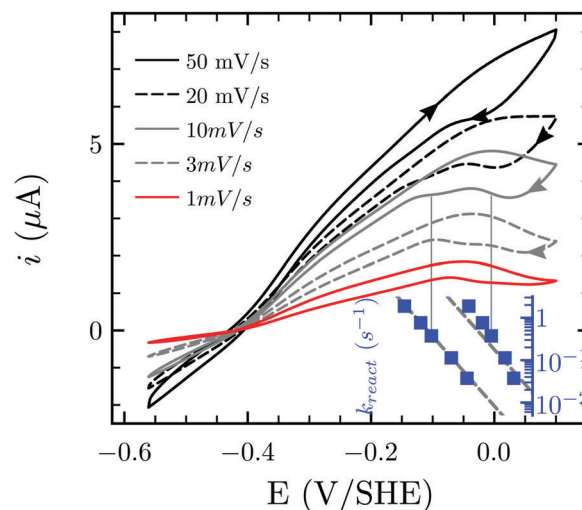
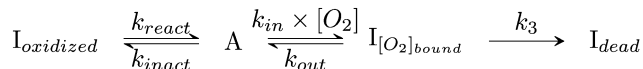


Fig. 6 Anaerobic oxidative inactivation measured by cyclic voltammetry. The position of the reactivation waves at high potential shifts to more reductive values at increasing scan rate. The inset shows (on the same x axis) the reactivation rate constant at the position of E_{switch} . Experimental conditions: $T = 30^\circ C$, pH 7.0, 1 atm H_2 , $\omega = 3$ k rpm.





Scheme 2 Kinetic model of aerobic inactivation of HDCR-Hase. The enzyme is in equilibrium between one active (A) and two inactive species, and I_{oxidized} is detected through the E_{switch} in Fig. 6. The unimolecular reaction following O_2 binding leads to the dead-end species I_{dead} .

Table 1 Kinetic parameters of CO and O_2 inhibition of HDCR at +40 mV per SHE, pH 7, 30 °C. The values are averaged from three independent measurements

I	k_{in} ($s^{-1} \text{ mM}^{-1}$)	k_{out} ($\times 10^{-3} s^{-1}$)	k_3 ($10^{-3} s^{-1}$)
CO	20 ± 3	25 ± 5	n.d.
O_2	6.5 ± 0.1	5.4 ± 0.1	3.2 ± 0.12

than with CO (note the inhibitor concentration plotted in the upper panel). Upon flushing O_2 from the cell, activity first increases before stabilizing at a lower level than before O_2 injection, suggesting that the aerobic inactivation occurs in two steps, only the second being irreversible. We fitted the data with the parameters of the kinetic model presented in Scheme 2,¹² by using the reactivation rate constant determined by the position of E_{switch} in CV ($0.038 s^{-1}$, inset Fig. 6). Analogously to the works of Orain and coworkers, the partial reversibility of the O_2 binding was necessary to satisfyingly reproduce the experimental traces, thus showing how HDCR reacts with O_2 .

The kinetic parameters of CO and O_2 inhibition are summarized in Table 1. Even though we have no direct experimental evidence that O_2 reacts with the active site, the likelihood with the works by Orain and coworkers strongly suggests that O_2 targets the Fe_2 subcluster. The reactivation step following oxygen binding (monomolecular rate k_{out}) was very recently shown not to be the simple, non redox unbinding of O_2 but rather its full reduction to water.²⁶ That HDCR-Hase active site is eventually destroyed upon O_2 exposure may prevent its applicability in industrial processes, but that is discarding recent developments in hydrogels as protective layers of oxygen sensitive catalysts.^{34–36}

At first glance, the entire HDCR complex displays a typical FeFe-Hase phenotype: it strongly favors proton reduction compared to NiFe-Hases, is inhibited by CO and O_2 , and produces two reversibly inactive species upon oxidation. Yet, CO inhibition is entirely reversible for HDCR (at least under the conditions we used here), which likely arises from specific structural properties that are yet to be deciphered. Thus, our results pave the way for a deeper investigation of the HDCR electrochemical behavior, and provide the essential underpinnings of future studies of HDCR reactivity towards CO_2 and formate. Our findings suggest that structural studies of HDCR will likely unlock the mystery of how to design a FeFe-Hase that remains undamaged by CO. Such CO tolerance of a FeFe-Hase, detected here for the first time, is of great value if one wants to use enzyme-based catalysts to process CO-containing syngas.

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