

Cite this: *RSC Adv.*, 2018, 8, 19818

Waste wool derived nitrogen-doped hierarchical porous carbon for selective CO₂ capture†

Yao Li,^{ac} Ran Xu,^a Xin Wang,^b Binbin Wang,^{id}*^b Jianliang Cao,^d Juan Yang*^{ac} and Jianping Wei*^{ac}

The goal of this research is to develop a low-cost porous carbon adsorbent for selective CO₂ capture. To obtain advanced adsorbents, it is critical to understand the synergetic effect of textural characteristics and surface functionality of the adsorbents for CO₂ capture performance. Herein, we report a sustainable and scalable bio-inspired fabrication of nitrogen-doped hierarchical porous carbon by employing KOH chemical activation of waste wool. The optimal sample possesses a large surface area and a hierarchical porous structure, and exhibits good CO₂ adsorption capacities of 2.78 mmol g⁻¹ and 3.72 mmol g⁻¹ at 25 °C and 0 °C, respectively, under 1 bar. Additionally, this sample also displays a moderate CO₂/N₂ selectivity, an appropriate CO₂ isosteric heat of adsorption and a stable cyclic ability. These multiple advantages combined with the low-cost of the raw material demonstrate that this sample is an excellent candidate as an adsorbent for CO₂ capture.

Received 28th March 2018
Accepted 16th May 2018

DOI: 10.1039/c8ra02701c

rsc.li/rsc-advances

1. Introduction

As industry and society are developing rapidly, the use of fossil fuels will continue to dominate worldwide, and carbon dioxide (CO₂) emissions are expected to continue increasing.^{1,2} CO₂ emissions have become a serious environmental issue of modern civilization because of their effects on global warming and the associated consequences.³ Accordingly, carbon capture and storage (CCS) is considered to be a useful approach to mitigate CO₂ emissions.⁴ Chemical absorption methods using aqueous amine solutions for CO₂ capture have been widely used in industry,⁵ but they are a double-edged sword, as having strong chemical interactions between CO₂ and amines results in a high capacity, but they also make the equipment suffer from serious corrosion and the system experiences a high energy penalty.⁶ However, solid amines, systems attaching alkylamine groups on highly hierarchical porous supports, exhibit very high CO₂ adsorption capacities with simulated flue gas and practical conditions with a lower energy penalty.^{7,8} The

beauty of these systems is that they can work under real flue gas conditions to capture very low concentrations of CO₂ in the mixture gas, associated with moisture, and at elevated temperatures. However the long-term cyclic stabilities are still a concerning problem. In comparison to chemical absorption, physical adsorption based on solid adsorbents is regarded as an alternative method. Varieties of solid adsorbents including silica,⁹ metal-organic frameworks (MOFs),¹⁰⁻¹² organic polymers,¹³ zeolites¹⁴ and porous carbon materials^{15,16} have become the focus for CO₂ capture research. Among them, porous carbon materials have attracted much attention due to their features of large surface area, high porosity, chemical and thermal stability, hydrophobicity and no toxicity, and they are regarded as the most promising CO₂ capture materials.¹⁵⁻¹⁹

As is well known, carbon adsorbents with remarkable CO₂ capacity are commonly those possessing large specific surface areas and hierarchical porous architectures with abundant fine micropores (<1 nm) and complementary mesopores, in which the fine micropores (<1 nm) are important for CO₂ adsorption, while the mesopores are useful for CO₂ diffusion.²⁰⁻²² Meanwhile, due to the fact that CO₂ is weakly acidic, nitrogen elements can be introduced into the carbon frameworks. Nitrogen-doped (N-doped) sites can act as basic active sites to enhance the interactions between CO₂ molecules and the carbon surface *via* base-acid interactions, and can subsequently improve the adsorption capacity and selectivity for CO₂.²²⁻²⁴ At present, numerous N-doped porous carbon materials have been reported for the capture of CO₂, and they are prepared by the carbonation of nitrogen-containing organic polymers.²⁵⁻²⁸ Unfortunately, the high cost of some polymer precursors and the complicated earlier synthetic processes

^aSchool of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo, Henan 454000, China. E-mail: yangjuanhpu@163.com; hpuwj@163.com

^bSchool of Materials Science and Engineering, Henan Polytechnic University, Jiaozuo, Henan 454000, China. E-mail: wangbb580@aliyun.com

^cState Key Laboratory Cultivation Base for Gas Geology and Gas Control, Henan Polytechnic University, Jiaozuo 454000, China

^dSchool of Chemistry and Chemical Engineering, Henan Polytechnic University, Jiaozuo 454000, China

† Electronic supplementary information (ESI) available: CO₂ adsorption data, CO₂/N₂ selectivity ratios, ideal adsorption solution theory calculations, isosteric heat of adsorption calculations and additional figures. See DOI: 10.1039/c8ra02701c



make it hard to scale up production of these porous carbon materials and their practical applications. For reducing the cost and making practical applications viable whilst simultaneously considering environmental factors, biomass materials, especially biomass waste, have been widely used as carbon sources because of their low cost, sustainability, and abundance.^{29–32} In addition, biomass precursors naturally contain some useful heteroatoms such as nitrogen that will be anchored on the surface of the carbon framework, and this will enhance the CO₂ adsorption capability of the carbon materials.^{32–34} Meanwhile, chemical activation with KOH is found to be a very common and useful method for the preparation of porous carbon materials,^{35–37} especially biomass-derived porous carbon materials.^{30–34,38} For instance, by means of KOH activation, Guo *et al.*³⁸ successfully transformed waste coffee grounds into an effective porous carbon sorbent material for CO₂ capture. Chen *et al.*³⁰ and Yang *et al.*³¹ used KOH to activate carbonized coconut shells and develop porous carbon adsorbents for CO₂ capture. Liang *et al.*³² reported the synthesis of N-doped microporous carbon by employing the steam-explosion of popcorn and subsequent KOH activation, in which the resulting carbon material was employed to give a high performance of CO₂ capture. Zhu *et al.*³³ synthesized N-doped nanoporous carbon from pine cones by means of chemical activation with KOH, and it exhibited a high CO₂ capture capacity. Alabadi *et al.*³⁴ obtained highly porous carbon from biomass carbonization and subsequent KOH activation, and it displayed a high CO₂ capture capacity.

Herein, with comprehensive considerations, we report a sustainable and scalable synthesis method by employing waste wool as the raw material. Pre-carbonization and subsequent KOH activation were used to prepare the N-doped hierarchical porous carbon. We chose waste wool as the carbon precursor mainly due to the following: (I) short wool fibres are generally discarded as waste due to their unsuitability for clothing applications, which wastes a resource;^{39,40} (II) wool is mostly composed of amino acids that are unique renewable natural materials with high nitrogen content;^{40,41} (III) functionalized porous carbon can be fabricated from biomass precursors to meet various demands. The resulting waste wool derived N-doped hierarchical porous carbon prepared by chemical activation with the moderate ratio of KOH/carbon = 3 (designated as WNPC-3) possessed a large specific surface area of 1351 m² g⁻¹, a hierarchical porous structure with a total pore volume of 0.78 m³ g⁻¹, a micropore volume as high as 0.54 m³ g⁻¹ and a fine micropore volume up to 0.30 m³ g⁻¹, and a nitrogen content of 4.41 wt%. The CO₂ adsorption capacity of WNPC-3 reached 2.78 mmol g⁻¹ at 25 °C and 3.73 mmol g⁻¹ at 0 °C, under atmospheric pressure (1 bar). Furthermore, WNPC-3 exhibited a moderate CO₂/N₂ selectivity for CO₂ capture from flue gas, an appropriate CO₂ isosteric heat of adsorption in the range of physical adsorption, and a stable CO₂ adsorption capacity after several cycles. Our study may provide a new method for the large-scale production of promising porous carbon adsorbents for selective CO₂ capture.

2. Experimental

2.1 Materials

Waste wool was obtained from Henan, China. Potassium hydroxide (KOH) and hydrochloric acid (HCl) were purchased from Sinopharm Chemical Reagent Co. Ltd. China and used as received without any further purification.

2.2 Sample preparation

The waste wool was thoroughly washed with distilled water and dried at 60 °C. The cleaned wool was pre-carbonized at 300 °C for 2 h with a heating rate of 3 °C min⁻¹ under a N₂ atmosphere, and was then cooled down to room temperature naturally. To simplify, the pre-carbonized wool was denoted WNC. Hereafter, in a typical KOH-activated process, the WNC (0.2 g) was mixed with the KOH activation agent (0.6 g) in 2.5 ml distilled water with a KOH/WNC mass ratio of 3 : 1, and then the resulting mixture was treated with ultrasound for 10 min to obtain a uniform carbon suspension in the KOH solution. Subsequently, the mixture was activated under N₂ protection at 600 °C for 1 h in a tubular furnace with a heating rate of 3 °C min⁻¹. After complete activation, the as-prepared sample was washed with suitable amounts of 0.1 M HCl solution and distilled water until neutral, and then dried at 60 °C for 12 h to obtain the final product. To investigate the effect of KOH dosage on the final product, a sequence of contrast experiments were carried out under the same conditions. For the convenience of the following discussion, the wool derived N-doped porous carbon materials prepared under different KOH dosages were designated as WNPC-*x* where *x* represents the weight ratio of KOH/WNC. For comparison, the WNC directly carbonized at 600 °C for 1 h without the addition of KOH was designated as WNPC.

2.3 Characterization

Field emission scanning electron microscopy (FE-SEM, Hitachi S-4800) with an energy dispersive X-ray spectrometer (EDS) and transmission electron microscopy (TEM, JEOL-21) were employed to examine the morphology, microstructure and elemental mapping of the carbon samples. Powder X-ray diffraction (XRD) was performed on a Bruker D8 advanced X-ray diffractometer using Cu K α radiation ($\lambda = 0.15406$ nm). Raman spectra were collected at an excitation wavelength of 514 nm using a Renishaw inVia spectrometer. Fourier transform infrared (FT-IR) spectra were obtained using a Nicolet iS10 FTIR spectrometer. X-ray photoelectron spectroscopy (XPS) was performed on a Thermo Scientific ESCALAB250 equipped with an Al K α excitation source. Elemental analysis (C, H and N) was performed on a dry basis using a VarioEL III Elemental Analyzer. Nitrogen adsorption–desorption isotherms were measured on a Quantachrome NOVA1000e sorption analyzer by nitrogen physisorption at –196 °C using the conventional volumetric technique. The specific surface area (S_{BET}) was calculated according to the multipoint Brunauer–Emmett–Teller (BET) method based on adsorption data in the relative pressure range between 0.005 to 0.05, and the total pore volume was determined from the amount of nitrogen adsorbed at



a relative pressure of about 0.99. The pore size distribution (PSD) was determined by non-local density functional theory (NLDFT) using nitrogen adsorption data and assuming a slit-shaped pore model. The volume of micropores (pores below 2 nm) and the volume of fine micropores (pores below 1 nm) were calculated based on PSD curves obtained using the NLDFT method.

2.4 CO₂ adsorption measurements

The CO₂ adsorption isotherms of the carbon samples were determined from 0 to 1 bar using an intelligent gravimetric analyzer (IGA-003) at 0 °C and 25 °C. The sample tube was immersed in an ice-water bath for the 0 °C test and a thermostatic water bath for the 25 °C test. Prior to the CO₂ adsorption test, the sample was dried and degassed in a vacuum at 200 °C for 3 h to remove any guest-molecules. After the sample was cooled down to the adsorption temperature, the dry mass was set and CO₂ gas was introduced into the system.

3. Results and discussion

3.1 Physicochemical characterization

In our synthetic process, two procedures including pre-carbonization and the subsequent KOH activation were carried out for the efficient fabrication of wool derived N-doped porous carbon with a hierarchical structure and high surface area; hence, the resulting carbon can be effectively used for selective CO₂ capture, as schematically presented in Fig. 1. The morphology and porous structure of representative sample WNPC-3 were studied using scanning electron microscopy (SEM). As shown in Fig. 2a, the SEM image reveals that the carbon sample possesses a sponge-like morphology characterized by many nested net cavities. The surface of WNPC-3 exhibits an extremely 3D porous structure formed by KOH activation (Fig. 2b). The micropores and mesopores with different pore-sizes of WNPC-3 are interconnected, and can be widely used for CO₂ capture (Fig. 2c). The overall morphology and porous structure of sample WNPC-3 were further studied using transmission electron microscopy (TEM). As can be seen

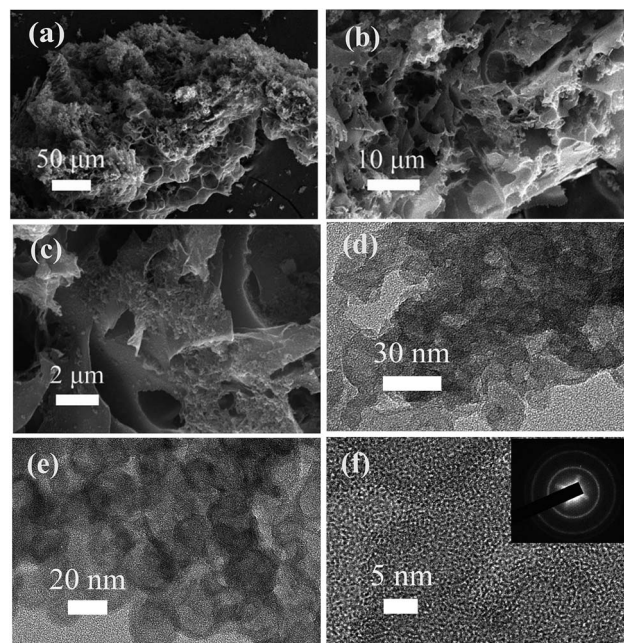


Fig. 2 (a–c) FE-SEM images, (d and e) TEM images and (f) HR-TEM image of the sample WNPC-3. The inset shows the SAED pattern.

in Fig. 2d and e, the low magnification view confirms that WNPC-3 maintains a continuous sponge-like morphology with a cross-linked porous texture, which is in agreement with previous SEM results. The high-resolution transmission electron microscopy (HR-TEM) image (Fig. 2f) shows that the randomly distributed worm-like micropores are formed by the stacking of disordered graphene layers.¹⁶ The selected area electron diffraction (SAED) pattern of WNPC-3 (inset in Fig. 2f) exhibits typical diffuse rings, reflecting the amorphous nature of carbon.

To determine the crystallite structure of a sample of WNPC-3, XRD and Raman spectra were recorded. The two broad peaks at around 22.5° and 43° in the XRD spectrum (Fig. 3a) correspond to typical reflections of the (002) and (100) planes of graphite, indicating the amorphous structure of WNPC-3.^{42,43} The Raman spectrum (Fig. 3b) exhibits two characteristic peaks for WNPC-3 at around 1330 cm⁻¹ (D-band) and 1590 cm⁻¹ (G-band), which correspond to disordered carbon and the ordered graphite lattice, respectively.^{42–44} The intensity ratio of the two bands (I_D/I_G) is known to be proportional to the number of defect sites in the graphitic carbon, that is, the higher the I_D/I_G ratio is, the lower the graphitization is.^{43,44} The calculated I_D/I_G ratio of WNPC-3 is 1.12, confirming that many defects exist in the carbon structure, which is consistent with the XRD results. The chemical bonding information of WNPC-3 was investigated using Fourier transform infrared (FT-IR) spectroscopy (Fig. 3c). The appearance of a broad absorption band at around 3430 cm⁻¹ can be assigned to N–H and/or O–H stretching vibrations.³⁴ The existence of a band at 1620 cm⁻¹ indicates the presence of C=C stretching vibrations in aromatic rings for the activated carbon.²⁷ The peak at around 1200–1000 cm⁻¹ relates to the stretching vibrations of C–N and/or C–O.²⁵ The weak peak



Fig. 1 Schematic illustrating the fabrication of WNPC-x and uses in selective CO₂ capture.



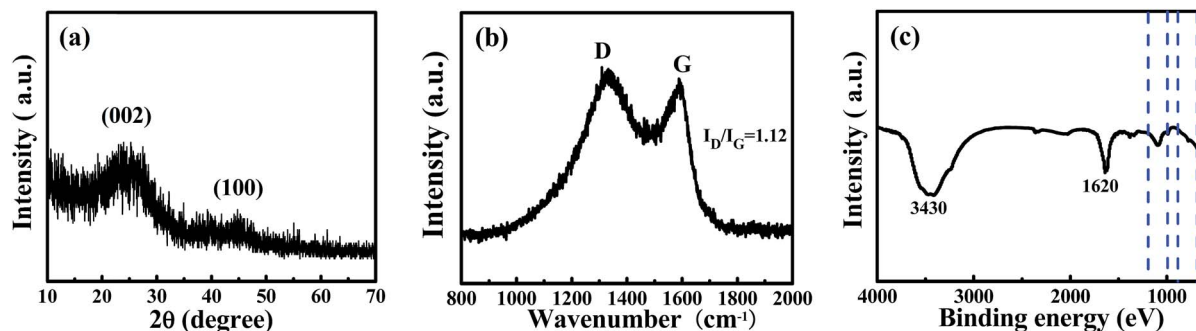


Fig. 3 (a) XRD, (b) Raman and (c) FT-IR spectra of the sample of WNPC-3.

between 900 and 650 cm^{-1} can be assigned to N-H and/or C-H out-of-plane deformation vibrations.^{25,26} Therefore, the FT-IR spectra preliminarily confirm that N-H and C-N species are in WNPC-3.

To further analyze the surface chemical states and the composition of WNPC-3, X-ray photoelectron spectroscopy (XPS) was employed to systematically investigate the intrinsic nature of the C, N and O species in WNPC-3. The full survey spectrum clearly shows the existence of three typical peaks for C 1s, N 1s and O 1s in the sample of WNPC-3 (Fig. 4a). The representative spectrum of C 1s can be deconvoluted into five peaks (Fig. 4b). The peak at about 285.9 eV confirms the presence of C-N in WNPC-3, while the dominant peak at 284.7 eV could be attributed to C-C.^{26,45} The peaks at about 285.4 eV, 286.7 eV and 287.8 eV correspond to C-OH,²⁶ C-O³⁴ and C=O,⁴¹ respectively. The high resolution N 1s spectrum reveals the chemical states of nitrogen atoms in WNPC-3 (Fig. 4c). The deconvoluted spectrum displays three nitrogen species with binding energies of 400.1 eV, 398.5 eV and 402.8 eV, which can be attributed as pyrrolic-N/pyridonic-N, pyridinic-N and pyridine N-oxides, respectively.^{25,26,41,45} Pyrrolic-N and pyridonic-N are hard to distinguish from each other within the accuracy of

XPS measurements, however, considering the greater stability of pyridonic-N compared to pyrrolic-N, pyridonic-N is more likely to be present in WNPC-3.²⁵⁻²⁷ The corresponding peak areas analysis shows that the amount of pyridonic-N is higher than that of the two others, and it has been reported that pyridonic-N acts as a main anchor for CO₂ capture.^{16,25,26} Three characteristic peaks are observed at 531.3 eV, 533.1 eV and 534.9 eV in the deconvoluted O 1s spectrum (Fig. 4d), which can be ascribed to O=C, O-C, and chemisorbed O₂ and/or H₂O bound to WNPC-3 respectively.^{26,41,45}

As previously reported,^{46,47} the C-O and C=O functional groups may play an important role in CO₂ adsorption and CO₂/N₂ selectivity, due to enhanced interaction forces between the O-decorated carbon framework and CO₂ molecules. Additionally, the SEM energy dispersive X-ray spectroscopy (EDS) mapping analysis for WNPC-3 shows that the elements of C, N and O are uniformly distributed in the sample (Fig. 4e-h).

The chemical compositions of a sample of WNPC-3 as well as the other samples of WNPC, WNPC-1 and WNPC-5 were further investigated by C, N and O elemental analysis, as presented in Table 1. As can be seen, the nitrogen content decreases from 11.25 wt% (un-activated WNPC) to 3.70 wt% (strongly activated

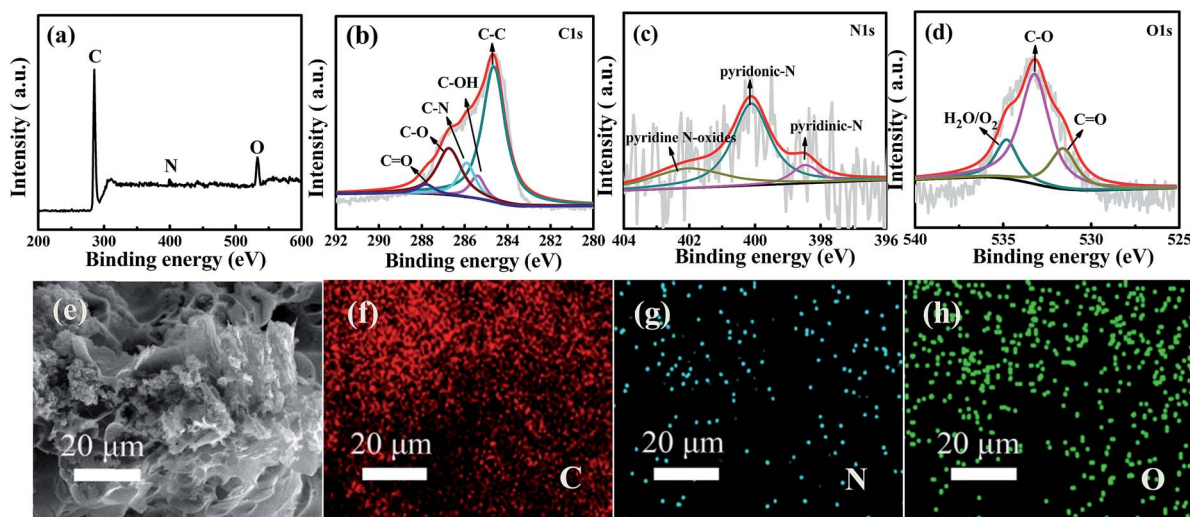


Fig. 4 XPS spectra of WNPC-3: (a) high-resolution full survey spectrum of (b) C 1s, (c) N 1s and (d) O 1s; (e-h) SEM image and the corresponding EDS element mappings of (f) C, (g) N and (h) O for WNPC-3.



Table 1 Chemical compositions of wool-derived carbon materials

Sample	Elemental composition (wt%)			
	N ^a	C ^a	H ^a	O ^b
WNCP	11.25	71.90	1.37	15.48
WNCP-1	4.57	70.73	1.64	23.06
WNCP-3	4.14	69.65	1.42	24.79
WNCP-5	3.70	67.47	1.68	27.15

^a Obtained from C, H and N elemental analysis. ^b Calculated by difference.

WNCP-5). Approximately 4.57 wt% of nitrogen is detected for the low-activated WNCP-1, while about 4.14 wt% is detected for moderately activated WNCP-3. The nitrogen content decreases with the increasing KOH/WNC weight ratio, which is consistent with the previously reported literature.^{23–27} There is a rapid drop in nitrogen content from un-activated WNCP to the activated WNCP-1. The nitrogen content decreases slowly when the KOH/WNC ratio increases from 1 to 5, especially with a KOH/WNC ratio from 1 to 3. However, with the nitrogen content decrease, the carbon content also decreases concomitantly with the KOH activation, while the hydrogen content appears to be relatively unchanged. Furthermore, the oxygen content is increased with the increase in the KOH/WNC ratio in the samples, from WNCP to WNCP-1 to WNCP-3 to WNCP-5, because the KOH activation promotes the oxidation process of the carbon.⁴⁸ The KOH activated carbon materials contain more O atoms, which could be attributed to the reaction of carbon with CO₂ evolved from K₂CO₃ and K₂O, as well as oxygen chemisorption from air.^{49,50} The increased oxygen content from WNCP to WNCP-5 should be due to the increased KOH/WNC ratio, which is consistent with the behavior of KOH activated carbon materials we have reported previously.^{26,45} Therefore the activated carbon materials can preserve more oxygen functional groups such as C=O and C–O.^{46,51}

The porosities of WNCP and the WNCP-*x* series were investigated by nitrogen adsorption–desorption isothermal analysis, as presented in Fig. 5, and the textural characteristics are shown in Table 2. The salt concentration (such as the KOH amount used in activation) can alter the shape of the adsorption–

Table 2 Textural characteristics and CO₂ uptakes for wool-derived carbon materials

Sample	Textural characteristics				CO ₂ uptake 25 °C (mmol g ⁻¹)
	S _{BET} ^a	V _{total} ^b	V _{micro} ^c	PV _{1 nm} ^d	
WNCP	447	0.22	0.18	0.11	1.48
WNCP-1	1010	0.57	0.37	0.15	2.33
WNCP-3	1352	0.78	0.54	0.30	2.78
WNCP-5	1420	0.86	0.52	0.18	2.35

^a S_{BET} is the specific surface area calculated by BET equations based on the adsorption data in the *P/P*₀ range from 0.005 to 0.05. ^b V_{total} is the total pore volume obtained at *P/P*₀ ~ 0.99. ^c V_{micro} is the cumulative micropore volume (pore size < 2 nm) analyzed using the NLDFT method. ^d PV_{1 nm} is the cumulative fine micropore volume (pore size < 1 nm) analyzed using the NLDFT method.

desorption isotherm, and thus alter the specific surface area and especially the pore-size distribution of the activated carbon materials.^{36–38} As can be seen from Fig. 5a, the un-activated sample WNCP has a very low nitrogen adsorption in the low pressure range and does not display a hysteresis loop in the middle pressure range, which reveals that only a small number of micropores exist in the WNCP. In contrast, all of the activated WNCP-*x* series samples display significantly enhanced nitrogen adsorption, exhibiting typical type-I/IV isothermal curves with sharp increases at low pressure and obvious hysteresis loops at middle pressures, which implies that micropores and mesopores all exist in WNCP-*x*. As the ratio of KOH/WNC increased from 1 to 3 and 5, the adsorption curve increased steeply at low pressure, indicating the development of the specific surface area and microporosity.^{36,38} Moreover, with the increasing KOH/WNC ratio, the isotherm knees of the activated samples are gradually widened to some extent, indicating the generation of some large micropores and/or small mesopores in the carbon framework.^{52,53} Fig. 5b shows the corresponding pore size distribution (PSD) curves of all samples, and these were calculated using the NLDFT model. The pore size of WNCP mainly centers at 0.93 nm indicating a microporous structure. The PSD curves of the activated WNCP-*x* series are distributed in the range of 0.50–4.00 nm indicating hierarchical porous structures. Interestingly, all activated samples (WNCP-1, WNCP-3

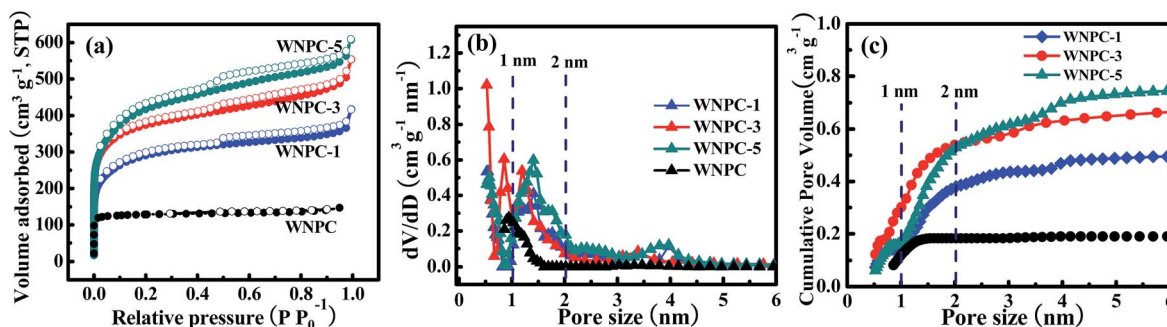


Fig. 5 (a) Nitrogen adsorption–desorption isotherms, (b) PSDs and (c) cumulative pore volumes against pore sizes for wool-derived carbon materials.



and WNPC-5) possess an important fraction of fine micropores (<1 nm). In particular, the moderately activated WNPC-3 exhibits an extraordinarily strong peak at 0.52 nm, indicating a large number of fine micropores (<1 nm) in the carbon framework. Furthermore, WNPC-3 also has two moderately strong peaks at 0.84 nm and 1.19 nm, and one weak peak at around 3.5 nm. In contrast, the low-activated WNPC-1 only exhibits two moderately strong peaks at 0.50 nm and 1.39 nm, and one weak peak at about 2.5 nm. Similarly, the strongly activated WNPC-5 only has two moderately strong peaks at 0.57 nm and 1.41 nm, and two weak peaks at around 2.5 nm and 4 nm. However, these PSD curves are slightly enlarged with the increasing KOH/WNC ratio, and this is probably caused by merging of neighboring small micropores into mesopores or larger ones due to the continuous KOH activation.^{38,52–54} The pore structures can be developed by the evolution of gaseous by-products during KOH activation.^{36,38} To the best of our knowledge, the chemical reaction between KOH and carbon proceeds as follows: $6\text{KOH} + \text{C} \rightarrow 2\text{K} + 3\text{H}_2 + 2\text{K}_2\text{CO}_3$, followed by K_2CO_3 decomposition and the reaction of $\text{K}/\text{K}_2\text{CO}_3/\text{CO}_2$ with carbon.^{36,55} Thus with increasing KOH activation, pore widening is observed. The progressive KOH etching on the carbon results in a gradual increase in both the specific surface area and the total pore volume. From Table 2, it can be observed that the strongly activated WNPC-5 has the largest specific area (S_{BET}) and total pore volume (V_{total}) of $1420 \text{ m}^2 \text{ g}^{-1}$ and $0.86 \text{ m}^3 \text{ g}^{-1}$, respectively, which are larger than those of un-activated WNPC ($S_{\text{BET}} = 447 \text{ m}^2 \text{ g}^{-1}$ and $V_{\text{total}} = 0.20 \text{ m}^3 \text{ g}^{-1}$), low-activated WNPC-1 ($S_{\text{BET}} = 1010 \text{ m}^2 \text{ g}^{-1}$ and $V_{\text{total}} = 0.57 \text{ m}^3 \text{ g}^{-1}$) and moderately activated WNPC-3 ($S_{\text{BET}} = 1352 \text{ m}^2 \text{ g}^{-1}$ and $V_{\text{total}} = 0.78 \text{ m}^3 \text{ g}^{-1}$). However, to the best of our knowledge, besides the specific surface area and total pore volume, the micropore volume (V_{micro}) and fine micropore volume ($\text{PV}_{1 \text{ nm}}$) are all very important for CO_2 capture.^{53,54,56–58} By analyzing the cumulative pore volume against the pore size (Fig. 5c), it is worth noting that WNPC-3 possesses the largest V_{micro} and $\text{PV}_{1 \text{ nm}}$ of $0.54 \text{ m}^3 \text{ g}^{-1}$ and $0.30 \text{ m}^3 \text{ g}^{-1}$, respectively, which are much larger than those of WNPC ($V_{\text{micro}} = 0.18 \text{ m}^3 \text{ g}^{-1}$ and $\text{PV}_{1 \text{ nm}} = 0.11 \text{ m}^3 \text{ g}^{-1}$), WNPC-1 ($V_{\text{micro}} = 0.37 \text{ m}^3 \text{ g}^{-1}$ and $\text{PV}_{1 \text{ nm}} = 0.15 \text{ m}^3 \text{ g}^{-1}$) and WNPC-5 ($V_{\text{micro}} = 0.52 \text{ m}^3 \text{ g}^{-1}$ and $\text{PV}_{1 \text{ nm}} = 0.18 \text{ m}^3 \text{ g}^{-1}$), as can be seen in Table 2. Furthermore, the percentage of microporosity ($V_{\text{micro}}/V_{\text{total}}$) for WNPC-3 can reach 69%, which is higher than other activated carbon samples (WNPC-1 is 64% and WNPC-5 is 60%). Although the surface area and total pore volume of WNPC-3 are smaller than those of WNPC-5, the CO_2 adsorption capability requires the co-operation of the micropore volume, the fine micropore volume and the percentage of microporosity, which can effectively guarantee the CO_2 capture performance for WNPC-3.

3.2 Adsorption performance

The CO_2 adsorption isotherms for the carbon samples were investigated at $25 \text{ }^\circ\text{C}$ under atmospheric pressure (1 bar), as shown in Fig. 6a. As Gadipelli *et al.*^{35,36,59} previously reported, the low pressure (~ 1 bar) adsorption behavior is mainly dependent on the narrow pore size distribution in the micropore region,

due to the caging effect, particularly for those pores smaller than 1 nm.^{20,59–61} WNPC-3 exhibits a significant fine micropore volume (Table 2), which can be attributed to its large number of fine micropores (centred on 0.52 nm and 0.84 nm). Therefore, WNPC-3 demonstrates a good CO_2 adsorption capacity of 2.78 mmol g^{-1} (at 1 bar and $25 \text{ }^\circ\text{C}$), which can be compared with those porous carbon materials with similar specific surface areas and/or pore-size distribution structures (Table S1†). Among the WNPC and WNPC-*x* samples, the corresponding relationship between CO_2 uptake and fine micropore volume can be clearly seen (Fig. 6b). WNPC-3 exhibits an obviously better CO_2 uptake (2.78 mmol g^{-1}) than those of WNPC (1.48 mmol g^{-1}), WNPC-1 (2.33 mmol g^{-1}) and WNPC-5 (2.35 mmol g^{-1}) (Table 2). The presence of a large number of fine micropores is interesting for gas storage applications.

Therefore, taking WNPC-3 as the representative sample, the CO_2 adsorption performance was measured at $0 \text{ }^\circ\text{C}$ and 1.0 bar, and it exhibited a larger CO_2 adsorption capacity of 3.72 mmol g^{-1} than that at $25 \text{ }^\circ\text{C}$ (Fig. 6c), indicating that the CO_2 adsorption is an exothermic process. As can be seen, the CO_2 uptake increases steadily without a distinct plateau in the isotherm for the entire pressure range, indicating that more CO_2 can be adsorbed at higher pressures. Thus, the CO_2 capture performance for WNPC-3 was further measured at a high pressure of 10 bar (under $0 \text{ }^\circ\text{C}$), and it could reach up to $10.39 \text{ mmol g}^{-1}$ (Fig. S1†).

Besides the high uptake of CO_2 , an excellent CO_2 absorbent should also demonstrate high CO_2 selectivity against other gases such as N_2 . As shown in Fig. 6c, the adsorption capacity of N_2 by WNPC-3 was also measured at $25 \text{ }^\circ\text{C}$ under 1 bar pressure. Clearly, the uptake of N_2 is just 0.36 mmol g^{-1} , which is much lower than the uptake of CO_2 under the same conditions. In fact, the CO_2 uptake is about 7.7 times the N_2 adsorption (Fig. 6c), and such a property is essential for CO_2 capture. The CO_2/N_2 selectivity was measured using Henry's law constants, which can be calculated from the ratio of the initial slopes for the pure gas isotherms.^{62–64} According to the initial slope calculation, the selectivity for CO_2 over N_2 for WNPC-3 is about 23 at $25 \text{ }^\circ\text{C}$ (Fig. S2†), indicating a high selectivity towards CO_2 . In addition, we further used ideal adsorbed solution theory (IAST)^{65–68} to predict CO_2/N_2 selectivity in binary gas mixtures using only pure gas isotherms measured at $25 \text{ }^\circ\text{C}$. In the calculations, the ratio of CO_2/N_2 is assumed to be 15/85, which is a typical component of flue gas.^{6,37,66,67,69} Herein, the dual-site Langmuir model (DL) and the single-site Langmuir model (L) were chosen to fit the CO_2 and N_2 adsorption isotherms, respectively, and then DL/L-IAST was utilized to estimate the CO_2/N_2 selectivity of WNPC-3 (Fig. S3†). As depicted in Fig. 6d, the IAST selectivity for CO_2/N_2 of WNPC-3 can reach 16 at $25 \text{ }^\circ\text{C}$ and 1 bar, indicating that it is an excellent prospect for industrial applications. To the best of our knowledge, CO_2 exhibits a higher quadrupole moment and polarizability than N_2 , and in comparison, N_2 is much more chemically inert and exhibits lower polarizability than CO_2 .⁶⁸ Therefore, the selectivity is influenced by the presence of N in the carbon framework, because N will create some electrostatic microdomains within the pore volume, which can play an important role in



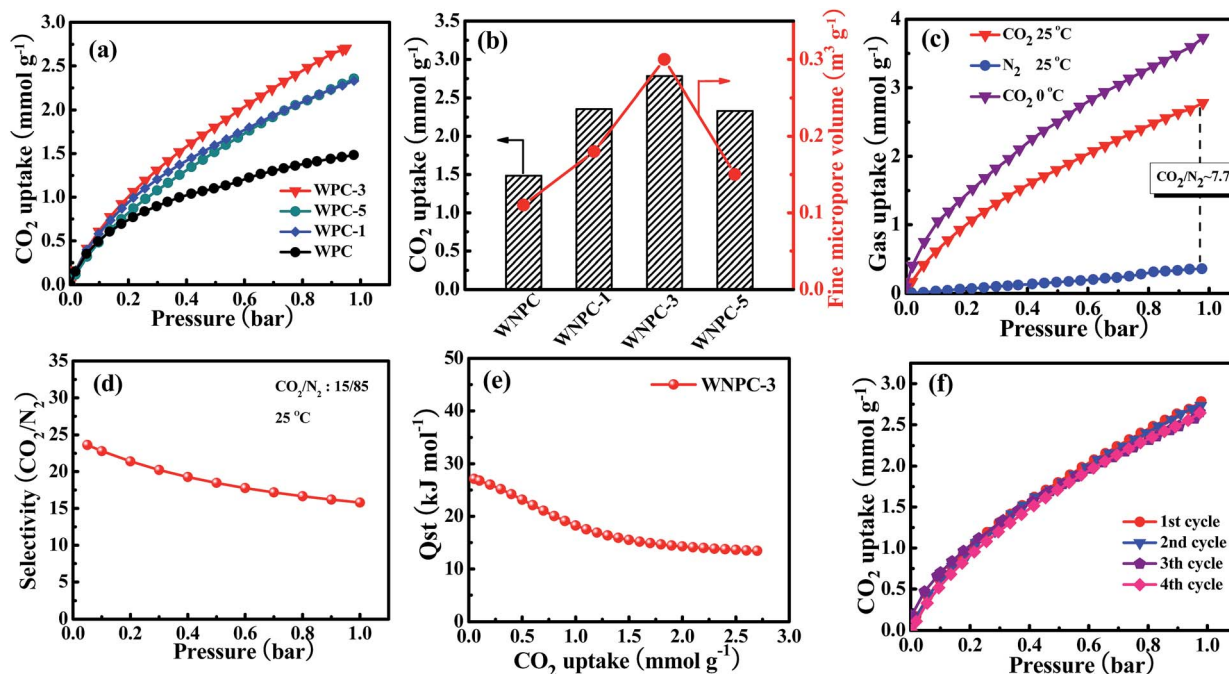


Fig. 6 (a) CO₂ adsorption isotherms at 25 °C and (b) corresponding relationship of CO₂ uptake and fine micropore volume for the carbon samples; (c) CO₂ and N₂ adsorption isotherms at 25 °C and 0 °C, (d) IAST selectivity for CO₂ over N₂ collected at 25 °C (assuming CO₂/N₂ is 15/85), (e) CO₂ isosteric heats of adsorption and (f) CO₂ multicycle adsorption isotherms at 25 °C for WNPC-3.

segregating the quadrupolar fluids N₂ and CO₂ through dipole and quadrupole moments.³⁷ Furthermore, the preserved oxygen functional groups in the carbon framework also play a crucial role in CO₂/N₂ selectivity, due to the enhanced interaction forces between the O-decorated carbon framework and CO₂ molecules.^{46,47} However, comparing with some other carbon materials reported in the literature (Table S1†), the CO₂/N₂ selectivity of WNPC-3 is just moderate. The moderate CO₂/N₂ selectivity can be explained by the large number of micropores (*ca.* 0.52–1.19 nm), in which N₂ may experience higher binding energies from the carbon surface through van der Waals' or electrostatic forces.³⁷ In addition, the selectivity of WNPC-3 was obtained from the pure gas adsorption isotherms, which assumes the interactions between the fluid molecules are negligible; therefore, the selectivity value can be regarded as a practical maximum.³⁷

As we know, the overall effects of micropore size and N-/O-dopants in the porous carbon materials are to increase the adsorbent–adsorbate interaction energy, which may incur a greater energy penalty for regeneration.^{38,68} Therefore, to understand the interaction strength of CO₂ molecules with WNPC-3, the isosteric heat of adsorption (Q_{st}) for WNPC-3 was calculated using a variant of the Clausius–Clapeyron equation,^{38,63,66,70} which was accomplished by collecting CO₂ adsorption isotherms at 0 °C and 25 °C and fitting the data to the DL model (Fig. S3†). As displayed in Fig. 6e, the calculated Q_{st} for WNPC-3 is in the range of 27–13 kJ mol⁻¹, with the CO₂ uptake varying from 0.05 to 2.7 mmol g⁻¹. At low CO₂ loading, the high initial Q_{st} value leads to a preferential adsorption of CO₂ over N₂, which can be attributed to the CO₂ molecules

being selectively adsorbed on the surface active nitrogen sites^{15,16} and the multiple pore wall interactions with CO₂ molecules.^{6,13} At high CO₂ loading, as the active nitrogen sites and microporous surface became gradually saturated, the availability of sorption sites progressively decreased, leading to a lowering in the adsorption heat.^{16,24} We note that the Q_{st} of WNPC-3 decreases mildly with the increasing CO₂ loading until a near-plateau is achieved, which suggests that the binding energies of CO₂ in the pores are heterogeneous.^{30,31} However, the Q_{st} value for WNPC-3 is comparable to that for un-doped carbon,³⁸ which is much below the energy of covalent bonds and consistent with the fully reversible CO₂ isotherm, suggesting that the CO₂ release can be achieved by a pressure drop without heating.^{13,30,31}

From the viewpoint of practical applications, the recyclability of an adsorbent is important, and thus, the multicycle adsorptions of CO₂ on WNPC-3 were conducted at 25 °C. As can be seen in Fig. 6f, the CO₂ uptake remains almost unchanged in four cycles, indicating that WNPC-3 has excellent recyclability and stability. It is worth noting that, after each adsorption cycle, the saturated WNPC-3 released CO₂ by a pressure drop without heating, which should be attributed to its appropriate Q_{st} values.

4. Conclusions

In summary, N-doped hierarchical porous carbon has been successfully synthesized in this work using renewable waste wool as the raw material. The resulting optimal sample WNPC-3 was endowed with a high specific surface area of 1351 m² g⁻¹,



a hierarchical porous structure with a total pore volume of $0.78 \text{ m}^3 \text{ g}^{-1}$, a micropore volume up to $0.54 \text{ m}^3 \text{ g}^{-1}$ and a fine micropore volume as high as $0.30 \text{ m}^3 \text{ g}^{-1}$, and a certain number of nitrogen and oxygen functional groups. The conspicuous synergetic effect of the textural characteristics and functional groups provides an excellent guarantee for CO_2 capture performance. We demonstrate that micropores are principally responsible for CO_2 capture at low pressure (1 bar). Remarkably, WNPC-3 exhibits a good CO_2 adsorption capability of 3.72 mmol g^{-1} under 0°C at atmospheric pressure (1 bar). Furthermore, an appropriate Q_{st} leads to WNPC-3 possessing an excellent CO_2/N_2 selectivity and a significant regenerability. More significantly, here the strategy we used provides an excellent method to make best use of the low-cost yet abundant resources endowed by nature to fabricate sustainable carbon adsorbents for selective CO_2 capture, thus opening new ways to set up an economical platform for practical applications.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was supported by the Henan Province Colleges and Universities Key Research Project (18A620002, 18A150005), China Postdoctoral Science Foundation (2018M632775), the Henan Polytechnic University Doctor Foundation (660107/017), the Academician Workstation Innovation Foundation (13160093/010), the Program for Innovative Research Team in University of Ministry of Education of China (IRT_16R22) and the NSFC (No. U1704146).

Notes and references

- R. S. Haszeldine, *Science*, 2009, **325**, 1647–1652.
- J. D. Figueroa, T. Fout, S. Plasynski, H. McIlvried and R. D. Srivastava, *Int. J. Greenhouse Gas Control*, 2008, **2**, 9–20.
- D. M. D'Alessandro, B. Smit and J. R. Long, *Angew. Chem., Int. Ed.*, 2010, **49**, 6058–6082.
- X. Ma, X. Wang and C. Song, *J. Am. Chem. Soc.*, 2009, **131**, 5777–5783.
- G. T. Rochelle, *Science*, 2009, **325**, 1652–1654.
- J. Kou and L. B. Sun, *Ind. Eng. Chem. Res.*, 2016, **55**, 10916–10925.
- S. Gadipelli, H. A. Patel and Z. Guo, *Adv. Mater.*, 2015, **27**, 4903–4909.
- S. Gadipelli, Y. Lu, N. T. Skipper, T. Yildirim and Z. Guo, *J. Mater. Chem. A*, 2017, **5**, 17833–17840.
- M. Niu, H. Yang, X. Zhang, Y. Wang and A. Tang, *ACS Appl. Mater. Interfaces*, 2016, **8**, 17312–17320.
- J. Yu, L. H. Xie, J. R. Li, Y. Ma, J. M. Seminario and P. B. Balbuena, *Chem. Rev.*, 2017, **117**, 9674–9754.
- S. Gadipelli, W. Travis, W. Zhou and Z. Guo, *Energy Environ. Sci.*, 2014, **7**, 2232–2238.
- S. Gadipelli and Z. Guo, *Chem. Mater.*, 2014, **26**, 6333–6338.
- T. Islamoglu, S. Behera, Z. Kahveci, T. D. Tessema, P. Jena and H. M. El-Kaderi, *ACS Appl. Mater. Interfaces*, 2016, **8**, 14648–14655.
- T. H. Nguyen, S. Kim, M. Yoon and T. H. Bae, *ChemSusChem*, 2016, **9**, 455–461.
- N. Fu, H. M. Wei, H. L. Lin, L. Li, C. H. Ji, N. B. Yu, H. J. Chen, S. Han and G. Y. Xiao, *ACS Appl. Mater. Interfaces*, 2017, **9**, 9955–9963.
- M. Yang, L. Guo, G. Hu, X. Hu, J. Chen, S. Shen, W. Dai and M. Fan, *Ind. Eng. Chem. Res.*, 2016, **55**, 757–765.
- A. S. Jalilov, G. Ruan, C. C. Hwang, D. E. Schipper, J. J. Tour, Y. Li, H. Fei, E. L. G. Samuel and J. M. Tour, *ACS Appl. Mater. Interfaces*, 2015, **7**, 1376–1382.
- J. Zhang, X. Wang, G. Qi, B. Li, Z. Song, H. Jiang, X. Zhang and J. Qiao, *Carbon*, 2016, **96**, 864–870.
- H. Wei, W. Qian, N. Fu, H. Chen, J. Liu, X. Jiang, G. Lan, H. Lin and S. Han, *J. Mater. Sci.*, 2017, **52**, 10308–10320.
- N. P. Wickramaratne and M. Jaroniec, *ACS Appl. Mater. Interfaces*, 2013, **5**, 1849–1855.
- M. Sevilla and A. B. Fuertes, *Energy Environ. Sci.*, 2011, **4**, 1765–1771.
- J. W. F. To, J. He, J. Mei, R. Haghpanah, Z. Chen, T. Kurosawa, S. Chen, W. G. Bae, L. Pan, J. B. H. Tok, J. Wilcox and Z. Bao, *J. Am. Chem. Soc.*, 2016, **138**, 1001–1009.
- G. Sethia and A. Sayari, *Carbon*, 2015, **93**, 68–80.
- L. Liu, Z. H. Xie, Q. F. Deng, X. X. Hou and Z. Y. Yuan, *J. Mater. Chem. A*, 2017, **5**, 418–425.
- X. Fan, L. Zhang, G. Zhang, Z. Shu and J. Shi, *Carbon*, 2013, **61**, 423–430.
- Y. Li, B. Zou, C. Hu and M. Cao, *Carbon*, 2016, **99**, 79–89.
- M. Sevilla, P. Valle-Vigón and A. B. Fuertes, *Adv. Funct. Mater.*, 2011, **21**, 2781–2787.
- D. Lee, C. Z. Zhang, C. Wei, B. L. Ashfeld and H. Gao, *J. Mater. Chem.*, 2013, **1**, 14862–14867.
- P. Wang, Y. Guo, C. Zhao, J. Yan and P. Lu, *Appl. Energy*, 2017, **201**, 34–44.
- J. Chen, J. Yang, G. Hu, X. Hu, Z. Li, S. Shen, M. Radosz and M. Fan, *ACS Sustainable Chem. Eng.*, 2016, **4**, 1439–1445.
- M. Yang, L. Guo, G. Hu, X. Hu, L. Xu, J. Chen, W. Dai and M. Fan, *Environ. Sci. Technol.*, 2015, **49**, 7063–7070.
- T. Liang, C. Chen, X. Li and J. Zhang, *Langmuir*, 2016, **32**, 8042–8049.
- B. Zhu, C. Shang and Z. Guo, *ACS Sustainable Chem. Eng.*, 2016, **4**, 1050–1057.
- A. Alabadi, S. Razzaque, Y. Yang, S. Chen and B. Tan, *Chem. Eng. J.*, 2015, **281**, 606–612.
- S. Gadipelli and Z. X. Guo, *Prog. Mater. Sci.*, 2015, **69**, 1–60.
- S. Gadipelli, J. Burrella and T. Yildirim, *Energy Environ. Sci.*, 2012, **5**, 6453–6459.
- K. V. Kumar, S. Gadipelli, K. Preuss, H. Porwal, T. Zhao, Z. X. Guo and M. M. Titirici, *ChemSusChem*, 2017, **10**, 199–209.
- W. Travis, S. Gadipelli and Z. Guo, *RSC Adv.*, 2015, **5**, 29558–29562.
- G. Cui, Y. Dong, B. Li, Y. Li and P. Wang, *Fibers Polym.*, 2017, **18**, 713–719.



- 40 G. Cui, Y. Dong, Y. Li, W. Shen and Z. Chen, *Color. Technol.*, 2017, **133**, 200–208.
- 41 L. Zhou, H. Cao, S. Zhu, L. Hou and C. Yuan, *Green Chem.*, 2015, **17**, 2373–2382.
- 42 H. Wei, H. Chen, N. Fu, J. Chen, G. Lan, W. Qian, Y. Liu, H. Lin and S. Han, *Electrochim. Acta*, 2017, **231**, 403–411.
- 43 D. Liu, W. Zhang, H. Lin, Y. Li, H. Lu and Y. Wang, *RSC Adv.*, 2015, **5**, 19294–19300.
- 44 T. Wei, X. Wei, Y. Gao and H. Li, *Electrochim. Acta*, 2015, **169**, 186–194.
- 45 Y. Li and M. Cao, *Chem.–Asian J.*, 2015, **10**, 1496–1504.
- 46 J. Wang, R. Krishna, X. Wu, Y. Sun and S. Deng, *Langmuir*, 2015, **31**, 9845–9852.
- 47 J. Wang, R. Krishna, J. Yang and S. Deng, *Environ. Sci. Technol.*, 2015, **49**, 9364–9373.
- 48 Y. Sudaryanto, S. B. Hartono, W. Irawaty, H. Hindarso and S. Ismadji, *Bioresour. Technol.*, 2006, **97**, 734–739.
- 49 R. Q. Sun, L. B. Sun, Y. Chun and Q. H. Xu, *Carbon*, 2008, **46**, 1757–1764.
- 50 S. J. Park and W. Y. Jung, *J. Colloid Interface Sci.*, 2002, **250**, 93–98.
- 51 J. L. Figueiredo, M. F. R. Pereira, M. M. A. Freitas and J. J. M. Órfão, *Carbon*, 1999, **37**, 1379–1389.
- 52 J. Cai, J. Qi, C. Yang and X. Zhao, *ACS Appl. Mater. Interfaces*, 2014, **6**, 3703–3711.
- 53 J. Ludwinowicz and M. Jaroniec, *Carbon*, 2015, **82**, 297–303.
- 54 C. Zhang, W. Song, Q. Ma, L. Xie, X. Zhang and H. Guo, *Energy Fuels*, 2016, **30**, 4181–4190.
- 55 M. A. Lillo-Ródenas, D. Cazorla-Amorós and A. Linares-Solano, *Carbon*, 2003, **41**, 267–275.
- 56 P. Cheng, T. Li, H. Yu, L. Zhi, Z. Liu and Z. Lei, *J. Phys. Chem. C*, 2016, **120**, 2079–2086.
- 57 N. P. Wickramaratne and M. Jaroniec, *Adsorption*, 2014, **20**, 287–293.
- 58 N. P. Wickramaratne, J. Xu, M. Wang, L. Zhu, L. Dai and M. Jaroniec, *Chem. Mater.*, 2014, **26**, 2820–2828.
- 59 S. Gadipelli, V. Krungleviciute, Z. X. Guo and T. Yildirim, *Energy Environ. Sci.*, 2014, **7**, 335–342.
- 60 Z. Zhang, J. Zhou, W. Xing, Q. Xue, Z. Yan, S. Zhuo and S. Z. Qiao, *Phys. Chem. Chem. Phys.*, 2013, **15**, 2523–2529.
- 61 V. Presser, J. McDonough, S. H. Yeon and Y. Gogotsi, *Energy Environ. Sci.*, 2011, **4**, 3059–3066.
- 62 J. Wang, I. Senkowska, M. Oschatz, M. R. Lohe, L. Borchardt, A. Heerwig, Q. Liu and S. Kaskel, *ACS Appl. Mater. Interfaces*, 2013, **5**, 3160–3167.
- 63 S. M. Mahurin, J. Gorka, K. M. Nelson, R. T. Mayes and S. Dai, *Carbon*, 2014, **67**, 457–464.
- 64 R. Narasimman, S. Vijayan and K. Prabhakaran, *RSC Adv.*, 2014, **4**, 578–582.
- 65 T. Islamoglu, M. G. Rabbani and H. M. El-Kaderi, *J. Mater. Chem. A*, 2013, **1**, 10259–10266.
- 66 S. Bandyopadhyay, A. G. Anil, A. James and A. Patra, *ACS Appl. Mater. Interfaces*, 2016, **8**, 27669–27678.
- 67 Y. Shi, J. Zhu, X. Liu, G. Geng and L. Sun, *ACS Appl. Mater. Interfaces*, 2014, **6**, 20340–20349.
- 68 S. Gadipelli and Z. X. Guo, *ChemSusChem*, 2015, **8**, 2123–2132.
- 69 R. Li, X. Ren, X. Feng, X. Li, C. Hu and B. Wang, *Chem. Commun.*, 2014, **50**, 6894–6897.
- 70 M. Dinca and J. R. Long, *J. Am. Chem. Soc.*, 2005, **127**, 9376–9377.

