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# Methanol to aromatics: isolated zinc phosphate groups on HZSM-5 zeolite enhance BTX selectivity and catalytic stability†

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HZSM-5 zeolite combined with unique zinc and phosphorus species, yields excellent selectivity (~85%) to BTX (benzene, toluene, xylenes) in aromatic products. It was found that both zinc and phosphorus species were highly distributed in the pores of the zeolite channel network to form isolated zinc phosphate groups, which directly bond to the surface of zeolite, leading to a strong Lewis acidic center and an optimized surface acidity distribution favorable for BTX formation and the hydrothermal stability of the catalyst.

The conversion of methanol to aromatics (MTA) has been turning into an increasingly important alternative source of light aromatics including benzene (B), toluene (T), xylenes (X), with the development of coal-, shale gas-, or biomass-derived methanol *via* the syngas route.<sup>1–4</sup> By modifying HZSM-5 with zinc ions,<sup>1–14</sup> light aromatics could be selectively produced. However, it has many drawbacks by exchanging zinc ions directly to HZSM-5, such as low selectivity, loss of zinc<sup>15</sup> and the coke formation on the surface of the catalyst. The catalytic dehydration of methanol produces large amounts of water vapor during MTA and the subsequent regeneration process at temperatures higher than the reaction temperature,<sup>16–18</sup> call for catalysts with high hydrothermal stability.<sup>19</sup> Therefore, the preservation of good activity and selectivity in the severe reaction and regeneration conditions of MTA processes requires the catalysts to maintain good thermal and hydrothermal stabilities, moreover, understanding the nature of, and controlling over stability of both zinc ions and HZSM-5 framework of the catalyst are among the main challenges in the field.

Modification of HZSM-5 by phosphorus (referred to as P/HZSM-5) is extensively used to improve the hydrothermal stability of HZSM-5 zeolite<sup>18,20–24</sup> in converting methanol to light olefins,<sup>25</sup> alkylation and/or disproportionation of aromatics.<sup>26,27</sup> However, the sole use of P-modified HZSM-5 catalyst is rarely reported in MTA reaction,<sup>7,28</sup> to the best of our knowledge. As shown in this work, the BTX formation over P/HZSM-5 catalyst is limited in comparison with Zn/HZSM-5 catalyst.

Nevertheless, it is generally accepted that phosphorus inhibits the dealumination of zeolites, which, in turn, increases their hydrothermal stability and catalytic selectivity. Our hypothesis is that the combination of P-modified HZSM-5 catalyst and Zn/HZSM-5 catalyst could enable both the enhancement of hydrothermal stability and aromatics selectivity of MTA catalysts. Several groups have reported that adding phosphorus to Zn/HZSM-5 promotes the activity and stability of the catalysts in light alkane aromatization by decreasing the loss of zinc,<sup>29–31</sup> as well as in aromatization of fluid catalytic cracking (FCC) fractions.<sup>31–34</sup> There are only a handful of ZnPHZ catalyst types used in MTA reaction,<sup>35,36</sup> and most of such reports have been focused on the reaction studies, not the catalyst structure. In the remainder of the Introduction, we will present our motivation of synthesizing a hybrid ZnPHZ catalyst.

Controlling acid properties is among the key factors for achieving selective transformation using HZSM-5 zeolites<sup>37,38</sup> In MTA reaction, the Lewis nature of hydroxyl zinc ions can accelerate the recombination of surface hydrogen,<sup>39,40</sup> suppress the cracking process to C<sub>3</sub> fragments by decreasing stronger Brönsted acid and enhance cyclization and dehydrogenation of C<sub>6</sub>=C<sub>9</sub> oligomer intermediates to aromatics.<sup>40</sup> Hersh *et al.*<sup>41</sup> reported reaction of NH<sub>3</sub> with the zinc ions of zinc phosphate glasses to form coordinately bound NH<sub>3</sub>, showing the Lewis nature of the insoluble zinc phosphate. Yuan *et al.*<sup>42</sup> reported the possibility to synthesize hydroxyl zinc phosphate materials by reacting phosphate groups with zinc nitrate. Hence, in order to reduce zinc loss in exchanged bridging hydroxyl groups during MTA process, an incorporation of stabilized phosphorus groups seems to be an attractive alternative. By anchoring the phosphorus group on P/HZSM-5 catalyst with the zinc species to form the insoluble zinc phosphate groups, it may inherit the hydrothermal stability from P-modified catalysts. In addition, the formation of insoluble zinc phosphate groups might

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contribute its Lewis nature for altering the acidity distribution, causing better aromatization properties in MTA reaction, as well as stabilizing the hydroxyl zinc ions by the formation of insoluble zinc phosphate groups.

Herein, we report preparation of Zn-P/HZSM-5 catalyst with isolated zinc phosphate groups, verification of its catalyst performance and characterization of the local structure and chemical state of Zn and its nearest neighbors that shed light on the nature of the Zn-P/HZSM-5 complex. The formation of zinc phosphate groups by adding zinc ions to P/HZSM-5 catalyst is studied by NMR. Detection of possible incorporation of zinc into phosphate groups and characterization of its nearest coordination sphere are accomplished by using XANES and EXAFS techniques in combination with FTIR measurements of the change of bridging hydroxyl groups. The Lewis nature of as-prepared zinc phosphate groups on Zn-P/HZSM-5 catalyst are identified by  $\text{NH}_3$ -TPD (temperature programmed desorption of ammonia) and Py-FTIR (FTIR spectroscopy using pyridine as a probe molecule) measurements. Finally, the catalyst performance of ZnPHZ (short for Zn-P/HZSM-5) in MTA reaction is interpreted by correlating catalyst structure and its acidic properties (the distribution of Brønsted acid and Lewis acid), as well as the comparative research with the reference catalysts including the parent HZSM-5, P/HZSM-5, Zn/HZSM-5 and P-Zn/HZSM-5, denoted as HZ, PHZ, ZnHZ and PZnHZ respectively as mentioned above.

The structural and crystalline characteristics of the samples were studied by XRD (ESI, Fig. S1a†). All of the samples were well crystallized as the MFI structure, as deduced from the XRD spectra. Table 1 shown the relative crystallinity of the samples as compared to the parent HZ sample. The relative crystallinity decreased to a certain extent for sample impregnated with orthophosphoric acid, and this might be due to the dealumination of the zeolite sample, surface modification and thermal treatment. After the addition of zinc to PHZ sample, the crystallinity of HZ for ZnPHZ sample decreased significantly, but the HZ support still kept the origin structure. Synchrotron based XRD (ESI, Fig. S1b†) and scanning TEM (ESI, Fig. S2†) were used to further confirm the absence of zinc oxides or zinc phosphate particles formed on the catalyst surface, indicating that the zinc species was highly dispersed, amorphous or singly bonds to the catalyst surface.

Surface area and micropore analysis datum were listed in Table 1, including the BET surface area ( $S_{\text{BET}}$ ), microporous surface area ( $S_{\text{micro}}$ ), external surface ( $S_{\text{ext}}$ ) and microporous

volume ( $V_{\text{micro}}$ ) of the parent HZ, PHZ and ZnPHZ samples. The results indicated that the BET surface area and microporous surface area were both slightly reduced by impregnation of phosphoric acid to the HZ sample and further reduced by the following introduction of zinc species to PHZ sample meanwhile, the external surface area was gradually increased, which gave the further explanation that both phosphorus acid and zinc ions were impregnated into the pore channels.<sup>47</sup>

MAS NMR spectra of HZ (no. 1), PHZ (no. 2) ZnPHZ (no. 3), reference material  $\text{Zn}_3(\text{PO}_4)_2$ , (no. 4, denoted as r- $\text{Zn}_3(\text{PO}_4)_2$ ) and PZnHZ (no. 5) samples were shown in Fig. 1 as the captions described respectively. Fig. 1a shown the  $^{29}\text{Si}$  spectra of HZ, PHZ and ZnPHZ samples, in which there were four characteristic peaks, had been deconvoluted and identified as  $\text{Q}_4$  [ $\text{Si}(\text{OSi})_4$ ] species (−112.3 ppm), inequivalent  $\text{Q}_4$  [ $\text{Si}(\text{OSi})_4$ ] (−115.9 ppm),<sup>24,48</sup>  $\text{Q}_4$  [ $\text{Si}(\text{OSi})_3(\text{OAl})$ ] (−105.9 ppm) and  $\text{Q}_3$  [ $\text{Si}(\text{OSi})_3(\text{OH})$ ] (−100.0 ppm).<sup>24,47,48</sup> Based on Loewenstein's rule,<sup>49</sup> the framework Si/Al ratio was calculated and list in Table 1.<sup>50</sup> It suggested that  $\text{H}_3\text{PO}_4$  impregnation to HZ sample followed by a subsequent thermal treatment at 550 °C led to sort of dealumination of the framework, whereas the addition of zinc species did not affect the zeolite framework.

Fig. 1b shown the  $^{27}\text{Al}$  MAS NMR spectra of HZ, PHZ and ZnPHZ samples. Typically, the spectra of the HZ sample consist of tetrahedrally coordinated framework sites (~54 ppm,  $\text{Al}_{\text{tet-f}}$ ), distorted tetrahedral coordinated framework sites (30–40 ppm,  $\text{Al}_{\text{tet-dis}}$ )<sup>51</sup> or tetrahedrally coordinated non-framework sites ( $\text{Al}_{\text{tet-nf}}$ ),<sup>52</sup> octahedrally coordinated non-framework aluminum species (−20 to 8 ppm,  $\text{Al}_{\text{oct}}$ )<sup>20</sup> or framework defect sites (−20–8 ppm,  $\text{Al}(\text{OSi})_3(\text{H}_2\text{O})_3$ ,  $\text{Al}_{\text{oct-f}}$ ).<sup>53</sup> For PHZ sample, the band at −8 ppm could be observed due to the association of the octahedral Al sites with phosphorus ( $\text{Al}_{\text{oct-o-p}}$ ).<sup>22,47,54</sup> The broad band appeared at the range of 45 to 15 ppm in comparison to the HZ sample. It suggested the increase of  $\text{Al}_{\text{tet-dis}}$  and  $\text{Al}_{\text{tet-nf}}$  sites, which was correlated with the bonding of Al with phosphorus species. For ZnPHZ sample, the bands at  $\text{Al}_{\text{tet-dis}}$ ,  $\text{Al}_{\text{tet-nf}}$ , and  $\text{Al}_{\text{oct-o-p}}$  sites were decreased, and a sharp band appeared at ~38 ppm. Obviously, all these phenomena suggested that the local environments of both tetrahedrally coordinated Al phosphoric groups and octahedral Al phosphoric groups redeploy after the addition of zinc species, moreover, the octahedral Al phosphoric groups combined with zinc ions to form a new structure.

Fig. 1c showed the  $^{31}\text{P}$  MAS NMR spectra of PHZ, ZnPHZ, PZnHZ samples and r- $\text{Zn}_3(\text{PO}_4)_2$ . The spectrum of PHZ sample

Table 1 Physicochemical characteristics of catalysts

Catalysts	$S_{\text{BET}}$ , $\text{m}^2 \text{g}^{-1}$	$S_{\text{micro}}^a$ , $\text{m}^2 \text{g}^{-1}$	$S_{\text{ext}}^a$ , $\text{m}^2 \text{g}^{-1}$	$V_{\text{micro}}$ , $\text{mL g}^{-1}$	Cry. <sup>b</sup> (%)	$X^c$ , %	$X^d$ , %
HZ	361	226	135	0.104	100	44.2	46.4
PHZ	357	210	147	0.096	91	51.5	53.4
ZnPHZ	349	199	150	0.091	65	50.1	51.1

<sup>a</sup>  $t$ -Plot method. <sup>b</sup> Cry. represents crystallinity based on XRD spectra, estimated by comparing the total XRD peak area of the zeolite sample in range of  $2\theta$  from 22° to 25° with that of the parent HZ having the strongest diffraction intensity. <sup>c</sup>  $X$  represents the Si/Al ratio based on NMR data by using dm2002 software.<sup>50</sup> <sup>d</sup>  $X$  represents the Si/Al ratio based on ICP-AES measurement.



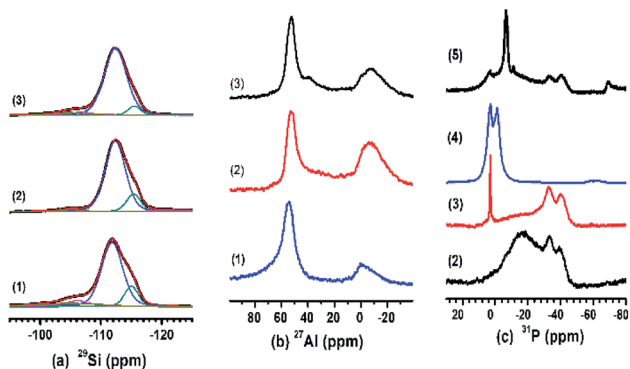


Fig. 1  $^{29}\text{Si}$  (a),  $^{27}\text{Al}$  (b),  $^{31}\text{P}$  (c) MAS NMR spectra of catalysts: (1) HZ, (2) PHZ, (3) ZnPHZ, (4)  $r\text{-Zn}_3(\text{PO}_4)_2$  and (5) PZnHZ.

(Fig. 1c(2)) featured two intensive peaks at  $-39$  ppm ( $(\text{SiO})_x\text{-Al}(\text{OP})_{4-x}$  species<sup>24</sup> with branching P sites in condensed polyphosphate,<sup>55</sup> polyphosphoric species,<sup>20</sup>),  $-33.5$  ppm ( $\text{Al}(\text{H}_2\text{O})_5(\text{PO}_4)^{55-58}$ ) and a broad peak with a maximum at about  $-17$  ppm from  $10$  to  $-40$  ppm (the specific Al-O-P structures, which could be short-chain pyrophosphoric acid or pyrophosphates bonding to non-framework Al<sup>59</sup> or to framework Al<sup>56</sup>). The spectrum of ZnPHZ (Fig. 1c(3)) showed a significant decrease for Al-O-P structures and a slight reduction for  $(\text{SiO})_x\text{-Al}(\text{OP})_{4-x}$  species and  $\text{Al}(\text{H}_2\text{O})_5(\text{PO}_4)$ . Comparison of its spectrum with that of  $r\text{-Zn}_3(\text{PO}_4)_2$ , as shown in Fig. 1c(4), indicated that the transformation of short-chain polyphosphoric species ( $10$ – $40$  ppm) on PHZ sample to zinc phosphate groups ( $3$  ppm) on ZnPHZ occurred. The  $^{31}\text{P}$  NMR spectrum of PZnHZ in Fig. 1c(5) featured a sharp contrast in the bands distribution from  $20$  to  $-80$  ppm, which clearly indicated that only a small amount of zinc phosphate groups showed up, which was totally different in the structure or configuration of zinc and phosphorus species from the ZnPHZ sample. The spectra of PZnHZ sample show that P did see Zn but not too much of it, which meant that zinc ions could find the phosphoric groups to form a new structure – zinc phosphate groups – during the preparation of ZnPHZ sample, whereas such structure was nowhere to

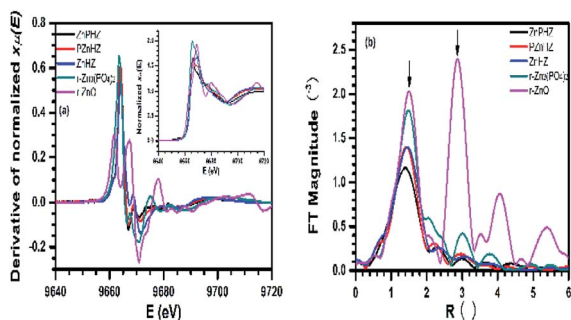


Fig. 2 (a) Derivative of normalized XANES region of absorption coefficient of ZnPHZ, PZnHZ, ZnHZ catalysts and  $r\text{-Zn}_3(\text{PO}_4)_2$  and  $r\text{-ZnO}$  (inset: normalized XANES region of absorption coefficients), and (b) Fourier transform magnitudes of corresponding  $k^2$ -weighted EXAFS spectra.

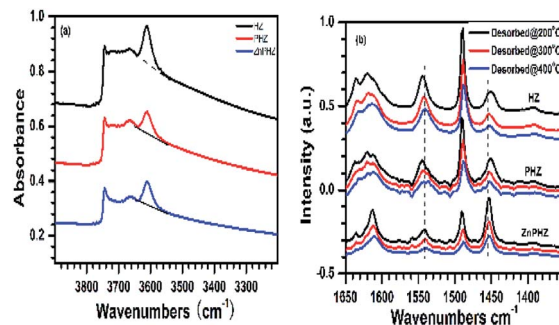


Fig. 3 (a) FTIR spectra measured at  $40$  °C after dehydration at  $450$  °C for  $1$  h and (b) Py-FTIR spectra measured at  $200$  °C,  $300$  °C and  $400$  °C after desorption at the corresponding temperatures of catalysts for: (1) HZ, (2) PHZ, (3) ZnPHZ.

be seen from P-perspective in  $^{31}\text{P}$  NMR spectrum of PZnHZ sample.

XANES spectra<sup>43–45</sup> related to Zn K-edge for ZnPHZ, PZnHZ, and ZnHZ samples and reference materials  $r\text{-Zn}_3(\text{PO}_4)_2$ , and  $r\text{-ZnO}$  (short for zinc oxide) were shown in Fig. 2a. Absorption edge energies (as calculated for the first inflection point of the edge rise) were  $9663.7$  eV for all samples except for the  $r\text{-Zn}_3(\text{PO}_4)_2$  for which the edge energy was  $9663.5$  eV. The XANES spectra of ZnPHZ showed the similar pattern to the  $r\text{-Zn}_3(\text{PO}_4)_2$  but quite different from  $r\text{-ZnO}$ . XANES data (Fig. 2a inset) demonstrated the similarity between Zn micro-environments in ZnPHZ sample and  $r\text{-Zn}_3(\text{PO}_4)_2$ , whereas the whiteline shape of PZnHZ catalyst was close to that in P-free sample of ZnHZ sample. It should be noted that all the samples were measured at room temperature after *in situ* water removal at  $430$  °C to eliminate the effect of water adsorption on XANES spectra. We thus concluded that the similarity of the whiteline shape between ZnPHZ and  $r\text{-Zn}_3(\text{PO}_4)_2$  accounts for the similar structures of phosphane groups that had different concentrations.

Fourier transforms (FT)-EXAFS data was shown in Fig. 2b. The peak positions were lower than real-space distances between Zn atoms and its nearest neighbors due to the photoelectron phase shift, not corrected for in Fig. 2b. The peak around  $1.60$  Å for  $r\text{-Zn}_3(\text{PO}_4)_2$  in the FT magnitude (shown by an arrow in Fig. 2b), which was attributed to the nearest oxygen neighbors with the bond Zn–O–P,<sup>60</sup> corresponded to a Zn–O bond length of  $2.04$  Å. The second main peak around  $3.05$  Å was

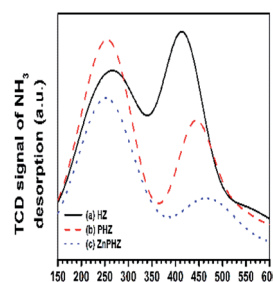


Fig. 4  $\text{NH}_3$ -TPD profiles of catalysts: (a) HZ, (b) PHZ, (c) ZnPHZ.



associated with the bond of Zn-P with the actual bond length of 3.28 Å. In order to quantitatively analyze the local structure of zinc species, data analysis of EXAFS spectra (ESI, Fig. S6†) was performed by using IFEFFIT package.<sup>61–63</sup> Theoretical photoelectron scattering amplitudes and phase shifts of Zn–O and Zn–P contributions were generated by FEFF6 software<sup>64</sup> using crystal structure of  $r\text{-Zn}_3(\text{PO}_4)_2$ . The passive electron reduction factor was fixed to 1.0, as found from the fit to the  $r\text{-ZnO}$ . The results obtained for the ZnPHZ system demonstrated that each Zn ion in the nearest coordination shell was surrounded on average by  $3.5 \pm 0.6$  Å of O atoms with a coordination distance  $1.95 \pm 0.02$  Å and mean squared bond length disorder  $\sigma^2 = 0.011 \pm 0.005$  Å<sup>2</sup>. Relatively large uncertainties prevented us from accurately measuring the number of Zn–P species in the second shell because of the correlation of the coordination numbers and bond length disorder in the fitness. Alternative models were compared, in which we added the Zn–Zn contribution (calculated theoretically using  $r\text{-ZnO}$  structure) as a possible second neighbor to Zn instead, or in addition to, Zn–P, but no reasonable results were obtained. Notably, we found that a model where Zn–Zn was the only contribution to the second coordination shell, as in the local structure of  $r\text{-ZnO}$ , was not consistent with the experimental spectra.

For PZnHZ sample, each Zn ion in the nearest coordination shell was surrounded on average by  $3.9 \pm 0.5$  Å of O atoms with a coordination distance  $1.96 \pm 0.01$  Å and  $\sigma^2 = 0.008 \pm 0.002$  Å<sup>2</sup>; for ZnHZ sample, each Zn ion in the nearest coordination shell was surrounded on average by  $4.1 \pm 0.6$  Å of O atoms with a coordination distance  $2.01 \pm 0.01$  Å and  $\sigma^2 = 0.008 \pm 0.002$  Å<sup>2</sup>. The main summary of the above results was that the Zn–O bond length changed significantly from PZnHZ to ZnHZ sample, whereas the coordination number was similar for the two samples. Such coordination number of *ca.* 4.0 of Zn–O was in agreement with the reported structure of ZnHZ catalyst measured after water removal,<sup>65</sup> which suggested Zn species were in a similar coordination environments in the first shell for both PZnHZ and ZnHZ samples. The shorter average Zn–O bond length in the former catalyst was consistent with the contribution of phosphate groups to the nearest environment of zinc ions, because the bond length of Zn–O in Zn–O–P groups in Hopeite structure varied from 1.90 to 2.05 Å (ESI, Fig. S7†), hence, had a fraction of shorter bonds compared to the ZnHZ system.

In brief, the EXAFS fitting results, taking together with other evidences from XANES, NMR and catalytic tests, supported the idea that both zinc species and phosphate groups existed as the form of zinc phosphate groups on ZnPHZ sample, which quite differentiated from those on ZnHZ and PZnHZ samples. The absence of Zn–Zn bond further suggested that the presence of these zinc phosphate groups was isolated.

Fig. 3a displayed FTIR spectra of the HZ, PHZ, and ZnPHZ samples. It could be clearly seen there were four hydroxyl bands, assigned as amorphous silica hydroxyl groups ( $3740\text{ cm}^{-1}$ ),<sup>66</sup> terminal framework silanols (Si–OH,  $3720\text{ cm}^{-1}$ ),<sup>67</sup> extra-framework aluminum species or partially hydrolyzed aluminum species ( $3660\text{--}3690\text{ cm}^{-1}$ ),<sup>68</sup> and bridging hydroxyl groups Si(OH)Al ( $3610\text{ cm}^{-1}$ ).<sup>69</sup> Both bands for P–OH groups<sup>41</sup> at  $3666\text{ cm}^{-1}$  and bands for Zn–OH groups<sup>41</sup> at  $3620\text{--}3674\text{ cm}^{-1}$  were not discerned

since they were obscured by the bands of Si–OH, Al–OH. It should be noted that the bands at  $3610\text{ cm}^{-1}$  were specific to the bridged hydroxyl groups. The peak height of the band at  $3610\text{ cm}^{-1}$  decreased when phosphorus was impregnated to HZ sample, suggesting that part of the bridging hydroxyl groups (Brönsted acid site) were eliminated by reacting with orthophosphoric acid. On the contrary, the bridging hydroxyl groups kept unchanged or even stronger when zinc was further impregnated to PHZ sample, indicating zinc ions were not exchanged with the bridging hydroxyl groups, properly evidenced that zinc ions reacted with phosphorus groups to form zinc phosphate groups.

Py-FTIR spectra of HZ, PHZ, and ZnPHZ samples after pyridine desorption at different temperatures were shown in Fig. 3b. The characteristic bands<sup>67,70</sup> were clearly observed at  $\sim 1450\text{ cm}^{-1}$  for Lewis acid sites and at  $1540\text{ cm}^{-1}$  for Brönsted acid sites. For both the different conditions of samples at the same temperature and the same catalyst at the different desorption temperature, the bands for Brönsted acid sites shifted to lower wavenumbers, whereas the bands for Lewis acid sites to higher wavenumbers. It was demonstrated that both Lewis acid sites and Brönsted acid sites had different strength of acid sites existed on the zeolite surface. Quantification of weak, medium, and strong acid sites for Brönsted and Lewis acid sites was performed according to the amount of pyridine desorption at different temperature by the same way as everywhere.<sup>2,35</sup> To allow semi-quantitative comparisons of the peak intensities, all Py-FTIR spectra were normalized using the area of the overtone lattice vibration bands of the zeolites at  $1990\text{ cm}^{-1}$  and  $1873\text{ cm}^{-1}$ , as conducted in the literatures.<sup>2,36,71</sup> Fig. 4 showed the acidities of different samples measured by  $\text{NH}_3\text{-TPD}$  method.<sup>15,40,72–76</sup> It was found that for HZ, PHZ and ZnPHZ samples: (1) the relative total acidity amount was 100%, 99.4% and 78.3%; (2) the weak acid amount was 100%, 128.1% and 118.8%; and (3) strong acid amount was 100%, 69.6%, and 35.4% respectively (ESI, details showed in Fig. S3†).

The effect of the reaction time on methanol conversion over ZnPHZ sample was shown in Fig. 5a. It could be seen that the catalyst exhibited a stable performance during the reaction procedure. All of the yields of  $\text{C}_1\text{--C}_5^+$  and benzene ( $\text{C}_6\text{A}$ )

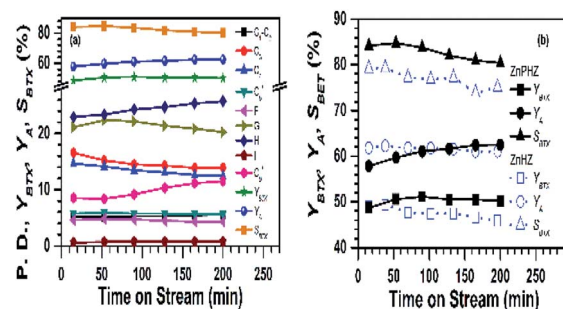


Fig. 5 (a) Product distribution (P. D.) of MTA reaction for catalyst ZnPHZ; (b) yield of BTX (YBTX), yield of aromatics (YA), selectivity to BTX (SBTX) of catalyst ZnPHZ in comparison with reference catalyst ZnHZ. Reaction conditions: 0.1 MPa,  $430^\circ\text{C}$ , 3.0 g catalyst, WHSV =  $2.0\text{ h}^{-1}$ .





hydrocarbons slightly decreased with time on stream (TOS), while the yields of toluene initially increased and then steadily remained. The  $C_9^+$  aromatics ( $C_9^+A$ ) yield continuously increased as prolong the reaction time. These phenomena implied that BTX and  $C_9^+$  aromatics might be produced through a common intermediate, such as ( $C_6^--C_9^+$ ) oligomer intermediates. The yield of BTX ( $Y_{BTX}$ ) was stable, and the selectivity to BTX shown only a slightly decrease due to the yield of total aromatics ( $Y_A$ ) slightly increased. For HZ, PHZ and ZnHZ catalyst, all showed the similar function in the effect of the reaction time on methanol conversion (ESI, Fig. S8†). Fig. 5b compared the performances of ZnHZ and ZnPHZ catalysts under the same reaction conditions. It clearly showed that ZnPHZ catalyst owned better selectivity to BTX.

Table 2 and Fig. S8† displayed the catalytic reactivity of ZnPHZ catalyst in the conversion of methanol to light aromatics, including the HZ, PHZ, ZnHZ, and PZnHZ catalysts. Methanol was completely converted on all catalysts under the same reaction conditions. The differences in the reaction performance could be attributed to changes in the nature of the catalytic sites present: (1) the parent HZ catalyst exhibited only 25.61% yield of BTX and 75.58% selectivity to BTX; By addition of Zn to PHZ, the ZnPHZ catalyst showed 50.59% yield of BTX (32.85% for PHZ) and 84.73% selectivity to BTX (81.89% for PHZ); (2) ZnPHZ catalyst showed different product distribution (featured as lower  $C_1-C_5^+$  light hydrocarbons and significantly lower  $C_9^+$  aromatics) from the ZnHZ catalyst; (3) toluene and xylene were the main products in the MTA reaction for all the catalysts, among which ZnPHZ catalyst had the maximal values of 22.39% and 23.40% for  $Y_T$  and  $Y_X$ , respectively; (4) ZnPHZ catalyst exhibited the superior performance to the reference catalysts, ZnHZ and PZnHZ samples. W. D. Xiao<sup>82</sup> *et al.* reported a MTA catalyst, HZSM-5 zeolite catalyst ( $SiO_2/Al_2O_3 = 30$ ) modified by 1.0 wt% ZnO and 2.0 wt% P, by using of the special titanium made U-shaped reactor, in the reaction condition of temperature range from 380 to 480 °C, pressure:15–50 kPa, obtained the best aromatic product:  $Y_A = 59.61\%$ , with  $Y_B = 8.50\%$ ,  $Y_T = 27.70\%$ ,  $Y_X = 20.18\%$ , which exhibited nearly the same yield of aromatics, slightly different to the PZnHZ catalyst in the BTX distribution, owing to the different content of Zn and P. Meanwhile, this MTA catalyst, similar to ZnPHZ catalyst, should contain the isolated zinc phosphate groups.

## Discussion

The IZPG (short for isolated zinc phosphate groups), as we mentioned above, were perfectly evidenced by XANES and EXAFS methods, as well as FTIR measurements. From the procedure of catalyst preparation method,<sup>47</sup> the local micro-environment of could be further deduced from the principal phosphorus groups which were confirmed to bond with zinc ions. As from the results of  $^{27}Al$  NMR spectra of ZnPHZ catalyst (ESI, Fig. S4†), the descent of  $Al_{tet-dis}$ ,  $Al_{tet-nfr}$  and  $Al_{oct-o-p}$  and an emerging sharp band at *ca.* 38 ppm suggested that the transformation of both tetrahedrally Al phosphoric groups and octahedrally Al phosphoric groups to zinc phosphoric groups took place. Meanwhile, from the  $^{31}P$  MAS NMR spectra (ESI, Fig. S5†), different amounts of zinc addition also demonstrates that  $(SiO)_xAl(OP)_{4-x}$  species (−39 ppm) gradually decreased, the nonreactive  $Al(H_2O)_5(PO_4)$  species (−33.5 ppm) remained unchanged, whereas the amount of zinc phosphate groups (3 ppm) increased step by step and the principal peak centred on −17 ppm was related to the specific Al–O–P structures, which could be assigned to short-chain pyrophosphoric acid or pyrophosphates bonding to non-framework  $Al^{59}$  or to framework  $Al^{55}$  and revealed systematic increase occurred at the bands of all distorted tetrahedral Al sites and a systematic decrease in octahedral Al sites. On the other hand, only a slight fluctuation appeared at the peak of tetrahedral Al sites (Brönsted acid sites) as the increase of zinc amount from 0 to 3.0% to PHZ catalyst. It was a compelling proof that preferential reaction between phosphorus groups and zinc ions took place by adding zinc ions to PHZ catalyst.

This unique structure of IZPG was also confirmed in comparison with the zinc environment of ZnHZ and PZnHZ samples, from the EXAFS data in *r*-space (ESI, Fig. S5†), the zinc micro-environment of ZnHZ and PZnHZ samples, exhibited a similar fluxion, which meant the coordination environments for both catalysts was similar, but quite different from ZnPHZ sample. It was also expected that the lower intensity of the Zn–O peak suggested a lower coordination numbers for Zn–P bonds in the ZnPHZ system compared to the PZnHZ and ZnHZ samples, as well as  $r-Zn_3(PO_4)_2$ , consistent with the conclusion made by examination of the XANES data (*vide supra*) that zinc phosphate groups were generated on ZnPHZ sample during the procedure of adding zinc ions to PHZ

Table 2 Reactivity of HZ, PHZ, ZnPHZ and ZnHZ catalysts in MTA

Catalysts	Yields (wt%)									$Y_{BTX}$ (wt%)	$Y_A$ (wt%)	$S_{BTX}$ (%)
	$C_1 + C_2$	$C_3$	$C_4$	$C_5^+$	B	T	X	EB	$C_9^+$	BTX	A	S
HZ	5.61	22.47	24.74	13.29	2.60	9.99	13.01	0.82	7.45	25.61	33.89	75.58
PHZ	5.15	27.51	21.09	6.14	4.07	13.78	15.00	0.64	6.62	32.85	40.12	81.89
ZnPHZ	5.08	15.20	14.13	5.89	4.80	22.39	23.40	0.74	8.37	50.59	59.70	84.73
ZnHZ <sup>a</sup>	6.17	12.16	12.98	6.90	3.27	18.24	26.20	0.87	13.20	47.71	61.78	77.23
PZnHZ <sup>a</sup>	7.85	13.89	14.09	11.45	2.38	14.23	19.87	1.32	13.75	33.00	47.13	70.01

<sup>a</sup> Data point: TOS@60 min; B = benzene, T = toluene; X = xylene;  $C_5^+$  = alkanes and olefins with  $C_5$  and plus;  $C_9^+$  = aromatics with  $C_9$  and plus; A = total aromatics.



catalyst. However, upon adding phosphoric acid to ZnHZ sample, the structure of zinc just slightly changed as evidenced in  $^{31}\text{P}$  NMR spectra. It should be noted that the amount of zinc phosphate groups on PZnHZ sample should be very low, if any.

From  $\text{NH}_3$ -TPD and Py-FTIR<sup>80,81</sup> results, we could further find the IZPG not only altered the acid strength distribution of the zeolite surface but also affected the total acidic amounts. As shown in Fig. 6 and Table S2,<sup>†</sup> the contributions of Lewis nature of IZPG could be deduced from the results by the ascent of Lewis acid distribution. *Via* the addition of zinc ions to PHZ sample, the summit of Lewis acid sites was shifted to a higher frequency, and indicated that zinc phosphate groups act as strong Lewis acid sites. It was reported that the reduction of the bridging hydroxyl groups (Brönsted acid sites) derived from its reaction with the supported orthophosphorus acid,<sup>77,78</sup> or as a result of the lattice dealumination by the dislodged aluminum species reacting with  $\text{H}_3\text{PO}_4$ ,<sup>47</sup> which interpreted the reduction of the strong acid peak in the curve of  $\text{NH}_3$ -TPD in the temperature range between 300–600 °C (Fig. 4). Meanwhile, the impregnation of HZ with phosphoric acid was accompanied by the creation of Brönsted acid sites with an acid strength lower than that of the bridging hydroxyls.<sup>22,66</sup>

It was thus the acid amount lost by the reduction of Brönsted acid sites or the other acid sites could be compensated by ammonia uptakes from phosphorus hydroxyl groups, which accounted for the total acid amount of PHZ sample was close to the HZ sample, which meant, the phosphoric groups reacted with zinc ions and further transformed to zinc phosphate groups. The loss of acid amount of ZnPHZ sample should be ascribed to the elimination of P–OH groups by the combination of zinc ions and P–OH groups. Therefore, the total acid amount was further reduced. It could be also concluded that the transformation from phosphate groups to zinc phosphate groups increased the high temperature peak of ammonia desorption from 444 °C to 470 °C from Fig. S3 and Table S1.<sup>†</sup> Therefore, the strength of IZPG could be identified as strong Lewis acid sites in agreement with the result.

Fig. 6 plotted the specific yield of BTX, yield of total aromatics and selectivity to BTX in correlation with the corresponding acidic distribution was plotted by It exhibited that

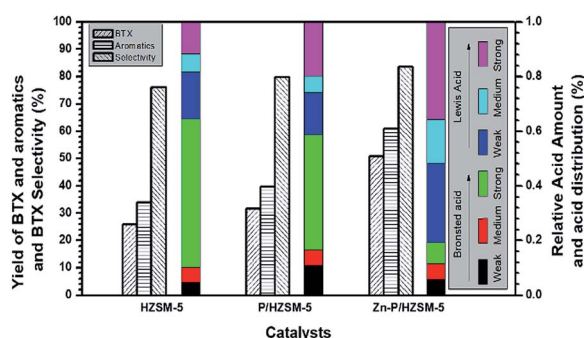


Fig. 6 Relationship between yields of BTX, aromatics and BTX selectivity, in MTA reaction, and the distribution of different type of acidic sites in weak, medium and strong acidic strength for HZ, PHZ, and ZnPHZ respectively. Reaction conditions see Fig. 5.

a significant increase was obtained over ZnPHZ catalyst with the change of the acidic distribution. As known to all, the acidic distribution of catalyst played an important role in the catalytic reactivity. The catalyst should have a moderate B/L ratio so as to obtain the high BTX yield, which preferable contribute the formation of BTX and also suppressed the generation of carbon, coke and heavy aromatics.<sup>2,36,40</sup> According to the reaction mechanism reported,<sup>2,6,40</sup> it could be deduced that the cracking or methylation of  $\text{C}_6^+=\text{C}_9^-$  oligomer intermediates was suppressed over ZnPHZ catalyst leading to the decrease of  $\text{C}_1$ – $\text{C}_5$  fraction and  $\text{C}_9^+$  aromatics, whereas the dehydrogenation reaction of  $\text{C}_6^+=\text{C}_8^-$  oligomer intermediates was enhanced over ZnPHZ catalyst leading to the high BTX selectivity. It was well accepted that exchanged zinc ions promoted the desorption of H atoms to  $\text{H}_2$ , which greatly restrained hydrogen transfer to olefins but facilitate dehydrogenation of cyclic olefins to produce aromatics.<sup>40</sup> In this case, IZPG might play a similar role as ZnHZ catalyst but with more suitable acidity distribution and better hydrothermal stability, as well as the MTA catalyst, Zn and P co-modified HZSM-5.<sup>35,36,82</sup>

As it is known to all, for the MTA process, zinc play the most popular enroller, employed by HZSM-5 zeolite, which associated with the acidic sites of zeolite framework, generated more Lewis acid ( $\text{ZnOH}^+$ ,  $\text{Zn}^{2+}$ -L acid center), make the catalyst more effective to convert the intermediate olefins into aromatics by dehydrogenation, *via* the expense of the silanol hydroxyl and proton acid sites. And the impregnation of phosphorus to ZSM-5 can also adjust the acidity of zeolite and improve its hydrothermal stability, but excessive introduction of P could lead to the covering of Brönsted acid sites and blockage of pores, resulting in MTA activity decreased.

In the methanol to hydrocarbon (MTH) reaction, both Brönsted acid sites and Lewis acid sites can regulate the conversion of methanol to dimethyl ether and the further formation of DME to low-carbon olefins ( $\text{C}_2^+=\text{C}_3^-$ ), the polymerization of low-carbon olefins to high-carbon olefins ( $\text{C}_4^+=\text{C}_8^-$ ). Brönsted acid sites can also catalyse the cyclization of higher olefins and the hydrogen transfer of cycloalkanes. In order to maximize the performance of certain MTA catalyst with IZPG species, there should be kept counterbalance of Brönsted acid sites to Lewis acid sites (B to L) ratio nearly 0.2, as Fig. 6 and Table S2<sup>†</sup> showed.

Table 3 and Fig. S9<sup>†</sup> shown the reactivity of the fresh ZnPHZ catalyst and the regenerated catalysts. Technically speaking, fixed bed reactor is not suitable for MTA process due to the deactivation rate.<sup>4,16,79</sup> In the present research, the catalyst was operated in the fixed bed reactor for 240 min, then the reaction was terminated to regenerate *in situ* to simulate the fluidized bed reaction for testing the stability of ZnPHZ catalyst. As indicated in Table 3, ZnPHZ catalyst exhibited excellent recoverable performance during as many as 5 cycles of reaction-regeneration were carried out. Only a slightly decrease could be found in the yield of BTX. It was pronounced that such catalyst has a robust structure with good thermal and hydrothermal stabilities. Table 4 summarized the Zn and P contents for the fresh and regenerated catalysts after reaction-regeneration cycles. The initial P and Zn contents in the fresh



Table 3 Reactivity of fresh ZnPHZ catalyst and regenerated catalyst<sup>a</sup>

Run no.	Yields (wt%)									$Y_{\text{BTX}}$ (wt%)	$Y_{\text{A}}$ (wt%)	$S_{\text{BTX}}$ (%)
	$\text{C}_1 + \text{C}_2$	$\text{C}_3$	$\text{C}_4$	$\text{C}_5^+$	B	T	X	EB	$\text{C}_9^+$	BTX	Aromatics	Selectivity
0	5.08	15.20	14.13	5.89	4.80	22.39	23.40	0.74	8.37	50.59	59.70	84.73
1	5.69	14.82	13.78	5.96	4.52	21.55	23.95	0.74	8.99	50.01	59.74	83.71
2	5.97	15.02	14.18	6.37	4.26	20.66	23.83	0.75	8.98	48.74	58.47	83.37
3	6.21	14.88	14.33	6.71	4.14	20.41	23.56	0.78	8.97	48.12	57.87	83.15
4	6.60	15.10	14.70	6.71	4.19	20.51	23.15	0.74	8.29	47.85	56.88	84.11
5	6.77	15.09	14.87	6.98	4.11	20.36	22.82	0.78	8.22	47.30	56.30	84.01

<sup>a</sup> Data point: TOS@60 min; B = benzene, T = toluene; X = xylene;  $\text{C}_5^+$  = alkanes and olefins with  $\text{C}_5$  and plus;  $\text{C}_9^+$  = aromatics with  $\text{C}_9$  and plus; A = total aromatics.

Table 4 Zn and P contents of the fresh and regenerated catalysts

Components	Fresh (wt%)	Regenerated (wt%) after each cycle					
		1 <sup>a</sup>	2 <sup>a</sup>	3 <sup>a</sup>	4 <sup>a</sup>	5 <sup>a</sup>	6 <sup>a</sup>
P@ZnPHZ	0.97	0.96	0.94	0.93	0.93	0.95	0.91
Zn@ZnPHZ	0.75	0.76	0.75	0.73	0.70	0.62	0.59
Zn@ZnHZ	0.73	0.53	—	—	—	—	—

<sup>a</sup> Regenerated catalysts analyzed using ICP-AES after each reaction-regeneration cycle. Prior to each cycle, the used catalyst were calcined in air at 550 °C for 240 min for coke removal.

ZnPHZ catalyst were 0.97% and 0.75% respectively. After each reaction-regeneration cycle, the content of P remains almost unchanged for all the 6 times running. Meanwhile, the final zinc content decreased slightly from 0.75% to 0.59% after 6 times running. For the ZnHZ catalyst, the zinc content definitely decreased from 0.73% to 0.53% after first run. It is also confirmed that the loss of zinc<sup>15,29–31</sup> took place for ZnHZ catalyst, while the ZnPHZ catalyst stabilized the phosphorus and zinc by the form of isolated zinc phosphate groups and further extended the ZnPHZ catalyst recycle regeneration times above 20 can be seen in Fig. S10.†

## Experimental procedures

### Catalyst preparation

The starting material, HZSM-5 with silica to alumina mole ratio of 100, was purchased from Shanghai Fuxu Molecular Sieves Co (China). PHZ catalyst, loading with 1.0 wt% phosphorus, was prepared by wetness impregnation as follows: (a) the impregnation solution was prepared by mixing 31.6 g of aqueous solution of orthophosphoric acid (10 wt%,  $\text{H}_3\text{PO}_4$ ) and 118.4 g  $\text{H}_2\text{O}$  at room temperature; (b) 100 g of HZSM-5 zeolite was added to the solution (a) with stirring at room temperature until dryness for over 5 hours; (c) the impregnated sample was subsequently dried at 393 K overnight and then calcined at 450 °C for 4 h. The ZnPHZ<sup>46</sup> (0.75 wt% zinc), was prepared by adding the 10.0 g P/HZSM-5 catalyst to 15.0 g of  $\text{Zn}(\text{NO}_3)_2$  solution (2.30 wt%,  $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ), followed by the same stirring, drying and calcination procedure as for the PHZ

catalyst. ZnHZ catalyst, with the Zn loading of 0.75 wt%, was prepared similar to ZnPHZ catalyst by impregnating HZ with  $\text{Zn}(\text{NO}_3)_2$  solution. The reference catalyst PZnHZ was prepared by impregnating ZnHZ with orthophosphoric acid. All the reference catalysts were prepared with the same P and Zn loading weight as ZnPHZ.

### Characterization

Surface area and micropore analysis were analyzed by nitrogen physisorption data (Micromeritics Tristar 3000, conducted in Sinopec SRIPT). The crystallinity of catalysts was measured by powder X-ray diffraction (Bruker Advance D8, conducted in Sinopec SRIPT; Beamline 14A of the National Synchrotron Light Source at Brookhaven National Laboratory). Scanning Transmission Electron Microscopy is used for confirmation of the absence of zinc oxide particles and the catalyst crystallinity of ZnPHZ (JEOL ARM200F, conducted in Hefei, China). NMR measurements were conducted at Sinopec SRIPT for <sup>29</sup>Si, <sup>27</sup>Al and <sup>31</sup>P MAS NMR spectra (Varian VNMR 400).

XAFS measurements were performed to identify the chemical states of zinc species. XAFS measurements were done at beamline X19A of the National Synchrotron Light Source at Brookhaven National Laboratory and Beamline BL2-2 of the Stanford Synchrotron Radiation Light source. The catalyst sample was grounded to fine powder and pressed into a pellet. All spectra were collected at room temperature after water removal at 430 °C in transmission mode.

Hydroxyl surface groups of HZ catalysts were characterized by Fourier Transform Infrared Spectroscopy (Nicolet 5700, conducted in Sinopec SRIPT).  $\text{NH}_3$ -TPD (Set up by Sinopec SRIPT) and Py-FTIR (Nicolet 380, conducted in Sinopec SRIPT) measurements were conducted to measure the catalyst acidity amount and the distribution of acidity type. Chemical analysis of the zeolite samples was performed by Inductively Coupled Plasma-Atomic Emission Spectrometry (ICP-AES, conducted in Sinopec SRIPT). The details are given in ESI.†

### Reaction evaluation

The HZ, PHZ, and ZnPHZ catalysts, as well as the reference catalyst ZnHZ, were respectively pressed, crushed and sieved to



obtain particles in the range of 12–20 mesh (1.4–1.7 mm) for catalytic evaluation in Sinopec SRIPT. Prior to the reaction, the catalysts were blown out with flowing nitrogen at 430 °C for 2 h. Methanol conversion was performed in a stainless-steel fixed bed reactor (650 mm length and 10 mm i.d.). The reaction conditions were weight hourly space velocity (WHSV) = 2.0 h<sup>-1</sup>, reaction temperature of 430 °C and atmospheric pressure. Methanol and the products were analyzed by an online gas chromatograph (Agilent GC-7890) with a flame ionization detector (FID). The tubing between outlet of the reactor and GC was kept at 240 °C for prohibiting the reaction products from condensing. The methanol conversion, BTX selectivity and yield of the products were calculated from the number of C atoms in the products.

## Conclusions

We demonstrated that isolated zinc phosphate groups can be successfully anchored to HZSM-5 zeolite channel network prepared by impregnating zinc ions to P-modified HZSM-5 catalyst, which has a good hydrothermal stability and a suitable Lewis acidity regulating the acidity distribution. The stable zinc phosphate groups on ZnPHZ enhance the hydrogen-transfer pathway to high BTX selectivity and suppress the methylation of BTX to heavy aromatics. This research may provide an alternative way to the effective MTA catalyst design for achieving high BTX selectivity and inhibiting the formation of heavy aromatics (C<sub>9</sub><sup>+</sup>) with good thermal and hydrothermal stabilities.

## Conflicts of interest

There are no conflicts to declare.

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## References

- 1 X. Niu, J. Gao, Q. Miao, M. Dong, G. Wang, W. Fan, Z. Qin and J. Wang, Influence of preparation method on the performance of Zn-containing HZSM-5 catalysts in methanol-to-aromatics, *Microporous Mesoporous Mater.*, 2014, **197**, 252–261.
- 2 G. Zhang, T. Bai, T. Chen, W. Fan and X. Zhang, Conversion of Methanol to Light Aromatics on Zn-Modified Nano-HZSM-5 Zeolite Catalysts, *Ind. Eng. Chem. Res.*, 2014, **53**(39), 14932–14940.
- 3 F. Wang, W. Xiao and G. Xiao, Atomic layer deposition of zinc oxide on HZSM-5 template and its methanol aromatization performance, *Catal. Lett.*, 2015, **145**, 860–867.
- 4 T. Wang, X. Tang, X. Huang, W. Qian, Y. Cui, X. Hui, W. Yang and F. Wei, Conversion of methanol to aromatics in fluidized bed reactor, *Catal. Today*, 2014, **233**(15), 8–13.
- 5 Y. Ono, H. Adachi and Y. Senoda, Selective conversion of methanol into aromatic hydrocarbons over zinc-exchanged ZSM-5 zeolites, *J. Chem. Soc., Faraday Trans. 1*, 1988, **84**, 1091–1099.
- 6 Y. Xin, P. Qi, X. Duan, H. Lin and Y. Yuan, Enhanced performance of Zn–Sn/HZSM-5 catalyst for the conversion of methanol to aromatics, *Catal. Lett.*, 2013, **143**, 798–806.
- 7 H. Jing, F. Yang, Y. Xia, J. Peng, J. Liu and Q. Zong, A study on the selectivity of methanol aromatization, *Pet. Sci. Technol.*, 2012, **30**(16), 1737–1746.
- 8 F. Yang, S. Wang, Y. Xia, W. Bi and W. Wang, Study on Methanol Aromatization over Zeolite Catalyst H/ZSM-5 Modified with Zinc Ions in Different Contents, *Pet. Sci. Technol.*, 2011, **29**(16), 1675–1684.
- 9 Y. Ni, A. Sun, X. Wu, J. Hu, T. Li and G. Li, Aromatization of Methanol over La/Zn/HZSM-5 Catalysts, *Chin. J. Chem. Eng.*, 2011, **19**(3), 439–445.
- 10 Y. Ni, A. Sun, X. Wu, G. Hai, J. Hu, T. Li and G. Li, The preparation of nano-sized H [Zn, Al] ZSM-5 zeolite and its application in the aromatization of methanol, *Microporous Mesoporous Mater.*, 2011, **143**(2–3), 435–442.
- 11 Y. Ni, W. Peng, A. Sun, W. Mo, J. Hu, T. Li and G. Li, High selective and stable performance of catalytic aromatization of alcohols and ethers over La/Zn/HZSM-5 catalysts, *J. Ind. Eng. Chem.*, 2010, **16**(4), 503–505.
- 12 Y. Inoue, K. Nakashiro and Y. Ono, Selective conversion of methanol into aromatic hydrocarbons over silver-exchanged ZSM-5 zeolites, *Microporous Mater.*, 1995, **4**(5), 379–383.
- 13 H. Ji, Q. Zhang, L. Chen and H. Shan, Study on the reaction performance of methanol to aromatics over Zn/HZSM-5 catalysts with alumina, *J. Fuel Chem. Technol.*, 2014, **42**(11), 1387–1393.
- 14 Y. Bi, Y. Wang, X. Chen, Z. Yu and L. Xu, Methanol aromatization over HZSM-5 catalysts modified with different zinc salts, *Chin. J. Catal.*, 2014, **35**(10), 1740–1751.
- 15 V. Abdelsayed, D. Shekhawat and M. Smith, Effect of Fe and Zn promoters on Mo/HZSM-5 catalyst for methane dehydroaromatization, *Fuel*, 2015, **139**(1), 401–410.
- 16 T. Tian, W. Qian, X. Tang, S. Yun and F. Wei, Deactivation of Ag/ZSM-5 Catalyst in the Aromatization of Methanol, *Acta Phys.-Chim. Sin.*, 2010, **26**(12), 3305–3309.
- 17 J. Song, Z. Di, C. Yang and J. Wu, Preparation of Small Crystalline ZSM-5 and its Application in Conversion of Methanol to Aromatic, *Adv. Mater. Res.*, 2012, **457–458**, 245–248.
- 18 H. Van der Bij, F. Meirer, S. Kalirai, J. Wang and B. Weckhuysen, Hexane Cracking over Steamed Phosphated Zeolite H-ZSM-5: Promotional Effect on





- Catalyst Performance and Stability, *Chem.-Eur. J.*, 2014, **20**(51), 16922–16932.
- 19 J. Otterstedt, Y. Zhu and J. Sterte, Effects of matrix alumina-silica ratio on the performance of heavy oil cracking catalysts containing zeolite Y in matrices of amorphous silica-alumina, *Appl. Catal.*, 1991, **70**(1), 43–52.
  - 20 T. Blasco, A. Corma and J. Triguero, Hydrothermal stabilization of ZSM-5 catalytic-cracking additives by phosphorus addition, *J. Catal.*, 2006, **237**(2), 267–277.
  - 21 G. Caeiro, P. Magnoux, M. Lopes, F. Ribeiro, S. Menezes, A. Costa and H. Cerqueira, Stabilization effect of phosphorus on steamed H-MFI zeolites, *Appl. Catal.*, A, 2006, **314**(2), 160–171.
  - 22 G. Lischke, R. Eckelt, G. Jerschke, B. Parltitz, E. Schreier, W. Storek, B. Zibrowius and G. Öhlmann, Spectroscopic and physicochemical characterization of P-Modified H-ZSM-5, *J. Catal.*, 1991, **132**(1), 229–243.
  - 23 G. Yang, J. Zhuang, Y. Wang, D. Zhou, M. Yang, X. Liu, X. Han and X. Bao, Enhancement on the hydrothermal stability of ZSM-5 zeolites by the cooperation effect of exchanged lanthanum and phosphoric species, *J. Mol. Struct.*, 2005, **737**(1–2), 271–276.
  - 24 J. Zhuang, D. Ma, G. Yang, Z. Yan, X. Liu, X. Liu, X. Han, X. Bao, P. Xie and Z. Liu, Solid-state MAS NMR studies on the hydrothermal stability of the zeolite catalysts for residual oil selective catalytic cracking, *J. Catal.*, 2004, **228**(1), 234–242.
  - 25 M. Kaarsholm, F. Joensen, J. Nerlov, R. Cenni, J. Chaouki and G. Patience, Phosphorous modified ZSM-5: Deactivation and product distribution for MTO, *Chem. Eng. Sci.*, 2007, **62**(18–20), 5527–5532.
  - 26 W. Kaeding, C. Chu, L. Young and S. Butter, Shape-selective reactions with zeolite catalysts: II. Selective disproportionation of toluene to produce benzene and p-Xylene, *J. Catal.*, 1981, **69**(2), 392–398.
  - 27 W. Kaeding, C. Chu, L. Young, B. Weinstein and S. Butter, Selective alkylation of toluene with methanol to produce para-Xylene, *J. Catal.*, 1981, **67**(1), 159–174.
  - 28 C. Chu, Aromatization reactions with zeolites containing phosphorus oxide. US Patent 4590321, 1986.
  - 29 H. Long, F. Jin, G. Xiong and X. Wang, Effect of lanthanum and phosphorus on the aromatization activity of Zn/ZSM-5 in FCC gasoline upgrading, *Microporous Mesoporous Mater.*, 2014, **198**(1), 29–34.
  - 30 Y. Li, W. Wu, E. Min and B. Sun, Intrinsic kinetics of ammoxidation of cyclohexanone to cyclohexanone oxime over HTS zeolite, *Pet. Process. Petrochem.*, 2003, **34**(11), 39–43.
  - 31 Y. Zhao, C. Cao, K. Tang and X. Hong, The Aromatization of Different FCC Naphtha Fractions over a P-Zn/HZSM-5 Catalyst, *Pet. Sci. Technol.*, 2011, **29**(10), 1009–1015.
  - 32 L. Zhao, J. Zhu, H. Wang, M. Wei, J. Ma and Y. Bai, Aromatization of FCC Gasoline Over Modified HZSM-5 Catalyst, *Pet. Sci. Technol.*, 2007, **25**(5), 577–584.
  - 33 Y. Zhao, H. Wang, M. Wei and C. Cao, Studies on Aromatization of Different FCC Naphtha Fraction Over P-Zn/HZSM-5 Catalyst, *Acta Pet. Sin.*, 2007, **23**(3), 96–100.
  - 34 J. Zhu, L. Zhao, G. Cui, M. Wei, H. Wei, H. Wang and J. Ma, Influence of ZnO and P<sub>2</sub>O<sub>5</sub> Content on Modified HZSM-5 on Aromatization of FCC Gasoline, *Pet. Sci. Technol.*, 2007, **25**(10), 1305–1311.
  - 35 J. Zhang, W. Qian, C. Kong and F. Wei, Increasing para-Xylene Selectivity in Making Aromatics from Methanol with a Surface-Modified Zn/P/ZSM-5 Catalyst, *ACS Catal.*, 2015, **5**(5), 2982–2988.
  - 36 J. Zhang, W. Qian, X. Tang, K. Shen, T. Wang, X. Huang and F. Wei, Influence of Catalyst Acidity on Dealkylation, Isomerization and Alkylation in MTA Process, *Acta Phys.-Chim. Sin.*, 2013, **29**(6), 1281–1288.
  - 37 C. Costa, I. Dzikh, J. Lopes, F. Lemos and F. Ribeiro, Activity-acidity relationship in zeolite ZSM-5. Application of Brönsted-type equations, *J. Mol. Catal. A: Chem.*, 2000, **154**(1–2), 193–201.
  - 38 R. Weber, J. Fletcher, K. Möller and C. O'Connor, The characterization and elimination of the external acidity of ZSM-5, *Microporous Mater.*, 1996, **7**(1), 15–25.
  - 39 L. Lubango and M. Scurrell, Light alkanes aromatization to BTX over Zn-ZSM-5 catalysts: Enhancements in BTX selectivity by means of a second transition metal ion, *Appl. Catal.*, A, 2002, **235**(1–2), 265–272.
  - 40 L. Yu, S. Huang, S. Zhang, Z. Liu, W. Xin, S. Xie and L. Xu, Transformation of Isobutyl Alcohol to Aromatics over Zeolite-Based Catalysts, *ACS Catal.*, 2012, **2**(6), 1203–1210.
  - 41 L. Hersh, E. Onyiriuka and W. Hertl, Amine-reactive surface chemistry of zinc phosphate glasses, *J. Mater. Res.*, 1995, **10**(8), 2120–2127.
  - 42 X. Yuan, B. Zhu, X. Ma, G. Tong, Y. Su and X. Zhu, Low Temperature and Template-Free Synthesis of Hollow Hydroxy Zinc Phosphate Nanospheres and Their Application in Drug Delivery, *Langmuir*, 2013, **29**(39), 12275–12283.
  - 43 O. Kleifeld, A. Frenkel, J. Martin and I. Sagi, Active site electronic structure and dynamics during metalloenzyme catalysis, *Nat. Struct. Mol. Biol.*, 2003, **10**, 98–103.
  - 44 O. Kleifeld, A. Frenkel and I. Sagi, Time-dependent XAS studies of trapped enzyme-substrate complexes of alcohol dehydrogenase from *Thermoanaerobacter brockii*, *J. Synchrotron Radiat.*, 2001, **8**, 978–980.
  - 45 O. Kleifeld, A. Frenkel, O. Bogin, M. Eisenstein, V. Brumfeld, Y. Burstein and I. Sagi, Spectroscopic Studies of Inhibited Alcohol Dehydrogenase from *Thermoanaerobacterbrockii*: Proposed Structure for the Catalytic Intermediate State, *Biochemistry*, 2000, **39**(26), 7702–7711.
  - 46 J. Wang, J. Qiao, Z. Jia and Z. Wang, CN Patent CN106607076A, 2015.
  - 47 J. Caro, M. Bülow, M. Derewinski, J. Haber, M. Hunger, J. Kärger, H. Pfeifer, W. Storek and B. Zibrowius, NMR and IR studies of zeolite H-ZSM-5 modified with orthophosphoric acid, *J. Catal.*, 1990, **124**(2), 367–375.
  - 48 E. Brunner, H. Ernst, D. Freude, T. Fröhlich, M. Hunger and H. Pfeifer, Magic-angle-spinning NMR studies of acid sites in zeolite H-ZSM-5, *J. Catal.*, 1991, **127**(1), 34–41.



- 49 W. Loewenstein, The distribution of aluminum in the tetrahedra of silicates and aluminates, *Am. Mineral.*, 1954, **39**(1–2), 92–96.
- 50 D. Massiot, F. Fayon, M. Capron, I. King, S. Calvé, B. Alonso, J. Dur, B. Bujoli, Z. Gan and G. Hoatson, Modelling one- and two-dimensional solid-state NMR Spectra, *Magn. Reson. Chem.*, 2002, **40**, 70–76.
- 51 S. Menezes, Y. Lam, K. Damodaran and M. Pruski, Modification of H-ZSM-5 zeolites with phosphorus. 1. Identification of aluminum species by  $^{27}\text{Al}$  solid-state NMR and characterization of their catalytic properties, *Microporous Mesoporous Mater.*, 2006, **95**(1–3), 286–295.
- 52 S. Menezes, V. Camorim, Y. Lam, R. Gil, A. Bailly and J. Amoureux, Characterization of extra-framework species of steamed and acid washed faujasite by MQMAS NMR and IR measurements, *Appl. Catal., A*, 2001, **207**(1–2), 367–377.
- 53 G. Woolery, G. Kuehl, H. Timken, A. Chester and J. Vartuli, On the nature of framework Brønsted and Lewis acid sites in ZSM-5, *Zeolites*, 1997, **19**(4), 288–296.
- 54 M. Kojima, F. Lefebvre and Y. Taàrit, Modification of siliceous zeolites using phosphorus pentachloride, *Zeolites*, 1992, **12**(6), 724–727.
- 55 K. Damodaran, J. Wiench, S. Menezes, Y. Lam, J. Trebosc, J. Amoureux and M. Pruski, Modification of H-ZSM-5 zeolites with phosphorus. 2. Interaction between phosphorus and aluminum studied by solid-state NMR spectroscopy, *Microporous Mesoporous Mater.*, 2006, **95**(1–3), 296–305.
- 56 P. Bautista, J. Campelo, A. Garcia, D. Luna, J. Marinas and A. Romero,  $\text{AlPO}_4\text{-Al}_2\text{O}_3$  catalysts with low alumina content: I. Structural and textural characterization of catalysts obtained with aqueous ammonia, *Appl. Catal., A*, 1993, **96**(2), 175–199.
- 57 L. Montagne, G. Palavit and M. Draoui, Mechanism of polyphosphate gel formation in the  $\text{Na}_2\text{O-Al}_2\text{O}_3\text{-P}_2\text{O}_5$  system, *J. Non-Cryst. Solids*, 1993, **155**(2), 115–121.
- 58 D. Müller, I. Grunze, E. Hallas and G. Ladwig, Hochfeld- $^{27}\text{Al}$ -NMR-Untersuchungen zur Aluminiumkoordination in kristallinen Aluminiumphosphaten Anorg, *Allg. Chem.*, 1983, **500**, 80–88.
- 59 K. Dixon and J. Mason, *Multinuclear NMR*, Springer US, 1987, p-369.
- 60 R. Hill and J. & Jones, The crystal structure of hopeite, *Am. Mineral.*, 1976, **61**, 987–995.
- 61 M. Newville, IFEFFIT : interactive XAFS analysis and FEFF fitting, *J. Synchrotron Radiat.*, 2001, **8**, 322–324.
- 62 M. Newville, P. Liviņš, Y. Yacoby, J. Rehr and E. Stern, Near-edge x-ray-absorption fine structure of Pb: A comparison of theory and experiment, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1993, **47**, 14126–14131.
- 63 B. Ravel and M. Newville, ATHENA, ARTEMIS, HEPHAESTUS: data analysis for X-ray absorption spectroscopy using IFEFFIT, *J. Synchrotron Radiat.*, 2005, **12**, 537–541.
- 64 S. Zabinsky, J. Rehr, A. Ankudinov, R. Albers and M. Eller, Multiple-scattering calculations of x-ray-absorption spectra, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 1995, **52**, 2995–3009.
- 65 J. Biscardi, G. Meitzner and E. Iglesia, Structure and Density of Active Zn Species in Zn/H-ZSM5 Propane Aromatization Catalysts, *J. Catal.*, 1998, **179**(1), 192–202.
- 66 M. Low and P. Ramamurthy, Infrared study of the surface properties of phosphoric acid impregnated silica, *J. Phys. Chem.*, 1968, **729**, 3161–3167.
- 67 J. Marques, I. Gener, P. Ayrault, J. Bordado, J. Lopes, F. Ribeiro and M. Guisnet, Dealumination of HBEA zeolite by steaming and acid leaching: distribution of the various aluminic species and identification of the hydroxyl groups, *C. R. Chim.*, 2005, **8**(3–4), 399–410.
- 68 X. Jiang, In situ FTIR studies of extraframework aluminum bound methoxy species in H-ZSM-5 zeolites, *J. Mol. Catal. A: Chem.*, 1997, **121**(1), 63–68.
- 69 M. Guisnet, P. Ayrault, C. Coutanceau, M. Alvarez and J. Datka, Acid properties of dealuminated beta zeolites studied by IR spectroscopy, *J. Chem. Soc., Faraday Trans.*, 1997, **93**(8), 1661–1665.
- 70 N. Brodu, M. Manero, C. Andriantsiferana, J. Pic and H. Valdés, Role of Lewis acid sites of ZSM-5 zeolite on gaseous ozone abatement, *Chem. Eng. J.*, 2013, **231**, 281–286.
- 71 S. Zheng, H. Heydenrych, A. Jentys and J. Lercher, Influence of Surface Modification on the Acid Site Distribution of HZSM-5, *J. Phys. Chem. B*, 2002, **106**(37), 9552–9558.
- 72 E. El-Malki, R. Santen and W. Sachtler, Introduction of Zn, Ga, and Fe into HZSM-5 Cavities by Sublimation: Identification of Acid Sites, *J. Phys. Chem. B*, 1999, **103**(22), 4611–4622.
- 73 P. Jacobs, E. Flanigen, J. Jansen and H. Bekkum, *Introduction to zeolite science & practice*, Elsevier, 2001.
- 74 B. Hunger, M. Heuchel, L. Clark and R. Snurr, Characterization of Acidic OH Groups in Zeolites of Different Types: An Interpretation of  $\text{NH}_3$ -TPD Results in the Light of Confinement Effects, *J. Phys. Chem. B*, 2002, **106**(15), 3882–3889.
- 75 L. Lin, S. Zhao, D. Zhang, H. Fan, Y. Liu and M. He, Acid Strength Controlled Reaction Pathways for the Catalytic Cracking of 1-Pentene to Propene over ZSM-5, *ACS Catal.*, 2015, **5**(7), 4048–4059.
- 76 Y. Ni, A. Sun, X. Wu, G. Hai, J. Hu, T. Li and G. Li, The preparation of nano-sized H[Zn, Al]ZSM-5 zeolite and its application in the aromatization of methanol, *Microporous Mesoporous Mater.*, 2011, **143**(2–3), 435–442.
- 77 W. Kaeding and S. Butter, Production of chemicals from methanol: I. Low molecular weight olefins, *J. Catal.*, 1980, **61**(1), 155–164.
- 78 H. Vinek, G. Rumpelmayr and J. Lercher, Catalytic properties of postsynthesis phosphorus-modified H-ZSM5 zeolites, *J. Catal.*, 1989, **115**(2), 291–300.
- 79 M. Castilla, A. Gayubo, A. Aguayo, J. Ar&es and J. Bilbao, Simulation and Optimization of Methanol Transformation into Hydrocarbons in an Isothermal Fixed-Bed Reactor under Reaction–Regeneration Cycles, *Ind. Eng. Chem. Res.*, 1998, **37**(6), 2383–2390.



- 80 G. Mekhemer, A. Nohman, N. Fouad and H. Khalaf, Surface to bulk characterization of phosphate modified aluminas, *Colloids Surf., A*, 2000, **161**(3), 439–446.
- 81 S. Kouva, J. Kanervo, F. Schüßler, R. Olindo, J. Lercher and O. Krause, Sorption and diffusion parameters from vacuum-TPD of ammonia on H-ZSM-5, *Chem. Eng. Sci.*, 2013, **89**(15), 40–48.
- 82 H. Li, X. Li and W. Xiao, Deactivation kinetics of individual C<sub>6</sub>–C<sub>9</sub> aromatics' generation from methanol over Zn and P co-modified HZSM-5, *RSC Adv.*, 2019, **9**, 22327–22335.

