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# Insights into the structure and ionic transport in 'water-in-bisalt' electrolytes for lithium-ion batteries†

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We investigated the dynamics and transport of lithium-ion water-in-bisalt (WiBS) electrolytes that contain lithium bis(trifluorosulfonimide) (LiTFSI) and lithium triflate (LiOTf) at different concentrations and temperatures using classical molecular dynamics simulations. The presented results are helpful to access the advantages of their use as electrolytes in Li-ion batteries. The structural analysis shows that the Li-ions have analogous interactions with the oxygen atoms of TFSI, OTf- and water. The calculated ionic conductivities from the current autocorrelation function are close to the experimental data for all the concentrations except the lowest one, in which case, the correlated conductivity is close to the experiment. However, the Nernst–Einstein route for calculating ionic conductivity overestimates the values by a reasonably high margin. Ion-cage correlation dynamics show increasing ion-cage lifetimes with increasing concentration, which indicates that the Li-ions remain within the anionic cages for a longer time at higher concentrations. At higher temperatures, this lifetime is seen to decrease. The statistics of non-coordinated Li-ions that are free from TFSI- and OTf- support the ion-cage dynamics.

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## 1. Introduction

Li-ion batteries<sup>1</sup> have been enjoying the prime limelight of energy research ever since they entered the market in 1991.<sup>2,3</sup> Since then, there have been many exciting formulations of them, and research has been progressively oriented to enhance the efficiencies of these batteries.<sup>4–6</sup> The cathodes of these batteries are typically fabricated from oxides of lithium manganese, lithium cobaltate, V<sub>2</sub>O<sub>5</sub>, FeS<sub>2</sub>, or lithium nickel cobalt manganese and the anodes are made out of metallic lithium, graphitic or hard carbon.<sup>7–13</sup> A Na-super-ionic-conductor-structured Na<sub>3</sub>V<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub>/C composite was also reported as a cathode electrode for rechargeable batteries.<sup>14,15</sup> Electrolytes form an essential part of the setup of a battery and are responsible for the energy transfer that occurs between the electrodes. Many electrolytes like organic liquid, solid-state or polymer varieties have been devised for use in Li-ion batteries.<sup>16–20</sup> However, the most popular and state-of-the-art batteries involve using organic carbonate solvents, and LiPF<sub>6</sub> as the salt, which is shown to be effective in the market but is not by any means a completely safe option.<sup>21</sup> This mixture has temperature dependencies that make it hazardous at temperatures

as low as 60 °C, and inefficient at temperatures lower than room temperature due to the high freezing point of carbonates.<sup>22,23</sup> Fire accidents have occurred during the use and production of these carbonate-based Li-ion batteries. This can be attributed to their low flash points and intolerance to omnipresent entities like moisture.<sup>4,24,25</sup> Lithium salts like LiPF<sub>6</sub>, which is the most commonly used, tend to form hydrofluoric acid within the battery casing in the presence of water, which can be corrosive.<sup>26,27</sup> Lithium salts also have low solubility in organic solvents. To dissolve these salts, one requires a solvent with a high dielectric constant. But, with a large dielectric constant, the solvent is likely to be highly viscous. The high viscosity of the electrolyte will diminish the ion transport and hence prove to be unsuitable.<sup>28</sup>

Acknowledging these drawbacks, efforts to make safer, fire-resistant and eco-friendly batteries have been carried out. Incorporating an additive like tetramethylsulfone with flame-retardant properties can serve the purpose. Many reports in the literature speak about the performance of electrolytes with additives.<sup>29–32</sup> Other alternative ways to make safer batteries demand a reformulation of the existing trend of making electrolytes. The new era of liquid electrolyte research for Li-ion batteries focuses on water usage as the primary solvent within a very high concentrated solution of lithium salt-water-in-salt electrolytes (WiSE).<sup>33</sup> Water, because of its narrow electrochemical window, was deemed unfit for usage in environments of high energy density, like inside Li-ion batteries, as it would dissociate. But by super-saturating water

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with LiTFSI, the electrochemical window of water can be expanded to  $\sim 3.0$  V, making it compatible with the various anodes and cathodes. This research direction also granted the research community with a Na-ion variant<sup>34–36</sup> of WiSE and expanded its application to 4.0 V processes<sup>37</sup> and higher. Once the lithium salt reaches its solubility limit, another lithium salt can be successfully dissolved to enhance the electrochemical window of water further. These are termed “Water-in-Bisalt” (WiBS)<sup>38</sup> electrolytes. WiBS electrolytes became popular as those having an extremely high concentration of ions and the most expanded electrochemical windows for water. There has been experimental work that reports the physicochemical properties of WiBS as well.<sup>39,40</sup> Studies on these aqueous electrolytes have provided valuable insights into many aspects of these electrolytes, and molecular dynamics simulations have served much in this respect.<sup>41–44</sup>

This current investigation focuses on understanding the structural and transport properties of a water-in-bisalt electrolyte (LiTFSI and LiOTf) using classical molecular dynamics simulations. As suggested in previous literature,<sup>39</sup> we use a third of the concentration of LiOTf as that of LiTFSI. We consider four concentration regimes: 5.1 m LiTFSI and 1.7 m LiOTf, 9 m LiTFSI and 3 m LiOTf, 15 m LiTFSI and 5 m LiOTf and 21 m LiTFSI and 7 m LiOTf. We also conduct a temperature-variable study on the mixture of 9 m LiTFSI and 3 m LiOTf. The calculated transport properties are compared with the available experimental data.

## 2. Computational methodology

Molecular dynamics simulations were performed using GRO-MACS version 5.1.2.<sup>45–50</sup> The molecular structures used in this study have been parameterized using the Generalized Amber Force Field (GAFF),<sup>51</sup> with the help of the Antechamber<sup>52</sup> package. Before the molecular dynamics simulations, the individual entities used in this study were subjected to geometry optimization through electronic structure methods using the B3LYP<sup>53–56</sup> functional with a 6-311+(2d,p) basis set and RESP model<sup>57,58</sup> to predict the partial atomic charges. The Gaussian09<sup>59</sup> package was used for this. In accordance with previous studies,<sup>60–62</sup> a charge scaling factor of 0.8 was used for Li<sup>+</sup>, TFSI- and OTf-. SPC/E<sup>63</sup> was the water model used. The complete list of force field parameters used in this study is provided in the ESI† The optimized structures used in this study are given in Fig. 1. Following this, the Packmol<sup>64</sup> package was used to randomly arrange the 1000 units in a cubic space. The numbers of different units to represent different concentrations used in this study are explained in Table S1 of the ESI.† We produced three randomly arranged initial configurations of sets of the same concentration to continue with our molecular dynamics simulations for better statistical averaging of transport properties and standard deviation calculation. The protocol followed in our work began by minimizing the energy of the initial configurations through the steepest descent algorithm. After that, each of the three systems was annealed

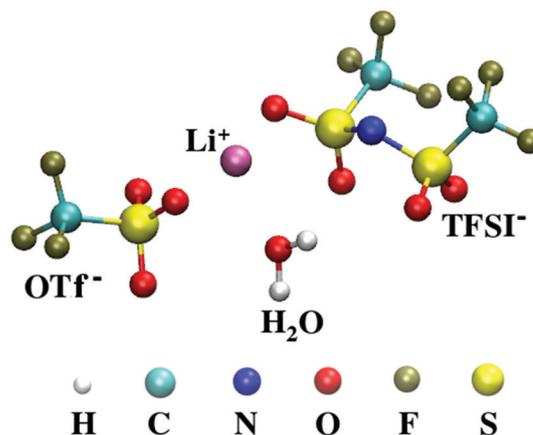


Fig. 1 The structures of all the chemical entities in this study.

to different temperatures, namely 498.15, 698.15 and 1098.15 K, by which slow cooling to 298.15 K was done with 20 K temperature drops at every 200 ps. They were provided with an additional 1 ns of equilibration concerning the *NVT* ensemble with a reference temperature of 298.15 K for all the simulations. Following this, we performed equilibrations concerning the *NPT* and *NVT* ensembles, in that order, for 50 ns on each system. The averaged box length (5–50 ns) after the *NPT* equilibration was used in the input for the *NVT* equilibration. This ensured that the average density was maintained correctly throughout the simulation. For the temperature and pressure control, the V-rescale<sup>65</sup> thermostat and the Berendsen<sup>66</sup> barostat algorithms were used, respectively. The production run was carried out within the *NVE* ensemble for 250 ns at an output writing frequency of 10 ps. The simulations for aqueous 15 m LiTFSI-5 m LiOTf and 21 m LiTFSI-7 m LiOTf were extended to 500 ns to facilitate calculations of correlated ionic conductivity. The convergence of physical properties after these simulations (density during the *NPT* equilibrations, the temperature during the *NVT* equilibrations and total energy and temperature during the *NVE* production run) is presented in Fig. S1 of the ESI† document. The linear and converging trends of these graphs show that the systems used for this study are well equilibrated. For calculations of the current autocorrelation function, ten *NVE* simulations were produced for a period of 100 ps each for each system in this study, with the trajectory and velocities saved every 2 fs after the final *NVE* simulations. *NVE* simulations for a further 4 ns were carried out in each case to calculate the ion-cage lifetimes and hydrogen bond dynamics, with an output writing frequency of 1 ps.

## 3. Results and discussion

### Density & structure of WiBS electrolytes

The densities of the electrolytes are shown in Fig. S1 (ESI†) concerning different concentrations and temperatures. The increase in concentration increases the density due to a more significant number of ions in the system. But as the temperature increases, density decreases due to occupying a larger volume.



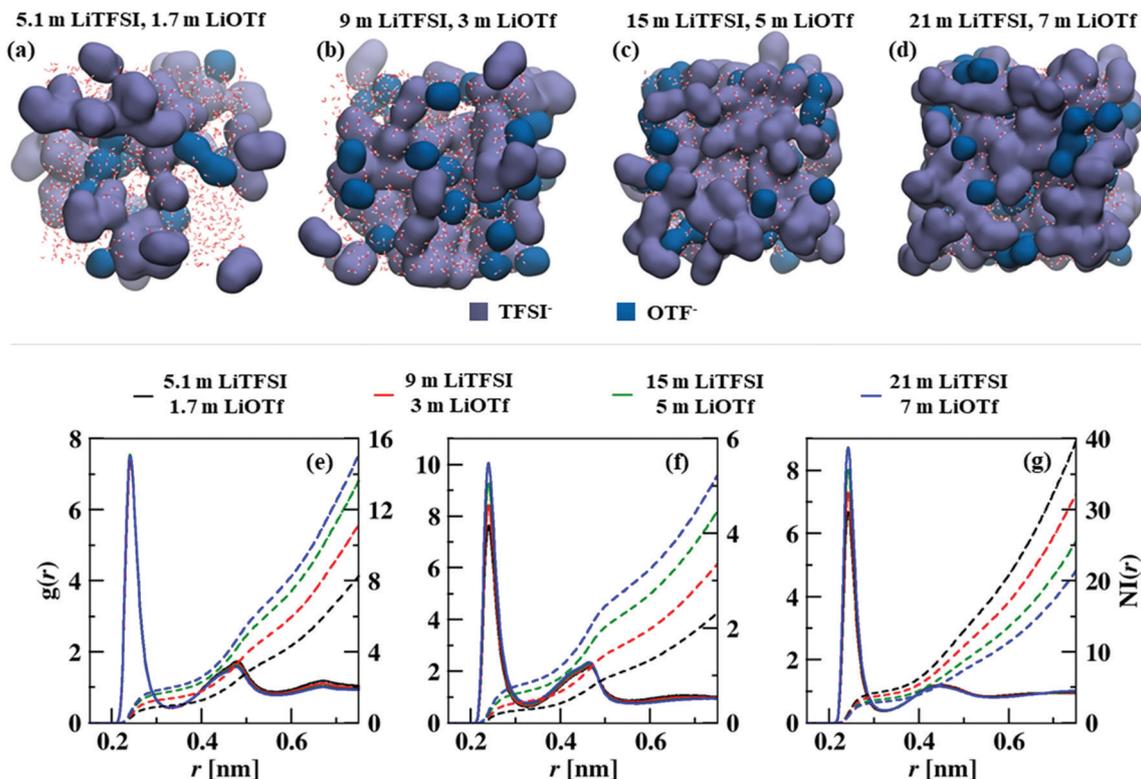


Fig. 2 (a–d) Snapshots of the water-in-bisalt system at different concentrations. RDF of the  $x$  m LiTFSI and  $x/3$  m LiOTf aqueous mixtures: (e)  $\text{Li}^+$ –O of TFSI $^-$ , (f)  $\text{Li}^+$ –O of OTf $^-$  and (g)  $\text{Li}^+$ –O of water. Anions are presented as large volumes; Li $^+$  and water are shown with atomistic details. The dashed lines represent the coordination numbers at various lengths from the reference atoms.

The thorough analysis of trajectories provides a distinction between the regions of ionic moieties of the system. The snapshots that are portraying various structures are presented in Fig. 2(a–d). As the concentration increases, the volume occupied by the surfaces representing TFSI $^-$  and OTf $^-$  increases. The water molecules move between these anionic regions, like ‘water channels’,<sup>43</sup> which are assumed to be present in concentrated aqueous electrolytes of batteries. This phenomenon was also reported earlier as ‘percolation’ based on graph theory related to molecular aggregation in aqueous solutions.<sup>67</sup> Since the anions contain oxygen atoms that can form hydrogen bonds with the water molecules, one can expect a strong hydrogen bonding network in these electrolyte systems. These dynamics will be investigated more thoroughly in the later sections.

For more quantitative information of the ionic structuring in this system, radial distribution functions (RDFs) were calculated between  $\text{Li}^+$  and oxygen atoms of TFSI $^-$ , OTf $^-$  and water, given in Fig. 2(e–g). Interestingly, all three of these correlations show similar ranges of interaction in their first solvation shells, *i.e.*, the first solvation shell peak remains unchanged mainly in terms of its height, even though the concentrations of lithium salts change drastically in each case. The position of these peaks also does not alter in any of the three interactions. The first solvation shell begins at a little beyond 0.20 nm and extends till  $\sim 0.33$  nm in all cases. The preliminary indication of these observations is that the solvation structure does not significantly change when the concentration is altered. TFSI $^-$

does not change its solvation characteristics towards  $\text{Li}^+$  even with significant changes in the overall concentration of this system, according to the RDF data, as represented in Fig. 2(e).

### Ionic conductivity

To study the transport of ions in these electrolytes, we calculated the mean squared displacement (MSD) of each ion in the system using the following formula:

$$\text{MSD} = \frac{1}{N} \sum_{i=1}^N [r_i(t) - r_i(0)]^2 \quad (1)$$

Where  $N$  is the total number of particles in the system and  $r_i(t)$  is the position of the  $i$ th particle at time  $t$ . The corresponding log–log plot of MSD and the  $\beta(t)$  vs.  $t$  plot<sup>68</sup> helps decide the electrolyte system’s diffusive regime.  $\beta(t)$  is defined as:

$$\beta(t) = \frac{d \ln(\text{MSD})}{d \ln(t)} \quad (2)$$

Along the simulation time, the log–log plots show a straight line, and the value of  $\beta(t)$  is unity, considered to be the diffusive regime of the electrolytes. The data for MSD, log–log plots and the  $\beta(t)$  plots are provided in Fig. 3.

Fig. 3(a) shows a decrease in the MSD of  $\text{Li}^+$  as concentration increases, while it shows a significant increase when the temperature is raised. The same effect is observed in the anions (Fig. 3(d)), although they traverse much lesser than the  $\text{Li}^+$ ,



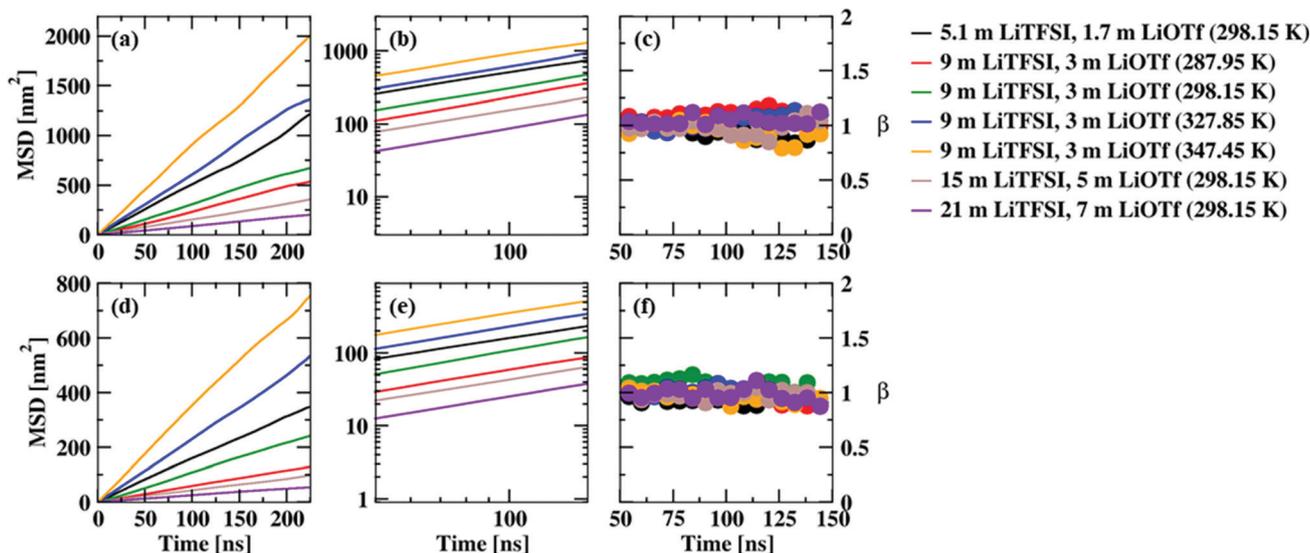


Fig. 3 (a) MSD vs. time, (b) the corresponding log–log plot and (c)  $\beta$  vs. time plots of  $\text{Li}^+$  and (d) MSD vs. time, (e) the corresponding log–log plot and (f)  $\beta$  vs. time plots of the anions.

attributed to their larger sizes and bulkier structures. The log–log plots and the  $\beta(t)$  plots are represented across a time of 50–150 ns of the simulation. This is the region where the former shows straight-line behavior and the latter converging to a value of 1. Hence, this is the diffusive regime for this aqueous LiTFSI–LiOTf system for all the studied concentrations and temperatures. To know the individual contributions to ionic conductivity, it is often preferred to use the Einstein relation<sup>69</sup> to derive the self-diffusion coefficients of each type of ion present in the system by fitting it in the diffusive regime:

$$D = \lim_{t \rightarrow \infty} \frac{1}{6Nt} \sum_{j=1}^N [r_j(t) - r_j(0)]^2, \quad (3)$$

where  $D$  is the self-diffusion coefficient,  $N$  is the total number of particles in the system,  $t$  is the length of the diffusive regime and,  $r_j(t)$  is the position of the  $j$ th particle at time  $t$ . From here, we apply these self-diffusion coefficients into the Nernst–Einstein<sup>70,71</sup> relation to compute the ionic conductivity of the system:

$$\sigma = \frac{Nq_+q_-}{Vk_B T} (D_+ + D_-) \quad (4)$$

Here,  $\sigma$  denotes the ionic conductivity,  $N$  the number of ionic species in the system,  $q_+$  and  $q_-$  the cationic and anionic charges, respectively,  $V$  the volume of the simulation box,  $k_B$  the Boltzmann constant,  $T$  the temperature at which the simulation is run and  $D_+$  and  $D_-$  represent the self-diffusion coefficients of the cation and anion, respectively. The ionic conductivity obtained through this route is presented in Fig. S2 (ESI<sup>†</sup>). The experimental values<sup>39</sup> are also provided for comparison. The ionic conductivity decreases with an increase in the salt concentrations due to the reduced mobility of the ions in highly concentrated electrolytes but increases with temperature. Eqn (4) provides the ionic conductivity directly by plugging in the values. Still, it is also observed to overestimate the ionic conductivity by a substantial margin

(as observed in Fig. S2, ESI<sup>†</sup>) since it does not consider the correlated motion of the ions. This motion has a severe impact on the actual transport that the ions take part in. To overcome this, the preferred choice is to calculate the correlated conductivity:<sup>33,72–74</sup>

$$\sigma = \frac{1}{6k_B TV} \lim_{t \rightarrow \infty} \frac{d}{dt} \left\langle \sum_{i=1}^N \sum_{j=1}^N q_i q_j \frac{[\vec{r}_i(t) - \vec{r}_i(0)] \cdot [\vec{r}_j(t) - \vec{r}_j(0)]}{[\vec{r}_i(t) - \vec{r}_j(0)]} \right\rangle. \quad (5)$$

Fig. 4 shows the calculated correlated ionic conductivities of all the studied concentrations and temperatures concerning their corresponding experimental counterparts as published by Ding *et al.*<sup>39</sup> The proximity of our calculated values to the experimental data shows the accuracy of our model. However, we observe that the calculated values of ionic conductivity show a deviation from experimental values at high concentrations. Following the trend of the experimental data, the ionic conductivity exhibits a decreasing behavior with the increase in concentration.

Another essential method to consider for the calculation of ionic conductivity is *via* the integration of the current autocorrelation function (CACF), which is calculated *via* a Green–Kubo relation:<sup>72,75,76</sup>

$$\sigma = \frac{1}{3k_B TV} \int_0^{+\infty} \langle \mathbf{J}(t_0 + t) \cdot \mathbf{J}(t_0) \rangle dt, \quad (6)$$

where  $\mathbf{J}$  is the electrical current which is obtained as the product of ionic charge ( $q$ ) and velocity ( $\mathbf{v}$ ) over  $N$  species:

$$\mathbf{J} = \sum_{i=1}^N q_i \mathbf{v}_i \quad (7)$$

This method has been popular among many researchers and has been deployed extensively in many ionic liquids.<sup>77–79</sup> The autocorrelation functions obtained in each case are presented in Fig. S3 and S4 (ESI<sup>†</sup>). To get appropriate ionic



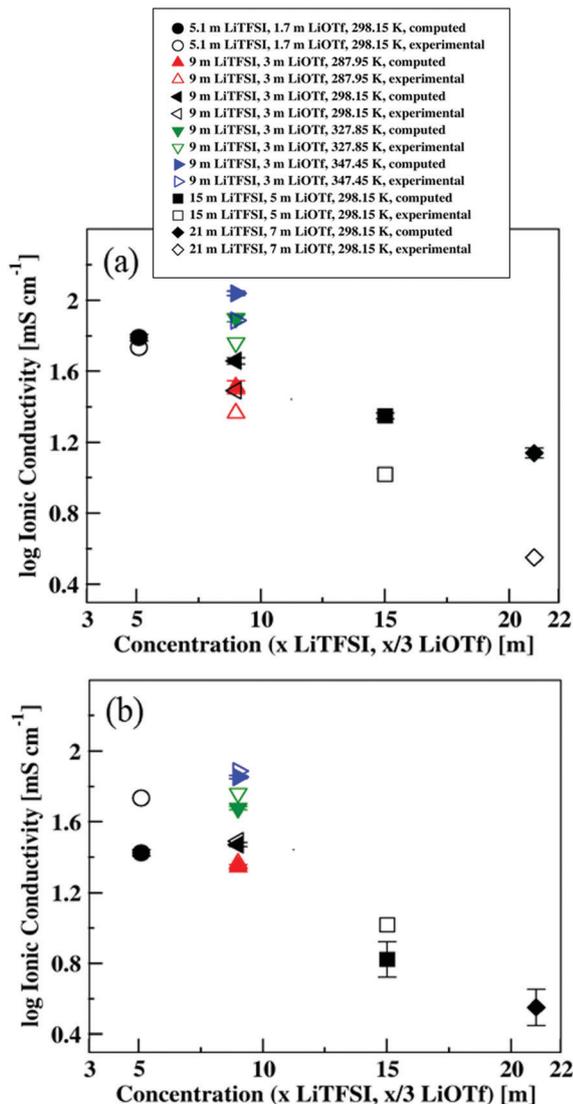


Fig. 4 Ionic conductivity of the electrolytes and comparison with experimental values at different concentrations and temperatures through various methods: (a) correlated ionic conductivity, (b) ionic conductivity from the current autocorrelation function. The legends and experimental values<sup>37</sup> have been provided for reference.

conductivity values, the Green–Kubo integral (eqn (6)) is evaluated over specific cutoff times. These values of ionic conductivity and the cutoff times used are recorded in Table S2 of the ESI.† The ionic conductivity obtained by this method is provided in Fig. 4(b). In this case, we observe that at a lower concentration of the electrolyte (at 5.1 m LiTFSI, 1.7 m LiOTf), the ionic conductivity is underestimated. Still, as the concentration increases, it predicts the values reasonably close to the experiment. At a concentration of 21 m LiTFSI and 7 m LiOTf, the calculated ionic conductivity values almost overlap with the experimental value.

These values are in a better agreement with the experiment across all concentrations than values calculated from either of the two methods individually, with minimal error in each case. After various analysis to find a suitable method to report the

conductivities, we found that except the lowest electrolyte concentration, the values obtained from CACF match well with that of experiments. However, the calculated correlated conductivity of the lowest concentration agrees well with the experimental value. These comparative values are shown in Fig. 4. The computed values also represent the change in conductivity concerning change in concentration and temperature correctly. Our models of both methods for reporting ionic conductivities can be justified as appropriately representative of the dynamic features of water-in-bisalt electrolyte in the mentioned concentrations and temperatures. As the concentration increases, the number of ions taking part in the transport increases, but the freedom for each ion to move decreases due to the rise in the effective total of attractive and repulsive Coulombic forces experienced by each ion. But when the temperature is increased, the ionic conductivity also increases due to the higher kinetic energy of the entities. In the light of commercial requirements of ionic conductivity for a Li-ion battery, these electrolytes can be considered along with state-of-the-art electrolytes.<sup>80,81</sup>

### Ion-cage lifetime

The ions in electrolytes are primarily surrounded by several counterions due to coulombic interactions; the additives disrupt the solvation structure by interacting with the ions. At a relatively high salt concentration like WiBS, the cation is trapped by anions in its first solvation shell. Due to strong coulombic interactions, the formed solvation shell appears as an ion cage structure. The trapped ions do not escape from the cage for high concentrated electrolytes and hop out with a larger time scale. The time they are trapped inside the cage can be correlated to ion cage lifetime that depends on the viscosity of the electrolyte. The ion cage structure plays a vital role in describing the overall dynamics of the electrolytes due to correlated interactions of counter ions. The dynamics of the escape process can be explained by investigating the time correlation function of the formation of cage structure. The method is like Luzar and Chandler's method<sup>82,83</sup> on hydrogen-bond dynamics in liquid water<sup>84–86</sup> that paved the way to significant insights into lifetimes and other vital properties of hydrogen bonds. The concept also was expanded into ionic liquid and other nonaqueous cases in the more recent past.<sup>85–88</sup> There have been two broad classifications while looking at the lifetimes of hydrogen bonds – continuous<sup>89</sup> and intermittent lifetime.<sup>90</sup> This idea can be generalized to any system, where there is a dynamic interaction between two moieties, and when there is an ionic entity solvated by other ionic groups forming an ion-cage.<sup>68,91,92</sup> The solvation of ionic entities can be viewed from the perspective of ionic cages. To understand the ionic dynamics, we calculated the ion-cage lifetimes, according to the equation:<sup>89,93–96</sup>

$$C(t) \approx \frac{\langle h(0)h(t) \rangle}{\langle h \rangle} \quad (8)$$

The function  $h(t)$  is dependent on a cutoff radius – it is treated to be unity if ionic groups of interest are within a



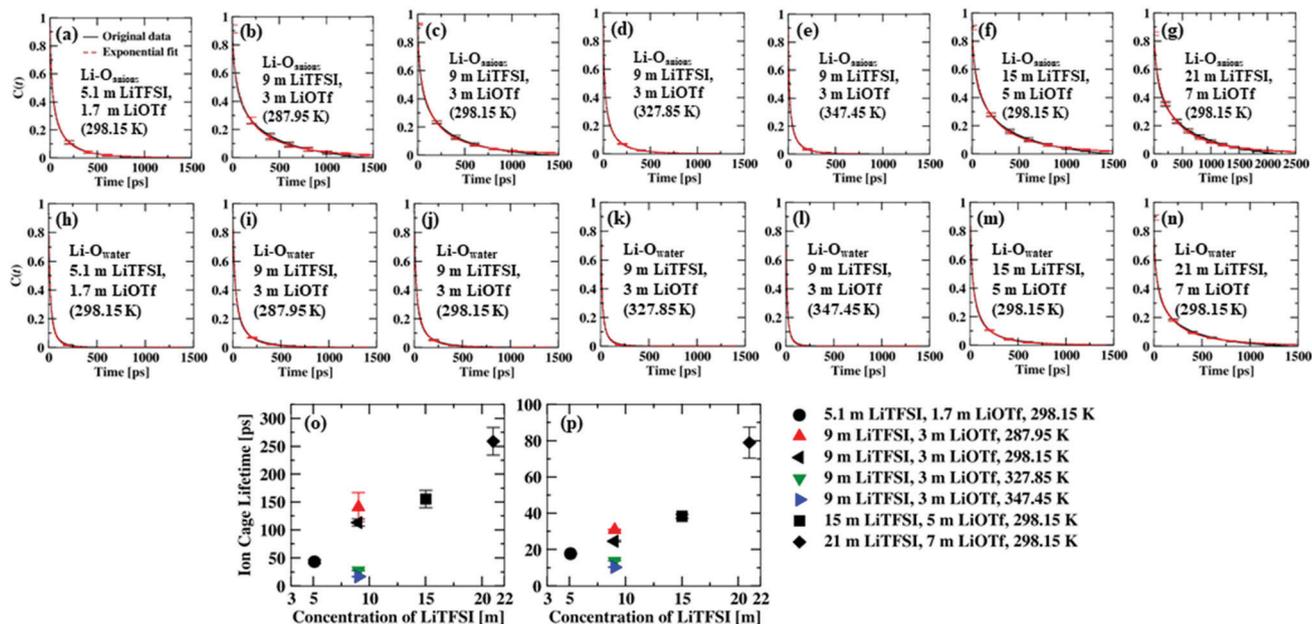


Fig. 5 Ion cage correlation functions and fitted curves for (a–g) Li–O of anion and (h–n) Li–O of water at different concentrations; ion cage lifetimes of (o) Li–O of anion and (p) Li–O of water at different concentrations and temperatures.

particular cutoff distance to each other. Otherwise, it is zero. The autocorrelation function  $C(t)$  provides the probability of  $\text{Li}^+$  and an anion that remain in the same cage until time  $t$ . According to the RDF presented in the earlier section of this manuscript, we understand that the first solvation shells do not extend beyond 0.33 nm. This distance is taken as the cutoff distance for this calculation. The decay of the autocorrelation function can be quantified by calculating the concerned time scale of the decay. Eqn (8) results in an autocorrelation function that has a decaying character, and which is then fitted with a stretched exponential function<sup>97</sup> as shown in eqn (9):

$$y = a_0 \exp\left(\frac{-x}{\tau_1}\right)^{\tau_2} \quad (9)$$

Here,  $\tau_1$  is ion-cage lifetime and  $\tau_2$  is the stretching parameter. For the interaction of  $\text{Li}^+$  with the oxygen atoms of TFSI and OTf<sup>-</sup>, the plots corresponding to eqn (8) and their corresponding fits with eqn (9) are provided in Fig. 5(a–g) for varying concentrations and temperatures of the electrolyte. The autocorrelation functions show good fitting concerning the stretched exponential function. The complete list of fitting parameters used here has been tabulated in the Table S3 (ESI<sup>†</sup>). Similarly, for the interaction of  $\text{Li}^+$  with the oxygen atoms of water, curves fitted with the stretched exponential function are shown in Fig. 5(h–n). The fitting parameters used for this are provided in Table S4 (ESI<sup>†</sup>). The ion-cage lifetimes derived from the fitting are consolidated in Fig. 5(o–p).

In both Li–O<sub>anions</sub> and Li–O<sub>water</sub> cases, we observe an increase in ion-cage lifetime values when the concentration increases. This is because of an increased number of anions that make it difficult for the  $\text{Li}^+$  to leave their vicinity and stay in the vicinity for a more extended period. However, when the

temperature increases, there is a decrease in the ion-cage lifetime, majorly because of the faster motion of the  $\text{Li}^+$  ions at higher temperatures. The rise in temperature increases the dynamics of the  $\text{Li}^+$ , and they tend to leave the ion-cage faster. The increasing MSD of the ions with increasing temperature complements this. Comparing Fig. 5(o and p), we observe that, even though the same trend is followed by ion-cage lifetimes, there is a significant difference in the values. For a concentration of 5.1 m LiTFSI and 1.7 m LiOTf,  $\text{Li}^+$  stays near the anion oxygen atoms for an average of 43.7 ps. But, in the case of oxygen molecules of water around the  $\text{Li}^+$ , the average lifetime is 17.8 ps. At higher concentrations, this effect is more pronounced. In the electrolyte system containing 21 m LiTFSI and 7 m LiOTf, the Li–O<sub>anions</sub> lifetime shows an average of 259.0 ps, while for Li–O<sub>water</sub>, it is only 79.0 ps. Ion-cage lifetimes are correlated to the ionic conductivity of the electrolytes. With increase in ion-cage lifetime, the counter ions stay close to each other, which affects the overall conductivity.

## 4. Conclusions

In this era where most of the research is focused on developing and advancing energy storage systems, the efficiency of electrolytes becomes essential. The new family of aqueous electrolytes has been in vogue as far as electrolyte research is concerned. We modeled the LiTFSI – LiOTf WiBS electrolyte system for various concentrations and temperatures and investigated their workings from a molecular dynamics perspective. Calculation of RDF shows that the interaction strength of  $\text{Li}^+$  with the oxygen atoms of TFSI<sup>-</sup>, OTf<sup>-</sup> and water are very similar, with minor changes in Li<sup>+</sup>–O of OTf<sup>-</sup> and Li<sup>+</sup>–O of water as the concentration increases. Our finding is in accord with the



earlier reported simulation study.<sup>98</sup> The calculation of mean squared displacement and the choice of an appropriate diffusive regime helped calculate the ionic conductivity of these electrolyte systems. The use of the Nernst–Einstein relation to calculate ionic conductivity showed a significant overestimation of values, while correlated conductivity calculations yielded values reasonably close to experimentally obtained ones. The ionic conductivity increases with temperature but decreases with an increase in concentration. The ions experience difficulty in free motion due to a higher number of attractive and repulsive forces. However, all these ionic conductivity values were found to satisfy commercial requirements and were higher than that of the state-of-the-art battery electrolytes. The ion-cage correlation functions calculated and fitted with a stretched exponential function helped derive the ion-cage lifetimes of the different concentrations of WiBS electrolytes and at different temperatures. These values showed an increase with increasing concentration and decreased with an increase in temperature. Through appropriate, the electrolytes have not been adopted in large scale commercial purposes. Further studies will be required to find the effects of change in thermodynamic conditions on the formation of solid and cathode electrolyte interfaces. The involved unwanted chemical reactions can enlighten the disadvantages of these electrolytes. Our results help us understand that these WiBS electrolyte systems are efficient in ion transport and have intriguing structural features. These analyses will help understand the microstructure of these electrolyte systems and help further the development of the same.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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