


 Cite this: *RSC Adv.*, 2021, 11, 34795

Investigation of element migration characteristics and product properties during biomass pyrolysis: a case study of pine cones rich in nitrogen

 Jielong Wu,[†] Liangcai Wang,^{†*} Huanhuan Ma^{*} and Jianbin Zhou ^{*}

To further understand the element migration characteristics and product properties during biomass pyrolysis, herein, pine cone (PC) cellulose and PC lignin were prepared, and their pyrolysis behavior was determined using thermogravimetric analysis (TGA). Subsequently, the PC was pyrolyzed in a vertical fixed bed reactor system at 400–700 °C for 60 min. The characteristics of element migration and the physicochemical properties of the pyrolysis products were analyzed and discussed. In the pyrolysis temperature range from 200 °C to 500 °C, there were two distinct weight loss peaks for PC. During the pyrolysis process, the C element was primarily retained in the biochar, while the O element mainly migrated into liquid and gaseous products in the form of compounds such as CO₂, CO, and H₂O. Besides, 28.42–76.01% of the N element in PC migrated into biochar. Of the three-phase products, the gases endow the lowest energy yield, while the energy of the biochar dominates the pyrolysis of the PC. Additionally, the N content and specific surface area for the PC-derived biochar obtained at 400 °C in a N₂ atmosphere were higher than those of the biochar derived from fiberboard.

Received 4th September 2021

Accepted 20th October 2021

DOI: 10.1039/d1ra06652h

rsc.li/rsc-advances

1. Introduction

Biomass is a clean and renewable resource, resulting from its wide distribution, abundance, CO₂ neutrality, and low emission of nitrogen and sulfur compounds.^{1–3} Unfortunately, the high water and oxygen contents of biomass lead to some drawbacks such as low burning rates and low flame temperatures for biomass combustion, as well as transport difficulties.^{4–6} Thus, relevant researchers often employ thermochemistry or biotechnology to convert biomass into solids, gases, and liquids to enhance the quality of biomass for integrated use, of which pyrolysis is a promising thermochemical process for biomass utilization.⁷ As is known, the pyrolysis of biomass involves a transformation of its phase. Meanwhile, the parent substance (*i.e.*, biomass) and the derivatives (*i.e.*, solids, gases, liquids) possess inherited relationships. As a result, the element content of the parent substance and the derivatives is a critical indicator of the degree of inheritance. It follows that it is essential to investigate the migration of elements during biomass pyrolysis.

Previous works have indicated that the release of CO₂ and CO during low-temperature (200–350 °C) pyrolysis (*viz.* torrefaction) of biomass allows for the elimination of oxygen faster than that caused by pure dehydration.^{8–15} Recently, numerous studies have shown that torrefaction can increase the carbon content and calorific value of biomasses, and reduce their oxygen content.^{16–19}

According to these, we can conclude that torrefaction leads to changes in the content of O and C elements, especially the O element. In other words, torrefaction causes the migration of O and C elements from biomass. Notably, most of the biomass torrefaction research has focused on the solid products of biomass, and the physicochemical changes, fuel properties, and further uses of torrefied biomass have been extensively reported.^{20,21} In fact, in addition to the solid products, there are small amounts of gaseous and liquid products.^{22,23} However, relatively few systematic studies have been performed on the migration laws of carbon and oxygen elements as the collection of small amounts of gaseous and liquid products is difficult. Biomass pyrolysis (400–800 °C) can significantly increase the yield of gaseous and liquid products.

On the other hand, previous studies have indicated that the doping of carbon-based materials with other heteroatoms (*e.g.*, N, P, and S) can further improve their properties.^{24–26} Schnucklake *et al.*²⁷ synthesized nitrogen-doped porous carbon using phenolic resin as the carbon source and pyrrole-2-carboxaldehyde as the nitrogen source. It was presented that the nitrogen-doped porous carbon shows promising activity for the positive side reaction. Laheäär *et al.*²⁸ used ammonia gas as the nitrogen source to modify activated carbon and indicated that the nitrogen-doped activated carbon with a nitrogen content of 4.50 wt% and a specific capacitance of 152 Fg⁻¹. Xu *et al.*²⁹ obtained biochar with 3.16 wt% N content by pyrolyzed the fiberboard containing phenolic resin. It was found that the biochar derived from fiberboard had a better adsorption effect on tetracycline. These previous studies have made significant progress in understanding that doped with N can enhance the

College of Materials Science and Engineering, Nanjing Forestry University, Nanjing, 210037, China. E-mail: wangliangcai@njfu.edu.cn; mahuanhuan@njfu.edu.cn; zhoujianbin@njfu.edu.cn

[†] These authors contribute equally to this work.



active site of carbon. However, exogenous nitrogen (*e.g.*, pyrrole-2-carboxaldehyde, ammonia gas, and phenolic resin) doping is not conducive to the uniform distribution of nitrogen in carbon materials, accompanied by the high cost. Therefore, biomass feedstocks with high nitrogen possess the potential to address the problem of uneven nitrogen doping and improve the active site of biomass-derived carbon. It follows that the nitrogen migration laws during pyrolysis of biomass feedstocks with high nitrogen are worthy of prior investigation.

Interestingly, pine cone (PC) is rich in nitrogen as an agroforestry waste, which is higher than that of other biomass like rice straw and grape stem, as well as is abundant in China.^{7,13} However, until now, most of the research on PC has focused on the development and investigation of natural medicinal extracts.³⁰ Consequently, the pyrolysis behavior of PC and the migration law of C, O, and N elements in the pyrolysis process have not been reported yet. In the present work, the physicochemical properties for biochar, liquid, and gaseous products generated at different temperatures were determined *via* proximate analysis, ultimate analysis, Karl-Fischer titration, and so on. Overall, this work has made further understand of the deoxygenation, decarbonization, and denitrogenation from PC during pyrolysis at different temperatures.

2. Experimental section

2.1. Materials

Pine cone (PC), employed as the feedstock for the pyrolysis experiment, was sourced from the Kuandian, Liaoning Province

of China. Before the test, the PC was dried in an oven at 105 °C for 24 h and then ground into a powder with a particle size of 0.130–0.180 mm. The PC cellulose and the PC lignin were prepared regarding the Chinese National Standards GB/T2677.10-1995 and the Chinese National Standards GB/T2677.8-1994, respectively.

2.2. Thermogravimetric experiment

Weigh loss characteristics of samples were carried out in TGA (TGA STA8000, PerkinElmer, Waltham, MA, USA). For each experiment, the sample weight, nitrogen flow rate, heating rate, and final pyrolysis temperature were ~10 mg, 50 mL min⁻¹, 20 °C min⁻¹, and 700 °C, respectively.

2.3. Pyrolysis experiment

The pyrolysis experiment was employed in a vertical fixed-bed (Blue M, Thermo Scientific, USA) reactor system, as presented in Fig. 1.

Approximately 30 g of PC was placed into the reactor, and before the experiment, the reactor was purged with nitrogen to remove air from the reactor, and then the nitrogen was turned off after 10 min. Subsequently, the operating parameters (temperatures) of the vertical fixed-bed reactor system were varied to examine the properties of biochar, liquid, and gaseous products at a residence time of 60 min. During the pyrolysis process, the biochar remained in the reactor. Meanwhile, the liquid and gaseous products were collected in a liquid collecting device and a gas collecting bag, respectively. The pyrolysis

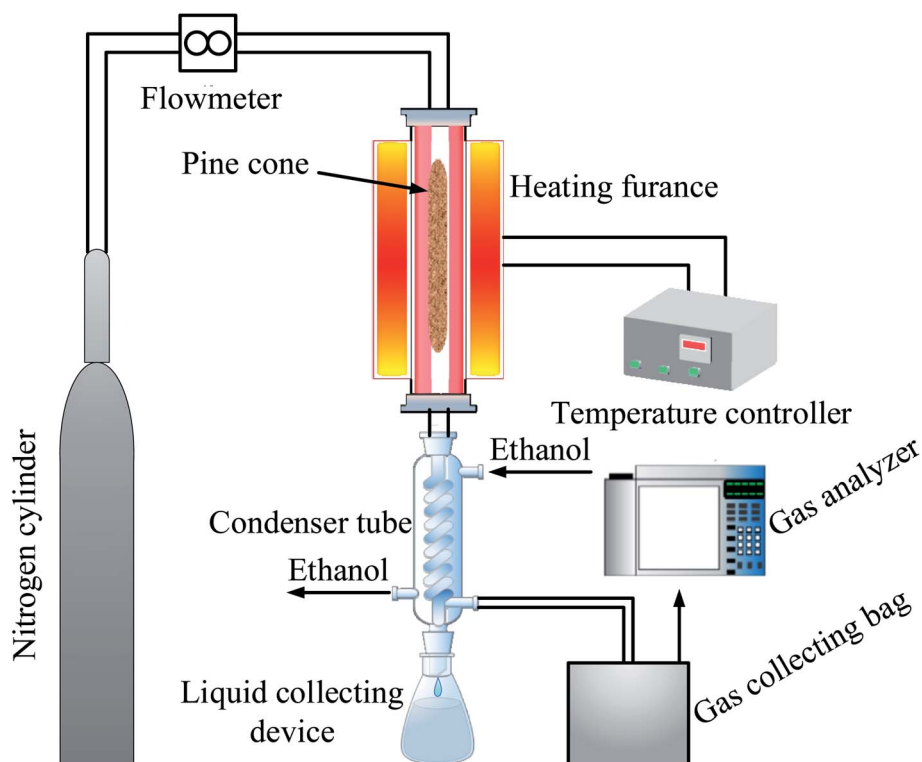


Fig. 1 A vertical fixed-bed reactor system.



experiment was repeated 3 times under the same experimental conditions to obtain enough products for subsequent testing. Besides, the volume concentration of each gas in the gaseous product was determined by a gas analyzer (Gasboard, Ruiyi Automatic Control Co., Ltd, Hubei, China).

2.4. Sample labels

Herein, the pine cone was named PC. Besides, PC-derived biochar (pyrolyzed pine cone) was labeled as PPC-*X*, where *X* is the pyrolysis temperature. As an example, PPC-400 stands for the PC-derived biochar obtained by pyrolyzing PC upon 400 °C under a heating rate of 20 °C min⁻¹ with a residence time of 60 min.

2.5. Analysis of pyrolysis products

Proximate analysis, ultimate analysis, and HHV of PC and PPC-*X* were performed regarding the Chinese National Standards GB/T28731-2012, an element analyzer (Vario macro cube, Elementar, Germany), and an adiabatic oxygen bomb calorimeter (XRY-1A, Changji Geological Instruments, China), respectively. The HHV of gaseous was determined *via* the gas analyzer.

The water content, pH, ultimate analysis, and composition of liquid were determined *via* Karl Fischer titration (KF-200, Mitsubishi Corporation, Japan), pH tester (E-201-C, Precision Scientific Instruments Co., Ltd, Shanghai, China), an element analyzer, and gas chromatography-mass spectrometry (Trace DSQ II, Thermo Scientific, USA), respectively.

2.6. Mass yield and energy yield of samples

Mass yield and energy yield were calculated by (1) and (2), respectively.

$$R = \frac{m_i}{m_0} \times 100\% \quad (1)$$

$$R_i = \frac{\text{HHV}_i}{\text{HHV}_0} \times R \quad (2)$$

Where *R*, *m*₀, and *m*_{*i*} are the mass yield (%) of the sample, the mass (g) of PC, and the mass (g) of the sample, respectively.

Other symbols of *R*_{*i*}, HHV₀, and HHV_{*i*} represent the energy yield (%) of the sample, the HHV₀ (MJ kg⁻¹) of PC, and the HHV_{*i*} (MJ kg⁻¹) of the sample, respectively.

3. Results and discussion

3.1. Thermogravimetric analysis of PC, PC cellulose, and PC lignin

The TGA (a) and DTG (b) curves of PC, PC cellulose, and PC lignin pyrolysis with a heating rate of 20 °C min⁻¹ are given in Fig. 2.

A notable difference was found in the pyrolysis behaviors of PC, PC cellulose, and PC lignin. The weight loss of PC happens early in the temperature ranging from 110 °C to 200 °C. Moreover, the DTG curve of PC endows two distinct weight loss peaks in the pyrolysis temperature ranging from 200 °C to 500 °C, at around 330 °C and 450 °C, respectively. Of these, the weight loss peak at about 330 °C was caused by the pyrolysis of lignin or hemicellulose, while the weight loss peak at about 450 °C was primarily ascribed to the existence of non-structural substances (*e.g.*, wax, fat, resin, tannin, sugars, and pigments). This is significantly different from other biomass shown only one peak such as bamboo,³¹ pinewood,³² and wheat straw,³³ while similar to palm kernel had two weight loss peaks.⁸ The weight percentage for the pyrolysis residue of PC being ~26%, which was consistent with the proximate analysis of PC (Table 1). Compared with the PC, PC cellulose was pyrolyzed in the lower temperature ranging from 200 °C to 380 °C and endows a narrow range of maximum weight loss upon 220–370 °C. Meanwhile, the weight percentage for pyrolysis residue was ~23%. Unlike the sharper DTG peaks of PC and PC cellulose, PC lignin was slowly pyrolyzed in the wider temperature ranging from 160 °C to 700 °C and generated the highest weight percentage for residue (~40%), this result was similar to the previous publication.⁸ Thence, the thermal stability of samples was determined: PC lignin > PC > PC cellulose.³⁴

3.2. Pyrolysis of PC

3.2.1 Product distribution. Natural polymeric components inter biomass primarily consist of hemicellulose, cellulose, and

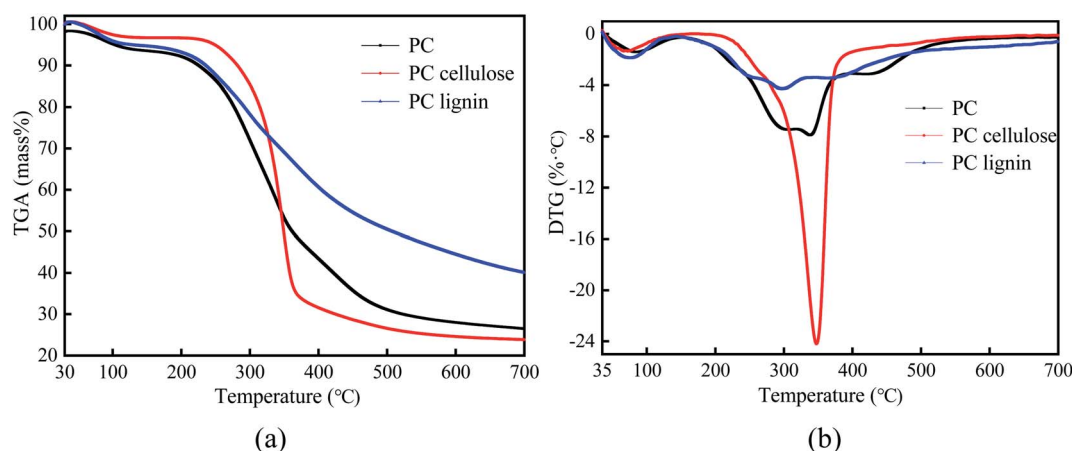


Fig. 2 TGA (a) and DTG (b) curves of PC, PC cellulose, and PC lignin.



Table 1 Physicochemical properties for PC and biochar

Samples	Proximate analysis (wt%, db)			Ultimate analysis (wt%, db)					HHV (MJ kg ⁻¹)	Energy yield (%)
	Volatile	Fixed carbon	Ash	C	H	N	S	O		
PC	73.98 ± 0.95	23.41 ± 0.44	2.61 ± 0.26	43.99 ± 0.49	3.65 ± 0.05	1.67 ± 0.07	0.51 ± 0.02	47.57 ± 0.89	17.86 ± 0.52	100
PPC-400	20.46 ± 0.77	71.69 ± 0.46	5.70 ± 0.32	66.11 ± 0.52	2.21 ± 0.04	2.79 ± 0.06	0.79 ± 0.03	22.40 ± 0.97	28.92 ± 0.59	73.68
PPC-500	16.57 ± 0.81	75.30 ± 0.49	7.99 ± 0.29	70.63 ± 0.48	1.09 ± 0.06	1.72 ± 0.05	0.53 ± 0.01	18.04 ± 0.89	29.68 ± 0.45	54.39
PPC-600	11.99 ± 0.87	79.47 ± 0.51	8.61 ± 0.34	74.07 ± 0.55	0.63 ± 0.03	1.65 ± 0.07	0.20 ± 0.02	14.84 ± 1.01	30.08 ± 0.65	51.01
PPC-700	9.48 ± 0.79	81.15 ± 0.45	8.96 ± 0.27	74.63 ± 0.51	0.53 ± 0.04	1.63 ± 0.06	0.15 ± 0.01	14.10 ± 0.88	30.31 ± 0.63	49.42

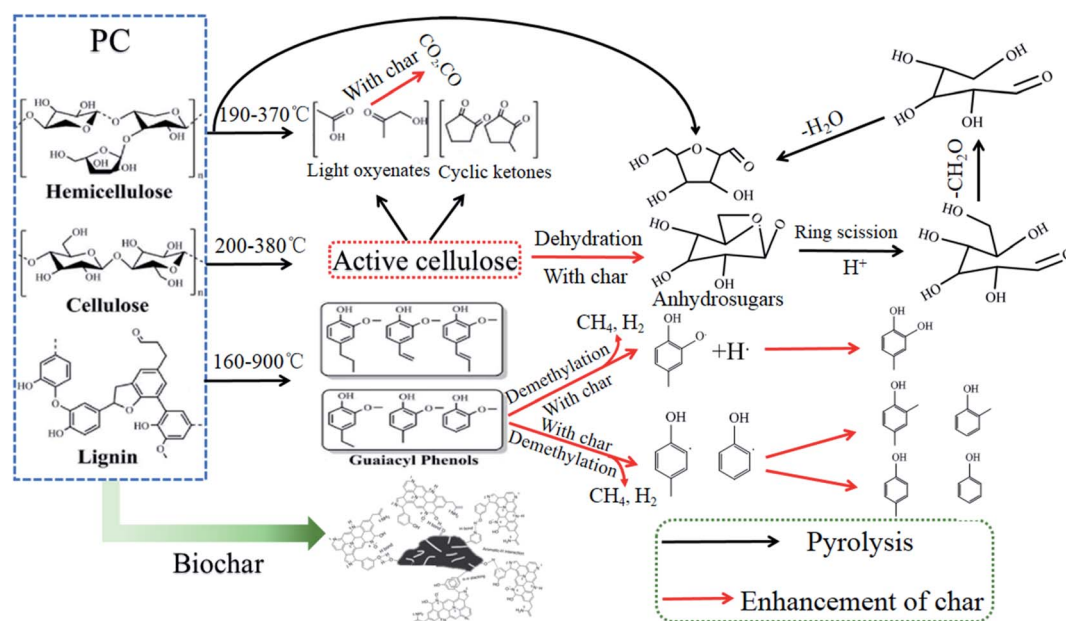


Fig. 3 Illustration of the main chemical reactions for the decomposition of PC.

lignin.³⁵ Consequently, Fig. 3 indicates the main chemical reaction illustration for the decomposition of PC.

It is well known that the weight loss of PC during pyrolysis primarily resulted from the evaporation of volatiles. Fig. 4 shows the product distribution of the PC pyrolysis at different temperatures.

From Fig. 4, it can seem that an increase in pyrolysis temperature, resulting in an outstanding reduction in the yield of biochar, but the yield of liquid presented a gradual increase. Meanwhile, the yield of gas has no significant difference.

The weight loss gradually increased with the pyrolysis temperature from 400 °C to 700 °C, and had a relatively considerable weight loss (70.88%) at 700 °C, since the hemicellulose, cellulose, lignin, and non-structural substances of PC strongly decomposed.³⁶ However, the increase in weight loss gradually slows down as the pyrolysis temperature increases. The sum of the yield of liquid and gas increased as the pyrolysis temperature increases, which was mainly attributed to the thermal cracking and lead to the formation of more volatiles.³⁷ The effect of pyrolysis temperature on PC mass yield was similar to the effect on other biomass (e.g., cotton stalk, eucalyptus, and rice husk).^{38–40}

3.2.2 Biochar

3.2.2.1 Physicochemical properties of biochar. Physicochemical properties for biochar are listed in Table 1.

The pyrolysis temperature has a notable effect on the physicochemical properties of biochar. The content of volatile gradually decreased as the pyrolysis temperature increases, such as 20.46% for PPC-400 and only 9.48% for PPC-700. Conversely, as the pyrolysis temperature increases, the ash

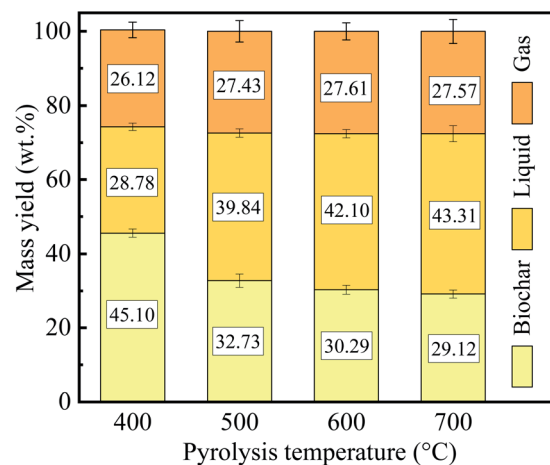


Fig. 4 Product distributions of the PC pyrolyzed at different temperatures.



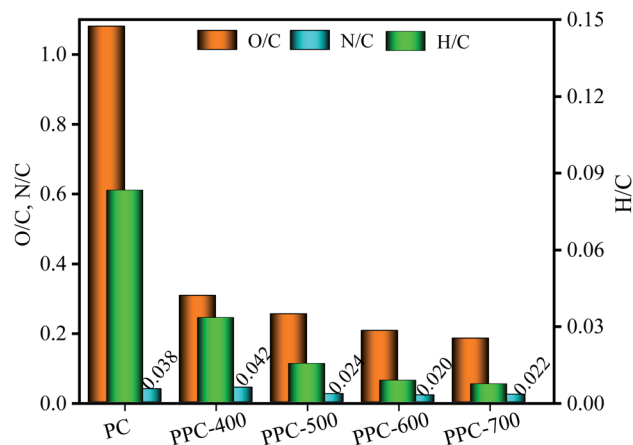


Fig. 5 H/C, O/C, and N/C element ratios for PC and PPC-X.

content increased as a result of the ash remaining in the PC. Meanwhile, the content of fixed carbon equally increased significantly. Similar results were obtained for coffee chaff⁴¹ and Japanese cedar.⁴² This suggests that the pyrolysis temperature resulted in lower volatile content, while the higher ash content was due to enhanced thermal decomposition for the PC. In addition, the nitrogen content of PPC-400 was higher, which was 2.79%, and the nitrogen content was over those of other biochar such as coffee chaff biochar,⁴¹ rick husk biochar,⁴³ and date seeds biochar.⁴⁴ However, the nitrogen content of PPC-400 was similar to that of fiberboard biochar.²⁹ In reviewing the literature, Li *et al.*⁴⁵ indicated the nitrogen content of bamboo biochar detected by element analyzer and XPS being 0.6% and 0.4%, respectively. Wang *et al.*⁴⁶ demonstrated the nitrogen content for lignin-derived porous carbon determined by element analyzer and XPS is 0.24% and 0%, respectively. Similarly, Xu *et al.*²⁹ illuminated the nitrogen content for fiberboard biochar detected by element analyzer and XPS being 3.42% and 2%, respectively. Notably, the nitrogen element content detected by an element analyzer is higher than the nitrogen element content detected by XPS. A plausible explanation for this result can be given as follows: element analyzer and XPS work on different principles. For the elemental analyzer, the element content of samples is determined by the detector after combustion, secondary combustion, reduction, and interference gas removal, while XPS according to Einstein's photoelectron effect to determines the elemental content on the surface of samples. In other words, ultimate analysis

demonstrates the elemental composition of samples, while XPS determines elemental content on the surface of samples. As such, when discussing the migration law of the N element, the N element determined by XPS will not be discussed if not mentioned otherwise.

3.2.2.2 H/C, O/C, and N/C element ratios. The S content of PC was intensely low and did not change much during the pyrolysis process. As the pyrolysis temperature increases, the formation and release of CH₄ and C₂H₆ lead to a slight decrease in H content. Besides, the content of both C and O in PC exceeds 40%. A sharp decrease in O content, from 45.57% for PC to 14.10% for PPC-700 with increasing the pyrolysis temperature. Notably, the C element was released during pyrolysis, but the C content increased increasingly, from 43.99% for PC to 74.63% for PPC-700, which was because of the weight loss of PC and the removal of a major amount of O element. In addition, the N element enrichment and N element release have effects on the N content of biochar during the pyrolysis process. The N content of PPC-400 was higher than that of PC, PPC-500, PPC-600, and PPC-700; from this, we can infer that the enrichment of N element was higher than the release of N element upon pyrolysis temperature was 400 °C.

Fig. 5 shows variation in H/C, O/C, and N/C element ratios for the PC and biochar along with pyrolysis temperature.

With an increase in pyrolysis temperature, the element ratios of N/C increased at first, and then they slowly decreased and tended to be stable. However, the element ratios of H/C and O/C for the biochar gradually decreased as the pyrolysis temperature increases. This indicates that large amounts of H and O elements were removed from the PC, while the C element was enriched during the pyrolysis process. Compared to the ranges of the H/C and O/C element ratios found in the previous publication for lignite, peat, bitumen, and anthracite, the PC contains more O and H elements than all coals.⁴⁷

3.2.3 Liquid. Results of water content, pH, and element analysis are shown in Table 2.

Liquid had a C content of 7.76–8.21% and an O content of 85.24–86.41%. Meanwhile, with an increase in pyrolysis temperature, the water content of liquid gradually increased from 73.03% to 77.89%. This result suggests that increased temperature promotes the dehydration reaction. Besides, with an increase in pyrolysis temperature, the pH also increased from 3.25 to 4.42. This was mainly due to the water content of liquid gradually increased.

To compare the composition of the liquids obtained at different temperatures, L-400 and L-700 were subjected to GC/

Table 2 Physicochemical properties for liquids obtained by pyrolysis of PC at different temperatures^a

Samples	Ultimate analysis (wt%)				Water content of liquid (wt%)	pH	HHV (MJ kg ⁻¹)	Energy yield (%)
	C	H	N	O				
L-400	8.21 ± 0.32	4.76 ± 0.03	0.62 ± 0.03	86.41 ± 0.62	73.03 ± 1.32	3.25 ± 0.27	10.40	16.80
L-500	7.99 ± 0.41	6.13 ± 0.04	0.64 ± 0.02	85.24 ± 0.53	74.56 ± 1.27	3.71 ± 0.32	7.89	17.60
L-600	7.76 ± 0.35	5.41 ± 0.05	0.81 ± 0.03	86.02 ± 0.57	76.45 ± 1.36	4.08 ± 0.38	8.74	20.60
L-700	7.82 ± 0.31	4.92 ± 0.03	0.92 ± 0.04	86.34 ± 0.62	77.89 ± 1.32	4.42 ± 0.29	10.12	24.54

^a L-XXX stands for liquid obtained from pyrolysis of PC at XXX temperature.



Table 3 Composition of L-400 and the relative content of the corresponding composition

Time (min)	Relative content (%)	Compound name	Molecular formula
5.774	17.12	Acetic acid	C ₂ H ₄ O ₂
11.961	9.08	Furfuryl alcohol	C ₅ H ₆ O ₂
18.256	5.21	Guaiacol	C ₇ H ₈ O ₂
17.945	4.23	Phenol	C ₆ H ₆ O
12.130	2.78	2-Methyl-2-cyclopenten-1-one	C ₆ H ₈ O
10.411	2.13	2-Cyclopentenone	C ₅ H ₆ O
20.411	1.95	<i>p</i> -Cresol	C ₇ H ₈ O
15.185	1.92	3-Methyl-2-cyclopenten-1-one	C ₆ H ₈ O
8.704	1.89	Pyrrrole	C ₄ H ₅ N
8.415	1.86	Cyclopentanone	C ₅ H ₈ O
12.632	1.81	3- <i>tert</i> -Butylcyclobutene	C ₈ H ₁₄
8.049	1.65	Propionic acid	C ₃ H ₆ O ₂
16.734	1.62	2,3-Dimethyl-2-cyclopenten-1-one	C ₇ H ₁₀ O
19.309	1.59	<i>o</i> -Cresol	C ₇ H ₈ O
21.169	1.57	2-Methoxy-4-methylphenol	C ₈ H ₁₀ O ₂
15.338	1.53	2,3-Dimethyl-butane	C ₆ H ₁₄
6.522	1.21	Hydroxyacetone	C ₃ H ₆ O ₂
23.433	1.12	4-Ethyl-2-methoxyphenol	C ₈ H ₁₂ O ₂
9.484	1.09	Dimethylmalonic acid	C ₅ H ₈ O ₄
6.615	1.03	2,4-Pentadienenitrile	C ₅ H ₅ N
21.633	1.01	2,4-Dimethylphenol	C ₈ H ₁₀ O
15.561	0.89	3,4-Dimethyl-2-cyclopenten-1-one	C ₇ H ₁₀ O
7.378	0.85	2-Methyl-2-pentanol	C ₆ H ₁₄ O
14.918	0.80	2,3-Dimethyl-2-cyclopenten-1-one	C ₇ H ₁₀ O
9.670	0.72	2-Methylcyclopentanone	C ₆ H ₁₀ O
17.007	0.58	2,3,4-Trimethyl-2-cyclopenten-1-one	C ₈ H ₁₂ O
22.332	0.41	Maltose	C ₆ H ₆ O ₃
8.234	0.34	4-Methylphenol	C ₇ H ₈ O
13.758	0.22	Phenol	C ₆ H ₆ O
22.243	0.16	Hydroxycarbamide	CH ₄ O ₂ N ₂

MS tests. As is known, the chromatographic peak area of a compound is considered to be linearly related to its content. Several representative compounds were selected as their comparatively higher peak area%. Table 3 lists the 30 components of L-400 with a relative content above 0.15%. Similarly, Table 4 exhibits the 34 components of L-700 with a relative content above 0.15%.

Table 3 indicates the top 5 products were acetic acid (17.12%), furfuryl alcohol (9.08%), guaiacol (5.21%), phenol (4.23%), and 2-methyl-2-cyclopenten-1-one (2.78%). Table 4 lists the top 5 products were acetic acid (11.88%), 1-2-benzenediol (8.92%), valeraldehyde (4.36%), 4-methylcatechol (3.38%), and 2-furan methanol (2.46%).

The liquids (*i.e.*, bio-oils) are intensely complex in composition and contains an army of compounds. Although they were not likely to identify each ingredient, the liquids can be divided into several main categories according to the functional groups determined by GC/MS: acids, phenols, ketones, esters, alcohol, N-containing compounds, aldehydes, sugar, and furans. Total content for liquids ranged from 68.37% for L-400 to 50.19% for L-700, resulting from some components present in liquids were not calculated. The main components of L-400 and L-700 are shown in Fig. 6(a) and (b), respectively.

As seen in Fig. 6(a), the relative contents of acids, phenols, ketones, alcohols, N-containing compounds, and sugar were

19.86%, 17.27%, 13.30%, 11.14%, 3.08%, and 0.41%, respectively. However, the relative content of sugar was below 1.00%. Compared with L-400, L-700 (as indicated in Fig. 6(b)) had fewer acids and more N-containing compounds, which is consistent with the results of the PH as well as the ultimate analysis. Notably, the composition of L-700 is more complex than that of L-400, which suggests the high temperature leads to the secondary decomposition of many substances.

3.2.4 Non-condensable gas. Fig. 7 shows the volume concentration of gases obtained from the PC pyrolysis.

The gaseous products were primarily CO₂, CO, CH₄, and H₂, which are derived from the decomposition of cellulose, hemicellulose, and lignin, and the mechanisms of their formation have been reported in the previous work.⁴⁸ Of these, CO₂ endows the highest volume concentration, followed by CO and CH₄, but pyrolysis temperature was 700 °C, the CH₄ volume concentration slightly more than the volume concentration of CO. With an increase in pyrolysis temperature, the CO volume concentration and the C_mH_n volume concentration have no significant difference, while the CH₄ volume concentration and H₂ volume concentration gradually increased. In reviewing the literature, CH₄ is mainly derived from the pyrolysis of methoxy, methyl, and methylene in lignin.⁴⁹ This suggests an increase in pyrolysis temperature, resulting in the lignin intensely decomposition, and produce more CH₄, which coincides with the



Table 4 Composition of L-700 and the relative content of the corresponding composition

Time (min)	Relative content (%)	Compound name	Molecular formula
1.769	11.88	Acetic acid	C ₂ H ₄ O ₂
12.893	8.92	1-2-Benzenediol	C ₆ H ₆ O ₂
10.492	4.36	Valeraldehyde	C ₅ H ₁₀ O
13.604	3.38	4-Methylcatechol	C ₇ H ₈ O ₂
5.150	2.46	2-Furan methanol	C ₅ H ₆ O ₂
11.248	1.96	3-Hydroxypyridine	C ₅ H ₅ ON
1.589	1.94	2-Thiourea	CH ₄ N ₂ S
2.229	1.89	3-Hydroxypropionic acid	C ₃ H ₆ O ₃
2.149	1.68	Acetoxyacetic acid	C ₄ H ₆ O ₄
8.977	1.38	2-Hydroxy-3-methylcyclopent-2-enone	C ₆ H ₈ O ₂
6.406	1.34	2-Methyl-2-imidazoline	C ₄ H ₈ N ₂
10.282	1.20	Guaiacol	C ₇ H ₈ O
8.497	1.14	N-Methylpiperidine	C ₆ H ₁₃ N
8.056	0.63	Phenol	C ₆ H ₆ O
10.903	0.45	3-Ethyl-2-hydroxy-2-cyclopenten-1-one	C ₇ H ₁₀ O ₂
18.486	0.43	Lauric acid	C ₁₂ H ₂₄ O ₂
10.808	0.40	Maltose	C ₆ H ₆ O ₃
15.750	0.37	4-Ethylresorcinol	C ₈ H ₁₀ O ₂
6.516	0.36	4-Hydroxybutyric acid	C ₄ H ₈ O ₃
7.656	0.36	2,4-Dimethylfuran	C ₆ H ₈ O
1.534	0.35	Hydroxycarbamide	CH ₄ O ₂ N ₂
12.458	0.35	2-Methoxy-4-(methoxymethyl)phenol	C ₉ H ₁₂ O ₃
5.450	0.32	Acetyl acetate	C ₅ H ₈ O ₃
9.572	0.31	Gamma-valerolactone	C ₅ H ₈ O ₂
10.082	0.31	4-Methylphenol	C ₇ H ₈ O
17.980	0.31	4-Hydroxy-3-methoxyphenylacetone	C ₁₀ H ₁₂ O ₃
13.879	0.27	4-Hydroxy-3-methoxystyrene	C ₉ H ₁₀ O ₂
13.984	0.27	m-Dihydroxybenzene	C ₆ H ₆ O ₂
7.846	0.25	Dibutylamine	C ₈ H ₁₉ N
19.751	0.24	Homovanillic acid	C ₉ H ₁₀ O ₄
1.564	0.18	Isopropylamine	C ₃ H ₉ N
7.001	0.17	3,5-Lutidine	C ₇ H ₉ N
8.822	0.17	1,2,5-Trimethylpyrrole	C ₇ H ₁₁ N
6.606	0.16	2,6-Dimethylpyrazine	C ₆ H ₈ N ₂

change of CH₄ volume concentration in this study. HHV for the gases of 400 °C, 500 °C, 600 °C, and 700 °C was 4.93 MJ kg⁻¹, 7.81 MJ kg⁻¹, 11.19 MJ kg⁻¹, and 13.68 MJ kg⁻¹, respectively. These results manifested that with an increase in pyrolysis temperature, the heating values of gaseous products gradually increased.

3.2.5 Distribution of O, C, and N in pyrolysis products. In the pyrolysis of biomass, the biomass was decomposed to produce biochar, liquid, and gaseous products. Besides, during pyrolysis, the O, C, and N elements from the biomass migrate into biochar, liquid, and gaseous products. Fig. 8(a-c) show the distribution of O, C, and N in the pyrolysis products, respectively.

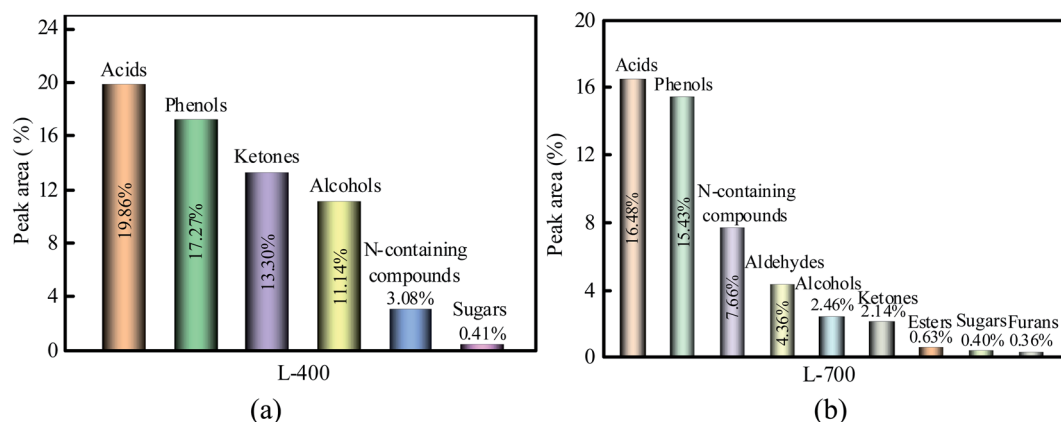


Fig. 6 Main components for L-400 and L-700 are shown in (a) and (b), respectively.



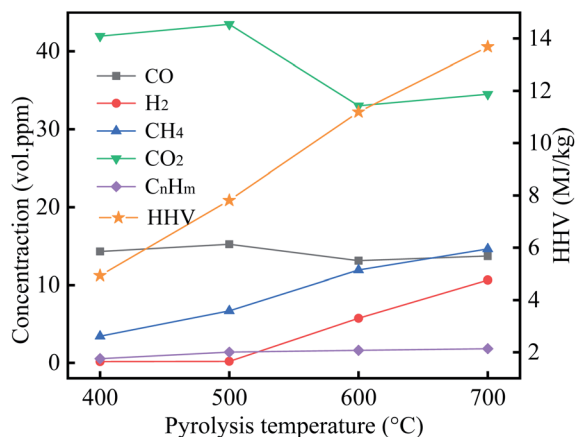


Fig. 7 Gases compositions and HHV with pyrolysis temperatures.

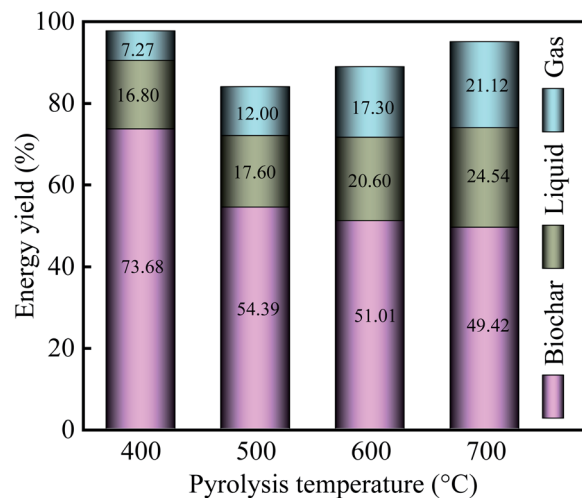


Fig. 9 Energy yield for pyrolysis products.

When the pyrolysis temperature increased from 400 °C to 700 °C, the proportion of O in biochar decreased from 24.42% to 8.63%. Similarly, the proportion of O in gaseous products decreased from 26.30% to 12.76%. In contrast, the proportion of O in liquid products increased from 52.28% to 78.13%. This means that higher temperatures intensified the deoxygenation reaction. Element O was removed from the PC and migrated into the liquid and gaseous products in the form of CO, H₂O,

CO₂, and oxygen-containing organic compounds. Notably, element O in PC was primarily transferred into H₂O, followed by CO₂ and CO. These results suggest that water and gaseous products play a vital role in deoxygenation.

When the pyrolysis temperature increased from 400 °C to 700 °C, the proportion of C in liquid products increased from

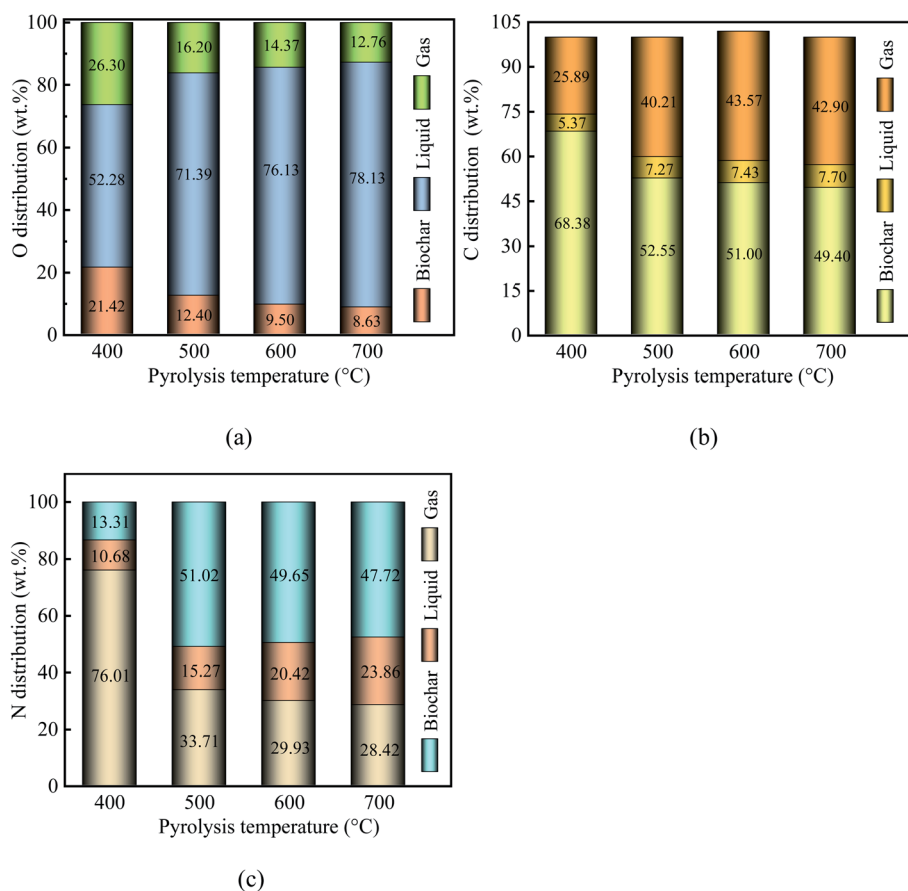


Fig. 8 Distribution of oxygen (a), carbon (b), and nitrogen (c) elements in the pyrolysis products.



Table 5 Studies concerning the removal of tetracycline employed biochar with high nitrogen content reported in the literature

Samples	Surface area (m ² g ⁻¹)	Pore volume (cm ³ g ⁻¹)	Average pore size (nm)	Nitrogen content (%)	Tetracycline removal efficiency (%)	Reference
BC300 ^a	32.2	0.022	2.5	3.54	55.45%	29
BC500 ^a	34.9	0.033	4.3	3.16	63.29%	
BC800 ^a	135.1	0.108	3.3	3.42	68.60%	
PPC-400	65.3	0.066	2.0	2.79	Further investigation	This study
PPC-N-400	246.4	0.230	1.9	3.98		

^a BCXXX stands for biochar derived from pyrolysis of fiberboard prepared at XXX °C, XXX can be 300, 500, and 800.

5.37% to 7.70%. Similarly, the proportion of C in gaseous products increased from 25.89% to 42.90%. In contrast, the proportion of O in biochar decreased from 68.38% to 49.40%. These results show that the C loss in PC was less than 50.60% over the pyrolysis temperature range. Meanwhile, with an increase in pyrolysis temperature, the proportion of N decreased from 76.01% for PPC-400 to 28.42% for PPC-700. As a result, the pyrolysis process of PC being a deoxygenation process along with C and N elements migration.

3.2.6 Energy yield for pyrolysis products. Energy yield for pyrolysis products is presented in Fig. 9. The total energy yield of pyrolysis products was below 100% resulted from the experimental errors during the collection and analysis of the pyrolysis products.

With an increase in pyrolysis temperature, the energy yield of biochar gradually decreased from 73.86% for PPC-400 to 49.42% for PPC-700, but the energy yield of liquid increased from 18.60% (400 °C) to 24.54% (700 °C). Among the three-phase products, the gases endow the lowest energy yield because it has the lowest mass yield. Notably, the energy of the biochar dominates the pyrolysis of the PC, which was consistent with the previous study.⁵⁰

3.3. Analysis of the potential for removal of tetracycline

Recently, it has been reported that biochar derived from fiberboard can remove tetracycline due to its high content of nitrogen and a certain specific surface area.²⁹ In this work, the nitrogen content of PPC-400 was similar to that of the biochar derived from fiberboard and its specific surface area was slightly higher than that of the biochar derived from fiberboard.²⁹ Interestingly, in this work, PPC-400 was obtained by pyrolysis of PC at 400 °C under the conditions of insufficient nitrogen atmosphere. Therefore, the biochar (PPC-N-400) prepared by pyrolyzing PC at 400 °C in a nitrogen atmosphere for 60 min has more nitrogen content and its specific surface area further increased. The nitrogen content and specific surface area of PPC-N-400 were higher than that of the biochar derived from fiberboard, as listed in Table 5.

Consequently, we can infer that the PPC-400 and PPC-N-400 have potential in the field for removing tetracycline. Particularly, PPC-N-400 had a significant removal effect, and its removal efficiency may be over 68.60%.²⁹

4. Conclusions

When PC was pyrolyzed, the effect of its pyrolysis temperature on the products was similar to the effect of torrefaction

pretreatment on the products. PC endows two distinct weight loss peaks in the pyrolysis temperature ranging from 200 °C to 500 °C. Of these, the weight loss peak at about 450 °C was primarily ascribed to the existence of non-structural substances. During the pyrolysis process, the deoxygenation, decarbonization, and denitrogenation of PC endow a significant effect on the physicochemical properties of biochar, liquid products, and gaseous products. After pyrolysis, oxygen was present in the gaseous state as CO₂ and CO, and also in the liquid products as oxygen-containing organic compounds and H₂O. Unlike oxygen, over 49.40% of carbon in PC was remained in PPC-X, while a small amount of carbon migrated into the liquid and gaseous products. Of note is that the energy of biochar dominates the pyrolysis of the PC. Furthermore, the nitrogen content and specific surface area of the PPC-N-400 were higher than that of the biochar derived from fiberboard. Therefore, we can infer that the PPC-N-400 has a significant effect on the removal of tetracycline.

Author contributions

Jielong Wu: data curation, investigation, and writing-original draft. Liangcai Wang: project administration, writing-original draft, editing, and supervision. Huanhuan Ma: visualization and methodology. Jianbin Zhou: supervision, writing-review, and funding acquisition.

Conflicts of interest

The authors declare no competing financial interest.

Acknowledgements

This work was supported by the National Promotion Project of China (No. 2020133136), the National Key Research and Development Plan of China (2016YFE0201800).

References

- G. Y. Wang, Y. J. Dai, H. P. Yang, Q. G. Xiong, K. G. Wang, J. S. Zhou, Y. C. Li and S. R. Wang, A review of recent advances in biomass pyrolysis, *Energy Fuels*, 2020, **34**(12), 15557–15578, DOI: 10.1021/acs.energyfuels.0c03107.
- S. S. Kim, H. V. Ly, J. Kim, J. H. Choi and H. C. Woo, Thermogravimetric characteristics and pyrolysis kinetics of



- alga sagarssum sp biomass, *Bioresour. Technol.*, 2013, **139**, 242–248, DOI: 10.1016/j.biortech.2013.03.192.
- 3 S. S. Idris, N. A. Rahman and K. Ismail, Combustion characteristics of Malaysian oil palm biomass, sub-bituminous coal and their respective blends via thermogravimetric analysis (TGA), *Bioresour. Technol.*, 2012, **123**, 581–591, DOI: 10.1016/j.biortech.2012.07.065.
- 4 A. Pimchuai, A. Dutta and P. Basu, Torrefaction of agriculture residue to enhance combustible properties, *Energy Fuels*, 2010, **24**(9), 4638–4645, DOI: 10.1021/ef901168f.
- 5 P. Rousset, C. Aguiar, N. Labbe and J. M. Commandre, Enhancing the combustible properties of bamboo by torrefaction, *Bioresour. Technol.*, 2011, **102**(17), 8225–8231, DOI: 10.1016/j.biortech.2011.05.093.
- 6 M. J. Prins, K. J. Ptasiński and F. J. J. G. Janssen, More efficient biomass gasification via torrefaction, *Energy*, 2006, **31**(15), 3458–3470, DOI: 10.1016/j.energy.2006.03.008.
- 7 K. H. Cen, J. Zhang, Z. Q. Ma, D. Y. Chen, J. B. Zhou and H. H. Ma, Investigation of the relevance between biomass pyrolysis polygeneration and washing pretreatment under different severities: Water, dilute acid solution and aqueous phase bio-oil, *Bioresour. Technol.*, 2019, **278**, 26–33, DOI: 10.1016/j.biortech.2019.01.048.
- 8 D. Ciolkosz and R. Wallace, A review of torrefaction for bioenergy feedstock production, *Biofuels, Bioprod. Biorefin.*, 2011, **5**(3), 317–329, DOI: 10.1002/bbb.275.
- 9 W. H. Chen, K. M. Lu and C. M. Tsai, An experimental analysis on property and structure variations of agricultural wastes undergoing torrefaction, *Appl. Energy*, 2012, **100**, 318–325, DOI: 10.1016/j.apenergy.2012.05.056.
- 10 T. Acharjee, C. Coronella and V. R. Vasquez, Effect of thermal pretreatment on equilibrium moisture content of lignocellulosic biomass, *Bioresour. Technol.*, 2011, **102**(7), 4849–4854, DOI: 10.1016/j.biortech.2011.01.018.
- 11 Y. Chen, L. C. Wang, M. Q. Zhao, H. H. Ma, D. Y. Chen, Y. M. Zhang and J. B. Zhou, Comparative study on the pyrolysis behaviors of pine cone and pretreated pine cone by using TGA-FTIR and pyrolysis-GC/MS, *ACS Omega*, 2021, **6**(5), 3490–3498, DOI: 10.1021/acsomega.0c04456.
- 12 B. Colin, J. L. Dirion, P. Arlabosse and S. Salvador, Quantification of the torrefaction effects on the grindability and the hygroscopicity of wood chips, *Fuel*, 2017, **197**, 232–239, DOI: 10.1016/j.fuel.2017.02.028.
- 13 S. R. Wang, G. X. Dai, B. Ru, Y. Zhao, X. L. Wang, G. Xiao and Z. Y. Luo, Influence of torrefaction on the characteristics and pyrolysis behavior of cellulose, *Energy*, 2017, **120**, 864–871, DOI: 10.1016/j.energy.2016.11.135.
- 14 S. R. Wang, G. X. Dai and B. Ru, Effects of torrefaction on hemicellulose structural characteristics and pyrolysis behaviors, *Bioresour. Technol.*, **218**, 1106–1114, DOI: 10.1016/j.biortech.2016.07.075.
- 15 G. X. Dai, Q. Zou, S. R. Wang, Y. Zhao, L. J. Zhu and Q. X. Huang, Effect of torrefaction on the structure and pyrolysis behavior of lignin, *Energy Fuels*, **32**, 4160–4166, DOI: 10.1021/acs.energyfuels.7b03038.
- 16 D. Ciolkosz and R. Wallace, A review of torrefaction for bioenergy feedstock production, *Biofuels, Bioprod. Biorefin.*, 2011, **5**(3), 317–329, DOI: 10.1002/bbb.275.2011.
- 17 M. J. C. Stelt, H. Gerhauser, J. H. A. Kiel and K. Ptasiński, Biomass upgrading by torrefaction for the production of biofuels: A review, *Biomass Bioenergy*, 2011, **35**(9), 3748–3762, DOI: 10.1016/j.biombioe.2011.06.023.
- 18 J. J. Chew and V. Doshi, Recent advances in biomass pretreatment-torrefaction fundamentals and technology, *Renewable Sustainable Energy Rev.*, 2011, **15**(8), 4212–4222, DOI: 10.1016/j.rser.2011.09.017.
- 19 Q. V. Bach and Ø. Skreiberg, Upgrading biomass fuels via wet torrefaction: A review and comparison with dry torrefaction, *Renewable Sustainable Energy Rev.*, 2016, **54**, 665–677, DOI: 10.1016/j.rser.2015.10.014.
- 20 Q. V. Bach, W. H. Chen, Y. S. Chu and Ø. Skreiberg, Predictions of biochar yield and elemental composition during torrefaction of forest residues, *Bioresour. Technol.*, 2016, **215**, 239–246, DOI: 10.1016/j.biortech.2016.04.009.
- 21 L. W. Li, Y. Q. Huang, D. Y. Zhang, A. Q. Zheng, Z. L. Zhao, M. Z. Xia and H. B. Li, Uncovering structure-Reactivity relationships in pyrolysis and gasification of biomass with varying severity of torrefaction, *ACS Sustainable Chem. Eng.*, 2018, **6**(5), 6008–6017, DOI: 10.1021/acssuschemeng.7b04649.
- 22 W. H. Chen, S. H. Liu, T. T. Juang, C. M. Tsai and Y. Q. Zhuang, Characterization of solid and liquid products from bamboo torrefaction, *Appl. Energy*, 2015, **160**, 829–835, DOI: 10.1016/j.apenergy.2015.03.022.
- 23 D. Y. Chen, J. M. Mei, H. P. Li, Y. M. Li, M. T. Lu, T. T. Ma and Z. Q. Ma, Combined pretreatment with torrefaction and washing using torrefaction liquid products to yield upgraded biomass and pyrolysis products, *Bioresour. Technol.*, 2017, **228**, 62–68, DOI: 10.1016/j.biortech.2016.12.088.
- 24 A. K. Mondal, K. Kretschmer, Y. F. Zhao, H. Liu, H. B. Fan and G. X. Wang, Naturally nitrogen doped porous carbon derived from waste shrimp shells for high-performance lithium ion batteries and supercapacitors, *Microporous Mesoporous Mater.*, 2017, **246**, 72–80, DOI: 10.1016/j.micromeso.2017.03.019.
- 25 W. Ai, Z. M. Luo, J. Jiang, J. H. Zhu, Z. Z. Du, Z. X. Fan, L. H. Xie, H. Zhang and T. Yu, Nitrogen and sulfur codoped graphene: multifunctional electrode materials for high-performance Li-ion batteries and oxygen reduction reaction, *Adv. Mater.*, 2014, **26**(35), 6186–6192, DOI: 10.1002/adma.201401427.
- 26 D. S. Yang, D. Bhattacharjya, S. Inamdar, J. Park and J. S. Yu, Phosphorus-doped ordered mesoporous carbons with different lengths as efficient metal-free electrocatalysts for oxygen reduction reaction in alkaline media, *J. Am. Chem. Soc.*, 2012, **134**(39), 16127–16130, DOI: 10.1021/ja306376s.
- 27 M. Schnucklake, L. Eifert, J. Schneider, R. Zeis and C. Rorh, Porous N- and S-doped carbon-carbon composite electrodes by soft-templating for redox flow batteries, *Beilstein J. Nanotechnol.*, 2019, **10**(1), 1131–1139, DOI: 10.3762/bjnano.10.113.



- 28 A. Laheäär, S. Delpoux-Ouldriane, E. Lust and F. Beguin, Ammonia treatment of activated carbon powders for supercapacitor electrode application, *J. Electrochem. Soc.*, 2014, **161**(4), A568–A575, DOI: 10.1149/2.051404jes.
- 29 D. L. Xu, Y. X. Gao, Z. X. Lin, W. R. Gao, H. Zhang, K. Karnowo, X. Hu, H. Q. Sun, S. S. A. Syed-Hassan and S. Zhang, Application of biochar derived from pyrolysis of waste fiberboard on tetracycline adsorption in aqueous solution, *Front. Chem.*, 2020, **7**, DOI: 10.3389/fchem.2019.00943.
- 30 J. Yi, H. Qu, Y. Wu, Z. Wang and L. Wang, Study on antitumor, antioxidant and immunoregulatory activities of the purified polyphenols from pinecone of *Pinus koraiensis* on tumor-bearing S180 mice in vivo, *Int. J. Biol. Macromol.*, 2016, **94**, 735–744, DOI: 10.1016/j.ijbiomac.2016.10.071.
- 31 Z. H. Jiang, Z. J. Liu, B. H. Fei, Z. Y. Cai, Y. Yu and X. E. Liu, The pyrolysis characteristics of moso bamboo, *J. Anal. Appl. Pyrolysis*, 2012, **94**, 48–52, DOI: 10.1016/j.jaap.2011.10.010.
- 32 X. L. Gu, X. Ma, L. X. Li, C. Liu, K. H. Cheng and Z. Z. Li, Pyrolysis of poplar wood sawdust by TG-FTIR and PY-GC/MS, *J. Anal. Appl. Pyrolysis*, 2013, **102**, 16–23, DOI: 10.1016/j.jaap.2013.04.009.
- 33 R. Azargohar, S. Nanda, J. A. Kozinski, A. K. Dalai and R. Sutarto, Effects of temperature on the physicochemical characteristics of fast pyrolysis bio-chars derived from Canadian waste biomass, *Fuel*, 2014, **125**, 90–100, DOI: 10.1016/j.fuel.2014.01.083.
- 34 V. Pasangulapati, A. Kumar, C. L. Jones and R. L. Huhnke, Characterization of switchgrass cellulose. Hemicellulose and lignin for thermochemical conversions, *J. Biobased Mater. Bioenergy*, 2012, **6**(3), 249–258, DOI: 10.1166/jbmb.2012.1216.
- 35 H. Yang, R. Yan, H. Chen, D. H. Lee and C. Zheng, Characteristics of hemicellulose, cellulose and lignin pyrolysis, *Fuel*, 2007, **86**(12), 1781–1788, DOI: 10.1016/j.fuel.2006.12.013.
- 36 L. Burhenne, J. Messmer, T. Aicher and M. P. Laborie, The effect of the biomass components lignin, cellulose and hemicellulose on TGA and fixed bed pyrolysis, *J. Anal. Appl. Pyrolysis*, 2013, **101**, 177–184, DOI: 10.1016/j.jaap.2013.01.012.
- 37 J. J. Chew, V. Doshi, S. T. Yong and S. Bhattacharya, Kinetic study of torrefaction of oil palm shell, mesocarp and empty fruit bunch, *J. Therm. Anal. Calorim.*, 2016, **126**(2), 1–7, DOI: 10.1007/s10973-016-5518-3.
- 38 Y. P. Xie, K. Zeng, G. Flamant, H. P. Yang, N. Liu, X. He, X. Y. Yang, A. Nzijou and H. P. Chen, Solar pyrolysis of cotton stalk in molten salt for bio-fuel production, *Energy*, 2019, **179**(JUL15), 1124–1132, DOI: 10.1016/j.energy.2019.05.055.
- 39 B. Arias, C. Pevida, J. Feroso, M. G. Plaza, F. Rubiera and J. J. Pis, Influence of torrefaction on the grindability and reactivity of woody biomass, *Fuel Process. Technol.*, 2008, **89**(2), 169–175, DOI: 10.1016/j.fuproc.2007.09.002.
- 40 D. Sahoo and N. Remya, Influence of operating parameters on the microwave pyrolysis of rice husk: biochar yield, energy yield, and property of biochar, *Biomass Convers. Biorefin.*, 2020, **8**, DOI: 10.1007/s13399-020-00914-8.
- 41 P. Quosai, A. Anstey, A. Mohanty and M. Misra, Characterization of biocarbon generated by high-and low-temperature pyrolysis of soy hulls and coffee chaff: for polymer composite applications, *R. Soc. Open Sci.*, 2018, **5**(8), 171970, DOI: 10.1098/rsos.171970.
- 42 K. Kameyama, T. Miyamoto and Y. Iwata, The preliminary study of water-retention related properties of biochar produced from various feedstock at different pyrolysis temperatures, *Materials*, 2019, **12**(11), 1732, DOI: 10.3390/ma12111732.
- 43 H. L. Wang, D. J. Wu, J. B. Zhou, H. H. Ma, D. L. Xu, B. Qian, S. Tao and Z. Wang, Preparation of supercapacitor electrode from gasified rice husk carbon, *Bioresources*, 2018, **13**, 4279–4289, DOI: 10.15376/biores.13.2.4279-4289.
- 44 A. Afnan and M. Robert, Predictable and targeted activation of biomass to carbons with high surface area density and enhanced methane storage capacity, *Energy Environ. Sci.*, 2020, **13**, 2967–2978, DOI: 10.1039/D0EE01340D.
- 45 T. T. Li, Z. H. Tong, B. Gao, Y. C. Li, A. Smyth and H. K. Bayabil, Polyethyleneimine-modified biochar for enhanced phosphate adsorption, *Environ. Sci. Pollut. Res.*, 2020, **27**, 7420–7429, DOI: 10.1007/s11356-019-07053-2.
- 46 L. C. Wang, J. L. Wu, H. H. Ma, G. L. Han, D. R. Yang, Y. Chen and J. B. Zhou, H₃PO₄-assisted synthesis of apricot shell lignin-based activated carbon for capacitors: understanding the pore structure/electrochemical performance relationship, *Energy Fuels*, 2021, **35**, 8303–8312, DOI: 10.1021/acs.energyfuels.1c00169.
- 47 M. Phanphanich and S. Mani, Impact of torrefaction on the grindability and fuel characteristics of forest biomass, *Bioresour. Technol.*, 2011, **102**(2), 1246–1253, DOI: 10.1016/j.biortech.2010.08.028.
- 48 Z. Q. Ma, J. H. Wang, H. Z. Zhou, Y. Zhang, Y. Y. Yang, X. H. Liu, J. W. Ye, D. Y. Chen and S. R. Wang, Relationship of thermal degradation behavior and chemical structure of lignin isolated from palm kernel shell under different process severities, *Fuel Process. Technol.*, 2018, **181**, 142–156, DOI: 10.1016/j.fuproc.2018.09.020.
- 49 Q. Liu, S. R. Wang, Y. Zheng, Z. Y. Luo and K. F. Cen, Mechanism study of wood lignin pyrolysis by using TG-FTIR analysis, *J. Anal. Appl. Pyrolysis*, 2008, **82**, 170–177, DOI: 10.1016/j.jaap.2008.03.007.
- 50 J. Park, Y. Lee, C. Ryu and Y. K. Park, Slow pyrolysis of rice straw: analysis of products properties, carbon and energy yields, *Bioresour. Technol.*, 2014, **155**, 63–70, DOI: 10.1016/j.biortech.2013.12.084.

