



Cite this: *J. Mater. Chem. A*, 2022, 10, 19412

## Advances in understanding and regulation of sulfur conversion processes in metal–sulfur batteries

Fangyi Shi,<sup>†ab</sup> Jingya Yu,<sup>†ac</sup> Chunhong Chen,<sup>†a</sup> Shu Ping Lau,<sup>b</sup> Wei Lv<sup>id</sup><sup>d</sup> and Zheng-Long Xu<sup>id</sup><sup>\*ace</sup>

Lithium–sulfur batteries (LSBs) have attracted intensive attention as promising next-generation energy storage systems, due to the high energy density and low cost of sulfur cathodes. Despite the substantial progress in improving LSBs' performance, their wide implementation still suffers from great challenges, including the difficulties in achieving practically high energy density with long cycle life and the concerns about the limited lithium resources. The former issue mainly arises from the insufficient understanding of the mechanics of the complex lithium–sulfur redox reactions, while the latter trigger the exploration of a range of new metal–sulfur systems, such as sodium–sulfur, potassium–sulfur, magnesium–sulfur, calcium–sulfur, and aluminum–sulfur batteries. These lithium-free metal–sulfur batteries (MSBs) have the potential to offer higher energy density or/and lower battery costs. The fundamental understanding and rational regulation of effective metal–sulfur conversion reactions are crucial for developing advanced and emerging MSBs. Herein, this work aims to overview the state-of-the-art progress in circumventing these issues of MSBs, in terms of working mechanisms, key factors determining the electrochemical behavior and battery performance. Advanced *in situ* characterization techniques used to disclose the sulfur conversion mechanisms are also elaborately discussed. Conclusions and perspectives for the future research direction in MSBs are proposed.

Received 21st March 2022  
Accepted 4th July 2022

DOI: 10.1039/d2ta02217f

rsc.li/materials-a

### 1. Introduction

Rechargeable batteries are expected to be promising systems for dealing with the energy crisis and environmental pollution

caused by the combustion of fossil fuels.<sup>1</sup> Since their successful launch in the 1990s, lithium-ion batteries (LIBs) have dominated the portable power market and are now penetrating into the green transportation sector *via* propelling electric vehicles.

<sup>a</sup>Department of Industrial and Systems Engineering, The Hong Kong Polytechnic University, Hung Hom, Hong Kong, P. R. China. E-mail: zhenglong.xu@polyu.edu.hk

<sup>b</sup>Department of Applied Physics, The Hong Kong Polytechnic University, Hung Hom, Hong Kong, P. R. China

<sup>c</sup>State Key Laboratory of Ultraprecision Machining Technology, The Hong Kong Polytechnic University, Hung Hom, Hong Kong, P. R. China

<sup>d</sup>Shenzhen Geim Graphene Center, Engineering Laboratory for Functionalized Carbon Materials, Tsinghua Shenzhen International Graduate School, Tsinghua University, Shenzhen, P. R. China

<sup>e</sup>Hong Kong Polytechnic University Shenzhen Research Institute, Shenzhen, 518057, P. R. China

<sup>†</sup> These authors contributed equally.



Fangyi Shi obtained her bachelor's degree from the Powder Metallurgy Research Institute, Central South University, China, in 2015. Now, she is studying for a PhD degree at the Hong Kong Polytechnic University. Her research interests include metal sulfur batteries and *in situ* characterization.



Shu Ping Lau is a Chair Professor in the Department of Applied Physics at the Hong Kong Polytechnic University. He obtained his PhD from the University of Wales Swansea. Prof. Lau's current research focuses on nanomaterials and energy materials, particularly the synthesis of 2D materials for optoelectronics, electrocatalysis, and energy storage applications.

Table 1 The comparison of metal–sulfur batteries

| Metal–sulfur batteries | Discharge products                             | Theoretical voltage ( $E^0/V$ ) <sup>8</sup> | Volume expansion ( $\Delta V$ , %) | Gravimetric energy density ( $W\ h\ kg^{-1}$ ) <sup>8</sup> | Volumetric energy density ( $W\ h\ l^{-1}$ ) <sup>8</sup> | Metal abundance (ppm) <sup>7</sup> |
|------------------------|--|--|------------------------------------|---|---|------------------------------------|
| Li–S                   | Li <sub>2</sub> S                              | 2.24   | 80                                 | 2612  | 2955  | 20                                 |
| Na–S                   | Na <sub>2</sub> S                              | 1.85   | 180                                | 1270  | 1545  | 23 600                             |
| K–S                    | K <sub>2</sub> S/K <sub>2</sub> S <sub>3</sub> | 1.88   | 309                                | 916   | 952   | 20 900                             |
| Mg–S                   | MgS  | 1.77   | 24                                 | 1685  | 3221  | 950                                |
| Ca–S                   | CaS  | 2.47   | 80                                 | 1838  | 3202  | 41 500                             |
| Al–S                   | Al <sub>2</sub> S <sub>3</sub>                 | 1.23   | 40                                 | 1319  | 2981  | 82 300                             |

However, the energy density of LIBs has encountered a bottleneck due to the limited capacity (below 300 mA h g<sup>-1</sup>) of metal oxide cathodes.<sup>1,2</sup> Exploring new battery systems with higher energy densities and lower cost than current LIBs is thus crucial to realize further electrification and carbon neutrality of our modern society. Among the few options, metal–sulfur electrochemistry has been considered promising due to the 2-electron redox reaction per sulfur atom, leading to an exceptionally high theoretical capacity of 1672 mA h g<sup>-1</sup> for sulfur cathodes. Owing to the appealing properties of low cost (\$150 per ton), eco-friendliness, and abundant supply of sulfur, metal–sulfur batteries (MSBs) are regarded as the next-generation energy storage devices.<sup>3,4</sup> Li–S batteries (LSBs) have been intensively investigated since the report on a high-performance CMK-3/sulfur cathode by Nazar's group in 2009.<sup>5,6</sup> Recently, propelled by the concerns over Li supply due to its limited and uneven distribution in the Earth's crust, research on Li-free metal–sulfur (*i.e.*, Na–S, K–S, Mg–S, and Ca–S) batteries has been prospering.<sup>5,7</sup> MSB systems share a similar cell configuration and working mechanisms. Their properties in terms of metal abundance, electrochemical properties, volume expansion, and energy density are summarized in Table 1.<sup>7,8</sup>

Unlike the intercalation chemistry of conventional LIB cathodes, metal–sulfur electrochemistry involves complicated phase transitions during cycling. Taking the LSB as an example, the discharging process involves the reduction of solid sulfur (S<sub>8</sub>) to soluble polysulfides (Li<sub>2</sub>S<sub>*n*</sub>, 4 ≤ *n* ≤ 8) and then to solid lithium sulfides (Li<sub>2</sub>S<sub>*n*</sub>, 1 ≤ *n* ≤ 2).<sup>9</sup> During the following

charging process, the lithium sulfides are oxidized to elemental sulfur inversely. The sulfur conversion processes are closely related to the starting materials, working conditions, and electrode structures. The soluble intermediates induce primary problems in LSBs, including the polysulfide shuttle effect, the corrosion of Li metal, the depletion of electrolyte due to the reaction of Li and S<sub>*x*</sub><sup>2-</sup>, and the isolation of active materials from conductive hosts.<sup>1</sup> The precipitation of insulating lithium sulfides from soluble polysulfides is kinetically sluggish, which deteriorates polysulfide diffusion and causes incomplete sulfur utilization. Other categories of problems of LSBs, such as the insulating nature of sulfur species and the large volume expansion of sulfur upon lithiation (*i.e.*, 80%), induce persistent challenges in conversion electrodes. Consequently, large polarization with poor rate capability and inferior cyclability are often prevalent in LSBs.

To address the above fundamental challenges, tremendous efforts have been devoted to engineering the cathode structure/chemistry and understanding the sulfur conversion mechanisms. In the early stage of LSB research, most studies focused on the development of composite cathodes for improved electrochemical performance,<sup>10</sup> such as porous carbon/sulfur and electrocatalyst/sulfur cathodes. In recent years, it has been convergently realized that it is imperative to achieve a better understanding of the reaction mechanisms and effective regulation of this system,<sup>11</sup> such as the redox process and the chemical/electrochemical reaction kinetics, to further pave the way towards commercial LSBs. Postmortem analyses of cycled LSBs have been conducted to monitor the chemical/physical states of active materials. However, considering that the polysulfide intermediates are air-sensitive and transient, *ex situ* characterization studies often fail in presenting the full picture of the electrochemical reaction occurring in LSBs. In contrast, various *in situ* characterization methods, such as *in situ* X-ray absorption near-edge structure (XANES) and X-ray diffraction (XRD) characterization, allow real-time detection of the chemical structure evolution in working batteries, enabling the decipherment of the complicated reaction processes without sample contaminants.<sup>11–22</sup> *In situ* characterization studies not only provide an in-depth understanding of the redox chemistry in MSBs, but also offer fundamental guidelines for the rational design of sulfur cathodes for achieving improved electrochemical performance.<sup>11</sup>

Some review papers have summarized the sulfur cathode engineering strategies for LSBs by highlighting the improvement in battery performance. However, several fundamental



Zheng-Long Xu is an assistant professor in the Department of Industrial and Systems Engineering at The Hong Kong Polytechnic University. He received his BSc in Materials Science and Engineering from Zhejiang University and PhD in Mechanical Engineering from The Hong Kong University of Science and Technology. His research group at PolyU focuses on developing new materials and devices for post-Li battery chemistries (*i.e.*, Li–S, Na-ion, and Ca-ion batteries) and operando characterization technologies (*i.e.*, *in situ* TEM).

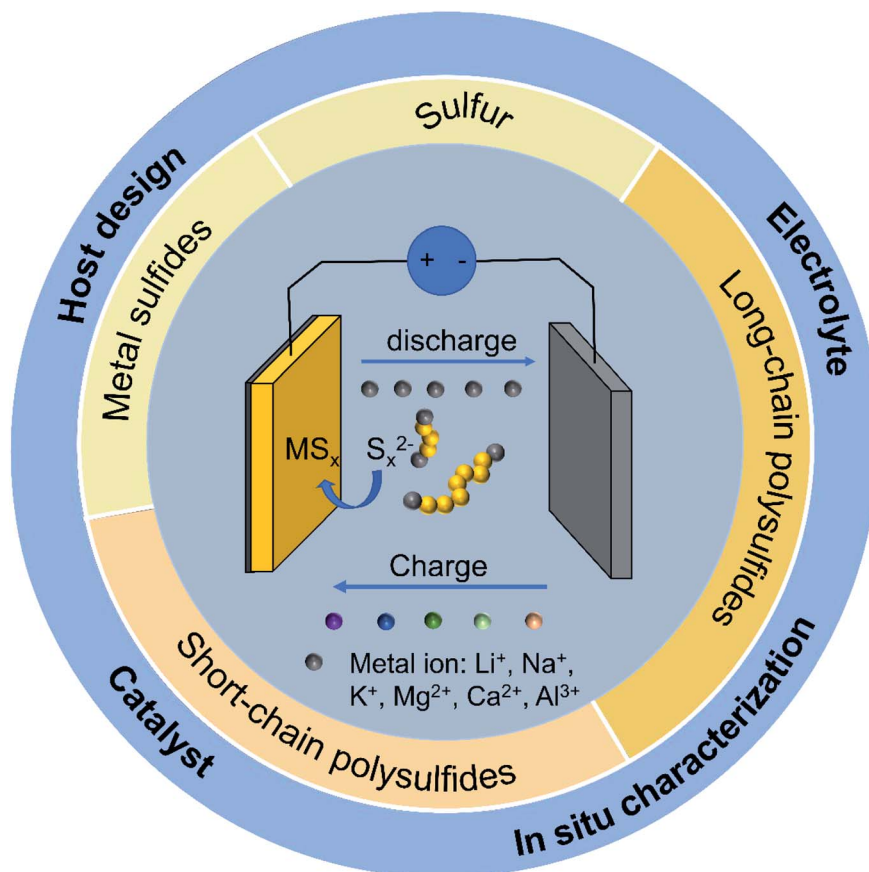


Fig. 1 Schematic illustration of representative strategies to regulate sulfur conversion in metal-sulfur batteries.

features from the recent developments of MSBs have rarely been explored, namely (i) the electrochemical and chemical working mechanisms in LSBs using different electrolytes, substrates, and catalysts; (ii) the sulfur conversion electrochemistry in Li-free MSB systems regarding the electrode/electrolyte compatibility, reaction kinetics for high valence cations, and the battery failing mechanisms; and (iii) the state-of-the-art understanding of sulfur conversion mechanics through *in situ* characterization. Here, this paper primarily discusses these aspects (Fig. 1). The reaction processes and strategies to regulate the sulfur conversion in LSBs will be elaborated by elucidating the correlation among starting materials, electrolytes, electrocatalysts, and reaction processes. Moreover, we discuss the most recent findings in Li-free MSBs, including Na-S, K-S, Mg-S, and Al-S cells with emphasis on surveying reaction processes and battery failure mechanisms. Subsequently, advanced *in situ* characterization tools to reveal the working mechanisms of MSBs are highlighted. Finally, our perspectives are provided on the remaining issues for future research in MSBs.

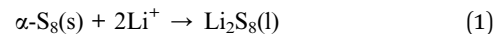
## 2. Li-S batteries

### 2.1 Reaction mechanisms in a typical Li-S battery

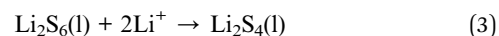
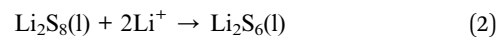
A typical LSB consists of a Li metal anode, a sulfur-based cathode, and a separator soaked with electrolyte inserted between them. The discharge/charge process is the reversible

conversion between S<sub>8</sub> and Li<sub>2</sub>S, involving complex phase transitions as shown in Fig. 2a.<sup>23,24</sup> The Li-S conversion process in discharge can be categorized into four regions as listed below:<sup>9</sup>

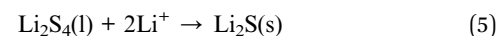
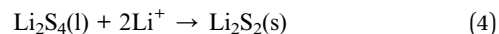
Region I (solid-liquid two-phase conversion, α-sulfur is lithiated to Li<sub>2</sub>S<sub>8</sub>):



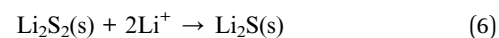
Region II (liquid-liquid single-phase conversion, Li<sub>2</sub>S<sub>8</sub> is lithiated to short-chain polysulfides):



Region III (liquid-solid two-phase conversion, Li<sub>2</sub>S<sub>4</sub> is reduced to Li<sub>2</sub>S<sub>2</sub>/Li<sub>2</sub>S):



Region IV (solid-solid single-phase conversion, Li<sub>2</sub>S<sub>2</sub> is lithiated to Li<sub>2</sub>S):



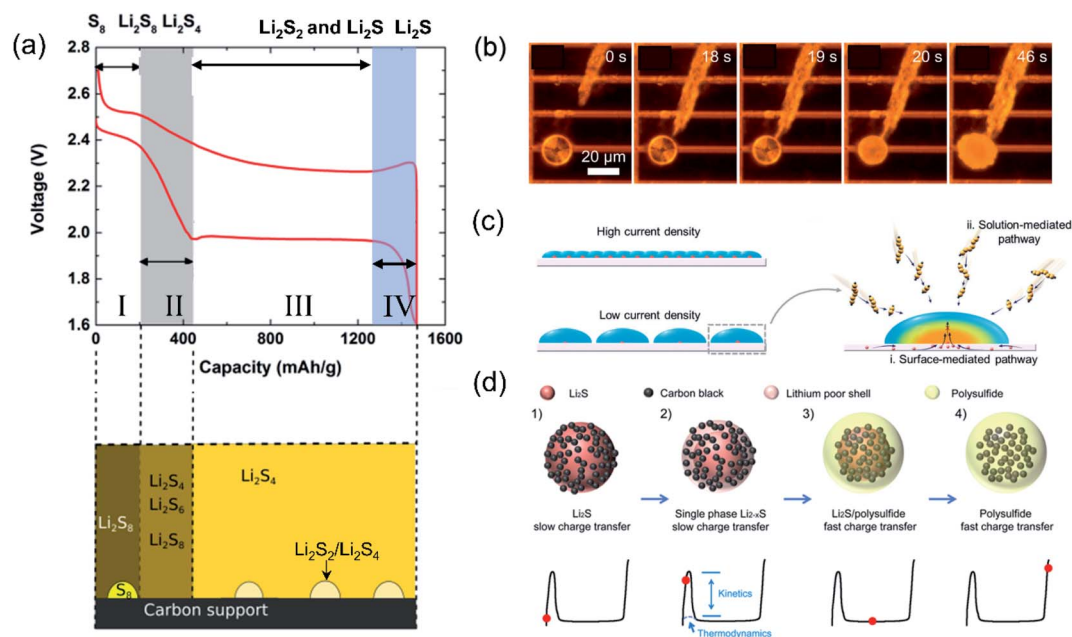


Fig. 2 (a) Schematic illustration of the reaction process and related reaction products of Li-S batteries. Reproduced with permission: Copyright 2019, Royal Society of Chemistry.<sup>41</sup> (b) Photo of liquid sulfur converted to solid sulfur. Reproduced with permission: Copyright 2019, National Academy of Sciences.<sup>28</sup> (c) The different  $Li_2S$  growth mechanisms under high current density and low current density. Reproduced with permission: Copyright 2019, Royal Society of Chemistry.<sup>42</sup> (d) Schematic diagram of the activation process of  $Li_2S$ . Reproduced with permission: Copyright 2012, American Chemistry Society.<sup>44</sup>

The diffusion of lithium polysulfides (LiPSs) is considered the most challenging issue, hindering the practical implementation of LSBs. In the following, we will give in-depth insights into the electrochemical/chemical reactions involving polysulfides in LSBs.

**2.1.1 Redox reaction between sulfur and lithium polysulfides.** In Region I, sulfur is converted to long-chain LiPSs ( $Li_2S_8$ ) with an apparent discharge plateau at approximately 2.4 V, which contributes  $209 \text{ mA h g}^{-1}$  ( $\sim 12.5\%$  of the theoretical capacity). During charging, the  $Li_2S_8$  can be reversibly delithiated to sulfur. Interestingly, *in situ* XRD studies show that the charging product is the monoclinic  $\beta$ -phase instead of the original orthorhombic  $\alpha$ -phase.<sup>25</sup>  $\beta$ -sulfur is considered stable normally above  $96^\circ\text{C}$  but it can stably exist in the electrochemical system at room temperature (RT).<sup>26</sup> Note that  $\beta$ -sulfur can also be obtained by the melt-diffusion method for sulfur/carbon cathodes.<sup>27</sup>

Another metastable sulfur species generated through electrochemical redox of polysulfides is liquid sulfur, which was recently observed during polysulfide oxidation on an Au substrate.<sup>28</sup> Liquid sulfur was also identified to form on the basal plane of two-dimensional (2D) materials (*i.e.*, graphite,  $MoS_2$ , and  $WS_2$ ).<sup>29</sup> If the 2D material is thick (tens of nanometers), however, solid sulfur nucleates at the edge areas. The liquid sulfur formed on the basal plane would be quickly transformed to solid  $\beta$ -sulfur once it comes in contact with the solid sulfur propagating from the edge areas (Fig. 2b). In addition, the formation of liquid sulfur was reported to be substrate-dependent, where no sulfur droplets were observed on glassy carbon, graphene-nickel foam, and carbon-coated

aluminum.<sup>28,30</sup> Compared to solid sulfur, liquid sulfur resulted in superior reaction kinetics and area capacities due to its unique mobility and reshaping capability.<sup>29</sup> Liquid sulfur also creates an opportunity to allow the conversion between sulfur and LiPSs to change from a solid/liquid reaction to a liquid/liquid reaction, which shows promise to design flow batteries and fast-charging batteries. However, studies on liquid sulfur chemistry are still in infancy. Several critical questions remain to be explored, namely (i) liquid sulfur is preserved much below sulfur's melting point ( $115^\circ\text{C}$ ).<sup>28</sup> The origin of this thermodynamically unstable phase is unclear; (ii) liquid sulfur was virtually observed in flooded-electrolyte LSBs, and the scenarios in high sulfur loading ( $>7 \text{ mg cm}^{-2}$ ) and lean-electrolyte ( $<4 \mu\text{L mg}^{-1}$ ) conditions have not been explored; (iii) liquid sulfur is metastable and readily dissolves in electrolyte. Preserving liquid sulfur for reversible liquid LSBs is also challenging.

**2.1.2 Redox reaction between long-chain and short-chain polysulfides.** In Region II, long-chain  $Li_2S_8$  is further reduced to short-chain  $Li_2S_x$  ( $4 < x \leq 6$ ) showing a slope from 2.4 to 2.1 V.<sup>31</sup> At the end of this stage, the viscosity of the electrolyte reaches the vertex arising from the major product  $S_4^{2-}$ .<sup>32</sup> This step associated with the liquid-liquid single-phase reaction is believed to exhibit fast reaction kinetics. The LiPSs' status is highly subject to electrolyte properties, such as the solvent species, the solubility of LiPSs, and salt concentration.<sup>33</sup> The electrolyte structure can also regulate the reaction pathway in Region II. For example, the stable  $S_3^{\cdot-}$  radical was generated through  $S_6^{2-}$  dissociation in a high-donor-number (DN) solvent electrolyte (*i.e.*, dimethyl sulfoxide, DMSO,  $DN_{\text{DMSO}} = 29.8$ ), whereas a low-DN solvent electrolyte (*i.e.*, dimethoxyethane/

dioxolane, DME/DOL,  $DN_{DOL} = 18$ ) mainly involves  $S_4^{2-}$  formation.<sup>32</sup>

Apart from the intrinsic LiPS chemistry, the extrinsic behavior of LiPSs (*e.g.*, diffusion, dissolution, and shuttling) can induce both favorable and unfavorable impacts on LSBs. The electronically insulating LiPSs are soluble in ether-based electrolytes. During discharging, they are susceptible to losing contact with the cathode and gradually diffuse to the anode side driven by the concentration gradient or/and electric field, resulting in the corrosion of Li metal and irreversible loss of active materials. During charging, the short-chain LiPSs deposited on Li metal would be re-oxidized and diffuse back to the cathode, leading to low coulombic efficiency and severe self-discharge. Therefore, the shuttling of LiPSs back and forth between electrodes, the so-called shuttling effect, results in amplified electrolyte depletion, capacity degradation, and battery failure.<sup>34</sup> Alternatively, LiPSs also play favorable roles in improving the reaction kinetics in LSBs. Upon discharging, LiPSs are able to react with insulating sulfur *via* chemical disproportionation (*e.g.*,  $S_8 + Li_2S_4 \rightarrow Li_2S_6$ ), thus dragging the insulating sulfur into the electrolyte for further conversion reaction. A similar effect also occurs in the charging process, where liquid LiPSs catalyze the oxidation of  $Li_2S$  to overcome its dramatically high activation energy barrier.<sup>34</sup> In short, soluble LiPS is a double-edged sword that is both harmful and beneficial to the Li-S electrochemistry. How to rationally manipulate the LiPS behavior to reinforce the advantageous properties while suppressing the negative effect is a challenging and rewarding direction for future LSB study.

### 2.1.3 Redox reaction between short-chain LiPSs and $Li_2S$ .

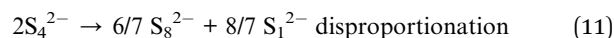
The further reduction from soluble  $Li_2S_4$  to solid  $Li_2S/Li_2S_2$  (Region III) is kinetically sluggish, and the solid-solid conversion kinetics between  $Li_2S$  and  $Li_2S_2$  in Region IV is slower. A potential dip is usually observed at the beginning of Region III, due to the centripetal polarization from highly viscous  $Li_2S_4$  (ref. 35) and the overpotential to drive solid phase nucleation.<sup>29</sup> Regions III and IV contribute  $1254 \text{ mA h g}^{-1}$  (*i.e.*, 75% of the theoretical capacity), and thus their reaction kinetics, depth, and reversibility play critical roles in the battery performance.

The electrochemical deposition of  $Li_2S_2/Li_2S$  from soluble polysulfides involves solid nucleation and growth behavior. Chiang *et al.*<sup>36</sup> demonstrated that the nucleation of lithium sulfides on conductive substrates occurred along the three-phase boundary between solid lithium sulfide precipitates, the conductive substrate, and the polysulfide solution. The deposition behavior is associated with the host surface chemistry,<sup>37</sup> separators,<sup>38</sup> and electrolyte structures.<sup>39</sup> For example, three-dimensional (3D)  $Li_2S$  precipitation was achieved by decorating carbon hosts with black phosphorus quantum dot (BPQD) catalysts.<sup>40</sup> High-DN solvent-based electrolytes can ameliorate the LiPS solubility to promote 3D  $Li_2S$  deposition.<sup>41</sup> In addition, current densities also influenced the deposition morphologies of  $Li_2S_2/Li_2S$ .<sup>42</sup> It was reported that the precipitation of  $Li_2S_2/Li_2S$  at a high current density ( $360 \mu\text{A cm}^{-2}$ ) followed a surface deposition route but a solution-mediated growth model at a low current density ( $9 \mu\text{A cm}^{-2}$ , Fig. 2c). As a result,  $Li_2S$  would form thin and continuous films with large nucleation density at high

current density, and in contrast, large and discrete  $Li_2S$  particles were observed at low deposition current.<sup>42,43</sup> Given the insulating nature of  $Li_2S/Li_2S_2$ , the in-solution growth model is more favorable with larger precipitate volumes and higher sulfur utilization than the surface-deposition counterpart.

During the charging process,  $Li_2S_2/Li_2S$  would be dissolved and converted to LiPSs. Similar to its precipitation mechanism, dissolution of  $Li_2S_2/Li_2S$  only occurs at the three-phase boundary among the  $Li_2S/Li_2S_2$ , host, and electrolyte with electronic and ionic conductivities.<sup>44</sup> At the beginning of the charging curve (Fig. 2a), a potential hill can be clearly observed, representing an extra driving force to activate the  $Li_2S_2/Li_2S$  oxidation.<sup>10,44</sup> The potential hill is related to several key parameters, namely (i) the phase and crystallinity of  $Li_2S/Li_2S_2$ , (ii) the electronic/ionic conductivity of the substrate, and (iii) the presence of mediators, such as LiPSs. Compared to highly crystalline  $Li_2S/Li_2S_2$ , oxidation of the amorphous phase was reported to be easier without residuals after full charging.<sup>45</sup> Because of the improved conductivity of few-layer graphene wrapped  $Li_2S$ , the  $Li_2S@graphene$  nanocapsules exhibited notable area capacities of  $8.1 \text{ mA h cm}^{-2}$  at a high loading of  $10 \text{ mg cm}^{-2}$ .<sup>46</sup> When micronized  $Li_2S$  is directly used as the cathode, it required an activation voltage of over 3.5 V, and the activation process is displayed in Fig. 2d.<sup>47</sup> After the first cycle, the overpotential for charging in the later cycles became much smaller. It is attributed to the presence of LiPSs to mediate the  $Li_2S$  dissolution.<sup>44</sup> Moreover,  $Li_2S$ -metal/carbon composites,<sup>47,48</sup> redox mediators in electrolytes,<sup>49,50</sup> and electrocatalysts<sup>51,52</sup> have also been demonstrated to be efficient in alleviating the  $Li_2S_2/Li_2S$  activation barrier for improved cycling capacities.

**2.1.4 Chemical reaction among polysulfides.** Apart from electrochemical reactions, chemical reactions among LiPSs also occur in LSBs and contribute capacities. In DMSO and DME/DOL electrolytes, for example, the (electro)chemical reactions can be depicted as follows:<sup>53</sup>



Taking the electrochemical reaction into consideration as well, we can find that the reaction process in LSBs is very complex. In addition, different solvents would induce different reaction pathways (both chemical and electrochemical reactions). For example, the disproportionation reactions in eqn (9) and (10) are prone to happen in electron-pair donor solvents with high dielectric constant (*i.e.*, DMSO). Some disproportionation reactions are disadvantageous to battery cycling. The solid products generated in the disproportionation reactions of LiPSs (eqn (9) and (11)) would increase the interfacial resistance by passivating electrode surfaces.<sup>54</sup> The disproportionation between LiPSs may also induce LiPS accumulation and

diffusion.<sup>55</sup> Therefore, understanding and regulating the chemical reactions are of significance to draw a whole picture of sulfur conversion chemistry and guide the  $\text{Li}_2\text{S}$  or  $\text{S}_8$  activation through selected disproportionation routes.<sup>56</sup>

## 2.2 Li-S conversion chemistry in other sulfur-containing materials

It is clearly observed from the above content that the formation and dissolution of LiPSs are inevitable and disruptive in LSBs. Apart from elaborating LiPS-retaining strategies,<sup>57</sup> avoiding and suppressing the existence of LiPSs in the sulfur conversion process can also improve the LSB cyclability. Some sulfur-containing compounds, including small sulfur molecules, organo-sulfur polymers, and metal sulfides, can meet this requirement.

**2.2.1 Small sulfur allotropes.** Confinement of small sulfur allotropes  $\text{S}_{2-4}$  in microporous carbon (pore size  $\sim 0.5$  nm, Fig. 3a) is a successful example to avoid LiPS diffusion in bulk electrolytes through a solid-solid conversion.<sup>58,59</sup> The narrow pores can successfully prevent the direct contact between sulfur

molecules and electrolytes by desolvating the solvated-Li before solid Li diffusion in the carbon host (Fig. 3b).<sup>58</sup> Therefore, the electrode can be cycled in both ether-based and carbonate-based electrolytes (Fig. 3c). The smaller sulfur molecules showed excellent cycling stability with capacities above  $600 \text{ mA h g}^{-1}$  after 500 cycles at  $400 \text{ mA g}^{-1}$ .

Despite the extended cycle life of LSBs, this approach faces several fundamental challenges. First, the charge-transfer kinetics depend on the electronically conductive carbon, resulting in  $\text{S}_{2-4}$ /microporous carbon with higher resistance than the 'open-type'  $\text{S}_8$ /porous carbon due to the large energy barriers for Li desolvation, solid Li-ion diffusion, and solid-solid Li-S conversion processes. Second, due to the limited space, the sulfur content is restricted to less than 50%,<sup>57,58</sup> which is far from sufficient to meet practically high energy LSBs demanding sulfur loadings of above 70 wt% and  $7 \text{ mg cm}^{-2}$ . Third, the conditions to realize solid-solid reactions are ambiguous. It is argued that solid electrolyte interface (SEI) layers formed on the surface of the sulfur/mesoporous carbon

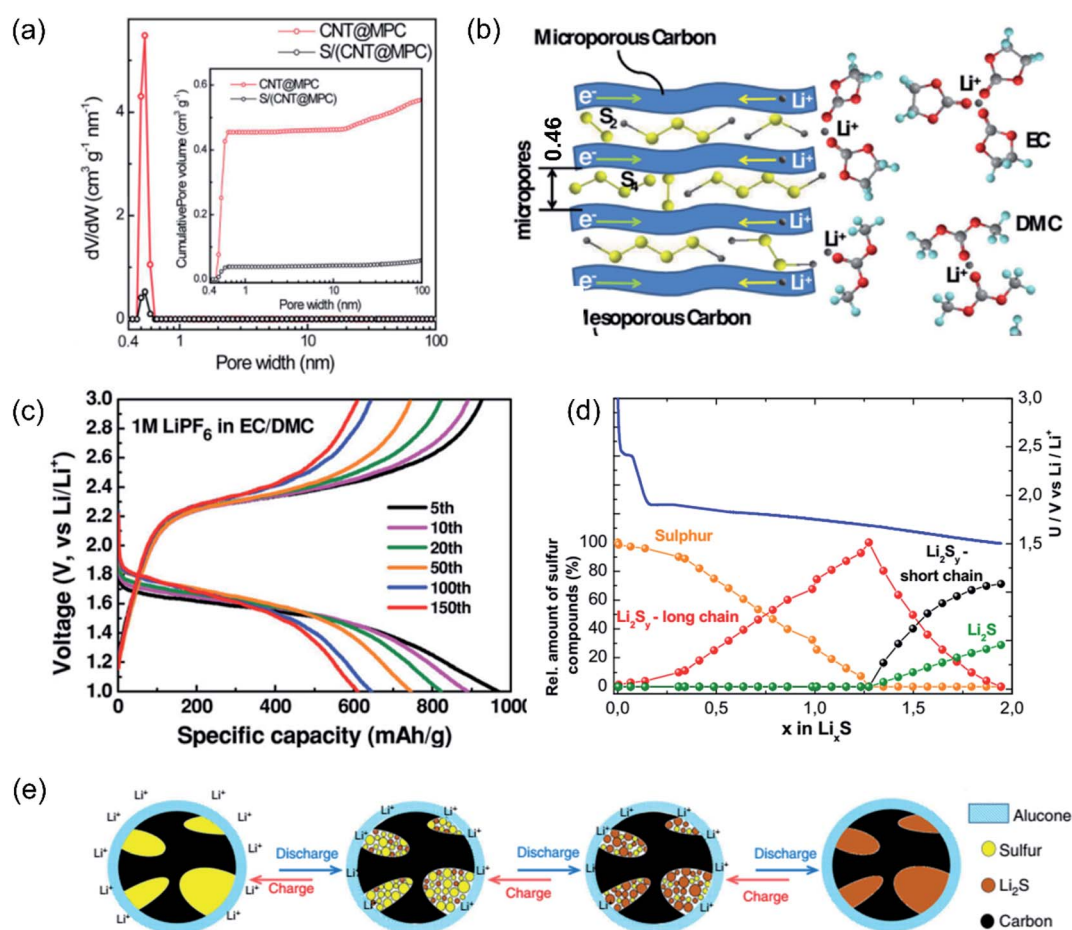


Fig. 3 (a) Sulfur confined by CNTs with 0.5 nm-sized pores. Reproduced with permission: Copyright 2012, American Chemistry Society.<sup>59</sup> (b) Exclusion of carbonate electrolyte molecules from 0.46 nm micropores. (c) Potential curves of  $\text{S}_{2-4}$  in a carbonate-based electrolyte. Reproduced with permission: Copyright 2014, Wiley-VCH.<sup>58</sup> (d) The change of relative amount of S, long-chain  $\text{Li}_2\text{S}_y$ , short-chain  $\text{Li}_2\text{S}_y$ , and  $\text{Li}_2\text{S}$  during the discharge process when using the ultra-microporous carbon/S as the cathode in carbonate solvent-based electrolytes. Reproduced with permission: Copyright 2018, Electrochemical Society.<sup>61</sup> (e) The proposed redox reaction process of alucone C-S cathodes in carbonate solvent-based electrolytes. Reproduced with permission: Copyright 2018, Nature Research.<sup>62</sup>

cathode would also trigger the solid–solid reaction,<sup>60</sup> disrupting the compulsory micropores. Fourth, the reduction mechanism of  $S_{2-4}$  in microporous carbon is under debate. Some papers proposed that  $S_{2-4}$  is lithiated to long-chain LiPSs, short-chain LiPSs, and finally  $Li_2S$ , similar to the lithiation of  $S_8$ , through *operando* XAS characterization (Fig. 3d).<sup>61</sup> Others argued that the redox process between  $S_{2-4}$  and Li only involves sulfur and  $Li_2S$  without any intermediates, the same as the alucone C–S cathodes in carbonate-based electrolytes (Fig. 3e).<sup>62</sup> Therefore, both the electrochemical performance and fundamental understanding of reaction mechanisms of small sulfur allotropes need investigation in future studies.

**2.2.2 Organosulfur polymers.** Organosulfur polymers consisting of organic groups and sulfur chains have also been widely investigated as promising alternatives to  $S_8$  to solve the problems of LiPSs.<sup>63</sup> In organosulfur compounds, sulfur atoms are covalently bonded with organic frameworks. This structure can inherently entrap sulfur species, particularly LiPSs, and avoid agglomeration or re-displacement of sulfur during cycling, and thus the sulfur utilization is improved, and the shuttle effect is suppressed by molecular immobilization.<sup>63</sup> The electrochemical process of organosulfur compounds can be classified into three types as shown in Fig. 4a.

The first class of organosulfur undergoes the solid–liquid–solid conversion path, resembling the electrochemical process of  $S_8$ .<sup>63</sup> A representative example is the poly(sulfur-random-1,3-diisopropenylbenzene) (S-DIB) which is synthesized by heating polymeric sulfur and DIB together.<sup>64</sup> The S-DIB displayed an  $S_8$ -

like discharge/charge potential profile with two typical reaction plateaus. Due to the chemical bonding of the copolymers, pristine S-DIB exhibited a reasonable cycle life of 100 cycles at 0.1C. Consequently, the S-DIB@CNT cathode was prepared with enhanced electrical and ionic conductivities,<sup>65</sup> and it presented a high initial capacity of  $1300 \text{ mA h g}^{-1}$  and a cycling capacity of  $880 \text{ mA h g}^{-1}$  at 1C. Inspired by the S-DIB structure, organosulfur polymers containing conjunction units of benzene rings, thiophene, and thiazine have also been exploited for improved battery performance.<sup>66</sup> Zhou *et al.*<sup>67</sup> prepared a linear copolymer containing thiokol rubber-like poly(methylene tetrasulfide) to stabilize LiPSs by forming strong chemical bonds (*e.g.*,  $Li-S_2-CH_2-S-Li$  or  $Li-S-CH_2CH_2-S-Li$ ). For this kind of organosulfur compound, the future study should pay attention to two key parameters, namely (i) the length of the sulfur chain and the organic unit, which determines the physicochemical stability and the sulfur content; (ii) the bandgap of polymers, which governs their conductivity and rate capability in LSBs.

The second class of organosulfur polymers only undergoes solid–solid reaction without the LiPS formation.<sup>68,69</sup> Sulfurized polyacrylonitrile (SPAN) is one of the most attractive examples with remarkable electrochemical cycling stability in carbonate-based electrolytes.<sup>70</sup> SPAN can be simply produced by heating mixtures of sulfur and acrylonitrile, which is polymerized and sulfurized into a conjugated structure as shown in Fig. 4b. During lithiation/delithiation, it was proposed that SPAN underwent a solid-phase conversion where the C–S bonds were reversibly broken and reformed.<sup>71</sup> It is noted that there are two

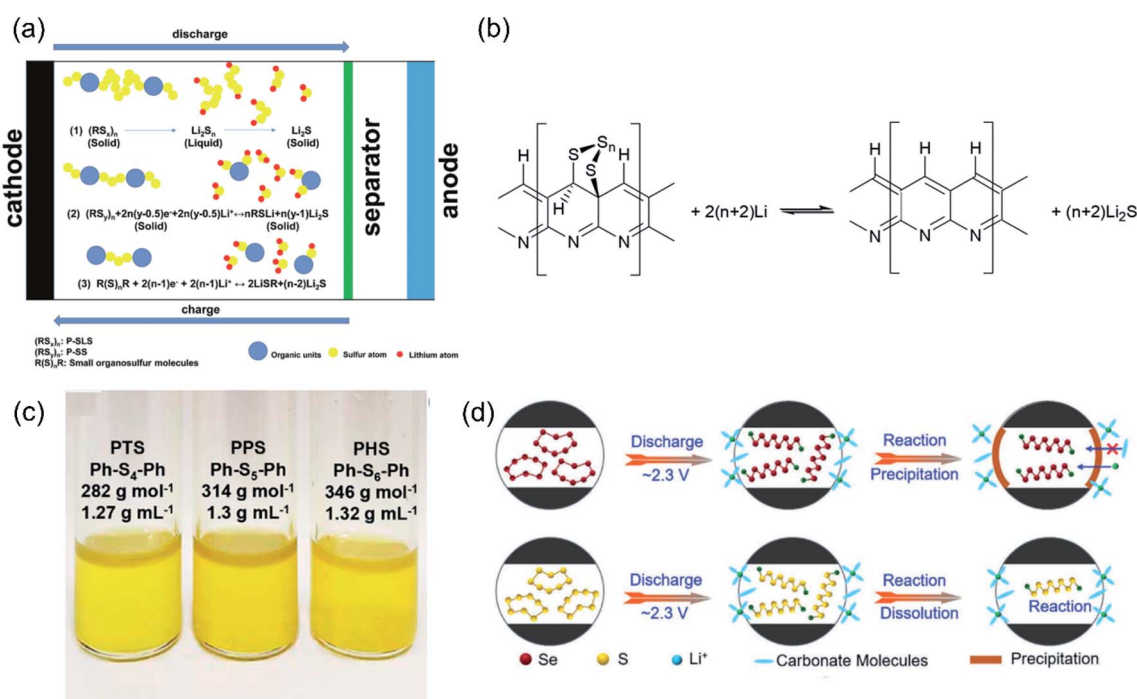


Fig. 4 (a) The different electrochemical processes of different organosulfur compounds.<sup>63</sup> Reproduced with permission: Copyright 2020, Royal Society of Chemistry. (b) The general reaction equation of the overall Li/SPAN reaction. Reproduced with permission: Copyright 2014, Multi-disciplinary Digital Publishing Institute.<sup>71</sup> (c) The photos of a series of liquid phenyl polysulfides. Reproduced with permission: Copyright 2018, American Chemistry Society.<sup>74</sup> (d) Schematic illustration of the CEI formed on CMK-3/Se and CMK-3/S cathodes in a carbonate-based electrolyte. Reproduced with permission: Copyright 2021, Wiley-VCH.<sup>76</sup>

models to explain the sulfur storage in SPAN. One is sulfur chains act as bridges to connect the conjugated PAN skeleton, another is the sulfur is siding chains on the conjugated PAN.<sup>72</sup> Although SPAN can avoid the shuttle effect, this kind of material also has problems, such as low sulfur loading (~40%), poor conductivity, and sluggish redox kinetics. In order to improve the conductivity and reaction kinetics, Wang *et al.*<sup>73</sup> reported a freestanding fibrous SPAN/CNT cathode. After activation, the cathode could maintain a reversible capacity of 1400 mA h g<sup>-1</sup> over 200 cycles at 200 mA g<sup>-1</sup>, and 1180 mA h g<sup>-1</sup> over 800 cycles at 800 mA g<sup>-1</sup>. Chen *et al.*<sup>72</sup> reported a Se-doped SPAN (Se<sub>x</sub>SPAN) cycling in carbonate-based and ether-based electrolytes. Interestingly, different from the solid–solid phase transition of pure SPAN in ether electrolytes,<sup>73</sup> a solid–liquid–solid transition path was detected for Se<sub>x</sub>SPAN with high rate capabilities. This study suggests that the sulfur conversion processes and electrochemical performance of SPAN are tunable by heteroatom doping. In addition to SPAN, sulfur-rich organosulfur materials with short sulfur-chains (S<sub>2–4</sub>) have also been reported to show LiPS-free cycling performance. Shadik *et al.*<sup>68</sup> incorporated the 2,3,4,6,8,9,10,12-octathia bicyclopenta[*b,c*]-5,11-anthraquinone-1,7-dithione (TPQD) skeleton with high capacity and soluble 1-4-benzoquinone (BQ) into TPQD-BQ organosulfides. The organic cathode delivered high capacities, great rate capability and stable cycling performance in LSBs. Zhang *et al.*<sup>69</sup> synthesized disulfide polymer (DSP) and trisulfide polymer (TSP) cathode materials. The electrolyte in optical cells containing TSP remained colorless during cycling, manifesting no LiPS formation.

As for the third type of organosulfur, they are usually small molecules in the liquid phase, undergoing a liquid–solid transformation in LSBs.<sup>63</sup> Bhargav *et al.*<sup>74</sup> synthesized phenyl polysulfides C<sub>6</sub>H<sub>5</sub>S<sub>x</sub>C<sub>6</sub>H<sub>5</sub> (4 ≤ x ≤ 6) as a liquid cathode, as shown in Fig. 4c. During lithiation, the phenyl polysulfides were reduced to solid Li<sub>2</sub>S and phenyl-SLi. Due to the liquid–solid conversion, the cell delivered great performance with a lean electrolyte, for example, an area capacity of 7.6 mA h cm<sup>-2</sup> was retained after 500 cycles at 1C under an E/S ratio of 3 μl mg<sup>-1</sup>.

**2.2.3 Inorganic sulfur compounds.** When some sulfur-containing inorganic compounds exhibit working voltages close to 2 V vs. Li/Li<sup>+</sup> and sulfur content of >40 wt%, they are regarded as sulfur-equivalent cathodes in LSBs.<sup>75</sup> Ye *et al.*<sup>75</sup> reported an amorphous MoS<sub>3</sub> as a LSB cathode. MoS<sub>3</sub> was proposed to have a chain-like structure consisting of Mo bridged by sulfide and disulfide ligands. The *operando* XAS spectrum was obtained to learn the reaction mechanisms of the MoS<sub>3</sub> cathode. It shows that both the sulfur and Mo were reduced during lithiation, but they did not form Li<sub>2</sub>S or polysulfides. The Li-ions were supposed to accumulate at the bridge sites between two adjacent sulfur atoms. No disintegration of sulfur or MoS<sub>3</sub> took place during cycling. As a result, the MoS<sub>3</sub> cathode delivered a high capacity of ~383 mA h g<sup>-1</sup> after 1000 cycles at 0.45 A g<sup>-1</sup>. Selenium (Se), an element in the same group as oxygen and sulfur, has also been compounded with S to form Se<sub>x</sub>S<sub>y</sub> as sulfur-equivalent cathodes in LSBs. It was found that the Se in CMK-3/Se<sub>x</sub>S<sub>y</sub> could induce the formation of a thin cathode electrolyte interface (CEI) layer on cathodes in carbonate

electrolytes.<sup>76</sup> As shown in Fig. 4d, electrolyte molecules would be blocked by the CEI to attack polysulfides or polyselenides encapsulated within the carbon host. The thickness of the CEI layer signified a positive relationship with the Se content. Thus, optimal CMK-3/Se<sub>5</sub>S<sub>3</sub> with a desirably thick CEI achieved a remarkable capacity retention of 609 mA h g<sup>-1</sup> after 300 cycles at 1 A g<sup>-1</sup>.<sup>77</sup>

Overall, in the past decade, tremendous progress has been achieved in understanding the fundamental mechanisms of sulfur conversion chemistry in LSBs. Inherently, the Li–S conversion behavior is determined by the stage of reaction, the nature of starting materials, and the intermediate chemical species. It is also observed that the complicated reaction processes involve both favorable (*i.e.*, disproportionation reaction to dissolve insulating sulfur or Li<sub>2</sub>S) and unfavorable (*i.e.*, sluggish conversion of polysulfides) steps. To improve the electrochemical performance, effective strategies have been developed to regulate the sulfur conversion processes which are interpreted in the following section.

## 2.3 Regulating the sulfur conversion chemistry

**2.3.1 Current collector engineering.** The current collector functions as the bridge between electric circuits and electrode materials.<sup>78</sup> It also has a great impact on the electrochemical behavior of LSBs. In general, the sulfur cathode is fabricated by casting a mixture of active materials, binders, and conductive carbon black on Al foil.<sup>79</sup> Other 2D films or foil materials such as Ni, Pt, Cu, and carbon cloth (CC) have also been investigated as potential current collectors. It is found that Cu and Ni are unstable as they are corroded by polysulfides or components in the electrolytes.<sup>80</sup> LSBs with CC and graphene film current collectors exhibit better electrochemical performance than the Al counterpart,<sup>81</sup> attributable to their larger surface area and better anti-corrosion capability.<sup>82</sup>

3D current collectors have also been studied as promising alternatives to their 2D counterparts in view of their interconnected conductive networks, large surface area, and abundant ion diffusion channels, all of which are important for high sulfur loading and fast reaction kinetics.<sup>83</sup> For example, 3D carbon nanotube (CNT) films have been prepared as current collectors for LSBs. Compared with 2D Al foil and graphene current collectors, LSBs with 3D CNT current collectors displayed much superior electrochemical performance (Fig. 5a) with a high cycling ability (95 cycles with 0.029% decay rate) under high sulfur loadings.<sup>82</sup> Other carbon materials have also been built into 3D current collectors, such as graphene foam (GF)<sup>84</sup> and 3D melamine formaldehyde-based carbon foam (MFC).<sup>85</sup> However, the nonpolar carbon cannot entrap LiPSs to suppress the shuttle effect in LSBs.

To regulate the entrapment and catalytic capability of current collectors for high-performance LSBs, surface modifications have been conducted for light and 3D carbon current collectors.<sup>86</sup> For example, we have prepared MoS<sub>2</sub>/carbon nanofiber (CNF) films by electrospinning.<sup>37</sup> Then, a catholyte containing polysulfides and electrolyte was dropped on MoS<sub>2</sub>/CNF films as cathodes. Owing to the 1T MoS<sub>2</sub> catalyst and the



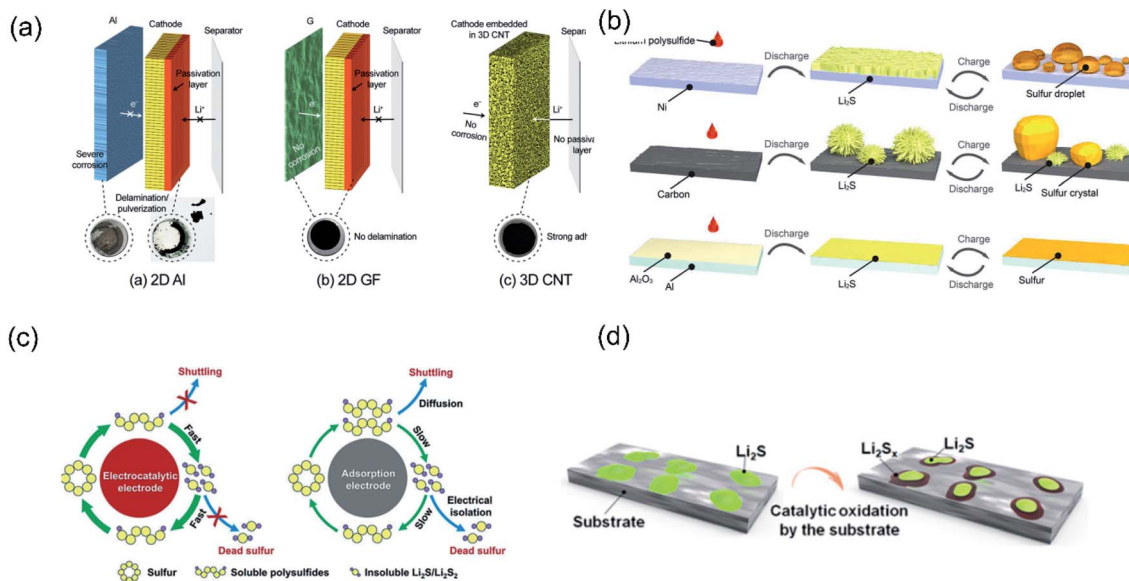


Fig. 5 (a) Comparison of 2D Al current collectors, 2D graphene foam current collectors, and 3D CNT current collectors. Reproduced with permission: Copyright 2016, Wiley-VCH.<sup>82</sup> (b) Schematic illustration of the sulfur species evolution on Ni, C, and Al substrates during charging and discharging processes. Reproduced with permission: Copyright 2020, The American Association for the Advancement of Science.<sup>30</sup> (c) The comparison of electrocatalytic electrodes and adsorption electrodes. Reproduced with permission: Copyright 2018, Elsevier.<sup>96</sup> (d) Schematic showing the promotion of Li<sub>2</sub>S dissolution to LiPSs on metal sulfides. Reproduced with permission: Copyright 2017, National Academy of Sciences.<sup>52</sup>

3D conductive carbon network, MoS<sub>2</sub>/CNF/Li<sub>2</sub>S<sub>6</sub> delivered a remarkable capacity retention of 9.3 mA h cm<sup>-2</sup> after 300 cycles with an exceptionally high sulfur loading of 12.9 mg cm<sup>-2</sup> and a lean electrolyte loading of 4.6 μl mg<sup>-1</sup>. A MoC decorated N-doped CNF current collector has also been proved to effectively mitigate the shuttle effect by taking advantage of the strong LiPS affinity for MoC.<sup>87</sup> A pyrrole polymer with strong chemical bonding with LiPSs was introduced into GF current collectors. The pyrrole GF/S cathode displayed a great cycling ability (over 100 cycles with 81% capacity retention) and high specific capacity (1220 mA h g<sup>-1</sup>).<sup>88</sup> In addition to polysulfide entrapment, functional current collectors have also been designed to regulate the LiPS conversion kinetics and the Li<sub>2</sub>S deposition behavior. For example, the Co,N-CNTs-CNS (carbon nanosheet)/CFC (carbon fiber cloth) current collector induced a 3D deposition of Li<sub>2</sub>S.<sup>89</sup> Compared to the routine 2D growth of Li<sub>2</sub>S, the 3D structure of Li<sub>2</sub>S enables higher LiPS utilization and thus effectively suppresses their diffusion to bulk electrolytes.

Apart from the discharging (or lithiation) process, the current collectors also play a non-negligible role in the charging process in LSBs. Using *in situ* optical microscopy, Zhou *et al.*<sup>30</sup> observed distinct sulfur growth behavior on Al, C, and Ni current collectors. They found that solid sulfur emerged on the carbon surface, while liquid sulfur droplets grew on Ni substrates (Fig. 5b). The different sulfur growth behaviors were attributed to different binding energies of S<sub>8</sub> with Ni, C, or Al substrates through DFT calculations. The moderate interaction between Ni and S<sub>8</sub> (−1.4 eV vs. −0.93 eV for S<sub>8</sub> on C, −5.44 eV for S<sub>8</sub> on Al) was the precondition for sulfur droplet formation. As aforementioned, liquid sulfur enables high mobility and fast

phase transition, thus accelerating the reaction kinetics in LSBs. Consequently, a lightweight, 3D Ni-coated melamine current collector was synthesized for high-rate and long-life LSBs. Similarly, two-dimensional materials (*i.e.*, MoS<sub>2</sub> and graphene)<sup>29</sup> or deposited Au layer<sup>90</sup> current collectors have also been reported to generate the liquid sulfur product with high area capacities in on-chip micro-LSBs.

Overall, the nature of current collectors is important in influencing the electrochemical behavior in both discharging and charging processes. Self-supporting and 3D current collectors are desirable as high-loading sulfur hosts. Functional materials on 3D networks are also recommended to accelerate the Li-S redox kinetics. Research on the impact of current collectors on the charging process is still in the initial stage. More efforts are expected to unveil the reasons for current collectors regulating the whole charging/discharging cycle in LSBs.

**2.3.2 Electrocatalyst design.** One of the fundamental challenges in sulfur utilization is the insulating nature of sulfur species. Therefore, tremendous efforts have been made to design carbon nanomaterials as highly conductive hosts for sulfur particles. Although improvement in electrochemical performance has been witnessed by compositing sulfur and conductive carbon, the long-term and high-rate capacities of such sulfur/carbon cathodes are often jeopardized due to the eventual dissolution of polysulfides caused by the weak interaction between polar polysulfides and nonpolar carbon. In this respect, studies on electrocatalysts, enabling chemical trapping and catalytic conversion of polysulfides, have recently been carried out and they demonstrated their effectiveness in

regulating sulfur conversion chemistry for high-performance LSBs. According to their functions and the report timeline, electrocatalysts can be divided into four categories, namely chemical adsorbers, adsorption–diffusion–conversion catalysts, bi-directional catalysts, and selective catalysts.

In the early stage of catalyst study for LSBs, it was believed that polar materials, such as N-doped carbon, metal oxides, and dichalcogenides, can form polar–polar interactions or Lewis acid-based bonding with LiPSs, thus preventing their diffusion.<sup>91</sup> One of the typical examples is mesoporous silica, which was added in the CMK-3/S composite as a sulfur reservoir to trap and store the soluble polysulfides during cycling, thus leading to better cycling stability than that of pure CMK-3/S.<sup>92</sup> Similarly, TiO<sub>2</sub>, NiO and CoO<sup>93–95</sup> have also been investigated to block the LiPS diffusion. However, it was quickly found that improvement in battery performance using these materials was limited because the entrapped LiPSs cannot be effectively converted to Li<sub>2</sub>S due to the poor electronic conductivities of these catalysts (Fig. 5c).<sup>96</sup>

To improve the sulfur usage rate and suppress LiPS diffusion, conductive catalysts were then reported to supply a consecutive LiPS adsorption–diffusion–conversion pathway.<sup>97</sup> Taking black phosphorus (BP) as an example, it possesses good bulk conductivity, a fast Li-ion diffusion constant, and high binding energies with polysulfides. Few-layered BP sheets were therefore adopted in separators<sup>98</sup> or current collectors<sup>99</sup> to suppress the diffusion of LiPSs. Through DFT calculations, we discovered that BP presented edge-selective catalytic properties, where the zig–zag terminated BP resulted in stronger binding energies with polysulfides at the edges than at terrace sites.<sup>40</sup> This finding suggests that we can largely increase the catalytic properties by downsizing BP flakes into BPQDs. The electrochemical performance revealed that BPQDs have a robust catalytic capability, and the porous carbon/S/BPQD cathodes presented rapid reaction kinetics and no shuttling of polysulfides. Another representative electrocatalyst worth mentioning is the TiO<sub>2</sub>/TiN heterostructure enabling smooth trapping–diffusion–conversion of polysulfides towards stable LSBs.<sup>100</sup> The heterostructure combined the merits of highly adsorptive TiO<sub>2</sub> (for trapping) and conductive TiN (for conversion), thus providing a complete strategy to synchronously realize LiPS adsorption and conversion. Other polar materials (*i.e.*, metal oxides, metal sulfides, and metal nitrides)<sup>101</sup> and single-atom catalysts (*i.e.*, Co–N–C and Fe–N–C)<sup>102</sup> have also been developed to enhance the reduction of LiPSs into Li<sub>2</sub>S.

The catalytic oxidation of Li<sub>2</sub>S during charging is equally important to obtain highly reversible LSBs. Zhou *et al.*<sup>52</sup> illustrated that VS<sub>2</sub>-, TiS<sub>2</sub>- and CoS<sub>2</sub>-modified cathodes promoted the dissolution and conversion of Li<sub>2</sub>S to LiPSs (Fig. 5d). Owing to the high binding energy between the isolated Li-ions and sulfur in sulfides, the metal sulfides would lower the energy barrier for the oxidation of Li<sub>2</sub>S to improve the Li<sub>2</sub>S decomposition kinetics. Inspired by the outstanding catalytic capability of Pt and Ni in fuel cells, noble metals were also investigated to reduce the energy barrier for the oxidation process of lithium sulfides to soluble LiPSs.<sup>103</sup> However, most of the synthesized catalysts function in one direction (reduction or oxidation)

because of their intrinsic electron donor or acceptor nature, which is unsatisfactory to accelerate the discharge/charge reactions in LSBs simultaneously. To mitigate this challenge, a TiO<sub>2</sub>–Ni<sub>3</sub>N<sub>2</sub> heterostructure<sup>104</sup> was prepared as a bidirectional catalyst. Typically, TiO<sub>2</sub> traps while Ni<sub>3</sub>N<sub>2</sub> catalytically reduces LiPSs during discharging, and both TiO<sub>2</sub> and Ni<sub>3</sub>N<sub>2</sub> catalyze the Li<sub>2</sub>S dissolution during charging. The sulfur cathode containing TiO<sub>2</sub>–Ni<sub>3</sub>N<sub>2</sub> delivered a low capacity decay rate of 0.038% per cycle over 900 cycles, accordingly.

When we recall the sulfur conversion processes in Section 2.1, it is found that the transformation of polysulfides from high order to low order is generally fast, but the kinetics of further reducing Li<sub>2</sub>S<sub>4</sub> to solid Li<sub>2</sub>S<sub>2</sub>/Li<sub>2</sub>S is slow. The kinetics mismatch would lead to saturation of polysulfides on the surface of catalysts and stall further LiPS adsorption. Therefore, precisely regulating sulfur conversion to ensure compatible LiPS formation and consumption speeds becomes another challenging issue for electrocatalyst design. Hua *et al.*<sup>105</sup> reported an In<sub>2</sub>O<sub>3</sub> catalyst that would selectively decelerate the conversion from S to LiPSs, while accelerating the reduction of Li<sub>2</sub>S<sub>4</sub> to Li<sub>2</sub>S. This catalysis could alleviate the accumulation of LiPSs around the cathode to suppress the shuttle effect, leading to enhanced electrochemical performance. The dynamically changing catalytic mechanism was unveiled by *in situ* Raman analysis. It showed that In<sub>2</sub>O<sub>3</sub> was reversibly converted to LiInS<sub>2</sub> to accelerate LiPS deposition to insoluble Li<sub>2</sub>S during discharging, while LiInS<sub>2</sub> was converted back to In<sub>2</sub>O<sub>3</sub> for activating Li<sub>2</sub>S oxidation during the following charging process. Similarly, Li *et al.*<sup>106</sup> reported a stepwise polysulfide conversion catalyst, defect-rich Co<sub>3</sub>O<sub>4</sub>/TiO<sub>2</sub> (denoted as p-Co<sub>3</sub>O<sub>4</sub>/n-TiO<sub>2</sub>-HPs). The Co<sub>3</sub>O<sub>4</sub> physicochemically immobilized pristine sulfur and controlled the reduction of S<sub>8</sub> to Li<sub>2</sub>S<sub>4</sub>, while the TiO<sub>2</sub> dots facilitated the diffusion and reduction of Li<sub>2</sub>S<sub>4</sub> to solid Li<sub>2</sub>S, which is attributed to the p-Co<sub>3</sub>O<sub>4</sub>/n-TiO<sub>2</sub> built-in electric field. As a result, the precisely regulated LSB delivered an exceptionally high rate capability at 10C with a low capacity decay rate of 0.07% per cycle over 500 cycles.

In summary, different kinds of materials display specific functions to catalyze the redox reactions of LSBs. Heterostructures signify the most promising strategy, which can combine specific functions of different catalysts into one structure, thus precisely regulating the sulfur conversion dynamics and kinetics for complex Li–S systems. Despite the encouraging progress, the investigations on electrochemical catalysts are still in the very beginning stage with a large room to explore. Several directions are suggested, namely (i) understanding and *in situ* evaluation of the structural evolution of catalysts during cycling, (ii) reducing the content of electrochemically inert catalysts in LSBs, and (iii) understanding the catalytic mechanisms under extreme conditions, such as high sulfur loading, lean electrolyte, and extreme working temperatures.

**2.3.3 Electrolyte engineering.** The electrolyte chemistry indicates considerable abilities to regulate the sulfur conversion behavior, thus critically affecting the energy density and cycling performance of LSBs. 1 M LiTFSI in equal volume DME and DOL is the most common electrolyte formula for LSBs. The

DME/DOL solvent presents limited LiPS dissolvability, enabling ready saturation of short-chain polysulfides, particularly under lean electrolyte conditions.<sup>107,108</sup> To mitigate this issue, Cheng *et al.*<sup>109</sup> designed a novel  $\epsilon$ -caprolactam/acetamide-based eutectic-solvent electrolyte, which had the ability to completely dissolve  $\text{Li}_2\text{S}_8$  and  $\text{Li}_2\text{S}$  (Fig. 6a). The phase transformation from ‘solid–liquid–solid’ in DME/DOL was turned to ‘solid–liquid’ in this new electrolyte. Therefore, the core problems of voltage polarization and  $\text{Li}_2\text{S}$  activation can be settled. Dominko *et al.*<sup>61</sup> studied the sulfur reduction processes in ether-based electrolytes (TEGDME : DOL with high LiPS solubility), fluorinated ether-based electrolytes (TTFE : DOL with low LiPS solubility), and carbonate-based electrolytes (EC : DMC, with  $\text{S}_{2-4}$ /microporous carbon cathode, no LiPS formation) by XAS characterization. In all three cases, the sulfur reduction went through the same processes, sulfur  $\rightarrow$  long-chain LiPSs  $\rightarrow$  short-chain LiPSs  $\rightarrow$   $\text{Li}_2\text{S}/\text{Li}_2\text{S}_2$ , with a difference in the type of polysulfides formed in the corresponding steps of discharge. When the sulfur was converted to LiPSs, the potential of the discharge plateau in the ether-based electrolyte was higher than that in the fluorinated ether-based electrolyte, indicating a positive relationship between LiPS solubility in the electrolyte and overpotential for discharging. The discharging product in the carbonate-based electrolyte was a mixture of  $\text{Li}_2\text{S}$  and  $\text{Li}_2\text{S}_2$  (molar ratio of 2 : 1), which is different from the end-product of  $\text{Li}_2\text{S}$  in coexistence with polysulfides in ether-based electrolytes.

The solvents with different DN can affect the Li–S redox pathways, intermediate species, and  $\text{Li}_2\text{S}$  deposition morphologies.<sup>32</sup> As shown in Fig. 6b, in the high-DN solvent electrolyte (*i.e.*, DMSO, DN = 29.8), Li–S reactions undergo multiple electrochemical and chemical reactions involving  $\text{S}_8^{2-}$ ,  $\text{S}_6^{2-}$ ,  $\text{S}_4^{2-}$ , and  $\text{S}_3^{\cdot-}$  where  $\text{S}_3^{\cdot-}$  is the most stable intermediate to convert to solid lithium sulfides. However, in the low-DN-solvent electrolyte (*i.e.*, DOL : DME),  $\text{S}_4^{2-}$  was the main intermediate before  $\text{Li}_2\text{S}_2/\text{Li}_2\text{S}$  deposition. It is clear that the presence of  $\text{S}_3^{\cdot-}$  is solvent-dependent. The reaction pathway involving the  $\text{S}_3^{\cdot-}$  radical was favorable to promote sulfur utilization by exacerbating dissociations to allow full conversion of sulfur and lithium sulfides.<sup>110</sup> High-DN-solvent DMSO is favourable for  $\text{S}_3^{\cdot-}$  formation, but it presents poor anodic stability against metallic Li. Note that the high-DN solvent always presents a high dielectric constant ( $\epsilon$ ).<sup>32</sup> Tetramethylurea (TMU) with better compatibility with Li metal and comparably high  $\epsilon$  ( $\epsilon = 23.6$ ) was investigated to form active  $\text{S}_3^{\cdot-}$  radicals.<sup>107</sup> Large amounts of  $\text{S}_3^{\cdot-}$  in the DOL/TMU co-solvent were confirmed by Raman characterization. The presence of  $\text{S}_3^{\cdot-}$  radicals enabled the efficient conversion of  $\text{Li}_2\text{S}$  in TMU during charging and the deposition of thick and porous  $\text{Li}_2\text{S}$  during discharging, whereas an appreciable performance was not observed in the DOL/DME electrolyte. The pouch cells using the TMU electrolyte delivered a remarkable capacity of  $1524 \text{ mA h g}^{-1}$  and a high energy density of  $324 \text{ W h kg}^{-1}$ .

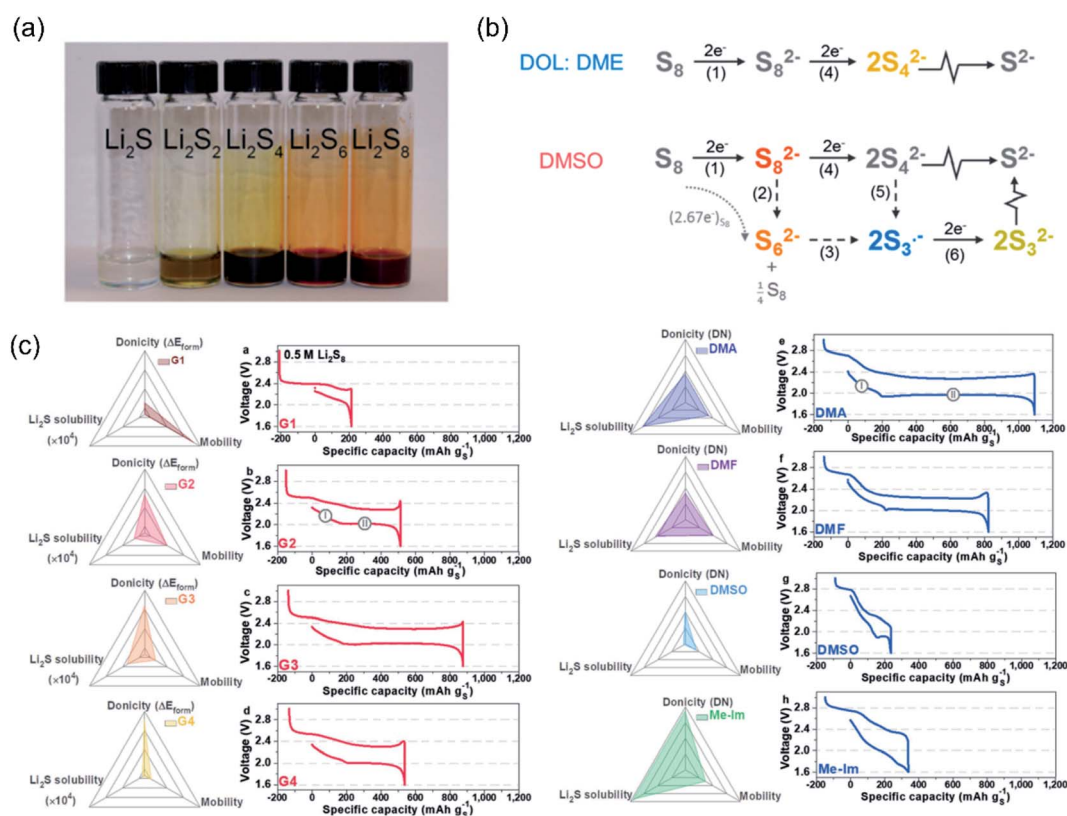


Fig. 6 (a)  $\text{Li}_2\text{S}$ ,  $\text{Li}_2\text{S}_2$ ,  $\text{Li}_2\text{S}_4$ ,  $\text{Li}_2\text{S}_6$ , and  $\text{Li}_2\text{S}_8$  dissolved in an  $\epsilon$ -caprolactam/acetamide based eutectic solvent electrolyte. Reproduced with permission: Copyright 2019, Wiley-VCH.<sup>109</sup> (b) Sulfur reaction pathways in DOL : DME and DMSO. Reproduced with permission: Copyright 2016, American Chemical Society.<sup>32</sup> (c) The relationship between solvent properties (*i.e.*, donicity,  $\text{Li}_2\text{S}$  solubility, and mobility) and battery performance. Reproduced with permission: Copyright 2019, Wiley-VCH.<sup>112</sup>

Although high DN solvents can facilitate the rapid and complete conversion of sulfur and  $\text{Li}_2\text{S}$  by increasing polysulfide dissolution, other electrolyte properties such as ionic conductivity, viscosity, and electrode wettability also govern the  $\text{Li}_2\text{S}$  deposition behavior. Pan *et al.*<sup>111</sup> explored  $\text{Li}_2\text{S}$  deposition in three representative solvents, including tetramethylene sulfone (TMS) with low-DN, DOL : DME with mid-DN, and DMSO with high-DN. SEM images showed that the deposited  $\text{Li}_2\text{S}$  on the carbon nanofiber surface was in the form of thin films in TMS, micro-sized “flower-like” sheets in DOL : DME, and small nanoparticles in DMSO. Although DMSO indicated 3D growth of  $\text{Li}_2\text{S}$ , the relatively small  $\text{Li}^+$  diffusion coefficient restricted the growth of small nucleation seeds into 3D  $\text{Li}_2\text{S}$ , causing inferior sulfur utilization and cycling capacities to those in the DOL : DME-based electrolyte. Li *et al.*<sup>112</sup> studied the effects of DN (high DN induces  $\text{Li}_2\text{S}$  3D deposition), dielectric constant (high  $\epsilon$  leads to high  $\text{Li}_2\text{S}$  solubility) and viscosity (high  $\eta$  leads to low polysulfide mobility and poor wettability) on the electrochemical deposition behavior of  $\text{Li}_2\text{S}$  (Fig. 6c). Among ether-based solvents, DME (G1) with low DN and  $\text{Li}_2\text{S}$  solubility displayed fast 2D lattice growth of  $\text{Li}_2\text{S}$  films and passivated the electrode surface impeding the further reduction reaction. The low  $\text{Li}_2\text{S}$  solubility and high viscosity of the TEGDME (G4) electrolyte induced insufficient sulfur utilization as well. In the high DN electrolyte group, the sulfur cathode displayed the largest discharge capacity of  $1100 \text{ mA h g}^{-1}$  in the DMA solvent due to the high  $\text{Li}_2\text{S}$  solubility, suitable DN and high ionic mobility. The battery with the highest-DN DMSO electrolyte displayed the smallest discharging capacity of  $220 \text{ mA h g}^{-1}$  because of the ultralow  $\text{Li}_2\text{S}$  solubility.

The polysulfide dissociation behavior can be tuned using the lithium salt species and concentration in electrolytes. Chu *et al.*<sup>113</sup> investigated how the salt anions with different DN could tailor the  $\text{Li}_2\text{S}$  deposition behavior. Lithium bromide (LiBr), lithium triflate (LiTf), and lithium bistriflimide (LiTFSI) with DN = 33.7, 16.9, and 5.4, respectively, were dissolved in DOL/DME as electrolytes. The battery with LiBr and LiTf-based electrolytes exhibited superior reversible capacities to that of LiTFSI electrolytes ( $1535, 1214$  vs.  $400 \text{ mA h g}^{-1}$ ) due to the high efficiency of  $\text{Li}_2\text{S}$  deposition and decomposition. 3D  $\text{Li}_2\text{S}$  micron particles were deposited on CC in LiTf and LiBr electrolytes, while a 2D passivating film was detected in LiTFSI electrolyte. The 3D deposition was related to the precipitated  $\text{Li}_2\text{S}$  possessing strong adsorption to  $\text{S}^{2-}$ . The free  $\text{S}^{2-}$  anions preferred to deposit on the surface of precipitated  $\text{Li}_2\text{S}$  seeds, resulting in a 3D growth of  $\text{Li}_2\text{S}$  under the action of high DN anions to promote free  $\text{S}^{2-}$  formation. Suo *et al.*<sup>114</sup> reported a solvent-in-salt electrolyte with high LiTFSI concentration in DOL : DME. In the 7 M highly concentrated electrolyte, few free solvent molecules significantly limited the dissolution and diffusion of LiPSs. LSBs with solvent-in-salt electrolytes delivered an initial capacity of  $1041 \text{ mA h g}^{-1}$  and 74% capacity retention after 100 cycles. However, high salt concentration causes problems of high cost, low ionic conductivity, and high viscosity.

Adding electrolyte additives to diluent electrolytes is another promising way to regulate LiPS dissociation in LSBs.  $\text{ZrO}(\text{NO}_3)_2$  with strong negative charge nature was employed as an additive

to regulate LiPS shuttling by exerting a strong repulsion force on LiPSs.<sup>115</sup> Yang *et al.*<sup>17</sup> introduced the bis(4-nitrophenyl) carbonate (BNC) additive to suppress LiPS diffusion by reaction with soluble  $\text{Li}_2\text{S}_8$  to form lithium 4-nitrophenolate (LiNPH) and insoluble lithium sulfides (Fig. 7a). Cobalt hexadecachlorophthalocyanine (CoPcCl) was added to electrolytes to lower the energy barrier for  $\text{Li}_2\text{S}$  decomposition as well as improve the LiPS conversion kinetics.<sup>116</sup> A nickel chloride dimethoxyethane adduct (NiDME) additive was also prepared to interact with  $\text{Li}_2\text{S}_n$  to form  $\text{NiCl}_2$ .<sup>39</sup>  $\text{NiCl}_2$  could suppress LiPS diffusion and accelerate its conversion, and the  $\text{NiCl}_2$  was returned to NiDME when  $\text{NiCl}_2 \cdot \text{Li}_2\text{S}_n$  is oxidized to sulfur during charging (Fig. 7b).

Solid-state electrolytes (SSEs) and hybrid electrolytes (*e.g.*, gel polymer electrolytes (GPEs) and solid-liquid hybrid electrolytes) have also been investigated to manipulate the sulfur conversion behavior. For example, a GPE with titanium-oxo cluster (TOC) fillers can suppress  $\text{Li}_2\text{S}_6$  dissolution due to the dense polymer matrix.<sup>117</sup> Fang *et al.*<sup>118</sup> designed a polyvinylidene fluoride (PVDF) wrapped sulfur cathode to work in a poly(ethylene oxide) (PEO)-GPE. This solid-state LSB exhibited a single-step solid-solid reaction without intermediary product generation. In order to improve the utilization of active materials and thermal stability of LSBs, SSEs have also been developed for LSBs.<sup>119,120</sup> Chiochan *et al.*<sup>119</sup> reported a metal-organic framework (MOF)-based solid electrolyte which used the Universitetet i Oslo (UIO) structure with a lithium sulfonate ( $-\text{SO}_3\text{Li}$ ) group (UIOSLi). The UIOSLi SSE can provide a great  $\text{Li}^+$  transport pathway and prevent LiPS diffusion simultaneously. Compared with the Celgard separator, the UIOSLi SSE showed excellent shuttling inhibition capability even after 7 days (Fig. 7c), which resulted in good cycling stability of the UIOSLi SSE-based LSB with the  $\text{Li}_2\text{S}_6$  catholyte at 0.2C after 250 cycles (capacity decay rate of 0.06% per cycle). The  $\text{Li}_7\text{P}_2.9\text{S}_{10.85}\text{Mo}_{0.01}$  ceramic electrolyte can also prevent the formation of LiPSs *via* a solid-solid reaction with one discharge plateau.<sup>121</sup> It is noted that for both SSEs and GPEs, the slow Li-ion migration kinetics and the high electrode/electrolyte interfacial impedance are the key challenges impeding high-power LSBs.

In summary, the sulfur conversion chemistry is highly dependent on different electrolyte chemistries, such as the physicochemical properties of the solvent, the salt concentration and anion species, electrolyte additives, and the electrolyte phases. In the past years, what was greatly ignored in electrolyte engineering is the lack of understanding of LSB electrochemistry under lean electrolyte conditions. The sulfur conversion mechanisms, reaction kinetics, reactant distribution, and electrode compatibility are largely different from those evaluated in flooded electrolytes. GPE and SSE studies are just in their beginning stage, which demands more research in the future.

**2.3.4 Separator engineering.** The separator is another critical component in a LSB system. The membranes inserted between cathodes and anodes intrinsically function to avoid internal short circuits but provide ion transport channels. Recently, modification of separators has attracted extensive

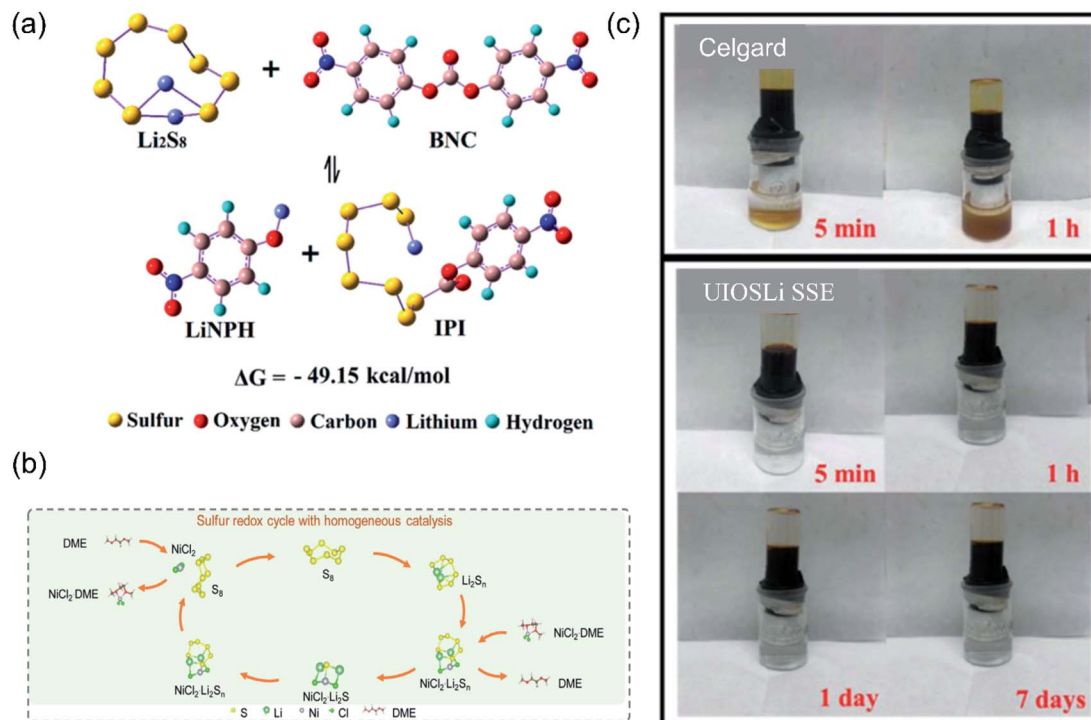


Fig. 7 (a) Schematic illustration of the reaction of bis(4-nitrophenyl) carbonate (BNC) with soluble  $\text{Li}_2\text{S}_8$  to produce lithium 4-nitrophenolate (LiNPH) and insoluble sulfur species. Reproduced with permission: Copyright 2019, American Chemical Society.<sup>17</sup> (b) Schematic demonstration of the NiDME additive working in a LSB. Reproduced with permission: Copyright 2020, Elsevier.<sup>39</sup> (c) The comparison of shuttle effect suppression ability between Celgard (up) and UIOSLi SSE (down). Reproduced with permission: Copyright 2020, Wiley-VCH.<sup>119</sup>

attention for suppressing the shuttle effect, boosting the reaction kinetics, and improving sulfur utilization in LSBs.

Among the strategies to mitigate the shuttle effect (trapping effect, shield effect and sieve effect), the trapping effect is the most common method. Functional separators can trap soluble LiPSs through physical, chemical and catalytic absorption effects.<sup>122</sup> Functional separators can trap LiPSs through physical blocking or/and chemical absorption. The trapped LiPSs on separators can be reutilized on conductive and catalytic surfaces, thus simultaneously achieving shuttle-free performance and high sulfur utilization. For instance, Hong *et al.*<sup>123</sup> reported a Ce-based metal-organic framework (MOF)/CNT coated separator. The porous CNT network with great electrical conductivity can physically trap LiPSs and reuse them on the secondary current collector. Moreover, the conversion of LiPSs was accelerated by the Ce-MOF catalyst. The synergistic effects of CNTs and Ce-MOFs effectively concealed the accumulation of LiPSs on separators. Desirable separators can also benefit the Li metal anodes. Li *et al.*<sup>124</sup> prepared a Janus separator to regulate the reaction on the cathode side and suppress the lithium dendrites. In particular, the single-atom Ru/reduced graphene oxide (rGO@Ru SAs) layer on the separators facing sulfur cathodes could immobilize and catalyze the LiPS conversions, whereas the layer of boron nitride nanosheets/cellulose nanofibers (BNNs@CNFs) toward the anode side homogenized the Li-ion flux for dendrite-free Li plating. Moreover, conductive coatings (*i.e.*, CNTs,<sup>123</sup> GO<sup>124</sup> and MXenes<sup>125</sup>) on separators are

also effective to decrease the interfacial resistance for improved sulfur utilization.

In short, to regulate sulfur conversion, separators should be endowed with multifunction, including the effective entrapment of LiPSs, the reuse of trapped sulfur, and the catalysis of Li-S redox kinetics.

### 3. Li-free metal sulfur batteries

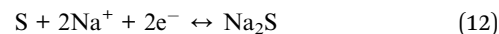
Following the great advances in LSBs, the sulfur cathode has been coupled with other alkali or alkaline earth metal anodes, such as Na, K, Mg, Ca, and Al, for Li-free MSBs. These metals are either available in the ocean or much richer than Li in the Earth's crust. In addition to addressing the concerns over unsustainability issues of Li metal anodes, some of these metals also have high reduction potentials or/and dendrite-free stripping/plating properties, and thus can contribute to high energy and safe MSBs. Briefly, the newly emerged "metal-sulfur" systems with similar conversion reactions to LSBs demonstrate great promise in either approaching high energy density or lowering the battery cost for large-scale applications. Li-free MSBs suffer from more sluggish reaction kinetics than LSBs, possibly due to the larger ionic radiuses (*e.g.*, Shannon's ionic radius of 0.76 for  $\text{Li}^+$ , 1.02 for  $\text{Na}^+$ , 1.38 for  $\text{K}^+$ , and 1.0 for  $\text{Ca}^{2+}$ ) and the higher polarization strength of multivalent ions.<sup>126</sup> In this section, we survey the state-of-the-art progress in understanding the mechanics and battery failure mechanisms of Li-free MSBs.

### 3.1 Na-S batteries

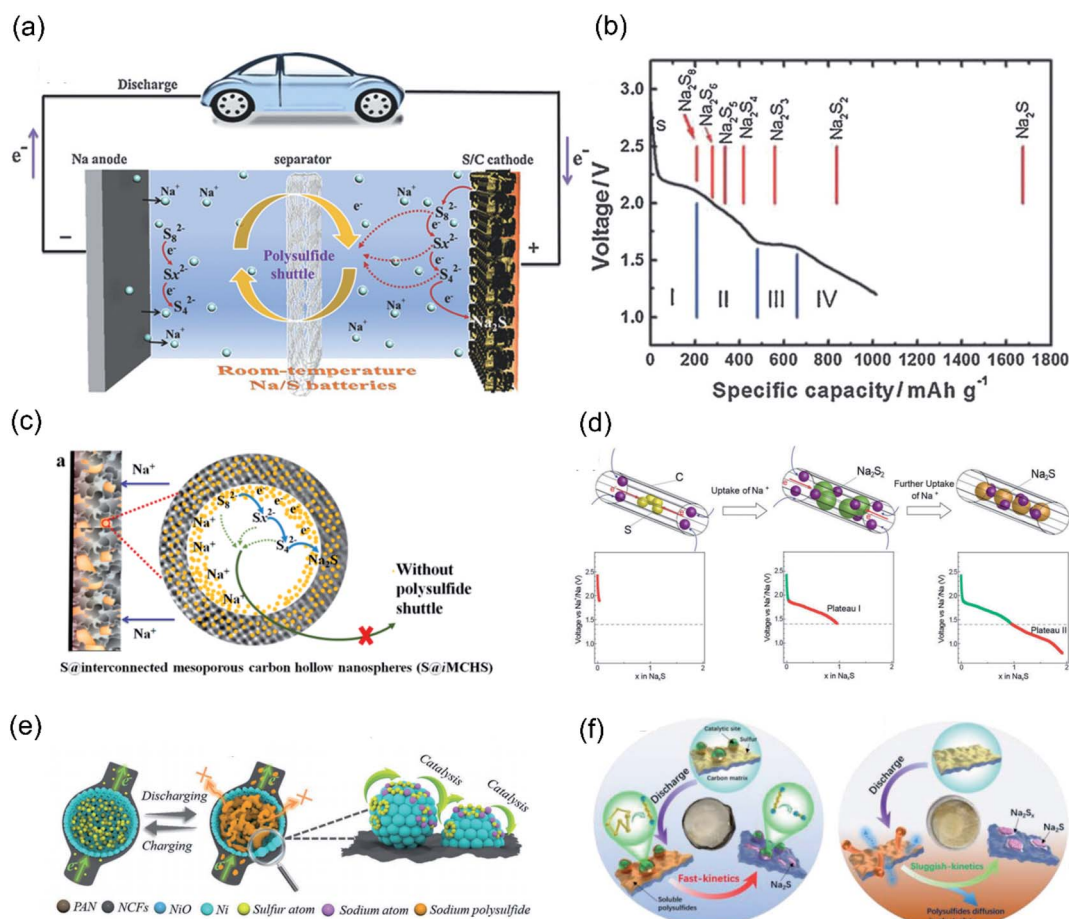
Sodium has similar physical and chemical properties to lithium and is an economically attractive substitute for lithium.<sup>127</sup> Indeed, the Na-S battery is nothing new, and has been successfully commercialized for stationary energy storage applications at high operating temperatures (300–350 °C) to melt electrodes and activate the solid beta-alumina electrolyte.<sup>128,129</sup> Unfortunately, the high operation temperature blocks its widespread application, particularly in electric vehicles. In this context, room-temperature sodium-sulfur batteries (RT-SSBs) have come into the research community's view in recent years to adopt the advantages of sulfur cathodes at low temperature and safer working conditions.<sup>130,131</sup> By taking advantage of the knowledge gained from LSBs, RT-SSBs have demonstrated discernible progress in fundamental understanding and improvement in battery performance.

A typical RT-SSB resembles the configuration of LSBs consisting of a sulfur/carbon cathode, a Na metal anode, and

a separator filled with an organic electrolyte (Fig. 8a).<sup>129</sup> During sodiation, the Na metal is oxidized to Na ions, which travel through the electrolyte/separator to reach the sulfur cathode. By accepting Na ions, sulfur will be reduced into sodium polysulfides ( $\text{Na}_2\text{S}_n$ ,  $4 \leq n \leq 8$ ) followed by  $\text{Na}_2\text{S}$ . RT-SSBs offer a high theoretical capacity of  $1672 \text{ mA h g}^{-1}$  and an energy density of  $1230 \text{ W h kg}^{-1}$  with  $\text{Na}_2\text{S}$  as the final product. During the following charging process,  $\text{Na}_2\text{S}$  will be oxidized back to sulfur. Na ions are reduced to Na metal, synchronously. The overall redox reactions can be described as:

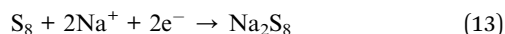


A series of sodium polysulfides are generated between the two solid-state end-products, similar to that in LSBs. The chemical composition and structures of reaction products at different discharging stages are illustrated in Fig. 8b,<sup>132</sup> which

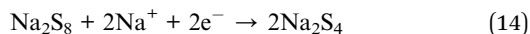


**Fig. 8** (a) The schematic of room temperature sodium-sulfur batteries. Reproduced with permission: Copyright 2017, Wiley-VCH.<sup>129</sup> (b) The discharge potential curve and the comparison between the theoretical (red) and practical discharge capacities (black). Reproduced with permission: Copyright 2014, Wiley-VCH.<sup>132</sup> (c) Sulfur encapsulated in the interconnected mesoporous carbon hollow nanospheres. Reproduced with permission: Copyright 2016, American Chemical Society.<sup>135</sup> (d) Small sulfur molecules ( $\text{S}_{2-4}$ ) confined in microporous carbon and the corresponding discharge curves. Reproduced with permission: Copyright 2014, Wiley-VCH.<sup>138</sup> (e) The schematic illustration of the hollow nickel unit to accommodate the volumetric expansion of sulfur and the catalytic effect of nickel atoms. Reproduced with permission: Copyright 2020, Wiley-VCH.<sup>143</sup> (f) Sulfur reaction mechanisms in  $\text{FeS}_2$ @ hierarchical carbon and pure hierarchical carbon. Reproduced with permission: Copyright 2020, Wiley-VCH.<sup>144</sup>

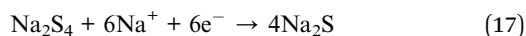
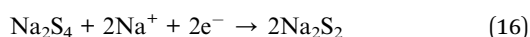
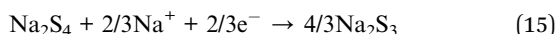
can be divided into four consecutive stages. At approximately 2.2 V, elemental sulfur is reduced into soluble Na<sub>2</sub>S<sub>8</sub> (Stage I):



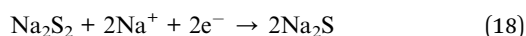
In the sloping region between 2.2 and 1.65 V, a liquid–liquid reaction between Na<sub>2</sub>S<sub>8</sub> and Na<sub>2</sub>S<sub>4</sub> occurs (Region II):



Subsequently, the soluble Na<sub>2</sub>S<sub>4</sub> is further reduced to insoluble Na<sub>2</sub>S<sub>3</sub>, Na<sub>2</sub>S<sub>2</sub>, or Na<sub>2</sub>S at approximately 1.65 V (Region III):



Residual Na<sub>2</sub>S<sub>2</sub> is finally reduced to Na<sub>2</sub>S in the sloping range of 1.65 to 1.20 V (Region IV):



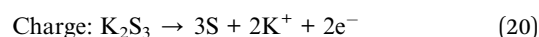
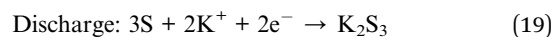
RT-SSBs inherit the intrinsic challenges of sulfur cathodes, such as the insulative nature of sulfur and sodium sulfides, volume expansion, and polysulfide shuttle effects.<sup>133</sup> RT-SSBs also suffer from problems such as the low reactivity of sulfur/Na<sub>2</sub>S<sub>x</sub> and the slow Na ion diffusion in electrolytes.<sup>134</sup> In this context, smart cathode structures, catalysts, and electrolytes have been investigated. In order to improve the conductivity and sulfur utilization in RT-SSBs, similar to LSBs, various porous carbon materials have been prepared for sulfur/carbon cathodes. For example, Wang *et al.*<sup>135</sup> reported interconnected mesoporous carbon hollow nanospheres (iMCHS) as an effective matrix to hold sulfur particles (Fig. 8c). The mesoporous carbon shell provided conductive paths to individual sulfur particles, thereby ensuring high sulfur utilization. As a result, the iMCHS/S cathode delivered a high capacity of 292 mA h g<sup>-1</sup> after 200 cycles. Further, functionalized and heteroatom-doped porous carbon materials were prepared to chemically adsorb polysulfides.<sup>136,137</sup> Xiao *et al.*<sup>136</sup> synthesized S,N-doped porous carbon with 3D tubular holes for sulfur storage. The uniform dispersion and incorporation of sulfur through covalent bonds in the carbon host were enabled by a vapor-infiltration method at high temperatures. Interestingly, the covalently bonded sulfur inhibited the formation of soluble polysulfides during cycling in the 1 M NaClO<sub>4</sub> PC electrolyte. Together with the strong polarity of the S,N-doped carbon to restrict sulfur diffusion, the cathode showed excellent long-term cycling stability for 1000 cycles and a rate capability of 543 mA h g<sup>-1</sup> at 5 A g<sup>-1</sup>. Ultra-microporous carbon/sulfur<sup>138</sup> and SPAN<sup>139</sup> have proven successful in LSBs and have also been used in RT-SSBs to eliminate the problematic polysulfides by transforming the Na–S reaction from “solid–liquid–solid” to “solid–solid” phase transformations. As shown in Fig. 8d, metastable small sulfur molecules (S<sub>2–4</sub>) were confined in microporous carbon.<sup>138</sup> In the confined space, NaS<sub>2</sub> can only be converted to small S<sub>2–4</sub>

molecules instead of the large S<sub>8</sub> ring during charging, further excluding the possible formation of soluble polysulfides. The “solid–solid” conversion SSBs lead to a high specific capacity of 1610 mA h g<sup>-1</sup> after 200 cycles.

Although porous carbon can physically constrain polysulfides for enhanced reversibility in RT-SSBs, carbon alone is apparently insufficient to accelerate the Na–S conversion.<sup>140</sup> The use of catalysts has become the main stream to improve electrochemical performance by engineering active sites to accelerate the diffusion–conversion process of polysulfides.<sup>141,142</sup> For metal catalysts in RT-SSBs, Zhang *et al.*<sup>130</sup> loaded transition-metal (M = Fe, Cu, and Ni) nanoclusters on hollow carbon nanospheres (HC)/sulfur composites. The M–S chemical bonds assisted the immobilization of sulfur and enhanced the activity and conductivity of the cathode. The battery thus remained at a high capacity of 394 mA h g<sup>-1</sup> after 1000 cycles at 0.1 A g<sup>-1</sup>. Ni is another representative metallic catalyst in RT-SSBs. Guo *et al.*<sup>143</sup> reported a 3D network (Ni-NCFs) host composed of nitrogen-doped carbon fibers (NCFs) and Ni hollow spheres. Each nickel hollow sphere could fully accommodate the volume expansion of sulfur during cycling and the nickel atoms displayed great catalytic effects (Fig. 8e). The cross-linked carbon fibers surrounding the nickel hollow spheres allowed the electrons to transport unimpeded, thus enhancing the conductivity of the electrodes. The results showed that the conductive Ni-NCF host could accelerate the electrochemical reaction kinetics by catalyzing the transformation of liquid polysulfides to solid Na<sub>2</sub>S. Yan *et al.*<sup>144</sup> prepared an FeS<sub>2</sub> nanograin/hierarchical carbon matrix (FeS<sub>2</sub>@NCM) as the host. The hierarchical carbon confined polysulfides and the FeS<sub>2</sub> nanograins absorbed and catalyzed polysulfides. Compared to the pure HCM, the FeS<sub>2</sub>@NCM exhibited better reaction kinetics (Fig. 8f). The cell delivered a reversible capacity of 395 mA h g<sup>-1</sup> after 850 cycles at 1 A g<sup>-1</sup>.

### 3.2 K–S batteries

As another member of alkali MSBs, the K–S battery (KSB) technology is just demonstrated to be possible compared to the Li–S and Na–S systems. Similar to LSBs, the reaction process of KSBs also involves complicated chemical and electrochemical reactions (Fig. 9a).<sup>145</sup> Besides the specified problems of Li/Na–S batteries that also exist for KSBs, potassiation of sulfur cathodes has a much larger volume change (300% for S → K<sub>2</sub>S vs. 80% for S → Li<sub>2</sub>S).<sup>146</sup> Moreover, the detailed reaction processes in KSBs are still under debate owing to the difficulties in analyzing potassium polysulfides such as K<sub>2</sub>S<sub>8</sub>, K<sub>2</sub>S<sub>5</sub>, and K<sub>2</sub>S<sub>3</sub>.<sup>147</sup> The final discharging products can be K<sub>2</sub>S<sub>3</sub> (Fig. 9b),<sup>148</sup> K<sub>2</sub>S<sub>2</sub>,<sup>145</sup> or K<sub>2</sub>S<sup>147,149</sup> (Fig. 9c), depending on the electrode material and electrolyte structure. The reaction pathway for most KSBs is that sulfur is reduced to long-chain polysulfides, short-chain polysulfides, and finally to K<sub>2</sub>S<sub>3</sub> (Fig. 9c). The discharge, charge, and overall reactions are shown below:



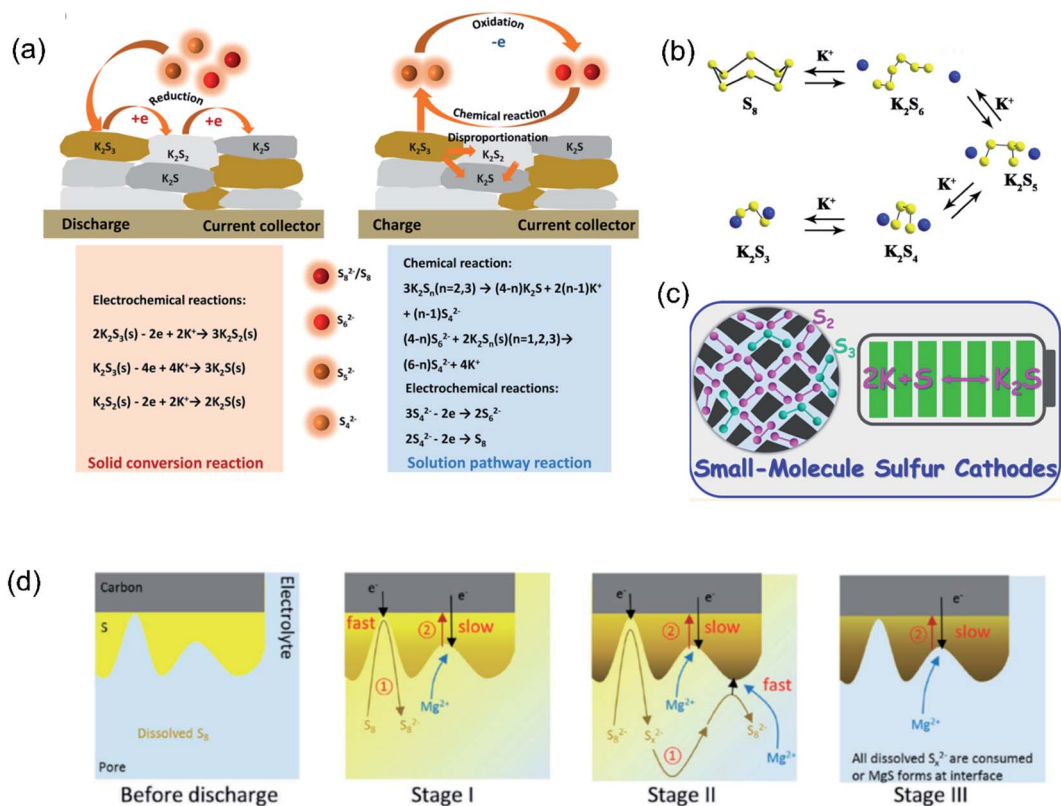


Fig. 9 (a) The electrochemical reactions and chemical reactions in K–S batteries. Reproduced with permission: Copyright 2018, American Chemical Society.<sup>145</sup> (b) The schematic of potassium–sulfur battery reaction process with the discharging product  $K_2S_3$ . Reproduced with permission: Copyright 2020, American Chemical Society.<sup>154</sup> (c) The schematic of potassium–sulfur battery reaction process in microporous carbon with the discharging product  $K_2S$ . Reproduced with permission: Copyright 2019, American Chemical Society.<sup>151</sup> (d) The schematic of the sulfur discharge reaction mechanism. Reproduced with permission: Copyright 2017, Wiley-VCH.<sup>159</sup>



$K_2S_3$  being the final product rather than  $K_2S$  may be caused by the low reactivity between sulfur and large K ions in the liquid electrolyte.

A survey of the recent progress in KSB research indicates that the knowledge gained on the path of developing LSBs and RT-SSBs provides paramount guidance towards dealing with the shuttle effect and slow reaction kinetics in KSBs.<sup>147–151</sup> For example, the ultramicroporous carbon/ $S_{2-4}$  cathode succeeded in long-term LSBs,<sup>58,59</sup> and RT-SSBs<sup>138</sup> were also studied in KSBs.<sup>151</sup> XPS and theoretical calculation analyses revealed that  $K_2S$  is the final potassiation product through the “solid–solid” reaction of  $2K + S \rightarrow K_2S$ , leading to a theoretical capacity of  $1672 \text{ mA h g}^{-1}$ . The reaction product is different from the  $K_2S_3$  for CMK-3/S<sup>148</sup> and the  $K_2S_2$  for  $K_2S_2/C$ .<sup>145</sup> Such a disparity was interpreted by theoretical calculations which proposed a disproportionation reaction of  $K_2S_2$  to form thermodynamically stable  $K_2S$  as the final potassiation product. The microporous carbon/small sulfur cathode showed a reversible capacity of  $869.9 \text{ mA h g}^{-1}$  after 150 cycles. A modified separator, highly concentrated electrolyte, and electrocatalyst have also been developed to regulate K–S conversions.<sup>147,152</sup> For

example, to promote the reduction kinetics from  $K_2S_3$  to  $K_2S$ , Lai *et al.*<sup>153</sup> reported imidazole-solvated copper catalysts to weaken the S–S bond of  $K_2S_3$  and promote the formation of  $K_2S$ , thus achieving a high sulfur capacity of  $922 \text{ mA h g}^{-1}$ . In order to suppress the polysulfide diffusion in KSBs, Ge *et al.*<sup>154</sup> prepared N-doped Co nanoclusters as a catalyst and coupled them with N-doped porous carbon. Both the N-doped carbon and Co nanoclusters can entrap polysulfides. Polysulfides can be smoothly converted on the surface of the Co nanocluster catalyst, thus fundamentally suppressing the shuttle effect in KSBs.

### 3.3 Mg–S batteries

Mg–S batteries have the highest volumetric energy density and lowest volume expansion among MSBs (as shown in Table 1). In addition, they display superior safety due to the nonvulnerable Mg dendrite formation during Mg plating/stripping in Mg anodes. The safe Mg–S batteries would be able to deliver a high theoretical capacity of  $1675 \text{ mA h g}^{-1}$  and an energy density of  $1330 \text{ W h kg}^{-1}$  by forming a  $Mg_2S$  final product. The high abundance of both sulfur and Mg also makes Mg–S batteries appealing as sustainable energy storage systems. The key challenge impeding the development of Mg–S batteries is now the



lack of compatible electrolytes for the high-valent Mg metal and effective transport of  $\text{Mg}^{2+}$  between anodes and cathodes.<sup>155</sup>

The first Mg–S battery was reported in 2011 using a non-nucleophilic electrolyte derived from hexamethyldisilazide magnesium chloride (HMDSMgCl) and  $\text{AlCl}_3$ ,<sup>156</sup> which broke the long-term difficulty in finding a non-nucleophilic electrolyte that was chemically compatible with both the sulfur cathode and Mg metal anode. Although this pioneering work only cycled two times with a capacity degradation from 1200 to 395  $\text{mA h g}^{-1}$ , it constituted the first step toward developing reversible Mg–S batteries. Later, the method to synthesize chloride electrolytes was simplified by a one-step reaction between magnesium-bis(hexamethyldisilazide)  $[(\text{HMDS})_2\text{Mg}]$  and  $\text{AlCl}_3$  in different ethers. The simplified synthesis route made it possible to further study and curb the Mg–S reaction pathways.<sup>157</sup> When a S/CMK400PEG cathode was discharged in the diglyme/PP14TFSI/ $(\text{HMDS})_2\text{Mg}$  electrolyte, it was found that  $\text{S}_8$  was reduced to soluble Mg polysulfide ( $\text{MgS}_4$ ), insoluble  $\text{MgS}_2$ , and finally to MgS, indicating an overall electrochemical reaction of  $\text{S} + \text{Mg} \rightarrow \text{MgS}$ .<sup>158</sup> Similar to LSBs, the reduction process associated with soluble polysulfides is much faster than the solid conversion from polysulfides to MgS (Fig. 9d).<sup>159</sup> Bieker *et al.*<sup>160</sup> studied the chemical stability and solubility of chemically prepared  $\text{Mg}_2\text{S}_8$  and  $\text{Li}_2\text{S}_8$  in various electrolytes by UV/vis spectroscopy. They found that the magnesium polysulfide has very similar disproportionation and dissociated equilibria to that observed for LiPSs. This finding implicates the possibility of cycling Mg–S batteries in a high- $\epsilon$  electrolyte to amplify the formation of beneficial  $\text{S}_3^{\cdot-}$ .<sup>161</sup>

The unfavorable electrolyte has thus far been considered the ‘Achille’s heel’ on the path of developing stable Mg–S batteries. To mitigate this challenge,  $\text{Mg}[\text{TFSI}]_2$ -diglyme was cycled in Mg–S cells, but it failed quickly due to the severe passivation layer of MgS and S–O on the Mg metal.  $\text{MgCl}_2$  was added to the above electrolyte to facilitate Mg plating by removing the detrimental passivation layers on Mg, thus giving rise to a 69% capacity retention after 110 cycles.<sup>162</sup> Nevertheless, chloride-containing electrolytes would severely corrode the Mg metal. The research community further explored non-corrosive electrolytes for stable Mg–S batteries. Zhao *et al.*<sup>163</sup> investigated a magnesium fluoroalkoxy borate electrolyte ( $\text{MgBOR}(\text{hfp})/\text{DME}$ ) for Mg–S batteries. The Cl-free Mg electrolyte allowed 100 times Mg stripping/plating with high coulombic efficiencies of >98%. The compatibility between the  $\text{MgBOR}(\text{hfp})$  electrolyte and sulfur cathodes was also demonstrated to be excellent with a reversible capacity of 200  $\text{mA h g}^{-1}$  after 100 cycles. Furthermore, the LiTFSI additive was introduced into the  $(\text{HMDS})_2\text{Mg}$ -based electrolyte to enhance the reversibility of Mg–S chemistry.<sup>164</sup> Two possible mechanisms were suggested for the enhanced reversibility: (i)  $\text{Li}^+$  may participate in the cathode reaction to form hybrid Mg/Li polysulfides, or (ii) the hard Lewis acid  $\text{Li}^+$  coordinates to low order Mg-polysulfides, thus enhancing the solubility and lowering the reoxidation energy barrier of polysulfides, finally making them electrochemically active. The LiTFSI-mediated electrolyte increased the reversible capacity from 200  $\text{mA h g}^{-1}$  to 1000  $\text{mA h g}^{-1}$  for more than 30 cycles.

The performance improvement in Mg–S batteries has also been demonstrated by using highly conductive carbon materials as sulfur hosts. For instance, sulfur particles were incorporated into carbon black, carbon nanotubes, and graphene to improve the sulfur utilization in Mg–S batteries.<sup>165–170</sup> Li *et al.*<sup>169</sup> reported a N,Co co-doped carbon framework as an effective S support where the Co catalyst, polar N-dopant and porous carbon structure work synergistically to improve the capacity reversibility, rate and cycling performance. Furthermore, microporous carbon/small sulfur electrodes were also explored to decrease the shuttle effect in Mg–S batteries.<sup>168</sup>

### 3.4 Ca–S batteries

In comparison to the Mg–S battery research, another type of alkaline-earth metal battery, namely the Ca–S battery, has just been demonstrated as proof-of-concept. The volume capacity and reduction potential of the Ca metal are close to those of metallic Li (2073  $\text{mA h cm}^{-3}$  vs. 2044  $\text{mA h cm}^{-3}$  and  $-2.9 \text{ V}$  vs. SHE vs.  $-3.04 \text{ V}$  vs. SHE).<sup>171,172</sup> Fortunately, Ca exhibits a much higher elemental abundance of 41 500 ppm than the 20 ppm of Li in the Earth’s crust (Table 1). These merits suggest that divalent Ca possesses high potential to be coupled with sulfur cathodes as high-energy and safe Ca–S batteries. However, the lack of compatible electrolytes for the reversible Ca metal anode and sulfur cathode restricts the Ca–S technology. So far, only three papers showed reversible Ca–S batteries.

Yu *et al.*<sup>173</sup> introduced a  $\text{LiCF}_3\text{SO}_3$  mediator into the  $\text{Ca}(\text{CF}_3\text{SO}_3)/\text{TEGDME}$  electrolyte to realize the first reversible Ca–S battery in 2019. The Li-ions in the electrolyte can react with the redox products of calcium polysulfides and facilitate ion diffusion in the bulk electrolyte and the SEI layer. This pioneering Ca–S cell showed a high discharge capacity of 800  $\text{mA h g}^{-1}$ . However, these cells consumed  $\text{LiCF}_3\text{SO}_3$  to form irreversible  $\text{Li}_2\text{S}$ , leading to the loss of capacity and limited lifetime of the batteries. Later, Li *et al.*<sup>174</sup> reported a high-voltage Ca–S cell (2.1 V) with the novel electrolyte calcium tetrakis(hexafluoroisopropoxy) borate,  $\text{Ca}[\text{B}(\text{hfp})_4]_2/\text{DME}$ . In the ether-based electrolyte, the reduction pathway of sulfur is very similar to that in LSBs, *e.g.*, sulfur was reduced to soluble polysulfides and then to solid CaS (Fig. 10a).<sup>171</sup> Insights into the electrochemical mechanism governing the Ca–S chemistry were also intensively examined by X-ray photoelectron spectroscopy and X-ray absorption spectroscopy.<sup>171</sup> These investigations demonstrate the possibility of exploring high-energy and sustainable Ca–S batteries.

### 3.5 Al–S batteries

Al–S batteries hold the potential to be the cheapest MSBs because Al is the most abundant metal element in the Earth’s crust. Each Al atom provides 3 electron transfers, thus achieving a high specific gravimetric capacity of 2980  $\text{mA h g}^{-1}$  and volumetric capacity of 8050  $\text{mA h cm}^{-3}$ , due to its relatively high density of 2.7  $\text{g cm}^{-3}$ . Al–S batteries can attain a high theoretical energy density of 1300  $\text{W h kg}^{-1}$  at an operating voltage of 1.23 V. Batteries assembled with high capacity and low-cost Al and sulfur have attracted increasing research attention.

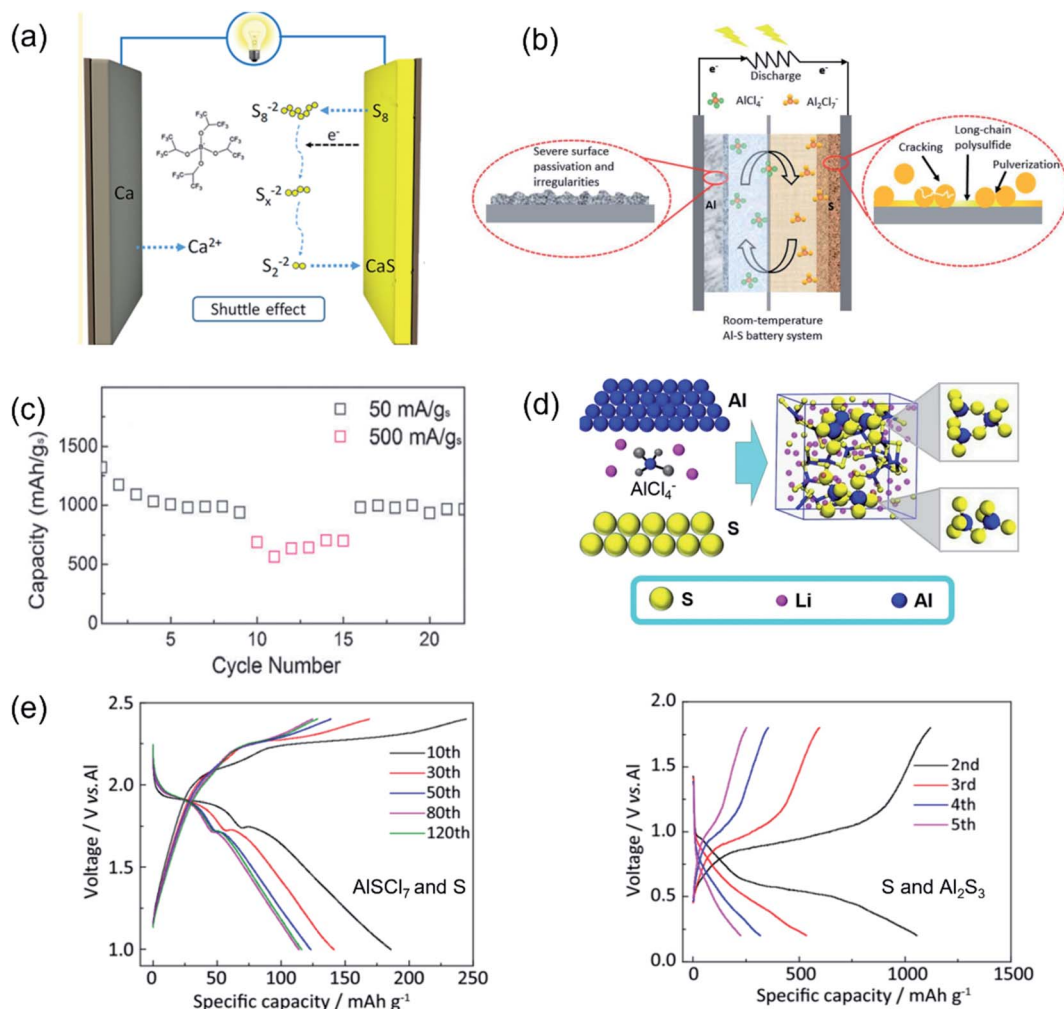


Fig. 10 (a) Schematic diagram of the Ca-S battery reaction process. Reproduced with permission: Copyright 2020, American Chemical Society.<sup>171</sup> (b) Schematic diagram of the reaction process and problems of aluminum-sulfur batteries in an ionic liquid electrolyte. Reproduced with permission: Copyright 2021, Royal Society of Chemistry.<sup>185</sup> (c) The cycling performance of Al-S batteries using a microporous activated carbon/sulfur cathode. Reproduced with permission: Copyright 2016, Wiley-VCH.<sup>177</sup> (d) Introducing Li<sup>+</sup>-ion mediation into the [EMIM]AlCl<sub>4</sub> ionic liquid in an Al-S battery system. Reproduced with permission: Copyright 2017, Elsevier.<sup>187</sup> (e) The charge and discharge curves of sulfur oxidation (S and Al<sub>2</sub>S<sub>3</sub>) and sulfur reduction (S and Al<sub>2</sub>S<sub>3</sub>) of Al-S batteries. Reproduced with permission: Copyright 2021, Springer Nature.<sup>178</sup>

The study of Al-S batteries can be traced back to the 1980s when the first nonaqueous Al-S battery was proposed by Marassi *et al.*<sup>175</sup> in 1977, and the aqueous Al-S battery was initiated by Licht *et al.*<sup>176</sup> in 1993. Although the concept was proposed almost 30 years ago, the development of reversibly high-energy Al-S batteries is still in its infancy. The main challenge lies in the lack of compatible electrolytes and feasible cathodes.<sup>177,178</sup> Different from other MSBs operated in ether or carbonate-based electrolytes, most Al-S batteries operate in ionic liquid electrolytes or deep eutectic solvent-based electrolytes. The mixture of anhydrous aluminum chloride (AlCl<sub>3</sub>) and 1-ethyl-3-methylimidazolium chloride (EMIC) ionic liquid is by far the most widely used electrolyte in Al-S batteries.<sup>179-184</sup> The Al-S reaction process in [EMIC]/AlCl<sub>3</sub> is described as follows (Fig. 10b):<sup>185</sup>



In an ionic liquid electrolyte system, a microporous carbon/S cathode was cycled as a rechargeable Al-S battery.<sup>177</sup> By confining sulfur in micropores, the sulfur and Al undergo solid-state conversion. The microporous C/S cathode delivered a high capacity of 1000 mA h g<sup>-1</sup>, even after 20 cycles (Fig. 10c). The successful implementation of the Al-S cell is attributed to the improved oxidation kinetics of AlS<sub>x</sub> by encapsulating sulfur from electrolyte attack and shortening the ion diffusion path with nanostructures. It is noted that there is not yet a standard electrolyte developed for Al-S systems, and thus detailed battery reaction mechanisms are elusive and preliminary.

In order to extend the cycle life of Al-S batteries, a carbonized metal-organic framework (MOF) with Cu was prepared to hold

Table 2 Summary of the performance of the representative lithium-free metal–sulfur batteries

| Materials  | Electrolyte   | Sulfur content (wt%)/or sulfur loading (mg cm <sup>-2</sup> ) | Initial discharge capacity (mA h g <sup>-1</sup> ) | Discharge (mA h g <sup>-1</sup> ) @ <i>n</i> cycles | Current density (mA g <sup>s</sup> <sup>-1</sup> ) |
|--|---|---|--|---|--|
| <b>Na-S</b>  |   |   |  |   |  |
| S/porous carbon fibers <sup>127</sup>                                | NaTFSI (2 M)/PC : FEC (1 : 1) + InI <sub>3</sub> (10 mM)  | 1.57 mg cm <sup>-2</sup>                                      | 1170   | 1007@50   | 167  |
| S/Fe-HC <sup>130</sup>   | NaClO <sub>4</sub> (1 M)/EC : DMC (1 : 1) + 5 wt% FEC   | 40%   | 1023   | 394@1000  | 100  |
| S/MOF-C <sup>136</sup>   | NaClO <sub>4</sub> (1 M)/P + 5 wt% FEC  | 37%   | 650  | 467@100   | 100  |
| SPAN <sup>139</sup>  | Na(PF) <sub>6</sub> /EC : DMC (1 : 1)   | 37.4%   | 360  | 270@1000  | 1000   |
| S/ZnS and CoS <sub>2</sub> (ref. 141)                                | NaClO <sub>4</sub> (1 M)/EC : DMC (1 : 1) ] + 5 wt% FEC   | 45.6%   | 1502   | 1405@100  | 2700   |
| S/Ni-N-doped carbon fibers <sup>143</sup>                            | NaClO <sub>4</sub> (1 M)/TEGDME   | 45%   | ~1410  | 570@1000  | 200  |
| S/carbon nanocage/FeS <sub>2</sub> (ref. 144)                        | NaClO <sub>4</sub> (1 M)/EC : DMC (1 : 1) + 3 wt% FEC   | 45.85%  | 431  | 233@270   | 1000   |
| S/Ni-MOF <sup>201</sup>  | NaClO <sub>4</sub> (1 M)/EC : DMC (1 : 1) + 5 wt% FEC   | 38.88%  | 1471   | 524@300   | 1673   |
| S/NiS <sub>2</sub> @N-doped CNT <sup>202</sup>                       | NaClO <sub>4</sub> (1 M)/EC : DMC (1 : 1) + 3 wt% FEC   | 22.4%   | 500  | 395@850   | 1000   |
| S/Mo <sub>2</sub> N-W <sub>2</sub> N@spherical carbon <sup>208</sup> | NaTFSI (2 M)/PC : FEC (1 : 1)   | 34.16%  | ~470   | 347@1000  | ~1673  |
|  |   |   | ~380   | 241@1000  | ~3346  |
|  |   |   | 960  | 401@750   | 1000   |
|  |   |   | ~1050  | 517@400   | 1000   |
| <b>K-S</b>   |   |   |  |   |  |
| S/CNT <sup>145</sup>   | KFSI (0.6 M)/DME  | 70%   | 720  | 184@5   | 50   |
| S/CNF <sup>147</sup>   | KCF <sub>3</sub> SO <sub>3</sub> (1 M)/TEGDME   | 50%   | 1160   | ~600@50   | ~167   |
| SPAN <sup>149</sup>  | KPF <sub>6</sub> (0.5 M)/EC : DMC (1 : 1)   | 45.5%   | 1050   | 997.5@100   | 837.5  |
| Microporous carbon/S <sup>151</sup>                                  | KPF <sub>6</sub> (0.8 M)/EC : DEC   | 20%   | ~1220 (2nd)  | 870@150   | 20   |
| S/CMK-S <sup>152</sup>   | KTFSI (5 M)/DEGDME  | 60.8%   | 606  | ~300@10   | 10   |
| S/Vulcan carbon <sup>153</sup>                                       | Cu(TFS) <sub>2</sub> (0.3 M)/KFSI (0.1 M)/Me-Im   | 56%   | ~650   | ~540@200  | 800  |
| Co,N-doped carbon/S <sup>154</sup>                                   | KPF <sub>6</sub> (0.8 M)/EC : DEC (1 : 1)   | 63.4%   | 657.1  | 355.3@150   | 200  |
| Iodine-doped/SPAN <sup>238</sup>                                     | KPF <sub>6</sub> (0.8 M)/EC : DEC (1 : 1)   | 17.7%   | 994  | 768@500   | ~837.5   |
| <b>Mg-S</b>  |   |   |  |   |  |
| S/Ketjenblack <sup>161</sup>   | LAGP/Mg (TFSI) <sub>2</sub> or Li(TFSI) <sub>2</sub> /DMSO (cathode)                                    | 76%   | ~1500  | 700@300   | ~668   |
| S@CMK-3 (ref. 163)   | Phenylmagnesium chloride solution/THF/AlCl <sub>3</sub> /LiCl   | 41.25%  | 800  | 200@100   | 167  |
| S/CNT <sup>166</sup>   | Mg(B(hfp) <sub>4</sub> ) <sub>2</sub> (0.8 M)/DEG : TEG (1 : 1)   | 64%   | 1247   | 1019@100  | 500  |
| S/Co,N-doped MOF <sup>169</sup>                                      | 0.5 M [Mg <sub>4</sub> Cl <sub>6</sub> (DME) <sub>6</sub> ][B(hfp) <sub>4</sub> ] <sub>2</sub>          | 29.2  | 600  | ~400@200  | 1673   |
| S@microporous carbon <sup>168</sup>                                  | Mg(HMDS) <sub>2</sub> (0.5 M)/AlCl <sub>3</sub> (1 M)/LiTFSI (1 M)/DGE                                  | 64.7%   | 878  | 368.0@200   | 167  |
| S/activated carbon cloth <sup>170</sup>                              | (PhMgCl) <sub>2</sub> -AlCl <sub>3</sub> (0.4 M)/LiCl (1 M)/THF   | ~10%  | 930  | 200@100   | ~167   |
| S/MOF derivative carbon <sup>169</sup>                               | (HMDS) <sub>2</sub> Mg-2AlCl <sub>3</sub> /LiTFSI   | 32.97%  | 600  | 400@200   | 1673   |
| S@mesoporous carbon <sup>239</sup>                                   | THFPB (0.5 M)/MgF <sub>2</sub> (0.05 M)/DME   | 85%   | 1081   | ~900@30   | 50   |
| S@rGO <sup>240</sup>   | (HMDS) <sub>2</sub> Mg/2AlCl <sub>3</sub> /MgCl <sub>2</sub> /TEGDME                                    | 49%   | ~1000  | 388@40  | 20   |
| <b>Ca-S</b>  |   |   |  |   |  |
| S/activated carbon cloth <sup>171</sup>                              | Ca[B(hfp) <sub>4</sub> ] <sub>2</sub> (0.5 M)/DME   | 10%   | ~900   | 200@15  | ~167   |
| S/CNF paper <sup>173</sup>   | LiCF <sub>3</sub> SO <sub>3</sub> (0.5)/Ca (CF <sub>3</sub> SO <sub>3</sub> ) <sub>2</sub> (0.2)/TEGDME | 2 mg cm <sup>-2</sup>   | ~800   | 300@20  | ~167   |
| S/Ketjenblack <sup>174</sup>   | Ca[B(hfp) <sub>4</sub> ] <sub>2</sub> (0.25 M)/DME  | 53%   | ~920   | 120@15  | n/a  |

Table 2 (Contd.)

| Materials                       | Electrolyte  | Sulfur content (wt%)/or sulfur loading (mg cm <sup>-2</sup> ) | Initial discharge capacity (mA h g <sup>-1</sup> ) | Discharge (mA h g <sup>-1</sup> ) @ <i>n</i> cycles | Current density (mA g <sup>-1</sup> ) |
|---------------------------------|--|---|--|---|---------------------------------------|
| <b>Al-S</b>                     |  |   |  |   |                                       |
| S/CNT <sup>178</sup>            | Urea-AlCl <sub>3</sub> (1 : 1.3)   | 18%   | 225  | ~120@200  | 200                                   |
| S/activated CNF <sup>179</sup>  | EMICl-AlCl <sub>3</sub> (1 : 1.3)  | 33%   | 1220   | ~600@10   | ~84                                   |
| S/SPAN <sup>180</sup>           | EMICl-AlCl <sub>3</sub> (1 : 1.5)  | 10%   | 320  | ~201@21   | 25                                    |
| BN/S/C <sup>181</sup>           | EMICl-AlCl <sub>3</sub> (1 : 1.5)  | 10%   | ~700   | 532@300   | 100                                   |
| S/CNT <sup>182</sup>            | EMICl-AlCl <sub>3</sub> (1 : 1.5)  | 58.8%   | 2129   | 375@10  | 50                                    |
|                                 | Urea-AlCl <sub>3</sub> (1 : 1.5)   | 58.8%   | 2359   | 125@10  | 50                                    |
| S/Co-based MoF <sup>183</sup>   | EMICl-AlCl <sub>3</sub> (1 : 1.3)  | 42%   | 693  | ~160@160  | 300                                   |
| S/carbonized-MOF <sup>186</sup> | EMICl-AlCl <sub>3</sub> (1 : 1.3)  | n/a   | 1200   | ~460@500  | 1000                                  |
| S/activated CNF <sup>187</sup>  | LiCF <sub>3</sub> SO <sub>3</sub> (0.5 M)/EMICl-AlCl <sub>3</sub> (1 : 1.25) | 33%   | 1000   | ~600@50   | ~170                                  |
| S/CMK-3 (ref. 188)              | EMIBr-AlCl <sub>3</sub> (1 : 1.3)  | 40%   | 1500   | ~180@20   | 251                                   |
|                                 | NBMPBr-AlCl <sub>3</sub> (1 : 1.3)   | 40%   | 1390   | ~450@20   | 251                                   |

sulfur particles.<sup>186</sup> The Cu in the carbon matrix can improve the conductivity of the matrix so that it decreased the sulfur conversion barrier. In addition, XRD and Auger spectrum analyses revealed S-Cu ionic clusters in the carbonized MOF/S composite, which facilitated the redox reaction and sulfur reversibility during cycling. As a result, the Al-S battery achieved a reversible capacity of 460 mA h g<sup>-1</sup> at the 500th cycle. To modify the electrolyte structure, Yu *et al.*<sup>187</sup> introduced LiCF<sub>3</sub>SO<sub>3</sub> into the [EMIM]AlCl<sub>4</sub> ionic liquid (denoted as Li<sup>+</sup>-Al[EMI]Cl<sub>4</sub>, see Fig. 10d). The presence of the Li<sup>+</sup>-ion mediator led to more soluble short chain Al polysulfides, which lowered the electrochemical kinetic barrier for the reduction or oxidation of Al polysulfides. XPS results and DFT calculations further suggested that the Li<sup>+</sup> ions promoted the reactivation of sulfide species by suppressing the formation of Al=S bonds upon full discharging. Operating in the Li<sup>+</sup>-mediated electrolyte, the Al-S battery achieved 50 cycles with a residual capacity of 600 mA h g<sup>-1</sup>. To mitigate the high dissociation energy from Al<sub>2</sub>Cl<sub>7</sub><sup>-</sup> to Al<sup>3+</sup> in the [EMIM]AlCl<sub>4</sub> ionic liquid electrolyte, Br atoms were incorporated to form Al<sub>2</sub>Cl<sub>6</sub>Br<sup>-</sup> for lower dissociation energies, which is another efficient method to improve the kinetic process in the Al-S system.<sup>188</sup> Another main obstacle for the Al-S system is the low reduction potential of sulfur (~1 V vs. SHE) in [EMIM]AlCl<sub>4</sub>. Li *et al.*<sup>178</sup> reported replacing EMIC with urea to cooperate with AlCl<sub>3</sub> for high voltage Al-S batteries. The reaction pathway changed from the redox of sulfur ↔ Al<sub>2</sub>S<sub>3</sub> in the EMIC/AlCl<sub>3</sub> electrolyte to AlSCl<sub>7</sub> ↔ sulfur in the AlCl<sub>3</sub>/urea electrolyte. The latter contributed a ~1.8 V discharging potential, which is much higher than the ~0.5 V for the former reaction path (Fig. 10e). Benefiting from the high electrochemical potential, the Al-S battery can run 200 cycles at around 1.8 V.

According to the above examinations of the Li-free MSBs, it is found that studies on the emerging battery systems are evidently in the early stage. Compared to LSBs, the high abundance of elemental resources and potentially high energy density of Li-free metal anodes (Table 1) motivate the exploration of these new MSB technologies. However, studies show that the emerging MSBs inherit the critical issues of LSBs, such as the insulation of active materials and polysulfide shuttling effects, coupled with emerging challenges associated with the lack of a suitable electrolyte for stable metal anode stripping/plating, sluggish reaction kinetics and poor cycling efficiencies. In particular, MSBs using alkali-metal anodes (*i.e.*, Na and K) face severe safety issues arising from the high chemical activity and dendrite-plating behavior of Na and K metals. Although alkaline-earth MSBs (Mg-S, Ca-S, and Al-S) pose better safety due to the dense and dendrite-free plating of metal anodes, these systems encounter problems of sluggish ion conductivity, the lack of a compatible electrolyte, and poor cycling stability. A general problem of Li-free MSBs is the huge volume expansion of sulfur particles during discharging (*i.e.*, 309% in K-S batteries and 180% for Na-S batteries), stemming from the larger ionic radius of Na<sup>+</sup> and K<sup>+</sup> than that of Li<sup>+</sup>. It could cause cathode degradation and rapid battery failure. Last but not least, fundamental understandings of the Li-free MSBs are far from sufficient. Some contradictory descriptions of the K-S

reaction are even reported. Therefore, intensive experimental and theoretical characterization studies are recommended to unveil their working processes before attempting to achieve high-performance Li-free MSBs.

To better explore the development direction of high-performance Li-free MSBs, we have summarized the performance of the state-of-the-art Li-free MSBs in Table 2. For the cathode structures, sulfur particles are widely incorporated into carbon hosts and catalysts to improve the electrochemical performance, similar to that in LSBs. Interestingly, different electrolytes are utilized for one MSB system, such as  $\text{NaClO}_4$  in TEGDME or  $\text{NaPF}_6$  EC/DMC for Na-S batteries, potentially due to immature electrolyte chemistry. Exploring desirable

electrolyte systems is certainly a crucial topic for these emerging MSB technologies. Except for Na-S batteries, most Li-free MSBs present moderate cycle life and low sulfur utilization, and hence more effort is required for engineering sulfur cathodes in future studies.

#### 4. *In situ* characterization to understand sulfur conversion mechanisms

The multi-step metal-sulfur reactions occurring during cycling lead to complex reaction mechanisms. An in-depth and systematic understanding of the reaction processes in MSBs will



Fig. 11 (a) *In situ* XRD of Li-S batteries during the discharge and charge process. Reproduced with permission: Copyright 2017, Springer Nature.<sup>9</sup> (b) *In situ* XRD of Na-S batteries and no sulfur signal at the end of the charge state. Reproduced with permission: Copyright 2019, Springer Nature. (c) *In situ* XRD of the sulfur oxidation and reduction process in Al-S batteries. Reproduced with permission: Copyright 2021, Springer Nature.<sup>178</sup> (d) *In situ* XRD contour images of MoB/S and C/S cathodes of Li-S batteries, and the corresponding charging-discharging curve. Reproduced with permission: Copyright 2020, Wiley-VCH.<sup>207</sup>

be beneficial to offer radical strategies to address the fundamental problems hindering their practical applications.<sup>8</sup> Manifold *in situ*/operando characterization methods have been undertaken to unveil the underlying mechanisms in MSBs, such as transmission electron microscopy (TEM),<sup>13,93,189–191</sup> ultraviolet-visible (UV-vis) absorption spectroscopy,<sup>32,192–195</sup> XANES,<sup>196–199</sup> and XRD.<sup>20,178,199–202</sup> Each characterization method has its specific strength in disclosing the structural or/and compositional evolutions.

*In situ* XRD is an effective method to probe the phase evolutions during charging and discharging, particularly for crystalline S<sub>8</sub> and metal sulfides.<sup>20,178,200</sup> As mentioned in Section 2.1, the *in situ* XRD study demonstrated the irreversibility of the  $\alpha$ -sulfur phase after the 1<sup>st</sup> cycle in LSBs.<sup>25</sup> Soluble LiPSs have long been considered undetectable by XRD, due to their lack of long-range order and rapid molecular reorientation in the bulk electrolyte. This was taken for granted until Conder *et al.*<sup>9</sup> found that long-chain LiPSs were visible when adsorbed at the silica surface of a glass-fiber separator. During lithiation, two broad peaks at 25.56° and 28.32° were formed along with the rapid disappearance of crystalline  $\alpha$ -sulfur peaks. The new peaks were assigned to long-chain LiPSs, whose intensity decreased over time towards the end of discharging processes, indicating the reduction of LiPSs into lithium sulfides (Fig. 11a). However, the LiPS peaks did not completely disappear during the whole discharging/charging process, indicating that the long-chain LiPSs adsorbed on glass-fiber separators were preserved, and for this reason, a lot of irreversible charge capacities were observed during cycling. They also directly monitored LiPSs in electrolytes without silica absorbers, and found negligible XRD peaks, indicating the importance of adsorption to form organized LiPS layers. *In situ* XRD has also been utilized to probe the phase evolutions in RT-SSBs.<sup>18,27</sup> By monitoring the reaction process of a NiS<sub>2</sub>/N-doped CNT/S cathode, it was observed that the XRD peak of crystalline sulfur disappeared after the first cycle, and reversible (dis)appearance of polysulfides (Na<sub>2</sub>S<sub>x</sub>) and Na<sub>2</sub>S occurred in the following cycles, illustrating a polysulfide and sodium sulfide conversion mechanism (Fig. 11b).<sup>202</sup> The reversible redox process between AlSCl<sub>7</sub> and S, S and Al<sub>2</sub>S<sub>3</sub> in Al–S batteries has also been verified by *in situ* XRD measurements (Fig. 11c).<sup>178</sup>

Apart from monitoring the intrinsic reaction processes, *in situ* XRD studies can provide circumstantial evidence for the favorable catalytic effect in MSBs.<sup>203–206</sup> According to the clear appearance and disappearance of sulfur and Li<sub>2</sub>S peaks during cycling in an *in situ* XRD test, Ye *et al.*<sup>205</sup> demonstrated that the heterostructure MoN–VN catalyst could regulate the LiPS diffusion and complete sulfur conversion during cycling, which was in sharp contrast to the MoN/S cathode retaining the  $\alpha$ -S<sub>8</sub> peaks during the whole discharging process. This result was in accordance with the high capacity of 708 mA h g<sup>−1</sup> at 2C for MoN–VN-based LSBs. He *et al.*<sup>207</sup> compared the XRD patterns of carbon/S and MoB/S cathodes using synchrotron *in situ* XRD measurement. Residual  $\alpha$ -S<sub>8</sub> peaks were detectable but the peaks for the lithiation product Li<sub>2</sub>S were indiscernible at the end of discharge for C/S, whereas the  $\alpha$ -S<sub>8</sub> peaks in MoB/S cathodes disappeared completely at the initial discharge which

is associated with the increasing peak intensity of Li<sub>2</sub>S (Fig. 11d). Such distinctive results illustrated that the MoB catalyst can restrict LiPS diffusion and facilitate the Li<sub>2</sub>S deposition/dissolution. Similarly, *in situ* XRD characterization illustrated the reversible redox between S and Na<sub>2</sub>S in a Mo<sub>2</sub>N–W<sub>2</sub>N catalyst-mediated RT-SSB.<sup>208</sup> *In situ* XRD has also been of service to identify the selective catalytic mechanisms in RT-SSBs. The distinctive XRD peak change from Na<sub>2</sub>S<sub>4</sub> to Na<sub>2</sub>S illustrates that in RT-SSBs with the Fe single-atom catalyst, short-chain polysulfides are readily catalyzed into Na<sub>2</sub>S. However, the generation of long-chain polysulfides is catalytically promoted in single-atom Pt modified RT-SSBs.<sup>22</sup>

Besides keeping track of sulfur phase change, *in situ* XRD is also a powerful tool to probe the phase evolution of electrocatalysts in MSBs.<sup>209,210</sup> Wang *et al.*<sup>209</sup> demonstrated the function of niobium tungsten oxide (NWO) in a working LSB. In the discharging process, the NWO peaks shifted to lower angles due to the formation of Li<sub>x</sub>NWO. The Li<sub>x</sub>NWO was demonstrated to play a unique role in promoting the LiPS conversion efficiency by acting as a Li-transfer bridge between LiPSs and Li<sub>2</sub>S, thus jumping across the sluggish solid–solid conversion from Li<sub>2</sub>S<sub>2</sub> to Li<sub>2</sub>S. In addition, the Li<sub>x</sub>NWO exhibited stronger chemical interactions with LiPSs. Likewise, Liu *et al.*<sup>210</sup> observed the reversible lithiation and delithiation of the TiS<sub>2</sub> catalyst in TiS<sub>2</sub>/S cathodes. This work claimed that the lithiated TiS<sub>2</sub> was the conductive catalyst and strong LiPS adsorber, rather than TiS<sub>2</sub>, revealing the dynamic nature of electrocatalysts during discharging/charging in LSBs. For Mg–S batteries, reversible chlorination of the Ag metal catalyst to prevent Ag<sub>2</sub>S formation for shielding the sulfur active material was demonstrated by an *in situ* XRD study.<sup>21</sup>

*In situ* TEM is a powerful tool to understand the electrochemical reaction dynamics of MSBs at high spatial and temporal resolutions by revealing the morphological evolution, phase change and chemical composition transformations.<sup>13,93,189–191</sup> By observing the lithiation process of sulfur particles sealed in CNTs under *in situ* TEM, Kim *et al.*<sup>14</sup> reported that sulfur was directly reduced to Li<sub>2</sub>S without the formation of any intermediates and the Li–S reaction front was flat, suggesting the interface of Li<sub>2</sub>S/S to be possibly electrically conductive (Fig. 12a). Our group studied the volume expansion of sulfur particles in meso- and microporous CNFs during lithiation by using *in situ* TEM.<sup>13</sup> It was found that the lithiation product, Li<sub>2</sub>S, was constrained within the microporous CNFs with only  $\approx$ 35% volume expansion and the carbon host remained intact without fracture. In contrast, the mesoporous CNF/S electrode exhibited a larger volume expansion of over 61% and overflowing of Li<sub>2</sub>S, a testament to its poor cycling stability in real batteries. Unlike the direct Li<sub>2</sub>S formation in LSB studies, under the same measurement conditions, sodiation of sulfur involved a series of intermediates, including Na<sub>2</sub>S<sub>x</sub> ( $x \geq 6$ ), Na<sub>2</sub>S<sub>5</sub>, Na<sub>2</sub>S<sub>4</sub>, and Na<sub>2</sub>S<sub>2</sub>, before approaching Na<sub>2</sub>S (Fig. 12b).<sup>191</sup> More interestingly, a large proportion of sulfur would not be converted to Na<sub>2</sub>S in RT *in situ* TEM study. When increasing the operating temperature to 200–300 °C, the discharge product would be Na<sub>2</sub>S<sub>2</sub> and Na<sub>2</sub>S without sulfur

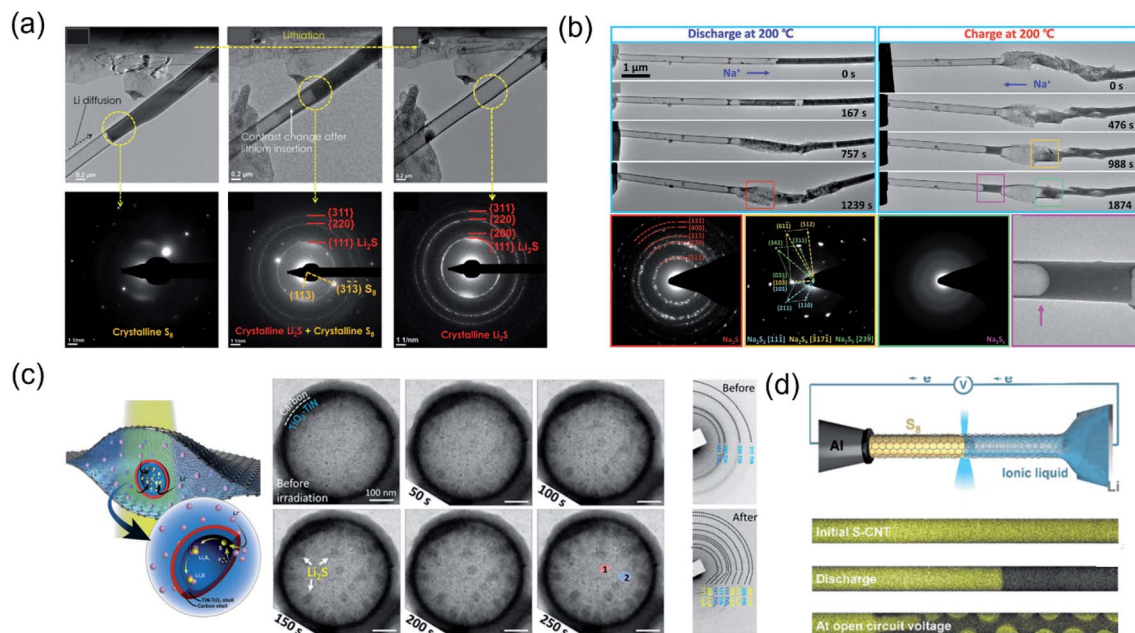


Fig. 12 (a) *In situ* TEM showing sulfur reduced to  $\text{Li}_2\text{S}$  directly in Li-CNT/S solid-state batteries. Reproduced with permission: Copyright 2015, Wiley-VCH.<sup>14</sup> (b) *In situ* TEM showing the evolution of sulfur going through  $\text{Na}_2\text{S}_x$  ( $x \geq 6$ ),  $\text{Na}_2\text{S}_5$ ,  $\text{Na}_2\text{S}_4$ ,  $\text{Na}_2\text{S}_2$ , and  $\text{Na}_2\text{S}$  in Na-CNT/S solid-state batteries. Reproduced with permission: Copyright 2021, Wiley-VCH.<sup>191</sup> (c) Schematic illustration of a graphene liquid battery and *in situ* TEM images of the  $\text{Li}_2\text{S}$  nucleation and growth in  $\text{TiO}_2$ -TiN hollow spheres. Reproduced with permission: Copyright 2019, Royal Society of Chemistry.<sup>93</sup> (d) Schematic of the *in situ* devices and sulfur distribution at initial, discharge, and open circuit voltage stages. Reproduced with permission: Copyright 2020, American Chemical Society.<sup>211</sup>

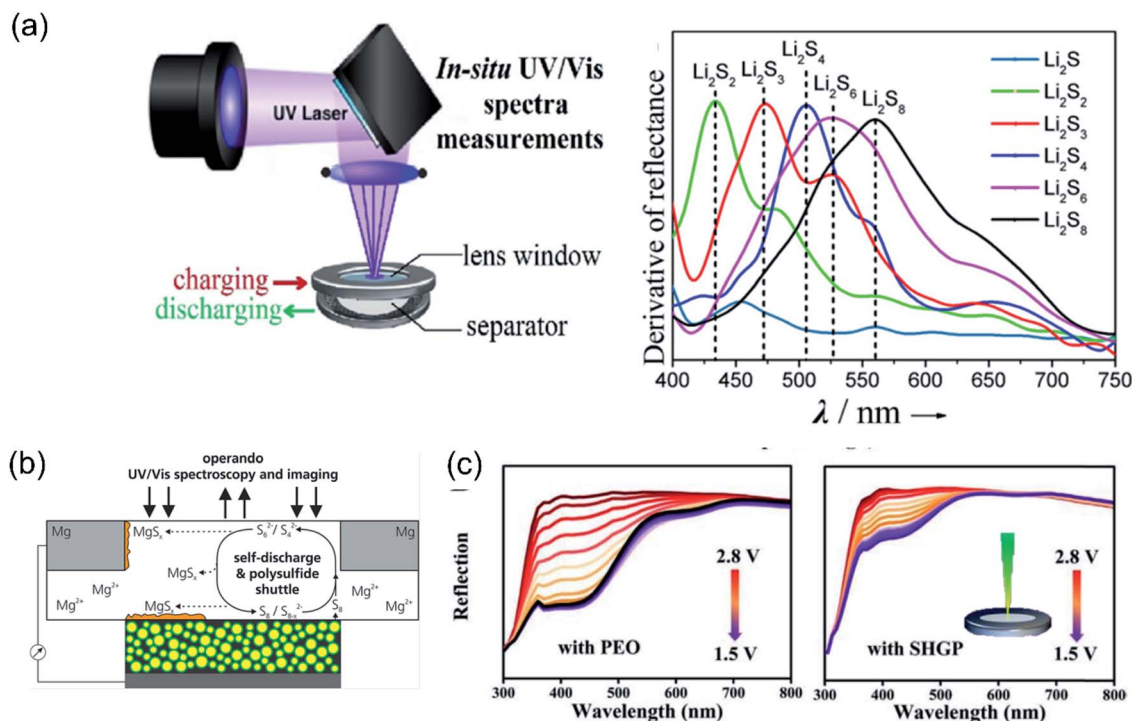


Fig. 13 (a) Schematic of the *in situ* UV-vis devices and related peaks of different sulfur species. Reproduced with permission: Copyright 2016, American Chemical Society.<sup>193</sup> (b) Schematic illustration of the proposed reaction process of the Mg-S battery based on the operational UV-vis spectroscopy and imaging results. Reproduced with permission: Copyright 2021, American Chemical Society.<sup>214</sup> (c) *In situ* UV-vis spectrum when using the poly (ethylene oxide) electrolyte and using an ultra-high ion-conducting gel polymer electrolyte. Reproduced with permission: Copyright 2019, Elsevier.<sup>194</sup>

residuals, which was attributable to the improved electron/ion transport kinetics at high temperatures.

Although these open-cell setups using metal/metal oxide as the counter electrode/electrolyte could provide useful information on the metal–sulfur reactions, they are infeasible to study

the formation and conversion of soluble polysulfides in real batteries. To mitigate this issue, our group has taken the first step towards realizing real-time observation of the nucleation and growth of solid lithium sulfides from soluble polysulfides by employing a graphene liquid cell (GLC)-based liquid *in situ*

**Table 3** Capabilities, limitations and application examples of *in situ* characterization techniques for metal–sulfur batteries

| <i>In situ</i> techniques | Capabilities   | Limitations  | Application in metal–sulfur battery study  |
|---------------------------|--|--|--|
| XRD                       | Monitor phase transitions of sulfur species during cycling   | Direct observation of soluble polysulfides by XRD remains challenging  | (1) Probe sulfur and sulfur species evolution during cycling <sup>9,20,178,219</sup><br>(2) Provide evidence for the profitable catalytic effect <sup>203–206</sup><br>(3) Probe the phase evolution of electrocatalysts <sup>21,209,210</sup>   |
| XANES                     | Probe S element reduction and oxidation state changes no matter whether it is crystal or amorphous, solid or liquid<br>Monitor the contributions of different sulfur compounds in the cathode during cycling | X-ray absorption fine structure is affected by the sulfate groups in the salt or the solvent   | (1) Study the capacity degradation mechanism <sup>198,220</sup><br><br>(2) Explore the reaction process and intermediates during the redox process <sup>61,178,198,199</sup><br>(3) Provide evidence for the profitable catalytic effect <sup>221,222</sup>  |
| XPS                       | Study chemical composition, charge transfer, and chemical bonds on the surface   | The cell design is complex   | (1) Analysis of interfaces of the electrode and electrolyte <sup>223–225</sup><br>(2) Provide evidence for the profitable catalytic effect. (semi- <i>in situ</i> XPS) <sup>226</sup>  |
| NMR                       | Monitor changes in the chemical structure which involves detection of radio frequency<br>Quantitative tracking of the species concentration  | The experimental setup is expensive<br><br>Achieving resolution below 100 $\mu\text{m}$ is hard<br>The alternating currents in the EC and NMR cause interferences                                      | Explore the reaction process <sup>143,150,171,227</sup>  |
| Raman                     | Monitor the compositional and structural changes of sulfur species/related species in the electrolyte or the surface of the electrode  | Hard to detect the signal of low-concentration soluble polysulfides  | (1) Explore the reaction process <sup>143,150,171,227</sup><br>(2) Provide evidence for the profitable catalytic effect <sup>227,228</sup><br>(3) Identify reaction intermediates in the electrolyte <sup>178,188,229</sup><br>(4) Provide evidence for suppression of the shuttle effect <sup>230–232</sup> |
| UV-vis                    | Monitor the evolution of soluble polysulfides qualitatively and quantitatively   | Limited detection of solid metal sulfides and it cannot be applied in solid-state batteries as well as carbonate-based electrolytes  | (1) Exploration of the conversion process between sulfur and sulfur species <sup>32,192,193</sup><br>(2) Monitor the shuttle effect <sup>15–18</sup>   |
| FTIR                      | Detect the chemical information of surface species   | The reflection is quite low for conductive carbon additives  | (1) Detect polysulfides and electrolyte interactions <sup>233</sup><br>(2) Quantify the order and concentration of soluble LiPSs in the electrolyte during cycling <sup>234</sup>  |
| AFM                       | Observe the surface morphology and structure   | The large volume change may make trackable features in the topography unrecognizable   | Observe the interfacial evolution of the electrode/electrolyte <sup>235–237</sup>  |
| TEM                       | (1) Morphology change of solid sulfur and metal sulfides<br><br>(2) Phase change and chemical composition transformations  | (1) Open-cell setups cannot be applied in liquid electrolyte systems<br><br>(2) The lithiation process of graphene liquid cells is ignited by electron beam, but it cannot achieve the cycling process | (1) Monitor the chemical composition transformation and volume expansion of the lithiation/delithiation process <sup>13,93,189,190</sup><br>(2) Observe the nucleation and growth of metal sulfides <sup>93,190</sup>  |



TEM technique (Fig. 12c).<sup>93</sup> By analyzing the lithiation of sulfur in a series of hollow spheres, including nonpolar carbon, polar/nonpolar TiO<sub>2</sub>-TiN/C spheres, and nonpolar/polar C/TiO<sub>2</sub>-TiN spheres, it was found that the sulfur host with inner polar materials resulted in the most favorable formation of lithium sulfides without the risk of polysulfide diffusion. For the C (outer wall)/TiO<sub>2</sub>-TiN (inner wall)/S structure, it is presented that the formation of lithium sulfides followed diffusion-controlled-to-reaction-limited growth kinetics and a crystalline-to-amorphous phase transition. The correlations established among the nucleation and growth dynamics of lithium sulfides, the immobilization of polysulfides and the chemical nature of host materials not only provided a whole picture of the unique liquid/solid transition in LSBs but also offered fundamental guidelines to design high-performance sulfur cathodes. In order to understand the polysulfide electrochemistry, Wang *et al.*<sup>211</sup> constructed a hollow CNT/S-ionic liquid electrolyte cell that allowed real-time imaging of polysulfide evolution in LSBs using an environmental TEM (Fig. 12d). They found that the long-chain LiPSs would be coordinated immediately by Py<sub>14</sub><sup>+</sup> cations in an ionic liquid electrolyte, which was mitigated by adding low polarized solvents in the electrolyte thus providing a rapid polysulfide-to-Li<sub>2</sub>S transition.

*In situ* UV is a useful tool to qualitatively/quantitatively determine soluble polysulfides in MSBs.<sup>212</sup> The peaks referring to Li<sub>2</sub>S<sub>8</sub>, Li<sub>2</sub>S<sub>6</sub>, Li<sub>2</sub>S<sub>4</sub>, and Li<sub>2</sub>S<sub>2</sub> can be clearly distinguished by UV-vis (Fig. 13a), which makes *in situ* UV feasible to give insights into the sulfur chemistry in a bulk electrolyte.<sup>32,192,193</sup> Xu *et al.*<sup>193</sup> analyzed the LiPS transformation in sulfhydryl-functionalized graphene nanosheets with a sulfur copolymer (S-GSH) cathode. With the proceeding of the discharge process, S-GSH was mainly converted to Li<sub>2</sub>S<sub>2</sub> and Li<sub>2</sub>S<sub>4</sub>, and then with further lithiation, the Li<sub>2</sub>S<sub>4</sub> and Li<sub>2</sub>S<sub>2</sub> intermediates were transformed to Li<sub>2</sub>S<sub>3</sub> and Li<sub>2</sub>S, respectively. During charging, the peaks referring to long-chain polysulfides were trivial. It was thus concluded that the sulfur conversion for S-GSH in LSBs is mainly based on S-S bond breakage/formation associated with the formation of short-chain LiPSs. The absence of highly soluble long-chain LiPSs has a prominent effect on immobilizing sulfur and ensuring superior cycling reversibility to conventional S/rGO counterparts. As mentioned in Section 2.3, the S<sub>3</sub><sup>-</sup> radical is essential to accelerate the Li<sub>2</sub>S precipitation, particularly under lean electrolyte conditions. By using *in situ* UV, Zou *et al.*<sup>32</sup> explored the relationship among polysulfide species, reaction pathways and the DN of solvent in LSBs. They demonstrated that the light S<sub>3</sub><sup>-</sup> radical was the main reaction intermediate in a high-DN solvent (*i.e.*, DMSO), while in a low-DN solvent (DOL : DME), S<sub>4</sub><sup>2-</sup> was a major intermediate. Through monitoring the signal changes of polysulfides in electrolytes, Zou *et al.*<sup>213</sup> proposed that large-size alkali metal cations (*i.e.*, Rb<sup>+</sup> and K<sup>+</sup>) could be more effective in stabilizing short-chain polysulfides than Na<sup>+</sup> and K<sup>+</sup>. For Mg-S batteries, the polysulfide structures and concentration evolution in a glyme-based electrolyte were surveyed by *in situ* UV-vis.<sup>214</sup> A reaction pathway was proposed with S<sub>8</sub>, S<sub>6</sub><sup>2-</sup> and S<sub>4</sub><sup>2-</sup> being present in the electrolyte as shown in Fig. 13b.

According to the change in UV-vis reflection intensity, the concentration of sulfur species can also be quantitatively analyzed, which is of importance to precisely confirm the polysulfide regulation effect.<sup>194</sup> For example, Zhou *et al.*<sup>194</sup> monitored the concentration of LiPSs on the surface of the anode side to check whether the ultra-high ion-conducting gel polymer (SHGP) electrolyte can suppress the shuttle effect. With the proceeding of the discharge process, the LiPS reflection intensity changes of LSBs assembled with poly(ethylene oxide) (PEO) and SHGP electrolytes are shown in Fig. 13c. The concentrations of soluble Li<sub>2</sub>S<sub>8</sub> and Li<sub>2</sub>S<sub>6</sub> maintained smaller values for an SHGP-assembled LSB, which indicates the effective blocking of LiPS diffusion. For RT-SSBs, soluble long-chain polysulfides would cause a shuttle effect and self-discharge, while insoluble short-chain polysulfides would slow down the reaction kinetics and passivate conductive hosts. *In situ* UV-vis analyses of an ultra-microporous carbon/small sulfur cathode showed no polysulfides during cycling, a testament to its excellent reversibility.<sup>19</sup>

In summary, *in situ* characterization techniques have been developed to provide deep insights into the phase transformation, metal polysulfide migration, and preservation of active materials with catalysts in MSBs. Apart from the representative *in situ* XRD, TEM and UV-Vis tools mentioned above, other advanced *ex situ/in situ* techniques such as Raman, FTIR, and NMR<sup>143,215</sup> have also been widely applied to explore the fundamental issues underpinning the MSB shuttle effect, for example, metal sulfide formation dynamics and the interaction of polysulfide intermediates with electrolytes and catalysts. The summary of representative *in situ/operando* characterization studies for MSBs is listed in Table 3. It is believed that a combination of various techniques offering characterized information would lead to a more integrated and insightful understanding of metal-sulfur mechanics for advanced MSBs.

## 5. Summary and perspective

In recent years, tremendous interest has been aroused to investigate MSBs as promising alternatives to conventional LIBs, due to the exceptionally high theoretical energy densities and the low cost of sulfur materials. This review is dedicated to summarizing the most recent advances in understanding sulfur conversion mechanisms and effective regulation strategies to achieve long-life and high-energy MSBs. We have initially summarized the current progress in LSBs and emphasized the Li-S reaction mechanisms and the roles of the current collectors, electrolytes and electrocatalysts in regulating the LiPS diffusion, reaction kinetics, and Li<sub>2</sub>S deposition behavior. It is unambiguous that the research community has built systemic understanding of Li-S electrochemistry with significantly improved battery performance. As a follow-up battery technology developed from Li-S, Li-free MSBs made with Na, K, Mg, Ca, and Al-metal anodes have also been summarized and explored in terms of the electrochemical reaction processes, electrode materials and challenges. It shows that the strategies developed for LSBs have also been adopted to explore the electrochemical reactions in Li-free MSBs. The polysulfide

immobilizing methods and the catalyst design to accelerate sulfur conversion kinetics, for example, have been demonstrated to be useful in both LSBs and Li-free MSBs. *In situ* characterization tools have been demonstrated as imperative and constructive for gaining insights into the complex sulfur conversion mechanisms in MSBs. Although discernible progress has been achieved so far, various fundamental challenges need to be addressed to promote the further development of MSBs. Based on the progress summarized in this review, we propose several suggestions for future studies of MSBs (Fig. 14).

### 5.1 Understanding the reaction mechanisms in MSBs

With the assistance of *in situ/ex situ* characterization techniques, we have gained comprehensive insights into Li-S reactions. However, the charge-discharge mechanisms of Li-free MSBs are still quite ambiguous. For example, there are contradictory descriptions of the first discharge step for Mg-S batteries, *i.e.*, some papers report the reduction of  $S_8$  to  $MgS_4$  (ref. 216), whereas others report  $MgS_8$  as the reduction product.<sup>217</sup> For the well-established LSB system, the studies of sulfur conversion chemistry under lean-electrolyte and high-loading conditions are very limited. The Li-S reaction processes observed under idealized conditions (*i.e.*, electrolyte/sulfur, E/S ratio  $>10 \mu\text{L mg}^{-1}$ ) would be significantly different from those under practical conditions (*i.e.*, E/S  $< 4 \mu\text{L mg}^{-1}$ ). Without

comprehensively understanding the conversion mechanisms of metal-sulfur systems, it would be puzzling and difficult to achieve rational regulation of advanced electrode materials for high-performance MSBs.

### 5.2 Suitable electrolytes for Li-free MSBs

There are few established electrolytes for the emerging Li-free MSBs. For example, the poor reversibility of Ca metal plating/stripping processes in ether electrolytes also considerably contributed to the short cycle life of a Ca-S battery.<sup>174</sup> Thus, further research should pay more attention to the exploitation of new electrolyte systems for Li-free MSBs. When developing an electrolyte, some principles or lessons should be followed, namely (i) the electrolytes should present compatibility with the sulfur species on the cathode side and the ability for reversible metal plating/stripping on the anode side. (ii) Their ability to obstruct polysulfide migration is also required to achieve desirable reversibility and thus long battery cycling life. (iii) The importance of solvents should not be underrated, given their direct influence on stable polysulfide species (*i.e.*,  $S_4^{2-}$  in DME/DOL and  $S_3^{1-}$  in DMSO) and the metal sulfide deposition morphologies.<sup>161</sup>

### 5.3 Catalyst design

Catalyst materials, particularly those with selective and bidirectional catalytic properties, have been demonstrated to

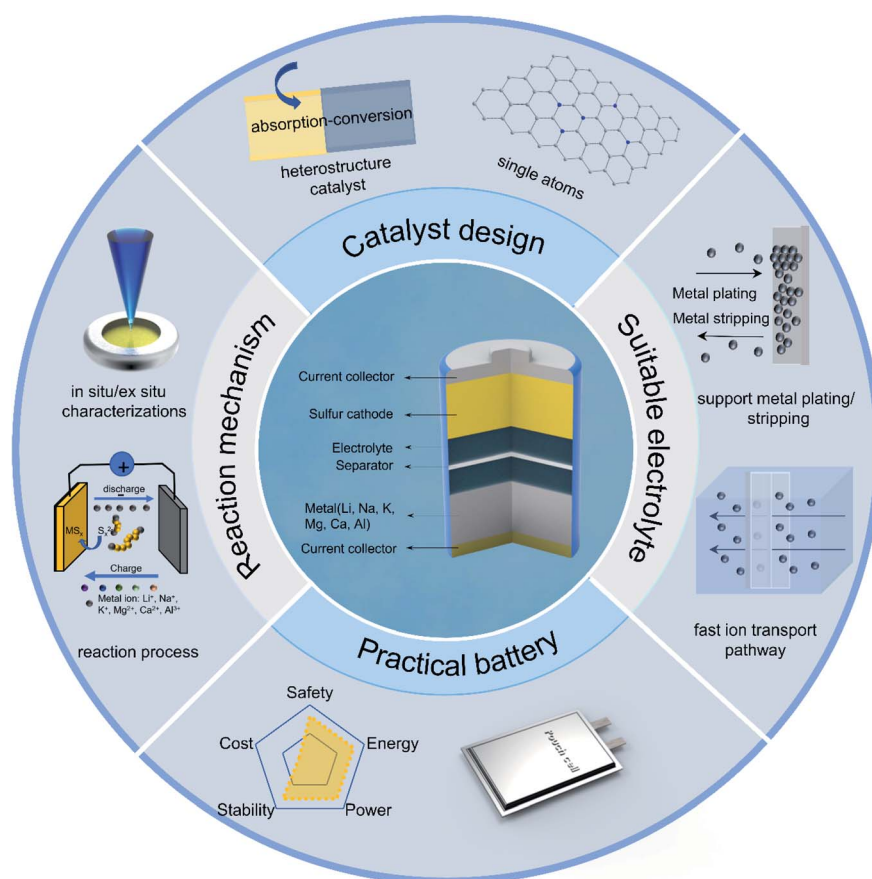


Fig. 14 The schematic illustration of the prospects of metal-sulfur batteries.

successfully regulate sulfur conversion kinetics in advanced LSBs. Catalysts can be widely employed in sulfur hosts, current collectors, and separators. Boosting the catalytic efficiency is thus critical to achieving great electrochemical performance. Separators modified with “single-atom array mimic” and ultrathin metal–organic framework (MOF) nano-sheets would immobilize the LiPS diffusion and guide dendrite-free Li metal deposition.<sup>218</sup> Some studies have also proved the effectiveness of catalysts in improving the performance of Li-free MSBs. For instance, in a K–S battery system, the operating voltage is limited to 2.4 V with K<sub>2</sub>S<sub>3</sub> formation for the CMK-3/S cathode,<sup>148</sup> whereas the charge voltage can reach 2.8 V with the final K<sub>2</sub>S product for an imidazole-solvated copper catalyst mediated cathode.<sup>153</sup> However, the functional mechanisms and structural design for catalysts in Li-free MSBs are still elusive, and thus more investigations in future studies are required. It is our belief that advances in a more fundamental understanding of the operating principles of various metal–sulfur chemistries by intensive studies in the future will definitely accelerate the implementation of MSBs in practical applications.

#### 5.4 Approach to practical MSBs

Great advances have been achieved in developing high-performance LSBs with impressive values reported in the literature, such as cycle life of 2000 cycles,<sup>209,210</sup> high rate capability at 40C,<sup>211,212</sup> or high capacities of over 1200 mA h g<sup>-1</sup>.<sup>213,214</sup> However, most of these studies were conducted using coin cell configurations with limited active materials and excessive amounts of electrolytes, which created a huge gap between the achievements in the lab and the expectations from the real world. To approach practical LSBs, several key parameters, namely a low E/S ratio, limited lithium anode and high sulfur loadings, should be emphasized in future studies.<sup>215</sup> Effective regulation of sulfur conversions will become more challenging, because of the low charge transfer kinetics, highly concentrated LiPSs and rapid failure of Li metal in practical cells. To circumvent these problems, we suggest developing powerful catalysts with high efficiency and selective and bi-directional catalytic capability to accelerate the redox kinetics and prevent LiPS accumulation in sulfur cathodes. The emerging electrolyte engineering strategies, such as highly solvating and sparingly solvating electrolyte structures, are also promising to prevent ‘dead sulfur’ formation in lean-electrolytes. Moreover, we also recommend transferring the know-how gained from dendrite-free Li metal studies to promote the LSB technology. With these guidelines and relentless efforts, Li–S technology is believed to offer its energy storage contribution to real markets in the near future. The study of Li-free MSBs is still in the infancy stage, and intensive fundamental studies are required to unveil the working mechanisms before following the success of LSBs in performance achievement.

#### Conflicts of interest

There are no conflicts to declare.

#### Acknowledgements

This work described in this paper was fully supported by grants from the Research Grants Council of the Hong Kong Special Administrative Region, China (Project No. PolyU25216121, PolyU15303219), the National Natural Science Foundation of China for Young Scholar (Project No. 52102310), and the Research Committee of the Hong Kong Polytechnic University under project codes A-PB1M, 1-BBXX and G-UAMV.

#### Notes and references

- Z. W. Seh, Y. Sun, Q. Zhang and Y. Cui, *Chem. Soc. Rev.*, 2016, **45**, 5605–5634.
- S. F. Ng, M. Y. L. Lau and W. J. Ong, *Adv. Mater.*, 2021, **33**, e2008654.
- M. Salama, Rosy, R. Attias, R. Yemini, Y. Gofer, D. Aurbach and M. Noked, *ACS Energy Lett.*, 2019, **4**, 436–446.
- S. H. Chung and A. Manthiram, *Adv. Mater.*, 2019, **31**, e1901125.
- S. Dorfler, S. Walus, J. Locke, A. Fotouhi, D. J. Auger, N. Shateri, T. Abendroth, P. Hartel, H. Althues and S. Kaskel, *Energy Technol.*, 2021, **9**, 2000694.
- X. Ji, K. T. Lee and L. F. Nazar, *Nat. Mater.*, 2009, **8**, 500–506.
- F. Shi, C. Chen and Z.-L. Xu, *Adv. Energy Mater.*, 2021, **3**, 275–301.
- H. Ye and Y. Li, *InfoMat*, 2022, e12291.
- J. Conder, R. Bouchet, S. Trabesinger, C. Marino, L. Gubler and C. Villevieille, *Nat. Energy*, 2017, **2**, 17069.
- Y. Son, J.-S. Lee, Y. Son, J.-H. Jang and J. Cho, *Adv. Energy Mater.*, 2015, **5**, 1500110.
- L. Zhang, T. Qian, X. Zhu, Z. Hu, M. Wang, L. Zhang, T. Jiang, J. H. Tian and C. Yan, *Chem. Soc. Rev.*, 2019, **48**, 5432–5453.
- Z. Wang, Y. Tang, L. Zhang, M. Li, Z. Shan and J. Huang, *Small*, 2020, **16**, e2001899.
- Z.-L. Xu, J.-Q. Huang, W. G. Chong, X. Qin, X. Wang, L. Zhou and J.-K. Kim, *Adv. Energy Mater.*, 2017, **7**, 1602078.
- H. Kim, J. T. Lee, A. Magasinski, K. Zhao, Y. Liu and G. Yushin, *Adv. Energy Mater.*, 2015, **5**, 1501306.
- H. Liu, W.-H. Lai, Y. Liang, X. Liang, Z.-C. Yan, H.-L. Yang, Y.-J. Lei, P. Wei, S. Zhou, Q.-F. Gu, S.-L. Chou, H. K. Liu, S. X. Dou and Y.-X. Wang, *J. Mater. Chem. A*, 2021, **9**, 566–574.
- W. Chen, T. Qian, J. Xiong, N. Xu, X. Liu, J. Liu, J. Zhou, X. Shen, T. Yang, Y. Chen and C. Yan, *Adv. Mater.*, 2017, **29**, 1605160.
- T. Yang, T. Qian, J. Liu, N. Xu, Y. Li, N. Grundish, C. Yan and J. B. Goodenough, *ACS Nano*, 2019, **13**, 9067–9073.
- X. Liu, T. Qian, J. Liu, J. Tian, L. Zhang and C. Yan, *Small*, 2018, **14**, e1801536.
- Q. Guo, S. Li, X. Liu, H. Lu, X. Chang, H. Zhang, X. Zhu, Q. Xia, C. Yan and H. Xia, *Adv. Sci.*, 2020, **7**, 1903246.
- S. Walus, C. Barchasz, R. Bouchet, J.-C. Leprêtre, J.-F. Colin, J.-F. Martin, E. Elkaim, C. Baetz and F. Alloin, *Adv. Energy Mater.*, 2015, **5**, 1500165.

- 21 Y. Xu, Y. Zhao, S. Zhao, J. Zhang, J. Li, J. Guo and Y. Zhang, *Energy Storage Mater.*, 2021, **42**, 513–516.
- 22 W. H. Lai, H. Wang, L. Zheng, Q. Jiang, Z. C. Yan, L. Wang, H. Yoshikawa, D. Matsumura, Q. Sun, Y. X. Wang, Q. Gu, J. Z. Wang, H. K. Liu, S. L. Chou and S. X. Dou, *Angew. Chem., Int. Ed.*, 2020, **59**, 22171–22178.
- 23 H. Yuan, H.-J. Peng, J.-Q. Huang and Q. Zhang, *Adv. Mater. Interfaces*, 2019, **6**, 1802046.
- 24 F. Qi, Z. Sun, X. Fan, Z. Wang, Y. Shi, G. Hu and F. Li, *Adv. Energy Mater.*, 2021, **11**, 2100387.
- 25 S. C. Jung and Y.-K. Han, *J. Power Sources*, 2016, **325**, 495–500.
- 26 C. Villevieille and P. Novák, *J. Mater. Chem. A*, 2013, **1**, 13089.
- 27 B. He, W.-C. Li, Y. Zhang, X.-F. Yu, B. Zhang, F. Li and A.-H. Lu, *J. Mater. Chem. A*, 2018, **6**, 24194–24200.
- 28 N. Liu, G. Zhou, A. Yang, X. Yu, F. Shi, J. Sun, J. Zhang, B. Liu, C. L. Wu, X. Tao, Y. Sun, Y. Cui and S. Chu, *Proc. Natl. Acad. Sci. U. S. A.*, 2019, **116**, 765–770.
- 29 A. Yang, G. Zhou, X. Kong, R. A. Vila, A. Pei, Y. Wu, X. Yu, X. Zheng, C. L. Wu, B. Liu, H. Chen, Y. Xu, D. Chen, Y. Li, S. Fakra, H. Y. Hwang, J. Qin, S. Chu and Y. Cui, *Nat. Nanotechnol.*, 2020, **15**, 231–237.
- 30 A. Y. Guangmin Zhou, G. Gao, X. Yu, J. Xu, C. Liu, Y. Ye, A. Pei, Y. Wu, Y. Peng, Y. Li, L. Zheng, K. Liu, L.-W. Wang and Y. Cui, *Sci. Adv.*, 2020, **6**, eaay5098.
- 31 S. S. Zhang and D. T. Tran, *J. Power Sources*, 2012, **211**, 169–172.
- 32 Q. Zou and Y. C. Lu, *J. Phys. Chem. Lett.*, 2016, **7**, 1518–1525.
- 33 Y. Liu, Y. Elias, J. Meng, D. Aurbach, R. Zou, D. Xia and Q. Pang, *Joule*, 2021, **5**, 2323–2364.
- 34 X. Yu and A. Manthiram, *Phys. Chem. Chem. Phys.*, 2015, **17**, 2127–2136.
- 35 J. Yan, X. Liu and B. Li, *Adv. Sci.*, 2016, **3**, 1600101.
- 36 F. Y. Fan, W. C. Carter and Y. M. Chiang, *Adv. Mater.*, 2015, **27**, 5203–5209.
- 37 Z.-L. Xu, N. Onofrio and J. Wang, *J. Mater. Chem. A*, 2020, **8**, 17646–17656.
- 38 G. Zeng, Y. Liu, D. Chen, C. Zhen, Y. Han and W. He, *Adv. Energy Mater.*, 2021, **11**, 2102058.
- 39 C. Luo, X. Liang, Y. Sun, W. Lv, Y. Sun, Z. Lu, W. Hua, H. Yang, R. Wang, C. Yan, J. Li, Y. Wan and Q.-H. Yang, *Energy Storage Mater.*, 2020, **33**, 290–297.
- 40 Z. L. Xu, S. Lin, N. Onofrio, L. Zhou, F. Shi, W. Lu, K. Kang, Q. Zhang and S. P. Lau, *Nat. Commun.*, 2018, **9**, 4164.
- 41 Q. Lin, L. Huang, W. Liu, Z. Li, R. Fang, D. W. Wang, Q. H. Yang and W. Lv, *Phys. Chem. Chem. Phys.*, 2021, **23**, 21385–21398.
- 42 L. Kong, J.-X. Chen, H.-J. Peng, J.-Q. Huang, W. Zhu, Q. Jin, B.-Q. Li, X.-T. Zhang and Q. Zhang, *Energy Environ. Sci.*, 2019, **12**, 2976–2982.
- 43 T. Zhang, M. Marinescu, S. Walus, P. Kovacik and G. J. Offer, *J. Electrochem. Soc.*, 2017, **165**, A6001–A6004.
- 44 Y. Yang, G. Zheng, S. Misra, J. Nelson, M. F. Toney and Y. Cui, *J. Am. Chem. Soc.*, 2012, **134**, 15387–15394.
- 45 H. Noh, J. Song, J.-K. Park and H.-T. Kim, *J. Power Sources*, 2015, **293**, 329–335.
- 46 G. Tan, R. Xu, Z. Xing, Y. Yuan, J. Lu, J. Wen, C. Liu, L. Ma, C. Zhan, Q. Liu, T. Wu, Z. Jian, R. Shahbazian-Yassar, Y. Ren, D. J. Miller, L. A. Curtiss, X. Ji and K. Amine, *Nat. Energy*, 2017, **2**, 17090.
- 47 M. R. Kaiser, Z. Han, J. Liang, S.-X. Dou and J. Wang, *Energy Storage Mater.*, 2019, **19**, 1–15.
- 48 Y. Feng, Y. Zhang, G. Du, J. Zhang, M. Liu and X. Qu, *New J. Chem.*, 2018, **42**, 13775–13783.
- 49 L. C. Gerber, P. D. Frischmann, F. Y. Fan, S. E. Doris, X. Qu, A. M. Scheuermann, K. Persson, Y. M. Chiang and B. A. Helms, *Nano Lett.*, 2016, **16**, 549–554.
- 50 C. Y. Chen, H. J. Peng, T. Z. Hou, P. Y. Zhai, B. Q. Li, C. Tang, W. Zhu, J. Q. Huang and Q. Zhang, *Adv. Mater.*, 2017, **29**, 1606802.
- 51 D.-Q. Cai, J.-L. Yang, T. Liu, S.-X. Zhao and G. Cao, *Nano Energy*, 2021, **89**, 106452.
- 52 G. Zhou, H. Tian, Y. Jin, X. Tao, B. Liu, R. Zhang, Z. W. Seh, D. Zhuo, Y. Liu, J. Sun, J. Zhao, C. Zu, D. S. Wu, Q. Zhang and Y. Cui, *Proc. Natl. Acad. Sci. U. S. A.*, 2017, **114**, 840–845.
- 53 Y.-C. Lu, Q. He and H. A. Gasteiger, *J. Phys. Chem. C*, 2014, **118**, 5733–5741.
- 54 M. Li, Y. Zhang, Z. Bai, W. W. Liu, T. Liu, J. Gim, G. Jiang, Y. Yuan, D. Luo, K. Feng, R. S. Yassar, X. Wang, Z. Chen and J. Lu, *Adv. Mater.*, 2018, **30**, e1804271.
- 55 J. Guo, Y. Huang, S. Zhao, Z. Li, Z. Wang, G. Shao and J. Liu, *ACS Nano*, 2021, **15**, 16322–16334.
- 56 H. Wang, Y. Shao, H. Pan, X. Feng, Y. Chen, Y.-S. Liu, E. D. Walter, M. H. Engelhard, K. S. Han, T. Deng, G. Ren, D. Lu, X. Lu, W. Xu, C. Wang, J. Feng, K. T. Mueller, J. Guo, K. R. Zavadil and J.-G. Zhang, *Nano Energy*, 2020, **76**, 105041.
- 57 G. Li, S. Wang, Y. Zhang, M. Li, Z. Chen and J. Lu, *Adv. Mater.*, 2018, **30**, e1705590.
- 58 Z. Li, L. Yuan, Z. Yi, Y. Sun, Y. Liu, Y. Jiang, Y. Shen, Y. Xin, Z. Zhang and Y. Huang, *Adv. Energy Mater.*, 2014, **4**, 1301473.
- 59 S. Xin, L. Gu, N. H. Zhao, Y. X. Yin, L. J. Zhou, Y. G. Guo and L. J. Wan, *J. Am. Chem. Soc.*, 2012, **134**, 18510–18513.
- 60 E. Markevich, G. Salitra, A. Rosenman, Y. Talyosef, F. Chesneau and D. Aurbach, *J. Mater. Chem. A*, 2015, **3**, 19873–19883.
- 61 R. Dominko, A. Vizintin, G. Aquilanti, L. Stievano, M. J. Helen, A. R. Munnangi, M. Fichtner and I. Arcon, *J. Electrochem. Soc.*, 2017, **165**, A5014–A5019.
- 62 X. Li, M. Banis, A. Lushington, X. Yang, Q. Sun, Y. Zhao, C. Liu, Q. Li, B. Wang, W. Xiao, C. Wang, M. Li, J. Liang, R. Li, Y. Hu, L. Goncharova, H. Zhang, T. K. Sham and X. Sun, *Nat. Commun.*, 2018, **9**, 4509.
- 63 X. Zhang, K. Chen, Z. Sun, G. Hu, R. Xiao, H.-M. Cheng and F. Li, *Energy Environ. Sci.*, 2020, **13**, 1076–1095.
- 64 W. J. Chung, J. J. Griebel, E. T. Kim, H. Yoon, A. G. Simmonds, H. J. Ji, P. T. Dirlam, R. S. Glass, J. J. Wie, N. A. Nguyen, B. W. Guralnick, J. Park, A. Somogyi, P. Theato, M. E. Mackay, Y. E. Sung, K. Char and J. Pyun, *Nat. Chem.*, 2013, **5**, 518–524.
- 65 G. Hu, Z. Sun, C. Shi, R. Fang, J. Chen, P. Hou, C. Liu, H. M. Cheng and F. Li, *Adv. Mater.*, 2017, **29**, 1603835.

- 66 H. Kim, J. Lee, H. Ahn, O. Kim and M. J. Park, *Nat. Commun.*, 2015, **6**, 7278.
- 67 H. Zhou, F. Yu, M. Wei, Y. Su, Y. Ma, D. Wang and Q. Shen, *Chem. Commun.*, 2019, **55**, 3729–3732.
- 68 Z. Shadik, H. S. Lee, C. Tian, K. Sun, L. Song, E. Hu, I. Waluyo, A. Hunt, S. Ghose, Y. Hu, J. Zhou, J. Wang, P. Northrup, S. M. Bak and X. Q. Yang, *Adv. Energy Mater.*, 2019, **9**, 1900705.
- 69 X. Zhang, G. Hu, K. Chen, L. Shen, R. Xiao, P. Tang, C. Yan, H.-M. Cheng, Z. Sun and F. Li, *Energy Storage Mater.*, 2022, **45**, 1144–1152.
- 70 Z. Pan, D. J. L. Brett, G. He and I. P. Parkin, *Adv. Energy Mater.*, 2022, 2103483.
- 71 S. Zhang, *Energies*, 2014, **7**, 4588–4600.
- 72 X. Chen, L. Peng, L. Wang, J. Yang, Z. Hao, J. Xiang, K. Yuan, Y. Huang, B. Shan, L. Yuan and J. Xie, *Nat. Commun.*, 2019, **10**, 1021.
- 73 X. Wang, Y. Qian, L. Wang, H. Yang, H. Li, Y. Zhao and T. Liu, *Adv. Funct. Mater.*, 2019, **29**, 1902929.
- 74 A. Bhargava, M. E. Bell, J. Karty, Y. Cui and Y. Fu, *ACS Appl. Mater. Interfaces*, 2018, **10**, 21084–21090.
- 75 H. Ye, L. Ma, Y. Zhou, L. Wang, N. Han, F. Zhao, J. Deng, T. Wu, Y. Li and J. Lu, *Proc. Natl. Acad. Sci. U. S. A.*, 2017, **114**, 13091–13096.
- 76 B. He, D. Liu, Z. Cheng, Z. Miao, Z. Rao, H. Zhang, L. Yuan, Z. Li and Y. Huang, *Adv. Energy Mater.*, 2021, **12**, 2102832.
- 77 H. Du, S. Feng, W. Luo, L. Zhou and L. Mai, *J. Mater. Sci. Technol.*, 2020, **55**, 1–15.
- 78 P. Zhu, D. Gastol, J. Marshall, R. Sommerville, V. Goodship and E. Kendrick, *J. Power Sources*, 2021, **485**, 229321.
- 79 W. Yang, R. Huang, Z. Ni, H. Cheng, S. Zhou, Y. Wang, X. Li, Y. Zhang and Y. Zhang, *Ionics*, 2022, **28**, 1713–1738.
- 80 I. Raguzin, S. Choudhury, F. Simon, M. Stamm and L. Ionov, *Adv. Mater. Interfaces*, 2017, **4**, 1600811.
- 81 A. Benitez, F. Luna-Lama, A. Caballero, E. Rodríguez-Castellón and J. Morales, *J. Energy Chem.*, 2021, **62**, 295–306.
- 82 H.-J. Peng, W.-T. Xu, L. Zhu, D.-W. Wang, J.-Q. Huang, X.-B. Cheng, Z. Yuan, F. Wei and Q. Zhang, *Adv. Funct. Mater.*, 2016, **26**, 6351–6358.
- 83 Y. Hu, W. Chen, T. Lei, Y. Jiao, J. Huang, A. Hu, C. Gong, C. Yan, X. Wang and J. Xiong, *Adv. Energy Mater.*, 2020, **10**, 2000082.
- 84 Y. Wang, J. Huang, X. Chen, L. Wang and Z. Ye, *Carbon*, 2018, **137**, 368–378.
- 85 Q. Zhao, Q. Zhu, J. Miao, Z. Guan, H. Liu, R. Chen, Y. An, F. Wu and B. Xu, *ACS Appl. Mater. Interfaces*, 2018, **10**, 10882–10889.
- 86 L. Kong, H.-J. Peng, J.-Q. Huang and Q. Zhang, *Nano Res.*, 2017, **10**, 4027–4054.
- 87 C. Shang, L. Cao, M. Yang, Z. Wang, M. Li, G. Zhou, X. Wang and Z. Lu, *Energy Storage Mater.*, 2019, **18**, 375–381.
- 88 K. Zhang, K. Xie, K. Yuan, W. Lu, S. Hu, W. Wei, M. Bai and C. Shen, *J. Mater. Chem. A*, 2017, **5**, 7309–7315.
- 89 D. Fang, Y. Wang, C. Qian, X. Liu, X. Wang, S. Chen and S. Zhang, *Adv. Funct. Mater.*, 2019, **29**, 1900875.
- 90 G. Zhou, A. Yang, Y. Wang, G. Gao, A. Pei, X. Yu, Y. Zhu, L. Zong, B. Liu, J. Xu, N. Liu, J. Zhang, Y. Li, L. W. Wang, H. Y. Hwang, M. L. Brongersma, S. Chu and Y. Cui, *Nat. Commun.*, 2020, **11**, 606.
- 91 X. Tang, Z. Xu, Z. Sun, J. Zhou, X. Wu, H. Lin, J. Rong, S. Zhuo and F. Li, *Energy Technol.*, 2019, **7**, 1900574.
- 92 X. Ji, S. Evers, R. Black and L. F. Nazar, *Nat. Commun.*, 2011, **2**, 325.
- 93 Z.-L. Xu, S. J. Kim, D. Chang, K.-Y. Park, K. S. Dae, K. P. Dao, J. M. Yuk and K. Kang, *Energy Environ. Sci.*, 2019, **12**, 3144–3155.
- 94 L. Hu, C. Dai, H. Liu, Y. Li, B. Shen, Y. Chen, S.-J. Bao and M. Xu, *Adv. Energy Mater.*, 2018, **8**, 1800709.
- 95 N. Wang, B. Chen, K. Qin, E. Liu, C. Shi, C. He and N. Zhao, *Nano Energy*, 2019, **60**, 332–339.
- 96 M. Yu, S. Zhou, Z. Wang, Y. Wang, N. Zhang, S. Wang, J. Zhao and J. Qiu, *Energy Storage Mater.*, 2019, **20**, 98–107.
- 97 H. Wang, W. Zhang, J. Xu and Z. Guo, *Adv. Funct. Mater.*, 2018, **28**, 1707520.
- 98 J. Sun, Y. Sun, M. Pasta, G. Zhou, Y. Li, W. Liu, F. Xiong and Y. Cui, *Adv. Mater.*, 2016, **28**, 9797–9803.
- 99 L. Li, L. Chen, S. Mukherjee, J. Gao, H. Sun, Z. Liu, X. Ma, T. Gupta, C. V. Singh, W. Ren, H. M. Cheng and N. Koratkar, *Adv. Mater.*, 2017, **29**, 1602734.
- 100 T. Zhou, W. Lv, J. Li, G. Zhou, Y. Zhao, S. Fan, B. Liu, B. Li, F. Kang and Q.-H. Yang, *Energy Environ. Sci.*, 2017, **10**, 1694–1703.
- 101 F. Wang, J. Li, J. Zhao, Y. Yang, C. Su, Y. L. Zhong, Q.-H. Yang and J. Lu, *ACS Mater. Lett.*, 2020, **2**, 1450–1463.
- 102 Z. Du, X. Chen, W. Hu, C. Chuang, S. Xie, A. Hu, W. Yan, X. Kong, X. Wu, H. Ji and L. J. Wan, *J. Am. Chem. Soc.*, 2019, **141**, 3977–3985.
- 103 Y. Liu, W. Kou, X. Li, C. Huang, R. Shui and G. He, *Small*, 2019, **15**, e1902431.
- 104 R. Wang, C. Luo, T. Wang, G. Zhou, Y. Deng, Y. He, Q. Zhang, F. Kang, W. Lv and Q. H. Yang, *Adv. Mater.*, 2020, **32**, e2000315.
- 105 W. Hua, H. Li, C. Pei, J. Xia, Y. Sun, C. Zhang, W. Lv, Y. Tao, Y. Jiao, B. Zhang, S. Z. Qiao, Y. Wan and Q. H. Yang, *Adv. Mater.*, 2021, **33**, 2101006.
- 106 H. Li, C. Chen, Y. Yan, T. Yan, C. Cheng, D. Sun and L. Zhang, *Adv. Mater.*, 2021, **33**, e2105067.
- 107 G. Zhang, H. J. Peng, C. Z. Zhao, X. Chen, L. D. Zhao, P. Li, J. Q. Huang and Q. Zhang, *Angew. Chem., Int. Ed.*, 2018, **57**, 16732–16736.
- 108 M. Zhao, B. Q. Li, H. J. Peng, H. Yuan, J. Y. Wei and J. Q. Huang, *Angew. Chem., Int. Ed.*, 2020, **59**, 12636–12652.
- 109 Q. Cheng, W. Xu, S. Qin, S. Das, T. Jin, A. Li, A. C. Li, B. Qie, P. Yao, H. Zhai, C. Shi, X. Yong and Y. Yang, *Angew. Chem., Int. Ed.*, 2019, **58**, 5557–5561.
- 110 M. Cuisinier, C. Hart, M. Balasubramanian, A. Garsuch and L. F. Nazar, *Adv. Energy Mater.*, 2015, **5**, 1401801.
- 111 H. Pan, J. Chen, R. Cao, V. Murugesan, N. N. Rajput, K. S. Han, K. Persson, L. Estevez, M. H. Engelhard, J.-G. Zhang, K. T. Mueller, Y. Cui, Y. Shao and J. Liu, *Nat. Energy*, 2017, **2**, 813–820.
- 112 Z. Li, Y. Zhou, Y. Wang and Y.-C. Lu, *Adv. Energy Mater.*, 2019, **9**, 1802207.

- 113 H. Chu, H. Noh, Y. J. Kim, S. Yuk, J. H. Lee, J. Lee, H. Kwack, Y. Kim, D. K. Yang and H. T. Kim, *Nat. Commun.*, 2019, **10**, 188.
- 114 L. Suo, Y. S. Hu, H. Li, M. Armand and L. Chen, *Nat. Commun.*, 2013, **4**, 1481.
- 115 J. Li, L. Zhang, F. Qin, B. Hong, Q. Xiang, K. Zhang, J. Fang and Y. Lai, *J. Power Sources*, 2019, **442**, 227232.
- 116 Z. Shi, L. Wang, H. Xu, J. Wei, H. Yue, H. Dong, Y. Yin and S. Yang, *Chem. Commun.*, 2019, **55**, 12056–12059.
- 117 F. Pei, S. Dai, B. Guo, H. Xie, C. Zhao, J. Cui, X. Fang, C. Chen and N. Zheng, *Energy Environ. Sci.*, 2021, **14**, 975–985.
- 118 R. Fang, H. Xu, B. Xu, X. Li, Y. Li and J. B. Goodenough, *Adv. Funct. Mater.*, 2020, **31**, 2001812.
- 119 P. Chiochan, X. Yu, M. Sawangphruk and A. Manthiram, *Adv. Energy Mater.*, 2020, **10**, 2001285.
- 120 R. Fang, B. Xu, N. S. Grundish, Y. Xia, Y. Li, C. Lu, Y. Liu, N. Wu and J. B. Goodenough, *Angew. Chem., Int. Ed.*, 2021, **60**, 17701–17706.
- 121 R.-c. Xu, X.-h. Xia, X.-l. Wang, Y. Xia and J.-p. Tu, *J. Mater. Chem. A*, 2017, **5**, 2829–2834.
- 122 Z. Wei, Y. Ren, J. Sokolowski, X. Zhu and G. Wu, *InfoMat*, 2020, **2**, 483–508.
- 123 X. J. Hong, C. L. Song, Y. Yang, H. C. Tan, G. H. Li, Y. P. Cai and H. Wang, *ACS Nano*, 2019, **13**, 1923–1931.
- 124 Y. Li, T. Gao, D. Ni, Y. Zhou, M. Yousaf, Z. Guo, J. Zhou, P. Zhou, Q. Wang and S. Guo, *Adv. Mater.*, 2022, **34**, e2107638.
- 125 N. Li, W. Cao, Y. Liu, H. Ye and K. Han, *Colloids Surf., A*, 2019, **573**, 128–136.
- 126 H. Yang, H. Li, J. Li, Z. Sun, K. He, H. M. Cheng and F. Li, *Angew. Chem., Int. Ed.*, 2019, **58**, 11978–11996.
- 127 X. Xu, D. Zhou, X. Qin, K. Lin, F. Kang, B. Li, D. Shanmukaraj, T. Rojo, M. Armand and G. Wang, *Nat. Commun.*, 2018, **9**, 3870.
- 128 K. B. Hueso, M. Armand and T. Rojo, *Energy Environ. Sci.*, 2013, **6**, 734–749.
- 129 Y. X. Wang, B. Zhang, W. Lai, Y. Xu, S. L. Chou, H. K. Liu and S. X. Dou, *Adv. Energy Mater.*, 2017, **7**, 1602829.
- 130 B. W. Zhang, T. Sheng, Y. X. Wang, S. Chou, K. Davey, S. X. Dou and S. Z. Qiao, *Angew. Chem., Int. Ed.*, 2019, **58**, 1484–1488.
- 131 D. Liu, Z. Li, X. Li, Z. Cheng, L. Yuan and Y. Huang, *ChemPhysChem*, 2019, **20**, 3164–3176.
- 132 X. Yu and A. Manthiram, *ChemElectroChem*, 2014, **1**, 1275–1280.
- 133 Y. Wang, Y. Zhang, H. Cheng, Z. Ni, Y. Wang, G. Xia, X. Li and X. Zeng, *Molecules*, 2021, **26**, 1535.
- 134 A. Y. S. Eng, V. Kumar, Y. Zhang, J. Luo, W. Wang, Y. Sun, W. Li and Z. W. Seh, *Adv. Energy Mater.*, 2021, **11**, 2003493.
- 135 Y. X. Wang, J. Yang, W. Lai, S. L. Chou, Q. F. Gu, H. K. Liu, D. Zhao and S. X. Dou, *J. Am. Chem. Soc.*, 2016, **138**, 16576–16579.
- 136 F. Xiao, X. Yang, H. Wang, J. Xu, Y. Liu, D. Y. W. Yu and A. L. Rogach, *Adv. Energy Mater.*, 2020, **10**, 2000931.
- 137 Z. Yang, R. Xiao, X. Zhang, X. Wang, D. Zhang, Z. Sun and F. Li, *Energy Environ. Sci.*, 2021, 1–18.
- 138 S. Xin, Y. X. Yin, Y. G. Guo and L. J. Wan, *Adv. Mater.*, 2014, **26**, 1261–1265.
- 139 H. Kim, M. K. Sadan, C. Kim, J. Jo, M. Seong, K.-K. Cho, K.-W. Kim, J.-H. Ahn and H.-J. Ahn, *Chem. Eng. J.*, 2021, **426**, 130787.
- 140 S. Li, Y. Han, P. Ge and Y. Yang, *ChemPlusChem*, 2021, **86**, 1461–1471.
- 141 H. Liu, W. Pei, W. H. Lai, Z. Yan, H. Yang, Y. Lei, Y. X. Wang, Q. Gu, S. Zhou, S. Chou, H. K. Liu and S. X. Dou, *ACS Nano*, 2020, **14**, 7259–7268.
- 142 X. L. Huang, S. X. Dou and Z. M. Wang, *Mater. Horiz.*, 2021, **8**, 2870–2885.
- 143 B. Guo, W. Du, T. Yang, J. Deng, D. Liu, Y. Qi, J. Jiang, S. J. Bao and M. Xu, *Adv. Sci.*, 2020, **7**, 1902617.
- 144 Z. Yan, Y. Liang, J. Xiao, W. Lai, W. Wang, Q. Xia, Y. Wang, Q. Gu, H. Lu, S. L. Chou, Y. Liu, H. Liu and S. X. Dou, *Adv. Mater.*, 2020, **32**, e1906700.
- 145 S. Gu, N. Xiao, F. Wu, Y. Bai, C. Wu and Y. Wu, *ACS Energy Lett.*, 2018, **3**, 2858–2864.
- 146 J. Ding, H. Zhang, W. Fan, C. Zhong, W. Hu and D. Mitlin, *Adv. Mater.*, 2020, **32**, 1908007.
- 147 X. Yu and A. Manthiram, *Energy Storage Mater.*, 2018, **15**, 368–373.
- 148 Q. Zhao, Y. Hu, K. Zhang and J. Chen, *Inorg. Chem.*, 2014, **53**, 9000–9005.
- 149 J.-Y. Hwang, H. M. Kim and Y.-K. Sun, *J. Mater. Chem. A*, 2018, **6**, 14587–14593.
- 150 X. Lu, M. E. Bowden, V. L. Sprenkle and J. Liu, *Adv. Mater.*, 2015, **27**, 5915–5922.
- 151 P. Xiong, X. Han, X. Zhao, P. Bai, Y. Liu, J. Sun and Y. Xu, *ACS Nano*, 2019, **13**, 2536–2543.
- 152 L. Wang, J. Bao, Q. Liu and C.-F. Sun, *Energy Storage Mater.*, 2019, **18**, 470–475.
- 153 N.-C. Lai, G. Cong and Y.-C. Lu, *J. Mater. Chem. A*, 2019, **7**, 20584–20589.
- 154 X. Ge, H. Di, P. Wang, X. Miao, P. Zhang, H. Wang, J. Ma and L. Yin, *ACS Nano*, 2020, **14**, 16022–16035.
- 155 Y. Lu, C. Wang, Q. Liu, X. Li, X. Zhao and Z. Guo, *Small Methods*, 2021, **5**, e2001303.
- 156 H. S. Kim, T. S. Arthur, G. D. Allred, J. Zajicek, J. G. Newman, A. E. Rodnyansky, A. G. Oliver, W. C. Boggess and J. Muldoon, *Nat. Commun.*, 2011, **2**, 427.
- 157 Z. Zhao-Karger, X. Zhao, D. Wang, T. Diemant, R. J. Behm and M. Fichtner, *Adv. Energy Mater.*, 2015, **5**, 1401155.
- 158 J. Zhu, J. Zou, H. Cheng, Y. Gu and Z. Lu, *Green Energy Environ.*, 2019, **4**, 345–359.
- 159 T. Gao, X. Ji, S. Hou, X. Fan, X. Li, C. Yang, F. Han, F. Wang, J. Jiang, K. Xu and C. Wang, *Adv. Mater.*, 2018, **30**, 1704313.
- 160 G. Bieker, J. Wellmann, M. Kolek, K. Jalkanen, M. Winter and P. Bieker, *Phys. Chem. Chem. Phys.*, 2017, **19**, 11152–11162.
- 161 Q. Zou, Y. Sun, Z. Liang, W. Wang and Y. C. Lu, *Adv. Energy Mater.*, 2021, **11**, 2101552.
- 162 T. Gao, S. Hou, F. Wang, Z. Ma, X. Li, K. Xu and C. Wang, *Angew. Chem.*, 2017, **129**, 13711–13715.
- 163 Z. Zhao-Karger, M. E. Gil Bardaji, O. Fuhr and M. Fichtner, *J. Mater. Chem. A*, 2017, **5**, 10815–10820.

- 164 T. Gao, M. Noked, A. J. Pearse, E. Gillette, X. Fan, Y. Zhu, C. Luo, L. Suo, M. A. Schroeder, K. Xu, S. B. Lee, G. W. Rubloff and C. Wang, *J. Am. Chem. Soc.*, 2015, **137**, 12388–12393.
- 165 W. Li, S. Cheng, J. Wang, Y. Qiu, Z. Zheng, H. Lin, S. Nanda, Q. Ma, Y. Xu and F. Ye, *Angew. Chem., Int. Ed.*, 2016, **128**, 6516–6520.
- 166 A. Du, Z. Zhang, H. Qu, Z. Cui, L. Qiao, L. Wang, J. Chai, T. Lu, S. Dong, T. Dong, H. Xu, X. Zhou and G. Cui, *Energy Environ. Sci.*, 2017, **10**, 2616–2625.
- 167 J. Häcker, C. Danner, B. Sievert, I. Biswas, Z. Zhao-Karger, N. Wagner and K. A. Friedrich, *Electrochim. Acta*, 2020, **338**, 135787.
- 168 W. Wang, H. Yuan, Y. NuLi, J. Zhou, J. Yang and J. Wang, *J. Phys. Chem. C*, 2018, **122**, 26764–26776.
- 169 X. Zhou, J. Tian, J. Hu and C. Li, *Adv. Mater.*, 2018, **30**, 1704166.
- 170 Z. Zhao-Karger, R. Liu, W. Dai, Z. Li, T. Diemant, B. P. Vinayan, C. Bonatto Minella, X. Yu, A. Manthiram, R. J. Behm, M. Ruben and M. Fichtner, *ACS Energy Lett.*, 2018, **3**, 2005–2013.
- 171 A. Scafuri, R. Berthelot, K. Pirnat, A. Vizintin, J. Bitenc, G. Aquilanti, D. Foix, R. Dedryvère, I. Arçon, R. Dominko and L. Stievano, *Chem. Mater.*, 2020, **32**, 8266–8275.
- 172 Z. L. Xu, J. Park, J. Wang, H. Moon, G. Yoon, J. Lim, Y. J. Ko, S. P. Cho, S. Y. Lee and K. Kang, *Nat. Commun.*, 2021, **12**, 3369.
- 173 X. Yu, M. J. Boyer, G. S. Hwang and A. Manthiram, *Adv. Energy Mater.*, 2019, **9**, 1803794.
- 174 Z. Li, B. P. Vinayan, T. Diemant, R. J. Behm, M. Fichtner and Z. Zhao-Karger, *Small*, 2020, **16**, e2001806.
- 175 G. Mamantov and R. Marassi, *US Pat.*, 4063005, 1997.
- 176 D. Peramunage, R. Dillon and S. Licht, *J. Power Sources*, 1993, **45**, 311–323.
- 177 T. Gao, X. Li, X. Wang, J. Hu, F. Han, X. Fan, L. Suo, A. J. Pearse, S. B. Lee, G. W. Rubloff, K. J. Gaskell, M. Noked and C. Wang, *Angew. Chem., Int. Ed.*, 2016, **55**, 9898–9901.
- 178 H. Li, R. Meng, Y. Guo, B. Chen, Y. Jiao, C. Ye, Y. Long, A. Tadich, Q. H. Yang, M. Jaroniec and S. Z. Qiao, *Nat. Commun.*, 2021, **12**, 5714.
- 179 X. Yu and A. Manthiram, *Adv. Energy Mater.*, 2017, **7**, 1700561.
- 180 W. Wang, Z. Cao, G. A. Elia, Y. Wu, W. Wahyudi, E. Abou-Hamad, A.-H. Emwas, L. Cavallo, L.-J. Li and J. Ming, *ACS Energy Lett.*, 2018, **3**, 2899–2907.
- 181 K. Zhang, T. H. Lee, J. H. Cha, R. S. Varma, J. W. Choi, H. W. Jang and M. Shokouhimehr, *Sci. Rep.*, 2019, **9**, 13573.
- 182 J. Lampkin, H. Li, L. Furness, R. Raccichini and N. Garcia-Araez, *ChemSusChem*, 2020, **13**, 3514–3523.
- 183 X. Xiao, J. Tu, Z. Huang and S. Jiao, *Phys. Chem. Chem. Phys.*, 2021, **23**, 10326–10334.
- 184 X. Zheng, R. Tang, Y. Zhang, L. Ma, X. Wang, Y. Dong, G. Kong and L. Wei, *Sustainable Energy Fuels*, 2020, **4**, 1630–1641.
- 185 Sungjemmenla, C. B. Soni and V. Kumar, *Nanoscale Adv.*, 2021, **3**, 1569–1581.
- 186 Y. Guo, H. Jin, Z. Qi, Z. Hu, H. Ji and L.-J. Wan, *Adv. Funct. Mater.*, 2019, **29**, 1807676.
- 187 X. Yu, M. J. Boyer, G. S. Hwang and A. Manthiram, *Chem*, 2018, **4**, 586–598.
- 188 H. Yang, L. Yin, J. Liang, Z. Sun, Y. Wang, H. Li, K. He, L. Ma, Z. Peng, S. Qiu, C. Sun, H. M. Cheng and F. Li, *Angew. Chem., Int. Ed.*, 2018, **57**, 1898–1902.
- 189 W. Tang, Z. Chen, B. Tian, H. W. Lee, X. Zhao, X. Fan, Y. Fan, K. Leng, C. Peng, M. H. Kim, M. Li, M. Lin, J. Su, J. Chen, H. Y. Jeong, X. Yin, Q. Zhang, W. Zhou, K. P. Loh and G. W. Zheng, *J. Am. Chem. Soc.*, 2017, **139**, 10133–10141.
- 190 Y. Hwa, H. K. Seo, J. M. Yuk and E. J. Cairns, *Nano Lett.*, 2017, **17**, 7086–7094.
- 191 Y. Li, Y. Tang, X. Li, W. Tu, L. Zhang and J. Huang, *Small*, 2021, **17**, e2100846.
- 192 X. Ding, S. Yang, S. Zhou, Y. Zhan, Y. Lai, X. Zhou, X. Xu, H. Nie, S. Huang and Z. Yang, *Adv. Funct. Mater.*, 2020, **30**, 2003354.
- 193 N. Xu, T. Qian, X. Liu, J. Liu, Y. Chen and C. Yan, *Nano Lett.*, 2017, **17**, 538–543.
- 194 J. Zhou, H. Ji, J. Liu, T. Qian and C. Yan, *Energy Storage Mater.*, 2019, **22**, 256–264.
- 195 J. Liu, T. Qian, M. Wang, X. Liu, N. Xu, Y. You and C. Yan, *Nano Lett.*, 2017, **17**, 5064–5070.
- 196 V. Celorrio, A. S. Leach, H. Huang, S. Hayama, A. Freeman, D. W. Inwood, D. J. Fermin and A. E. Russell, *ACS Catal.*, 2021, **11**, 6431–6439.
- 197 N. V. Srinath, A. Longo, H. Poelman, R. K. Ramachandran, J.-Y. Feng, J. Dendooven, M.-F. Reyniers and V. V. Galvita, *ACS Catal.*, 2021, **11**, 11320–11335.
- 198 Y. Xu, Y. Ye, S. Zhao, J. Feng, J. Li, H. Chen, A. Yang, F. Shi, L. Jia, Y. Wu, X. Yu, P. A. Glans-Suzuki, Y. Cui, J. Guo and Y. Zhang, *Nano Lett.*, 2019, **19**, 2928–2934.
- 199 C. Wu, Y. Lei, L. Simonelli, D. Tonti, A. Black, X. Lu, W. H. Lai, X. Cai, Y. X. Wang, Q. Gu, S. L. Chou, H. K. Liu, G. Wang and S. X. Dou, *Adv. Mater.*, 2022, **34**, e2108363.
- 200 E. Zhao, K. Nie, X. Yu, Y. S. Hu, F. Wang, J. Xiao, H. Li and X. Huang, *Adv. Funct. Mater.*, 2018, **28**, 1707543.
- 201 C. Ye, Y. Jiao, D. Chao, T. Ling, J. Shan, B. Zhang, Q. Gu, K. Davey, H. Wang and S. Z. Qiao, *Adv. Mater.*, 2020, **32**, e1907557.
- 202 Z. Yan, J. Xiao, W. Lai, L. Wang, F. Gebert, Y. Wang, Q. Gu, H. Liu, S. L. Chou, H. Liu and S. X. Dou, *Nat. Commun.*, 2019, **10**, 4793.
- 203 C. Ma, Y. Zhang, Y. Feng, N. Wang, L. Zhou, C. Liang, L. Chen, Y. Lai, X. Ji, C. Yan and W. Wei, *Adv. Mater.*, 2021, **33**, e2100171.
- 204 H. Ci, J. Cai, H. Ma, Z. Shi, G. Cui, M. Wang, J. Jin, N. Wei, C. Lu, W. Zhao, J. Sun and Z. Liu, *ACS Nano*, 2020, **14**, 11929–11938.
- 205 C. Ye, J. Yan, H. Jin, A. D. Slattery, K. Davey, H. Wang and S.-Z. Qiao, *Angew. Chem., Int. Ed.*, 2018, **57**, 16703–16707.
- 206 J. Qian, F. Wang, Y. Li, S. Wang, Y. Zhao, W. Li, Y. Xing, L. Deng, Q. Sun, L. Li, F. Wu and R. Chen, *Adv. Funct. Mater.*, 2020, **30**, 2000742.

- 207 J. He, A. Bhargav and A. Manthiram, *Adv. Mater.*, 2020, **32**, e2004741.
- 208 S. Zhang, Y. Yao, X. Jiao, M. Ma, H. Huang, X. Zhou, L. Wang, J. Bai and Y. Yu, *Adv. Mater.*, 2021, **33**, e2103846.
- 209 L. Wang, Z.-Y. Wang, J.-F. Wu, G.-R. Li, S. Liu and X.-P. Gao, *Nano Energy*, 2020, **77**, 105173.
- 210 X.-C. Liu, Y. Yang, J. Wu, M. Liu, S. P. Zhou, B. D. A. Levin, X.-D. Zhou, H. Cong, D. A. Muller, P. M. Ajayan, H. D. Abruña and F.-S. Ke, *ACS Energy Lett.*, 2018, **3**, 1325–1330.
- 211 Z. Wang, Y. Tang, X. Fu, J. Wang, Z. Peng, L. Zhang and J. Huang, *ACS Appl. Mater. Interfaces*, 2020, **12**, 55971–55981.
- 212 J. H. Tian, T. Jiang, M. Wang, Z. Hu, X. Zhu, L. Zhang, T. Qian and C. Yan, *Small Methods*, 2019, **4**, 1900467.
- 213 Q. Zou, Z. Liang, G. Y. Du, C. Y. Liu, E. Y. Li and Y. C. Lu, *J. Am. Chem. Soc.*, 2018, **140**, 10740–10748.
- 214 J. Häcker, D. H. Nguyen, T. Rommel, Z. Zhao-Karger, N. Wagner and K. A. Friedrich, *ACS Energy Lett.*, 2021, **7**, 1–9.
- 215 D. Zhang, X. Zhang, B. Wang, S. He, S. Liu, M. Tang and H. Yu, *J. Mater. Chem. A*, 2021, **9**, 8966–8974.
- 216 Z. Zhao-Karger, X. Zhao, D. Wang, T. Diemant, R. J. Behm and M. Fichtner, *Adv. Energy Mater.*, 2015, **5**, 401155.
- 217 P. Wang, K. Küster, U. Starke, C. Liang, R. Niewa and M. R. Buchmeiser, *J. Power Sources*, 2021, **515**, 230604.
- 218 Y. Li, S. Lin, D. Wang, T. Gao, J. Song, P. Zhou, Z. Xu, Z. Yang, N. Xiao and S. Guo, *Adv. Mater.*, 2020, **32**, e1906722.
- 219 A. Robba, A. Vizintin, J. Bitenc, G. Mali, I. Arçon, M. Kavčič, M. Žitnik, K. Bučar, G. Aquilanti, C. Martineau-Corcoss, A. Randon-Vitanova and R. Dominko, *Chem. Mater.*, 2017, **29**, 9555–9564.
- 220 C. Zech, P. Hönicke, Y. Kayser, S. Risse, O. Grätz, M. Stamm and B. Beckhoff, *J. Mater. Chem. A*, 2021, **9**, 10231–10239.
- 221 Q. Pang, D. Kundu, M. Cuisinier and L. F. Nazar, *Nat. Commun.*, 2014, **5**, 4759.
- 222 X. Yang, X. Gao, Q. Sun, S. P. Jand, Y. Yu, Y. Zhao, X. Li, K. Adair, L. Y. Kuo, J. Rohrer, J. Liang, X. Lin, M. N. Banis, Y. Hu, H. Zhang, X. Li, R. Li, H. Zhang, P. Kaghazchi, T. K. Sham and X. Sun, *Adv. Mater.*, 2019, **31**, e1901220.
- 223 C. Zha, D. Wu, X. Gu and H. Chen, *J. Energy Chem.*, 2021, **59**, 599–607.
- 224 A. Benayad, J. E. Morales-Ugarte, C. C. Santini and R. Bouchet, *J. Phys. Chem. A*, 2021, **125**, 1069–1081.
- 225 M. I. Nandasiri, L. E. Camacho-Forero, A. M. Schwarz, V. Shutthanandan, S. Thevuthasan, P. B. Balbuena, K. T. Mueller and V. Murugesan, *Chem. Mater.*, 2017, **29**, 4728–4737.
- 226 Y. Zhang, S. Yang, S. Zhou, L. Zhang, B. Gu, Y. Dong, S. Kong, D. Cai, G. Fang, H. Nie and Z. Yang, *Chem. Commun.*, 2021, **57**, 3255–3258.
- 227 B. W. Zhang, T. Sheng, Y. D. Liu, Y. X. Wang, L. Zhang, W. H. Lai, L. Wang, J. Yang, Q. F. Gu, S. L. Chou, H. K. Liu and S. X. Dou, *Nat. Commun.*, 2018, **9**, 4082.
- 228 Q. Yang, T. Yang, W. Gao, Y. Qi, B. Guo, W. Zhong, J. Jiang and M. Xu, *Inorg. Chem. Front.*, 2020, **7**, 4396–4403.
- 229 A. Kumar, A. Ghosh, M. Forsyth, D. R. MacFarlane and S. Mitra, *ACS Energy Lett.*, 2020, **5**, 2112–2121.
- 230 R. K. Bhardwaj, S. Jayanthi, P. S. Adarakatti, A. K. Sood and A. J. Bhattacharyya, *ACS Appl. Mater. Interfaces*, 2020, **12**, 28120–28128.
- 231 R. K. Bhardwaj, R. Gomes and A. J. Bhattacharyya, *J. Phys. Chem. Lett.*, 2022, **13**, 1159–1164.
- 232 J. Wang, S. Cheng, W. Li, L. Jia, Q. Xiao, Y. Hou, Z. Zheng, H. Li, S. Zhang, L. Zhou, M. Liu, H. Lin and Y. Zhang, *Nano Energy*, 2017, **40**, 390–398.
- 233 C. Dillard, A. Singh and V. Kalra, *J. Phys. Chem. C*, 2018, **122**, 18195–18203.
- 234 N. Saqib, G. M. Ohlhausen and J. M. Porter, *J. Power Sources*, 2017, **364**, 266–271.
- 235 X.-C. Hu, Y. Shi, S.-Y. Lang, X. Zhang, L. Gu, Y.-G. Guo, R. Wen and L.-J. Wan, *Nano Energy*, 2018, **49**, 453–459.
- 236 S. Y. Lang, Y. Shi, Y. G. Guo, D. Wang, R. Wen and L. J. Wan, *Angew. Chem., Int. Ed.*, 2016, **55**, 15835–15839.
- 237 S. Y. Lang, Y. Shi, Y. G. Guo, R. Wen and L. J. Wan, *Angew. Chem., Int. Ed.*, 2017, **56**, 14433–14437.
- 238 S. Ma, P. Zuo, H. Zhang, Z. Yu, C. Cui, M. He and G. Yin, *Chem Commun.*, 2019, **55**, 5267–5270.
- 239 Z. Zhang, Z. Cui, L. Qiao, J. Guan, H. Xu, X. Wang, P. Hu, H. Du, S. Li, X. Zhou, S. Dong, Z. Liu, G. Cui and L. Chen, *Adv. Energy Mater.*, 2017, **7**, 1602055.
- 240 D. Muthuraj, A. Ghosh, A. Kumar and S. Mitra, *ChemElectroChem*, 2018, **6**, 684–689.