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## Surface engineering on a microporous metal–organic framework to boost ethane/ethylene separation under humid conditions†

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Recently, examples of metal–organic frameworks (MOFs) have been identified displaying ethane (C<sub>2</sub>H<sub>6</sub>) over ethylene (C<sub>2</sub>H<sub>4</sub>) adsorption selectivity. However, it remains a challenge to construct MOFs with both large C<sub>2</sub>H<sub>6</sub> adsorption capacity and high C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> adsorption selectivity, especially under humid conditions. Herein, we reported two isorecticular MOF-5 analogues (JNU-6 and JNU-6-CH<sub>3</sub>) and their potential applications in one-step separation of C<sub>2</sub>H<sub>4</sub> from C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> mixtures. The introduction of CH<sub>3</sub> groups not only reduces the pore size from 5.4 Å in JNU-6 to 4.1 Å in JNU-6-CH<sub>3</sub> but also renders an increased electron density on the pyrazolate N atoms of the organic linker. JNU-6-CH<sub>3</sub> retains its framework integrity even after being immersed in water for six months. More importantly, it exhibits large C<sub>2</sub>H<sub>6</sub> adsorption capacity (4.63 mmol g<sup>-1</sup>) and high C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> adsorption selectivity (1.67) due to the optimized pore size and surface function. Breakthrough experiments on JNU-6-CH<sub>3</sub> demonstrate that C<sub>2</sub>H<sub>4</sub> can be directly separated from C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> (50/50, v/v) mixtures, affording benchmark productivity of 22.06 and 18.71 L kg<sup>-1</sup> of high-purity C<sub>2</sub>H<sub>4</sub> (≥99.95%) under dry and humid conditions, respectively.

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As one of the seven world-changing chemical separations, olefin/paraffin separation accounts for more than 0.3% of global energy consumption.<sup>1</sup> Ethylene (C<sub>2</sub>H<sub>4</sub>) is an important chemical feedstock in petrochemical industries, with a global production capacity of over 200 million tons in 2023.<sup>2</sup> At present, C<sub>2</sub>H<sub>4</sub> is mainly produced *via* steam cracking of ethane (C<sub>2</sub>H<sub>6</sub>) in industry, which would inevitably leave a certain amount of C<sub>2</sub>H<sub>6</sub> in the obtained C<sub>2</sub>H<sub>4</sub>. Given that the C<sub>2</sub>H<sub>6</sub> impurity may interfere with the polymerization process, further purification is required and the polymer-grade (≥99.95%) C<sub>2</sub>H<sub>4</sub> is highly desired in the manufacture of value-added chemicals. Owing to their very similar physicochemical properties and molecular sizes (3.81 × 4.08 × 4.82 Å<sup>3</sup> and 3.28 × 4.18 × 4.84 Å<sup>3</sup> for C<sub>2</sub>H<sub>6</sub> and C<sub>2</sub>H<sub>4</sub>, respectively), the industrial C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separation relies on cryogenic distillation, which is energy intensive and requires high distillation towers with many trays in order to achieve high reflux ratios.<sup>3</sup>

Compared to traditional distillation, non-thermal separation technologies using porous materials are of great significance to energy-efficient separation economy.<sup>4,5</sup> Metal–organic frameworks (MOFs), also known as porous coordination polymers (PCPs),<sup>6–8</sup> have been extensively investigated in hydrocarbon separation due to their highly tunable pore geometry and surface chemistry. With regard to C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separation, MOFs can be categorized into two types: C<sub>2</sub>H<sub>6</sub>-selective and C<sub>2</sub>H<sub>4</sub>-selective. For C<sub>2</sub>H<sub>4</sub>-selective MOFs, desorption by heat or purge is necessary in order to obtain C<sub>2</sub>H<sub>4</sub>, which likely would result in C<sub>2</sub>H<sub>6</sub> contamination. For example, the benchmark C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> sieving MOF, UTSA-280,<sup>9</sup> can realize complete exclusion of large-sized C<sub>2</sub>H<sub>6</sub> molecules and an infinite C<sub>2</sub>H<sub>4</sub> over C<sub>2</sub>H<sub>6</sub> selectivity, yet C<sub>2</sub>H<sub>4</sub> with only 99.1% purity was reported upon desorption.

By contrast, C<sub>2</sub>H<sub>6</sub>-selective MOFs allow for direct production of C<sub>2</sub>H<sub>4</sub> in a single adsorption step, which could potentially save *ca.* 40% of energy consumption (0.4 to 0.6 GJ ton<sup>-1</sup> of C<sub>2</sub>H<sub>4</sub>) for C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> separation.<sup>10</sup> Considering the numbers of hydrogen atoms on the surface of C<sub>2</sub>H<sub>6</sub> and C<sub>2</sub>H<sub>4</sub> molecules (6 *vs.* 4), controlled surface engineering with polar functions (*e.g.*, N- and O-containing groups) on the pore walls may facilitate non-classic hydrogen bonding and stronger affinity toward C<sub>2</sub>H<sub>6</sub> than C<sub>2</sub>H<sub>4</sub>.<sup>5,11–16</sup> Nevertheless, water vapor may compete for the interactions with those polar functional groups, leading to substantially reduced separation potential under humid

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conditions. For example, the benchmark  $C_2H_6$ -selective MOF,  $Fe_2(O_2)(dobdc)$ ,<sup>17</sup> demonstrated an excellent  $C_2H_6$  over  $C_2H_4$  selectivity with a record separation factor of *ca.* 4.4. The material itself, however, is extremely sensitive to moisture and has to be handled in a glove box. Recent studies show that nonpolar pore environments can prevent moisture from entering inside the frameworks and therefore retain the  $C_2H_4/C_2H_6$  separation potential even under humid conditions. More importantly, nonpolar pore surfaces may still facilitate  $C_2H_6$  over  $C_2H_4$  selectivity due to their slightly different polarizability ( $C_2H_6$ :  $44.7 \times 10^{25} \text{ cm}^3$ ,  $C_2H_4$ :  $42.5 \times 10^{25} \text{ cm}^3$ ). For instance, the MOF FJI-H11-Me-(des),<sup>18</sup> featuring nonpolar pore surfaces comprised of aromatic rings and alkyl groups, exhibits a stable  $C_2H_6$  over  $C_2H_4$  separation capacity in a wide range of relative humidities (RHs). However, the overall separation potential was limited due to its moderate adsorption capacity for  $C_2H_6$  ( $2.58 \text{ mmol g}^{-1}$ ). Until now, it remains a challenge to construct MOFs with both large  $C_2H_6$  adsorption capacity and high  $C_2H_6$  over  $C_2H_4$  adsorption selectivity to break the adsorption/selectivity trade-off limitation, especially under humid conditions.

Isorecticular chemistry allows for the design and synthesis of MOFs with tailor-made pore dimensions and functions for selective binding of one over the other in  $C_2H_4/C_2H_6$  separation. The methyl ( $CH_3$ ) group is electron-donating, and its effect on gas adsorption and separation has been well documented.<sup>19–21</sup> In addition, the  $CH_3$  group is considered strongly hydrophobic, and the MOF decorated with  $CH_3$  groups usually exhibits low water adsorption capacity even at high RH, which could effectively suppress the competition of water vapor for adsorption sites. Herein, we selected  $Zn_4O(PyC)_3$  (termed here as JNU-6,  $H_2PyC = \text{pyrazole-4-carboxylic acid}$ ), an isorecticular MOF-5 analogue,<sup>22–24</sup> as the platform for surface functionalization *via* linker methylation. We found that the introduction of  $CH_3$  groups not only reduces the pore size from 5.4 Å in JNU-6 to 4.1 Å in JNU-6- $CH_3$  but also renders an increased electron density on the pyrazolate N atoms of the organic linker. As a result, JNU-6- $CH_3$  retains its framework integrity even after being immersed in water for six months. More importantly, it exhibits large  $C_2H_6$  adsorption capacity ( $4.63 \text{ mmol g}^{-1}$ ) and high  $C_2H_6/C_2H_4$  adsorption selectivity (1.67) due to the optimized pore size and surface function. Breakthrough experiments on JNU-6- $CH_3$  demonstrate benchmark productivity of 22.06 and 18.71  $\text{L kg}^{-1}$  of high-purity  $C_2H_4$  ( $\geq 99.95\%$ ) from a  $C_2H_6/C_2H_4$  (50 : 50) mixture under dry and humid conditions, respectively.

To apply reticular chemistry and address the separation challenge of  $C_2H_6/C_2H_4$  under humid conditions, it is crucial to find a  $C_2H_6$ -selective MOF that can be easily functionalized. In this work, we selected an isorecticular analogue of MOF-5 as the platform for the introduction of  $CH_3$  groups. A solvothermal reaction of  $Zn(NO_3)_2$  with pyrazole-4-carboxylic acid or 3-methylpyrazole-4-carboxylic acid in a mixed solution of DEF/ $H_2O$  afforded high-quality block crystals of JNU-6 and JNU-6- $CH_3$ , respectively. Single crystal X-ray diffraction (SCXRD) analyses reveal that JNU-6 and JNU-6- $CH_3$  are of cubic crystal structure isorecticular to MOF-5. It should be pointed out that both JNU-6 and JNU-6- $CH_3$  were reported by Zhong and co-workers recently for  $n\text{-C}_4\text{H}_{10}/\text{iso-C}_4\text{H}_{10}$  separation during our

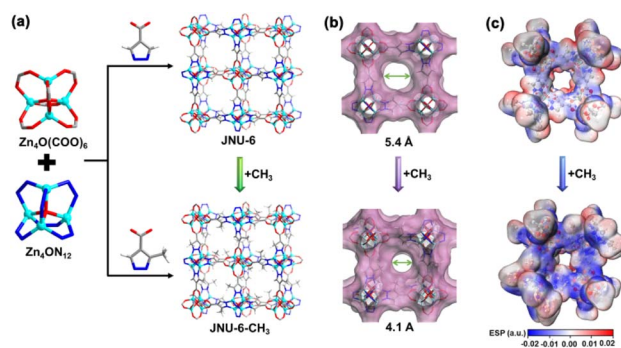


Fig. 1 (a) Isostructural frameworks of JNU-6 and JNU-6- $CH_3$  assembled with two six-connected  $Zn_4O$  SBUs and their respective organic linkers. (Color code: Zn, cyan; C, dark gray; N, blue; O, red; H, white). (b) Connolly surface analysis of JNU-6 and JNU-6- $CH_3$ , depicting the reduced pore size upon the introduction of  $CH_3$  groups. (c) Electrostatic potential mapping of JNU-6 and JNU-6- $CH_3$ , depicting the increased electron density on pyrazolate N atoms upon the introduction of  $CH_3$  groups.

preparation of this paper.<sup>25</sup> In the crystal structures, two types of octahedral  $Zn_4O$  SBUs (secondary building units,  $Zn_4ON_{12}$  and  $Zn_4O(COO)_6$ ) are connected by ditopic organic linkers to form a 3-dimensional (3D) network with interconnected cubic-shaped cages (Fig. 1a). The introduction of  $CH_3$  groups on the pore surface decreases the aperture size from 5.4 Å to 4.1 Å (Fig. 1b), making it more comparable to the kinetic diameters of  $C_2H_6$  and  $C_2H_4$  ( $C_2H_6 = 4.44 \text{ Å}$ ,  $C_2H_4 = 4.16 \text{ Å}$ ).<sup>26</sup> Density functional theory (DFT) calculations were carried out to generate the mapping of electrostatic potential (ESP) on JNU-6 and JNU-6- $CH_3$ . As shown in Fig. 1c, an increased electron density was observed on the pyrazole rings of JNU-6- $CH_3$ , particularly around the N atoms, owing to the electron-donating effect of the  $CH_3$  groups. Such an electrostatic potential in JNU-6- $CH_3$  indicates an increased surface dipole, which may potentially facilitate the discrimination of  $C_2H_6$  from  $C_2H_4$  due to their slightly different polarizability.

The phase purity and crystallinity of the bulk JNU-6 and JNU-6- $CH_3$  samples were checked by powder X-ray diffraction (PXRD) analyses, showing good agreement with the ones simulated from their respective crystal structures.  $N_2$  adsorption/desorption isotherms at 77 K were measured to investigate the porosity of JNU-6 and JNU-6- $CH_3$ . As shown in Fig. 2a, both of them exhibit type-I adsorption/desorption isotherms characteristic of microporous materials. Due to the introduction of  $CH_3$  groups, the calculated Brunauer–Emmett–Teller (BET) surface area of JNU-6- $CH_3$  is slightly decreased from  $1411 \text{ m}^2 \text{ g}^{-1}$  in JNU-6 to  $1270 \text{ m}^2 \text{ g}^{-1}$ , and the calculated pore volume is also decreased from  $0.59 \text{ cm}^3 \text{ g}^{-1}$  in JNU-6 to  $0.51 \text{ cm}^3 \text{ g}^{-1}$ . Further, the pore size distribution was determined by the Horvath–Kawazoe model and the dominant pore diameters exhibit the same trend, with values decreasing from 5.4 Å in JNU-6 to 4.1 Å in JNU-6- $CH_3$  (Fig. 2a, inset).

Single-component adsorption isotherms of JNU-6 and JNU-6- $CH_3$  for  $C_2H_6$  and  $C_2H_4$  were measured at 298 K. As exhibited in Fig. 2b, the  $C_2H_6$  adsorption capacity is substantially larger than  $C_2H_4$  in the entire pressure range (0–1 bar) for both JNU-6 and



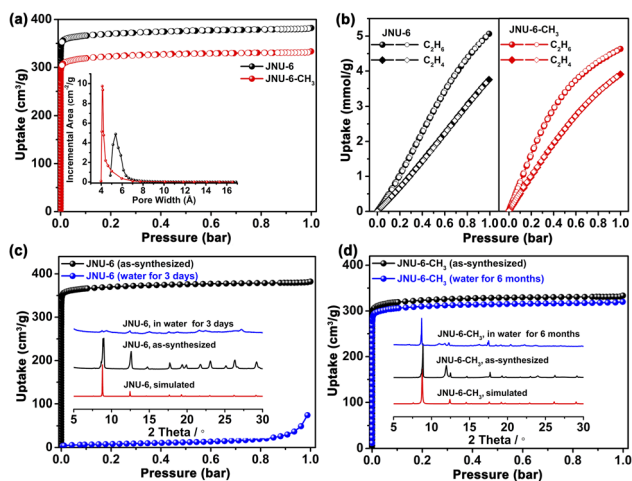


Fig. 2 (a)  $\text{N}_2$  adsorption/desorption isotherms of JNU-6 and JNU-6- $\text{CH}_3$  at 77 K. Inset shows the difference in their pore size distribution. (b)  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$  adsorption/desorption isotherms of JNU-6 and JNU-6- $\text{CH}_3$  at 298 K. (c) Comparison of  $\text{N}_2$  adsorption isotherms at 77 K and PXRD patterns of the as-synthesized JNU-6 and water-treated JNU-6 (being soaked in water for 3 days). (d) Comparison of  $\text{N}_2$  adsorption isotherms at 77 K and PXRD patterns of the as-synthesized JNU-6- $\text{CH}_3$  and water-treated JNU-6- $\text{CH}_3$  (being soaked in water for 6 months).

JNU-6- $\text{CH}_3$ . The maximum uptakes for  $\text{C}_2\text{H}_4$  are  $84.4 \text{ cm}^3 \text{ g}^{-1}$  ( $3.77 \text{ mmol g}^{-1}$ ) and  $88.1 \text{ cm}^3 \text{ g}^{-1}$  ( $3.93 \text{ mmol g}^{-1}$ ) on JNU-6 and JNU-6- $\text{CH}_3$ , respectively, while the uptakes for  $\text{C}_2\text{H}_6$  can reach up to  $113.6 \text{ cm}^3 \text{ g}^{-1}$  ( $5.07 \text{ mmol g}^{-1}$ ) and  $103.7 \text{ cm}^3 \text{ g}^{-1}$  ( $4.63 \text{ mmol g}^{-1}$ ) on JNU-6 and JNU-6- $\text{CH}_3$ , respectively. The  $\text{C}_2\text{H}_6$  uptakes on JNU-6 and JNU-6- $\text{CH}_3$  are comparable to or larger than those of most of the  $\text{C}_2\text{H}_6$ -selective MOFs, such as  $\text{Cu}(\text{Qc})_2$  ( $1.84 \text{ mmol g}^{-1}$ ),<sup>27</sup> MUF-15 ( $4.69 \text{ mmol g}^{-1}$ ),<sup>28</sup> NKMOF-8-Br ( $4.22 \text{ mmol g}^{-1}$ ),<sup>29</sup> FJI-H11-Me-(des) ( $2.58 \text{ mmol g}^{-1}$ ),<sup>18</sup>  $\text{Ni}(\text{In})_2$  ( $3.05 \text{ mmol g}^{-1}$ ),<sup>30</sup> AzoleTh-1 ( $4.47 \text{ mmol g}^{-1}$ ),<sup>31</sup> and NPU-1 ( $4.5 \text{ mmol g}^{-1}$ ).<sup>32</sup> We applied the ideal adsorbed solution theory (IAST) to calculate the adsorption selectivity, and the IAST selectivity of JNU-6- $\text{CH}_3$  for a  $\text{C}_2\text{H}_6/\text{C}_2\text{H}_4$  (50 : 50) mixture at 298 K can reach up to 1.67 (Fig. S4–S9†), which is comparable to those of the reported benchmark MOF adsorbents, such as MUF-15 (1.96),<sup>28</sup> NKMOF-8-Br (2.65),<sup>29</sup> NKMOF-8-Me (1.88),<sup>29</sup>  $\text{Ni}(\text{In})_2$  (2.44),<sup>30</sup> AzoleTh-1 (1.46),<sup>31</sup> and NPU-1 (1.32).<sup>32</sup> Isothermic heat of adsorption ( $Q_{\text{st}}$ ) was calculated by fitting adsorption isotherms at 273, 283, and 298 K using the dual-site Langmuir–Freundlich model (Fig. S10–S19†). At 298 K, the  $Q_{\text{st}}$  of JNU-6 at zero loading was determined to be  $24.0 \text{ kJ mol}^{-1}$  and  $20.9 \text{ kJ mol}^{-1}$  for  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$ , respectively, while the  $Q_{\text{st}}$  of JNU-6- $\text{CH}_3$  at zero loading was determined to be  $24.7 \text{ kJ mol}^{-1}$  vs.  $23.9 \text{ kJ mol}^{-1}$  for  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$ , respectively. The data confirm the stronger thermodynamic affinity toward  $\text{C}_2\text{H}_6$  than  $\text{C}_2\text{H}_4$  in both materials. Moreover, the reduced pore size in JNU-6- $\text{CH}_3$  may allow for an increased host–guest interaction between the framework and gas molecules, resulting in adsorption affinity stronger than JNU-6 for both  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$ . Meanwhile, the  $Q_{\text{st}}$  values of both JNU-6 and JNU-6- $\text{CH}_3$  are much lower than those of  $\text{Fe}_2(\text{O}_2)(\text{dobdc})$  ( $67 \text{ kJ mol}^{-1}$ ),<sup>17</sup> IRMOF-8 ( $52.5 \text{ kJ mol}^{-1}$ ),<sup>33</sup> PAF-40-Fe ( $47.8 \text{ kJ mol}^{-1}$ ),<sup>34</sup> Zn-atz-

ipa ( $45.8 \text{ kJ mol}^{-1}$ ),<sup>35</sup> and MAF-49 ( $60 \text{ kJ mol}^{-1}$ ).<sup>12</sup> The relatively low  $Q_{\text{st}}$  value may facilitate easy regeneration and low energy consumption during the desorption process, reflecting the advantages of pore surface engineering with nonpolar functional groups. Furthermore, ten continuous adsorptions for  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$  were carried out on an ASAP2020 gas sorption instrument. As shown in Fig. S20–S23,† both JNU-6 and JNU-6- $\text{CH}_3$  retain adsorption capacity over ten cycles, indicating that the samples can be fully regenerated by vacuum at room temperature.

To test their water stability, JNU-6 and JNU-6- $\text{CH}_3$  were soaked in water for days and then subjected to PXRD and gas adsorption measurements. As shown in Fig. 2c, JNU-6 lost most of the crystallinity and porosity after being soaked in water for three days. In contrast, the crystallinity and structural integrity of JNU-6- $\text{CH}_3$  can be well retained after being soaked in water for six months (Fig. 2d). Water vapor adsorption measurements for JNU-6 and JNU-6- $\text{CH}_3$  were carried out and both of them show S-shaped adsorption isotherms characteristic of pore filling (Fig. 4b), and the limited water uptake at low pressure suggests that the water affinity on the MOF surface is relatively low. With the linker methylation, higher water vapor pressure is required to induce the pore filling, indicating further increased hydrophobicity of MOF pores from JNU-6 and JNU-6- $\text{CH}_3$ . Overall, the introduction of  $\text{CH}_3$  groups renders JNU-6- $\text{CH}_3$  with an optimized pore size, increased surface dipole, and improved hydrolytic stability, which prompted us to further study its potential for  $\text{C}_2\text{H}_6/\text{C}_2\text{H}_4$  separation under humid conditions.

To verify the preferential adsorption of  $\text{C}_2\text{H}_6$  over  $\text{C}_2\text{H}_4$  on JNU-6 and JNU-6- $\text{CH}_3$ , we first performed computational modeling studies using grand canonical Monte Carlo (GCMC) simulations.<sup>35,36</sup> The simulated  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$  adsorption isotherms are in good agreement with the experimental ones at 298 K and 1 bar, and the probability density distributions of  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$  reveal that both  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$  are preferentially adsorbed at the corners of the cubic-shaped cages in both JNU-6 and JNU-6- $\text{CH}_3$  (Fig. S24–S27†). Take JNU-6- $\text{CH}_3$  as an example, there are six  $\text{C-H}\cdots\pi$  interactions between the H atoms of  $\text{C}_2\text{H}_6$  and the pyrazole rings of the linkers with  $\text{H}\cdots\pi$  distances from 2.93 to 3.41 Å. In comparison, there are fewer  $\text{C-H}\cdots\pi$  interactions between  $\text{C}_2\text{H}_4$  and the pyrazole rings of the linkers with  $\text{H}\cdots\pi$  distances from 3.0 to 3.85 Å (Fig. 3b and e). Further, an independent gradient model based on Hirshfeld partition (IGMH) analysis on the optimized structures was developed. As shown in Fig. 3c and f, multiple green isosurfaces were observed for both  $\text{C}_2\text{H}_6$  and  $\text{C}_2\text{H}_4$ , indicating the existence of vdW interactions between the gas molecules and the three pyrazole rings. The static binding energies ( $\Delta E$ ) for  $\text{C}_2\text{H}_6$  on JNU-6 and JNU-6- $\text{CH}_3$  were calculated to be 18.04 and  $22.23 \text{ kJ mol}^{-1}$ , respectively, higher than those for  $\text{C}_2\text{H}_4$  (17.22 and  $20.15 \text{ kJ mol}^{-1}$ ). These values further confirm the weak vdW nature of the host–guest interactions between gas molecules and the nonpolar pore surfaces, which favors the adsorption of  $\text{C}_2\text{H}_6$  over  $\text{C}_2\text{H}_4$ .

To evaluate the actual separation capability of JNU-6 and JNU-6- $\text{CH}_3$  for  $\text{C}_2\text{H}_6/\text{C}_2\text{H}_4$  mixtures, we first performed dynamic column breakthrough experiments in which a  $\text{C}_2\text{H}_6/\text{C}_2\text{H}_4$  (50/





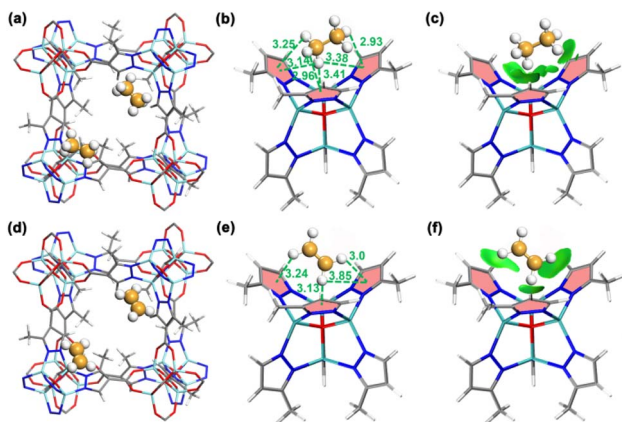


Fig. 3 Primary adsorption sites for  $C_2H_6$  (a) and  $C_2H_4$  (d) in JNU-6- $CH_3$  determined by Monte Carlo (GCMC) simulations. C–H... $\pi$  interactions (green dashed lines) for  $C_2H_6$  (b) and  $C_2H_4$  (e) at the primary adsorption site of JNU-6- $CH_3$ . Independent gradient model based on Hirshfeld partition (IGMH) analysis for  $C_2H_6$  (c) and  $C_2H_4$  (f) at the primary adsorption site of JNU-6- $CH_3$  (green surfaces represent vdW interactions). (Color code: Zn, cyan; C, dark gray; N, blue; O, red; H, white. The distance unit is in Å).

50, v/v) mixture was introduced over the activated JNU-6 or JNU-6- $CH_3$  at a flow rate of  $2 \text{ mL min}^{-1}$  and 298 K. As shown in Fig. 4c, JNU-6 can separate  $C_2H_6$  from the  $C_2H_6/C_2H_4$  mixture with an estimated productivity of  $4.92 \text{ L kg}^{-1}$  of high-purity  $C_2H_4$  ( $\geq 99.95\%$ ) under dry conditions. Surprisingly, JNU-6- $CH_3$  exhibits significantly improved separation capacity under similar conditions, and the data are in good agreement with the simulated breakthrough curve (Fig. S29<sup>†</sup>). As shown in Fig. 4d,  $C_2H_4$  and  $C_2H_6$  were detected to break through the column at the time points of  $52.7 \text{ min g}^{-1}$  and  $67.9 \text{ min g}^{-1}$ , respectively. During the above time period, high-purity  $C_2H_4$  ( $\geq 99.95\%$ ) can be collected with an estimated  $C_2H_4$  productivity of  $22.06 \text{ L kg}^{-1}$ , which is about four times that of JNU-6 and the highest among those of the reported MOFs under similar conditions, including JNU-2 ( $21.2 \text{ L kg}^{-1}$ ),<sup>13</sup>  $Fe_2(O_2)(\text{dobdc})$  ( $17.7 \text{ L kg}^{-1}$ ),<sup>17</sup> Tb-MOF-76-( $NH_2$ ) ( $17.66 \text{ L kg}^{-1}$ ),<sup>37</sup> TJT-100 ( $16.38 \text{ L kg}^{-1}$ ),<sup>38</sup> MUF-15 ( $14 \text{ L kg}^{-1}$ ),<sup>28</sup> UiO-67-( $NH_2$ )<sub>2</sub> ( $12.32 \text{ L kg}^{-1}$ ),<sup>5</sup> MAF-49 ( $6.23 \text{ L kg}^{-1}$ ),<sup>12</sup> and  $Cu(Qc)_2$  ( $4.0 \text{ L kg}^{-1}$ )<sup>27</sup> (Fig. 4f).

To further examine the moisture effect on the separation capability for  $C_2H_6/C_2H_4$ , we performed differential scanning calorimetry (DSC) measurements of heat flow upon introducing water vapor,  $C_2H_4$ , and  $C_2H_6$  on JNU-6 and JNU-6- $CH_3$ . For JNU-6, the experimental  $Q_{st}$  for water vapor,  $C_2H_4$ , and  $C_2H_6$  is 0.2, 10.2, and  $15.7 \text{ kJ mol}^{-1}$ , respectively (Fig. S38<sup>†</sup>), while for JNU-6- $CH_3$ , the experimental  $Q_{st}$  for water vapor,  $C_2H_4$ , and  $C_2H_6$  is 1.7, 12.2, and  $16.0 \text{ kJ mol}^{-1}$ , respectively (Fig. 4a), both indicative of significantly stronger binding affinity for  $C_2H_6$  and  $C_2H_4$  than for water vapor. This, together with water vapor adsorption measurements (Fig. 4b), suggests that JNU-6- $CH_3$  may be able to maintain the high separation capability for  $C_2H_6/C_2H_4$  mixtures under humid conditions. Breakthrough experiments were thus performed on JNU-6 and JNU-6- $CH_3$  for a  $C_2H_6/C_2H_4$  (50/50, v/v) mixture under 98% RH conditions. As revealed in Fig. 4c and d, the purity of  $C_2H_4$  dropped from 99.95% to 99.2% for JNU-6,

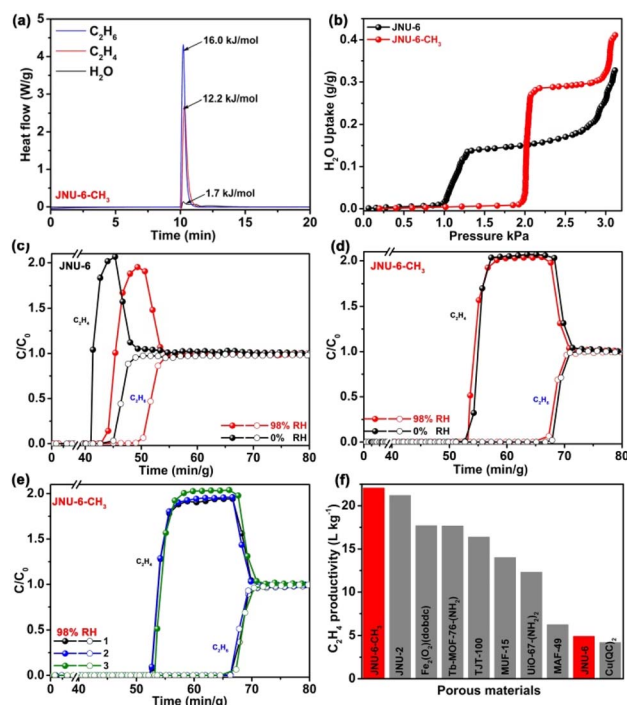


Fig. 4 (a) Differential scanning calorimetry (DSC) measurements of heat flow upon introducing  $C_2H_6$ ,  $C_2H_4$ , and water vapor on JNU-6- $CH_3$  at a flow rate of  $10 \text{ mL min}^{-1}$  at 298 K. (b) Water vapor adsorption isotherms of JNU-6 and JNU-6- $CH_3$  at 298 K. (c) Experimental breakthrough curves on JNU-6 (1.0 g) for a  $C_2H_6/C_2H_4$  (50/50, v/v) mixture at a flow rate of  $2.0 \text{ mL min}^{-1}$  and 298 K under 0% RH and 98% RH conditions. (d) Experimental breakthrough curves on JNU-6- $CH_3$  (0.85 g) for a  $C_2H_6/C_2H_4$  (50/50, v/v) mixture at a flow rate of  $2.0 \text{ mL min}^{-1}$  and 298 K under 0% RH and 98% RH conditions. (e) Three cycles of breakthrough experiments on JNU-6- $CH_3$  for a  $C_2H_6/C_2H_4$  (50/50, v/v) mixture at a flow rate of  $2.0 \text{ mL min}^{-1}$  and 298 K under 98% RH conditions. (f) Comparison of the  $C_2H_4$  productivity estimated from breakthrough curves for JNU-6- $CH_3$ , JNU-6, and other reported porous materials.

likely due to its hydrolytic instability (Fig. 2c), whereas the purity of  $C_2H_4$  remained over 99.95% with only slightly dropped productivity ( $18.71 \text{ L kg}^{-1}$ ) for JNU-6- $CH_3$ . The results confirm that the introduction of  $CH_3$  groups in the framework can indeed improve separation capability, especially under humid conditions. Furthermore, continuous breakthrough experiments under humid conditions were carried out, revealing the retained separation performance of JNU-6- $CH_3$  over three cycles (Fig. 4e and S31<sup>†</sup>).

To further study the effect of methylation degree on adsorption separation performance, we synthesized JNU-6-( $CH_3$ )<sub>2</sub> with 3,5-dimethylpyrazole-4-carboxylic acid. JNU-6-( $CH_3$ )<sub>2</sub> also shows preferential adsorption of  $C_2H_6$  over  $C_2H_4$ , especially in the low-pressure range (Fig. S33<sup>†</sup>). However, its  $C_2H_6$  and  $C_2H_4$  adsorption amounts at 0.5 bar are almost the same, and the adsorption of  $C_2H_6$  and  $C_2H_4$  on JNU-6-( $CH_3$ )<sub>2</sub> is significantly lower than those on JNU-6- $CH_3$  and JNU-6 in the high-pressure range, likely due to the reduced porosity of JNU-6-( $CH_3$ )<sub>2</sub> (Fig. S32a<sup>†</sup>). As a result, dynamic column breakthrough experiments on JNU-6-( $CH_3$ )<sub>2</sub> reveal a poor separation for a  $C_2H_6/C_2H_4$  (50/50, v/v) mixture at a flow rate of  $2.0 \text{ mL min}^{-1}$



and 298 K (Fig. S32d†). On the other hand, JNU-6-CF<sub>3</sub> was synthesized by using 5-trifluoromethyl-4-carboxylic acid as a ligand. JNU-6-CF<sub>3</sub> also shows preferential adsorption of C<sub>2</sub>H<sub>6</sub> over C<sub>2</sub>H<sub>4</sub>. The maximum uptake of C<sub>2</sub>H<sub>6</sub> on JNU-6-CF<sub>3</sub> is 3.49 mmol g<sup>-1</sup> (Fig. S34b†), which is nearly 25% less than that of JNU-6-CH<sub>3</sub>, likely due to the reduced porosity of JNU-6-CF<sub>3</sub> (Fig. S35a†). The water vapor adsorption isotherm of JNU-6-CF<sub>3</sub> displays almost no water uptake over the entire pressure range (Fig. S34c†), reflecting its extremely high hydrophobicity. We evaluated dynamic column breakthrough experiments on JNU-6-CF<sub>3</sub> for a C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> (50/50, v/v) mixture at a flow rate of 2.0 mL min<sup>-1</sup> and 298 K. As shown in Fig. S34d,† a clean separation of C<sub>2</sub>H<sub>6</sub> from the C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> mixture can be realized under either dry or 98% RH conditions with no obvious decrease in separation performance. Based on the breakthrough curves, ca. 10.5 L kg<sup>-1</sup> of high-purity C<sub>2</sub>H<sub>4</sub> (≥99.95%) can be recovered from the C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>6</sub> (50/50) mixture in a single breakthrough operation, which is about half of that of JNU-6-CH<sub>3</sub>. The results indicate that further increase of methylation degree or introducing more hydrophobic CF<sub>3</sub> groups may not be necessarily favorable for the C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> separation, and both adsorption capacity and adsorption selectivity have to be considered to achieve high separation efficiency.

In summary, we have successfully demonstrated a surface engineering strategy to boost the separation potential of C<sub>2</sub>H<sub>4</sub> from C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> mixtures under either dry or humid conditions. The introduction of CH<sub>3</sub> groups on an isoreticular MOF-5 analogue (JNU-6) renders the obtained JNU-6-CH<sub>3</sub> with enhanced hydrolytic stability and a more suitable pore environment for C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> separation. JNU-6-CH<sub>3</sub> retains its framework integrity even after being immersed in water for six months, and it exhibits large C<sub>2</sub>H<sub>6</sub> adsorption capacity (4.63 mmol g<sup>-1</sup>) and high C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> adsorption selectivity (1.67) due to the optimized pore size and surface function. Breakthrough experiments reveal benchmark productivity of 22.06 and 18.71 L kg<sup>-1</sup> of high-purity C<sub>2</sub>H<sub>4</sub> (≥99.95%) from a C<sub>2</sub>H<sub>6</sub>/C<sub>2</sub>H<sub>4</sub> (50/50, v/v) mixture under dry and humid conditions, respectively. This work offers a promising approach for designing MOFs to overcome the adsorption/selectivity trade-off limitation in paraffin/olefin separation.

## Data availability

The data that support the plots within this paper and other findings of this study are available from the corresponding authors upon reasonable request. The X-ray crystallographic coordinates for structures reported in this Article have been deposited at the Cambridge Crystallographic Data Centre (CCDC), under deposition numbers CCDC 2259108, 2258075, and 2286047.†[https://www.ccdc.cam.ac.uk/data\\_request/cif](https://www.ccdc.cam.ac.uk/data_request/cif)

## Author contributions

H. Z., W. L., and D. L. conceived and designed the research. X.-J. X., H. Z., and W. L. co-wrote the manuscript. X.-J. X. and Q.-Y. C. planned and executed the synthesis, characterization, and gas separation studies. Y. W. and R. H. performed the theoretical

simulations. X.-J. X. carried out the structural analyses. All authors participated in and contributed to the preparation of the manuscript.

## Conflicts of interest

There are no conflicts to declare.

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