## ChemComm

### COMMUNICATION



View Article Online View Journal | View Issue

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Cite this: Chem. Commun., 2024, 60, 10918

Received 19th July 2024, Accepted 29th August 2024

DOI: 10.1039/d4cc03620d

rsc.li/chemcomm

# Electrochemical reduction of nitrate to hydroxylamine on gold electrode<sup>†</sup>

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In this study, we explore the efficacy of gold (Au) as a selective electrocatalyst for the reduction of nitrate to hydroxylamine, a valuable nitrogen-based chemical, while also evaluating the by-product formation of ammonia. We systematically optimized various experimental parameters including nitrate concentration, pH, and applied potential. We found that at an applied potential of -0.7 V vs. RHE in 0.1 M HNO<sub>3</sub>, Au achieves a 230.1  $\pm$  19  $\mu$ mol NH<sub>2</sub>OH h<sup>-1</sup> cm<sup>-2</sup> yield, with a 34.2  $\pm$  2.8% faradaic efficiency. This study underscores the potential of Au as an efficient and selective electrocatalyst for generating value-added nitrogen products through an electrochemical pathway.

Nitrogen, an element essential to all life, manifests in numerous forms, from its stable diatomic gas in the atmosphere to a myriad of nitrogen-containing molecules such as ammonia, nitrate, and organic compounds. Human activities, from industrial manufacturing to agriculture, transform these nitrogen states in ways that significantly impact the global nitrogen cycle. Such transformations—either as unintended byproducts in chemical and combustion processes or through deliberate production of fertilizers and chemicals—distort natural pathways.<sup>1,2</sup> Nitrate, the most oxidized form of nitrogen, is a well know pollutant in water bodies, which in excess threatens the biodiversity of ecosystems and has proven to have negative health effects.<sup>3,4</sup> Additionally, excesses are eventually removed by natural denitrification processes, performed by microbial organisms. Due to poor selectivity, this also leads to the production of significant amounts of nitrous oxide (N<sub>2</sub>O), a potent greenhouse gas.<sup>5</sup> Converting waste nitrates into valuable chemicals represents a key aspect of sustainable development and poses a significant challenge that engages engineering and research communities worldwide.

The electrochemical reduction of nitrate (NO<sub>3</sub>RR) is gaining prominence as a method that is not only energy-efficient in producing valuable products but also environmentally beneficial for treating water pollution.<sup>4</sup> This process can yield a variety of nitrogen products with different oxidation states; however, research has predominantly focused on producing ammonia,<sup>6</sup> often overlooking the potential for selective reduction to hydroxylamine (NH2OH). Hydroxylamine deserves further investigation due to its critical role as a precursor in the synthesis of ε-caprolactam for Nylon-6 production, which consumes more than 95% of the world's estimated production of 800 000 tons per year.<sup>7,8</sup> Additionally, the potential of NH<sub>2</sub>OH as a renewable energy carrier amplifies its significance.9,10 Traditional methods for producing NH<sub>2</sub>OH, such as the Raschig process and catalytic hydrogenation of nitric oxide, face challenges including the use of toxic reagents such as SO2 or NO, harsh conditions, complex processes, low conversion rates and environmental hazards.<sup>11</sup> Selective electrochemical NO<sub>3</sub>RR to NH<sub>2</sub>OH conversion presents a greener, more sustainable, cost-effective, and operationally simpler alternative. Concentrating on electrochemical routes, especially for the selective production of hydroxylamine, could drastically lower the carbon footprint as well as environmental impact of the synthesis of this key industrial chemical. This underscores the importance of targeted research into optimizing NO<sub>3</sub>RR selectivity and efficiency. Recent studies have identified mercury as an effective electrode material for the electrochemical NO<sub>3</sub>RR to NH<sub>2</sub>OH.<sup>12</sup> However, its utility is considerably restricted due to toxicity concerns and the challenges of handling it in its liquid form. Compared to standard NO3RR reactions performed in

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<sup>†</sup> Electronic supplementary information (ESI) available: Materials and experimental details. See DOI: https://doi.org/10.1039/d4cc03620d



Fig. 1 (A) Pathways for surface adsorbed hydrogen, \*H, generation under acidic or neutral/alkaline conditions; (B) schematic representation of the experimental approach used for the  $NO_3RR$ , including the H-cell configuration and ion chromatography for product analysis.

neutral conditions, which use nitrate salts and lead to the generation of stoichiometric alkali metal hydroxide byproducts, exploring the reaction in acidic nitrate conditions becomes interesting.<sup>13-15</sup> The increased acidity, compared to alkaline and neutral conditions, provides ample protons for sustained NO<sub>3</sub><sup>-</sup> hydrogenation reactions, resulting in an enhanced conversion rate of NO<sub>3</sub><sup>-</sup> and more energy-efficient NH<sub>2</sub>OH and NH<sub>3</sub> generation (Fig. 1A).<sup>15</sup> The hydrogen evolution reaction (HER) inevitably competes with NO3RR in acidic media. Such conditions necessitate careful electrode material selection to mitigate corrosion. Among noble metal-based electrodes, palladium generally favors NH<sub>3</sub> production,<sup>16</sup> while platinum is known for its efficacy in the hydrogen evolution reaction. Given these considerations, gold emerges as a particularly suitable material, noted for its durability and exceptional resistance to corrosion, even in strongly acidic conditions. This prompted our investigation into the capabilities of Au as an electrode for NO<sub>3</sub>RR, particularly focusing on its selectivity for NH2OH production. We rigorously tested the effects of applied potential, NO<sub>3</sub><sup>-</sup> concentration, and the pH of the electrolyte on the selectivity and electrochemical activity of Au towards NH<sub>2</sub>OH. Our experiments revealed a significant peak faradaic efficiency (FE) of 34.2  $\pm$  2.8% for NH<sub>2</sub>OH at an applied potential of -0.7 V versus RHE in a 0.1 M HNO<sub>3</sub> solution. Notably, the NO<sub>3</sub><sup>-</sup> concentration was found to have a profound impact on both the yield and selectivity towards NH2OH, with yields diminishing from 230.1  $\pm$  19  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup> in 0.1 M NO<sub>3</sub><sup>-</sup> to zero at 1 M KNO<sub>3</sub>. Furthermore, the optimum yield of NH<sub>2</sub>OH, 333  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup>, was achieved at a pH of 0.3 in H<sub>2</sub>SO<sub>4</sub> with a 0.1 M NO<sub>3</sub><sup>-</sup> concentration. These findings underline the potential of Au electrodes to serve as both an efficient and selective catalyst for the electrochemical reduction of NO3<sup>-</sup> to NH2OH, offering an environmentally friendly alternative to conventional production methods and mitigating associated environmental impacts.

The nitrate reduction is a complicated multi-electron, multiproton transfer process. The electroreduction of  $NO_3^-$  to  $NH_2OH$ involves the transfer of eight protons and six electrons. Conversely, the production of  $NH_3$  from  $NO_3^-$  requires ten protons and eight electrons for electroreduction. Consequently, the HER inevitably emerges as a competing reaction for  $NO_3RR$  in acidic media. The reactions in this work are summarized in eqn (1)–(3), where  $E^0$  is relative to the standard hydrogen electrode (SHE):

$$NO_3^- + 8H^+ + 6e^- \rightarrow NH_3OH^+ + 2H_2O \quad E^0 = 0.73 \text{ V} \text{ vs. SHE}$$
(1)



Fig. 2 Characterization and performance of a Au electrode in electrochemical NO<sub>3</sub>RR: (A) XRD pattern, (B) comparative LSV curves for the Au wire electrode measured in 0.1 M HNO<sub>3</sub> and 0.1 M H<sub>2</sub>SO<sub>4</sub>, (C) influence of applied potential on the NO<sub>3</sub>RR yield rates of NH<sub>2</sub>OH and NH<sub>3</sub>, and (D) faradaic efficiency integrated over 1 hour in 0.1 M HNO<sub>3</sub>.

$$NO_3^- + 10H^+ + 8e^- \rightarrow NH_4^+ + 3H_2O \quad E^0 = 0.88 \text{ V} \text{ vs. SHE}$$
(2)

$$2H^+ + 2e^- \rightarrow H_2 \quad E^0 = 0 \text{ V } \nu s. \text{ SHE}$$
(3)

The morphology of the Au wire (diam. 0.5 mm, 99.999% pure) electrode was analyzed using scanning electron microscopy, revealing an irregular surface texture as illustrated in Fig. S1, (ESI<sup>†</sup>). Compositional analysis through energy-dispersive X-ray spectroscopy confirmed that this electrode solely exists of Au, with the detailed spectrum shown in Fig. S2, (ESI<sup>†</sup>). To ascertain the crystallinity of the electrode, X-ray diffraction was employed, with the results displayed in Fig. 2A. The recorded XRD pattern clearly exhibits the characteristic peaks of pure gold at  $38.2^{\circ}$ ,  $44.4^{\circ}$ , and  $65.58^{\circ}$ . These peaks correspond to the (111), (200), and (220) crystallographic planes of Au, respectively. These results are in agreement with standard data (JCPDS 04-0784), confirming the purity of the Au wire.

We commenced our study by evaluating the electrocatalytic behavior of the Au electrode in 0.1 M HNO3 and H2SO4 solutions, respectively, employing linear sweep voltammetry (LSV) for this characterization. This approach allowed us to assess the electrode's activity across a range of potentials from 0 V to -1 V vs. RHE (Fig. 2B). A notable increase in current density was observed beyond -0.3 V vs. RHE in 0.1 M HNO<sub>3</sub>, peaking at  $-266 \text{ mA cm}^{-2}$  at -1 V vs. RHE. The elevated current density in HNO<sub>3</sub>, compared to that in  $H_2SO_4$  (without  $NO_3^-$ ), underscores the Au electrode's specific activity towards NO<sub>3</sub><sup>-</sup> reduction. Subsequent, our focus shifted to identifying the reaction products produced in an H-shaped three-electrode quartz cell, which was partitioned by a Nafion 117 membrane and contained 0.1 M HNO<sub>3</sub> as the electrolyte (Fig. 1B). The products of the NO3RR were monitored using ion chromatography (IC), which revealed only the presence of NH<sub>3</sub> and NH<sub>2</sub>OH (Fig. S3, ESI<sup>†</sup>). Subsequent experiments aimed to determine the impact of various applied potentials on the

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production rates and selectivity of these identified products. By experimenting with potentials ranging from -0.3 V to -0.8 V vs. RHE (Fig. S4, ESI<sup>†</sup>), we observed that the yield of NH<sub>2</sub>OH increased with more negative potentials, increasing from 6.7  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup> at -0.3 V vs. RHE to 254.3  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup> at -0.8 V vs. RHE (Fig. 2C). Additionally, the FE for NH<sub>2</sub>OH production demonstrated a progressive increase from 10.6% at -0.3 V vs. RHE, peaking at 34.2  $\pm$  2.8% at -0.7 V vs. RHE, and then slightly declining to 32.6% at -0.8 V vs. RHE (Fig. 2D), possibly due to the enhanced competition from the HER at these more negative potentials. The yield and FE of H<sub>2</sub> were determined to be 482.7  $\pm$  40.3  $\mu mol~h^{-1}~cm^{-2}$  and 27.1  $\pm$  0.9% at -0.7 V vs. RHE, respectively (Fig. S5, ESI<sup>+</sup>). The NH<sub>3</sub> yield measured from UV-vis method (81  $\pm$  10.1  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup>) was close to IC method (89  $\pm$  11.9  $\mu$ mol h<sup>-1</sup> cm<sup>-2</sup>) at -0.7 V vs. RHE, indicative of the reliability of the determined experimental data (Fig. S6, ESI<sup>†</sup>). Notably, throughout these experiments, the yields and FE for NH<sub>3</sub> were consistently lower than those for NH<sub>2</sub>OH, highlighting a pronounced selectivity towards NH<sub>2</sub>OH production.

To examine the effect of nitrate concentration on product selectivity while maintaining a constant pH of 1, experiments were conducted at an applied potential of -0.7 V vs. RHE using 0.1 M HNO<sub>3</sub> as the electrolyte and varying concentrations of KNO<sub>3</sub>; for the most dilute nitrate solution, a 0.05 M KNO3 solution was used with its pH adjusted to 1 using H<sub>2</sub>SO<sub>4</sub> (Fig. S7, ESI<sup>†</sup>). Fig. 3 illustrated the trends in product yield and FE with nitrate concentration at pH 1, demonstrating that the highest yield and FE of NH<sub>2</sub>OH were achieved at a nitrate concentration of 0.1 M. At a reduced nitrate concentration of 0.05 M, the diminished adsorption of nitrate anions on the Au surface, likely slowed the NO3RR reaction. Also at increased nitrate concentrations, a marked decline in NH<sub>2</sub>OH yield and FE were observed. Note that, the detected hydroxylamine concentration consistently decreases over time, likely due to its oxidation by HNO<sub>2</sub> in acidic medium (NH<sub>2</sub>OH +  $HNO_2 \rightarrow N_2O + 2H_2O$ ). This was confirmed by a control experiment where KNO2 was added to a 0.1 M HNO3 solution containing NH<sub>2</sub>OH. As shown in Fig. S8, (ESI<sup>+</sup>), there was a sharp drop in NH<sub>2</sub>OH concentration following the addition. The reduced yields for both NH<sub>2</sub>OH and NH<sub>3</sub> at higher nitrate concentrations are likely due to additional nitrate adsorbates obstructing the Au surface. It is assumed that adsorbed hydrogen or water is necessary for nitrate to undergo NH<sub>3</sub> conversion. Further analysis involved measuring the pH of the electrolyte solution post-reaction (Table S1, ESI†). Clearly, higher starting nitrate concentrations resulted in increased pH levels. Specifically, the pH increments post-reaction were ordered as follows: 0.1 M (pH = 1.30) < 0.3 M (pH = 1.73) < 0.3 M (pH = 1.0.5 M (pH = 1.96) < 0.7 M (pH = 2.20) < 1 M (pH = 2.74). The increased pH was attributed to the consumption of eight protons to produce  $NH_3OH^+$  and ten protons to produce  $NH_4^+$ , respectively.

To investigate the effect of pH on the selectivity and yield of electrocatalytic NO<sub>3</sub>RR over the Au electrode, we modulated the electrolyte's pH, adjusted  $H_2SO_4$  while keeping 0.1 M KNO<sub>3</sub> constant, and applied a potential of -0.7 V vs. RHE for 1 hour (Fig. S9, ESI†). Fig. 4A and B and Fig. S10 (ESI†) illustrated that the selectivity and yield of NH<sub>2</sub>OH and NH<sub>3</sub> significantly



**Fig. 3** Variation in NH<sub>2</sub>OH (A) and NH<sub>3</sub> (B) yield rates across different nitrate concentrations at pH 1; performance assessed at an applied potential of -0.7 V vs. RHE over a 2-hour reaction time; (C) yield rates and (D) faradaic efficiency of NH<sub>2</sub>OH and NH<sub>3</sub> across different nitrate concentrations at pH 1 with an applied potential of -0.7 V vs. RHE for a duration of 1 hour.

depended on the acidity of the solution, particularly at pH values below 0.5. The yield of  $NH_2OH$  notably increased from 63.5 µmol h<sup>-1</sup> cm<sup>-2</sup> at pH 2 to 333.1 µmol h<sup>-1</sup> cm<sup>-2</sup> at pH 0.3, but then decreased to 146.6 µmol h<sup>-1</sup> cm<sup>-2</sup> at pH 0. Meanwhile, the yield of  $NH_3$  consistently rose at lower electrolyte pH levels, with a significant uptick observed within the pH range of 0 to 0.5, culminating in a yield of 792.5 µmol h<sup>-1</sup> cm<sup>-2</sup> at pH 0. These data highlight the substantial impact of acidity on the



Fig. 4 Yield rates of NH<sub>2</sub>OH (A) and NH<sub>3</sub> (B) across various pH levels, assessed in a solution of 0.1 M KNO<sub>3</sub> with H<sub>2</sub>SO<sub>4</sub> adjusting the pH, at an applied potential of -0.7 V vs. RHE for a period of 1 hour; (C) the Gibbs free energy diagram for NO<sub>3</sub>RR on Au wire; (D) the possible NO<sub>3</sub>RR pathway on the Au electrode.

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performance and selectivity of the Au electrode in the reduction of nitrate. At more acidic conditions, there is an increased proton availability facilitating the reaction outlined in eqn (1) and (2) for NH<sub>2</sub>OH and NH<sub>3</sub> production. However, this also favors the competing HER.

To evaluate the stability of the Au wire, five consecutive cycles were performed in 0.1 M HNO<sub>3</sub> at -0.7 V vs. RHE, with each cycle lasting 1 hour. The consistent NH<sub>2</sub>OH yield rate and FE observed indicate the favorable stability of the Au electrode under these conditions (Fig. S11, ESI<sup>†</sup>). SEM analysis of the Au wire after reaction showed preserved surface microstructure, with no apparent damage observed (Fig. S12, ESI<sup>†</sup>). Furthermore, also the XRD patterns remained unchanged (Fig. S13, ESI†). The current response results from LSV remained similar except for a slight increase (Fig. S14, ESI<sup>+</sup>), which may be attributed to the improved activation of the catalyst. Elemental analysis via inductively coupled plasma mass spectrometry (ICP-MS) analysis evidenced that there was no detectable  $Au^{3+}$ leaching in the electrolyte after reaction (Table S2, ESI<sup>+</sup>). These results demonstrated that Au wire serves as a robust catalyst under acidic conditions for the NO<sub>3</sub>RR conversion to NH<sub>2</sub>OH and NH<sub>3</sub>.

To elucidate the mechanism of nitrate reduction on Au wire, density functional theory (DFT) calculations on Au (111) facet were performed. Fig. 4C details these simulations, which begins with the spontaneous adsorption of nitrate onto the Au electrode surface, marked by a favorable Gibbs free energy change of -0.75 eV. The reduction sequence involves adsorbed nitrate  $(NO_3^*)$  being reduced to adsorbed nitrite  $(NO_2^*)$  which is then converted to NO\*. The subsequent step involves the reduction of this adsorbed nitric oxide to hydroxylamine oxime (NOH\*), identified as the rate-determining step (RDS) in this pathway, requiring an energy of 0.35 eV. NOH\* is then further reduced to NHOH\*, NH2OH\* and finally NH2OH desorbes. Conversely, the formation of NH<sub>3</sub> from NHOH\* involves multiple steps beginning with NHOH\* first converting to NH\*, followed by NH2\*, then to NH3\* before NH3\* desorbs to produce NH<sub>3</sub> (Fig. 4D and Fig. S15, ESI<sup>†</sup>). The lower Gibbs free energies of the formation and the desorption of NH2OH\* indicate it occurs spontaneously, inherently favoring the formation of NH<sub>2</sub>OH (Table S3, ESI<sup>†</sup>). The relatively simplicity of the NH<sub>2</sub>OH pathway, compared to the multi-step process required for NH<sub>3</sub> formation, predominantly drives the selective formation of NH<sub>2</sub>OH. The energy barrier of the RDS from Au (0.35 eV) is lower than that of other reported catalysts, such as Ni (0.37 eV),<sup>17</sup> Rh (0.39 eV),<sup>17</sup> Pd (0.72 eV),<sup>17</sup> PdFe (0.74 eV),<sup>18</sup> Cu/Cu<sub>2</sub>O  $(0.84 \text{ eV})^{19}$  and Fe<sub>3</sub>C–Cu<sub>3</sub>  $(1.28 \text{ eV})^{20}$  (Table S4, ESI†).

In summary, this study establishes Au as a highly effective electrocatalyst for the selective  $NO_3^-$  reduction to  $NH_2OH$ . Through meticulous experimentation involving electrolyte composition, nitrate concentration, pH and applied potential, we achieved an  $NH_2OH$  yield of 230.1  $\pm$  19 µmol h<sup>-1</sup> cm<sup>-2</sup> under optimal conditions. This performance is notably exceeding the yields commonly reported in the literature and achieves a faradaic efficiency of  $34.2 \pm 2.8\%$  at -0.7 V vs. RHE, setting a

new benchmark in electrochemical nitrate reduction. This study provides an understanding of the electrolyte engineering of nitrate solutions and may motivate further studies into gold or other materials to selectively generate NH<sub>2</sub>OH and other products from waste nitrates.

This work is supported by Internal Funds KU Leuven (C14/23/090), the National Natural Science Foundation of China (No. 52303151, No. 52161135302, No. 52211530489), the Research Foundation of Flanders (FWO, No. G0F2322N, No. VS06523N, No. 1298323N, No. 1SA3321N). J. H acknowledges support of the MPI as a fellow.

#### Data availability

The data supporting this article have been included as part of ESI. $\dagger$ 

#### Conflicts of interest

There are no conflicts to declare.

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