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# Engineering *in situ*: N-doped porous carbon-confined FeF<sub>3</sub> for efficient lithium storage†

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Metal fluorides confined in heteroatom-doped carbon nanostructures are viewed as one of the most promising high capacity cathodes for high-performance lithium rechargeable batteries. Herein, we present a facile *in situ* reaction approach to synthesize nitrogen-doped porous carbon (NPC)-confined metal fluorides, which involves *in situ* etching toward a Schiff-base organic precursor and fluorination of metal oxides by polytetrafluoroethylene during a one-step heating process. The afforded NPC-confined FeF<sub>3</sub> (FeF<sub>3</sub>@NPC) facilitates fast Li<sup>+</sup>/e<sup>−</sup> diffusion kinetics, accommodates severe volume fluctuation and reduces the FeF<sub>3</sub> cathode dissolution, thus providing an outstanding high-rate capacity of 181 mA h g<sup>−1</sup> at 5 C, accompanied by superior cycle life within 500 cycles at 2 C. This novel approach opens up new horizons to design high-performance nanoconfined metal fluoride-based materials for sustainable energy applications.

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## Introduction

Lithium-metal fluoride batteries have attracted intensive research interest for prospective next-generation electrochemical energy-storage devices owing to their high theoretical energy density and operating voltage.<sup>1</sup> In recent years, lots of studies have been focused on revealing the reaction mechanisms and optimizing the electrochemical properties of metal fluoride cathodes (FeF<sub>3</sub>, CoF<sub>2</sub>, and CuF<sub>2</sub>).<sup>2,3</sup> Compared to Co and Cu, Fe possesses more abundant resources, and eco-friendly and low-cost properties. In addition, FeF<sub>3</sub>, as a typical member of the metal fluorides, has impressive advantages in terms of the considerable theoretical capacity (712 mA h g<sup>−1</sup>), energy density (1500 W h L<sup>−1</sup>), and high average potential (~2.74 V), which are conducive to future large-scale applications.<sup>4–6</sup> Despite these appealing features, the commercialization of Li-FeF<sub>3</sub> batteries is seriously hindered by multiple challenges, including the highly insulating electronic/ionic characteristics of FeF<sub>3</sub>, the significant volumetric change upon delithiation/lithiation, and the dissolution of FeF<sub>3</sub>

during cycling, which inevitably lead to limited high-rate capability and poor long-term cyclability.<sup>7–9</sup>

To circumvent the aforementioned challenges, numerous purposeful efforts have been committed to designing and preparing nanostructured conductive carbon matrices that serve as the coating or carrier of FeF<sub>3</sub>, such as mesoporous carbon, carbon spheres, heteroatom-doped carbon, carbon nanotubes, and graphene.<sup>10–15</sup>

Among a variety of carbons, heteroatom-doped carbon nanostructures containing confined FeF<sub>3</sub> have impressive merits: (i) carbon frameworks can improve the conductivity of FeF<sub>3</sub>; (ii) confined carbon-coated space can tolerate the volumetric changes of active materials; (iii) nano-confinement can reduce the metal fluoride cathode dissolution during cycling to some extent; and (iv) heteroatom doping can boost the lithium storage performance of FeF<sub>3</sub> owing to additional active sites for metal ion storage.<sup>16,17</sup> Nevertheless, the synthesis of nanoconfined heteroatom-doped carbon-coated FeF<sub>3</sub> usually involves complicated synthetic processes and toxic/corrosive gases (e.g., HF and NF<sub>3</sub>).<sup>18–20</sup> More importantly, deriving from *ex situ* synthesis methods, the conductive contact between FeF<sub>3</sub> and carbon matrices is quite weak. Thus, developing a simple, *in situ* engineering approach without using toxic/corrosive gases to prepare nanoconfined heteroatom-doped carbon-coated FeF<sub>3</sub> is highly desirable.

In this contribution, we propose a general approach for *in situ* synthesis of nitrogen-doped porous carbon-confined metal fluorides (e.g., FeF<sub>3</sub>@NPC, CoF<sub>2</sub>@NPC, CuF<sub>2</sub>@NPC, and AlF<sub>3</sub>@NPC), by a straightforward heating treatment using a Schiff-base organic precursor (SOP) as a carbon, nitrogen, and template agent source, metal oxides as metal precursors, and

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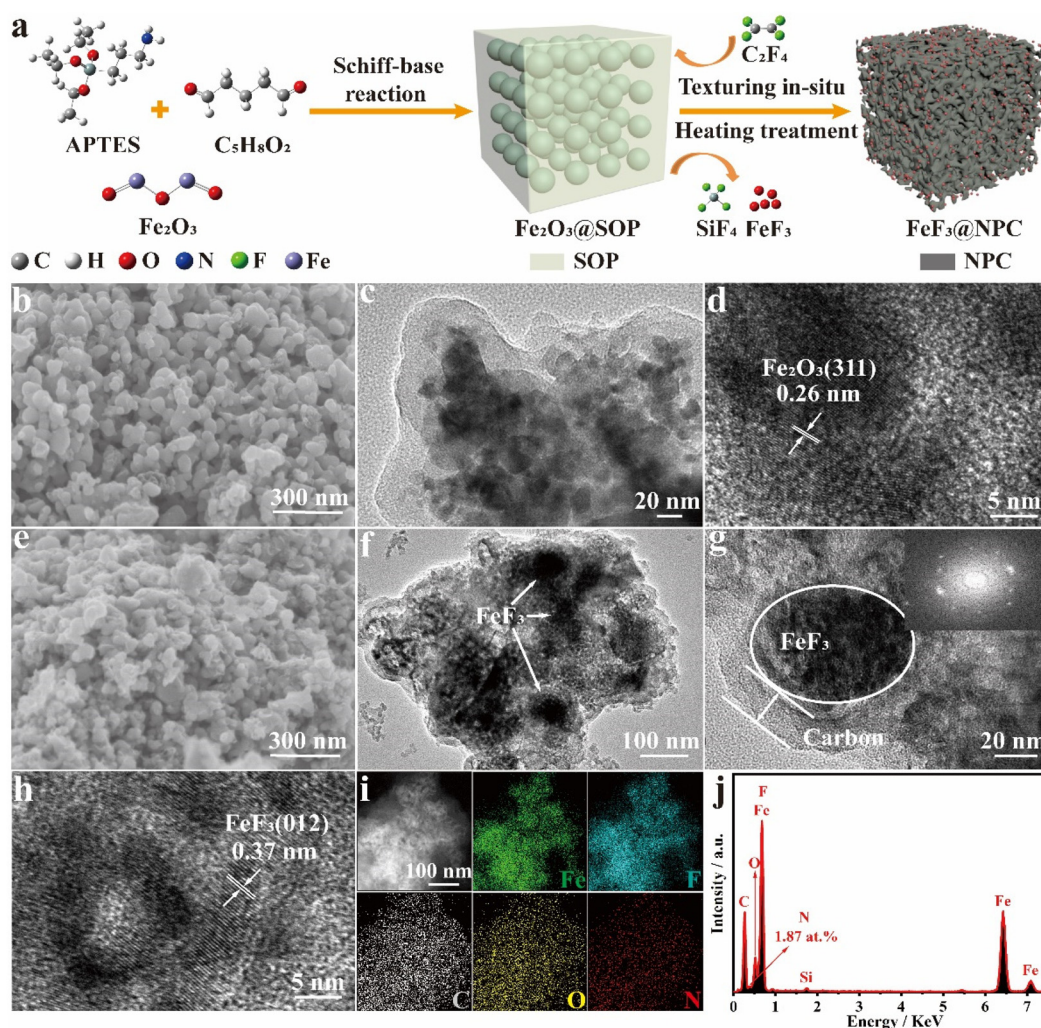


polytetrafluoroethylene (PTFE) as an etching and fluorinating agent. In a well-constructed  $\text{FeF}_3\text{@NPC}$  nanocomposite, a nitrogen-doped micro/mesoporous carbon shell surrounding the  $\text{FeF}_3$  nanoparticles enables good nanoconfinement ability, ideal conductive contact, high pore volume space, and suitable active sites for the  $\text{FeF}_3$  electrode, bringing about superior electrochemical performance. This novel strategy offers the possibility to design multifunctional carbon-confined metal fluoride materials in a facile, environmentally benign, and controllable way for efficient lithium rechargeable batteries.

## Results and discussion

Fig. 1a illustrates *in situ* synthesis toward  $\text{FeF}_3\text{@NPC}$ , involving a Schiff-base reaction between 3-aminopropyltriethoxysilane (APTES) and glutaraldehyde ( $\text{C}_5\text{H}_8\text{O}_2$ ) to generate SOP-encapsulated  $\text{Fe}_2\text{O}_3$  ( $\text{Fe}_2\text{O}_3\text{@SOP}$ ), followed by heating treatment to obtain  $\text{FeF}_3\text{@NPC}$ . During the heating process, PTFE can com-

pletely decompose at 606 °C to produce tetrafluoroethylene gas ( $\text{C}_2\text{F}_4$ ) (Fig. S1†),<sup>21</sup> which will fluorinate  $\text{Fe}_2\text{O}_3$  into  $\text{FeF}_3$  and react with Si/O elements of SOP to etch the SOP template, forming N-doped porous carbon-confined  $\text{FeF}_3$ . As shown in SEM and TEM images (Fig. 1b–d),  $\text{Fe}_2\text{O}_3\text{@SOP}$  shows an interconnected spheroidal morphology, with a spheroidal size of around 40–120 nm, and the pristine  $\text{Fe}_2\text{O}_3$  nanoparticles (Fig. S2†) are encapsulated within the SOP. After heating  $\text{Fe}_2\text{O}_3\text{@SOP}$ , for the as-prepared  $\text{FeF}_3\text{@NPC}$ , the morphology and spheroidal size are similar to those of  $\text{Fe}_2\text{O}_3\text{@SOP}$ , except that the  $\text{Fe}_2\text{O}_3$  nanoparticles and SOP are transformed into  $\text{FeF}_3$  nanoparticles and porous carbon, respectively (Fig. 1e/f). *In situ* formed carbon layers are uniformly coated surrounding the  $\text{FeF}_3$ , and the lattice fringe spacing of 0.37 nm can be ascribed to the (110) plane of the  $\text{FeF}_3$  phase (Fig. 1g/h).<sup>11</sup> The elemental mappings of  $\text{FeF}_3\text{@NPC}$  (Fig. 1i) show the homogeneous distribution of Fe, F, C, O and N elements and the overlapped F and Fe signals surrounded by the C signal. The extremely weak Si peak (0.53 at% for the residual Si content)



**Fig. 1** (a) Schematic illustration of  $\text{FeF}_3\text{@NPC}$  synthesis. (b) SEM, (c) TEM, and (d) HRTEM images of  $\text{Fe}_2\text{O}_3\text{@SOP}$ . (e) SEM image, (f and g) TEM images, (h) HRTEM image, (i) STEM and corresponding elemental mappings, and (j) EDX spectrum of  $\text{FeF}_3\text{@NPC}$ .



suggests the removal of Si in the SOP, and the N doping content in the FeF<sub>3</sub>@NPC is found to be 1.87 at% (Fig. 1j).

The diffraction peaks of FeF<sub>3</sub>@NPC are clearly indexed to FeF<sub>3</sub> (JCPDS No. 33-0647) (Fig. 2a), suggesting the successful conversion of Fe<sub>2</sub>O<sub>3</sub> into FeF<sub>3</sub>. In the FTIR spectra of FeF<sub>3</sub>@NPC (Fig. 2b), the peaks at 539 and 1265 cm<sup>-1</sup> correspond to the stretching vibrations of Fe-F and C-N, respectively,<sup>15,22</sup> further indicating the formation of FeF<sub>3</sub> and N doping of the carbon framework. The Raman spectrum of FeF<sub>3</sub>@NPC exhibits two intense peaks appearing at approximately 1361 cm<sup>-1</sup> (D-band) and 1581 cm<sup>-1</sup> (G-band) (Fig. S3†). The intensity ratio (*I<sub>D</sub>*/*I<sub>G</sub>*) is 1.01, implying that there are abundant structural defects in the FeF<sub>3</sub>@NPC,<sup>23</sup> thus favoring Li<sup>+</sup> transfer kinetics.<sup>24</sup> The electrical conductivity of FeF<sub>3</sub>@NPC evaluated by a four-point probe technique is 0.56 S cm<sup>-1</sup>, which is higher than that of pure FeF<sub>3</sub> ( $2.53 \times 10^{-9}$  S cm<sup>-1</sup>),<sup>25</sup> demonstrating the enhanced conductivity of FeF<sub>3</sub> with a N-doped porous carbon coating. The constituent element state occurring in FeF<sub>3</sub>@NPC was investigated by XPS (Fig. 2c), showing the presence of C, F, Fe, C, N, and O. The Fe 2p spectrum (Fig. 2d) exhibits Fe 2p<sub>1/2</sub> and Fe 2p<sub>3/2</sub> peaks appearing

at 728.8 and 714.9 eV, and their respective satellite peaks located at 721.1 and 710.1 eV, respectively, indicating that the Fe species in the FeF<sub>3</sub>@NPC are expressed as Fe<sup>3+</sup> valence states. The typical bonding type at 685.9 eV of the F 1s spectrum (Fig. 2e) corresponds to the F-Fe<sup>3+</sup> bonds,<sup>26</sup> further proving the formation of FeF<sub>3</sub>. The N 1s spectrum (Fig. 2f) shows three peaks corresponding to graphitic N, pyridinic N, and pyrrolic N, which is conducive to enhancing the electronic conductivity and active material absorbability of the carbon matrix.<sup>27,28</sup> The C 1s spectrum (Fig. 2g) shows four evident peaks corresponding to C-C, C-N/C-O, O-C=O, and C-F,<sup>29</sup> where the former three can be ascribed to carbonization of SOP, and the fourth is caused by the slight fluorination of carbon. The N<sub>2</sub> sorption analysis of FeF<sub>3</sub>@NPC presents hierarchical micro-mesoporous structures, which is affirmed using pore-size distribution (Fig. 2h).<sup>24,30</sup> Two different kinds of pores are created from the *in situ* concurrent PTFE-based etching and fluorination. The specific surface area of FeF<sub>3</sub>@NPC is determined to be as high as 167.1 m<sup>2</sup> g<sup>-1</sup>, together with the pore volume of 0.32 cm<sup>3</sup> g<sup>-1</sup>. The air-exposed TGA curve of FeF<sub>3</sub>@NPC shows a mass loss between 50 and

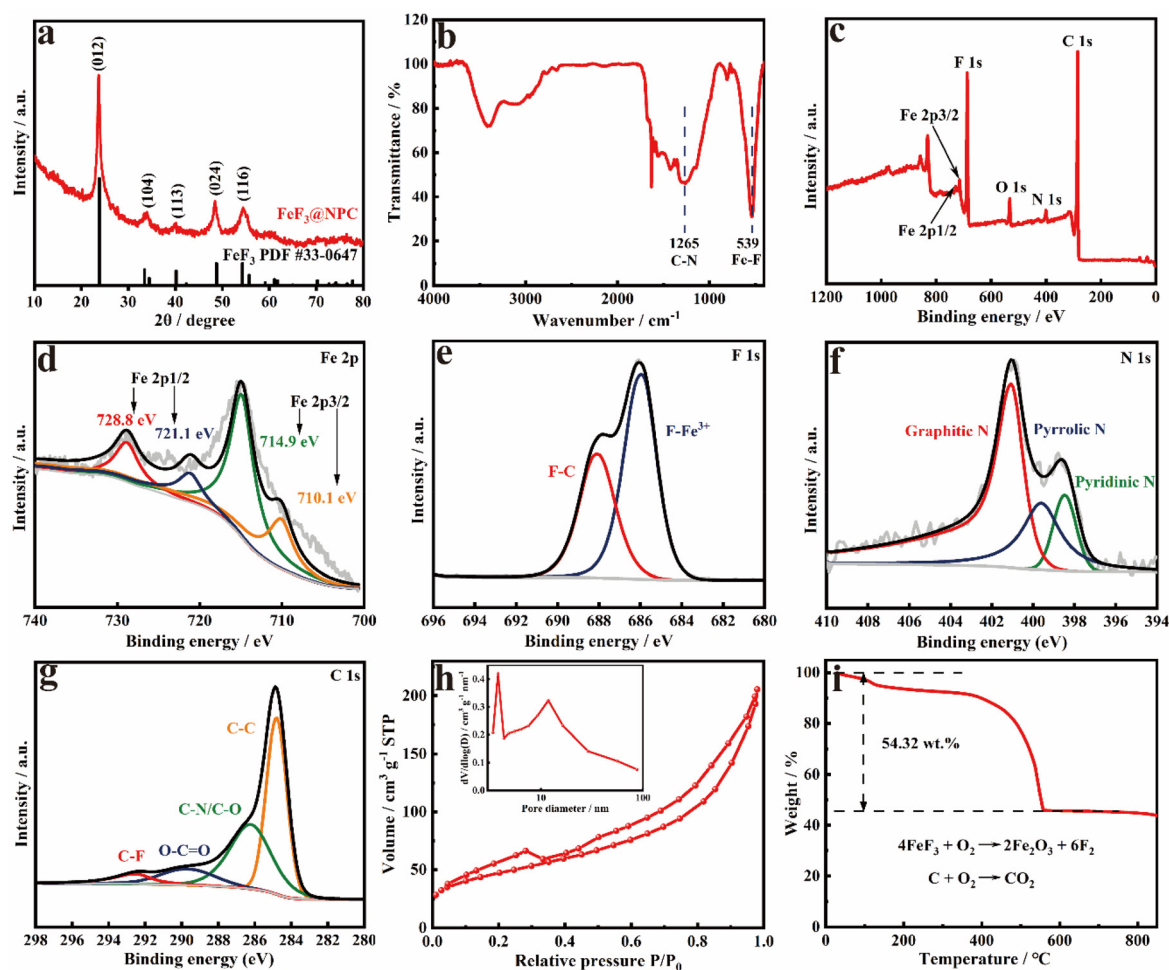


Fig. 2 (a) XRD patterns, (b) FTIR spectra, (c) XPS survey spectrum, (d) Fe 2p, (e) F 1s, (f) N 1s and (g) C 1s XPS spectra, (h) N<sub>2</sub> sorption isotherm and pore size distribution, and (i) TGA curve in air of FeF<sub>3</sub>@NPC.





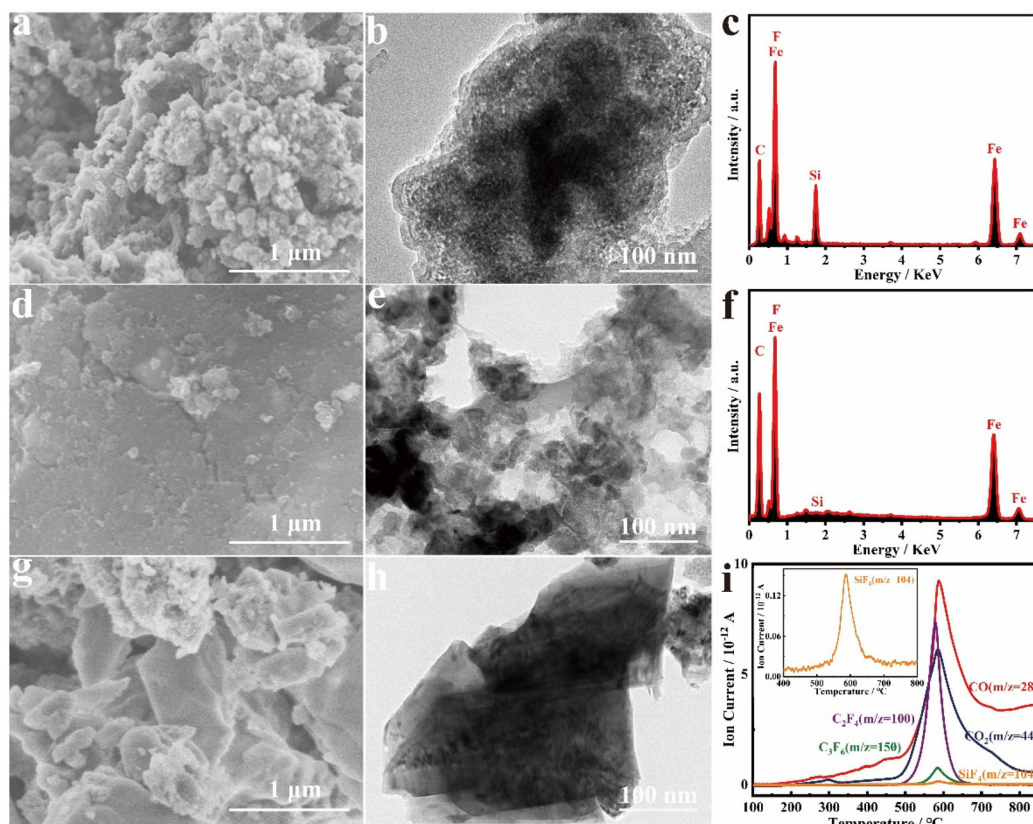
800 °C (Fig. 2i), demonstrating that the residue ( $\text{Fe}_2\text{O}_3$ ) at 800 °C is 54.32 wt%. Accordingly, it is determined that the content of  $\text{FeF}_3$  in  $\text{FeF}_3\text{@NPC}$  is 64.55 wt%.

The effects of the mass ratio of PTFE to  $\text{Fe}_2\text{O}_3\text{@SOP}$  and heat treatment temperature on the formation of  $\text{FeF}_3\text{@NPC}$  were explored. As the mass ratio of  $\text{PTFE}/\text{Fe}_2\text{O}_3\text{@SOP}$  decreases from 6:1 to 3:1, the interconnected spheroidal morphology remains unchanged (Fig. 3a/b), but Si in the SOP cannot be completely etched, which can be shown by EDS analysis (Fig. 3c). On increasing the mass ratio of  $\text{PTFE}/\text{Fe}_2\text{O}_3\text{@SOP}$  to 10:1, the interconnected spheroidal shape collapses and the carbon content increases (Fig. 3d–f), implying a decrease of the active substance  $\text{FeF}_3$ . Thus, PTFE is critical for creating a nanoconfined spheroidal carbon shell and tuning the  $\text{FeF}_3$  content. Increasing the heating temperature to 800 °C, the spheroidal  $\text{FeF}_3\text{@NPC}$  nanoparticles are aggregated into a blocky morphology (Fig. 3g/h), which indicates that a higher heating temperature affects the regular morphology of  $\text{FeF}_3\text{@NPC}$ . To further explore the formation of  $\text{FeF}_3\text{@NPC}$ , TG and gas emission curves of the PTFE and  $\text{Fe}_2\text{O}_3\text{@SOP}$  mixture were constructed. The TG curve (Fig. S4†) shows that PTFE and  $\text{Fe}_2\text{O}_3\text{@SOP}$  react violently at around 580 °C, which can be attributed to the fluorination of  $\text{Fe}_2\text{O}_3$

based on the major gas product ( $\text{C}_2\text{F}_4$ ) of PTFE in the pyrolysis process and the etching of Si in the SOP through the reaction of Si with  $\text{C}_2\text{F}_4$  to generate  $\text{SiF}_4$  (g) (Fig. 3i),<sup>24,31</sup> resulting in the formation of  $\text{FeF}_3\text{@NPC}$ .

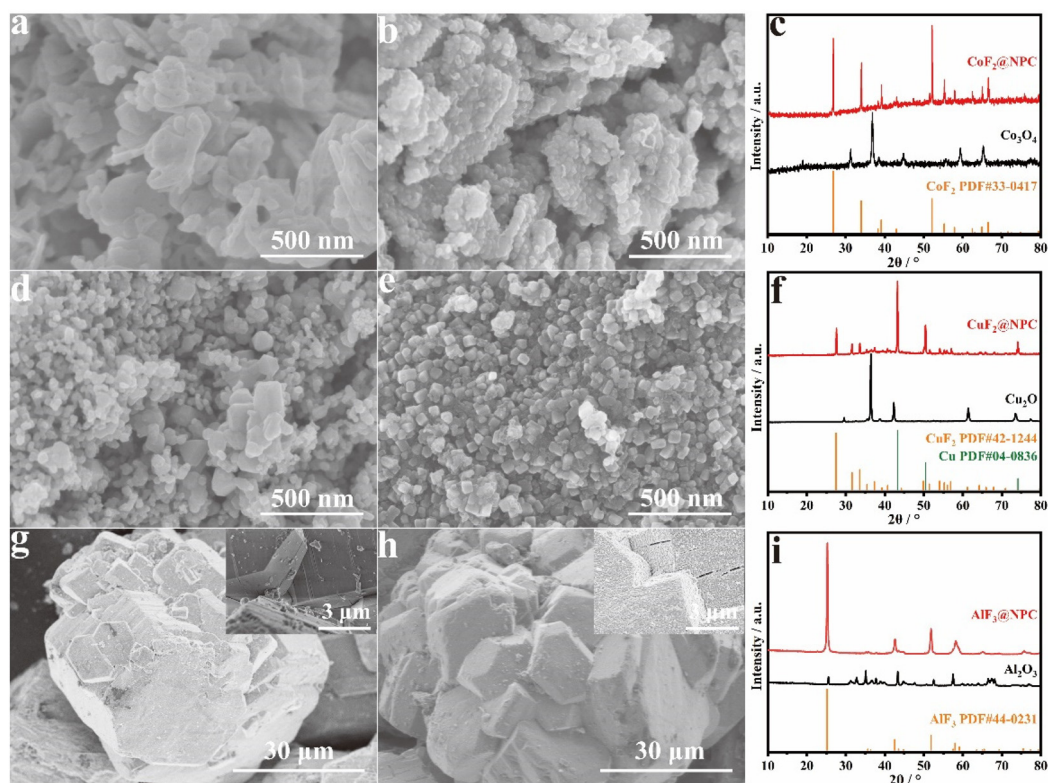
The successful synthesis of  $\text{FeF}_3\text{@NPC}$  has inspired us to explore the possibility of utilizing the *in situ* reaction approach in the preparation of other N-doped porous carbon-confined metal fluorides. Indeed, as seen in the SEM images and XRD patterns shown in Fig. 4,  $\text{CoF}_2\text{@NPC}$ ,  $\text{CuF}_2\text{@NPC}$ , and  $\text{AlF}_3\text{@NPC}$  can be easily synthesized using common metal oxides such as  $\text{Co}_3\text{O}_4$ ,  $\text{Cu}_2\text{O}$  and  $\text{Al}_2\text{O}_3$ , respectively, which can be further supported by the EDS spectra of  $\text{CoF}_2\text{@NPC}$ ,  $\text{CuF}_2\text{@NPC}$ , and  $\text{AlF}_3\text{@NPC}$  (Fig. S5–7†).

To systematically assess the electrochemical properties of  $\text{FeF}_3\text{@NPC}$ ,  $\text{FeF}_3\text{@NPC}/\text{Li}$  cells with an  $\text{FeF}_3\text{@NPC}$  cathode were constructed. The CV profiles of the  $\text{FeF}_3\text{@NPC}$  cathode in the initial cathodic sweep show a pair of cathodic/anodic peaks at 2.93/3.15 V (Fig. 5a), which correspond to lithiation/delithiation of the  $\text{FeF}_3$  crystal structure, respectively.<sup>32,33</sup> An additional pair of cathodic/anodic peaks at 3.28/3.40 V is exhibited, relating to the redox reactions of  $\text{Li}^+$  with  $\text{FeF}_3$  to form the  $\text{Li}_{0.5}\text{FeF}_3$  intermediate.<sup>34</sup> The cathodic/anodic peaks are almost overlapped during the subsequent cycles, implying



**Fig. 3** (a) SEM image, (b) TEM image, and (c) EDX spectrum of the product obtained by the mass ratio of  $\text{PTFE}/\text{Fe}_2\text{O}_3\text{@SOP} = 3:1$ . (d) SEM image, (e) TEM image, and (f) EDX spectrum of the product obtained by the mass ratio of  $\text{PTFE}/\text{Fe}_2\text{O}_3\text{@SOP} = 10:1$ . (g) SEM image, and (h) TEM image of the product obtained under 800 °C. (i) Gas emission curves of PTFE and  $\text{Fe}_2\text{O}_3\text{@SOP}$  mixture during the pyrolysis process.





**Fig. 4** (a) SEM image of  $\text{Co}_3\text{O}_4$ , (b) SEM image, and (c) XRD patterns of  $\text{CoF}_2@\text{NPC}$ . (d) SEM image of  $\text{Cu}_2\text{O}$ , (e) SEM image, and (f) XRD patterns of  $\text{CuF}_2@\text{NPC}$ . (g) SEM image of  $\text{Al}_2\text{O}_3$ , (h) SEM image and (i) XRD patterns of  $\text{AlF}_3@\text{NPC}$ .

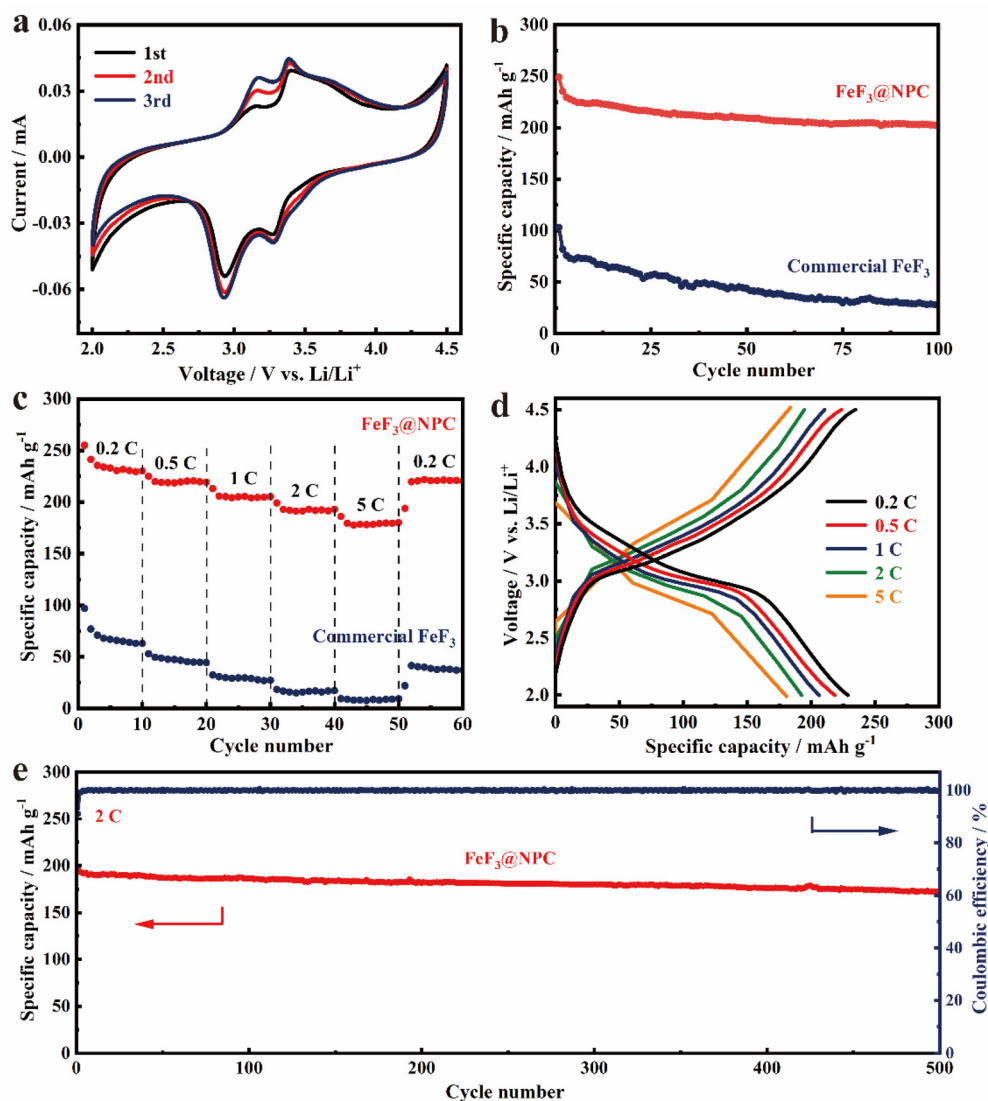
excellent electrochemical stability of  $\text{FeF}_3@\text{NPC}$ . The cycling performance of  $\text{FeF}_3@\text{NPC}$  and commercial  $\text{FeF}_3$  cathodes is presented in Fig. 5b. The  $\text{FeF}_3@\text{NPC}$  cathode delivers excellent specific capacities of 249 and 203  $\text{mA h g}^{-1}$  at 0.2 C over 1 and 100 cycles, respectively. In contrast, the commercial  $\text{FeF}_3$  cathode suffers significant capacity decay, and only maintains a low capacity of 29  $\text{mA h g}^{-1}$  over 100 cycles, attributable to poor mechanical and interfacial stability. In addition, the specific capacity of the NPC cathode is only 16  $\text{mA h g}^{-1}$  over 100 cycles (Fig. S8†), revealing that the capacity contribution of NPC can be negligible. Compared with reported  $\text{FeF}_3$  cathode materials, the  $\text{FeF}_3@\text{NPC}$  cathode showcases comparable or better electrochemical properties (Table S1†). The rate capability of the  $\text{FeF}_3@\text{NPC}$  cathode is presented at different C-rates (Fig. 5c/d). At varying C-rates from 0.2 to 5 C, the  $\text{FeF}_3@\text{NPC}$  cathode exhibits high specific capacities of 229, 218, 205, 193, and 181  $\text{mA h g}^{-1}$ , respectively. As the current returns to 0.2 C, a high reversible capacity of 221  $\text{mA h g}^{-1}$  can be recovered. In sharp contrast, the commercial  $\text{FeF}_3$  cathode delivers ultralow capabilities of 63, 44, 27, 18, and 9  $\text{mA h g}^{-1}$ , respectively, signifying the outstanding rate capability of  $\text{FeF}_3@\text{NPC}$ . This good rate performance proves the improved electrochemical kinetics and rapid electronic/ionic transport characteristics of  $\text{FeF}_3@\text{NPC}$ , which can be buttressed by the relatively low charge-transfer resistance ( $R_{\text{ct}}$ ) (Fig. S9†). The long cycle life of the  $\text{FeF}_3@\text{NPC}$  cathode was evaluated at 2 C

(Fig. 5g). The  $\text{FeF}_3@\text{NPC}$  cathode preserves a stable reversible capacity of 172  $\text{mA h g}^{-1}$  over 500 cycles of charge/discharge, corresponding to a superior capacity retention of 86.9% and a low capacity decay of 0.026%  $\text{cycle}^{-1}$ , accompanied by an almost 100% coulombic efficiency, evidencing the structural advantage of  $\text{FeF}_3@\text{NPC}$ .

The integrity of the  $\text{FeF}_3@\text{NPC}$  cathode after cycling was investigated with the postmortem SEM analysis (Fig. 6a/b and S10†). After the cycling test, the  $\text{FeF}_3@\text{NPC}$  cathode well maintains its original morphology without cracks, revealing the structural integrity of the cathode. The elemental analysis and TEM image of the cycled  $\text{FeF}_3@\text{NPC}$  cathode (Fig. 6c/d) show that the C, F and Fe elements are still homogeneously distributed in the carbon conduction network, and the N-doped porous carbon shell surrounding the  $\text{FeF}_3$  nanoparticles remains intact, further indicating good robustness of the cathode and effective prevention of  $\text{FeF}_3$  dissolution into the electrolyte. Compared to the  $\text{FeF}_3@\text{NPC}$  cathode before cycling, the thickness variation of the cycled  $\text{FeF}_3@\text{NPC}$  cathode is only 11.2% (Fig. 6e/f), implying that the well-constructed  $\text{FeF}_3@\text{NPC}$  nanocomposite can effectively accommodate severe volume fluctuation of  $\text{FeF}_3$ . Thus, the resulting  $\text{FeF}_3@\text{NPC}/\text{Li}$  batteries present excellent lithium storage performance.

To investigate the electrochemical kinetics of the  $\text{FeF}_3@\text{NPC}$  cathode, CV curves at different scanning rates (0.2,





**Fig. 5** (a) CV curves of  $\text{FeF}_3\text{@NPC}$  at  $0.2 \text{ mV s}^{-1}$ . (b) Cycling performance of  $\text{FeF}_3\text{@NPC}$  and commercial  $\text{FeF}_3$  at  $0.2 \text{ C}$ . (c) Rate performance of  $\text{FeF}_3\text{@NPC}$  and commercial  $\text{FeF}_3$  at different rates from  $0.2 \text{ C}$  to  $5 \text{ C}$ . (d) Voltage profiles of  $\text{FeF}_3\text{@NPC}$  at different current densities. (e) Long-term cycling performance of  $\text{FeF}_3\text{@NPC}$  at  $2 \text{ C}$ .

$0.3, 0.4, 0.5, 0.6, 0.7, 0.8$ , and  $0.9 \text{ mV s}^{-1}$ ) are presented in Fig. 7a. All the CV curves maintain the same trend, and the redox current intensity increases with the upswing of scanning rates, demonstrating the reversibility of the electrochemical conversion reaction for the  $\text{FeF}_3\text{@NPC}$  cathode.<sup>20</sup> Moreover, the slight redox peak shifts imply that the  $\text{FeF}_3\text{@NPC}$  cathode possesses fast kinetics. The relationship between the current ( $i$ ) and the scanning rate ( $\nu$ ) obeys eqn (1) and (2):<sup>35</sup>

$$i = a\nu^b \quad (1)$$

$$\log(i) = b \log(\nu) + \log(a) \quad (2)$$

where  $b$  represents the  $\text{Li}^+$  storage coefficient. The  $\log(\nu) - \log(i)$  plots of the  $\text{FeF}_3\text{@NPC}$  cathode (Fig. 7b) show that the calculated  $b$ -values of the anodic and cathodic peaks are  $0.82$  and  $0.67$ , indicating considerable capacitive characteristics of

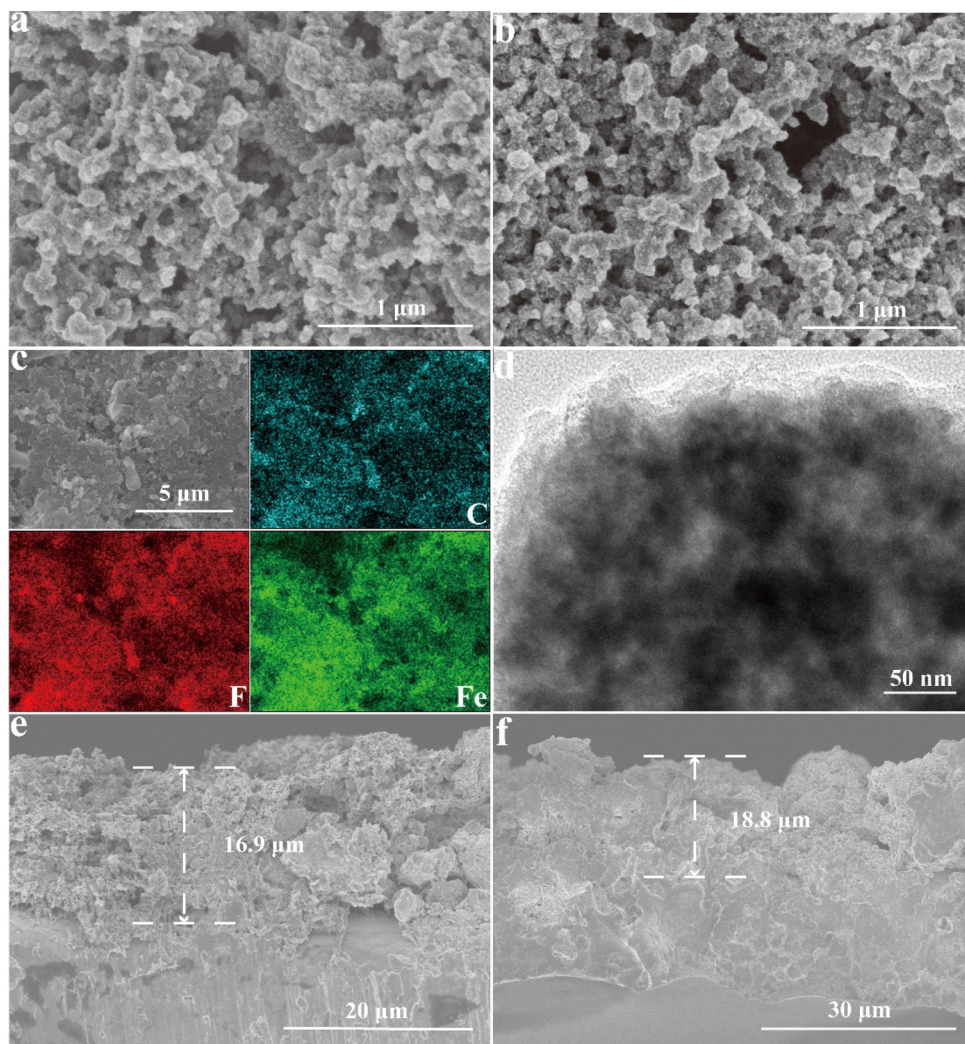
$\text{FeF}_3\text{@NPC}$ . The contribution rate of  $\text{Li}^+$  capacitance can be quantified through eqn (3):<sup>36</sup>

$$i(V) = k_1\nu + k_2\nu^{1/2} \quad (3)$$

where  $i(V)$  represents the combination of capacitive contribution ( $k_1\nu$ ) and diffusion-controlled contribution ( $k_2\nu^{1/2}$ ). A typical capacitive contribution at  $0.9 \text{ mV s}^{-1}$  is presented in Fig. 7c, and the variation of capacitive contribution and diffusion contribution under different scanning rates for  $\text{FeF}_3\text{@NPC}$  is shown in Fig. 7d. Obviously, as the scanning rates increase, the capacitive contribution rises gradually, accompanied by reduced diffusion contribution. The pseudo-capacitive contribution of the  $\text{FeF}_3\text{@NPC}$  cathode can reach up to  $75\%$ . The superior pseudocapacitive properties facilitate







**Fig. 6** (a and b) SEM images of the  $\text{FeF}_3$ @NPC cathode before and after 100 cycles. (c) EDS elemental mappings, and (d) TEM image of the  $\text{FeF}_3$ @NPC cathode after 100 cycles. (e and f) Cross-sectional SEM images of the  $\text{FeF}_3$ @NPC cathode before and after 100 cycles.

fast  $\text{Li}^+$  storage, thus endowing the  $\text{FeF}_3$ @NPC cathode with outstanding cycle life and high-rate capability.

## Experimental

### Chemicals and materials

Polytetrafluoroethylene (PTFE),  $\text{Fe}_2\text{O}_3$  powder,  $\text{Co}_3\text{O}_4$  powder,  $\text{Cu}_2\text{O}$  powder,  $\text{Al}_2\text{O}_3$  powder, glutaraldehyde solution (50% in  $\text{H}_2\text{O}$ ), 3-aminopropyltriethoxysilane (APTES), commercial  $\text{FeF}_3$ , *N*-methyl pyrrolidone (NMP), and polyvinylidene fluoride (PVDF) were purchased from Aladdin (China). Acetylene black (AB) was offered from Guangzhou Lithium Force Energy Technology Co. (China), commercial electrolyte using EC/DMC/DEC (v/v/v = 1:1:1) solvent with 1 M  $\text{LiPF}_6$  was purchased from Shanghai Xiaoyuan Energy Technology Co. (China).

### Synthesis of $\text{Fe}_2\text{O}_3$ @SOP

APTES (2.66 g, 12.0 mmol) and  $\text{Fe}_2\text{O}_3$  (2.87 g, 18.0 mmol) were placed in a 500 mL glass bottle with  $\text{C}_2\text{H}_5\text{OH}/\text{H}_2\text{O}$  (v/v = 60 mL : 240 mL) and stirred for 1 h. Then, glutaraldehyde solution (50% in  $\text{H}_2\text{O}$ , 2.40 g, 12.0 mmol) was added dropwise and kept under vigorous stirring for 6 h. The precipitate was washed with  $\text{C}_2\text{H}_5\text{OH}/\text{H}_2\text{O}$  and subsequently dried at 80 °C, yielding a Schiff-base organic precursor containing  $\text{Fe}_2\text{O}_3$ , *i.e.*,  $\text{Fe}_2\text{O}_3$ @SOP.

### Synthesis of $\text{FeF}_3$ @NPC

0.5 g of  $\text{Fe}_2\text{O}_3$ @SOP and 3.0 g of PTFE powder were well ground for 0.5 h, and then calcined at 650 °C for 4 h under an Ar atmosphere to obtain  $\text{FeF}_3$ @NPC. Other NPC-confined metal fluorides were synthesized *via* the same procedures with different metallic oxides.



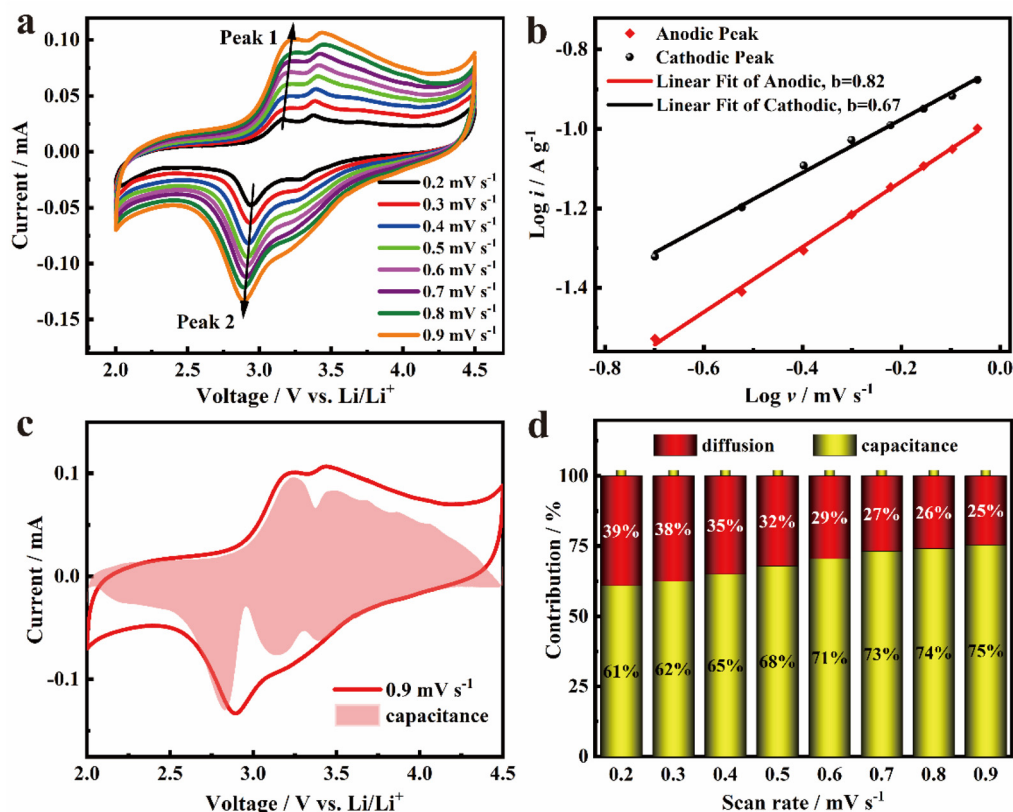


Fig. 7 (a) CV curves at different scanning rates; (b) the fitted  $b$  values determined by the peak current and scanning rate; (c) schematic diagram of the capacitive contribution at  $0.9 \text{ mV s}^{-1}$ ; and (d) capacity contribution ratio at various scanning rates of  $\text{FeF}_3\text{@NPC}$ .

## Material characterization

The surface morphology, elemental mapping, and micro-structure characterization were analyzed using a transmission electron microscope (TEM, Hitachi S-4800) and a scanning electron microscope (SEM, Hitachi S-4800). The chemical states were collected using an X-ray photoelectron spectrometer (XPS, ESCALAB250). The conductivity was measured using a four-point probe instrument (RTS-9). FTIR spectra were recorded using a Nicolet iS50. The crystal structures were obtained using an X-ray diffractometer (XRD, X'Pert Pro MPD) and a Raman spectrometer (HORIBA Jobin Yvon). The  $\text{N}_2$  adsorption isotherm and pore-size distribution were tested on an SI-MP-10. Pyrolysis characteristics were analysed on a TG-MS analyzer (STA449 F3). Thermogravimetric analysis (TGA) was performed using a PCPFEIFFER VACUUMTGA-7 analyzer.

## Electrochemical measurement

To prepare the electrode, a mixture of 80 wt%  $\text{FeF}_3\text{@NPC}$  or commercial  $\text{FeF}_3$ , 10 wt% acetylene black (AB) conductive agent, and 10 wt% polyvinylidene fluoride (PVDF) binder in  $N$ -methyl pyrrolidone (NMP) was cast on aluminum foil and dried at  $90^\circ\text{C}$  for 12 h. The  $\text{FeF}_3$  mass loading was approximately  $1.2\text{--}1.6 \text{ mg cm}^{-2}$ . A 2025-type coin cell assembly was

conducted inside an Ar-filled glovebox (Mikrouna) by using  $\text{FeF}_3\text{@NPC}$  or commercial  $\text{FeF}_3$  as the cathode, lithium sheet as the anode, polypropylene membrane as the separator, and 1 M  $\text{LiPF}_6/\text{EC}:\text{DMC}:\text{DEC}$  ( $v/v/v = 1:1:1$ ) as the electrolyte. Cyclic voltammetry (CV) measurements ( $0.2 \text{ mV s}^{-1}$ , 2.0–4.5 V) and electrochemical impedance spectroscopy (EIS) measurements (0.01 Hz to 0.1 MHz) were recorded using a Zahner IM6 electrochemical workstation. The galvanostatic discharge/charge tests were conducted using a Neware multichannel battery system. The electrochemical capacities of the electrodes were based on the mass of  $\text{FeF}_3$ .

## Conclusions

In summary, an innovative *in situ* synthetic approach is proposed to make N-doped porous carbon-confined metal fluorides. The afforded  $\text{FeF}_3\text{@NPC}$  with a confined N-doped carbon-coated space can facilitate fast  $\text{Li}^+/\text{e}^-$  diffusion kinetics, buffer severe volume fluctuation and prevent the active substance  $\text{FeF}_3$  from interacting with the electrolyte, thus enabling a high capacity utilization of  $249 \text{ mA h g}^{-1}$  at 0.2 C, together with remarkable C-rate capability and excellent cycle life. This work opens up an efficient pathway for developing nanocon-





fined metal fluoride-based materials to improve lithium batteries.

## Author contributions

Jinlong Hu: conceptualization, methodology, investigation, formal analysis, writing – original draft, and writing – review & editing. Weijun Xu: resources and software. Lingzhi Zhang: supervision and writing – review & editing.

## Data availability

The data supporting this article have been included as part of the ESI.†

The data that support the findings of this study are available from the corresponding author upon reasonable request.

## Conflicts of interest

There are no conflicts to declare.

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