


 Cite this: *RSC Adv.*, 2024, 14, 6234

# Experimental study of the effects of a magnetic field/magnetic field-ferromagnetic nanocomposite pour point depressant on wax deposition†

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A magnetic field and pour point depressant, as a new avenue for improving the submarine pipeline flow of waxy oils, has attracted increasing attention along with the development of efficient wax mitigation techniques. Although advances have been made recently in understanding the rheological behavior and crystallization properties of waxy oils, the effect of magnetic field and pour point depressants on wax deposition remains an open question. In this work, a ferromagnetic nanocomposite pour point depressant (FNPPD) was prepared. The variations in wax deposition mass and component under the effect of different magnetic treatments and magnetic field-FNPPDs were investigated using cold fingers and high-temperature gas chromatography. It was evident that both the high-intensity and high-frequency magnetic fields generated by the magnet and magnetic coil can effectively reduce the deposition mass and have a long-term magnetic history effect. The synergistic effect of magnetic fields and FNPPDs concurrently reduced the thickness/mass and wax content in the deposition layer, as compared to the individual use of magnetic fields or FNPPDs. The wax precipitation properties and wax crystal morphology of waxy oils under the action of the magnetic field were characterized by differential scanning calorimetry, focused beam reflectance measurement and polarizing microscopy experiments, and the mechanism of the magnetic field was elaborated from the perspective of crystallization kinetics by combining the fitting analysis of Avrami and size-independent growth model.

Received 27th December 2023

Accepted 1st February 2024

DOI: 10.1039/d3ra08875h

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## 1. Introduction

The prevalence of wax deposition raises a very urgent need in the field of the flow assurance of waxy oils in pipelines to explore wax mitigation techniques including various physical (heating, electric and magnetic fields, and mixing/dilution)<sup>1,2</sup> and chemical treatments (pour point depressants and microorganisms).<sup>3,4</sup> The magnetic fields and pour point depressants have recently received attention due to their cost-effectiveness compared to other techniques.<sup>5,6</sup> The magnetic fields used in waxy oils mainly include electromagnetic coils and permanent magnets.<sup>7,8</sup> Based on these two types of magnetic processing equipment, scholars have explored the influencing factors of magnetic field intensity, frequency, treatment temperature and time, *etc.*<sup>9–11</sup>

Chen *et al.*<sup>12</sup> measured the viscosity of a variety of Chinese crude oils using a magnetic rheometer at different magnetic field intensities (0–1 T). At 1 T, the viscosity of highly paraffinic oil and heavy oil was comparatively low, and the viscosity reduction efficiency could reach 13–26%. The viscosity reduction mechanism of the magnetic field was proposed by the morphology of suspended crude oil particles. Other factors are also thought to affect magnetic treatment efficiency.<sup>13</sup> The viscosity of waxy oils under different magnetic treatment conditions such as treatment temperature, shear rate, and intensity of magnetic field were compared.<sup>14,15</sup> The viscosity reduction efficiency increased with the decrease in magnetic treatment temperature or shear rate. Through the cold finger wax deposition experiment, Wen *et al.*<sup>15</sup> preliminarily found the inhibition of magnetic treatment on wax deposition mass and rate. It was suggested that the magnetic field promoting the nucleation of wax crystal was the major cause of reducing viscosity and inhibiting deposition of magnetized oil, as observed using a polarizing microscope. In addition to the magnetic coil used by these scholars, Nguyen *et al.*<sup>16</sup> studied the deposition and viscosity reduction efficiency of Vietnam crude oil under the action of neodymium–iron–boron (Nd–Fe–B) magnets. A few seconds (<5 s) of magnetization treatment can effectively reduce the viscosity, and the magnet inhibition

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† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d3ra08875h>



deposition efficiency can reach 20–25% in a flowline apparatus. It was also found that magnetic treatment has a better viscosity reduction effect on waxy crude oil with high resin and asphaltene contents.

The magnetic field frequency has been paid sufficient attention in most previous studies and it deserves further investigation. The thermal effect of high-frequency magnetic field was widely used due to its uniform heating, energy conservation, high efficiency, and controllable process.<sup>17–19</sup> The synergistic application of ferromagnetic nanoparticles and a high-frequency magnetic field on the biomedical industry is certainly the most mature, mainly used in organ transplantation,<sup>20,21</sup> cancer treatment,<sup>22,23</sup> and so on.

Andreina *et al.*<sup>24</sup> found that the magnetocaloric effect was decided by the intensity and frequency of the magnetic field rather than the nanoparticle size and composition. Ferromagnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles (10 mg Fe per mL) can achieve high-temperature rise rates of up to 321 °C min<sup>-1</sup> under the 42.5 kA m<sup>-1</sup>, 278 kHz alternating magnetic field. Prachi *et al.*<sup>25</sup> first tried to apply the magnetocaloric effect for flow assurance in subsea flowlines. He embedded ferromagnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles into the inner wall coating of the submarine pipe. Under the action of the high-frequency alternating magnetic field, the nano-coating on the inner surface of the pipeline can generate heat, so as to prevent the formation of methane hydrate and wax. It was found that ferromagnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles dispersed in solutions or embedded in the coating had a similar magnetocaloric effect. The magnetocaloric efficiency of pipelines in the flowing state was about 5–8 times higher than that in the static state. The synergy of magnetic field and pour point depressant can provide a new way for inhibition of wax deposition in oil and gas pipelines. Huang *et al.*<sup>26</sup> studied the effects of magnetic field intensity and frequency on the yield stress of waxy oils and waxy oils with nanocomposite pour point depressants under an alternating magnetic field. The reduction rate of yield stress of magnetized doped waxy oils up to 80% was double that of waxy oils under the magnetic field.

The inhibition of magnetic treatment on wax deposition motivated extensive research, which nevertheless did not culminate in a satisfactory understanding of the characteristics and mechanism of wax deposition layer under magnetic treatment. Moreover, the effect of magnetic field-ferromagnetic nanocomposite pour point depressant (FNPPD) synergy on wax deposition remains an open question. In this article, the effects of different magnetic treatments (high-frequency electromagnetic coil and Nd–Fe–B magnet) and magnetic field-FNPPD on the variation in wax deposition mass and component were investigated using cold fingers and HTGC. The FNPPD hybrid of nano iron oxide particles and EVA copolymers was prepared, and the deposition characteristics of waxy oils under the synergistic action of magnetic field and FNPPD were explored. The combined wax precipitation characteristic experiments, Avrami and size-independent growth theory, were used to analyze the mechanism of the magnetic field on wax deposition.

## 2. Materials and methods

### 2.1. Materials

The waxy oil contained 10 wt% paraffin wax and model oil (D80) with a wax appearance temperature of 28.3 °C (Fig. 9a). At 35 °C, the viscosity was 1.18 mPa s. The paraffin wax was produced by Daqing Refining and Chemical Company, with a carbon number distribution range of C25–C41.<sup>27</sup> The wax precipitation characteristic curve of the waxy model oil at different temperatures is shown in Fig. 9b.

The ferromagnetic nanocomposite pour point depressant (FNPPD) used in our experiments was synthesized by the ultrasonic blending of organically modified ferromagnetism nanoparticles Fe<sub>3</sub>O<sub>4</sub> and ethylene/vinyl acetate copolymers. Ferromagnetism nanoparticles Fe<sub>3</sub>O<sub>4</sub> (20 nm) and ethylene/vinyl acetate copolymers (VA content 32 wt%) were purchased from Beijing InnoChem Science & Technology Co., Ltd. In order to improve the dispersion of nanoparticles, organically modified magnetic nanoparticles were prepared by a modified silica coating method, which was obtained by hydrolysis of tetraethyl orthosilicate and methacryloxy propyl trimethoxy silane and followed by the surface radical polymerization reaction of methyl methacrylate. For more details on synthetic processes and methodologies of the FNPPD, we referred the reader to recent articles by Frickel *et al.*<sup>28</sup> and Nayeem *et al.*<sup>29</sup> To ensure the homogeneity of the nanocomposites, EVA copolymers were dissolved in a D130 model oil at a concentration of 3 wt%, followed by ultrasonic processing with organically modified ferromagnetism nanoparticles at 40 kHz for 2 h. Then, EVA copolymers and nanoparticles in a mass ratio of 5/1 were added to the waxy oil for our experiments.

### 2.2. Methods

**2.2.1 Cold finger deposition experiments.** A cold finger apparatus was used to study the wax deposition of the undoped waxy oil and doped waxy oil (with FNPPD) under the magnetic field, by investigating the growth of deposition thickness as a function of time. The cold finger apparatus was made of two cold fingers, a stirring paddle and a reservoir. There were two circulating water baths controlling the temperature of the cold finger and reservoir. The oil temperature was 35 °C (wax appearance temperature = 28.3 °C) and the coolant temperature for each case was adjusted to maintain the initial inner wall temperature of cold fingers at 15 °C. A stirring rate of 300 rpm provided the hydrodynamics for the waxy oil. The wax deposition mass and deposition components were obtained by the weighing method and chromatographic test analysis, respectively. Further experimental details are shown in Table 1. Each set of experiment was performed in triplicate.

**2.2.2 Magnetic treatment.** From a field operation point of view, magnetic treatment equipment is mostly installed at the wellhead of a gathering pipeline or at the entrance of a long-distance pipeline transporting waxy oils. The magnetic treatment temperature was controlled at a high temperature (40 °C, above the wax precipitation point). A few seconds (10 s) of magnetic processing time was set. Two types of magnetic



Table 1 Experimental protocol and details

Conditions	Parameters
Samples	(1) Undoped waxy oil, (2) waxy oil with 50 ppm FNPPD (doped waxy oil), (3) undoped waxy oil with magnet treatment, (4) doped waxy oil with magnet treatment, (5) undoped waxy oil with magnetic coil treatment, (6) doped waxy oil with magnetic coil treatment
Temperature	Oil temperature 35 °C, wall temperature 15 °C
Magnetic treatment	Processing at 40 °C for 10 s
Stirring speed	300 rpm
Time	0.5, 1, 3, 6, 9 h

treatment include the Nd–Fe–B magnet and the high-frequency electromagnetic coil. Specifically, a magnet was swiped across the outer surface of the measuring cylinder containing 40 °C waxy oils for about 10 s. The measuring cylinder containing 40 °C waxy oils was inserted into the center of the coil and the machine was turned on to process for 10 s.

A circular neodymium–iron–boron magnet with a diameter of 25 mm and a thickness of 6.9 mm was used to generate a high-intensity magnetic field. The magnetic field intensity of the magnet tested using a Gauss meter was 50 mT (range: 200 mT; accuracy:  $\pm 2.0\%$ ).

A variable frequency power supply-magnetic coil system BTG-15 KW made in China was used to generate a high-frequency oscillating magnetic field (ESI Material A†). The power supply provides alternating current to the coil with a varying frequency between 30 and 100 kHz, thereby generating an oscillating magnetic field inside the coil. The oscillation frequency and magnetic field intensity are closely related to the coil structure. A ten-turn coil (radius: 5 cm; height: 13 cm) was used to produce a 50 kHz field. The magnetic field intensity in the center of the coil is 5 mT.

**2.2.3 High-temperature gas chromatography.** A few wax depositions scraped from the surface of the cold finger were dissolved in 0.5 mL of carbon disulfide and encapsulated in a sample vial. An Agilent 7890 was used to test the carbon number distribution of the deposition sample with magnetic treatment and/or FNPPD. The key procedures of HTGC were set as follows: (1) the oven temperature was initiated at 50 °C for 1 min and then heated to 430 °C at a rate of 9 °C min<sup>-1</sup>; (2) when the hydrogen flame ionization detector reached the set temperature of 430 °C, air and hydrogen were mixed and ignited in a certain proportion (air: 400 mL min<sup>-1</sup>, H<sub>2</sub>: 30 mL min<sup>-1</sup>); and (3) after the detector received a stable signal, the automatic sampler ran and injected 0.2  $\mu$ L of carbon disulfide dissolved test sample each time. Each test sample was put into two injection bottles and measured twice.

**2.2.4 Differential scanning calorimetry.** Heat flow curves of the experimental oil samples were tested using a TA Q2000 for the analysis of the wax appearance temperature and wax precipitation amount under the action of the magnetic field and/or FNPPD. The temperature ramp procedure was uniform as follows: isothermal at 60 °C for 1 min, followed by cooling to –20 °C at a cooling rate of 5 °C min<sup>-1</sup>. Each oil sample was measured three times to ensure that the error of experimental results was within 0.5 °C.

**2.2.5 Polarizing microscopy and focused beam reflectance measurement.** Polarizing microscopy (BX51, OLYMPUS) and focused beam reflectance measurement (METTLER TOLEDO) were performed, which allowed obtaining the wax crystal size, number, and morphology of waxy crystals under the action of the magnetic field. For details on the experimental devices, we suggest the readers to refer to our previous articles.<sup>30</sup>

The wax crystal size, number, and morphology can be performed in different ways (shear histories, thermal conditions, *etc.*), all of which strongly and directly affect the morphology of waxy crystals. In all the experiments, the beaker for the oil sample was equipped with a circulating water bath and an agitator, so that the cooling process and stirring speeds could be controlled. Before characterization and observation, the oil sample was cooled from 35 °C to 15 °C. The cooling rate was maintained constant at 0.5 °C min<sup>-1</sup> via the same pump speed of the water bath (F25 Julabo, Germany). In order to compare and analyze the wax crystal of the experimental sample in a flowing state, the stirring speed was set to the same value (300 rpm) for different oil samples. After the constant temperature at 15 °C for 5 min, we started recording the number and size of crystals. Finally, we dipped the oil sample in the experimental beaker with a dropper and dropped it on the slide. A 20 $\times$  magnification objective lens was used to observe the morphology of waxy crystals. Sampling and observation were repeated.

### 2.2.6 Crystallization kinetics analysis

**2.2.6.1 Avrami.** Avrami equation is the well-known principle to gain insights into such crystallization kinetics.<sup>31–33</sup> Continuing efforts have been dedicated to deducing and simplifying Avrami's original equation,<sup>34,35</sup> especially application in bulk crystallization. For waxy oils,<sup>36,37</sup> the Avrami equation can be written as follows:

$$\log[-\ln(1 - X(t))] = \log K + n \log(t) \quad (1)$$

where  $X(t)$  is the degree of crystallinity and  $t$  is the time (min). By plotting  $\log[-\ln(1 - X(t))]$  versus  $\log(t)$  and fitting linearly using the least-square method, the slope of the straight-line  $n$  and the intersection  $K$ , which is related to the crystal morphology and quantity, can be extracted. The degree of crystallinity  $X(t)$  was calculated based on the wax precipitation amount estimated from the integral of the heat flow curve obtained from DSC tests.  $X(t)$  in eqn (1) is the ratio of wax precipitation amount at time  $t$  to total wax precipitation. The analysis of the fitting



parameters of the Avrami equation allows us to further evaluate the crystallization kinetics of waxy oils with the magnetic field and/or FNPPD.

**2.2.7 Size-independent growth.** Size-independent growth (SIG) is a widely used quantitative method to estimate the nucleation and growth rate of crystal.<sup>38,39</sup> The mathematical expression of the SIG model is shown as eqn (2) and (3):

$$\ln n(L) = \ln n_0 - L/G\tau \quad (2)$$

$$B = n_0G \quad (3)$$

where  $n(L)$  is the crystal density ( $\text{mm}^{-3}$ ),  $n_0$  is the nucleus density ( $\text{mm}^{-3}$ ),  $L$  is the chord length (m),  $G$  is the growth rate of crystals ( $\text{m s}^{-1}$ ),  $\tau$  is the mean residence time of waxy oils in the beaker volume (s),  $B$  is the nucleation rate ( $\text{s}^{-1} \text{m}^{-3}$ ). By linearly fitting the crystal size distribution data, the intercept  $\ln n_0$  and slope  $-1/(G\tau)$  were obtained. For the known average residence time of crystal suspensions, the calculation results of nucleation rate and growth rate of undoped/doped waxy oils before and after magnetic field treatment can be obtained. This has important consequences for our understanding of the mechanism of wax deposition under the action of the magnetic field.

## 3. Results and discussion

### 3.1. Wax deposition mass

As shown in Fig. 1, the growth curve of the deposition layer after wax oil treatment with a magnet or magnetic coil is positioned farther to below the undoped waxy oil. The growth of wax deposition layers was inhibited by magnetic treatment at different deposition times. For example, at 9 h, the wax deposition mass decreased from 9.3 g to 8.3 g and 8.1 g under the action of the magnet and magnetic coil, respectively. The wax deposition mass inhibition efficiency was 10.75% (with magnet) and 12.90% (with magnetic coil). These results indicated that high temperature (above the wax appearance temperature), short time (10 s), and off-line magnetic treatment can effectively inhibit wax deposition.

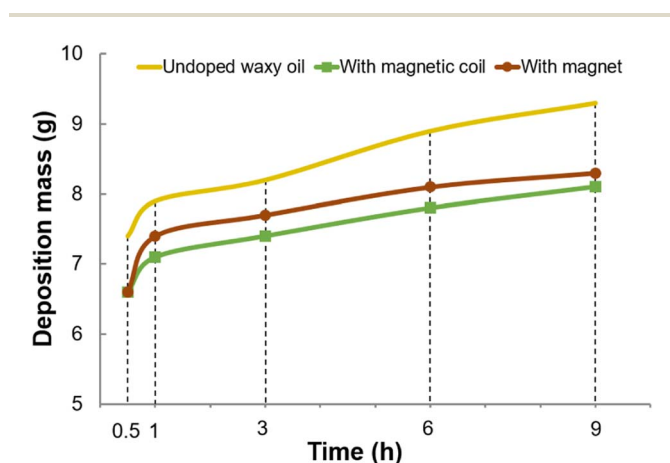


Fig. 1 Deposition mass of undoped waxy oils under different magnetic treatments.

After long-distance and time-consuming pipeline transportation, the temperature of magnetized oil near the pipe wall will decrease below the wax precipitation point, making the dissolved waxy molecules crystallized and deposited near the pipe wall. It is of interest to investigate the historical effects of magnetic treatment, which is accomplished by wax deposition experiments with magnetic treatment and left at room temperature for 24 h. The growth curves of wax deposition after magnetic treatment without resting and after resting for 24 h almost overlap, covering both the undoped/doped waxy oil and magnetic treatment with magnet/magnetic coil (Fig. 2). It was shown that both the high-intensity and high-frequency magnetic fields generated by the magnet and magnetic coil have historical effects. The obtained experimental results demonstrated the promising prospects of magnetic processing applications.

Additionally, the effect of wax deposition mass inhibition by the combined magnetic field and FNPPD was investigated.

The experimental data presented in Fig. 3 provided that the magnetic field can further improve the wax deposition mass efficiency of the FNPPD. The deposition mass of the doped waxy oil with the magnet or magnetic coil treatment was less than that of the doped waxy oil. As can be seen, by comparison to the result in Fig. 3, the wax deposition mass of the doped waxy oil with the magnetic coil is larger than that of the doped waxy oil with the magnet. The combined action of the magnet and FNPPD has a better suppression effect on the wax deposition mass compared to the magnetic coil. It is important to point out that the magnetocaloric effect of the magnetic coil might cause the oil temperature to rise (the doped waxy oil can be rapidly heated from 40 °C to around 80 °C with the 10 s magnetic coil treatment), disentanglement of EVA copolymers and destabilization of the structure of FNPPD, thus resulting in the magnetic coil and agent working together poorly.<sup>46</sup> For instance, the 9 h deposition mass of the doped waxy oil (with 50 ppm FNPPD) under the action of the magnet and magnetic coil was 6.5 g and 7.9 g, and the wax deposition inhibition efficiency was 30.11% and 15.05%, respectively. Moreover, we noted that the wax inhibition efficiency was up to 30.11% with the combined action of magnet and FNPPD, and its inhibition efficiency is about triple that of a single magnetic treatment or FNPPD. The 9 h deposition mass inhibition efficiency of the undoped waxy oil by the magnet and FNPPD was 10.75% and 11.83%, respectively. It is estimated that the 30.11% inhibition efficiency of wax deposition mass under the combined action of magnet and FNPPD exceeds the sum of the magnetic treatment and FNPPD ( $10.75\% + 11.83\% = 22.58\%$ ) by about 7.5%. This combination acts in synergy to inhibit wax deposition. A similar rule, shown in Fig. 4, exists for the other deposition time.

### 3.2. Wax deposition components

The composition attributes of the wax deposition layer such as the critical carbon number, carbon number distribution and wax content (sum of the proportion of  $C \geq 18$  components) were compared under two magnetic treatments *via* HTGC analysis.

As can be seen from Fig. 5 (red arrows), the critical carbon number of wax deposition does not change significantly with the magnetic fields/FNPPD. Contrast differences to deposition



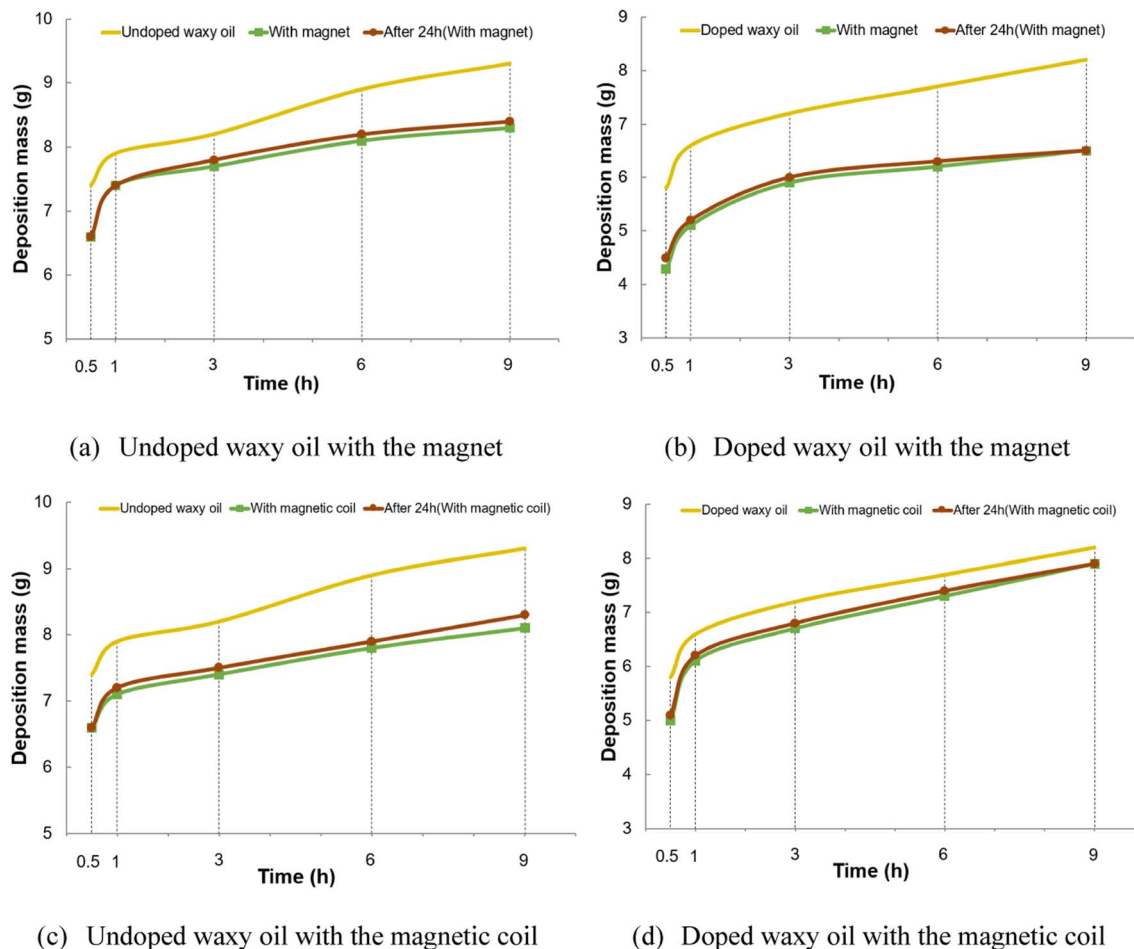


Fig. 2 Wax deposition process after magnetic treatment with 0 and 24 h of resting.

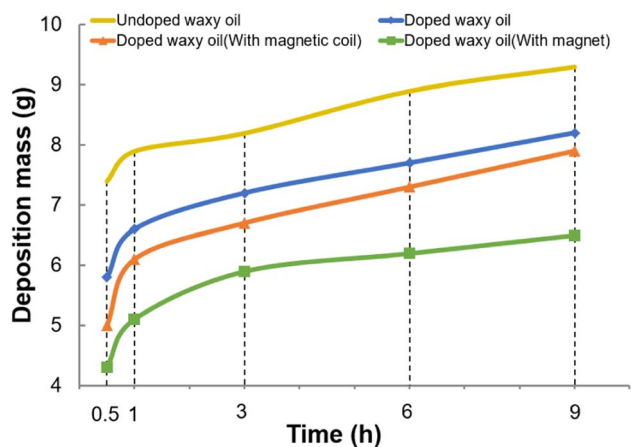


Fig. 3 Deposition mass of the doped waxy oil under different magnetic treatments.

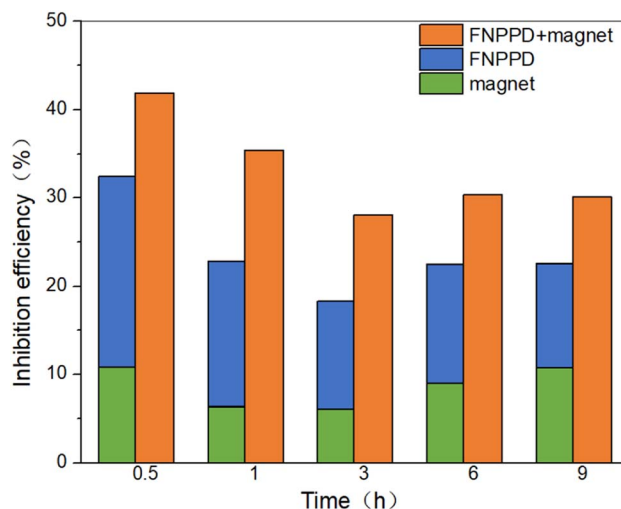


Fig. 4 Analysis of the synergistic effect efficiency of the magnet and FNPPD.

components were mainly reflected in the diffusion and deposition of high carbon wax molecules above the critical carbon number ( $\geq C_{25}$ ). Fig. 6 compares the carbon number distribution of the deposition layer of the undoped/doped waxy oil under the action of the magnet or magnetic coil at 3 h and 9 h deposition time.

Fig. 6 showed that high levels of the heavy component wax content in the deposition layer were distinctive of the undoped/doped waxy oil with the magnetic coil (green area chart).



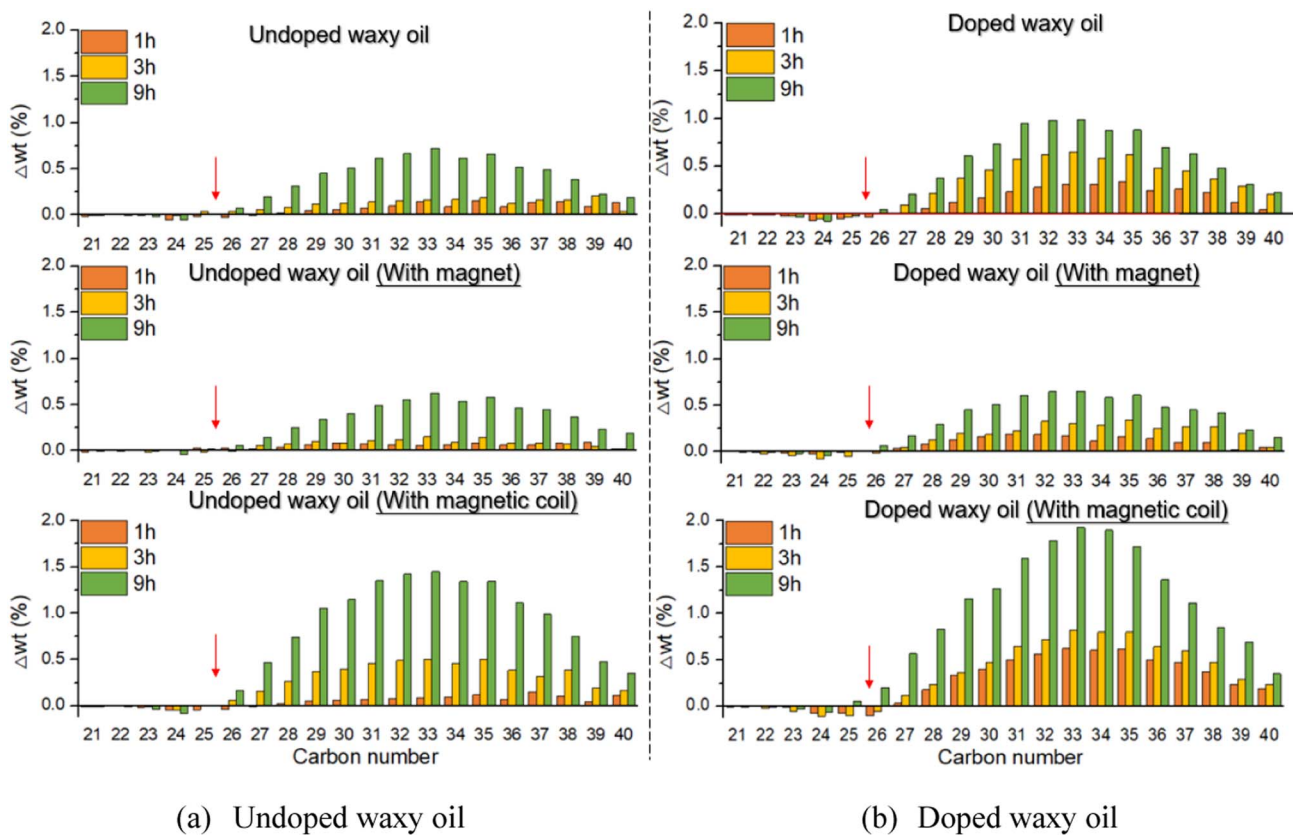


Fig. 5 Difference in the carbon number distribution with different magnetic treatments.

However, the high-intensity magnetic field generated by the magnet reduced the heavy component wax content in the deposition layer (orange area chart). Complementarily, the summary graph of the total wax content (sum of the proportion of  $C \geq 18$  components) of the undoped/doped waxy oil deposition layer as a function of time under the action of the magnet and magnetic coil enabled us to verify this argument.

As shown by the black arrows in Fig. 7, the total wax content of the undoped/doped waxy oil deposition layer decreased under the magnet action at different deposition times while an opposite trend was apparent on the magnetic coil. A possible partial explanation of this fact is as follows. The magnetocaloric effect of the magnetic coil might trigger an increase in the oil temperature and the difference between the oil and the wall temperature, leading to an enhanced diffusion drive of wax molecules. Furthermore, the effect of the combination of magnetic field and FNPPD on the wax content of the deposition layers was investigated.

In comparison to the wax content of the deposited layer without magnetic fields, the amount of the doped waxy oil with the magnetic coil was significantly bigger (Fig. 8 orange line). Unsurprisingly, the wax content of the deposited layer would be further increased if the magnetic coil together with the FNPPD was applied to the doped waxy oil. Note that the magnet used in this study can reduce the 9 h wax content of the doped waxy oil deposit layer (Fig. 8 green line and yellow line). In the case of the above-mentioned example, with the magnet, the 9 h wax

content of the doped waxy oil deposit layer would decrease from 19.34% (doped waxy oil) to 16.92% (doped waxy oil with the magnet).

The synergistic effect between the magnet and the FNPPD appeared, resulting in an increase of 1.36% (undoped waxy oils: 15.56%; doped waxy oils with magnet: 16.92%) to the wax content of the 9 h deposition layer, which is less than that obtained using the FNPPD or magnet alone ( $3.78 - 2.22 = 1.56\%$ ). In particular, the wax content of the 9 h deposition layer increased by 3.78% (undoped waxy oils: 15.56%; doped waxy oils: 19.34%) and decreased by 2.22% (undoped waxy oils: 15.56%; undoped waxy oils with the magnet: 13.34%) for doped waxy oils and waxy oils with the magnet, respectively. The motivation for this synergistic effect and magnetic field action is related to the wax precipitation properties and crystallization kinetics in general, as discussed below.

### 3.3. Discussion and analysis

Clearly, using the magnetic treatment enables the undoped/doped waxy oil to reduce the wax appearance temperature and wax precipitation amount (Fig. 9 and Table 2). For the undoped waxy oil, after applying the magnetic treatment, the wax appearance temperature reduced from 28.28 °C to 24.58 °C. The wax appearance temperature, however, reduced from about 28.49 °C to 25.89 °C as the doped waxy oil was treated with magnetic fields in Fig. 9 and Table 2. The percentage of the



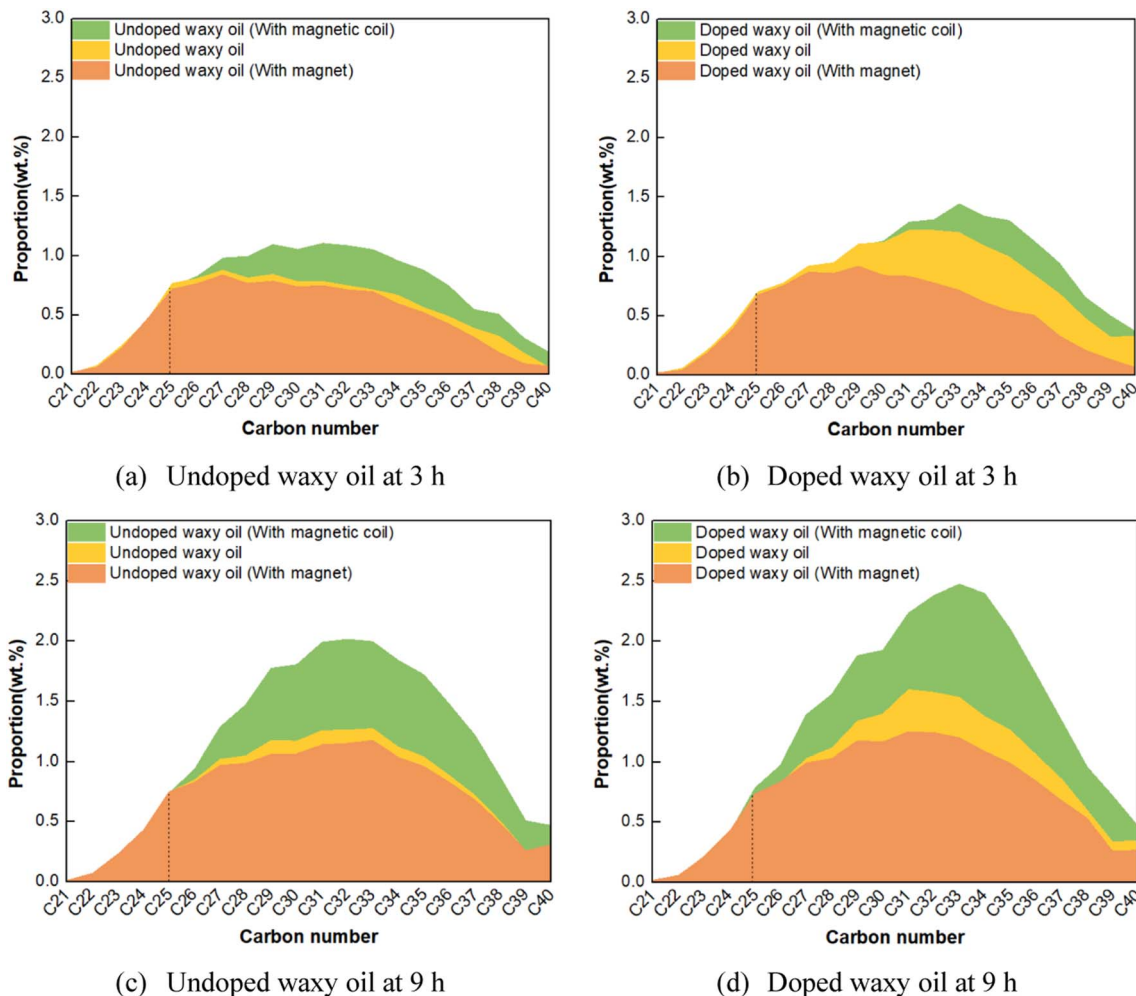


Fig. 6 Carbon number distribution of the deposition layer with the magnet or magnetic coil.

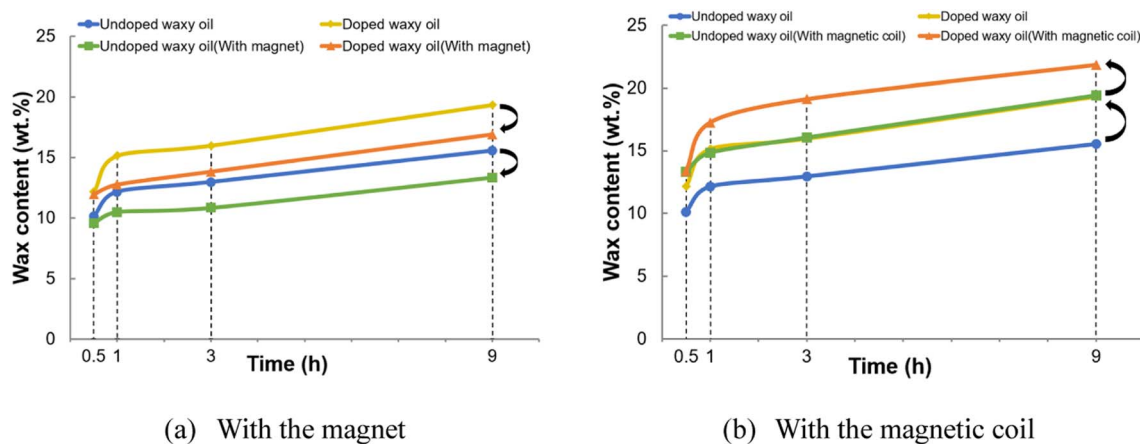


Fig. 7 Wax content in the deposition layer with the magnet or magnetic coil.

cumulative percentage wax precipitation at 15 °C (wall temperature) was also included.

The magnetization energy of the magnetic field reduces solid-liquid interfacial tension and supersaturation.<sup>40,41</sup> As

a result, the equilibrium concentration (total wax content minus wax precipitation amount) increases and the wax precipitation amount decreases. The thermodynamic theory of wax deposition will also emphasize the variation in wax



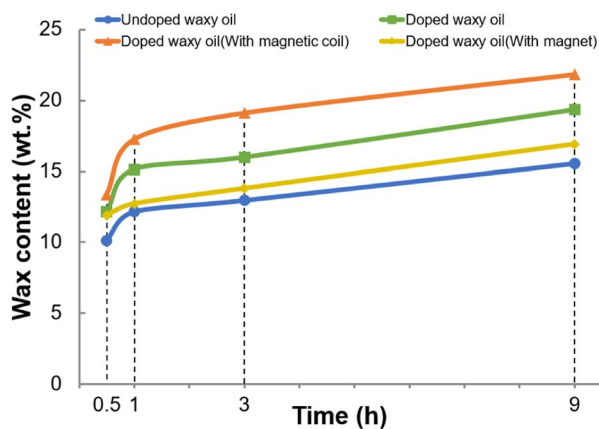


Fig. 8 Wax content of the doped waxy oil in the deposition layer under different magnetic treatments.

precipitation characteristics, such as the wax appearance temperature and the amount of wax precipitation as important factors in determining the wax deposition inhibition efficiency. Given the decrease in the wax appearance temperature and wax precipitation amount as a result of using the magnetic field, the mass and component of wax deposition would further be suppressed by the magnet. Due to the minimum amount of wax precipitation with the synergistic effect of the FNPPD and magnetic field, it is feasible in the application to reduce the thickness and hardness of field pipeline deposition.

There is some crystallization kinetics information available by analyzing the wax precipitation curves using the Avrami theory, explaining the mechanisms behind inhibiting the wax deposition by the magnetic field. We performed line fitting on the crystallinity regarding wax precipitation amount using least-squares matching, and the fitting diagram is shown in Fig. 10. The  $R^2$  value of the Avrami model fitting of different experimental oil samples was greater than or equal to 0.96. This implies that the Avrami theory is a strictly feasible solution to explore the magnetic field action mechanism.

The Avrami index  $n$  and crystallization kinetic parameters  $K$  obtained from the slope and intercept of the Avrami fitting plot are summarized in Fig. 11 and 12.

The Avrami exponent  $n$  is related to the morphological structures of crystals. In general, for polymeric and organic systems, the Avrami exponents are 1, 2, and 3 for needle, disc, and spherical crystals, respectively. As can be seen from Fig. 11, the  $n$  values of all four waxy oils were between 1 and 2. The magnetic field or/and FNPPD did not significantly change the crystal morphology, which remained mainly needle and disc-like. However, with the action of the magnetic field, the undoped/doped waxy oil was decreasing slightly in the  $n$  value and this decrease will most likely be accompanied by a decrease in wax crystal size. The  $n$  value of the undoped waxy oil decreased from 1.86 to 1.61. The  $n$  value of the doped waxy oil decreased from 1.73 to 1.71.

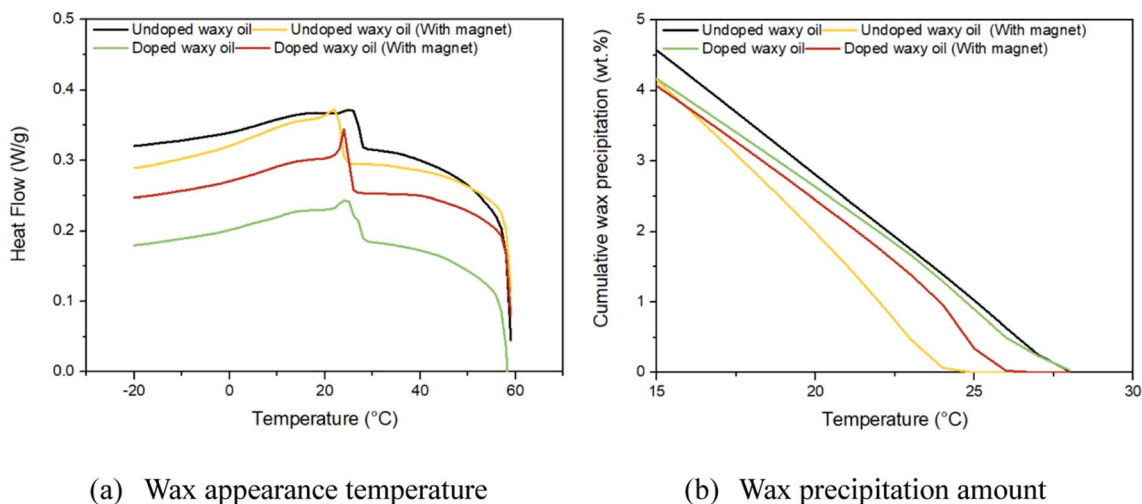


Fig. 9 Wax precipitation properties of the waxy oil under magnetic treatment.

Table 2 Summary of the wax appearance temperature and wax precipitation amount results

	Wax appearance temperature, °C	Cumulative percentage wax precipitation at 15 °C, wt%
Waxy oil	28.28	4.57
Waxy oil with magnet	<b>24.58</b>	<b>4.16</b>
Waxy oil with FNPPD	28.49	4.17
Waxy oil with magnet-FNPPD	<b>25.89</b>	<b>4.07</b>





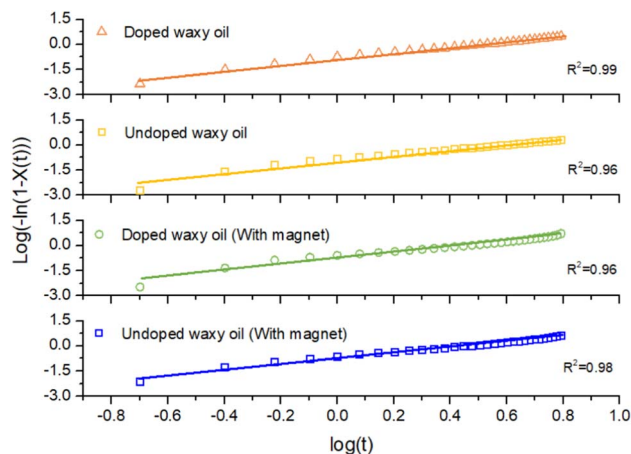


Fig. 10 Avrami fitting diagram for the waxy oil under magnetic treatment.

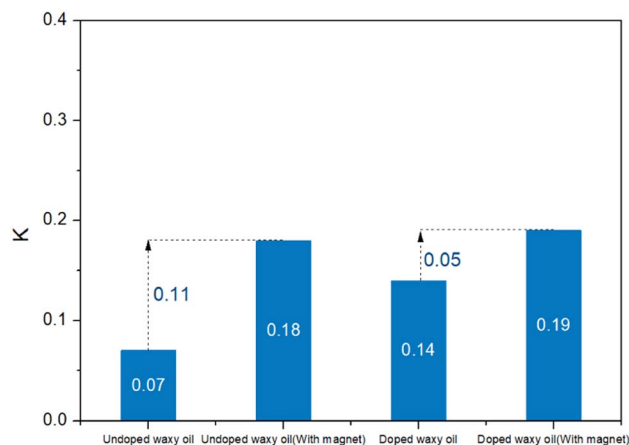


Fig. 12 Summary of  $K$  values in the fitting results of the Avrami equation.

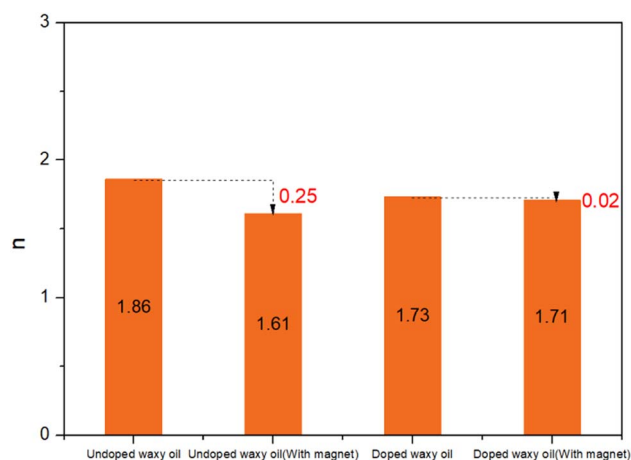


Fig. 11 Summary of  $n$  values in the fitting results of the Avrami equation.

The most obvious thing was the  $K$  increase in the doped/undoped waxy oil with the action of the magnetic field. Specific results are shown in Fig. 12, where the  $K$  value of the undoped waxy oil showed a 1.6-fold increase from 0.07 to 0.18. The doped waxy oil showed an approximately 36% increase from 0.14 to 0.19. The  $K$  value was determined by the number and morphology of wax crystals, as described in eqn (4)

$$K = gNv^n, \quad (4)$$

where  $g$  and  $N$  are the geometrical factor and number of wax crystals,  $v$  is the growth rate, and  $n$  is the Avrami exponent.<sup>42</sup> The  $n$  value of the waxy oil slightly decreased when the magnetic fields were applied. It was inferred that the increase in the  $K$  value under the magnetic field in this case study was mainly attributed to the increasing number of wax crystals. Correspondingly, there was a significant increase in the number of wax crystals compared to the untreated oil sample. The results from the FBRM and polarized light microscopy supported this view (Table 3 and Fig. 14).

Table 3 Summary of wax crystal number and density

	Wax crystal number	Wax crystal density, $\text{mm}^{-3}$
Undoped waxy oil	29987.67	0.60
Undoped waxy oil (with magnet)	44191.48	0.88
Doped waxy oil	61793.33	1.24
Doped waxy oil (with magnet)	62314.44	1.25

To further elucidate the mechanism of magnetic field action from the perspective of crystallization kinetics, the SIG kinetic model was used to analyze its crystallization nucleation and growth rate parameters. We implemented the linear fitting based on the size distribution of wax crystals, and the fitting results are shown in Fig. 13 and Table 4.

It can be seen that in all four cases the points and high  $R^2$  values reflect a good linear fit, indicating the effectiveness of SIG crystallization kinetics analysis. Comparing the nucleation rate and growth rate results, it was found that under magnetic field treatment, the nucleation rate of the undoped/doped waxy oil increased, while the growth rate decreased. It is possible that the reduction in interfacial tension and free energy due to magnetization energy of the magnetic fields would lead to a reduced nucleation barrier, resulting in a larger nucleation rate and more wax crystals. In addition, there is a decrease in the wax crystal growth rate and wax crystal size on account of a smaller supersaturation with the magnetic field. More importantly, the effect of the magnetic field on the number and morphology of the wax crystals will further weaken their ability to encapsulate oil, and can thus potentially inhibit wax deposition.<sup>43</sup> Once the magnetic field was used in conjunction with the FNPPD, the synergistic effect can be shown by a nucleation rate of the relative maxima and minima in the growth rate. Superparamagnetic nano- $\text{Fe}_3\text{O}_4$  in the FNPPD increases the magnetic susceptibility and magnetization energy of waxy oils, further amplifies the magnetic field effect, and thus improves the wax deposition inhibition efficiency.



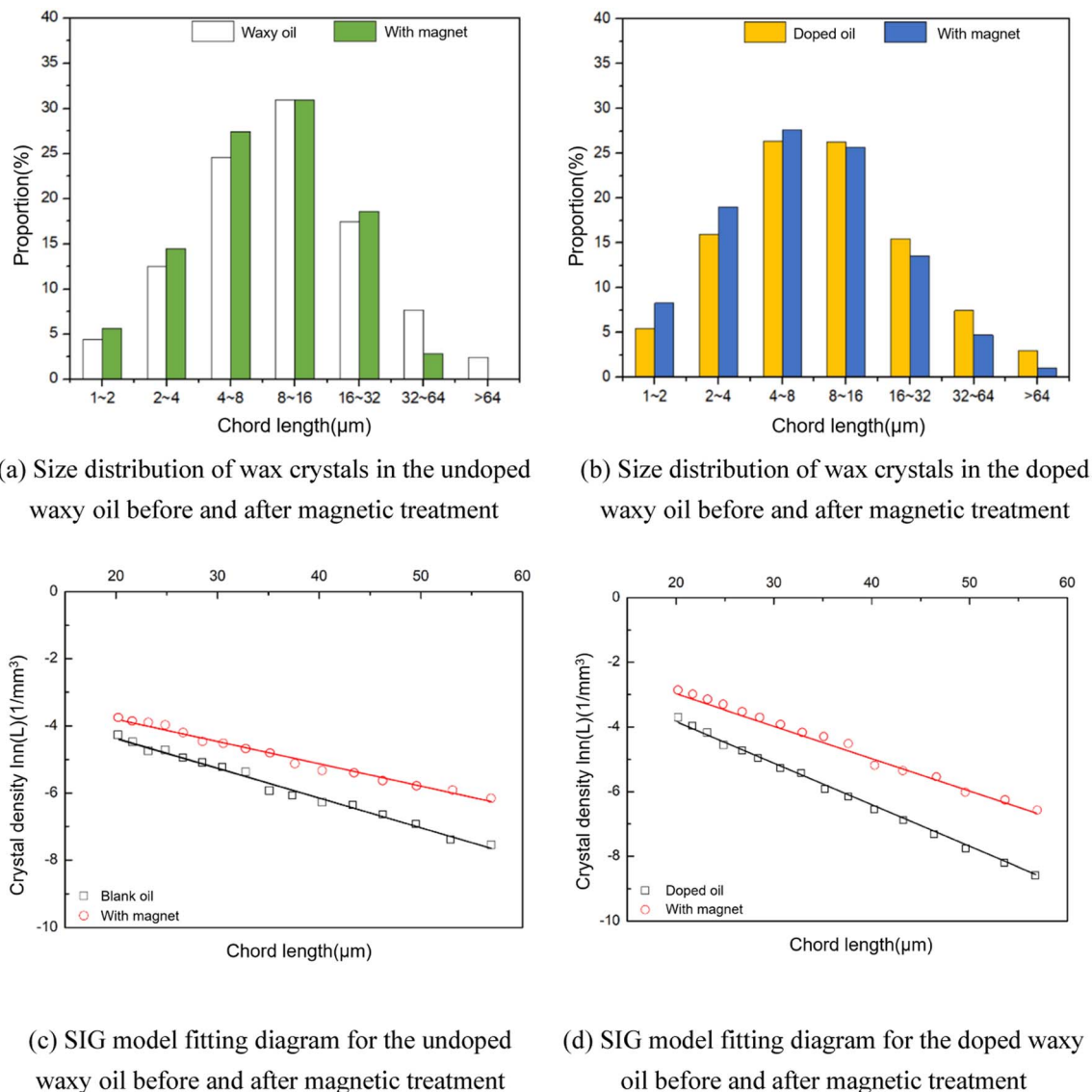


Fig. 13 Crystal size distribution and SIG model fitting diagram.

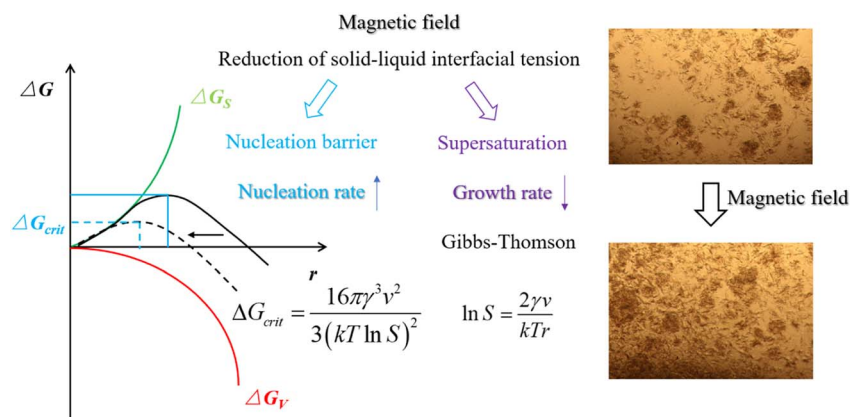


Fig. 14 Schematic of the wax deposition mechanism of the magnetic field.



Table 4 Nucleation and growth rate of the undoped/doped waxy oil before and after magnetic field treatment

	Fitted equation ( $L > 20 \mu\text{m}$ )	$R^2$	$G$ ( $\text{m s}^{-1}$ )	$B$ ( $\text{s}^{-1} \text{m}^{-3}$ )
Undoped waxy oil	$\ln n(L) = -2.4701 - 0.0921L$	0.94	$1.206 \times 10^{-8}$	$1.02 \times 10^9$
Undoped waxy oil (with magnet)	$\ln n(L) = -2.3508 - 0.0717L$	0.94	$1.162 \times 10^{-8}$	$1.11 \times 10^9$
Doped waxy oil	$\ln n(L) = -1.1410 - 0.0998L$	0.92	$1.113 \times 10^{-8}$	$3.56 \times 10^9$
Doped waxy oil (with magnet)	$\ln n(L) = -0.9867 - 0.1083L$	0.96	$1.026 \times 10^{-8}$	$3.82 \times 10^9$

## 4. Conclusions

The objectives of this work are to investigate the effect of applying magnetic fields and their combination with a ferromagnetic nanocomposite pour point depressant (FNPPD) on the wax deposition layer, such as wax deposit mass, carbon number distribution, and wax content. Furthermore, we explored the underlying inhibition mechanisms by analysis of wax precipitation characteristics, wax crystal number and size, and crystallization kinetics.

The wax deposition mass of waxy oils can be effectively reduced using high-frequency magnetic fields and high-intensity magnetic fields generated by magnetic coils and magnets, even after 24 h resting time. The magnetocaloric effect caused by the high-frequency magnetic field can further promote the wax deposition aging, resulting in an increase in the heavy component wax content and total wax content of the deposition layer. The magnetization energy of the magnetic field caused a drop in the solid-liquid interfacial tension/free energy and wax molecular nucleation barrier, leading to an increase in the crystal number/nucleation rate and a reduction in the growth rate/encapsulated oil amount. Given the decrease of the wax appearance temperature and wax precipitation amount as a result of using the magnetic field, the mass and component of wax deposition would further be suppressed. Note that if the magnetic field-FNPPD was used, there was synergistic inhibition of wax deposition. The detrimental effects of the FNPPD causing an increase in the wax content/hardness in the deposition layer could be reduced by the magnetic field-FNPPD approach.

## Nomenclature

FNPPD	Ferromagnetic nanocomposite pour point depressant
Nd-Fe-B	Neodymium-iron-boron
EVA	Ethylene/vinyl acetate
VA	Vinyl acetate
DSC	Differential scanning calorimeter
HTGC	High-temperature gas chromatography
FBRM	Focused beam reflectance measurement
$X$	Crystallinity
$t$	Time
SIG	Size-independent growth
$n$	Crystal density
$L$	Chord length

$G$	Growth rate
$\tau$	Mean residence time
$B$	Nucleation rate
$n$	Avrami index
$K$	Crystallization kinetic parameter
$g$	Geometrical factor
$N$	Number of crystals
$\nu$	Growth rate

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was supported by the National Natural Science Foundation of China (Grant No. 52274061 & 52004039 & 51974037), China Postdoctoral Science Foundation (Grant No.2023T160717 & 2021M693908), CNPC Innovation Found (Grant No. 2022DQ02-0501), Changzhou Applied Basic Research Program (Grant No. CJ20230030), The major project of universities affiliated with Jiangsu Province basic science (natural science) research (Grant No.21KJA440001), The Jiangsu Qinglan Project, Changzhou Longcheng Talent Plan – Youth Science and Technology Talent Recruitment Project.

## References

- 1 E. Bell, Y. Lu, N. Daraboina and C. Sarica, *J. Nat. Gas Sci. Eng.*, 2021, **88**, 103798.
- 2 C. Balan, D. Broboana, E. Gheorghiu and L. Velas, *J. Non-Newtonian Fluid Mech.*, 2008, **154**, 22–30.
- 3 Y. Chi, J. Yang, C. Sarica and N. Daraboina, *Energy Fuels*, 2019, **33**, 2797–2809.
- 4 W. Li, H. Li, H. Da and K. Hu, *Fuel Process. Technol.*, 2021, **217**, 106817.
- 5 H. Huang, W. Wang, Z. Peng, K. Li, D. Gan, S. Zhang, Y. Ding, H. Wu and J. Gong, *J. Pet. Sci. Eng.*, 2019, **175**, 828–837.
- 6 H. Huang, W. Wang, Z. Peng, Y. Ding, K. Li, Q. Li and J. Gong, *Fuel*, 2018, **221**, 257–268.
- 7 H. Huang, W. Wang, Z. Peng, F. Yang, X. Zhang, Y. Ding, K. Li, C. Wang, D. Gan and J. Gong, *Langmuir*, 2020, **36**, 591–599.
- 8 X. Chen, L. Hou, W. Li, S. Li and Y. Chen, *J. Mol. Liq.*, 2018, **249**, 1052–1059.
- 9 R. Tao and X. Xu, *Energy Fuels*, 2006, **20**, 2046–2051.



- 10 F. Homayuni, A. A. Hamidi, A. Vatani, A. A. Shaygani and R. F. Dana, *Pet. Sci. Technol.*, 2011, **29**, 2407–2415.
- 11 J. L. Goncalves, A. J. F. Bombard, D. A. W. Soares and G. B. Alcantara, *Energy Fuels*, 2010, **24**, 3144–3149.
- 12 C. Jiang, L. Guo, Y. Li, S. Li, Y. Tian, L. Ma and J. Luo, *Colloids Surf., A*, 2021, **629**, 127372.
- 13 J. L. Goncalves, A. J. F. Bombard, D. A. W. Soares, R. D. M. Carvalho, A. Nascimento, M. R. Silva, G. B. Alcantara, F. Pelegrini, E. D. Vieira, K. R. Pirota, M. I. M. S. Bueno, G. M. S. Lucas and N. O. Rocha, *Energy Fuels*, 2011, **25**, 3537–3543.
- 14 J. Jing, W. Shi, Q. Wang and B. Zhang, *Energy Sources, Part A*, 2019, **44**, 5080–5093.
- 15 W. Shi, J. Jing, Q. Wang and B. Zhang, *Pet. Sci. Technol.*, 2021, **39**, 878–895.
- 16 P. T. Nguyen, V. V. Nguyen, Q. K. L. Bui, Q. V. Ngo and V. H. Pham, *SPE Asia Pacific Oil and Gas Conference*, SPE 68749, 2001.
- 17 X. Zhang and Y. Zhang, *Int. J. Therm. Sci.*, 2021, **164**, 106897.
- 18 C.-H. Park, S.-J. Kang, L. D. Tijjing, H. R. Pant and C. S. Kim, *Ceram. Int.*, 2013, **39**, 9785–9790.
- 19 A. A. Adewunmi, M. S. Kamal and T. I. Solling, *J. Pet. Sci. Eng.*, 2021, **196**, 107680.
- 20 C. A. M. Iglesias, J. C. R. de Araujo, J. Xavier, R. L. Anders, J. M. de Araujo, R. B. da Silva, J. M. Soares, E. L. Brito, L. Streck, J. L. C. Fonseca, C. C. Pla Cid, M. Gamino, E. F. Silva, C. Chesman, M. A. Correa, S. N. de Medeiros and F. Bohn, *Sci. Rep.*, 2021, **11**, 11867.
- 21 N. Manuchehrabadi, Z. Gao, J. Zhang, H. L. Ring, Q. Shao, F. Liu, M. McDermott, A. Fok, Y. Rabin, K. G. M. Brockbank, M. Garwood, C. L. Haynes and J. C. Bischof, *Sci. Transl. Med.*, 2017, **9**, 379.
- 22 J.-H. Lee, J.-T. Jang, J.-S. Choi, S. H. Moon, S.-H. Noh, J.-W. Kim, J.-G. Kim, I.-S. Kim, K. I. Park and J. Cheon, *Nat. Nanotechnol.*, 2011, **6**, 418–422.
- 23 M. I. A. Abdel Maksoud, M. M. Ghobashy, A. S. Kodous, R. A. Fahim, A. I. Osman, A. A. H. Al-Muhtaseb, D. W. Rooney, M. A. Mamdouh, N. Nady and A. H. Ashour, *Nanotechnol. Rev.*, 2022, **11**, 372–413.
- 24 A. Chiu-Lam, E. Staples, C. J. Pepine and C. Rinaldi, *Sci. Adv.*, 2021, **7**, 3005.
- 25 M. Prachi, H. Chun and L. B. Steven, *International Petroleum Technology Conference*, 2014, IPTC-18090-MS.
- 26 H. Huang, W. Wang, Z. Peng, K. Li, Y. Ding, W. Yu, D. Gan, C. Wang, Y. Xue and J. Gong, *Pet. Sci.*, 2020, **17**, 838–848.
- 27 C. Wang, M. Zhang, W. Wang, Q. Ma, S. Zhang, H. Huang, Z. Peng, H. Yao, Q. Li, Y. Ding and J. Gong, *Energy Fuels*, 2020, **34**, 12239–12246.
- 28 N. Frickel, R. Messing, T. Gelbrich and A. M. Schmidt, *Langmuir*, 2010, **26**, 2839–2846.
- 29 J. Nayeem, M. A. A. Al-Bari, M. Mahiuddin, M. A. Rahman, O. T. Mefford, H. Ahmad and M. M. Rahman, *Colloids Surf., A*, 2021, **611**, 125857.
- 30 C. Wang, H. Chen, H. Shi, K. Ma, Q. Ma and J. Gong, *ACS Omega*, 2022, **7**, 11200–11207.
- 31 P. Zemenova, R. Kral, M. Rodova, K. Nitsch and M. Nikl, *J. Therm. Anal. Calorim.*, 2020, **141**, 1091–1099.
- 32 R. Wang, S. Zou, B. Jiang, B. Fan, M. Hou, B. Zuo, X. Wang, J. Xu and Z. Fan, *Cryst. Growth Des.*, 2017, **17**, 5908–5917.
- 33 K. Dimitra and C. Konstantinos, *Thermochim. Acta*, 2021, **704**, 179030.
- 34 M. Avrami, *J. Chem. Phys.*, 1939, **7**, 1103–1112.
- 35 M. Avrami, *J. Chem. Phys.*, 1940, **8**, 212–224.
- 36 L. Ismail, R. E. Westacott and X. Ni, *Chem. Eng. J.*, 2008, **137**, 205–213.
- 37 A. Hosseinipour, A. Japper-Jaafar, S. Yusup and L. Ismail, *Int. J. Eng., Trans. A*, 2019, **32**, 18–27.
- 38 B. Wierzbowska, N. Hutnik, K. Piotrowski and A. Matynia, *Cryst. Growth Des.*, 2011, **11**, 1557–1565.
- 39 D. B. Sigourney, B. H. Letcher, M. Obedzinski and R. A. Cunjak, *J. Fish Biol.*, 2010, **72**, 2435–2455.
- 40 M. Dalvi-Isfahan, N. Hamdami, E. Xanthakis and A. Le-Bail, *J. Food Eng.*, 2017, **195**, 222–234.
- 41 Q. Guan, Y. Liu, B. Ling, G. Zeng, H. Ji, J. Zhang and Q. Zhang, *Int. J. Chem. Kinet.*, 2020, **52**, 463–471.
- 42 S. Z. D. Cheng and B. Wunderlich, *Macromolecules*, 1988, **21**, 3327–3328.
- 43 Y. Gan, Q. Cheng, Z. Wang, J. Yang, W. Sun and Y. Liu, *J. Pet. Sci. Eng.*, 2019, **179**, 56–69.

