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## Fine-regulation of gradient gate-opening in nanoporous crystals for sieving separation of ternary C3 hydrocarbons†

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The adsorptive separation of ternary propyne (C<sub>3</sub>H<sub>4</sub>)/propylene (C<sub>3</sub>H<sub>6</sub>)/propane (C<sub>3</sub>H<sub>8</sub>) mixtures is of significant importance due to its energy efficiency. However, achieving this process using an adsorbent has not yet been accomplished. To tackle such a challenge, herein, we present a novel approach of fine-regulation of the gradient of gate-opening in soft nanoporous crystals. Through node substitution, an exclusive gate-opening to C<sub>3</sub>H<sub>4</sub> (17.1 kPa) in NTU-65-FeZr has been tailored into a sequential response of C<sub>3</sub>H<sub>4</sub> (1.6 kPa), C<sub>3</sub>H<sub>6</sub> (19.4 kPa), and finally C<sub>3</sub>H<sub>8</sub> (57.2 kPa) in NTU-65-CoTi, of which the gradient framework changes have been validated by *in situ* powder X-ray diffractions and modeling calculations. Such a significant breakthrough enables NTU-65-CoTi to sieve the ternary mixtures of C<sub>3</sub>H<sub>4</sub>/C<sub>3</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> under ambient conditions, particularly, highly pure C<sub>3</sub>H<sub>8</sub> (99.9%) and C<sub>3</sub>H<sub>6</sub> (99.5%) can be obtained from the vacuum PSA scheme. In addition, the fully reversible structural change ensures no loss in performance during the cycling dynamic separations. Moving forward, regulating gradient gate-opening can be conveniently extended to other families of soft nanoporous crystals, making it a powerful tool to optimize these materials for more complex applications.

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## Introduction

Efficient separation of the ternary C3 hydrocarbons is crucial for the petrochemical industry as C<sub>3</sub>H<sub>6</sub> is an essential feedstock for valuable commodities.<sup>1</sup> Currently, the separation process involves energy-intensive catalytic hydrogenation and cryogenic distillation, which accounts for nearly 3% of all separation energy.<sup>1–3</sup> Therefore, there is a need for a more energy-efficient technology for this task. Adsorption separation using porous materials, specifically porous coordination polymers (PCPs), shows great promise due to their finely designed pore chemistry.<sup>4–13</sup> In this regard, recent progress has been made in binary separations using strategies such as  $\pi$ -complexation,

sieving strategies and kinetic diffusion.<sup>14–23</sup> However, the similar molecular sizes and kinetic diameters exacerbate the challenge of C<sub>3</sub>H<sub>4</sub>/C<sub>3</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> separation, particularly by one material.

Recent research has shown that the purification of ethylene from a complex mixture of C2 hydrocarbons and carbon dioxide can be achieved using sequentially packed sorbents, where the three impurities were captured by three PCPs.<sup>24</sup> Although this strategy requires overcoming the difficulties of preparation of the three materials, and also their rational packing, it enables us to believe that integrating gradient sorbent–sorbate interactions may address the challenge of C<sub>3</sub>H<sub>4</sub>/C<sub>3</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> separation in a single domain, as well as the precise understanding of hierarchical sites or gradient gate-openings.

The concept of hierarchical sites holds certain theoretical feasibility, but its implementation is hindered by the significant limitations in rational assembly of these sites in a confined nanospace. Comparably, the strategy of gradient gate-openings shows promising prospects. Since the early reports of soft crystals,<sup>25,26</sup> the soft nature of these materials has been gradually understood, that is, the stronger the interaction, the earlier the gate-opening.<sup>27,28</sup> In addition, soft frameworks can exhibit sensitive responses to even extremely small stimuli.<sup>29–31</sup> Given these advantages, significant efforts have been dedicated to the construction of soft PCPs;<sup>27,29,32–35</sup> however, neither the fine pre-design nor function-oriented synthesis of such a material,

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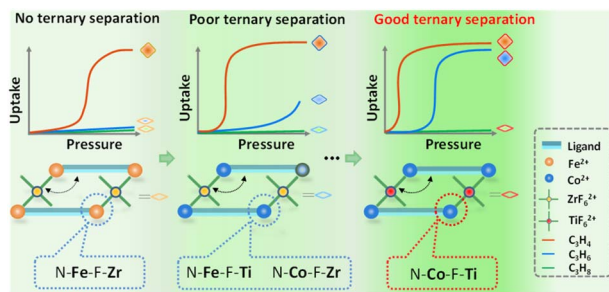
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Scheme 1 Illustration of fine-regulation of gradient gate-opening in soft NTU-65-series via node substitution for sieving separation of C<sub>3</sub> hydrocarbons in a single domain.

whose framework can sequentially recognize these similar molecules, has yet been reported.

During our investigation of porous materials,<sup>20,36,37</sup> we have reported a soft crystal, NTU-65, [Cu(L)<sub>2</sub>(SiF<sub>6</sub>)] (L = 1,4-di(1*H*-imidazolyl)benzene). The temperature dependent gate-opening allows it to show a sieving separation of C<sub>2</sub>H<sub>4</sub>/C<sub>2</sub>H<sub>2</sub>/CO<sub>2</sub> mixtures.

However, this framework cannot separate the equimolar C<sub>3</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> due to a small difference in uptake at this ratio caused by the gate-opening effect which either occurs too early or too late (Fig. S2†). Inspired by reticular chemistry<sup>38</sup> and NTU-65, herein, we report a fine tuning of the framework softness *via* node substitution in a series of PCPs (NTU-65-series: NTU-65-FeZr, NTU-65-FeTi, NTU-65-CoZr and NTU-65-CoTi, Scheme 1), as the metal nodes may alter the transformation characteristics of soft structures. As expected, a sole gate-opening toward C<sub>3</sub>H<sub>4</sub> in NTU-65-FeZr evolves into a gradient response to C<sub>3</sub>H<sub>4</sub> and C<sub>3</sub>H<sub>6</sub> in NTU-65-CoTi, yielding an unprecedented breakthrough of sieving separation of C<sub>3</sub>H<sub>4</sub>/C<sub>3</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub>.

## Results and discussion

Solvothermal reactions of L and the corresponding metal salt provide NTU-65-series (Fig. S3†). They crystallize in the monoclinic system (Table S1†) and adopt the same coordination configurations. The M1 centres (M1: Fe<sup>2+</sup> or Co<sup>2+</sup>) of NTU-65-series are connected by four imidazole N atoms in a planar configuration from four L and two F atoms in the axial vertex from two M<sub>2</sub>F<sub>6</sub><sup>2-</sup> (M<sub>2</sub>: Zr<sup>4+</sup> or Ti<sup>4+</sup>) ions. As a result, cross-linked 2D channels are observed in the packed frameworks, although the window apertures undergo minimal changes (Fig. 1a, b and S4–S8†), along with similar accessible volumes (43.5%, 44.8%, 42.4% and 44.8%).<sup>39</sup> To reach the adjacent nodes, the dihedral angle between the benzene and imidazole rings in L in NTU-65-series shows significant changes. For example, the angle of the L<sub>Cis</sub> in NTU-65-FeZr is as large as 14.81°, while this angle decreases to 3.45° in NTU-65-FeTi (Fig. 1c). Additionally, the dihedral angle in L<sub>Trans</sub> in NTU-65-CoTi is up to 22.69°. Therefore, different degrees of softness are expected in the NTU-65-series. Phase purity of the four crystals has been confirmed by X-ray powder diffraction measurement (Fig. S9†). In addition, all samples are thermally stable, up to 350 °C (Fig. S10†).

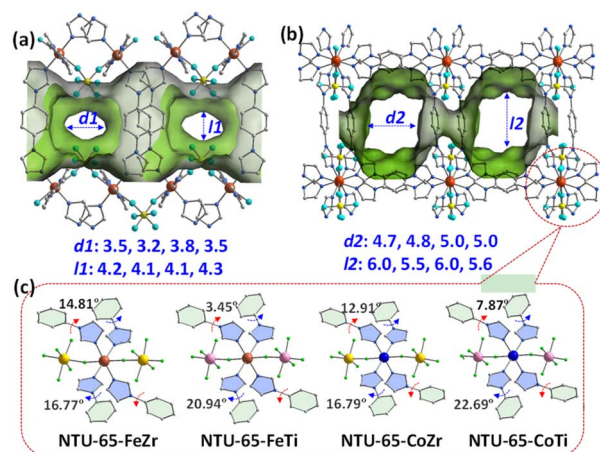


Fig. 1 Crystal structure of NTU-65-series along the *a*-axis (a) and *b*-axis (b). Comparison of the dihedral angle in L in NTU-65 series (c).

Permanent porosity of the activated NTU-65-series was evaluated using N<sub>2</sub> adsorption measurements at 77 K (Fig. S12†). Initially, all samples show minimal N<sub>2</sub> uptake until reaching  $P/P_0 = 0.61, 0.26, 0.27$  and  $0.24$ . However, a peculiar ‘kink’ phenomenon occurred in all of them. This is due to the rapid increase in adsorption capacity of the crystals after instantaneous gate-opening under this condition, accompanied by a rapid decrease in system pressure, to  $P/P_0 = 0.10, 0.07, 0.05$  and  $0.04$ , respectively. Subsequently, N<sub>2</sub> uptake increases with increased pressure in NTU-65-FeZr, while type-I adsorption isotherms were observed in NTU-65-FeTi and NTU-65-CoTi. Differently, NTU-65-CoZr exhibits a second adsorption platform before reaching  $P/P_0 = 0.6$ , followed by pressure-dependent uptake. Despite these differences, all four crystals demonstrated a similar maximum N<sub>2</sub> capacity (219.5 to 236.2 cm<sup>3</sup> g<sup>-1</sup>). Evaluated by using these isotherms, the crystals exhibit comparable surface areas (540–610 m<sup>2</sup> g<sup>-1</sup>) and pore volumes (0.34–0.36 cm<sup>3</sup> g<sup>-1</sup>) (Fig. S13, S14 and Table S2†). Additionally, all isotherms display desorption hysteresis, confirming the filling effect of the soft frameworks.<sup>40,41</sup>

To further investigate structural softness, CO<sub>2</sub> isotherms were collected at 195 K, as CO<sub>2</sub> may interact differently with the frameworks compared to N<sub>2</sub>.<sup>42,43</sup> Unlike the ‘kink’ phenomenon in the above N<sub>2</sub> isotherms, all CO<sub>2</sub> uptakes of the NTU-65-series increase with elevated pressure. Meanwhile, gradient adsorption platforms indicating sequential gate-openings were clearly observed in NTU-65-series. For NTU-65-FeZr, the first gate-opening occurs at 2.1 kPa, followed by the second and third gate-opening at 22.8 and 56.3 kPa, respectively (Fig. 2a). However, NTU-65-FeTi shows an earlier first gate-opening pressure (OP) of 1.7 kPa. The second and third gate-openings in NTU-65-FeZr merge into one in NTU-65-FeTi, at 31.4 kPa (Fig. 2b). Notably, three gate-openings appear again in NTU-65-CoZr (starting at 0.8, 14.6 and 45.8 kPa), whose responsive pressures are all lower than that of NTU-65-FeZr, and the first OP is also lower than that of NTU-65-FeTi (Fig. 2c). Remarkably, NTU-65-CoTi exhibits an advancement of the first OP at 0.5 kPa, followed by a second quick uptake at 18.8 kPa (Fig. 2d). Therefore, these isotherms



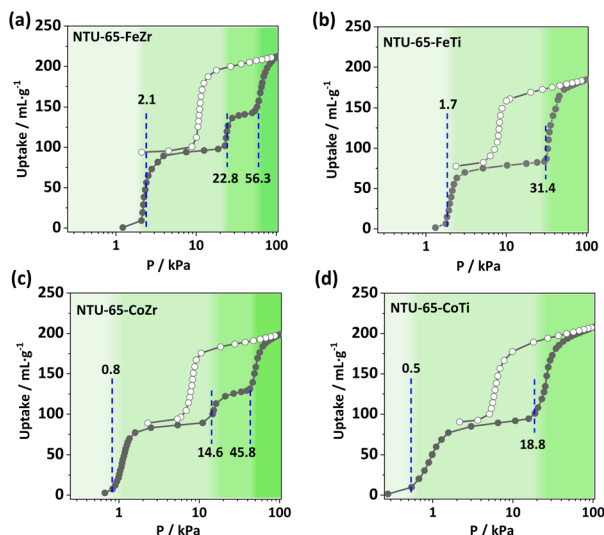


Fig. 2  $\text{CO}_2$  adsorption isotherms of NTU-65-series (a)–(d) at 195 K.

indicate that the four activated crystals possess non-porous characteristics and can be opened by  $\text{N}_2$  or  $\text{CO}_2$  once the stimuli exceed the energy barrier controlling the framework closure. Meanwhile, the gradually decreased pressure (2.1 to 0.5 kPa) for the first gate-opening reflects the fact that the four frameworks show different sensitivities to external stimuli. Additionally, the difference in multi-step gate-openings in them validates the effectiveness of the node substitution strategy in regulation of the framework with gradient softness, which may provide a promising platform for sequential recognition of gases with extremely small differences.

To investigate the function of gradient and sensitive gate-openings, adsorption isotherms of  $\text{C}_3\text{H}_4$ ,  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  were collected on NTU-65-series (Fig. 3 and S15–S18†). NTU-65-FeZr

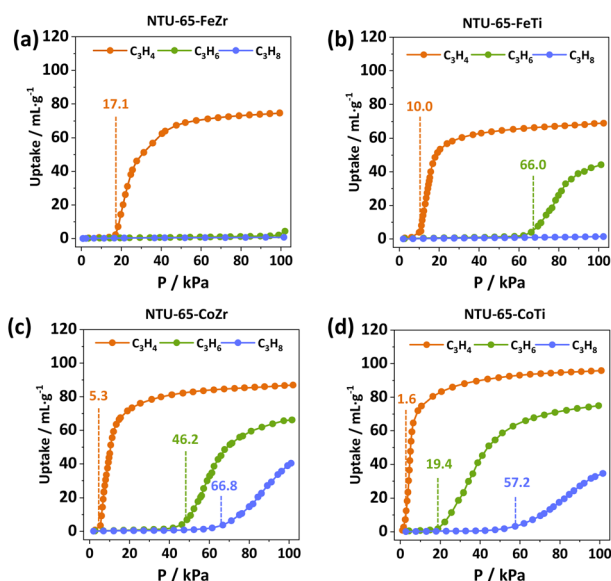


Fig. 3  $\text{C}_3\text{H}_4$ ,  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  adsorption isotherms of NTU-65-series (a)–(d) at 273 K.

exhibits minimal uptake of  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  at the threshold pressure, whereas  $\text{C}_3\text{H}_4$  adsorption begins at 17.1 kPa with a maximum capacity of  $74.7 \text{ cm}^3 \text{ g}^{-1}$  (Fig. 3a). Meanwhile, the starting OP is advanced to 10.0 kPa in NTU-65-FeTi, along with nearly the same  $\text{C}_3\text{H}_4$  capacity ( $69.0 \text{ cm}^3 \text{ g}^{-1}$ ) (Fig. 3b). Unlike NTU-65-FeZr,  $\text{C}_3\text{H}_6$  molecules open the framework of NTU-65-FeTi at 66.0 kPa with a capacity of  $44.2 \text{ cm}^3 \text{ g}^{-1}$  at 100 kPa (Fig. 3c). Interestingly, the OP of the three gases ( $\text{C}_3\text{H}_4$ : 5.3 kPa,  $\text{C}_3\text{H}_6$ : 46.2 kPa and  $\text{C}_3\text{H}_8$ : 66.8 kPa) exhibit a forward movement again in NTU-65-CoZr (Fig. 3d). However, the isotherms indicate two crucial issues that may arise during the dynamic separation of such ternary mixtures: (1) insufficient partial pressure for  $\text{C}_3\text{H}_4$  adsorption (far larger than 1 kPa); and (2) lower separation performance between  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  (small uptake difference of only  $7.6 \text{ cm}^3 \text{ g}^{-1}$  at around 50 kPa). Remarkably, these issues may be solved by using NTU-65-CoTi, which exhibits rapid uptake of  $\text{C}_3\text{H}_4$  at 1.6 kPa and a significantly improved uptake difference between  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$ , reaching as high as  $55.9 \text{ cm}^3 \text{ g}^{-1}$  at 50 kPa. Additionally, the total  $\text{C}_3\text{H}_4$  capacity is increased to  $95.9 \text{ cm}^3 \text{ g}^{-1}$ . Moreover, the uptake ratios of binary mixtures ( $\text{C}_3\text{H}_4/\text{C}_3\text{H}_6$ ,  $\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$  and  $\text{C}_3\text{H}_4/\text{C}_3\text{H}_8$ ) were significantly and simultaneously improved compared to that of other benchmark materials (Table 1 and S3†).

To confirm the systemic structural changes, *in situ* powder X-ray diffraction patterns/sorption measurements were performed (Fig. 4). The characteristic peaks corresponding to crystal faces of  $[0\ 2\ 0]$  and  $[0\ 0\ 1]$  in the as-synthesized phases (at about  $6.5^\circ$  and  $7.2^\circ$ ) become weaker and shift to a higher-angle region in the activated crystals, indicative of structural contraction commonly observed in flexible PCPs. However, these two peaks reappear at similar positions to those obtained from their as-synthesized phases after an increase in pressure. Additionally, these open structures transform back into the closed state when the pressure decreases to a very low value, showing reversible sorption and structural changes in NTU-65-series. In addition, gas-loaded crystallographic analysis has also been attempted to explore the detailed structural changes. However, the small crystal size and crack after activation results in extremely weak or no diffraction. To understand the trend in softness of these PCPs, we conducted density functional theory (DFT) calculations taking  $\text{C}_3\text{H}_4$  as the probe molecule (Fig. S20†). Previously, we have shown that the gate-opening pressure of PCPs induced by gas adsorption is dependent on the binding energy of the gas molecule with the PCP.<sup>44</sup> We therefore calculated the binding energies of  $\text{C}_3\text{H}_4$  with the NTU-65-series. The binding energy increases (becomes more negative) in the following order: NTU-65-FeZr ( $-7.8 \text{ kcal mol}^{-1}$ ) < NTU-65-FeTi ( $-8.1 \text{ kcal mol}^{-1}$ ) < NTU-65-CoZr ( $-8.5 \text{ kcal mol}^{-1}$ ) < NTU-65-CoTi ( $-9.1 \text{ kcal mol}^{-1}$ ). This is consistent with the order of gate-opening pressure of these PCPs in response to  $\text{C}_3\text{H}_4$  adsorption for these PCPs (Fig. 3).

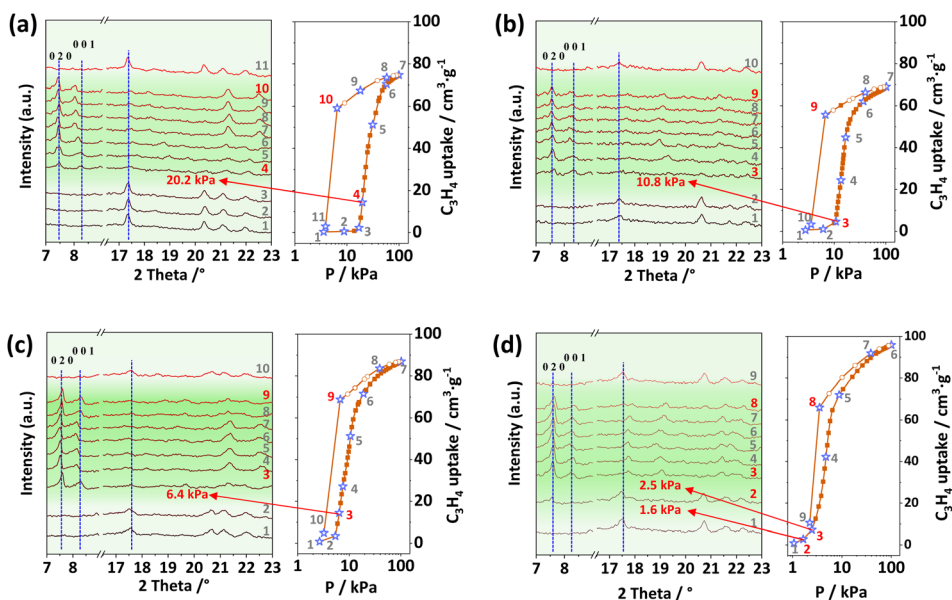
The sequential recognition of C3 hydrocarbons encouraged us to perform dynamic separations. Given the commonly encountered ratio of C3 hydrocarbons in industry, a simulated feed-gas of  $\text{C}_3\text{H}_4/\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$  (0.5/49.75/49.75, v/v/v) was used for breakthrough experiments at 273 K. Consistent with the single-component gas isotherms,  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  elute simultaneously





Table 1 Summarized capacities ( $\text{cm}^3 \text{g}^{-1}$ ) and uptake ratios of C3 hydrocarbons for NTU-65-series at 273 K

PCPs	$\text{C}_3\text{H}_4$	$\text{C}_3\text{H}_6$	$\text{C}_3\text{H}_8$	Uptake ratios		
	0.1 bar	0.5 bar	0.5 bar	$\text{C}_3\text{H}_4/\text{C}_3\text{H}_6$ (0.1/0.5)	$\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$ (0.5/0.5)	$\text{C}_3\text{H}_4/\text{C}_3\text{H}_8$ (0.1/0.5)
NTU-65-CoTi	73.93	57.44	1.55	1.28	37.05	47.70
NTU-65-CoZr	46.24	8.55	0.96	5.41	8.91	48.17
NTU-65-FeTi	3.93	1.27	0.73	3.01	1.74	5.34
NTU-65-FeZr	0.59	0.74	0.51	0.80	1.45	1.16

Fig. 4 *In situ* PXRD patterns of NTU-65-FeZr (a), NTU-65-FeTi (b), NTU-65-CoZr (c) and NTU-65-CoTi (d) during  $\text{C}_3\text{H}_4$  adsorption/desorption at 273 K.

from the NTU-65-FeZr sample bed, while  $\text{C}_3\text{H}_4$  was captured until  $85.8 \text{ min g}^{-1}$ , showing impossible ternary separation (Fig. 5a). For NTU-65-CoZr,  $\text{C}_3\text{H}_8$  was detected as the first elution at  $19.3 \text{ min g}^{-1}$ , followed by  $\text{C}_3\text{H}_6$  at  $27.8 \text{ min g}^{-1}$ . Additionally,  $\text{C}_3\text{H}_4$  passes through the column at  $106.3 \text{ min g}^{-1}$  (Fig. 5b). Considering the OP of  $\text{C}_3\text{H}_6$  (46.2 kPa) and the small uptake difference ( $7.6 \text{ cm}^3 \text{g}^{-1}$ ) of  $\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$  in NTU-65-CoZr, the observable separation time of  $\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$  should be attributed to the slight pore opening, caused by accumulated  $\text{C}_3\text{H}_6$  adsorption. This phenomenon is similar to the selective  $\text{C}_3\text{H}_4$  or  $\text{C}_2\text{H}_2$  capture in GeFSIX-dps-Zn<sup>45</sup> and Co(4-DPDS)<sub>2</sub>MoO<sub>4</sub>,<sup>46</sup> respectively, where the partial pressures of  $\text{C}_3\text{H}_4$  (10 kPa) or  $\text{C}_2\text{H}_2$  (1 kPa) in the feed-gas for breakthrough separations are lower than that of the corresponding OPs ( $\sim 16 \text{ kPa}$  and  $\sim 17 \text{ kPa}$ ) of the frameworks at the same temperature. In addition, a similar and insufficient ternary separation was also observed in NTU-65-FeTi. Remarkably, NTU-65-CoTi exhibits a significant separation of the ternary mixture of  $\text{C}_3\text{H}_4/\text{C}_3\text{H}_6/\text{C}_3\text{H}_8$ , in which highly pure  $\text{C}_3\text{H}_8$  elutes out at  $17.0 \text{ min g}^{-1}$ , while the outflows of  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_4$  from the sample bed are around  $41.1 \text{ min g}^{-1}$  and  $132.9 \text{ min g}^{-1}$  (Fig. 5c). Additionally, the further extended retention time of  $\text{C}_3\text{H}_4$  (from  $85.8 \text{ min g}^{-1}$  in NTU-65-FeZr to  $132.9 \text{ min g}^{-1}$  in NTU-65-CoTi) reflects the increased

cumulative effect in NTU-65-series, as structural deformation becomes easier. To the best of our knowledge, the PCPs, including rigid and soft frameworks, have been widely explored for gas separations; however, this is the first example that can separate C3 hydrocarbons in one-step in a single domain. Furthermore, this promising separation was also confirmed at increased velocity (5 and  $10 \text{ mL min}^{-1}$ ) of such ternary mixtures, as well as the binary mixtures (Fig. S21–S27 and Tables S4–S7†). More importantly, due to the reversible structural changes, there is almost no performance loss during the cycling measurements on NTU-65-CoTi (Fig. 5d and S28†), a critical factor in evaluating the feasibility of the adsorbents.

Based on these breakthrough results, how the NTU-65-CoTi might be possible to procure pure  $\text{C}_3\text{H}_6$  and  $\text{C}_3\text{H}_8$  are mostly expected. As shown in Fig. 5e, two beds are needed, Bed A and B, both packed with NTU-65-CoTi.<sup>47,48</sup> During the adsorption cycle, the two beds A and B operate sequentially. The operation of Bed A and B should last for at least  $130 \text{ min g}^{-1}$  and  $35 \text{ min g}^{-1}$ , respectively. Highly pure  $\text{C}_3\text{H}_8$  (99.9%, GC limitation) is recovered from Bed B at the end of the adsorption cycle. After termination of the adsorption cycle, both Bed A and B are subjected to counter-current vacuum desorption. From Bed A, the product  $\text{C}_3\text{H}_4$  with improved concentration (from 0.5% to



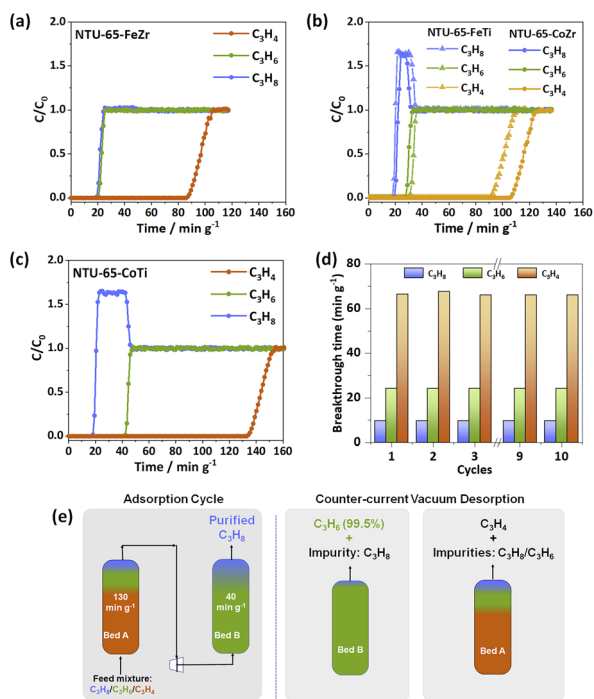


Fig. 5 Breakthrough curves of NTU-65-series (a)–(d) for  $C_3H_4/C_3H_6/C_3H_8$  (0.5/49.75/49.75, v/v/v,  $2 \text{ mL min}^{-1}$ ) at 273 K. Cycling performance of NTU-65-CoTi ( $5 \text{ mL min}^{-1}$ ) (d). Schematic representation of the separation of C3 ternary mixtures using two packed beds of NTU-65-CoTi in a vacuum swing adsorption process (e).

6.3%) can be obtained, while from Bed B, the product  $C_3H_6$  can be harvested with a purity approaching 99.5%.

## Conclusions

In summary, due to the demand for energy-efficient separation of C3 hydrocarbons, we here report a gradient regulation of framework softness *via* the node substitution approach. The exclusive response to  $C_3H_4$  in NTU-65-FeZr has been tailored into a sequential capture of  $C_3H_4$  and  $C_3H_6$  in NTU-65-CoTi. This breakthrough enables an unprecedented ability for sieving separation of the ternary  $C_3H_4/C_3H_6/C_3H_8$  mixtures in a single domain. By following designed procedures, highly pure  $C_3H_8$  (99.9%) and  $C_3H_6$  (99.5%) can be obtained. Moving forward, given that the conditions for feasible gas separation vary significantly, the precise understanding and ability to tune the gate-openings of soft PCPs are particularly important, potentially indicating a path to other challenging multi-component systems.

## Data availability

The data supporting the findings of this study are available within the article and/or its ESI.†

## Author contributions

J. D. conceived the research idea and designed the experiments. S. L. and Y. H. conducted the experiments. S. L., Y. H., J. W.,

Y. L., and J. T. analysed and discussed the data. J. Z. and K. R. performed the calculations. J. D. and K. G. wrote the paper. All authors offered constructive comments on the manuscript.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

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