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Sunlight-driven and gram-scale vanillin production via Mn-defected γ -MnO₂ catalyst in aqueous environment†

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The production of vanillin from biomass offers a sustainable route for synthesizing daily-use chemicals. However, achieving sunlight-driven vanillin synthesis through H₂O activation in an aqueous environment poses challenges due to the high barrier of H₂O dissociation. In this study, we have successfully developed an efficient approach for gram-scale vanillin synthesis in an aqueous reaction, employing Mn-defected γ -MnO₂ as a photocatalyst at room temperature. Density functional theory calculations reveal that the presence of defective Mn species (Mn³⁺) significantly enhances the adsorption of vanillyl alcohol and H₂O onto the surface of the γ -MnO₂ catalyst. Hydroxyl radical ([•]OH) species are formed through H₂O activation with the assistance of sunlight, playing a pivotal role as oxygen-reactive species in the oxidation of vanillyl alcohol into vanillin. The Mn-defected γ -MnO₂ catalyst exhibits exceptional performance, achieving up to 93.4% conversion of vanillyl alcohol and 95.7% selectivity of vanillin under sunlight. Notably, even in a laboratory setting during the daytime, the Mn-defected γ -MnO₂ catalyst demonstrates significantly higher catalytic performance compared to the dark environment. This work presents a highly effective and promising strategy for low-cost and environmentally benign vanillin synthesis.

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Introduction

Vanillin, a highly popular spice worldwide, is extensively used in food additives, perfumes, and daily-use chemicals.¹ Traditionally, it is derived from fossil fuels through the Solvay route,² which involves the oxidation of vanillyl alcohol to vanillin using methanol as a solvent. In addition to the Solvay route, about

15% of vanillin is directly isolated from depolymerized lignin derivatives through upcycling,^{3–5} presenting an eco-friendly method that avoids reliance on fossil fuels. However, only approximately 2% of lignin currently undergoes conversion to value-added chemicals, with the remaining 98% being incinerated for energy in the pulp and paper industry. Consequently, a significant challenge in terms of sustainability and environmental protection lies in the valorization of lignin.^{6–9} Among potential approaches, the synthetic vanillin market, producing around 17 000 tons per year, primarily relies on fossil-based routes. Chemical conversions of lignin-derived compounds, such as vanillyl alcohol, offer a sustainable and cost-effective route to replenish the synthetic vanillin market.¹⁰ Unfortunately, most lignin-to-vanillin processes operate in organic solvents, requiring high temperature/O₂ pressure,⁶ and consuming artificial energy due to recrystallization and solvent extraction steps.¹¹ In response to these drawbacks, the development of sunlight-driven organic transformations through the construction of novel heterogeneous catalyst materials that are efficient and separable even in aqueous reactions holds promise for the sustainable synthesis of valuable chemicals.¹²

The water-participated route for alcohol oxidation signifies a noteworthy advancement in organic synthesis,¹³ offering a novel and sustainable approach to vanillin synthesis. However, this oxidation process encounters challenges due to the energy-

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demanding O–H bond activation of H₂O.¹⁴ While light-driven H₂O dissociation has emerged as an attractive method to activate the O–H bond, the limited success cases of this process mainly rely on noble metal catalysts and artificial light sources, such as a Xenon lamp.¹⁵ An effective strategy for manipulating the H₂O dissociation pathway, including the energy requirement for O–H bond activation and the chemical nature of the active metal/oxygen species, involves the coordination engineering of metal oxide catalysts. The coordination engineering of bismuth (Bi) and oxygen (O) sites in the BiOBr catalyst has successfully demonstrated the enhancement of ethylbenzene oxidation through sunlight-driven reduction of the adsorption barrier for H₂O activation.¹⁵ However, investigations into the sunlight-driven synthesis of vanillin in an aqueous environment using metal oxides remain relatively scarce.

MnO₂, a transition metal oxide, has garnered significant attention as a heterogeneous catalyst for catalytic oxidation reactions, owing to its inherent advantages, including multivalence (Mn²⁺, Mn³⁺, and Mn⁴⁺)¹⁶ and a variable structure (α -, γ -, ϵ -, R-, and β -MnO₂).¹⁷ Among these structures, γ -MnO₂, characterized by a disordered structure comprising the intergrowth of β -MnO₂ and R-MnO₂, stands out as one of the most extensively studied manganese dioxides.^{18,19} Herein, we report the successful fabrication of a Mn-defected γ -MnO₂ catalyst for the water-participated oxidation of vanillyl alcohol to vanillin in an aqueous reaction under sunlight illumination. Our approach offers several notable advantages (Table S1†): (1) the use of H₂O as a green reaction medium and oxygen source, promoting environmental sustainability; (2) utilization of sunlight as the energy source for H₂O activation, reducing reliance on artificial light sources; (3) conducting the reaction at room temperature, minimizing energy requirements, and enabling milder reaction conditions; (4) the possibility of achieving gram-scale reactions, allowing for large-scale production; (5) a separable, additive-free, and carbon-efficient protocol, enhancing the overall efficiency and sustainability of the process.

Results and discussion

γ -MnO₂ catalysts with defects in Mn species were obtained through a hydrothermal process (Fig. 1a, see ESI† for preparation details). The crystal structures of the as-prepared γ -MnO₂ catalysts were characterized using powder X-ray diffraction (PXRD). As shown in Fig. 1b and S1,† regardless of the amount of urea, the synthesized γ -MnO₂, γ -MnO₂(1), and γ -MnO₂(10) catalysts (1 and 10 referring to the feeding amount of urea) exhibit peaks at $2\theta = 22.4^\circ$, 37.0° , 42.3° , and 56.0° , corresponding to the (120), (131), (300), and (160) planes, respectively. These planes are well indexed to the layered γ -MnO₂ (JCPDS-14-0644).^{20,21} For comparison, MnO₂ catalysts with different crystal structures, such as α -MnO₂, β -MnO₂, and ϵ -MnO₂, were synthesized using different raw materials²² and characterized by PXRD (Fig. S2†). Scanning electron microscopy (SEM) and transmission electron microscopy (TEM) analyses reveal that the as-prepared γ -MnO₂ particles exhibit a spherical shape with a size of 6 μm (Fig. 1c), in which nanorods with a thickness of several tens of nanometers are assembled (Fig. 1d and e). In the selected area electron

diffraction (SAED) pattern (Fig. 1f) and high-resolution TEM (HRTEM) image (Fig. 1g) of γ -MnO₂ nanorods, crystalline spaces of 0.24 and 0.39 nm corresponding to the (131)^{23,24} and (120)^{25,26} planes of γ -MnO₂, respectively, are observed, consistent with the XRD results. Energy-dispersive X-ray spectroscopy (EDS) mapping confirms the uniform dispersion of Mn and O throughout the γ -MnO₂ particle (Fig. 1h). Notably, no N residue is observed for γ -MnO₂ according to X-ray photoelectron spectroscopy (XPS) characterization (Fig. S3a†). Both γ -MnO₂(1) and γ -MnO₂(10) particles synthesized in the presence of urea exhibit a morphology observed in SEM images (Fig. S4†), a crystal structure observed in TEM images (Fig. S5†), and N₂ adsorption-desorption isotherms (Fig. S6†) similar to γ -MnO₂ synthesized without urea.

XPS is a regular and powerful tool used to identify the surface elemental species and electronic states of materials. Fig. 2 and S7–S10† show the Mn 3s, Mn 2p, and O 1s XPS patterns of the as-prepared α -MnO₂, β -MnO₂, ϵ -MnO₂, and γ -MnO₂ catalysts. The ΔE_s (binding energy between two peaks of Mn 3s multiplet splitting) of the γ -MnO₂ catalysts in the range of 4.5–5.1 eV confirm the presence of Mn³⁺ species (Fig. 2a),²⁷ indicating the coexistence of both Mn³⁺ and Mn⁴⁺ species in these catalysts. The average oxidation states (AOS) of Mn species are calculated using the following formula.^{28,29}

$$\text{AOS} = 8.956 - 1.126\Delta E_s$$

As shown in Fig. 2a, the calculated AOS values are 3.2, 3.4, and 3.9 for γ -MnO₂, γ -MnO₂(1), and γ -MnO₂(10), respectively, consistent with the Mn³⁺/Mn⁴⁺ ratios (Fig. S7a–c,† Mn³⁺/Mn⁴⁺ = 1.54, 1.36, and 1.28 for γ -MnO₂, γ -MnO₂(1), and γ -MnO₂(10) particles, respectively). It's worth noting that the oxygen defects (O_d) remain almost constant in γ -MnO₂, γ -MnO₂(1), and γ -MnO₂(10) (37.2–39.3%), as shown in Fig. S7d–f.† Interestingly, MnO₂ with different crystal structures exhibits varying degrees of Mn defects (Mn_d) associated with Mn³⁺ species (Fig. 2b). The calculated AOS values are 3.8, 3.8, and 4.0 for α -MnO₂, β -MnO₂, and ϵ -MnO₂, respectively, with corresponding ratios of Mn³⁺/Mn⁴⁺ being 1.51, 1.50, and 1.47 (Fig. S8†). The highest ratio of Mn³⁺/Mn⁴⁺ (1.54) in γ -MnO₂ among the MnO₂ is ascribed to its most abundant Mn_d caused by the coordination unsaturation between the lattice oxygen and lattice Mn. Typically, unsaturated metal species and O_d species, which are active in various oxidation reactions, coexist in metal oxides.^{30,31} It is well known that Mn_d, caused by coordination unsaturation between lattice oxygen and lattice Mn, can be tuned by inducing O_d or adjusting non-metal dopant amounts.^{32–34} Contrary to the almost constant presence of O_d species (Fig. 2c), significantly higher N dopants are observed in γ -MnO₂(1) and γ -MnO₂(10) compared to γ -MnO₂ (Fig. S3†).³⁵ The N anionic (N³⁻) dopants possess excess negative charges compared to the O anionic (O²⁻),³⁶ leading to a higher AOS of Mn species due to the charge compensation for higher N dopants. A similar higher AOS of Mn species in MnO₂ was previously observed with boron doping.³⁷ For comparison, we synthesized α -MnO₂ catalysts with different O_d sites. As shown in Fig. 2d and S9,† surface O_d sites in α -MnO₂ catalysts significantly increase after the addition of urea during



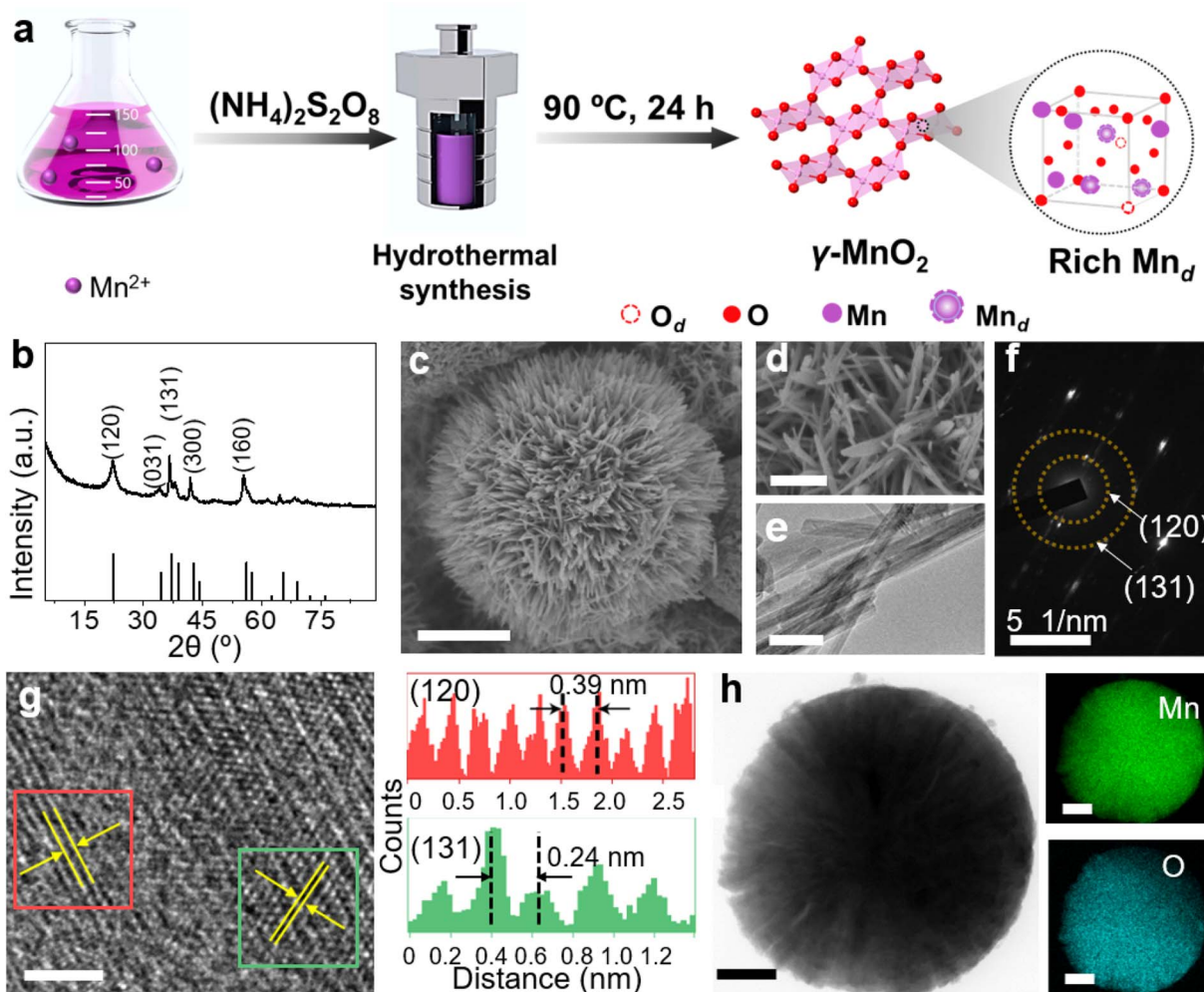


Fig. 1 (a) Schematic synthesis process of γ - MnO_2 catalysts with Mn defects (Mn_d). (b) PXRD pattern, (c and d) SEM images, (e) TEM image, (f) SAED pattern, and (g) HRTEM image (left) and corresponding intensity plot (right) of γ - MnO_2 catalyst. (h) EDX elemental maps showing the distributions of Mn and O. Scale bars: (c) 2 μm , (d) 500 nm, (e) 50 nm, (g) 2 nm, (h) 1 μm .

the hydrothermal process, while the Mn^{3+} species remain almost constant (Fig. S10[†]). The nearly unchanged ratio of $\text{Mn}^{3+}/\text{Mn}^{4+}$, despite the differing amounts of O_d species in α - $\text{MnO}_2(1)$ and α - $\text{MnO}_2(10)$, may be attributed to the presence of N anionic residues. The detailed mechanisms of O_d species formation are beyond the scope of the current stage of study and will be pursued in our future work.

To demonstrate the practicality of our approach, we conducted a gram-scale oxidation of vanillyl alcohol to vanillin in an aqueous environment as a model reaction, and the results are presented in Table 1. For the catalytic reaction, 0.77 g of vanillyl alcohol, 6.0 mL of H_2O , and 10.0 mmol of catalyst were added to a quartz reactor and stirred at room temperature under sunlight for 10 h while exposed to air. No product is obtained in the absence of a catalyst (Table 1, entry 1). The as-prepared MnO_2 catalysts, including α -, β -, ε -, and γ - MnO_2 (Table 1, entries 2–9), are found to be active for the oxidation of vanillyl alcohol to vanillin. MnO_2 catalysts with more abundant O_d (Fig. 2d), such as α - $\text{MnO}_2(1)$ and α - $\text{MnO}_2(10)$, exhibit lower catalytic performance compared to α - MnO_2 with fewer O_d ,

indicating that O_d species are not a key factor in promoting the catalytic activity of MnO_2 catalysts for the oxidation under sunlight. The γ - MnO_2 catalyst exhibits the highest catalytic activity and vanillin selectivity, converting vanillyl alcohol to vanillin with a yield of nearly 90% (Table 1, entry 2), outperforming the γ - $\text{MnO}_2(1)$ and γ - $\text{MnO}_2(10)$ catalysts (Table 1, entries 3,4). Since γ - MnO_2 , γ - $\text{MnO}_2(1)$, and γ - $\text{MnO}_2(10)$ catalysts have similar surface O_d species (Fig. 2c), Brunauer–Emmett–Teller (BET) surface areas (Fig. S6[†]), and surface morphologies (Fig. 1c, d and S4[†]), the superior catalytic performance of the γ - MnO_2 catalyst among them can be attributed to the most abundant Mn_d species on the surface (Fig. 3a). Similarly, the best vanillin selectivity and superior catalytic performance displayed by γ - MnO_2 , compared to other MnO_2 catalysts with diverse crystal structures (Table 1, entries 2–5 and 9–10), can be attributed to the prevalence of its Mn_d species (Fig. 3). Given the significant influence of factors, such as solvent and temperature, on the catalytic oxidation reaction of vanillyl alcohol,³⁸ we explored various conditions using the γ - MnO_2 catalyst to determine the optimal reaction parameters.



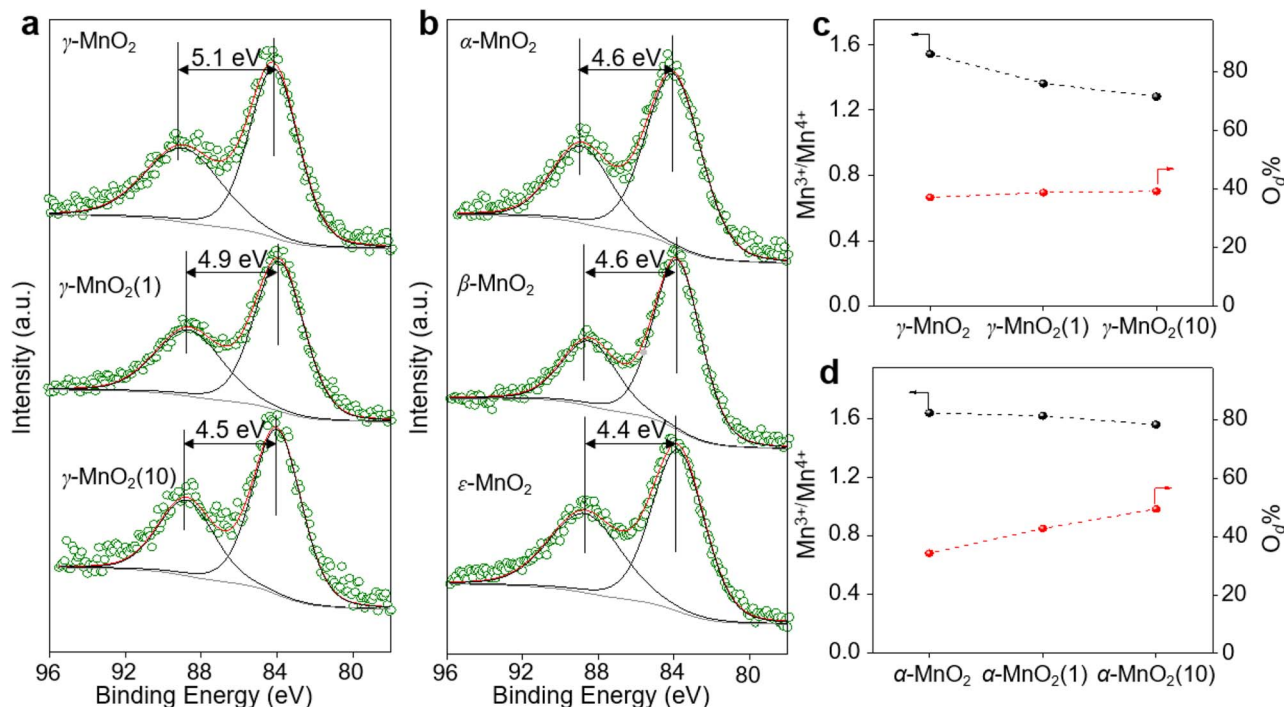
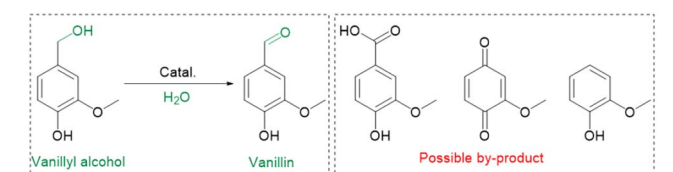


Fig. 2 Mn 3s XPS spectra for (a) γ -MnO₂ with different amounts of urea added in the synthesis and (b) MnO₂ with different crystal structures. The molar ratio of Mn³⁺/Mn⁴⁺ and percentage of oxygen defects (O_d) in different (c) γ -MnO₂ and (d) α -MnO₂.

Table 1 Oxidation of vanillyl alcohol to vanillin over various catalysts



Entry	Catalyst	Con.%	Sel.% ^a	Yield%
1	—	n.d.	—	—
2	γ -MnO ₂	93.4	95.7	89.4
3	γ -MnO ₂ (1)	66.3	95.5	63.3
4	γ -MnO ₂ (10)	63.3	94.9	60.1
5	α -MnO ₂	60.8	86.3	52.5
6	α -MnO ₂ (1)	25.5	45.7	11.7
7	α -MnO ₂ (10)	26.0	54.0	14.0
8	β -MnO ₂	63.0	94.4	59.5
9	ϵ -MnO ₂	61.4	91.3	56.1

^a Selective generation of vanillin. Reaction conditions: vanillyl alcohol (0.77 g), Solvent (H₂O, 6.0 mL), catalyst 10.0 mmol, open to air, sunlight, 30 °C, 10 h. (n.d. = Not detected).

The γ -MnO₂ catalyst exhibits remarkably superior catalytic performance at 30 °C (Table S2†) and when using H₂O as a solvent (Table S3†). The significant improvement in the catalytic performance of γ -MnO₂ catalyst in H₂O compared to other solvents (Table S3†) may be attributed to the role of H₂O in activating O₂/H₂O to form key active O species, as discussed in the following section on the mechanism.

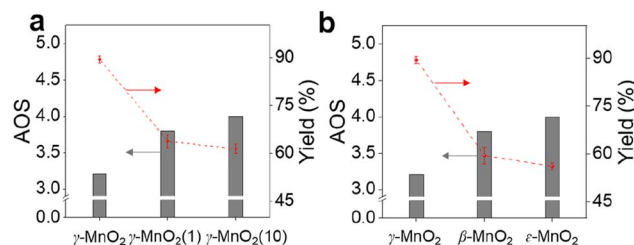


Fig. 3 Catalytic performance of γ -MnO₂ and comparison catalysts for oxidation of vanillyl alcohol to vanillin. (a) AOS-yield of vanillin on γ -MnO₂, (b) AOS-yield of vanillin on MnO₂ with various crystal structures.

To elucidate its superior catalytic performance, the catalytic mechanism of the oxidation of vanillyl alcohol over the γ -MnO₂ catalyst was evaluated. In comparison to the impressive catalytic performance under O₂ (Fig. 4a, eqn (1)), the oxidation of vanillyl alcohol is dramatically suppressed (~6.5% yield of vanillin) when the reaction is performed under N₂ (Fig. 4a, eqn (2)), confirming that oxidation over the γ -MnO₂ catalyst mainly occurs through a dissolved oxygen species-mediated route.³⁹ After the reaction under the N₂ atmosphere, the ratio of surface Mn³⁺/Mn⁴⁺ species increases from 1.54 to 1.63 (Fig. S11†), indicating the involvement of Mn species in the catalytic cycle.

Considering the importance of oxygen in determining oxidative activity, we further elucidate the role of dissolved oxygen species in sunlight oxidation through scavenger control experiments. Despite the addition of furfuryl alcohol (FFA, an efficient scavenger of ¹O₂) to the reactants, the yield of vanillin is 89.4% (Fig. 4a, eqn (3)), indicating that FFA does not affect



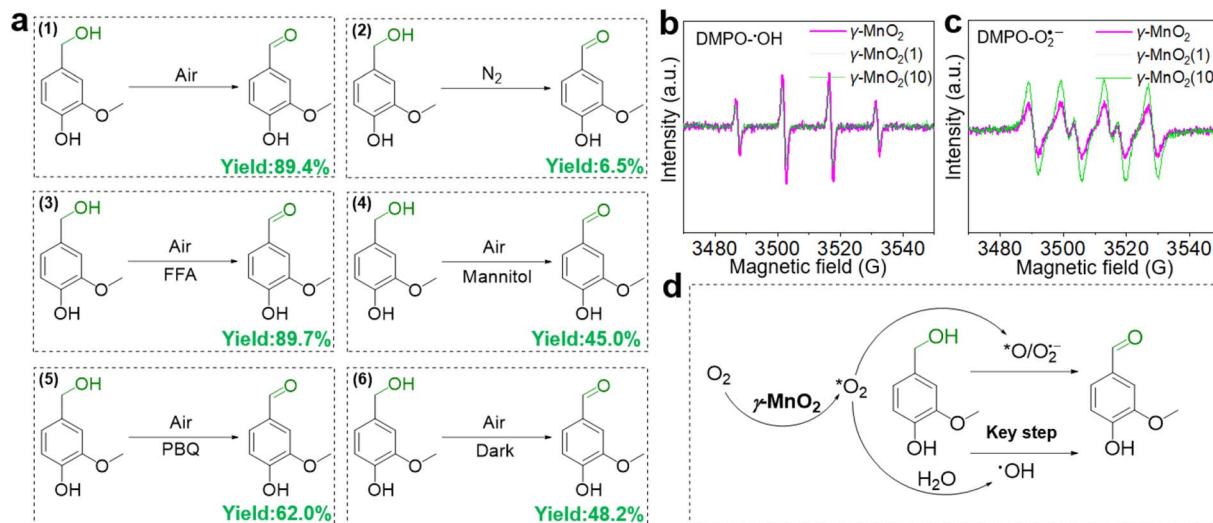


Fig. 4 Exploring the role of oxygen species in the oxidation of vanillyl alcohol over γ -MnO₂ catalyst. (a) Oxidation of vanillyl alcohol under different atmospheres or with various quenchers. (b and c) EPR spectra of DMPO- OH^{\bullet} and DMPO- $\text{O}_2^{\bullet-}$ over various γ -MnO₂ catalysts. (d) Proposed the role of oxygen species in the oxidation of vanillyl alcohol. $\text{O}_2^{\bullet-}$ refers to the adsorbed oxygen.

the activity of the γ -MnO₂ catalyst. On the other hand, mannitol (an efficient scavenger of OH^{\bullet}) causes a significant decrease in the yield of vanillin (~45.0%) (Fig. 4a, eqn (4)). With 1,4-Benzoquinone (PBQ, an efficient scavenger of $\text{O}_2^{\bullet-}$) added during the reaction, only a normal conversion inhibition of vanillyl alcohol is observed and ~62.0% yield of vanillin is obtained (Fig. 4a, eqn (5)). The above analyses confirm that the oxidation of vanillyl alcohol to vanillin under sunlight occurs with the assistance of $\text{O}_2^{\bullet-}$ and OH^{\bullet} species derived from $\text{O}_2/\text{H}_2\text{O}$ activation by the γ -MnO₂ catalyst.

Electron paramagnetic resonance (EPR) was employed to confirm the presence of $\text{O}_2^{\bullet-}$ and OH^{\bullet} species during the oxidation process.⁴⁰ Under the reaction conditions, a quadruple peak with an intensity ratio of 1:2:2:1 is observed for the characteristic peak of pyrroline nitrogen oxide (DMPO)- OH^{\bullet} (Fig. 4b).⁴¹ Another quadruple peak with an intensity ratio of 1:1:1:1 is observed for the characteristic peak of DMPO- $\text{O}_2^{\bullet-}$ (Fig. 4c),⁴² indicating the formation of $\text{O}_2^{\bullet-}$ and OH^{\bullet} species. Notably, the peak intensity of DMPO- OH^{\bullet} over the γ -MnO₂ catalyst with superior catalytic activity is stronger than that of γ -MnO₂(1) and γ -MnO₂(10) catalysts with mediocre activity. In contrast, the intensities of DMPO- $\text{O}_2^{\bullet-}$ over the γ -MnO₂ catalyst shows opposite trends. These results further support that OH^{\bullet} species are the key reactive oxygen species in the oxidation reaction of vanillyl alcohol *via* γ -MnO₂ under sunlight (Fig. 4d), consistent with the results in Fig. 4a. Meanwhile, the stronger DMPO- OH^{\bullet} signal for γ -MnO₂ compared to the other two samples indicates enhanced OH^{\bullet} generation due to the rich-Mn_d. Interestingly, under dark conditions, the γ -MnO₂ catalyst achieves a ~48.2% yield of vanillin (Fig. 4a, eqn (6)), similar to the 45.0% yield obtained when mannitol is added to the reaction mixture (Fig. 4a, eqn (4)). Additionally, the γ -MnO₂ catalyst exhibits broad light absorption from ultraviolet to visible light, effectively covering most of the solar spectrum (Fig. S12[†]). This

characteristic enables the abundant generation of OH^{\bullet} species under natural light exposure at 30 °C.

Based on the above analysis, O₂, H₂O, and sunlight emerge as key factors influencing the catalytic performance of the γ -MnO₂ catalyst in the oxidation of vanillyl alcohol. Previous studies have demonstrated that OH^{\bullet} species can be generated from H₂O/O₂ mixtures on δ -MnO₂ or Mn/Na₂WO₄/SiO₂ catalysts under sunlight conditions.^{43,44} To verify the formation of OH^{\bullet} species in H₂O/O₂ mixtures over the γ -MnO₂ catalyst, *in situ* IR spectroscopy was employed, and the results are depicted in Fig. 5. The stretching vibration peaks of OH^{\bullet} species at ~2820, 3711, 3735 and 3750 cm⁻¹ intensify with prolonged sunlight illumination (Fig. 5). However, the stretching vibration of OH^{\bullet} species is not observed in the absence of H₂O (Fig. 5a, black curve) or under dark conditions (Fig. 5a, blue curve). These results indicate that both H₂O and sunlight play crucial roles in the formation of OH^{\bullet} species in H₂O/O₂ mixtures. In the oxidation reaction, oxygen is considered to be the ideal oxidant, with H₂O and H₂O₂ identified as by-products. Identifying these by-products is vital for elucidating the reaction

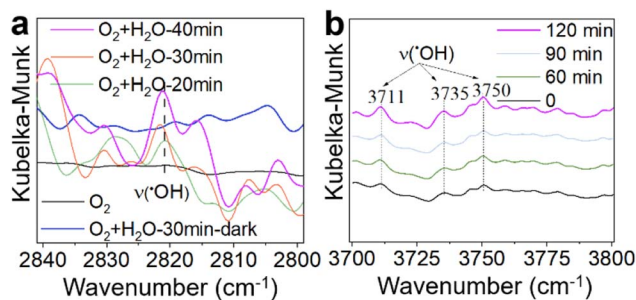


Fig. 5 *In situ* diffuse reflectance IR spectra (DRIFTS) of activation of O₂/H₂O over γ -MnO₂ catalyst. (a) Activation of O₂/H₂O under various conditions. (b) Activation of O₂/H₂O under sunlight illumination.



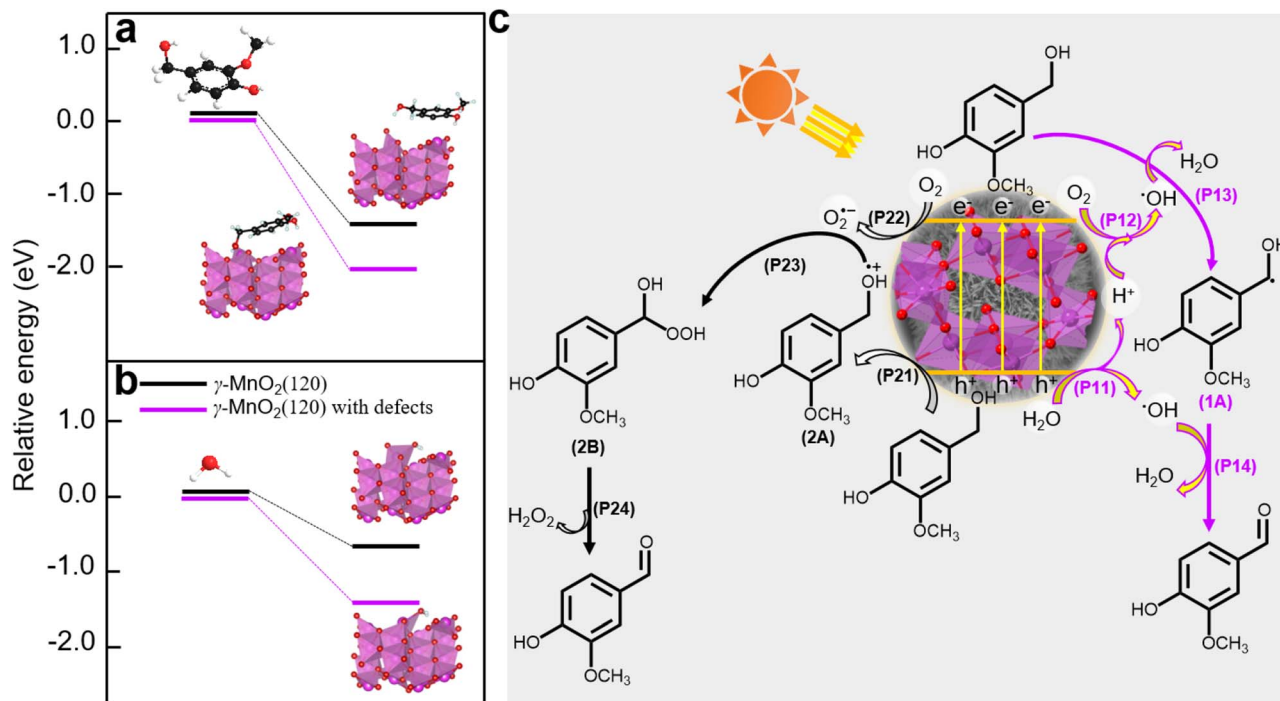


Fig. 6 (a) DFT calculations for vanillyl alcohol adsorbed on γ -MnO₂ catalyst with/without defects. (b) DFT calculations for H₂O adsorbed on γ -MnO₂ catalyst with/without defects. (c) A plausible mechanism of oxidation of vanillyl alcohol to vanillin over γ -MnO₂ catalyst under air atmosphere.

mechanism, especially as \cdot OH species could be produced from H₂O₂ species. Further investigation into the by-product of H₂O₂ species was conducted using the iodometry method, and the results are presented in Fig. S13.† A peak at \sim 365 nm, assigned to the formation of H₂O₂, is detected under sunlight illumination. However, H₂O₂ species are not produced under dark conditions. Similar results are obtained in the absence of a reactant or γ -MnO₂ catalyst. These findings confirm that H₂O₂ species, as a by-product, are produced during the oxidation of vanillyl alcohol to vanillin over the γ -MnO₂ catalyst with the assistance of sunlight illumination.

Density functional theory (DFT) calculations were employed to elucidate the adsorption sites on the γ -MnO₂ catalyst, comprising a perfect (120) facet and defective (120) facets (Fig. S14†). The DFT calculations (Fig. 6a and b) reveal that vanillyl alcohol and H₂O preferentially adsorb on the Mn_d species (Mn³⁺ species) of defective (120) facets, regardless of the presence of O_d species for both models. The preference of vanillyl alcohol for adsorption on the Mn_d species is further supported by DFT calculations in Fig. 6a and S15,† illustrating the interaction between Mn³⁺ species of MnO₂ and vanillyl alcohol. This interaction results in an adsorption energy of -217.3 kJ mol⁻¹ (Fig. S15†), significantly exceeding the adsorption energy of -131.5 kJ mol⁻¹ observed for MnO₂ featuring only O_d sites. Similarly, H₂O exhibits a preference for adsorption on the Mn_d species rather than O_d sites, as depicted in Fig. 6b. Furthermore, oxygen molecules from the air can also be absorbed by the Mn_d. Previous studies have reported the adsorption of oxygen molecules on Mn_d in MnO₂ catalysts.⁴⁵

Based on the analysis and insights gleaned from previous studies,^{10,46,47} we propose a plausible mechanism for the oxidation of vanillyl alcohol to vanillin using the γ -MnO₂ catalyst in air (Fig. 6c). In this mechanism, O₂, H₂O, and vanillyl alcohol are simultaneously adsorbed onto the catalyst. Under sunlight illumination, electrons (e⁻) and holes (h⁺) are separated from the surface of the γ -MnO₂ catalyst. During this step, adsorbed H₂O accepts holes (h⁺) to form \cdot OH species, releasing H⁺ species (P11, Fig. 6c). Simultaneously, vanillyl alcohol accepts holes (h⁺) to generate alcohol radical species (2A) (P21, Fig. 6c). Adsorbed oxygen can accept e⁻ from the γ -MnO₂ catalyst surface to form O₂^{-•} species (P22, Fig. 6c), or it can combine with protons generated from P11 to form \cdot OH species (P12, Fig. 6c). The formation of \cdot OH species from O₂ and H₂O in oxide-based catalysts, including MnO₂, has also been proposed^{44,48} Vanillyl alcohol radical (1A, Fig. 6c) is selectively obtained by combining the adsorbed vanillyl alcohol with \cdot OH species (P13, Fig. 6c), which further converts to vanillin through a subsequent reaction with \cdot OH species (P14, Fig. 6c). The positive radical of vanillyl alcohol (2A, Fig. 6c) reacts with O₂^{-•} species to produce the alcohol peroxo species (2B) (P23, Fig. 6c), eventually converting to vanillin and releasing H₂O₂ (P24, Fig. 6c). Under these conditions, the catalytic cycle is completed, and the γ -MnO₂ catalyst is ready for the next catalytic process.

Conclusions

In summary, we have successfully fabricated manganese oxide-based catalysts with different Mn defects on MnO₂ with various



crystal structures and on γ -MnO₂ with different amounts of urea. Comprehensive structural characterization highlights the significance of urea in tuning the coordination environment of Mn species in γ -MnO₂ and the O species in α -MnO₂. In the gram-scale oxidation of vanillyl alcohol to vanillin, the Mn-defected γ -MnO₂ catalyst demonstrates excellent photocatalytic performance compared to the O-defected α -MnO₂ catalyst and other type (β , ϵ)-MnO₂ catalysts. DFT calculations and control experiments demonstrate that the defected-Mn species in the γ -MnO₂ catalyst facilitate the adsorption of vanillyl alcohol and H₂O, which converts to the corresponding 'OH species under natural light illumination. The synergistic effect of the Mn-defected species and 'OH species plays a crucial role in enhancing the photocatalytic performance in the aerobic oxidation of vanillyl alcohol to vanillin over the γ -MnO₂ catalyst. This study not only presents effective methods for tuning the coordination environments of Mn atoms in MnO₂ for the selective oxidation of vanillyl alcohol to vanillin but also provides valuable insights for the development of advanced transition metal oxide photocatalysts.

Author contributions

Q. Ke, Y. Zhang and C. Wan: conceptualization, methodology, and writing – original draft. Y. Zhang, J. Tang, S. Li, X. Guo, T. Hamada, and S. M. Osman: data curation, chemical experiments, and formal analysis. Q. Ke, and C. Wan: funding acquisition and investigation. C. Wan, M. Han, Y. Kang, and Y. Yamauchi: supervision and writing – review & editing.

Conflicts of interest

There are no conflicts to declare.

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References

- 1 R. Singathi, R. Raghunathan, R. Krishnan, S. K. Rajendran, S. Baburaj, M. P. Sibi, D. C. Webster and J. Sivaguru, *Angew. Chem., Int. Ed.*, 2022, **61**, e202203353.
- 2 B. Schaefer, *Natural Products in the Chemical Industry*, Springer, Berlin, 2014.
- 3 X. Shen, Q. Meng, Q. Mei, H. Liu, J. Yan, J. Song, D. Tan, B. Chen, Z. Zhang, G. Yang and B. Han, *Chem. Sci.*, 2020, **11**, 1347–1352.
- 4 Z. Xiang, W. Han, J. Deng, W. Zhu, Y. Zhang and H. Wang, *ChemSusChem*, 2020, **13**, 4199–4213.
- 5 D. Zhu, L. Xu, S. Sethupathy, H. Si, F. Ahmad, R. Zhang, W. Zhang, B. Yang and J. Sun, *Green Chem.*, 2021, **23**, 9554–9570.
- 6 W. Sun, S. Wu, Y. Lu, Y. Wang, Q. Cao and W. Fang, *ACS Catal.*, 2020, **10**, 7699–7709.
- 7 Z. Pan, A. Puente-Urbina, A. Bodi, J. A. van Bokhoven and P. Hemberger, *Chem. Sci.*, 2021, **12**, 3161–3169.
- 8 M. Fache, B. Boutevin and S. Caillol, *ACS Sustainable Chem. Eng.*, 2016, **4**, 35–46.
- 9 M. B. Figueirêdo, I. Hita, P. J. Deuss, R. H. Venderbosch and H. J. Heeres, *Green Chem.*, 2022, **24**, 4680–4702.
- 10 B.-C. Li, N. N. Huy, J.-Y. Lin, S. Phattarapattamawong, G. Lisak, H. Wang and K.-Y. A. Lin, *J. Environ. Chem. Eng.*, 2021, **9**, 106092.
- 11 R. Zhang, R. Maltari, M. Guo, J. Kontro, A. Eronen and T. Repo, *Ind. Crops Prod.*, 2020, **145**, 112095.
- 12 J. Dai, A. F. Patti, G. N. Styles, S. Nanayakkara, L. Spiccia, F. Arena, C. Italiano and K. Saito, *Green Chem.*, 2019, **21**, 2005–2014.
- 13 B. N. Zope, D. D. Hibbitts, M. Neurock and R. J. Davis, *Science*, 2010, **330**, 74–78.
- 14 C.-R. Chang, X.-F. Yang, B. Long and J. Li, *ACS Catal.*, 2013, **3**, 1693–1699.
- 15 X. Cao, A. Huang, C. Liang, H.-C. Chen, T. Han, R. Lin, Q. Peng, Z. Zhuang, R. Shen, H. M. Chen, Y. Yu, C. Chen and Y. Li, *J. Am. Chem. Soc.*, 2022, **144**, 3386–3397.
- 16 J. Li, H. Yuan, Q. Zhang, K. Luo, Y. Liu, W. Hu, M. Xu and S. Xu, *Phys. Chem. Chem. Phys.*, 2020, **22**, 27272–27279.
- 17 D. A. Kitchaev, S. T. Dacek, W. Sun and G. Ceder, *J. Am. Chem. Soc.*, 2017, **139**, 2672–2681.
- 18 X. Zeng, G. Cheng, Q. Liu, W. Yu, R. Yang, H. Wu, Y. Li, M. Sun, C. Zhang and L. Yu, *Ind. Eng. Chem. Res.*, 2019, **58**, 13926–13934.
- 19 J. C. Hunter, *J. Solid State Chem.*, 1981, **39**, 142–147.
- 20 X. Luo, X. Tang, J. Ni, B. Wu, C. Li, M. Shao and Z. Wei, *Chem. Sci.*, 2023, **14**, 1679–1686.
- 21 X. Yan, T. Gan, S. Shi, J. Du, G. Xu, W. Zhang, W. Yan, Y. Zou and G. Liu, *Catal. Sci. Technol.*, 2021, **11**, 6369–6373.
- 22 K.-Y. A. Lin, W.-D. Oh, M.-W. Zheng, E. Kwon, J. Lee, J.-Y. Lin, X. Duan and F. Ghanbari, *J. Colloid Interface Sci.*, 2021, **592**, 416–429.
- 23 S. Ndayiragije, Y. Zhang, Y. Zhou, Z. Song, N. Wang, T. Majima and L. Zhu, *Appl. Catal., B*, 2022, **307**, 121168.



- 24 C. Wang, Y. Zeng, X. Xiao, S. Wu, G. Zhong, K. Xu, Z. Wei, W. Su and X. Lu, *J. Energy Chem.*, 2020, **43**, 182–187.
- 25 L. Ni, Z. Wu, G. Zhao, C. Sun, C. Zhou, X. Gong and G. Diao, *Small*, 2017, **13**, 1603466.
- 26 F. Lai, J. Feng, R. Yan, G. C. Wang, M. Antonietti and M. Oschatz, *Adv. Funct. Mater.*, 2018, **28**, 1801298.
- 27 Y. Li, X. Wei, S. Han, L. Chen and J. Shi, *Angew. Chem., Int. Ed.*, 2021, **60**, 21464–21472.
- 28 A. Singh, O. Sel, H. Perrot, V. Balland, B. Limoges and C. Laberty-Robert, *J. Mater. Chem. A*, 2021, **9**, 1500–1506.
- 29 Z. Zhou, X. Zheng, M. Liu, P. Liu, S. Han, Y. Chen, B. Lan, M. Sun and L. Yu, *ChemSusChem*, 2022, **15**, e202200612.
- 30 Q. Zhang, G. Xie, M. Duan, Y. Liu, Y. Cai, M. Xu, K. Zhao, H. Tai, Y. Jiang and Y. Su, *ACS Appl. Nano Mater.*, 2023, **6**, 17445–17456.
- 31 J. Tang, J. Chen, Z. Zhang, Q. Ma, X. Hu, P. Li, Z. Liu, P. Cui, C. Wan, Q. Ke, L. Fu, J. Kim, T. Hamada, Y. Kang and Y. Yamauchi, *Chem. Sci.*, 2023, **14**, 13402–13409.
- 32 H. Liu, W. Jia, X. Yu, X. Tang, X. Zeng, Y. Sun, T. Lei, H. Fang, T. Li and L. Lin, *ACS Catal.*, 2021, **11**, 7828–7844.
- 33 Q. Ke, Y. Jin, F. Ruan, M. N. Ha, D. Li, P. Cui, Y. Cao, H. Wang, T. Wang, V. N. Nguyen, X. Han, X. Wang and P. Cui, *Green Chem.*, 2019, **21**, 4313–4318.
- 34 D. Sun, L. Peng, Y. Yang, Y. Fang, S. P. Jiang and Z. Shao, *J. Catal.*, 2022, **409**, 48–58.
- 35 C. Chen, G. Xie, J. Dai, W. Li, Y. Cai, J. Li, Q. Zhang, H. Tai, Y. Jiang and Y. Su, *Nano Energy*, 2023, **116**, 108788.
- 36 A. V. Emeline, N. V. Sheremetyeva, N. V. Khomchenko, V. K. Ryabchuk and N. Serpone, *J. Phys. Chem. C*, 2007, **111**, 11456–11462.
- 37 Y. Liu, M.-S. Niu, X. Yi, G. Li, H. Zhou and W. Gao, *Appl. Surf. Sci.*, 2021, **561**, 150081.
- 38 J. Estrada-Pomares, S. Ramos-Terrón, G. Lasarte-Aragonés, R. Lucena, S. Cárdenas, D. Rodríguez-Padrón, R. Luque and G. de Miguel, *J. Mater. Chem. A*, 2022, **10**, 11298–11305.
- 39 F. Li, J. Tang, Q. Ke, Y. Guo, M. N. Ha, C. Wan, Z. Lei, J. Gu, Q. Ling, V. N. Nguyen and W. Zhan, *ACS Catal.*, 2021, **11**, 11855–11866.
- 40 J. Li, G. Xie, J. Jiang, Y. Liu, C. Chen, W. Li, J. Huang, X. Luo, M. Xu, Q. Zhang, M. Yang and Y. Su, *Nano Energy*, 2023, **108**, 108234.
- 41 S. Mu, H. Lu, Q. Wu, L. Li, R. Zhao, C. Long and C. Cui, *Nat. Commun.*, 2022, **13**, 3694.
- 42 Y. Yang, B. Cheng, J. Yu, L. Wang and W. Ho, *Nano Res.*, 2023, **16**, 4506–4514.
- 43 S. Das, A. Samanta and S. Jana, *ACS Sustainable Chem. Eng.*, 2017, **5**, 9086–9094.
- 44 K. Takanahe and E. Iglesia, *Angew. Chem., Int. Ed.*, 2008, **47**, 7689–7693.
- 45 J. Shi, T. Qi, B.-C. Sun, G.-W. Chu and J.-F. Chen, *Chem. Eng. J.*, 2022, **440**, 135802.
- 46 Q. Zhu, P. Zhan, C. Zhang, R. Chen, C. Ren, H. Zhao, W. Ren, J. Zhang, P. Qin and D. Cai, *ChemPhotoChem*, 2023, **7**, e202200337.
- 47 M. Bellardita, S. Yurdakal, B. S. Tek, Ç. Değirmenci, G. Palmisano, V. Loddo, L. Palmisano, J. Soria, J. Sanz and V. Augugliaro, *J. Environ. Chem. Eng.*, 2021, **9**, 105308.
- 48 S. Zhao, Y. Wen, X. Liu, X. Pen, F. Lü, F. Gao, X. Xie, C. Du, H. Yi D. Kang and X. Tang, *Nano Res.*, 2020, **13**, 1544–1551.

