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# Reversible and irreversible reaction mechanisms of Li–CO<sub>2</sub> batteries†

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Li–CO<sub>2</sub> batteries are considered a versatile solution for CO<sub>2</sub> utilization. However, their development, including reversibility and efficiency, is impeded by an inadequate understanding of Li–CO<sub>2</sub> electrochemistry, particularly the decomposition of carbon and the generation of by-product O<sub>2</sub>. Here, using typical Ru(0001) (reversible) and Ir(111) (irreversible) as model catalysts and employing state-of-the-art first-principles calculations, the rechargeable/reversible reaction mechanisms of Li–CO<sub>2</sub> batteries are disclosed. We find that electrolyte, often neglected or oversimplified in Li–CO<sub>2</sub> modelling, plays an essential role in CO<sub>2</sub> activation and C–C coupling affects the generation pathways of discharge intermediates due to the sluggish kinetics. The results rationalize experimental observations, which are also examined by constant-potential modelling. Specifically, by exploring the kinetics of the charging process, we discover that the reversibility of Ru(0001) is attributed to its ability to suppress O–O coupling while co-oxidizing Li<sub>2</sub>CO<sub>3</sub> and carbon. In contrast, Li<sub>2</sub>CO<sub>3</sub> decomposition on Ir(111) preferentially produces O<sub>2</sub>, during which carbon can only be partially decomposed. These findings solve long-standing questions and highlight the necessity of describing the explicit solvent effect in modelling, which can promote further studies on Li–CO<sub>2</sub> batteries.

## Introduction

Li–CO<sub>2</sub> batteries have garnered extensive attention from the scientific community owing to their high potential for CO<sub>2</sub> fixation while simultaneously enabling energy storage with a theoretical energy density of 1876 W h kg<sup>−1</sup>.<sup>1–3</sup> In contrast to Li-ion batteries, their performance is governed by Li–CO<sub>2</sub> electrochemistry, which operates according to the following reaction: 4Li + 3CO<sub>2</sub> ↔ 2Li<sub>2</sub>CO<sub>3</sub> + C (*E*<sub>0</sub> = 2.8 V vs. Li/Li<sup>+</sup>).<sup>4–7</sup> However, CO<sub>2</sub> reduction during the discharging process is kinetically sluggish, which results in large discharging overpotentials, and a high charge voltage is also required to decompose the discharge product, Li<sub>2</sub>CO<sub>3</sub>, due to its wide bandgap of 5.03 eV and high thermodynamic stability ( $\Delta G_f = -1132.1$  kJ mol<sup>−1</sup>).<sup>8,9</sup> The inadequate decomposition of the discharge product carbon limits energy efficiency and leads to an irreversible reaction (e.g., 2Li<sub>2</sub>CO<sub>3</sub> → 4Li<sup>+</sup> + 4e<sup>−</sup> + 2CO<sub>2</sub> + O<sub>2</sub>).<sup>10–12</sup> Moreover, the passivation of catalyst surfaces and instability of electrolytes affect the cycle performance of Li–CO<sub>2</sub> batteries. Such issues pose massive challenges to the practical applications of Li–CO<sub>2</sub> batteries, thereby inspiring the rational design of catalysts that demonstrate high reversibility and low overpotentials.<sup>13–15</sup>

Uncovering the underlying mechanisms can facilitate the design of efficient catalysts.<sup>16–21</sup> Based on experimental characterization and theoretical calculations, much effort has been expended to reveal the reaction pathway on the catalysts, which directly determines the reversibility of Li–CO<sub>2</sub> electrochemistry.<sup>22–25</sup> For the discharging process, C–C coupling, such as the dimerization of \*CO<sub>2</sub> (\* indicates an adsorption site) and the reaction of \*Li<sub>2</sub>CO<sub>2</sub> and \*CO<sub>2</sub>, was regarded as the essential steps for Li<sub>2</sub>CO<sub>3</sub> formation.<sup>12,18,26</sup> However, the dominant coupling step and reaction pathway are still controversial. Another important issue is that the oxidative decomposition mechanism of Li<sub>2</sub>CO<sub>3</sub> and carbon remains quite ambiguous. For example, in principle, the as-formed O species can react with carbon, but in the case of most catalysts, such as Au(111) and Ir(111), only the decomposition of Li<sub>2</sub>CO<sub>3</sub> has been observed; both O<sub>2</sub> and CO<sub>2</sub> were found to evolve concomitantly during the charging process.<sup>3,26–30</sup> Note that the generated O<sub>2</sub> may contain aggressive singlet oxygen (<sup>1</sup>O<sub>2</sub>), which can attack battery components and cause severe parasitic reactions.<sup>13,31</sup> In the cases of Ru-based metal catalysts, Li<sub>2</sub>CO<sub>3</sub> and carbon disappear together and only CO<sub>2</sub> is released, corresponding to a reversible process.<sup>3</sup> However, to date, no satisfactory explanation for such phenomena exists. It is of great significance to gain a mechanistic understanding of Li–CO<sub>2</sub> electrochemistry.

Herein, we investigate the underlying mechanisms of Li–CO<sub>2</sub> electrochemistry by conducting comprehensive first-principles calculations to provide fundamental insights into the reversibility with a focus on the initial charge and discharge

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processes. Ru(0001) and Ir(111) are selected as model catalysts because the former has been extensively reported to achieve good reversibility in Li-CO<sub>2</sub> electrochemistry, while the latter suffers from irreversibility issues. The modelling results show that the electrolyte can facilitate the activation of CO<sub>2</sub>, and the disproportionation of \*CO<sub>2</sub> corresponds to the predominant kinetic barrier for the discharging process. The two catalysts exhibit different CO<sub>2</sub> charging processes. Ru(0001) can suppress O-O coupling to form O<sub>2</sub> while co-oxidizing carbon and Li<sub>2</sub>CO<sub>3</sub> to generate CO<sub>2</sub>, thereby ending a complete battery cycle. By contrast, in the case of Ir(111), Li<sub>2</sub>CO<sub>3</sub> decomposes and releases both CO<sub>2</sub> and O<sub>2</sub>, and carbon can only be partially decomposed into small fragments.

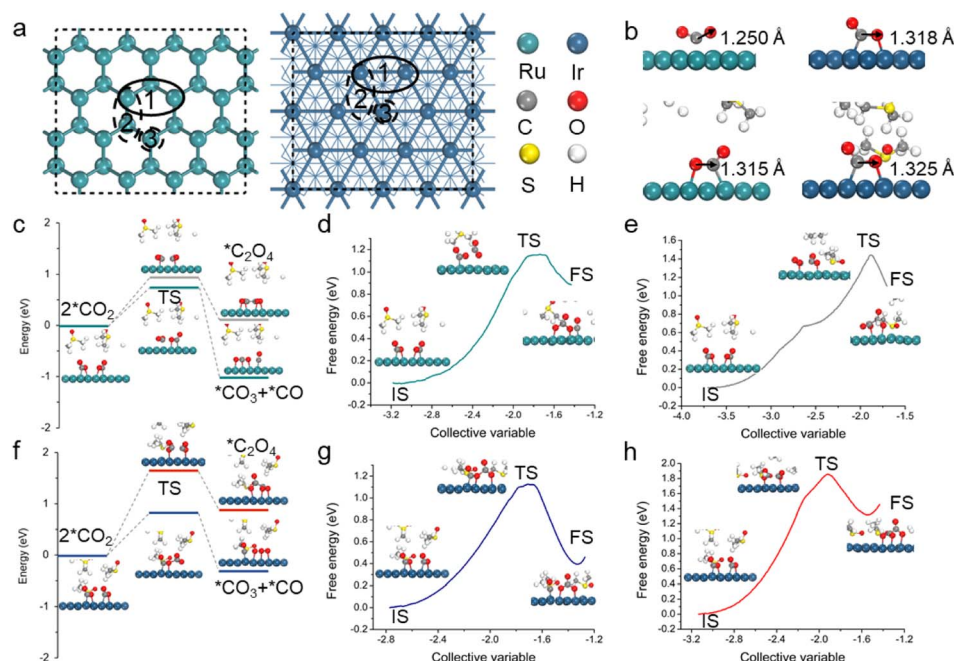
## Results and discussion

To explore rechargeable/reversible mechanisms of Li-CO<sub>2</sub> batteries, the Ru(0001) and Ir(111) surfaces were constructed (Fig. 1a). We first investigated the discharge process with a focus on the CO<sub>2</sub> activation (forming \*CO<sub>2</sub>) and subsequent C-C coupling that are crucial steps in the Li-CO<sub>2</sub> electrochemistry. Note that the interactions between reaction intermediates and solvent molecules can be strong, thereby affecting the discharge pathways; for example, prior experiments have indicated that the addition of DMSO can induce the generation of oxalate intermediates.<sup>32,33</sup> However, the solvent effect is often neglected or oversimplified in Li-CO<sub>2</sub> electrochemistry modelling. Hence, an explicit description of

the solvent effect was conducted, where DMSO was chosen as a demonstration.

Different CO<sub>2</sub> adsorption sites on the two surfaces were investigated. Fig. 1b shows the lowest-energy structure of \*CO<sub>2</sub> in which the CO<sub>2</sub> molecule is chemically adsorbed onto Ru(0001) and Ir(111) with a dual-site adsorption configuration. The adsorption free energies are −0.35 eV for Ru(0001) and −0.30 eV for Ir(111). It is worth mentioning that the solvent effect has resulted in an extension of the C-O bond length with respect to both the Ru(0001) and Ir(111) surfaces, with an increase from 1.250 Å to 1.315 Å for the former and 1.318 Å to 1.325 Å for the latter, indicating an overall stronger CO<sub>2</sub> adsorption in both cases (Fig. 1b). The dual-site adsorption presents a longer C-O bond length, which may facilitate bond breaking in the subsequent disproportionation reaction. Please also note that in the case of Ru, the configuration of \*CO<sub>2</sub> changes from single-site adsorption (forming a Ru-C bond) to dual-site adsorption (forming Ru-O and Ru-C bonds) after considering the solvent effect. These results highlight the essential role of electrolytes in the activation of CO<sub>2</sub> and demonstrate the necessity of describing the explicit solvent effect in Li-CO<sub>2</sub> electrochemistry modelling.

The activated \*CO<sub>2</sub> species can undergo direct dimerization to form oxalate or carbonate intermediates, and they are also available to be coupled with the lithiated intermediates, including \*LiCO<sub>2</sub> and \*Li<sub>2</sub>CO<sub>2</sub>. After adsorbing the first CO<sub>2</sub> molecule, the second CO<sub>2</sub> molecule is also activated; the adsorption energies are −0.31 and −0.20 eV for Ru(0001) and



**Fig. 1** (a) Structures and possible adsorption sites of the Ru(0001) (left) and Ir(111) (right) surfaces. (b) The most stable CO<sub>2</sub> adsorption configurations of Ru(0001) and Ir(111) in a vacuum (upper) and DMSO solvent (bottom). C, O, S, H, Ru, and Ir are represented by gray, red, yellow, white, green, and dark cyan spheres, respectively. (c and f) Energy barriers of C-C coupling on (c) Ru(0001) and (f) Ir(111), in which the DESW and CBD methods are employed. The insets show geometric structures of the initial state (IS), transition state (TS), and final state (FS). (d and e) Free energy profiles of the (d) CO<sub>2</sub> disproportionation and (e) dimerization pathways on Ru(0001). (g and h) Free energy profiles of the (g) CO<sub>2</sub> disproportionation and (h) dimerization pathways on Ir(111).



Ir(111), respectively. To find the most likely reaction path, we performed a kinetic analysis using the double-ended surface walking (DESW) and constrained Broyden dimer (CBD) approaches.<sup>34,35</sup> Note that the methods can determine a low-energy pathway linking two minima even without iterative optimization of the path, from which the transition state (TS) can be located readily. As shown in Fig. S1 and S2,<sup>†</sup>  $^*\text{CO}_2$  is more favourable to disproportionate into  $^*\text{CO}_3$  and  $^*\text{CO}$  for both Ru(0001) and Ir(111). However, the coupling of  $^*\text{Li}_2\text{CO}_2$  and  $^*\text{CO}_2$  on Ru(0001) tends to generate oxalates, while in the case of Ir(111), the formation of carbonates is still predominant. As mentioned above, polar electrolytes have a significant impact on the formation of discharge intermediates. Therefore, *ab initio* molecular dynamics (AIMD) simulations were performed to obtain explicit DMSO structures for the Ru(0001) and Ir(111) surfaces (Fig. S3<sup>†</sup>),<sup>36</sup> and both reaction pathways under solvent conditions were further analysed.

The kinetic results involving the solvation effect shown in Fig. 1c and f indicate that the disproportionation pathway ( $2^*\text{CO}_2 \rightarrow ^*\text{CO}_3 + ^*\text{CO}$ ) is more energetically favourable than the dimerization pathway ( $2^*\text{CO}_2 \rightarrow ^*\text{C}_2\text{O}_4$ ). For the disproportionation pathway, the energy barriers of Ru(0001) and Ir(111) are 0.76 and 0.83 eV, respectively, which are lower than those of the dimerization pathway (0.96 and 1.65 eV). In addition, to further catch the solvent network, the slow-growth method was also employed to sample the energy change of the aforementioned optimal reaction pathway; multiple independent slow-growth samplings for each step were conducted (Fig. 1d, e, g, h and S4<sup>†</sup>). The results prove that  $^*\text{CO}_2$  on the catalysts has a higher propensity towards undergoing disproportionation to form  $^*\text{CO}_3$  and  $^*\text{CO}$ , which is consistent with the above kinetic results (Fig. 1c and f). Note that we also conducted slow-growth simulations up to 50 ps and found similar results. This is not surprising as highly polar electrolytes do not directly participate in the Li- $\text{CO}_2$  reactions, which is different from typical aqueous electrochemical reactions (e.g., the hydrogen evolution reaction and the reduction of  $\text{CO}_2$  and  $\text{H}_2\text{O}$  to  $\text{CH}_3\text{OH}$ ). On a different note, the competing coupling of  $^*\text{Li}_2\text{CO}_2$  and  $^*\text{CO}_2$  to form  $^*\text{Li}_2\text{C}_2\text{O}_4$  in DMSO also exhibits a high energy barrier on the Ru(0001) surface (Fig. S5<sup>†</sup>). Therefore, the disproportionation of  $^*\text{CO}_2$  to form  $^*\text{CO}_3$  and  $^*\text{CO}$  is the dominant pathway for Ru(0001) and Ir(111).

The  $\text{Li}_2\text{CO}_3$  and carbon formation processes were subsequently investigated using the constant charge method (Fig. 2).<sup>2,12,24</sup> The relative free energy changes ( $\Delta G$ ) are summarized in Table S1.<sup>†</sup> Please also note that the modelling of the Li- $\text{CO}_2$  reaction still faces many challenges, such as accurately describing the formation process of  $\text{Li}_2\text{CO}_3$ ; currently, one common strategy is to simplify it to a  $\text{Li}_2\text{CO}_3$  moiety, which successfully explains the reaction processes and operation potentials.<sup>2,11,12,22,24,25</sup> This strategy was adopted in this work. It was found that after the disproportionation of  $^*\text{CO}_2$ ,  $^*\text{CO}_3$  can convert to  $^*\text{Li}_2\text{CO}_3$  via two-step lithiation reactions, which are both thermodynamically spontaneous for the Ru(0001) and Ir(111) surfaces (Fig. 2). Subsequently,  $^*\text{Li}_2\text{CO}_3$  desorbs to produce the first  $\text{Li}_2\text{CO}_3$  species, whereas the previously generated  $^*\text{CO}$  remains on the catalyst surface.

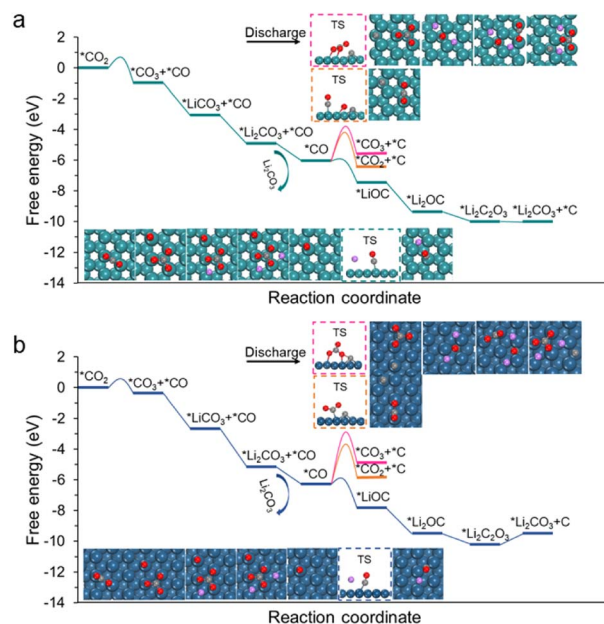


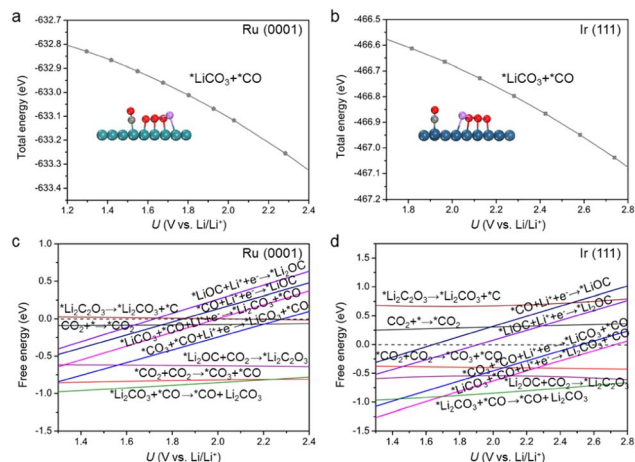
Fig. 2 Free energy diagrams of  $\text{CO}_2$  reduction (discharging process) on the (a) Ru(0001) and (b) Ir(111) surfaces. Insets display geometric structures of free slabs, adsorbates, and key transition states that are highlighted by dashed boxes. The structures of transition states are shown in Fig. S6 and S7.<sup>†</sup>

The remaining question is whether CO undergoes disproportionation or participates in subsequent lithiation reactions. According to our calculations,  $^*\text{CO}$  lithiation to form  $^*\text{LiOC}$  is an exothermic reaction, with respective  $\Delta G$  values of  $-1.43$  eV for Ru(0001) and  $-1.54$  eV for Ir(111); in accordance with our expectations, the kinetic barriers of such a lithiation step are small (less than 0.3 eV). By contrast, the disproportionation of  $^*\text{CO}$  to form  $^*\text{C}$  and  $^*\text{CO}_2$  is considerably endothermic, and the kinetic barriers are as high as 1.92 and 2.98 eV for Ru(0001) and Ir(111), respectively. We also calculated the coupling of  $^*\text{CO}$  and  $^*\text{CO}_2$  to form  $^*\text{CO}_3$  and  $^*\text{C}$  but found that the relative kinetic barriers are very high (2.31 and 3.28 eV). These results suggest that the two reactions are difficult to occur. Moreover, the lithiation of  $^*\text{LiOC}$  to  $^*\text{Li}_2\text{OC}$  is exothermic, and the as-formed  $^*\text{Li}_2\text{OC}$  can react with  $\text{CO}_2$  to form  $^*\text{Li}_2\text{C}_2\text{O}_3$  and then decompose into  $^*\text{Li}_2\text{CO}_3$  and  $^*\text{C}$  species. Such a decomposition step is slightly endothermic by 0.07 eV for Ru(0001) and 0.66 eV for Ir(111).

The theoretical limiting potential ( $U_L$ ) is an important indicator to bridge the experimental activity, such as discharge potential. Based on the free-energy diagrams in Fig. 2,  $U_L$  was identified to be 1.43 V for Ru(0001) and 1.54 V for Ir(111). To better simulate electrochemical environments, we performed constant potential modelling, which can describe the effects of the surface charge of catalysts on electrochemical reactions.<sup>37–40</sup> The total energy of each reaction intermediate as a function of potential is fitted (Figs. S8 and S9<sup>†</sup>), and Fig. 3a and b show the fitting results for  $^*\text{LiCO}_3$  and  $^*\text{CO}$  intermediates on Ru(0001) and Ir(111), respectively. We found that the  $U_L$  values of Ru(0001) and Ir(111) obtained based on the constant potential







**Fig. 3** (a and b) Total energy of the absorbed  $\text{Li}_2\text{CO}_3$  and  $\text{CO}$  species of (a) Ru(0001) and (b) Ir(111) as a function of potential. (c and d) Free energy changes of discharge elementary reactions of (c) Ru(0001) and (d) Ir(111) based on the constant potential method.

method are close to the above constant charge results (Fig. 3c and d), and these values are in agreement with experimental observations.<sup>41</sup> These results demonstrate the rationality of our proposed discharge mechanism. Considering the computational cost, the constant charge method was used in subsequent calculations.

Compared with the discharge reaction, the charging mechanism is relatively complex and ambiguous. According to whether the discharge products  $\text{Li}_2\text{CO}_3$  and carbon can be completely decomposed, the charging process can be divided into reversible and irreversible reactions.<sup>3,25,27–29</sup> Please note that the reversibility can be influenced by many aspects, such as discharge product-caused passivation of catalyst surfaces, instability of electrolytes, and the incomplete decomposition of discharge products that directly determines the reversibility of  $\text{Li}-\text{CO}_2$  reactions. In this modelling work, we focused on the decomposition of discharge products during the charging process.

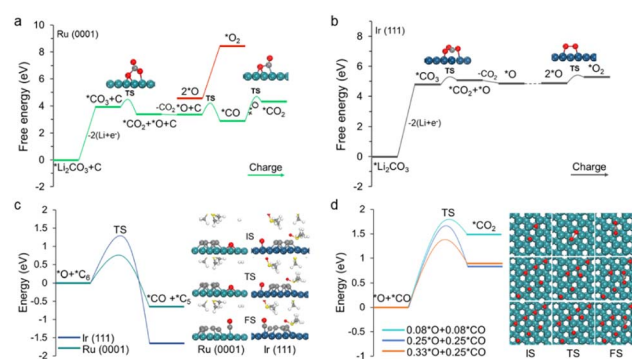
It was previously reported that both chemical and electrochemical pathways may exist for the decomposition of  $\text{Li}_2\text{CO}_3$ .<sup>42,43</sup> For most reported catalysts, only the decomposition of  $\text{Li}_2\text{CO}_3$  was observed during the charging process while carbon was partially decomposed.<sup>3,12–15</sup> Meanwhile, for exceptional catalysts such as Ru, no satisfactory explanation of the underlying mechanism of the oxidation of  $\text{Li}_2\text{CO}_3$  and carbon has been provided. In this regard, we proposed two possible mechanisms and performed corresponding calculations, as discussed later.

The discharge product carbon is a complex system; in principle, its decomposition is the gradual transformation of large fragments into small fragments. According to our calculations, the decomposition of carbon on Ru(0001) is much more energetically favourable than that on Ir(111), and as the number of C atoms in the carbon fragments decreases, the energy barrier for removing C atoms typically increases. For example, we investigated the kinetics of removing a C atom from  $\text{C}_{13}$  and  $\text{C}_6$  clusters (Fig. S10†). The results show that the decomposition barrier

of the  $\text{C}_{13}$  cluster is 0.38 and 0.94 eV for Ru(0001) and Ir(111), respectively. In the case of the  $\text{C}_6$  cluster, the barriers are significantly higher, being 1.45 eV for Ru(0001) and 1.98 eV for Ir(111). Note that after the carbon six-membered ring is broken, the subsequent barrier is moderate; for instance, the barrier of removing a C atom from a  $\text{C}_5$  cluster is 1.05 eV for Ru(0001) and 1.21 eV for Ir(111).

However, the decomposition of carbon and  $\text{Li}_2\text{CO}_3$  might not be simply oxidized separately but is a co-oxidation process.<sup>27</sup> Thus, we further include the contributions from  $\text{Li}_2\text{CO}_3$  in carbon decomposition. Herein, the  $\text{C}_6$  cluster is adopted as the representative model because its decomposition exhibits the largest energy barrier compared with other carbon fragments (Fig. S10†). For the charging process,  $\text{Li}_2\text{CO}_3$  first loses two Li and then generates  $\text{CO}_3$  via two delithiation steps (Fig. 4a and b), and the kinetic barriers are 0.67 and 0.83 eV for Ru(0001) and Ir(111), respectively (Fig. S11†). The relative free energy changes are summarized in Tables S2 and S3.† These steps are relatively easy to occur on both Ru(0001) and Ir(111) by applying moderate charging voltage. The further decomposition of  $\text{CO}_3$  to  $\text{CO}_2$  and  $\text{O}$  is also energetically favourable, displaying a moderate barrier of 0.51 eV and 0.50 eV on Ru(0001) and Ir(111), respectively.

The remaining question is how  $\text{O}$  is oxidized. Two possible reaction pathways for  $\text{O}$  oxidation were studied. In the first pathway,  $\text{O}$  species couple with one another to generate  $\text{O}_2$ , corresponding to the irreversible charge; in the second pathway,  $\text{O}$  attacks carbon to form carbon oxides, which enables a complete battery cycle. It was found that the as-formed  $\text{O}$  species can facilitate the carbon decomposition on both the Ru(0001) and Ir(111) surfaces (Fig. S12†). Meanwhile, in accordance with our expectations, the reaction of  $\text{O}$  with the  $\text{C}_6$  cluster to form  $\text{CO}$  and  $\text{C}_5$  on Ru(0001) exhibits a moderate energy barrier (0.86 eV), whereas in the case of Ir(111), the value is as high as 1.60 eV (Fig. S12†). To further investigate the oxidative decomposition of carbon, the reaction energy barriers with respect to the DMSO solvent were also computed (Fig. 4c). A slight decline in the respective energy barriers was observed,



**Fig. 4** (a and b) Calculated energetic profiles of the charging process of (a) Ru(0001) and (b) Ir(111). (c) Energy barriers for the oxidative decomposition of a  $\text{C}_6$  cluster to form  $\text{C}_5$  and  $\text{CO}$  on Ru(0001) and Ir(111). (d) Energy barriers for  $\text{CO}$  oxidation under different  $\text{CO}$  and  $\text{O}$  coverages.



validating the feasibility (infeasibility) of oxidative decomposition of carbon on Ru (Ir).

Finally, the adsorbed CO species over Ru(0001) can react with another \*O to form \*CO<sub>2</sub>. Although the energy barrier of the \*CO oxidation reaction is slightly high, it becomes more favourable as the coverage of \*O and \*CO increases (Fig. 4d). This is also consistent with previous reports that CO oxidation on Ru will be more active under high gas pressure.<sup>44,45</sup> On a different note, the dimerization of \*O to form O<sub>2</sub> on Ru(0001) is virtually impossible on account of the massive changes in a free energy of 3.90 eV (Fig. 4a). In the case of Ir(111), the \*O intermediate preferentially couples with another \*O species to generate O<sub>2</sub>, which is attributed to a moderate kinetic barrier (0.53 eV). Note that high O coverage reduces the energy barrier of O–O coupling on Ir(111), and while a similar situation occurs in Ru(0001), the energy barrier is still very high (Fig. S13†). Overall, the above modelling results demonstrate that Li<sub>2</sub>CO<sub>3</sub> and carbon can be co-oxidized on Ru to conclude a complete battery cycle, while Ir(111) can only partially decompose carbon into small fragments together with oxidizing Li<sub>2</sub>CO<sub>3</sub> into CO<sub>2</sub> and O<sub>2</sub>. Therefore, our observations are in good agreement with the aforementioned experimental phenomena.<sup>3,28</sup>

To gain a fundamental understanding of the difference in the oxidation of carbon on Ru(0001) and Ir(111), the surface charge distributions of \*C adsorbed on the two metal surfaces were assessed through a Bader charge analysis. As shown in Fig. S14,† a considerable amount of electronic charge is transferred from both metal surfaces to the \*C species. The electron transfer value of the Ru(0001) surface (1.39e) significantly exceeds that of the Ir(111) surface (1.02e), corresponding to a substantially stronger Coulomb interaction between C and Ru(0001). In addition, the continuous formation of the \*O intermediate on the Ru(0001) surface results in the former being widely distributed on the latter, which also facilitates reactions between \*O and \*C to generate CO<sub>2</sub>.

## Conclusions

In conclusion, using comprehensive first-principles calculations, the complete reversible and irreversible mechanism pathways of Li–CO<sub>2</sub> batteries were disclosed for the first time. The modelling results highlighted that the electrolyte may play an essential role in the activation of CO<sub>2</sub>; both Ru(0001) and Ir(111) prefer to undergo the direct disproportionation of \*CO<sub>2</sub> to \*CO<sub>3</sub> and \*CO during the discharge process. The constant-potential calculations verified the rationality of our reaction mechanism. Moreover, we elucidated the reversible co-oxidation process of the discharge products carbon and Li<sub>2</sub>CO<sub>3</sub> on Ru(0001) as well as the rationale for the partial decomposition of carbon and the generation of O<sub>2</sub> on Ir(111). Our findings provide a solution to long-standing questions and impart ample guidance in the development of reversible Li–CO<sub>2</sub> batteries.

## Methods

### First-principles calculations

All first-principles calculations were performed using the Vienna *ab initio* simulation package (VASP) with the projector augmented wave method and Perdew–Burke–Ernzerhof (PBE) generalized gradient approximation exchange–correlation functional.<sup>46–48</sup> The cutoff energy was set to 400 eV after a series of tests, and the criteria were set as 10<sup>−5</sup> eV for energy and 0.05 eV Å<sup>−1</sup> for force. The Brillouin zone was sampled using a Monkhorst–Pack 3 × 3 × 1 *k*-point grid, and the Grimme-D3 approach was applied to describe the dispersion interactions.<sup>49</sup> The reaction pathways and transition states were located using the double-ended surface walking (DESW) and constrained Broyden dimer (CBD) methods, as implemented in the LASP software.<sup>34,35</sup> All transition states have been verified by using vibrational frequency calculations (only one imaginary frequency). Note that these methods can determine a low-energy pathway linking two minima even without iterative optimization of the path, from which the transition state (TS) can be located readily.

### Structure models

The lattice parameters of bulk Ru and Ir are optimized to be  $a = b = 2.719$  Å,  $c = 4.297$  Å, and  $a = b = c = 3.872$  Å, respectively, which are consistent with experimental values. Two typical metal surfaces, *i.e.*, Ru(0001) and Ir(111), were constructed using 2 × 4 × 1 supercells. A vacuum region of 15 Å thickness along the *z* direction was chosen to eliminate the interactions between neighbouring surfaces. Specifically, to better describe the reactions in the electrode interface, we considered the solvent effect and potential effect, which are often neglected or oversimplified in the Li–CO<sub>2</sub> electrochemistry modelling. A typical electrolyte, DMSO, was adopted to describe the solvent effect on reaction pathways as a demonstration; five explicit DMSO molecules fill the vacuum gap to provide an experimental density of  $\rho = 1.1$  g cm<sup>−3</sup>.<sup>36</sup> Note here that other electrolytes (*e.g.*, TEGDME) were not considered because they have negligible influence on reversibility. The top layer, the adsorbates, and all DMSO molecules are allowed to relax while the remaining atoms are fixed during the calculations. For the Ru(0001) and Ir(111) surfaces, we first performed 10 ps AIMD simulations to obtain explicit DMSO structures. Then, adsorbates were placed on the metal surfaces for further study of the CO<sub>2</sub> electrochemical processes.

### Slow-growth simulations

The slow-growth method was used to sample the free-energy change during the disproportionation reaction.<sup>50,51</sup> Nose–Hoover thermostat was adopted to keep temperature at 300 K.<sup>52</sup> The corresponding increment speed of the CV was within the range between 0.0003 and 0.0004 CV per step, and the simulation time ranged from 5 to 10 ps depending on the length of the reaction pathways. We performed multiple independent slow-growth simulations for each step, and all results revealed that the



disproportionation pathway ( $2^*\text{CO}_2 \rightarrow ^*\text{CO}_3 + ^*\text{CO}$ ) is more energetically favourable than the dimerization pathway ( $2^*\text{CO}_2 \rightarrow ^*\text{C}_2\text{O}_4$ ). In addition, we also conducted slow-growth simulations up to 50 ps and found no impact on determining the dominant pathway.

### Free energy calculations

The free energy change ( $\Delta G$ ) for each elemental step was calculated using

$$\Delta G = \Delta E + \Delta E_{\text{ZPE}} - T\Delta S \quad (1)$$

where  $\Delta E$ ,  $\Delta E_{\text{ZPE}}$  and  $\Delta S$  are the total electronic energy difference, zero-point energy difference and entropy change ( $T = 298$  K), respectively. For adsorbates, all  $3N$  degrees of freedom were treated as harmonic vibrations, while the contributions from the catalyst surfaces were neglected. For  $\text{CO}_2$ , the adsorption energy can be calculated according to the following equation:

$$E_{\text{ads}} = E_{\text{total}} - E_{\text{slab}} - E_{\text{adsorbate}} \quad (2)$$

where  $E_{\text{total}}$  represents the electronic energy of the total system,  $E_{\text{slab}}$  is the energy of the adsorbate-free slab, and  $E_{\text{adsorbate}}$  represents the energy of the adsorbate moiety.

### Data availability

The computational data supporting the findings can be found in the article and ESI,<sup>†</sup> and are available from the authors upon reasonable request.

### Author contributions

Y. L. designed the research, X. Z. and Y. W. demonstrated the initial idea and collected all the data. X. Z., Y. W. and Y. L. wrote the paper and all authors commented on it.

### Conflicts of interest

The authors declare no competing financial interests.

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