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# Effects of chemical pretreatment on the enzymatic hydrolysis of post-consumer waste viscose†

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The pretreatment of post-consumer waste viscose before enzymatic hydrolysis was tested and evaluated to develop a tertiary recycling strategy for waste viscose, as no such strategy currently exists. There were differences between hydrolyzability of pre-consumer and post-consumer viscose, as we obtained 100% glucose yield from pre-consumer viscose while only 60–80% could be achieved from post-consumer, which we attributed to the inhibition – induced by contaminants that accumulated in the post-consumer viscose during its manufacture and use. Dilute alkali and acid pretreatment were applied to improve the hydrolysis of post-consumer viscose, although both of them proved unsuccessful strategies as alkali and acid pretreatment reduced glucose yield up to 28% and 44%, respectively. We concluded that avoiding pretreatment altogether was the most energy-efficient and resource-efficient alternative with regard to the saccharification of waste viscose. Thus, the economic viability of (enzymatically) saccharifying waste viscose depends entirely on the inherent hydrolyzability of the feedstock and its price.

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## Sustainability spotlight

The demand for viscose fibers continue to rise, but efficient recycling strategies are still lacking, which leads to vast amounts of textile waste accumulating in landfills worldwide. Due to the low degree of polymerization of viscose, alternatives to fiber-to-fiber recycling must be implemented. In this work, we identify challenges with recycling viscose post the use phase and evaluate different approaches to overcome these challenges. Ultimately, we identify avoiding pretreatment altogether as the most efficient strategy from an energy and resource perspective, for recycling post-consumer viscose *via* saccharification. This work aligns closely with the 12<sup>th</sup> Sustainable Development Goal identified by the UN in that it contributes to improving resource utilization, and fosters sustainable consumption, in viscose manufactory.

## 1 Introduction

Waste textiles are becoming an increasingly significant environmental problem. Approximately 113 million tons of fibers were produced globally in 2021, most of which was used for apparel.<sup>1</sup> Although much effort is being directed toward developing processes to recycle waste textiles, such a practice remains limited. In 2017, the Ellen MacArthur Foundation reported that less than 1% of textile fibers that were dedicated to the production of apparel were derived from recycled textiles. Further, only 12% of waste textiles were recycled into a lower-value application, whereas 73% were landfilled or incinerated.<sup>2</sup>

Viscose production suffers from having a high environmental impact due to its reliance on toxic processing chemicals and its intensive chemical, water, and energy use.<sup>2</sup> Nevertheless, the demand for MMCFs, such as viscose, is estimated to grow significantly.<sup>1</sup> Thus, the environmental incentives for developing efficient methods for recycling post-consumer waste viscose are substantial. Although fiber-to-fiber recycling is preferred, not every type of waste textile can be recycled in such a manner. For instance, viscose, the most ubiquitous manmade cellulosic fiber (MMCF) on the market,<sup>1</sup> has limited potential for fiber-to-fiber recycling due to its low degree of polymerization.<sup>3</sup>

The hydrolysis of waste viscose into glucose for the production of valuable chemicals is an attractive potential alternative pathway toward valorization.<sup>4</sup> Viscose can be hydrolyzed chemically and enzymatically.<sup>4,5</sup> Chemical hydrolysis methods, such as acid hydrolysis, are typically faster than enzymatic hydrolysis, which, conversely, can be performed at lower temperatures and generate a biocompatible broth.<sup>5–7</sup>

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Post-consumer textiles are more recalcitrant to hydrolysis and generally harder to recycle than pre-consumer textiles,<sup>4,8–12</sup> further complicating the saccharification of post-consumer textiles. This complexity arises from the incorporation of various additives into apparel during processing, the accumulation of contaminants throughout the lifecycle of the garment, and degradation due to wear and tear. For example, certain finishers effect significant resistance against the hydrolysis of textiles,<sup>13</sup> and reactive dyes impair the enzymatic depolymerization of cellulose.<sup>14</sup>

Various pretreatment methods are commonly applied to improve the sugar yields of hard-to-hydrolyze materials in biorefineries.<sup>15,16</sup> For example, alkaline treatment of cellulose-based textiles can be employed for many reasons, including improving enzymatic digestibility, targeting the removal of textile finishing agents, and separating fiber types in fiber blends.<sup>6,13,17–23</sup> Sodium hydroxide (NaOH) is a popular agent for pretreating cellulosic materials, but its strong hydrolyzing ability often damages the raw material and can lead to losses in material.<sup>16,17,23</sup> Such losses during pretreatment with NaOH are especially notable in the pretreatment of viscose, wherein even dilute concentrations of NaOH decrease viscose fiber content.<sup>6</sup> Alternatively, sodium carbonate (Na<sub>2</sub>CO<sub>3</sub>) can be used as an alkaline agent during pretreatment, resulting in less loss of material when applied to cellulosic waste textiles, compared with NaOH.<sup>16,23</sup>

In this study, we report that post-consumer waste viscose has inherent resistance toward hydrolysis, evaluating various pretreatment methods that are typically used in biorefining with regard to minimize this resistance and increasing the sugar yield. The pretreatment approaches comprised an acidic (sulfuric acid) and alkaline (sodium carbonate) method, each with and without gradual washing of the pretreated waste viscose. The results of this study will facilitate and provide useful insights into the development of tertiary recycling alternatives for post-consumer waste viscose.

## 2 Materials and methods

### 2.1 Collection and preparation of raw materials

The waste viscose was post-consumer 100% viscose that was purchased from a textile sorter (Lounais-Suomen Jätehuolto, Turku, Finland). The waste viscose was separated into a colored fraction and a white fraction. Textile trimmings that were not made of viscose, including seams, labels, buttons, and decorative details, were removed from the garments using a circular textile knife ( $\varnothing$  45 mm, Stoff & Stil, Malmö, Sweden). The textiles were then reduced to  $\sim 10 \times 10$  mm pieces in a textile shredder with a  $170 \times 107$  mm chamber and 15 mm blades (Filamaker, Kaufungen, Germany).

The control material was white pre-consumer 100% virgin viscose fabric (woven) (Textil & Metallskrot Skrotten AB, Kinna, Sweden) and medicinal cotton (VWR International, Radnor, PA, USA). The virgin viscose was cut into smaller pieces using the circular textile knife, which were then shredded into  $\sim 10 \times 10$  mm pieces in the textile shredder. The medicinal cotton was

not treated in any way and it was directly subjected to enzymatic hydrolysis in all experiments.

### 2.2 Enzymatic hydrolysis of nontreated viscose

**2.2.1 Effect of increased enzyme loading.** Colored waste viscose, white waste viscose, and white virgin viscose were added to a solids loading of 5% to separate 100 mL Erlenmeyer flasks that contained citrate–sodium citrate buffer. Six enzyme loadings (0.05, 0.10, 0.15, 0.20, 0.25, and 0.30 g enzyme blend per g dry textiles) were added to the flasks, resulting in a total mass of 100 g. The flasks were sealed and incubated for 96 h at  $50 \pm 3$  °C and  $270 \pm 10$  rpm, after which the contents were vacuum-filtered through a filter cloth with a pore size of 100  $\mu$ m. The hydrolysis experiments were conducted in duplicate. Samples from the liquid products that were obtained after the completion of hydrolysis were withdrawn and analyzed.

The enzyme blend was Cellic CTec 2 (Novozymes, Bagsværd, Denmark). The citrate–sodium citrate buffer (0.1 M and pH 5) was prepared in 5 L batches: 43.08 g of citric acid monohydrate and 86.77 g of sodium citrate dihydrate in 4 L distilled water. The pH was adjusted to 5 with sulfuric acid and sodium hydroxide as needed, and distilled water was added to a total volume of 5 L.

### 2.3 Pretreatment of waste viscose

**2.3.1 Alkaline pretreatment of waste viscose.** White and colored waste viscose underwent alkaline pretreatment using sodium carbonate (Na<sub>2</sub>CO<sub>3</sub>) for 1 h at 70, 120, and 170 °C. For each pretreatment, 760 g of Na<sub>2</sub>CO<sub>3</sub> solution was prepared, to which 40 g dry waste viscose was added and mixed. The pretreatment at 120 and 170 °C was conducted for 1 h in a Polyclave laboratory pressure reactor system equipped with a Cyclone 300 stirrer unit (both Büchi AG, Uster, Switzerland). The mixture was stirred at 200 rpm for 1 minute every 10 minutes to avoid agglomeration on the impeller. The pretreatment at 70 °C was performed for 1 h in a water bath. The contents were manually mixed occasionally. After completion of the pretreatment, the liquid was removed using an HP5M filter press (Fischer Maschinenfabrik GmbH, Neuss, Germany). The pretreated viscose was then washed with deionized water before enzymatic hydrolysis.

Pretreated viscose was subjected to enzymatic hydrolysis in Falcon tubes, with a total mass of 20 g; the mass of pretreated viscose corresponded to a solids loading of 5 wt% dry textiles, and enzymes were added to 0.05, 0.10, or 0.15 g enzyme blend per g dry viscose. Samples that contained medicinal cotton and untreated colored waste viscose were also hydrolyzed as controls. The tubes were incubated for 96 h at  $50 \pm 3$  °C and  $270 \pm 10$  rpm; the enzymatic hydrolysis was performed in duplicate. After hydrolysis, the contents were vacuum-filtered through a filter cloth with a pore size of 100  $\mu$ m. Samples of the liquid product were collected and analyzed.

**2.3.2 Acidic pretreatment of waste viscose.** White and colored waste viscose underwent acidic pretreatment with sulfuric acid (H<sub>2</sub>SO<sub>4</sub>) at 2 concentrations (15 wt% and 30 wt%) for 30 min at 30 °C and 50 °C in a water bath. For each pretreatment, 760 g of either H<sub>2</sub>SO<sub>4</sub> solution was prepared, to



which 40 g of dry waste viscose was added. After the pretreatment, the material was vacuum-filtered through a filter cloth (pore size 100  $\mu\text{m}$ ), washed with deionized water, and subjected to enzymatic hydrolysis, as described in Section 2.3.1.

#### 2.4 Gradual washing of pretreated waste viscose

White and colored waste viscose was pretreated as described in Sections 2.3.1 and 2.3.2, except for the wash steps. Pretreated viscose was washed with diluted pretreatment solution that contained 3 wt%  $\text{Na}_2\text{CO}_3$  or 10 wt%  $\text{H}_2\text{SO}_4$ , depending on the pretreatment. After the first wash, the materials were vacuum-filtered through a filter cloth (pore size 100  $\mu\text{m}$ ) and washed with 1 wt%  $\text{Na}_2\text{CO}_3$  or 5 wt%  $\text{H}_2\text{SO}_4$  solution for the alkali-pretreated and acid-pretreated viscose, respectively. After the second wash, the materials were vacuum-filtered, washed with deionized water, and vacuum-filtered again before being subjected to enzymatic hydrolysis, as detailed in Section 2.3.1.

#### 2.5 Analyses

**2.5.1 Analysis of raw material and glucose.** Samples of post-consumer waste viscose, pretreated viscose, and control materials were analyzed to determine the total solids (TS) and cellulose content. TS were analyzed by drying the samples at 105  $^\circ\text{C}$  overnight in an oven. The cellulose content was determined per the National Renewable Energy Laboratory (NREL), based on 2-step acid hydrolysis using sulfuric acid.<sup>24</sup>

The samples for this analysis were evaluated by high-performance anion exchange chromatography with pulsed amperometric detection (HPAEC-PAD) on an ICS3000 system (Dionex, Sunnyvale, CA, USA) equipped with a CarboPac PA1 column, GP50 gradient pump, and AS50 autosampler. The HPAEC-PAD analysis was performed at 30  $^\circ\text{C}$  and an eluent flow rate of 1  $\text{mL min}^{-1}$ . Deionized and degassed water, degassed sodium hydroxide solution (200  $\text{mmol per L NaOH}$ ), and degassed sodium hydroxide and sodium acetate solution (200  $\text{mmol per L NaOH}$ , 170  $\text{mmol per L NaAc}$ ) were used as eluents. The chemicals for the eluents were purchased from Merck (Merck KGaA, Darmstadt, Germany). In cases in which the HPAEC-PAD data indicated a cellulose content near 100%, the cellulose content of the samples was calculated by subtracting the mass of the dried unhydrolyzed solid residue from the oven-dried weight of the raw materials. All compositional analyses were performed in triplicate.

Samples obtained from the enzymatic hydrolysis were passed through a syringe filter (pore size 0.22  $\mu\text{m}$ ) and analyzed for sugar content on a Shimadzu LC-20 AD high-performance liquid chromatography (HPLC) system that was equipped with a Shimadzu RID 10A refractive index detector (Shimadzu Corporation, Kyoto, Japan) and a Carbosep CHO 782 column (Concise Separations, San Jose, CA, USA), which was operated at 70  $^\circ\text{C}$  and 50 bar, with 0.6  $\text{mL min}^{-1}$  deionized water as eluent.

**2.5.2 Enzyme adsorption.** Duplicates of each of the 3 shredded textile materials (colored waste viscose, white waste viscose, and white virgin viscose), corresponding to 5 g dry textiles, were added to bluecap bottles with approximately 94 g

sodium citrate buffer each, resulting in a solids loading of 5% dry textiles after addition of the enzyme blend. The bottles were placed in an ice bath with magnetic stirrers. After 30 min, 0.75 g of Cellic CTec 2, corresponding to an enzyme loading of 0.15 g enzyme blend per g dry textiles, was added and mixed. The enzymes were allowed to adsorb to the textile samples for 6 h with constant agitation, after which samples of the supernatant were collected.

The supernatants were centrifuged before being subjected to protein quantification. The concentration of unbound proteins in the samples was measured using Coomassie Plus (Bradford) Assay Reagent (Thermo Fisher Scientific, Waltham, MA, USA), and the absorbance at 595 nm was measured on a UV-1800 UV-VIS spectrophotometer (Shimadzu Corporation, Kyoto, Japan). The concentrations were determined against bovine serum albumin (BSA).

**2.5.3 Yield calculations.** Pretreatment and enzymatic hydrolysis experiments were evaluated based on glucose and overall yield. Glucose yield refers to the amount of glucose obtained with respect to the maximum amount contained in the substrate of the enzymatic hydrolysis (pretreated or not) while overall yield refers to the amount of glucose obtained with respect to the maximum amount contained in the starting material. This means that the overall yield takes into account any possible loss of substrate during pretreatment, while glucose yield is only a measure of the efficiency of the enzymes.

## 3 Results and discussion

### 3.1 Material composition

The waste viscose (colored and white) had a TS content of 95.8% ( $\pm 0.1\%$ ) and consisted of 99.1% cellulose (standard deviation 0.3%). The virgin viscose had a TS content of 94.0% ( $\pm 0.8\%$ ) and a cellulose content of 99.6% (standard deviation 0.4%). The TS content of the medicinal cotton was 93.4% ( $\pm 0.5\%$ ), with a cellulose content of 98.9% (standard deviation 0.5%). Data for the pretreated waste viscose can be found in Table S1.†

### 3.2 Effect of enzyme loading

Increased enzyme loadings resulted in higher glucose yields for all raw materials, although 0.3 g enzyme blend per g dry textiles was insufficient to hydrolyze the waste viscose completely. The virgin viscose achieved near-total hydrolysis at an enzyme loading of 0.15 g enzyme blend per g dry textiles, whereas the glucose yields for the colored and white waste viscose samples peaked at 80% and 60%, respectively (Fig. 1). Increasing the enzyme loading improves the hydrolysis yield of lignocellulosic biomass to a plateau, after which additional enzyme loading does not enhance yields significantly.<sup>15,25</sup> Consequently, it is not possible for glucose yields of the waste viscose samples to approach that of virgin viscose through increases in enzyme loading.

That post-consumer waste viscose was more recalcitrant toward hydrolysis was not unexpected. Many finishing agents can be added to the fabric between the spinning of the fibers and the



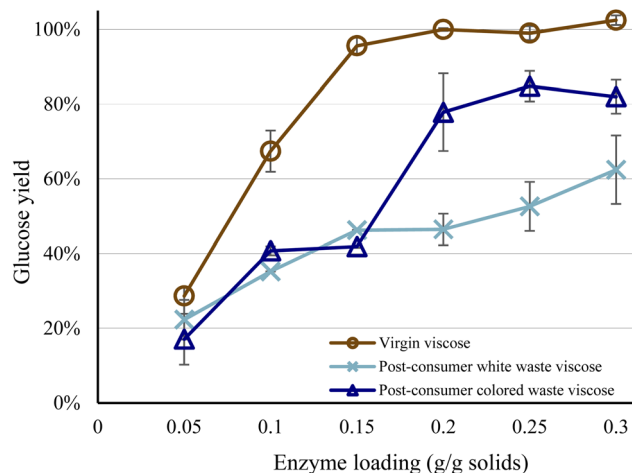


Fig. 1 Glucose yield as a function of enzyme loading, at a residence time of 96 h. Error bars show the spread between duplicates.

Table 1 Protein concentration of supernatant samples following enzyme adsorption to textiles

Sample	Protein concentration ( $\text{mg mL}^{-1}$ )
White pre-consumer viscose	0.52 ( $\pm 0.03$ )
White post-consumer viscose	0.50 ( $\pm 0.01$ )
Colored post-consumer viscose	0.54 ( $\pm 0.02$ )

sale of the garment. The type of finisher depends on the customer's requirements and thus differs between fabrics,<sup>26</sup> and certain finishing agents can significantly inhibit enzymatic activity against textiles.<sup>13</sup> Further, worn textiles come into contact with contaminants during use, such as oily organic substances in perspiration, human skin, sebum, and clay minerals, as well as oils from food, cosmetics, and machinery.<sup>27,28</sup> Whereas some of these contaminants are readily removed during washing, others, such as sebum, do not desorb and thus accumulate in textiles,<sup>28,29</sup> suggesting that these contaminants caused the recalcitrance of waste viscose samples toward hydrolysis.

The origin of the recalcitrance of post-consumer waste viscose toward hydrolysis was examined by analyzing the adsorption of enzyme on samples of colored and white waste viscose and virgin viscose. The adsorption of enzyme was similar across all samples (Table 1), indicating that their resistance to hydrolysis did not stem from the inaccessibility of enzymes to waste viscose. Instead, we attributed the recalcitrance of waste viscose to inhibition of the active site.

### 3.3 Pretreatment of waste viscose

The most efficient method of improving glucose yields beyond the point at which they have been maximized by enzyme loading is pretreatment.<sup>15</sup> The effects of alkaline and acidic pretreatment were thus examined with regard to overcoming the resistance of post-consumer waste viscose to hydrolysis compared with virgin viscose. A consolidated table presenting

the different pretreatment conditions tested as well as the cellulose recovery and glucose yield obtained at each condition can be found in Appendix B of the ESI Table S2.†

**3.3.1 Alkaline pretreatment.** The glucose yield after pretreating colored post-consumer waste viscose with 5%  $\text{Na}_2\text{CO}_3$  at temperatures below 120 °C was similar to that of nontreated post-consumer waste (Fig. 2). In contrast, pretreatment at higher temperatures (170 °C) led to a pronounced decrease in glucose yields, indicating that increased severity during pretreatment fails to improve yields. Thus, dilute alkaline pretreatment does not result in higher enzymatic activity and, in point of fact, further impedes depolymerization of the material.

As shown above, pretreatment with  $\text{Na}_2\text{CO}_3$  effected losses in cellulose prior to enzymatic hydrolysis. Thus, because pretreatment did not improve enzymatic activity, the overall yields (based on the cellulose in the starting material) were lower for all pretreated samples *versus* nontreated material (Fig. 2). Losses in cellulose during alkali pretreatment of waste cotton have been reported,<sup>23</sup> but we observed such decreases under milder pretreatment conditions, due to the lower degree of polymerization and crystallinity of waste viscose. Thus, based on its greater proclivity to degrade during pretreatment, waste viscose can only be pretreated under mild conditions to avoid unacceptable cellulose losses; such conditions, however, are insufficient to increase the amenability to enzymes. As a result, alkali pretreatment is not a feasible strategy for overcoming the resistance of waste viscose.

**3.3.2 Acidic pretreatment.** Pretreatment with 15%  $\text{H}_2\text{SO}_4$  lowered glucose yields slightly compared with nontreated material at the highest enzyme loading but decreased them substantially at the lowest loading (Fig. 3). Increasing the concentration of  $\text{H}_2\text{SO}_4$  in the pretreatment to 30% impaired the hydrolysis further, resulting in lower glucose yields at all enzyme loadings. In certain cases, waste viscose that was pretreated with 30%  $\text{H}_2\text{SO}_4$  performed worse than medicinal cotton, which is more difficult to depolymerize due to the higher recalcitrance of its cellulose structure.<sup>6</sup> Thus, acid pretreatment failed to have the positive effect on waste viscose that has been reported for other cellulosic materials,<sup>30,31</sup> highlighting the uniqueness of this waste stream and necessitating alternative strategies to circumvent its enzymatic inhibition.

Pretreatment with 15%  $\text{H}_2\text{SO}_4$  led to no extensive loss in cellulose, whereas cellulose levels fell by roughly 5% with 30%  $\text{H}_2\text{SO}_4$ . As a result, the overall yield approximated the glucose yield in all cases (Fig. 3). Exposure of waste cotton to higher concentrations of sulfuric acid (60% to 80%) induces extensive cellulose degradation.<sup>8</sup> Because waste viscose is significantly more susceptible to degradation than waste cotton,<sup>6</sup> it is unlikely that increased acid concentrations will improve the efficiency of the process. As with alkali pretreatment, the results indicate that waste viscose can only be pretreated under mild conditions to avoid unacceptable losses in cellulose, but these conditions are insufficient to increase enzymatic activity.

The results of the acid pretreatment should be interpreted with caution, because the enzymatic hydrolysis was performed using the same batch of enzyme blend as for the alkaline pretreatment studies, albeit several months later. The



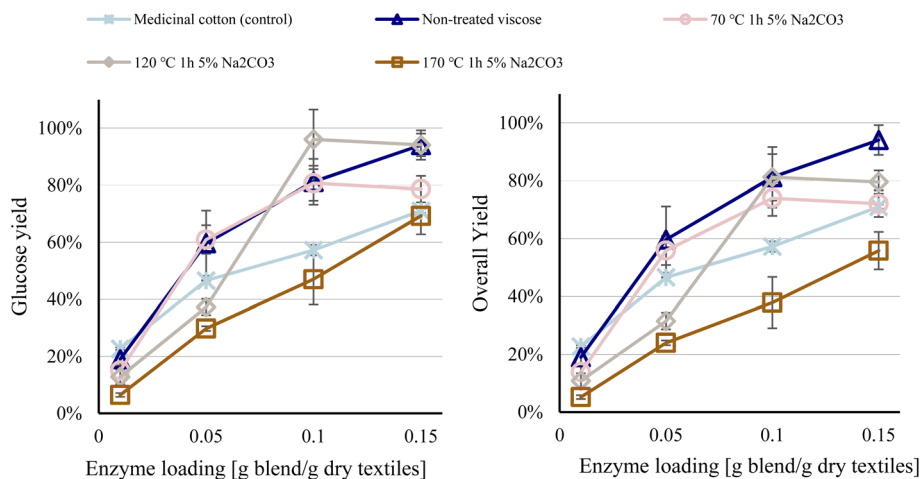


Fig. 2 Glucose and overall yields on alkaline pretreatment of colored post-consumer waste viscose.

performance of the enzymes declined during this period, as evidenced by the 16% lower glucose yield for the control material (medicinal cotton) between the 2 experiments. Thus, despite the lower yields in Fig. 3 *versus* Fig. 2, the 2 pretreatment methods performed similarly, with the optimal condition for each method resulting in approximately the same overall yield as nontreated waste viscose.

### 3.4 Post-pretreatment gradual washing

We hypothesized that the unexpected negative effect of chemical pretreatment on waste viscose was attributed to the formation of a boundary layer that results from washing immediately with deionized water following pretreatment, impeding the activity of enzymes against the pretreated material. Gradual washing could thus reduce the evolution of such a boundary layer by decreasing the concentration gradient to which the pretreated waste viscose is exposed during the wash. Gradual washing is common in the textile and pulp industries, which frequently apply countercurrent washing to limit the generation of wastewater. Thus, a series of experiments was conducted, in which the pretreated materials

were washed twice with increasingly dilute solutions of  $\text{Na}_2\text{CO}_3$  and  $\text{H}_2\text{SO}_4$  for the alkaline and acidic pretreated materials, respectively, before a third wash with deionized water, followed by enzymatic hydrolysis.

The incorporation of a gradual wash step after the pretreatment of waste viscose with  $\text{Na}_2\text{CO}_3$  increased glucose yields compared with pretreated waste viscose that did not undergo a gradual wash (Fig. 4). Without gradual washing, the pretreated material performed slightly worse than the nontreated material but performed modestly better with it. This improvement demonstrates that this post-pretreatment procedure is an important determinant of the efficiency of the process and influences the effect of pretreatment on waste viscose. It also strengthens the hypothesis that gradual washing reduces the formation of a boundary layer that impedes enzymatic hydrolysis and explains the lower glucose yields in the previous experiments.

Gradual washing with  $\text{H}_2\text{SO}_4$  after acidic pretreatment decreased glucose yields compared with no gradual washing (Fig. 5). This decline coincided with a drop in pH on addition of

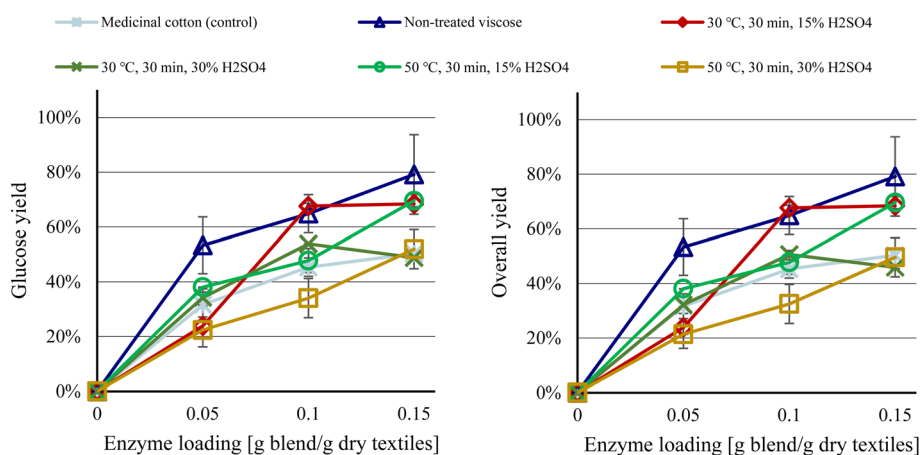


Fig. 3 Glucose and overall yields for pretreated colored post-consumer waste viscose after acidic pretreatment.



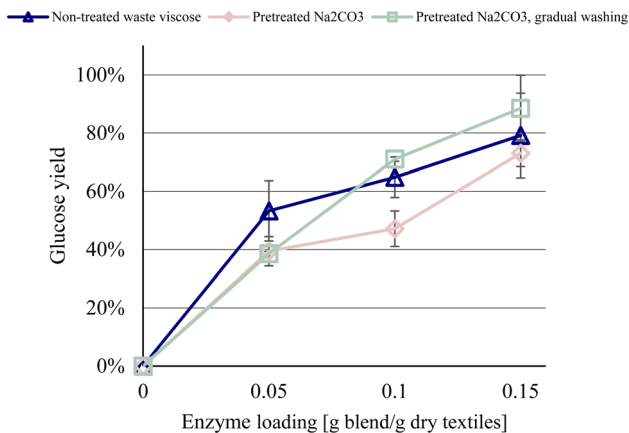


Fig. 4 Glucose yield of alkali pretreated post-consumer waste viscose (70 °C, 1 h, 5% Na<sub>2</sub>CO<sub>3</sub>) with and without gradual washing.

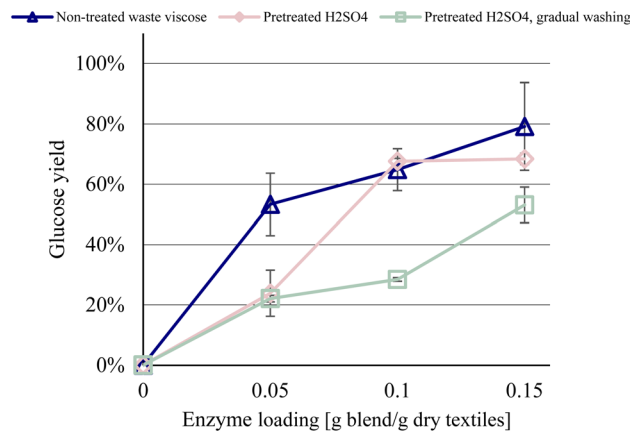


Fig. 5 Glucose yield of acid pretreated post-consumer waste viscose (30 °C, 30 min, 15% H<sub>2</sub>SO<sub>4</sub>) with and without gradual washing.

washed pretreated material to the buffer, indicating the presence of residual H<sub>2</sub>SO<sub>4</sub> in the washed pretreated material, explaining the lower enzymatic activity. We conclude that the gradual washing procedure in this case results in insufficient acid removal prior to enzymatic hydrolysis, necessitating a prolonged sequence with additional wash steps.

Despite the improved efficiency due to gradual washing, the increase in glucose yield remained limited compared with the non-treated material, when applying alkali pretreatment. Further, application of acid pretreatment effected no clear improvements, and gradual washing in the post-pretreatment step would need to be prolonged to completely remove residual acid. Thus, although post-pretreatment is beneficial in certain cases, the inhibition that is associated with waste viscose cannot be overcome through chemical pretreatment.

### 3.5 Comparison with other cellulosic feedstocks

Post-consumer waste viscose exhibited mass losses even under mild pretreatment conditions, negating any improvement in hydrolyzability. This behavior eliminates the benefit of pretreatment before enzymatic hydrolysis, because it fails to improve the overall yield of the process. To ensure that no mass losses occur, the severity of the pretreatment must be lowered to a level at which there is no increase in the hydrolyzability of the post-consumer waste viscose. This property is notable, because it distinguishes post-consumer waste viscose from other types of cellulosic feedstocks in biorefinery applications, such as lignocellulosic biomass.

There are abundant previous studies that demonstrate the positive effect of pretreatment on other types of materials. For example, pretreating cotton with 20% NaOH at 100 °C increasing glucose yield from 26.2% to 98.6%<sup>5</sup> while pretreatment with 5% Na<sub>2</sub>CO<sub>3</sub> (the same chemical used in this study) at 200 °C increased the glucose yield from 30% to 80%.<sup>23</sup> There is a stark difference between these results and those obtained for viscose in this study, as pretreatment with 5% Na<sub>2</sub>CO<sub>3</sub> at 170 °C actually led to a decrease of the glucose yield which is the opposite behavior as that observed for cotton. There are also

clear differences between viscose and other lignocellulosic feedstocks beyond textile fibers. For example, pretreating bamboo with sulfuric acid at 180 °C led to an increase in glucose yield from 2.5% to 49.4%<sup>30</sup> while glucose yield for viscose samples treated with sulfuric acid was lower than for untreated viscose in this study. Once again, viscose exhibits opposite changes in hydrolyzability upon pretreatment and it is therefore clear that this feedstock has a unique behavior in biorefinery applications that requires adjusting process concepts and conditions in a different manner compared to previously studied feedstocks.

Post-consumer waste viscose contains cellulose II, the thermodynamically more stable crystal lattice and the confirmation that is assumed by the regenerated cellulose that is recovered.<sup>32</sup> Cellulose II is more susceptible to hydrolytic degradation than cellulose I, which is the naturally occurring crystal lattice in plant biomass.<sup>6,32,33</sup> However, the difference in hydrolyzability between cotton and viscose textiles is greater<sup>6</sup> than what is expected from the disparities between cellulose I and II; further, we have shown that this difference is more pronounced when comparing post-consumer waste cotton<sup>23</sup> with post-consumer waste viscose, although this difference depends on the presence of textile additives.

Previous studies show that it would also be possible to convert waste cotton into glucose *via* acid hydrolysis.<sup>4</sup> Acid hydrolysis delivered higher yields than those obtained in this study or, alternatively, similar yields at higher concentration of glucose.<sup>4</sup> However, the mixture obtained from enzymatic hydrolysis would be biocompatible, that is, it would be possible to directly ferment it without any treatment while the mixture from acid hydrolysis would require a separation step to remove the acid, for which there are no commercially attractive alternatives. Thus, in spite of the lower efficiency in the production of glucose, enzymatic hydrolysis seems a more promising technology due to advantages in downstream processing and biocompatibility of the product.

Post-consumer waste viscose is a unique second-generation cellulosic feedstock, because its valorization by enzymatic hydrolysis does not benefit from pretreatment. Thus, the price of the



downstream product, glucose, and the economics of the process depend entirely on the intrinsic characteristics of the feedstock—*i.e.*, its hydrolyzability and cost. Consequently, efficient and low-cost sourcing of the feedstock are paramount to the economic viability of sugar production from waste viscose, and even if such feedstock becomes available, the process and economics would nevertheless rely heavily on the substances that are introduced to the material during the manufacturing and use phases.

## 4 Conclusions

Post-consumer waste viscose is resistant to enzymatic hydrolysis. This recalcitrance was noted for white and colored waste viscose, of which the former was more resistant. In contrast, pre-consumer virgin viscose fabric was completely hydrolyzed at moderate enzyme loadings above 0.15 g Cellic CTec 2 per g dry textiles. The recalcitrance of post-consumer waste viscose likely stems from inhibition of the viscose by contaminants that are introduced during garment manufacture and use, such as textile finishers and sebum.

The recalcitrance against enzymatic hydrolysis of post-consumer waste viscose can be partially overcome by increasing the enzyme loading, although it is insufficient to hydrolyze the material completely. Pretreatment of waste viscose with Na<sub>2</sub>CO<sub>3</sub> or H<sub>2</sub>SO<sub>4</sub> over a range of conditions, followed by a wash with deionized water prior to hydrolysis, does not improve glucose yields. Gradual washing after the pretreatment increased the glucose yield when using Na<sub>2</sub>CO<sub>3</sub> (70 °C, 1 h, 5%) and decreased it with H<sub>2</sub>SO<sub>4</sub>, compared with the hydrolysis of nontreated waste viscose. Thus, only one of the pretreatment procedures that were tested can overcome the inhibition and effect higher enzymatic activity and glucose yields.

However, the improvement in glucose yield following the combination of pretreatment and gradual washing is counteracted by mass losses during pretreatment with Na<sub>2</sub>CO<sub>3</sub>. This property is notable, differentiating post-consumer waste viscose from other second-generation cellulosic feedstocks, because otherwise effective pretreatment methods fail to improve the overall yield of saccharification. Thus, the cost of the glucose that is produced *via* enzymatic hydrolysis of post-consumer waste viscose depends heavily on the price of the feedstock and its inherent hydrolyzability. Consequently, higher enzyme loadings and lower process efficiency will be associated with post-consumer waste viscose compared with its pre-consumer counterpart, prompting us to conclude that (enzymatically) saccharifying this waste stream will become more expensive after the use phase.

## Data availability

Data used in this study is contained within the article.

## Author contributions

Edvin Bågenholm-Ruuth: conceptualization, data curation, formal analysis, investigation, methodology, supervision,

validation, visualization, writing – original draft, writing – review & editing. Mahla Bagherigeldardi: data curation, investigation, validation, writing – original draft. Caroline Gustafsson: conceptualization, data curation, formal analysis, investigation, methodology, validation, visualization. Miguel Sanchis-Sebastiá: conceptualization, formal analysis, methodology, project administration, supervision, validation, visualization, writing – review & editing. Ola Wallberg: conceptualization, funding acquisition, project administration, resources.

## Conflicts of interest

Authors Mahla Bagherigeldardi and Miguel Sanchis-Sebastiá are employed by ShareTex AB. Authors Edvin Bågenholm-Ruuth, Miguel Sanchis-Sebastiá, and Ola Wallberg owns shares in ShareTex AB. Author Caroline Gustafsson declares no financial interests.

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