

Cite this: *J. Mater. Chem. A*, 2024, 12, 30329

# Regulating NO<sub>2</sub> adsorption at ambient temperature by manipulating copper species as binding sites in copper-modified SSZ-13 zeolites†

Mingzhe Sun,<sup>‡ab</sup> Tianqi Wang,<sup>‡ab</sup> Calvin Ku,<sup>a</sup> Aamir Hanif,<sup>‡ab</sup> Tian Tian,<sup>‡c</sup> Bernt Johannessen,<sup>de</sup> Qinfen Gu,<sup>‡\*d</sup> Ziyi Li,<sup>‡\*f</sup> Patrick Sit<sup>‡\*a</sup> and Jin Shang<sup>‡\*abg</sup>

Atmospheric NO<sub>2</sub> pollution poses significant risks to human health and the environment even at low concentrations, necessitating the development of efficient technologies for its removal under ambient conditions. In this study copper (Cu)-modified SSZ-13 zeolites (referred to as Cu<sup>n+</sup>SSZ-13 where *n* represents the valence state of Cu) were developed for NO<sub>2</sub> removal by adsorption. Cu<sup>n+</sup>SSZ-13 zeolites containing Cu species with different valence states and proportions were prepared by reducing a Cu<sup>2+</sup>-exchanged SSZ-13 zeolite (Cu<sup>2+</sup>SSZ-13) using H<sub>2</sub> at different temperatures. The Cu<sup>n+</sup>SSZ-13 reduced at 190 °C showed the highest NO<sub>2</sub> removal capacity (1.79 mmol g<sup>-1</sup>), outperforming pristine SSZ-13 and Cu<sup>2+</sup>SSZ-13 by 52.3% and 19.4%, respectively. The improvement was due to the increased amount of adsorption sites (Cu<sup>+</sup> and H<sup>+</sup>) and the stronger affinity of Cu<sup>+</sup> than Cu<sup>2+</sup> for NO<sub>2</sub>, as confirmed by density functional theory (DFT) calculations. The generation of Cu<sup>0</sup> nanoparticles and moisture in zeolites during reduction was undesirable for NO<sub>2</sub> adsorption. However, this could be eliminated by lowering the reduction temperature and performing thermal activation, respectively. This work provides systematic methods for designing zeolite adsorbents for ambient NO<sub>2</sub> removal and offers insights into the burgeoning field of air pollution control.

Received 25th June 2024  
Accepted 6th October 2024

DOI: 10.1039/d4ta04399e

rsc.li/materials-a

## 1. Introduction

Nitrogen oxides (NO<sub>x</sub>), including NO and NO<sub>2</sub>, are primarily emitted from mobile and stationary sources such as vehicles and industries. NO<sub>x</sub> have raised public concerns due to their detrimental effects on both human health and ecosystems.<sup>1–3</sup> For example, NO<sub>x</sub> can interact with other air pollutants such as volatile organic compounds (VOCs) under sunlight, leading to

the formation of secondary pollutants such as smog and highly irritating gases.<sup>4–6</sup> Meanwhile, NO<sub>x</sub> themselves, as toxic components, can directly affect human health by decreasing lung function and causing respiratory symptoms, even at low concentrations.<sup>7</sup> As NO<sub>2</sub> is more active and around 30 times more toxic than NO,<sup>8</sup> NO<sub>2</sub> is categorized as a criteria pollutant representing NO<sub>x</sub>. Thus, atmospheric NO<sub>2</sub> pollution and its control have attracted increased attention in recent decades, particularly in densely populated urban areas. For example, the concentration of roadside NO<sub>2</sub> in Hong Kong remains at a harmful level (80 μg m<sup>-3</sup>),<sup>9</sup> which is twice the World Health Organization (WHO) standard (40 μg m<sup>-3</sup>).<sup>10</sup> The complex and congested nature of Hong Kong makes it challenging to dilute the roadside NO<sub>2</sub>. Therefore, efforts to abate atmospheric NO<sub>2</sub> should focus on both reducing NO<sub>2</sub> emissions in exhaust gases and removing NO<sub>2</sub> from the ambient air.

De-NO<sub>x</sub> technologies, such as selective catalytic reduction (SCR) and selective non-catalytic reduction (SNCR), have been extensively developed and implemented, delivering high efficiency in NO<sub>x</sub> removal (99%).<sup>11–13</sup> However, the operating temperature window (300–1100 °C) of these technologies makes their application prohibitive in low-temperature NO<sub>x</sub> (e.g., atmospheric NO<sub>x</sub>) abatement. Moreover, the generation of NH<sub>3</sub> (as a reductant) by decomposing urea solution at low temperatures (<180 °C) poses a significant challenge for the SCR

<sup>a</sup>School of Energy and Environment, City University of Hong Kong, Tat Chee Avenue, Kowloon, Hong Kong SAR, P. R. China. E-mail: patrick.h.sit@cityu.edu.hk; jinshang@cityu.edu.hk

<sup>b</sup>City University of Hong Kong Shenzhen Research Institute, Nanshan District, Shenzhen 518000, P. R. China

<sup>c</sup>Department of Applied Biology and Chemical Technology, The Hong Kong Polytechnic University, Hung Hom, Hong Kong SAR, P. R. China

<sup>d</sup>Australian Synchrotron, ANSTO, 800 Blackburn Road, Clayton, VIC 3168, Australia. E-mail: qinfeng@ansto.gov.au

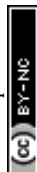
<sup>e</sup>Institute for Superconducting & Electronic Materials, University of Wollongong, Wollongong, NSW 2522, Australia

<sup>f</sup>School of Energy and Environmental Engineering, University of Science and Technology Beijing, Beijing 100083, China. E-mail: ziyili@ustb.edu.cn

<sup>g</sup>Low-Carbon and Climate Impact Research Center, School of Energy and Environment, City University of Hong Kong, Hong Kong, P. R. China

† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4ta04399e>

‡ These authors contributed equally to this work.



process.<sup>14</sup> In addition, stricter regulations have increased the urgency for low-temperature NO<sub>x</sub> emission control. Adsorption is considered an alternative approach for NO<sub>x</sub> removal at low temperature. However, most adsorbents have only been evaluated for NO<sub>x</sub> adsorption at temperatures above 80 °C,<sup>15–17</sup> omitting NO<sub>2</sub> adsorption under ambient conditions. Thus, this study aims to develop effective NO<sub>2</sub> adsorbents, with high NO<sub>2</sub> adsorption capacity and selectivity, for atmospheric NO<sub>2</sub> abatement at ambient temperature.

Adsorbents that exhibit a specific affinity for NO<sub>2</sub> with moderate strength can afford high NO<sub>2</sub> selectivity and capacity, making them desirable for NO<sub>2</sub> adsorption. Given the presence of  $\pi$  bonds in the NO<sub>2</sub> molecule, materials containing transition metal species are promising candidates for NO<sub>2</sub> adsorption due to their unique interaction ( $\pi$ -complexation) with NO<sub>2</sub>, which enables  $\pi$ -backdonation from a d orbital metal center to the  $\pi^*$  orbitals of the  $\pi$ -structured molecules.<sup>18</sup> This interaction, with moderate strength, bridges the gap between physisorption and chemisorption, enabling the  $\pi$ -complexation adsorbents to exhibit both high selectivity and good reversibility.<sup>19</sup> Copper (Cu), an affordable and abundant transition metal that has been extensively studied and used in high-temperature NO<sub>x</sub> SCR, has emerged as a promising candidate for NO<sub>2</sub> adsorption.<sup>20–24</sup> For instance, Cu-containing carbon showed a high NO<sub>2</sub> removal capacity at room temperature, while the low thermal stability of carbon materials causes them to burn readily during regeneration at high temperatures.<sup>20</sup> Cu nanoparticle (NP) loaded silica (KCC-1) has been reported to be an effective NO<sub>2</sub> adsorbent, with the highly dispersed Cu NPs serving as effective adsorption sites for NO<sub>2</sub>.<sup>25</sup> However, NO<sub>2</sub> adsorption and dissociation on Cu<sup>2+</sup> and Cu<sup>+</sup> have not been studied. Cu-based metal-organic frameworks (MOFs) showed enhanced NO<sub>2</sub> adsorption due to increased porosity and the reactive adsorption of NO<sub>2</sub> on Cu.<sup>24</sup> However, the high cost and low thermal/hydrothermal stability of MOFs limit their applications in real-world gas adsorption processes.

Small-pore zeolites, characterized by their three-dimensional porous structures, high thermal stability, and large surface areas, have extensive applications in gas adsorption and separation.<sup>26</sup> Zeolites can also serve as unique ligands that tune the  $\pi$ -complexation between NO<sub>2</sub> and Cu.<sup>27</sup> Sierraalta *et al.* have demonstrated that Cu species-containing zeolites showed a stronger affinity for NO<sub>2</sub> molecules than those containing other transition metals (Ag and Au).<sup>28</sup> Onitsuka *et al.* reported that zeolites infused with Cu salts showed enhanced performance in adsorbing NO<sub>x</sub> at a low concentration of about 5 ppm.<sup>29</sup> Note that extra-framework cations in zeolites are the dominant adsorption sites, whose properties dictate gas adsorption performance.<sup>30</sup> For instance, the valence state of these cations can affect NO<sub>2</sub> adsorption performance, particularly the affinity of the adsorbent for NO<sub>2</sub>. For specific types of cations, such as Cu, their valence state is directly related to the radius and the occupancy of the valence shell. Compared with Cu<sup>2+</sup>, Cu<sup>+</sup> and Cu<sup>0</sup> possess higher valence shell occupancies and fewer constraints (due to the larger radius) on the valence shell electrons, allowing more d-orbital electrons to be back-donated to the  $\pi^*$  orbital of NO<sub>2</sub>. Consequently, the  $\pi$ -complexation

occurring between NO<sub>2</sub> and Cu ions at lower states (Cu<sup>+</sup> and Cu<sup>0</sup>) is anticipated to improve gas-host interaction, leading to a higher affinity for NO<sub>2</sub>.

Herein, we prepared Cu<sup>*n*+</sup>SSZ-13 zeolites (*n* = 0, 1, and 2) by reducing a Cu<sup>2+</sup>-exchanged SSZ-13 zeolite under a H<sub>2</sub> atmosphere and systematically studied their NO<sub>2</sub> removal performance and mechanisms. Thanks to the formation of Cu<sup>+</sup> ions and the increased number of adsorption sites, Cu<sup>*n*+</sup>SSZ-13 zeolites showed enhanced NO<sub>2</sub> uptake and insignificant NO release. This work suggests that the tuning of Cu species as specific binding sites in zeolites could be an effective approach for regulating the affinity of zeolites for NO<sub>2</sub> adsorption.

## 2. Experimental

### 2.1 Synthesis

**2.1.1 Synthesis of H<sup>+</sup>SSZ-13 (Si/Al = 12).** The synthesis of H<sup>+</sup>SSZ-13 (Si/Al = 12) was conducted following a previously reported method.<sup>31</sup> Specifically, 39.6 g of *N,N,N*-trimethyl-1-adamantanamine hydroxide (TMAdaOH, 25 wt%, SACHEM Inc.) and 19.5 g of tetraethyl orthosilicate (TEOS, sigma 98%) were mixed with 4.05 g of deionized (DI) water. This mixture was stirred for 2 h at room temperature in a sealed polypropylene bottle. Afterwards, 1.05 g of aluminum ethoxide (Strem Chemical, 99%) was added to the mixture and stirred for another 1 h. The gel was then transferred into a 100 mL Teflon-lined autoclave and heated at 140 °C under static conditions for 6 days. After the crystallization, the product was filtered, thoroughly washed with DI water, and then dried at 80 °C overnight. Finally, the product was calcined in an air atmosphere at 550 °C for 8 h with a ramping rate of 2 °C min<sup>-1</sup>.

**2.1.2 Synthesis of Cu<sup>2+</sup>SSZ-13.** The synthesis of Cu<sup>2+</sup>SSZ-13 involved a liquid-phase ion exchange process, a common approach for incorporating extra-framework cations into zeolites. Typically, 0.5 g of the as-synthesized H<sup>+</sup>SSZ-13 was dispersed in 50 mL of 0.5 M NH<sub>4</sub>NO<sub>3</sub> and stirred for 12 h at 80 °C, with the process being repeated four times to ensure thorough ion exchange. The resulting NH<sub>4</sub><sup>+</sup>SSZ-13 product was filtered, thoroughly washed with DI water, and dried at 80 °C overnight. Then, 0.5 g of the as-synthesized NH<sub>4</sub><sup>+</sup>SSZ-13 was dispersed in 50 mL of 0.5 M Cu(NO<sub>3</sub>)<sub>2</sub> solution and stirred for 12 h at 80 °C, again being repeated four times. The resulting Cu<sup>2+</sup>SSZ-13 was collected by filtration, washed extensively with DI water, and dried at 353 K overnight.

**2.1.3 Synthesis of H<sub>2</sub>-reduced Cu<sup>*n*+</sup>SSZ-13 samples.** A series of Cu<sup>*n*+</sup>SSZ-13 samples were prepared by reducing Cu<sup>2+</sup>SSZ-13 under a H<sub>2</sub> atmosphere at various temperatures. H<sub>2</sub>-temperature programmed reduction (TPR) was conducted on a Micromeritics ASAP 2950 instrument to identify optimal reduction conditions for the preparation of Cu<sup>*n*+</sup>SSZ-13. The signal of H<sub>2</sub> during the reduction process was detected using a thermal conductivity detector (TCD). Then, 0.1 g of Cu<sup>2+</sup>SSZ-13 was placed in a tube furnace and thermally treated under argon at 350 °C (ramping rate = 2 °C min<sup>-1</sup>) for 4 h to remove the pre-adsorbed impurities. After cooling to room temperature, 5% H<sub>2</sub> (balanced with Ar, 20 cc min<sup>-1</sup>) was continuously purged and Cu<sup>2+</sup>SSZ-13 was heated at 100 °C to 700 °C for 3 h (ramping



rate = 2 °C min<sup>-1</sup>). The resulting products are named Cu<sup>n+</sup>SSZ-13-reducing temperature-R (e.g., Cu<sup>n+</sup>SSZ-13-100-R).

## 2.2 Characterization

Synchrotron powder X-ray diffraction (PXRD) was measured using a Mythen-II detector at the PD beamline, Australian Synchrotron, ANSTO. To understand the valence state and the coordination environment of the Cu ions in Cu<sup>n+</sup>SSZ-13 samples, Cu K-edge X-ray absorption near-edge structure (XANES) and extended X-ray absorption fine structure (EXAFS) spectra were collected at the XAS beamline, Australian Synchrotron, ANSTO. The morphologies of the samples were investigated using a scanning electron microscope (SEM) (EVO MA10, ZEISS, Germany). The specific surface area and pore volume of Cu<sup>n+</sup>SSZ-13-190-R before and after NO<sub>2</sub> dynamic column adsorption, as well as fresh H<sup>+</sup>SSZ-13, were determined using a 3Flex Surface Characterization Analyzer (Micromeritics Instrument Corp., USA) using N<sub>2</sub> at -196 °C. Prior to measurement, the samples were degassed on the 3Flex Surface Characterization Analyzer at 300 °C for 3 h. The chemical composition (e.g., Si/Al and metal/Al ratios) of the samples was determined by Energy dispersive spectroscopy (EDX) using an EDX detector (Oxford Aztec Energy X-MAX 50) installed in a SEM (FEI Quanta 450 FEG). The *in situ* Fourier Transform Infrared (FTIR) spectra of Cu<sup>n+</sup>SSZ-13-190-R were recorded on an IRAffinity-1 FTIR spectrophotometer (Shimadzu, Japan) at 25 °C, with an NO<sub>2</sub> concentration of 1000 ppm and a flow rate of 60 mL min<sup>-1</sup>. Before the measurement, Cu<sup>n+</sup>SSZ-13-190-R was thermally treated in the FTIR cell under a N<sub>2</sub> atmosphere at 200 °C for 8 h to remove the pre-adsorbed gases and moisture.

## 2.3 Fixed-bed NO<sub>2</sub>/NO dynamic column adsorption at room temperature

The dynamic column breakthrough (DCB) of NO<sub>x</sub> was measured using a fixed-bed system (Fig. S1†) under ambient conditions (25 °C, 1 bar). The adsorbent (0.1 g) was well mixed with non-reactive glass beads (3 mm in diameter) to generate a homogeneous bed, and then packed into a stainless-steel tube. Unless otherwise specified, the samples were degassed at 300 °C under argon before NO<sub>x</sub> adsorption until the pre-adsorbed moisture was completely removed, as monitored by a Mass Spectrometer (Stanford Research Systems UGA300). Subsequently, NO<sub>2</sub> or NO (both at 1000 ppm) in helium was purged through the column at a total inlet flow rate of 60 mL min<sup>-1</sup> at 25 °C. The concentrations of NO<sub>2</sub> and NO in the outlet gas were measured using an electrochemical sensor (RAE Systems, MultiRAE Plus PGM-50/5P).

## 2.4 Density functional theory (DFT) calculation

DFT calculations were performed using the QUANTUM ESPRESSO package.<sup>32–35</sup> Ultrasoft pseudopotentials with the Perdew–Burke–Ernzerhof exchange–correlation functional were employed.<sup>36</sup> The plane wave cutoffs were 30 Ry and 240 Ry for wavefunctions and the augmented charge density, respectively. The semiempirical Grimme's DFT-D3 scheme was used for van der Waals interaction correction.<sup>37</sup> The SSZ-13 zeolite has a 1 ×

1 × 1 supercell with a total trigonal P supercell size of 13.675 Å × 13.675 Å × 14.767 Å. Three Si atoms were replaced with Al atoms. To maintain the charge balance, hydrogen atoms were added near the Al atoms according to the charge of the inserted transition metal ions. The 6-membered ring (6MR) has been identified as the most favorable location for the extra-framework cations.<sup>38</sup> Thus, we examined the local structures of the Cu ions in the 6MR, with 2 Si atoms being replaced by 2 Al atoms.

## 3. Results and discussion

### 3.1 Characterization of adsorbents

Cu<sup>2+</sup>SSZ-13 was prepared from H<sup>+</sup>SSZ-13 by an ion-exchange method, where Cu<sup>2+</sup> substituted the extra-framework H<sup>+</sup> cations (Fig. 1a). The synchrotron PXRD patterns of Cu<sup>2+</sup>SSZ-13 indicated the high purity and crystallinity characteristic of chabazite (CHA)-type SSZ-13 zeolite (Fig. 1b). As displayed in the SEM image (Fig. 1c), Cu<sup>2+</sup>SSZ-13 particles possess an elliptical shape and smooth exterior surfaces. Cu<sup>n+</sup>SSZ-13 zeolites were then prepared by reducing Cu<sup>2+</sup>SSZ-13 under H<sub>2</sub>. Prior to the reduction, H<sub>2</sub>-TPR was conducted to determine the optimal reduction temperature (Fig. 1d). With the temperature increasing, two H<sub>2</sub> consumption peaks appeared at around 200 and 400 °C, which were attributed to the reduction of Cu<sup>2+</sup> at various locations within the zeolite.<sup>39</sup> It is noteworthy that Cu<sup>2+</sup> ions at different locations within the zeolite require different energy levels to be reduced. For example, the six-membered ring (6MR) in CHA is the most stable site for Cu<sup>2+</sup>, demanding more energy for reduction than those situated at an eight-membered ring (8MR).<sup>40,41</sup> To achieve varying levels of Cu<sup>2+</sup> reduction in SSZ-13 zeolite, both low (≤250 °C) and high temperature (≥390 °C) ranges were adopted.

Upon high-temperature reduction (390, 490, and 750 °C), the structure of Cu<sup>n+</sup>SSZ-13 samples remained intact, as evidenced by the unchanged PXRD peak locations of Cu<sup>n+</sup>SSZ-13 and Cu<sup>2+</sup>SSZ-13 (Fig. 2a). However, the undesirable formation of Cu<sup>0</sup> occurred on the external surface of the zeolite (Fig. 2c). Rietveld refinement of PXRD indicated that the crystallite size of these Cu<sup>0</sup> particles (17, 23, and 25 nm at 390, 490, and 750 °C, respectively) increased with the increasing reduction temperature (Fig. S2†). The X-ray absorption spectroscopy (XAS) results showed that higher reduction temperatures resulted in a shift towards lower energy and a reduction in intensity of the white line peak (Fig. 2b), corresponding to decreases in the valence state and the occupancy of d orbitals of Cu ions.<sup>42</sup> These observations suggest that during the reduction, Cu<sup>2+</sup> migrated from the supercage to the external surface of zeolites and aggregated to form metallic Cu particles (Fig. 2c). This mitigation process can be explained by the *R*-plot EXAFS spectra (Fig. 2b, inset). Two peaks appearing at 1.7 Å and 2.2 Å were ascribed to the Cu–O and Cu–Cu bonds, respectively, arising from the coordination of Cu ions with lattice oxygen atoms in the zeolite (Cu–O) and Cu–Cu bonds in elementary Cu.<sup>43</sup> The intensity of the Cu–O peak decreased while that of the Cu–Cu peak increased upon reduction at higher temperatures, indicating that more Cu<sup>2+</sup> migrated from the cage to the external



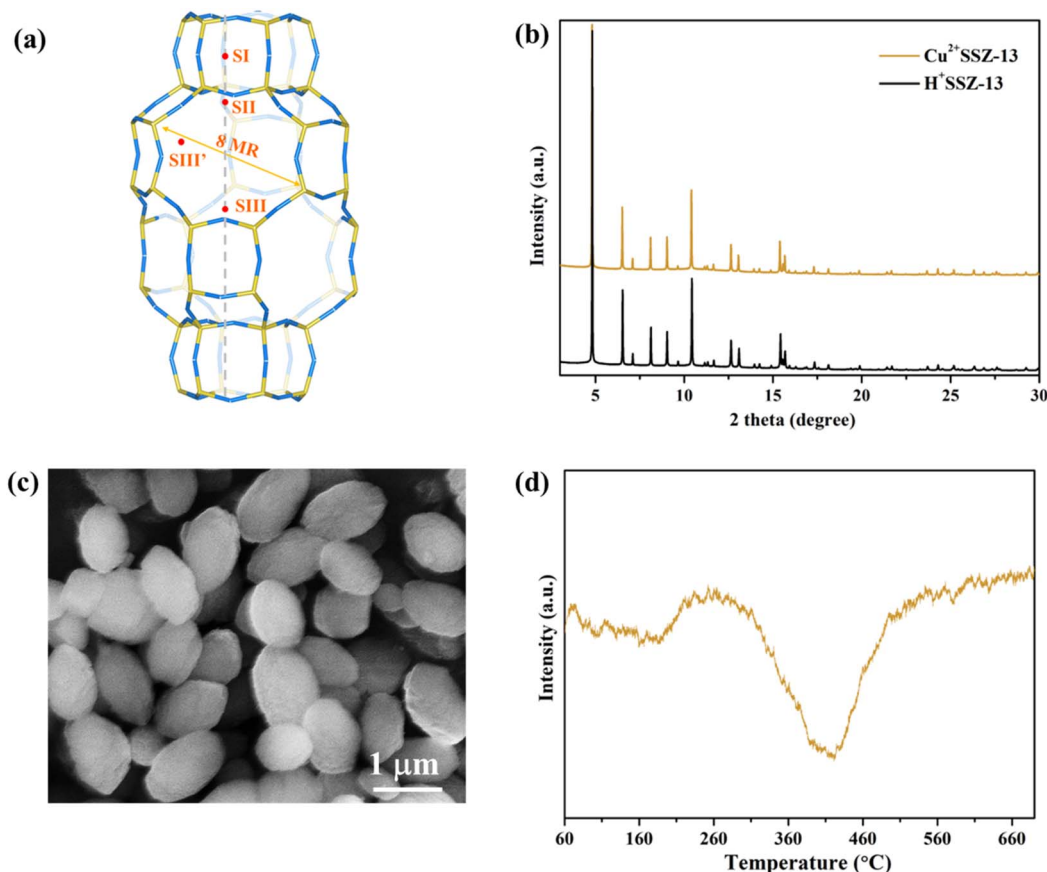


Fig. 1 (a) Illustration of the local crystal structure of chabazite (CHA) zeolites. SI–SIII' are the possible positions of extra-framework cations; (b) synchrotron powder X-ray diffraction patterns of  $\text{Cu}^{2+}\text{SSZ-13}$  and pristine  $\text{H}^+\text{SSZ-13}$  (wavelength = 0.7735 Å); (c) SEM image of  $\text{Cu}^{2+}\text{SSZ-13}$ ; and (d)  $\text{H}_2$ -TPR profile of  $\text{Cu}^{2+}\text{SSZ-13}$ .

surface of zeolites to form elementary Cu. This result is consistent with the reduced lattice parameters of  $\text{Cu}^{n+}\text{SSZ-13}$  at high reduction temperatures (Fig. 2d), which was attributed to the contraction of the zeolite lattice due to negative thermal expansion.<sup>44</sup>

It is acknowledged that the well dispersed extra-framework cations in zeolites serve as the dominant active adsorption sites for gas molecules.<sup>27,45,46</sup> Therefore, the presence of bulk  $\text{Cu}^0$  NPs on the external surface of zeolites should be minimized. Consequently, a further decrease in the reduction temperature was implemented. No characteristic peaks of elementary Cu were observed in the PXRD patterns of  $\text{Cu}^{n+}\text{SSZ-13}$  samples reduced at 100, 150, 170 and 190 °C (Fig. 3a), indicating the absence of  $\text{Cu}^0$ . The XAS results showed the changes in  $\text{Cu}^{2+}/\text{Cu}^+$  levels within zeolites (Fig. 3b). The weak absorption peak ranging between 8975 and 8980 eV is the fingerprint of  $\text{Cu}^{2+}$ , which is assigned to a dipole-forbidden  $1s \rightarrow 3d$  transition.<sup>47</sup> The characteristic peak of  $\text{Cu}^+$  was observed at 8980–8985 eV, corresponding to the  $1s \rightarrow 4p$  transition.<sup>48</sup> As the reduction temperature increased, the  $\text{Cu}^{2+}$  peak at 8978 eV diminished, while the  $\text{Cu}^+$  peak at 8984 eV gradually increased, suggesting that a higher reduction temperature facilitated the conversion of  $\text{Cu}^{2+}$  to  $\text{Cu}^+$ . The edge peak at 8993–8997 eV, known as the 'white line' of  $\text{Cu}^{2+}$ , indicates a higher oxidation

state when the peak intensity is greater.<sup>48</sup> As the reduction temperature increased, the intensity of the white line decreased, further suggesting a transformation of  $\text{Cu}^{2+}$  to  $\text{Cu}^+$ .

### 3.2 $\text{NO}_2$ adsorption

The  $\text{NO}_2$  adsorption performance of  $\text{Cu}^{n+}\text{SSZ-13}$  reduced at different temperatures (*i.e.*, 100, 150, 170, and 190 °C) was validated by  $\text{NO}_2$  dynamic adsorption at room temperature (Fig. 4a). Prior to  $\text{NO}_2$  adsorption, the adsorbents were activated at 300 °C under Ar to remove the pre-adsorbed impurities. The  $\text{NO}_2$  adsorption capacity of the  $\text{Cu}^{n+}\text{SSZ-13}$  samples increased with the increasing reduction temperature (Fig. 4b), which is attributed to a higher proportion of  $\text{Cu}^+$  being present at a higher reduction temperature. The linear correlation between the  $\text{NO}_2$  capacity and the reduction temperature encouraged us to tentatively raise the reduction temperature to 250 °C, intending to further improve the  $\text{NO}_2$  adsorption capacity. However, the  $\text{NO}_2$  adsorption over  $\text{Cu}^{n+}\text{SSZ-13-250-R}$  was found to be even lower than that of the unreduced sample ( $\text{Cu}^{2+}\text{SSZ-13}$ ). This result was caused by the formation of  $\text{Cu}^0$  particles on the external surface of the zeolite (see the SEM image in Fig. S3†), which reduced the number of accessible active adsorption sites for  $\text{NO}_2$  molecules. The highest  $\text{NO}_2$  adsorption





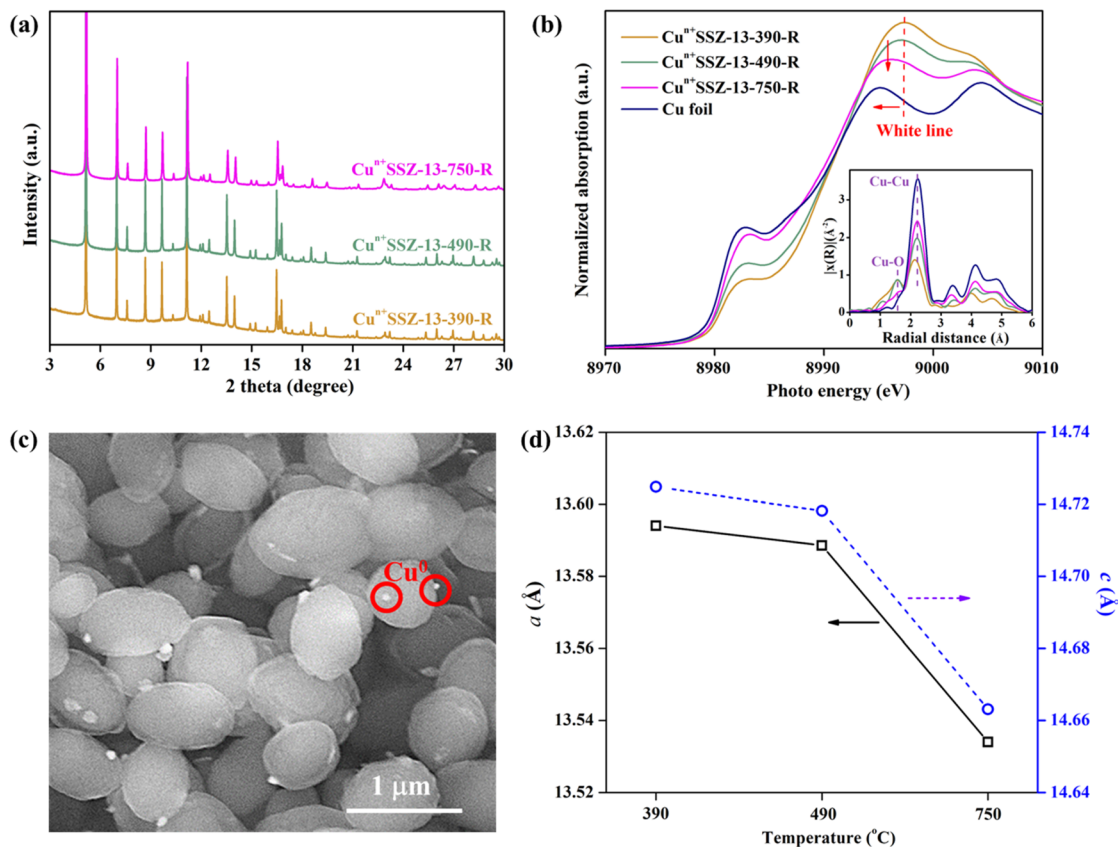


Fig. 2 (a) PXRD patterns (wavelength: 0.8275 Å) and (b) Cu K-edge XAS spectra of Cu<sup>n+</sup>SSZ-13 reduced by H<sub>2</sub> at 390, 490, and 750 °C (inset: Fourier transformed EXAFS modulation with phase correction in the *k*-range of 3.0–12.5 Å<sup>-1</sup>, *k*<sup>2</sup>-weighted); (c) SEM image of Cu<sup>n+</sup>SSZ-13-390-R; and (d) variation of unit cell parameters (*a* and *c*) of Cu<sup>n+</sup>SSZ-13 in relation to the H<sub>2</sub>-reduction temperature.

capacity, achieved by Cu<sup>n+</sup>SSZ-13-190-R, was 1.79 mmol g<sup>-1</sup> (Fig. 4b). This capacity demonstrated a significant increase of 19.4% and 52.3% with respect to that of Cu<sup>2+</sup>SSZ-13 and pristine H<sup>+</sup>SSZ-13, respectively, substantially surpassing the performance of the reported metal-modified zeolites (Table S1<sup>†</sup>). The above results clearly show that the H<sub>2</sub> reduction of Cu<sup>2+</sup>SSZ-13 effectively improves the NO<sub>2</sub> adsorption capacity, which is attributed to the increased affinity of binding sites for NO<sub>2</sub>.

To assess the impact of NO<sub>2</sub> adsorption on the specific surface area and pore volume of the Cu-modified zeolite, N<sub>2</sub> adsorption-desorption isotherms were recorded for Cu<sup>n+</sup>SSZ-13-190-R before and after NO<sub>2</sub> dynamic adsorption (Fig. 4c, d and Table S2<sup>†</sup>). Post-adsorption, the BET surface area of Cu<sup>n+</sup>SSZ-13-190-R remained largely unchanged, while the pore volume slightly increased from 0.34 to 0.40 cm<sup>3</sup> g<sup>-1</sup> which was probably due to the formation of additional interparticle

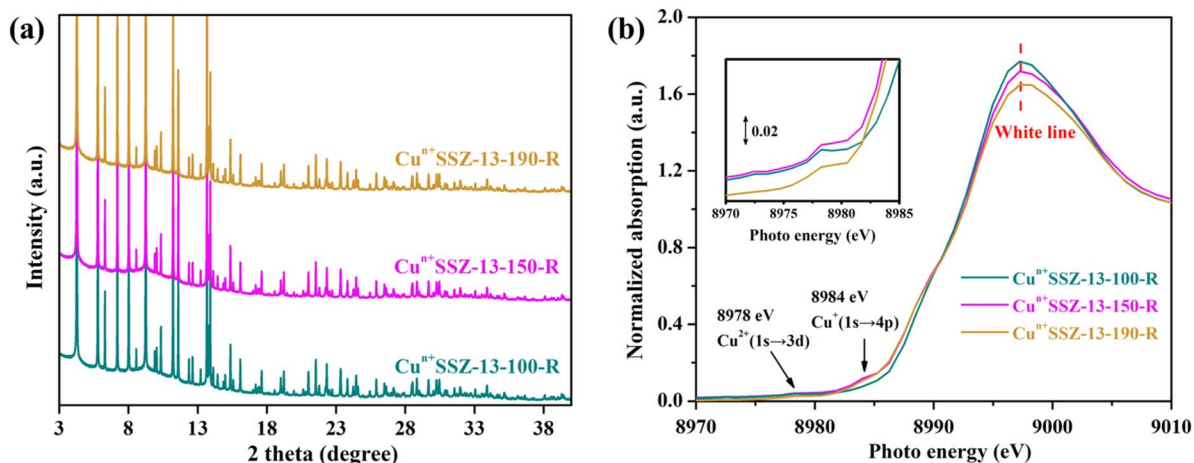


Fig. 3 (a) PXRD patterns (wavelength of 0.6880 Å) and (b) Cu K-edge XAS of Cu<sup>n+</sup>SSZ-13 reduced by H<sub>2</sub> at 100, 150, 170 and 190 °C.



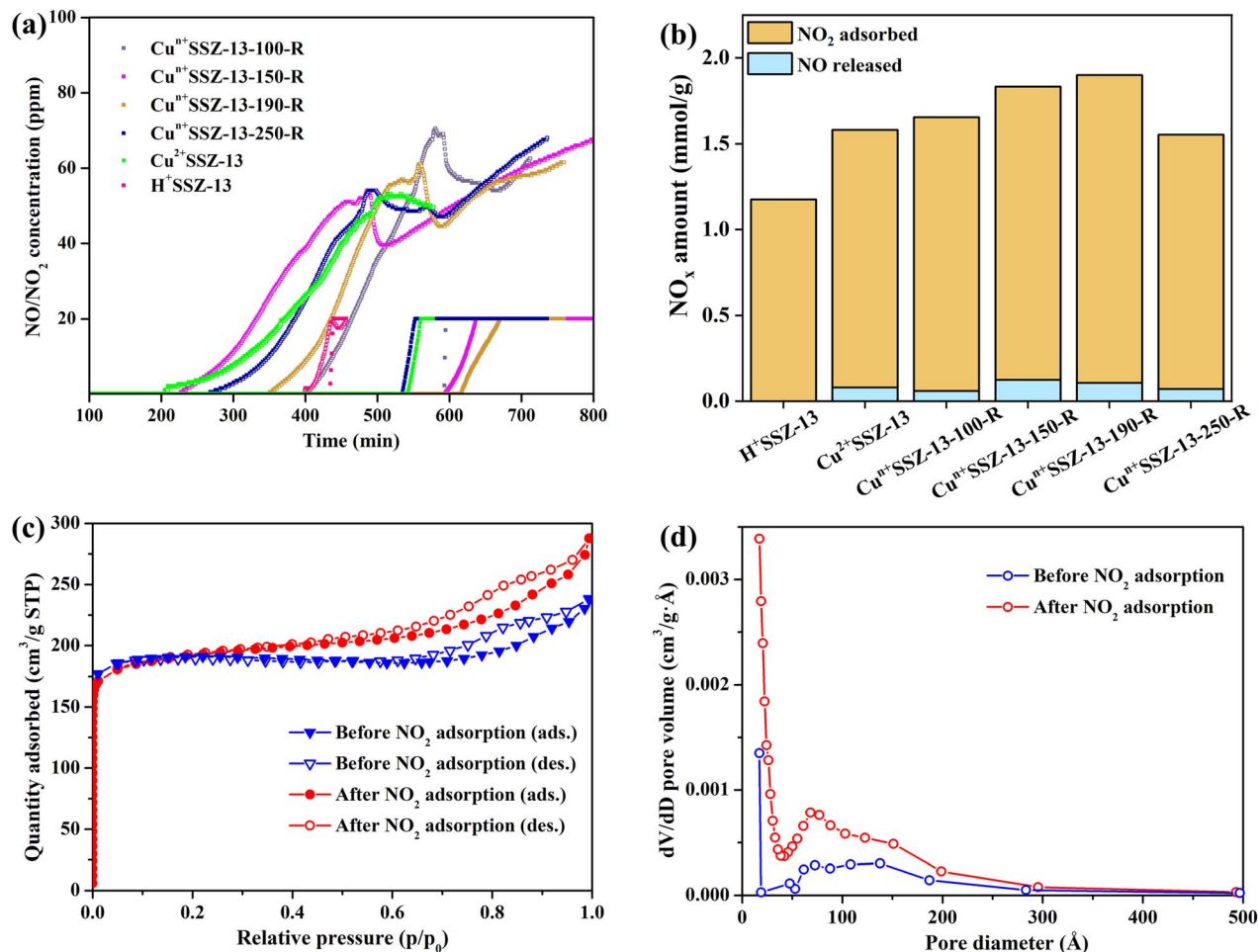
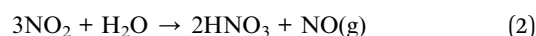
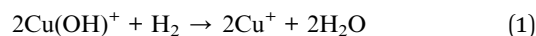


Fig. 4 (a)  $\text{NO}_2$  (1000 ppm) dynamic column adsorption at room temperature on  $\text{H}^+$ SSZ-13,  $\text{Cu}^{2+}$ SSZ-13 and  $\text{Cu}^{n+}$ SSZ-13 samples with thermal activation. The hollow ( $\square$ ) and solid ( $\blacksquare$ ) dots represent the concentration of NO and  $\text{NO}_2$ , respectively. (b) The corresponding  $\text{NO}_2$  adsorption capacity and NO released amount. (c)  $\text{N}_2$  adsorption–desorption isotherms ( $-196^\circ\text{C}$ ) and (d) pore size distributions of  $\text{Cu}^{n+}$ SSZ-13-190-R before and after  $\text{NO}_2$  (1000 ppm) dynamic column adsorption.

stacking pores. Therefore, the porous structures of  $\text{Cu}^{n+}$ SSZ-13-190-R remained largely unaffected after a cycle of  $\text{NO}_2$  dynamic adsorption. It is anticipated that the lifespan and adsorption capacity of  $\text{Cu}^{n+}$ SSZ-13-190-R can be substantially preserved by regenerating it through a gentle heating process to drive off adsorbed water and  $\text{NO}_2$ . Furthermore, in comparison with  $\text{H}^+$ SSZ-13 without Cu modification, which featured micropores with a Brunauer–Emmett–Teller (BET) surface area of  $771.69\text{ m}^2\text{ g}^{-1}$  and a pore volume of  $0.38\text{ cm}^3\text{ g}^{-1}$  (Fig. S4†),  $\text{Cu}^{n+}$ SSZ-13-190-R exhibited a micro-mesoporous structure with a reduced surface area ( $557.97\text{ m}^2\text{ g}^{-1}$ ) and pore volume ( $0.34\text{ cm}^3\text{ g}^{-1}$ ). Despite the larger surface area and pore volume of the unmodified  $\text{H}^+$ SSZ-13, the Cu-modified  $\text{Cu}^{n+}$ SSZ-13-190-R demonstrated a higher  $\text{NO}_2$  adsorption capacity. This finding suggests that the incorporation of Cu into the SSZ-13 zeolite significantly enhances the  $\text{NO}_2$  adsorption process, playing a more important role than the surface area and pore volume. Therefore, while surface area and pore volume are important factors in adsorption processes, the unique role of Cu within the SSZ-13 zeolite is the key determinant for the improved  $\text{NO}_2$  removal performance.

To evaluate the effect of moisture on  $\text{NO}_2$  adsorption, experiments were conducted on non-activated  $\text{Cu}^{n+}$ SSZ-13 samples (*i.e.*, without thermal treatment prior to  $\text{NO}_2$  adsorption). Compared with  $\text{Cu}^{2+}$ SSZ-13, the non-activated  $\text{Cu}^{n+}$ SSZ-13 samples showed a decreased  $\text{NO}_2$  capacity and an increased release of NO (Fig. S5†). The decline in capacity was due to the presence of moisture within zeolites generated during the  $\text{H}_2$  reduction process (eqn (1)). Such moisture would poison the active adsorption sites (Cu ions) by forming Cu hydrates and blocking sites intended for  $\text{NO}_2$  adsorption, thereby reducing the  $\text{NO}_2$  capacity. FTIR analysis (Fig. S6†) suggested that the moisture could facilitate  $\text{NO}_2$  transformation into  $\text{NO}_3^-$  and gaseous NO (eqn (2)).<sup>49</sup> After a certain time, the amount of released NO decreased, and the NO release curves stabilized, suggesting the moisture was gradually consumed by  $\text{NO}_2$ . Therefore, the thermal activation process is essential to mitigate the negative effects of moisture on  $\text{NO}_2$  adsorption.



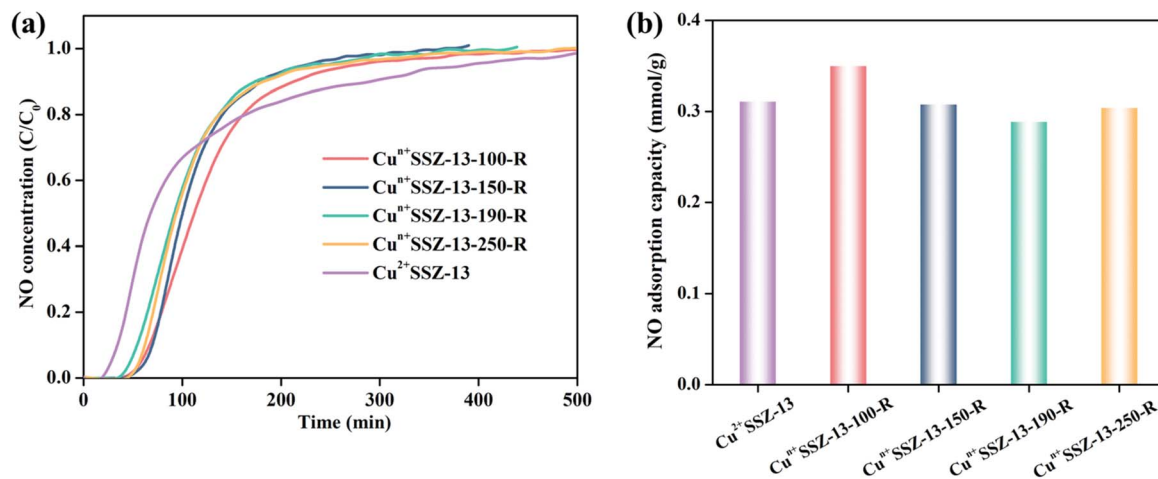


Fig. 5 (a) NO (1000 ppm) dynamic adsorption on  $\text{Cu}^{2+}\text{SSZ-13}$  samples at room temperature; and (b) the corresponding NO adsorption capacity.

In addition to improving  $\text{NO}_2$  capacity, moisture removal also contributed to the decrease of NO release, which was evident from the longer NO retention time and the more gradual slopes of NO release curves (Fig. 4a). However, the correlation between the amount of NO released and the reduction temperature was inconsistent, which resulted from the different NO retention abilities of the samples. For example,  $\text{Cu}^{2+}\text{SSZ-13-100-R}$  showed the highest NO adsorption capacity (Fig. 5), aligning with the lowest amount of NO released (Fig. 4b). The NO adsorption capacity decreased with the increasing reduction temperature from 100 to 190 °C, while it

increased when the reduction temperature was further raised to 250 °C.

Our  $\text{Cu}^{2+}\text{SSZ-13}$  adsorbent, which exhibits an enhanced capacity for ambient  $\text{NO}_2$  abatement yet sensitivity to moisture, can be effectively used for the reduction of  $\text{NO}_2$  emission from the engine pipeline when combined with desiccant materials or condensation systems that remove moisture from the exhaust gas. Additionally, our zeolite can be used in air purifiers or industrial settings to remove  $\text{NO}_2$ , incorporating moisture control mechanisms such as heating elements or moisture-absorbing materials. Given the well-preserved specific surface area and pore volume after  $\text{NO}_2$  adsorption, as evidenced by

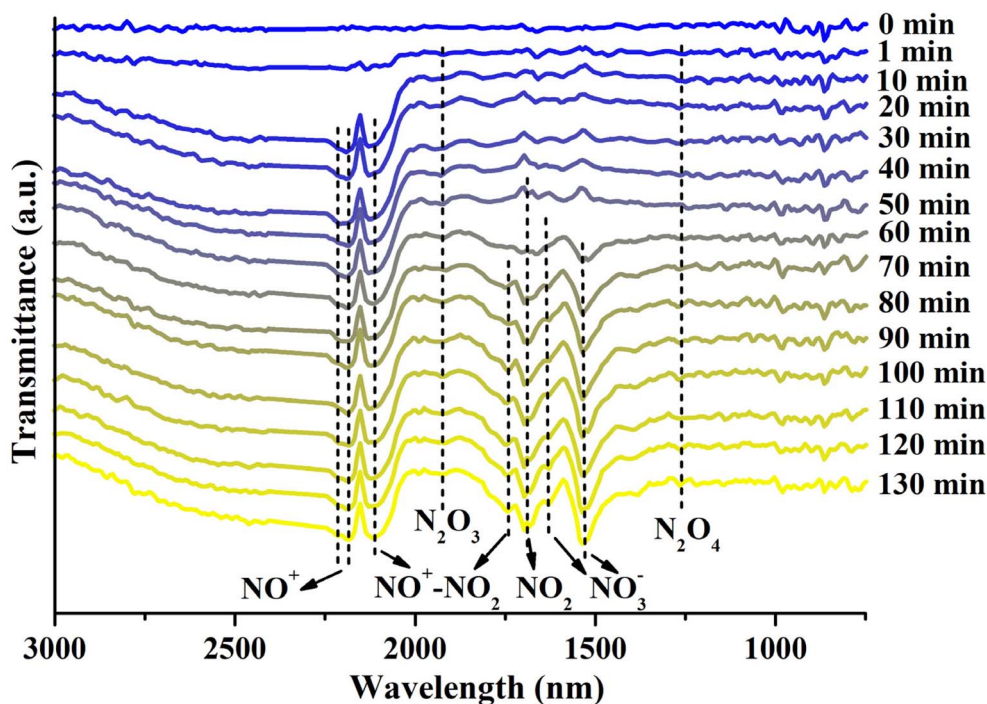


Fig. 6 *In situ* FTIR spectra of  $\text{Cu}^{2+}\text{SSZ-13-190-R}$  during  $\text{NO}_2$  adsorption, with the background of the fresh sample subtracted (conditions:  $\text{NO}_2$  concentration of 1000 ppm, flow rate of  $60 \text{ mL min}^{-1}$ , 25 °C).



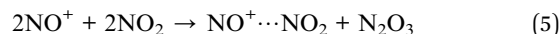
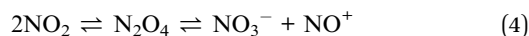
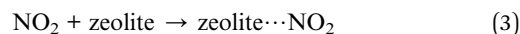


porous property analysis, the Cu<sup>n+</sup>SSZ-13-190-R adsorbent is expected to maintain its performance over multiple cycles of adsorption and thermal regeneration, thereby ensuring a long lifespan in the aforementioned practical applications.

### 3.3 Discussion of the mechanism

To elucidate the mechanism of NO<sub>2</sub> adsorption on our Cu-modified zeolite, *in situ* FTIR analysis of the Cu<sup>n+</sup>SSZ-13-190-R zeolite during the NO<sub>2</sub> adsorption process was carried out (Fig. 6). The FTIR spectra revealed the presence of adsorbed NO<sub>2</sub> at 1690 cm<sup>-1</sup>,<sup>50</sup> which tended to form an N<sub>2</sub>O<sub>4</sub> dimer (1261 cm<sup>-1</sup>)<sup>51</sup> in small-pore zeolites due to the confinement effect.<sup>45</sup> The adsorbed N<sub>2</sub>O<sub>4</sub> can undergo ionization in the zeolite to form NO<sub>3</sub><sup>-</sup> and NO<sup>+</sup>.<sup>52,53</sup> As anticipated, the formation of nitrites was observed, including bridging NO<sub>3</sub><sup>-</sup> (1630 cm<sup>-1</sup>) and monodentate NO<sub>3</sub><sup>-</sup> (1534 cm<sup>-1</sup>).<sup>54,55</sup> Meanwhile, the asymmetric band at around 2178 cm<sup>-1</sup>, corresponding to two NO<sup>+</sup> stretches at 2214 and 2178 cm<sup>-1</sup>, is indicative of the generation of NO<sup>+</sup> intermediates,<sup>56</sup> which can serve as an adsorption site for NO<sub>2</sub>.<sup>45</sup> The formation of NO<sup>+</sup>-NO<sub>2</sub> complexes was confirmed by the presence of an N-O stretch at 1741 cm<sup>-1</sup> accompanied by another NO stretch at 2109 cm<sup>-1</sup>,<sup>56</sup> as well as a weak band at 1925 cm<sup>-1</sup> assigned to N<sub>2</sub>O<sub>3</sub>,<sup>54</sup> a product of NO<sub>2</sub>

adsorption on NO<sup>+</sup>.<sup>57</sup> Although a small amount of NO was released during NO<sub>2</sub> adsorption due to NO<sub>2</sub> dissociation caused by oxygen vacancies, no distinct FTIR peaks indicative of adsorbed NO were observed. Based on these findings, the mechanism for NO<sub>2</sub> adsorption on the Cu<sup>n+</sup>SSZ-13-190-R zeolite during adsorption was proposed, as shown in eqn (3)–(6).

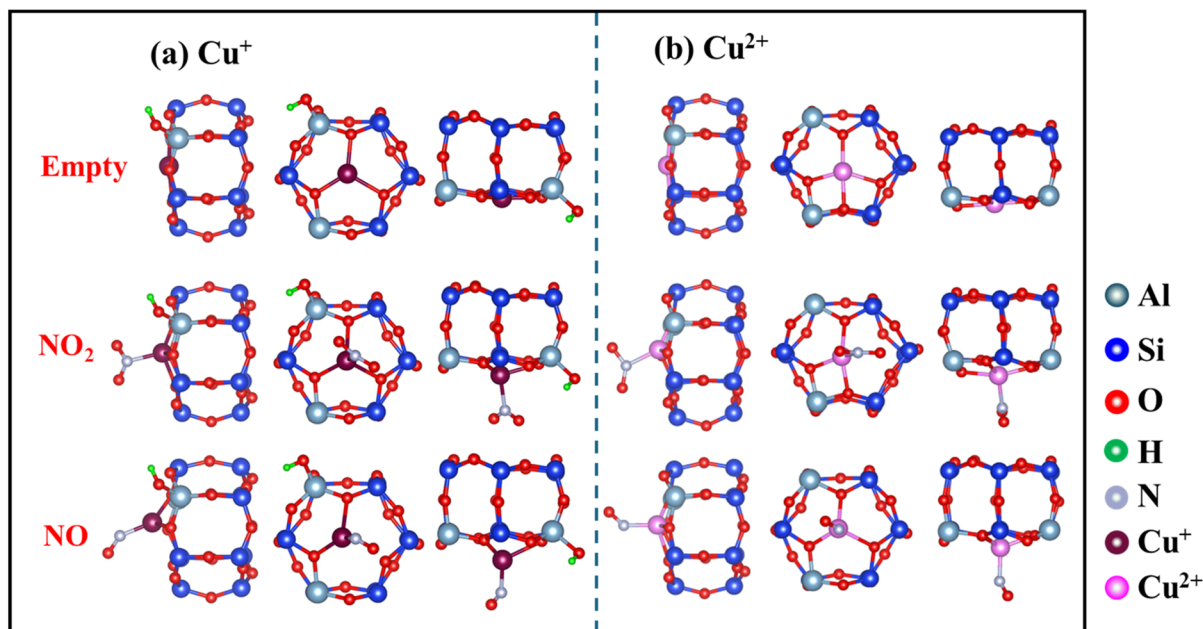


To understand the effects of copper valence states on NO<sub>2</sub> adsorption in zeolites, DFT calculations were conducted to study the electronic and structural changes associated with Cu<sup>+</sup> and Cu<sup>2+</sup> ions upon NO<sub>2</sub> adsorption. As shown in Fig. S7,† the number of cations (Cu<sup>+</sup> and H<sup>+</sup>) in the zeolite after H<sub>2</sub> reduction is increased. As the cations would serve as major adsorption sites, the increase in cation density would afford more binding sites for NO<sub>2</sub> adsorption. Moreover, as shown in Table 1, the formation of Cu<sup>+</sup> (binding energy of 20.06 kcal mol<sup>-1</sup>), which has a higher affinity for NO<sub>2</sub> than Cu<sup>2+</sup> (binding energy of 14.36 kcal mol<sup>-1</sup>), strengthens the interaction with NO<sub>2</sub> through π-complexation. Thus, the increase in the density of adsorption sites with increasing binding strength enables greater NO<sub>2</sub> uptake.

The optimized local structures of NO<sub>2</sub>/NO adsorbed on Cu<sup>+</sup> and Cu<sup>2+</sup> in SSZ-13 zeolites were analyzed (Fig. 7). When NO<sub>2</sub> or NO is adsorbed, Cu–O bonds are partially disrupted, and the

**Table 1** The binding energy (kcal mol<sup>-1</sup>) of NO<sub>2</sub> and NO molecules upon adsorption on Cu<sup>+</sup> and Cu<sup>2+</sup> in the SSZ-13 zeolite calculated by density functional theory (DFT)

	NO <sub>2</sub>	NO
Cu <sup>+</sup>	-20.06	-30.31
Cu <sup>2+</sup>	-14.36	-30.78



**Fig. 7** Comparison of optimized local structures of NO<sub>2</sub>/NO adsorbed on Cu<sup>+</sup> and Cu<sup>2+</sup> cations in the SSZ-13 zeolite. The top, middle, and bottom images respectively depict the naked cation, and the cation interacting with NO<sub>2</sub> and NO, all located at the 6 MR sites.







## References

- Z. Chen, J.-N. Wang, G.-X. Ma and Y.-S. Zhang, *Lancet*, 2013, **382**, 1959.
- V. L. Feigin, G. A. Roth, M. Naghavi, P. Parmar, R. Krishnamurthi, S. Chugh, G. A. Mensah, B. Norrving, I. Shiue and M. Ng, *Lancet Neurol.*, 2016, **15**, 913–924.
- P. M. Edwards, S. S. Brown, J. M. Roberts, R. Ahmadov, R. M. Banta, J. A. Degouw, W. P. Dube, R. A. Field, J. H. Flynn and J. B. Gilman, *Nature*, 2014, **514**, 351–354.
- P. Georgopoulos, S. Arunachalam and S. Wang, *J. Air Waste Manage. Assoc.*, 1997, **47**, 838–850.
- D. Pudasainee, B. Sapkota, M. L. Shrestha, A. Kaga, A. Kondo and Y. Inoue, *Atmos. Environ.*, 2006, **40**, 8081–8087.
- M. Shao, Y. Zhang, L. Zeng, X. Tang, J. Zhang, L. Zhong and B. Wang, *J. Environ. Manage.*, 2009, **90**, 512–518.
- G. B. Marks, W. Ezz, N. Aust, B. G. Toelle, W. Xuan, E. Belousova, C. Cosgrove, B. Jalaludin and W. T. Smith, *Environ. Health Perspect.*, 2010, **118**, 1476–1482.
- R. Pastel and R. Sausa, *Appl. Opt.*, 1996, **35**, 4046–4052.
- The Government of the Hong Kong Special Administrative Region - Press Releases, *EPD announces air quality monitoring results in 2019, 2020*, <https://www.info.gov.hk/gia/general/202001/20/P2020012000874.htm>.
- Z. Hu, Z. Shen and J. C. Yu, *Environ. Sci. Technol.*, 2017, **51**, 7076–7083.
- J. W. Girard, C. Montreuil, J. Kim, G. Cavataio and C. Lambert, *SAE Int. J. Fuels Lubr.*, 2009, **1**, 488–494.
- C. Lambert, R. Hammerle, R. McGill, M. Khair and C. Sharp, *SAE Trans.*, 2004, 580–589.
- L. Muzio, G. Quartucy and J. Cichanowicz, *Int. J. Environ. Pollut.*, 2002, **17**, 4–30.
- V. Schmeisser, M. Weibel, L. S. Hernando, I. Nova, E. Tronconi and M. P. Ruggeri, *SAE Int. J. Commer. Veh.*, 2013, **6**, 190–199.
- H.-Y. Chen, J. E. Collier, D. Liu, L. Mantarosie, D. Durán-Martín, V. Novák, R. R. Rajaram and D. Thompsett, *Catal. Lett.*, 2016, **146**, 1706–1711.
- C. Wan and J. Li, *Carbohydr. Polym.*, 2015, **134**, 144–150.
- Y. Zheng, L. Kovarik, M. H. Engelhard, Y. Wang, Y. Wang, F. Gao and J. n. Szanyi, *J. Phys. Chem. C*, 2017, **121**, 15793–15803.
- R. T. Yang, *Adsorbents: Fundamentals and Applications*, John Wiley & Sons, 2003.
- A. Takahashi, R. T. Yang, C. L. Munson and D. Chinn, *Langmuir*, 2001, **17**, 8405–8413.
- M. Sun, A. Hanif, T. Wang, Q. Gu and J. Shang, *Sep. Purif. Technol.*, 2023, **314**, 123563.
- Y. Tian, M. Kong, Z. Tao, C. Yang, S. Shang, Q. Gu, D. C. Tsang, L. Li and J. Shang, *J. Hazard. Mater.*, 2023, **441**, 129962.
- M. Sun, A. Hanif, T. Wang, C. Yang, D. C. Tsang and J. Shang, *J. Hazard. Mater.*, 2021, **418**, 126400.
- S. Shang, C. Yang, Y. Tian, Z. Tao, A. Hanif, M. Sun, H. H. S. Wong, C. Wang and J. Shang, *ACS ES&T Eng.*, 2020, **1**, 375–384.
- S. Shang, C. Yang, C. Wang, J. Qin, Y. Li, Q. Gu and J. Shang, *Angew. Chem., Int. Ed.*, 2020, **59**, 19680–19683.
- B. Levasseur, A. M. Ebrahim and T. J. Bandoz, *J. Colloid Interface Sci.*, 2012, **377**, 347–354.
- M. Sun, Q. Gu, A. Hanif, T. Wang and J. Shang, *Chem. Eng. J.*, 2019, **370**, 1450–1458.
- L. Rodriguez-Santiago, M. Sierka, V. Branchadell, M. Sodupe and J. Sauer, *J. Am. Chem. Soc.*, 1998, **120**, 1545–1551.
- A. Sierraalta, R. Añez and M.-R. Brussini, *J. Phys. Chem. A*, 2002, **106**, 6851–6856.
- S. Onitsuka, M. Ichiki and T. Watanabe, *US Pat.*, 5158582, 1992.
- D. Barthomeuf and B.-H. Ha, *J. Chem. Soc., Faraday Trans. 1*, 1973, **69**, 2158–2165.
- J. Yun and R. Lobo, *Catal. Sci. Technol.*, 2015, **5**, 264–273.
- P. Hohenberg and W. Kohn, *Phys. Rev.*, 1964, **136**, B864–B871.
- W. Kohn and L. J. Sham, *Phys. Rev.*, 1965, **140**, A1133–A1138.
- P. Giannozzi, O. Andreussi, T. Brumme, O. Bunau, M. B. Nardelli, M. Calandra, R. Car, C. Cavazzoni, D. Ceresoli, M. Cococcioni, N. Colonna, I. Carnimeo, A. D. Corso, S. d. Gironcoli, P. Delugas, J. R. A. DiStasio, A. Ferretti, A. Floris, G. Fratesi, G. Fugallo, R. Gebauer, U. Gerstmann, F. Giustino, T. Gorni, J. Jia, M. Kawamura, H. Y. Ko, A. Kokalj, E. Küçükbenli, M. Lazzeri, M. Marsili, N. Marzari, F. Mauri, N. L. Nguyen, H. V. Nguyen, A. Otero-de-la-Roza, L. Paulatto, S. Poncé, D. Rocca, R. Sabatini, B. Santra, M. Schlipf, A. P. Seitsonen, A. Smogunov, I. Timrov, T. Thonhauser, P. Umari, N. Vast, X. Wu and S. Baroni, *J. Phys.: Condens. Matter*, 2017, **29**, 465901.
- G. Paolo, B. Stefano, B. Nicola, C. Matteo, C. Roberto, C. Carlo, C. Davide, L. C. Guido, C. Matteo, D. Ismaila, C. Andrea Dal, G. Stefano de, F. Stefano, F. Guido, G. Ralph, G. Uwe, G. Christos, K. Anton, L. Michele, M.-S. Layla, M. Nicola, M. Francesco, M. Riccardo, P. Stefano, P. Alfredo, P. Lorenzo, S. Carlo, S. Sandro, S. Gabriele, P. S. Ari, S. Alexander, U. Paolo and M. W. Renata, *J. Phys.: Condens. Matter*, 2009, **21**, 395502.
- J. P. Perdew, K. Burke and M. Ernzerhof, *Phys. Rev. Lett.*, 1996, **77**, 3865–3868.
- S. Grimme, *J. Comput. Chem.*, 2006, **27**, 1787–1799.
- R. Zhang, J.-S. McEwen, M. r. Kollár, F. Gao, Y. Wang, J. Szanyi and C. H. Peden, *ACS Catal.*, 2014, **4**, 4093–4105.
- Q. Guo, F. Fan, D. Lighthart, G. Li, Z. Feng, E. J. Hensen and C. Li, *ChemCatChem*, 2014, **6**, 634–639.
- A. G. Greenaway, I. Lezcano-Gonzalez, M. Agote-Aran, E. K. Gibson, Y. Odarchenko and A. M. Beale, *Top. Catal.*, 2018, **61**, 175–182.
- J. H. Kwak, H. Zhu, J. H. Lee, C. H. Peden and J. Szanyi, *Chem. Commun.*, 2012, **48**, 4758–4760.
- G. Yalovega, V. Shmatko, A. Funik and M. Brzhezinskaya, *Adv. Mater.*, 2016, 299–315.
- T. N. Huan, E. S. Andreiadis, J. Heidkamp, P. Simon, E. Derat, S. Cobo, G. Royal, A. Bergmann, P. Strasser and H. Dau, *J. Mater. Chem. A*, 2015, **3**, 3901–3907.
- N. Shi, Y. Song, X. Xing and J. Chen, *Coord. Chem. Rev.*, 2021, **449**, 214204.



- 45 M. Sun, C. Ku, Z. Tao, T. Wang, C. Wen, A. Hanif, C. Wang, Q. Gu, P. Sit and J. Shang, *Results Eng.*, 2023, **18**, 101134.
- 46 C. Bian, D. Li, Q. Liu, S. Zhang, L. Pang, Z. Luo, Y. Guo, Z. Chen and T. Li, *Chin. Chem. Lett.*, 2022, **33**, 1169–1179.
- 47 R. C. Ambrosio and E. A. Ticianelli, *J. Electroanal. Chem.*, 2005, **574**, 251–260.
- 48 W. C. Gomes, A. d. O. W. Neto, P. M. Pimentel, D. M. de Araújo Melo and F. R. G. Silva, *Colloids Surf., A*, 2013, **426**, 18–25.
- 49 F. Delachaux, C. Vallières, H. Monnier and M.-T. Lecler, *Adsorption*, 2019, **25**, 95–103.
- 50 U. Bentrup, M. Richter and R. Fricke, *Appl. Catal., B*, 2005, **55**, 213–220.
- 51 A. Mahmood, X. Wang, X. Xie and J. Sun, *Colloids Surf., A*, 2021, **626**, 127058.
- 52 Z.-M. Wang, T. Arai and M. Kumagai, *Ind. Eng. Chem. Res.*, 2001, **40**, 1864–1871.
- 53 C. Sedlmair, B. Gil, K. Seshan, A. Jentys and J. A. Lercher, *Phys. Chem. Chem. Phys.*, 2003, **5**, 1897–1905.
- 54 M. Kantcheva and E. Z. Ciftlikli, *J. Phys. Chem. B*, 2002, **106**, 3941–3949.
- 55 K. Hadjiivanov, V. Avreyska, D. Klissurski and T. Marinova, *Langmuir*, 2002, **18**, 1619–1625.
- 56 K. Khivantsev, N. R. Jaegers, H. A. Aleksandrov, L. Kovarik, M. A. Derewinski, Y. Wang, G. N. Vayssilov and J. Szanyi, *Nat. Commun.*, 2021, **12**, 6033.
- 57 K. I. Hadjiivanov, *Catal. Rev.*, 2000, **42**, 71–144.

