

## PAPER

[View Article Online](#)  
[View Journal](#) | [View Issue](#)Cite this: *Energy Adv.*, 2024,  
3, 1653

## Intrinsic effects of electrolytes on lithium metal deposition and dissolution investigated through a separator-free cell†

Tomoki Takahashi,‡ Di Wang, ‡ Jinkwang Hwang \* and  
Kazuhiko Matsumoto \*

Lithium metal batteries are a significant promise for next-generation energy storage due to their high energy density. However, challenges persist in their commercialization stemming from issues during the lithium deposition/dissolution processes, such as low Coulombic efficiency, dendrite formation, and dead-lithium formation. Addressing these challenges requires careful electrolyte design to enhance the reversibility of the lithium metal negative electrode by modifying solvation structures and engineering interfaces. The Coulombic efficiency of lithium deposition/dissolution is one of the most crucial factors in evaluating the performance of electrolytes toward lithium metal, although this is influenced by various factors. In this study, a separator-free cell is adopted to minimize extraneous influences and focus on assessing the intrinsic effects of electrolytes on lithium deposition/dissolution. 48 different electrolytes based on three salts of Li[PF<sub>6</sub>], Li[FSA] and Li[TFSA] varying in solvents were investigated with or without additives. Moreover, Raman spectroscopy and X-ray photon spectroscopy enhance the discussion by revealing variations in the major species of solid electrolyte interphase components under different electrolyte conditions.

Received 17th April 2024,  
Accepted 29th May 2024

DOI: 10.1039/d4ya00245h

[rsc.li/energy-advances](https://rsc.li/energy-advances)

## 1 Introduction

Lithium-ion batteries (LIBs) have gained widespread popularity due to their long lifespan.<sup>1</sup> Over the past three decades, their performance has significantly increased.<sup>2,3</sup> However, the energy density of LIBs based on intercalation electrode materials is gradually approaching its theoretical limit, which fails to meet the increasing demands for higher energy densities in energy storage systems.<sup>4,5</sup> Specifically, a target of 500 W h kg<sup>−1</sup> has been set for next-generation secondary batteries, while conventional LIBs usually offer energy densities below 300 W h kg<sup>−1</sup> (based on a LIB including active materials and cell-housing components).<sup>6–8</sup> In response to this challenge, lithium metal batteries (LMBs), which employ lithium metal as the negative electrode material, have been attracting attention as the next-generation batteries to fulfill these demands.<sup>9–11</sup> The use of lithium metal negative electrode is particularly promising, offering the lowest standard reduction potential (−3.04 V vs.

SHE), which results in higher working voltages than any other negative electrodes, and a theoretical capacity that is about ten times higher than that of graphite (3860 mA h g<sup>−1</sup> vs. 340 mA h g<sup>−1</sup> based on the charged state). Furthermore, the study on lithium metal negative electrode is expanding beyond current positive electrode materials to explore conversion-type positive electrode materials, such as in lithium–sulfur (Li–S) batteries and lithium–air (Li–air) batteries.<sup>12</sup>

Despite the promising features of lithium metal negative electrodes, they face several challenges that limit their practical application in secondary batteries, one of which is the poor reversibility of lithium deposition/dissolution processes.<sup>13,14</sup> Firstly, uneven lithium ion flux and surface defects can lead to dendritic lithium metal growth, worsening with cycling and increasing the risk of short circuits and fires due to potential piercing of the separator and contact with the cathode. Secondly, the high reactivity of lithium metal with the electrolyte leads to irreversible side reactions and the formation of solid electrolyte interphase (SEI). A robust and effective SEI can prevent further side reactions, while organic-dominated SEI with low ionic conductivity (for example, derived from commonly used carbonate electrolytes) degrades metal electrode performance. Furthermore, lithium deposition/dissolution accompanies significant volume changes and internal structure destruction, potentially damaging the existing SEI and leading to continuous

Graduate School of Energy Science, Kyoto University, Yoshida-honmachi, Sakyo-ku,  
Kyoto 606-8501, Japan. E-mail: [matsumoto.kazuhiko.4c@kyoto-u.ac.jp](mailto:matsumoto.kazuhiko.4c@kyoto-u.ac.jp),  
[hwang.jinkwang.5c@kyoto-u.ac.jp](mailto:hwang.jinkwang.5c@kyoto-u.ac.jp)

† Electronic supplementary information (ESI) available: Detailed material preparation, physical and chemical data, additional electrochemical measurement data and results. See DOI: <https://doi.org/10.1039/d4ya00245h>

‡ Equal contribution.

consumption of the freshly exposed lithium metal and electrolyte. This process also led to the formation of inactive lithium, known as “dead lithium”, causing capacity loss. It is crucial to highlight that the mechanical properties of the SEI are highly dependent on a balanced composition. An optimal SEI should consist of a robust inorganic inner layer to improve reversibility and a flexible organic outer layer to accommodate the volumetric changes during cycling. These issues not only consume a large amount of electrolyte and active lithium but also increase battery impedance, leading to severe capacity degradation.<sup>15</sup> To solve these problems, several strategies have been proposed focusing on electrolyte engineering,<sup>16–19</sup> the formation of artificial SEI and interface modification,<sup>20–22</sup> utilizing the three-dimensional structure of current collectors,<sup>23,24</sup> and modifying separators.<sup>25,26</sup>

Among these strategies, electrolyte engineering stands out as an effective and facile method for enhancing battery performance and longevity.<sup>27,28</sup> On one hand, the use of base solvents compatible with lithium metal, such as ethers and ionic liquids, offers relatively better reduction stability and robust SEI formation capabilities, resulting in improved reversibility of lithium deposition and dissolution.<sup>18,29,30</sup> Another widely studied approach for stabilizing the SEI involves the use of additives. For example, the addition of FEC (fluoroethylene carbonate) has been reported to lead to the formation of a stable and LiF-rich SEI, effectively suppressing dendrite growth.<sup>16</sup> Moreover, the concept of high-concentration electrolytes has facilitated the accessibility of lithium metal negative electrodes, bringing the role and impact of solvation chemistry in battery electrolytes into intensive focus.<sup>31</sup> In this context, the Coulombic efficiency (CE) of lithium metal deposition and dissolution process on a current collector, typically Cu, serves as a crucial indicator of electrolyte performance.<sup>32–34</sup> However, CE measurements are susceptible to various factors, making it difficult to reproduce results even with similar cell designs and complicating the comparison across different electrolytes. For instance, in the widely used lithium–copper coin cells lab level, the reversibility of lithium metal is significantly influenced by cell components, including the porous separator and

spring,<sup>35–37</sup> conventional polyolefin-based microporous separators play an essential role in electronically insulating the positive and negative electrodes while also regulating lithium-ion transport, which is a critical factor in lithium metal deposition/dissolution. Additionally, mechanical pressure plays a significant role in determining the morphology and cycling behavior of the ductile lithium metal.

Therefore, to focus on the electrolyte properties affecting the reversibility of lithium metal, other influencing factors need to be eliminated. This study aims to obtain comprehensive data on the impact of electrolytes on the deposition and dissolution of lithium metal. So thus, herein, separator-free cells are employed as shown in Fig. 1a and b, which replace the separator with a hollow spacer with a fixed thickness of 1 mm. The hollow tube-shaped space (thickness of 1 mm, outer diameter 20 mm and inner diameter of 12 mm) is filled with the electrolyte, and the electrodes are separated by the liquid electrolyte, eliminating variability introduced by conventional separators. This setup also allows for minimizing external factors of the microporous separator and the impact of pressure on different performance evaluations. Meanwhile, commonly used lithium salts were examined, including Li[PF<sub>6</sub>], Li[FSA] (FSA<sup>−</sup> = bis(fluorosulfonyl)amide), and Li[TFSA] (TFSA<sup>−</sup> = bis(trifluoromethanesulfonyl)amide), as well as a variety of electrolyte solvents encompassing ethers, carbonates, sulfones, phosphates, and Ionic liquids. Additionally, two prevalent additives, FEC and LiNO<sub>3</sub> were selected. A total of 48 combinations have been prepared using different concentrations of lithium salts, solvents, and additives. All the electrolyte species involved are shown in Fig. 1c.

## 2. Experimental details

### 2.1 Materials

All the moisture- and air-sensitive materials were handled and prepared under a dry Ar gas atmosphere (H<sub>2</sub>O < 1 ppm and O<sub>2</sub> < 1 ppm) in a glove box (Miwa Manufacturing Co., Ltd). All the prepared electrolytes are listed in Table S1 (ESI<sup>†</sup>). Three

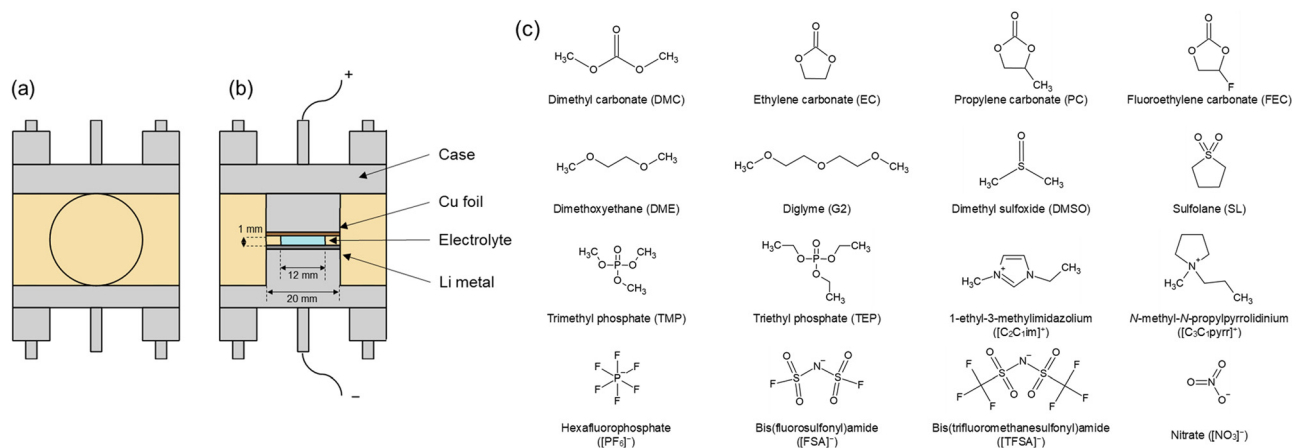


Fig. 1 Schematic illustration of a separator-free cell: (a) Front and (b) cross-sectional views. (c) Anion, cation, and solvents species comprising electrolytes involved in the investigation.



types of salts were used: Li[PF<sub>6</sub>] (Kishida Chemical, purity > 99.9%), Li[FSA] (Kishida Chemical, purity > 99.9%), and Li[TFSA] (Kishida Chemical, purity > 99.9%), and twelve types of solvents were employed (see Fig. 1c for abbreviation): SL (Kishida Chemical, purity > 99.5%), TMP (Kishida Chemical, purity > 99.0%), TEP (Kishida Chemical, purity > 99.0%), DMC (Kishida Chemical, purity > 99.5%), PC (Kishida Chemical, purity > 99.5%), EC:DMC (1:1 v/v, Kishida Chemical, purity > 99.5%), AN (Kishida Chemical, purity > 99.5%), DMSO (Kishida Chemical, purity > 99.0%), G2 (Kishida Chemical, purity > 99.0%), DME (Kishida Chemical, purity > 99.5%), [C<sub>3</sub>C<sub>1</sub>pyrr][FSA] (Kanto Chemical, purity > 99.9%), [C<sub>2</sub>C<sub>1</sub>im][FSA] (Kanto Chemical, purity > 99.9%), [C<sub>3</sub>C<sub>1</sub>pyrr][TFSA] (Kanto Chemical, purity > 99.9%), and [C<sub>2</sub>C<sub>1</sub>im][TFSA] (Kanto Chemical, purity > 99.9%). FEC (Kishida Chemical, purity > 99.5%) and LiNO<sub>3</sub> (Sigma Aldrich, purity > 99.99%) were used for additives. Li[FSA], Li[TFSA], [C<sub>3</sub>C<sub>1</sub>pyrr][FSA], [C<sub>2</sub>C<sub>1</sub>im][FSA], [C<sub>3</sub>C<sub>1</sub>pyrr][TFSA], and [C<sub>2</sub>C<sub>1</sub>im][TFSA] were vacuum-dried at 60 °C for more than 24 h.

### 2.3 Cell assembly and electrochemical measurements

A separator-free cell shown in Fig. 1a and b was employed for electrochemical measurements. The working electrode was Cu foil, and the counter electrode was lithium metal with a diameter of 20 mm. Oxides on the Cu foil surface were removed with dilute hydrochloric acid and washed with ethanol in an atmospheric environment. The cell was subsequently assembled under an Ar atmosphere. Lithium metal was cut and shaped after removing the surface oxides. A spacer was placed between the electrodes, and the interior hollow of the spacer (inner diameter: 12 mm, thickness: 1 mm) was filled with the electrolyte.

Lithium deposition/dissolution measurements were conducted using an electrochemical measurement apparatus (VSP, Bio-Logic Co). The operating temperature was maintained at 25 °C in a thermostatic chamber (SU221, ESPEC), and the tests were initiated after 3-hour rest. At a constant current density (1 mA cm<sup>-2</sup>), lithium was deposited onto the Cu foil (1 mA h cm<sup>-2</sup>), followed by the dissolution with the reversed current. The cutoff voltage was set at -0.5 V for the deposition reaction and +0.5 V for the dissolution reaction. The tests were conducted for 10 cycles.

### 2.4 Characterization

The SEI layer components were analyzed using X-ray photoelectron spectroscopy (XPS) (JEOL, JPS-9030, Mg K $\alpha$  source). The electrodes after electrochemical tests limited to one cycle were washed with PC and THF (tetrahydrofuran), and then dried under vacuum. Raman spectra were recorded on a Raman instrument (Thermo Scientific, DXR3) using the 532 nm excitation line of a diode-pumped solid-state laser.

## 3 Results and discussion

### 3.1 Cycle performance of Li metal deposition/dissolution

The lithium deposition/dissolution behavior on a Cu working electrode was scrutinized in separator-free cells for 46 different electrolytes, excluding Li[PF<sub>6</sub>] in either DME or G2 due to its

low solubility (<1 M).<sup>38</sup> Table 1 collates the first and second CEs, the average CE for overall 10 cycles, and the overpotential at 0.2 mA h cm<sup>-2</sup> during the second cycle of lithium deposition/dissolution test in the Li/Cu cell. The specific charge-discharge curves for each electrolyte are presented in Fig. S1–S3 (ESI<sup>†</sup>). In cases where the voltage fell below the cutoff or short-circuited to 0 V from the second cycle onward, preventing the same amount of lithium deposition, the CE was calculated for the preceding cycles. Otherwise, the CE was calculated for each cycle based on the ratio of the quantities of electricity during deposition (1 mA h cm<sup>-2</sup>) and dissolution.

The performance of the investigated electrolytes is visually represented in a descending order of CE for the first (Fig. 2a) and second cycles (Fig. 2b), respectively. Overall, the use of the separator-free cell results in lower CEs compared to conventional coin cells with separators. For instance, 1 M Li[FSA] in DME exhibited an initial CE of only 26.2% and an average CE of merely 41.8%, significantly lower than the values of over 97% reported in the literature using PP separators.<sup>18</sup> This discrepancy arises because separators in coin cells exert additional pressure on the electrode surface, thereby enhancing the density and reversibility of lithium deposition. However, in separator-free cells, the electrode distance is maintained by spacers, leading to no pressure on the electrolyte within these spacers and, consequently, insufficient interfacial pressure to anchor lithium metal on the electrode surface or reactivate generated dead lithium. Nonetheless, these cells minimize the impact of external factors from cell assembly and experimental handling, allowing for a focused examination of the key factors affecting the performance of the electrolyte itself. From the trends of CE in Fig. 2, these influencing factors can still be categorically divided into the type of solvent and salt, salt concentration, and the presence of additive. Each parameter will be further discussed in subsequent Sections in 3.2.

It is also noteworthy that in certain cycles, such as with 4 M Li[FSA]:EC:DMC + FEC, the 8th CE exceeded 100% (Fig. S2j, ESI<sup>†</sup>). Such an anomaly was included in the average value calculation because the CE exceeding 100% is attributed to “dead lithium” generated in earlier cycles becoming conductive again, and dissolving back into the electrolyte.<sup>39</sup> Furthermore, results for electrolytes such as 1 M Li[PF<sub>6</sub>]-TEP, which fell below the cutoff voltage immediately after the first cycle, were excluded from the CE calculation due to almost no lithium being deposited. For the IL electrolyte containing 20 mol% Li[TFSA]-[C<sub>2</sub>C<sub>1</sub>im][TFSA] (Fig. S3l, ESI<sup>†</sup>), even when the cutoff voltage was set to  $\pm 2.5$  V, it reached this limit during the first cycle's lithium deposition process, resulting in no reversible lithium deposition and dissolution reaction. In 20 mol% Li[TFSA]-[C<sub>3</sub>C<sub>1</sub>pyrr][TFSA] (Fig. S3k, ESI<sup>†</sup>), although the cell voltage reached the cutoff limit during the lithium deposition process in all cycles, a small amount of lithium dissolution was observed. These outcomes are likely due to the relatively high viscosity and low ionic conductivity of the TFSA-based ionic liquids,<sup>40</sup> coupled with the increased overpotential due to the longer working distance of 1 mm in separator-free cells



**Table 1** Summary of the first cycle, the second cycle, and the average Coulombic efficiency (CE) and overpotential at 0.2 mA h cm<sup>-2</sup> in the second cycle of Li metal deposition/dissolution tests

Salt	Concentration	Solvent	Additive	1st CE (%)	2nd CE (%)	Average CE (%)	Overpotential (V)
Li[PF <sub>6</sub> ]	1 M	SL		26.4	39.1	48.7	0.177
Li[PF <sub>6</sub> ]	1 M	TMP		5.2	7.2	7.2 <sup>a</sup>	0.302
Li[PF <sub>6</sub> ]	1 M	TEP					
Li[PF <sub>6</sub> ]	1 M	DMC					
Li[PF <sub>6</sub> ]	1 M	PC		67.0	78.0	73.2	0.155
Li[PF <sub>6</sub> ]	1 M	EC:DMC		54.8	76.3	84.6	0.125
Li[PF <sub>6</sub> ]	1 M	EC:DMC	3 wt% FEC	83.3	94.4	86.1 <sup>a</sup>	0.032
Li[PF <sub>6</sub> ]	1 M	AN					
Li[PF <sub>6</sub> ]	1 M	DMSO		19.3	29.7	27.1 <sup>a</sup>	0.112
Li[PF <sub>6</sub> ]	1 M	G2		—	—	—	—
Li[PF <sub>6</sub> ]	1 M	DME		—	—	—	—
Li[FSA]	1 M	SL		68.3	84.2	81.5	0.072
Li[FSA]	1 M	TMP					
Li[FSA]	1 M	TEP					
Li[FSA]	1 M	DMC		1.1	2.0	2.5	0.184
Li[FSA]	1 M	PC		60.5	78.8	80.0	0.122
Li[FSA]	1 M	PC	3 wt% FEC	85.4	92.5	92.7	0.167
Li[FSA]	4 M	PC		89.6	92.4	88.4	0.118
Li[FSA]	4 M	PC	3 wt% FEC	84.6	93.3	84.4	0.120
Li[FSA]	1 M	EC:DMC		49.4	86.0	84.1	0.068
Li[FSA]	1 M	EC:DMC	3 wt% FEC	89.0	90.0	84.4	0.094
Li[FSA]	4 M	EC:DMC		82.4	89.1	88.7	0.070
Li[FSA]	4 M	EC:DMC	3 wt% FEC	82.2	94.4	92.0	0.105
Li[FSA]	1 M	AN					
Li[FSA]	1 M	DMSO		21.3	34.9	34.4	0.054
Li[FSA]	1 M	G2					
Li[FSA]	1 M	DME		26.2	40.2	41.8	0.034
Li[FSA]	1 M	DME	3 wt% LiNO <sub>3</sub>	67.2	90.2	90.2 <sup>a</sup>	0.071
Li[FSA]	4 M	DME		66.4	70.0	60.6 <sup>a</sup>	0.058
Li[FSA]	20 mol%	[C <sub>3</sub> C <sub>1</sub> pyrr][FSA]		44.1	71.9	68.1	0.094
Li[FSA]	40 mol%	[C <sub>3</sub> C <sub>1</sub> pyrr][FSA]		66.9	74.5	72.9	0.080
Li[FSA]	20 mol%	[C <sub>2</sub> C <sub>1</sub> im][FSA]		69.9	61.3	63.3	0.045
Li[FSA]	40 mol%	[C <sub>2</sub> C <sub>1</sub> im][FSA]		81.2	70.3	77.8	0.054
Li[TFSA]	1 M	SL		58.7	80.2	70.0	0.071
Li[TFSA]	1 M	TMP					
Li[TFSA]	1 M	TEP		11.1	19.6	15.3 <sup>a</sup>	0.281
Li[TFSA]	1 M	DMC		4.4	7.7	3.2	0.201
Li[TFSA]	1 M	PC		44.4	83.0	83.7	0.134
Li[TFSA]	1 M	EC:DMC		57.2	87.1	90.3	0.070
Li[TFSA]	1 M	EC:DMC	3 wt% FEC	77.0	73.2	87.5	0.078
Li[TFSA]	1 M	AN					
Li[TFSA]	1 M	DMSO					
Li[TFSA]	1 M	G2		15.8	16.8	16.4	0.065
Li[TFSA]	1 M	DME		19.3	13.1	10.7	0.091
Li[TFSA]	1 M	DME	3 wt% LiNO <sub>3</sub>	86.5	91.2	91.7	0.078
Li[TFSA]	Saturated	DME		26.5	60.9	60.5	0.116
Li[TFSA]	20 mol%	[C <sub>3</sub> C <sub>1</sub> pyrr][TFSA]					
Li[TFSA]	20 mol%	[C <sub>2</sub> C <sub>1</sub> im][TFSA]					

<sup>a</sup> Electrolytes that lost cycle performance within 10 cycles. Average CE was calculated using data from only the 2nd cycle for 1 M Li[PF<sub>6</sub>]-TEP, the 2nd to the 7th cycles for 1 M Li[PF<sub>6</sub>]-EC:DMC 3 wt% FEC, the 2nd to the 4th cycles for 1 M Li[PF<sub>6</sub>]-DMSO, only the 2nd cycle for 1 M Li[FSA]-DME 3wt% LiNO<sub>3</sub>, the 2nd to the 6th cycles for 4 M Li[FSA]-DME, and the 2nd to the 3rd cycles for 1 M Li[TFSA]-TEP.

compared to traditional microporous separators (measured in tens of micrometers).

### 3.2 Parameters for Li metal deposition/dissolution

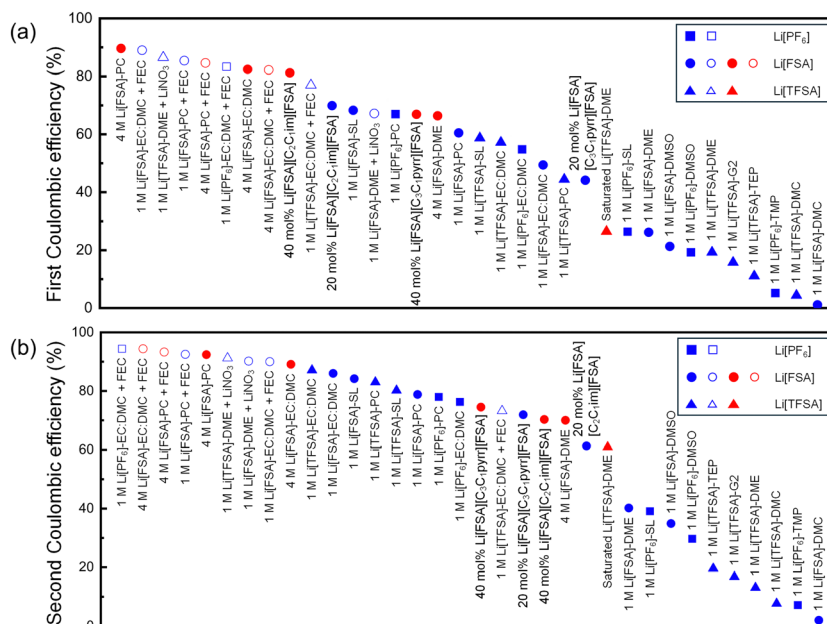
**3.2.1 Effects of salt and solvent.** As illustrated in Fig. 2 and Table 1, under conditions of 1 M concentration without additives, the CE varied significantly, depending on the type of solvents rather than the type of salts. For example, as compared to the lowest and highest Coulombic efficiencies in the second cycle using the same salts. The results observed as Δ70.8% (comparing 1 M Li[PF<sub>6</sub>]-TMP to 1 M Li[PF<sub>6</sub>]-PC), Δ84.0% (comparing 1 M Li[FSA]-DMC to 1 M Li[FSA]-EC:DMC), and

Δ79.4% (comparing 1 M Li[TFSA]-DMC to 1 M Li[TFSA]-EC:DMC). At this concentration, these variations indicate a strong dependency of lithium deposition/dissolution on the type of solvent used.

Notably, certain solvents such as AN, TEP, DMC, TMP, and DMSO exhibited similar behaviors. These solvents caused either an inability to cycle due to the reaction potential immediately reaching the cutoff voltage or a significantly low CE below 20% (Fig. S4, ESI†). This poor cyclability can be attributed to the chemical instability of the electrolytes. Electrolytes based on such as AN can be severely decomposed during lithium deposition. In fact, yellow decomposition products







**Fig. 2** The CE of lithium deposition/dissolution test for the investigated electrolytes in the separator-free cell (Li/Cu) for (a) the first and (b) second cycles. Square, circle, and triangle symbols indicate Li[PF<sub>6</sub>]-, Li[FSA]-based, and Li[TFSA]-based electrolytes, respectively. Blue color indicates the concentration of 1 M electrolytes and red color does the high concentrations of 4 M, 40 mol%, or saturated electrolytes. Filled and unfilled symbols denote the absence and presence of additives, respectively.

were observed in 1 M Li[FSA]-AN. AN spontaneously reacts with lithium metal, a strong reductant, which can lead to irreversible cycles.<sup>41</sup> The absence of a correlation between the overpotential and the CE during the second cycle further supports the notion that the issue stems from the reductive stability of the electrolyte, rather than solvation, ion transport, or other kinetic factors (see Fig. S2, ESI†).

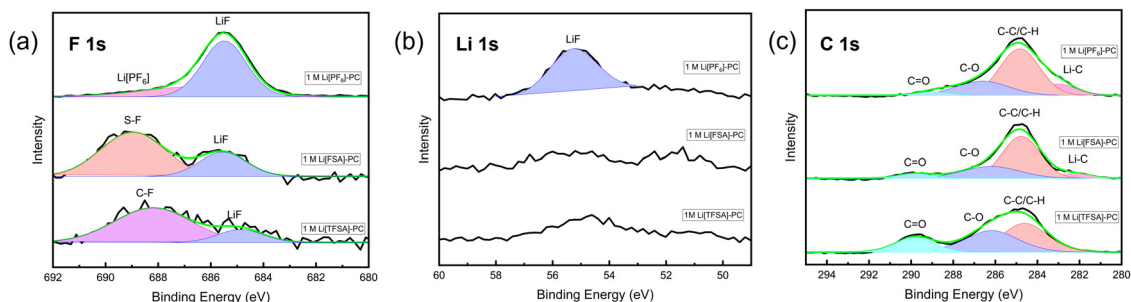
In contrast, SL, PC, and EC:DMC-based electrolytes show high CE. On the other hand, pure DMC solvents resulted in lower cycle performance; however, the inclusion of EC to form EC:DMC mixtures led to enhanced cycling performance. This improvement is attributed to the preferential formation of Li<sup>+</sup> and EC pairs, which are believed to form stable SEI and inhibit further electrolyte decomposition.<sup>42</sup> Upon comparing the CE of nine electrolytes derived from three distinct solvents (SL, PC, and EC:DMC) and salts (Li[PF<sub>6</sub>], Li[FSA], Li[TFSA]), a higher CE was not consistently attributed to specific solvents or salts (Fig. S5, ESI†). The results suggest that Li[PF<sub>6</sub>] with PC, Li[FSA] with SL,

and Li[TFSA] with EC:DMC were good matches. However, 1 M Li[PF<sub>6</sub>]-SL shows a clearly lower CE.

The bad match between Li[PF<sub>6</sub>] and SL might be caused by the close reductive potentials of SL and [PF<sub>6</sub>]<sup>-</sup>.<sup>43</sup> In contrast, [FSA]<sup>-</sup> and [TFSA]<sup>-</sup> undergo reductive decomposition at higher potentials, leading to the formation of inorganic SEI components such as LiF.

For subsequent experiments, PC was selected, which demonstrated high compatibility with all the three salts, to further analyze the composition of the SEI. Fig. 3 shows the results of XPS analysis for the PC-based electrolytes to characterize the composition of the SEI layer on Cu electrodes after one cycle.

The F 1s spectra of the Cu substrates in 1 M Li[PF<sub>6</sub>]-PC, 1 M Li[FSA]-PC, and 1 M Li[TFSA]-PC electrolytes reveal the presence of LiF in the SEI across all the electrolytes with its quantity correlating with the CE value in the first cycle CE. It was further corroborated in the Li 1s spectra, where a significant increase



**Fig. 3** XPS analysis of the SEI layers formed on Cu foil in the 1 M Li[PF<sub>6</sub>]-PC, 1 M Li[FSA]-PC, and 1 M Li[TFSA]-PC. (a) F 1s, (b) Li 1s, and (c) C 1s regions.

in peaks attributed to LiF was observed in 1 M Li[PF<sub>6</sub>]-PC, consistent with the F 1s spectra. The existence of LiF in SEI, which contributes to the rigid frame due to its very low solubility, effectively enhances the reversibility of lithium deposition/dissolution process, despite that its detailed mechanism still remains a topic of debate in research.<sup>44</sup> The C 1s spectra demonstrated peaks associated with the decomposition of the solvent, underscoring the solvent's contribution to the SEI formation under conventional salt concentrations. Fig. 4 shows the Raman spectra of three PC-based electrolytes. The peaks associated with free PC (712 cm<sup>-1</sup>) and solvated PC (720 cm<sup>-1</sup>) were observed across all the electrolytes.<sup>45</sup> Although there are still some differences in SEI components by the type of salts, uncoordinated solvent molecules are prevalent and participate in SEI formation alongside inorganic components derived from anions under the condition of 1 M concentration.

**3.2.2 Effects of concentration.** Comparing electrolytes at low concentrations (1 M in solvent systems or 20 mol% in ionic liquid systems) and high concentrations (4 M and saturated in organic solvent systems, or 40 mol% in ionic liquid systems), an increasing in concentration led to an increase in CE (Fig. 5). A notable example is Li[FSA] in DME, where the CE in the first cycle increased from 26.2 to 66.4% as the salt concentration was raised. This trend of increasing CE with concentration was also observed in previously reported separator-equipped coin cells using the Li[FSA]-DME system.<sup>18</sup> However, the addition of FEC and LiNO<sub>3</sub> did not further improve the 1st cycle CE at high-concentration electrolytes. It is important to note that the first cycle CE is not affected by an additive in the high concentration electrolytes. The further role of additives will be discussed later in 3.2.3.

Fig. 6 illustrates the variation in Raman shift with increased concentration for Li[FSA]-DME. The peaks at 719, 732, and 750 cm<sup>-1</sup> are attributed to the S-N-S bending mode of [FSA]<sup>-</sup> in solvent-separated ion pairs (SSIP), contact ion pairs (CIP), and ion aggregates (AGGs), respectively.<sup>46,47</sup> Furthermore, the peaks

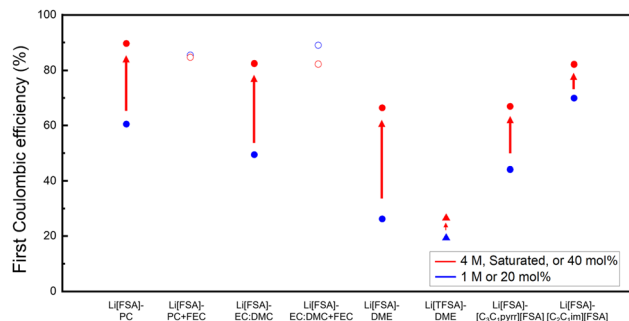


Fig. 5 Effects of electrolyte concentration on the 1st cycle Coulombic efficiency of Li metal deposition/dissolution.

around 823 and 849 cm<sup>-1</sup> are assigned to the the C-O-C stretching mode of uncoordinated DME, while the peak around 874 cm<sup>-1</sup> originates from DME coordinated with Li<sup>+</sup>. As the concentration increased, the peak intensity of uncoordinated DME decreased, while that of Li<sup>+</sup>-coordinated DME increased. Furthermore, the peak associated with SSIP declined, and the peak corresponding to AGGs appeared.

The composition of the SEI layer on Cu electrodes after one cycle was characterized using XPS for 1 M Li[FSA]-PC, 4 M Li[FSA]-PC, and 1 M Li[FSA]-PC + FEC electrolytes. The F 1s, Li 1s, and C 1s spectra of the three electrolytes are shown in Fig. 7a, b and c, respectively. Focusing on 1 M Li[FSA]-PC and 4 M Li[FSA]-PC, the XPS analysis of the F 1s peak identified S-F and LiF as predominant components, indicating an increased presence of LiF in the 4 M electrolyte compared to the 1 M variant. This observation suggests a greater involvement of the decomposition of [FSA]<sup>-</sup> within the SEI layer. It is because, in highly concentrated electrolytes, the coordination structure around Li<sup>+</sup> changes significantly, with Li<sup>+</sup> being coordinated more by anions rather than solvent molecules. This transformation leads to the formation of a more stable and inorganic-rich SEI. The enhanced contribution of anions to SEI formation in highly concentrated electrolytes results in a more robust SEI

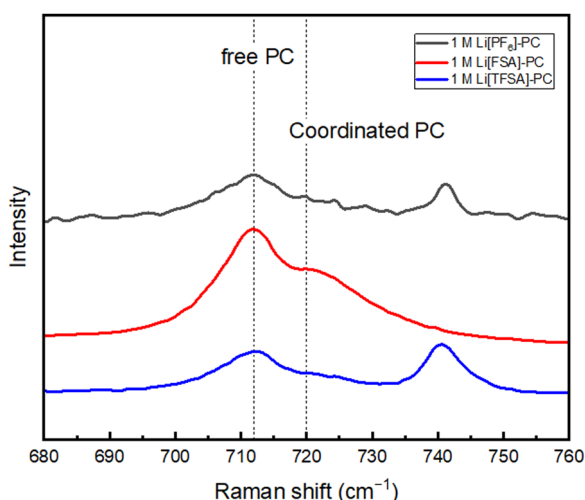


Fig. 4 Raman spectra of 1 M Li[PF<sub>6</sub>]-PC, 1 M Li[FSA]-PC, and 1 M Li[TFSa]-PC.

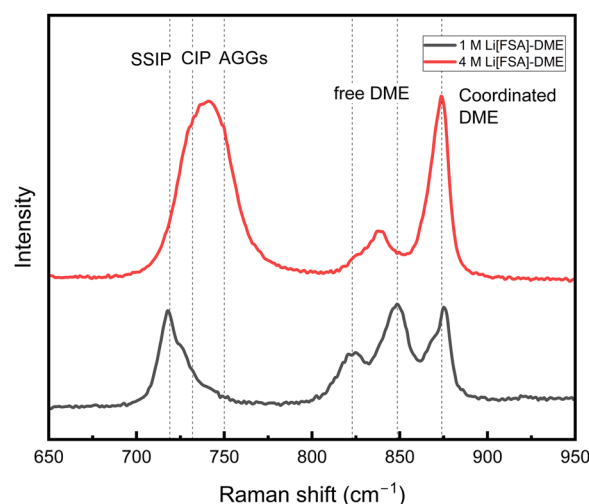


Fig. 6 Raman spectra of 1 M Li[FSA]-DME and 4 M Li[FSA]-DME.



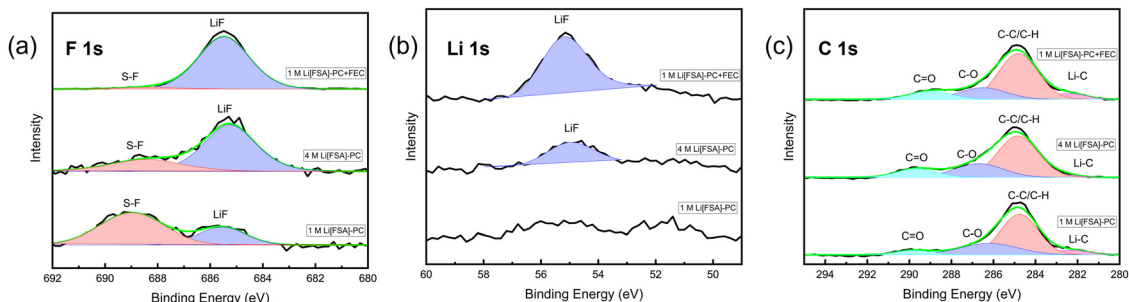


Fig. 7 XPS analysis of the SEI layers formed on Cu foil in the 1 M Li[FSA]-PC, 4 M Li[FSA]-PC, and 1 M Li[FSA]-PC + FEC. (a) F 1s, (b) Li 1s, and (c) C 1s regions.

that is less reactive with the electrolyte. The XPS analysis of the Li 1s peak is consistent with the F 1s spectra, revealing that the 4 M electrolyte contained a higher proportion of LiF within the SEI. The C 1s peaks indicate solvent decomposition in both the electrolytes.

**3.2.3 Effects of additive.** Fig. 8 indicates the change in CE in the first cycle due to the addition of FEC and LiNO<sub>3</sub>. Comparing adjacent electrolytes, at 1 M concentration, the inclusion of additives notably enhanced the first cycle CE in all electrolytes. This enhancement at 1 M concentration is attributed to the role of additives in the initial formation of the SEI layer. As shown in the XPS spectra (Fig. 7), the addition of FEC led to an increase in the amount of LiF. Given the lower LUMO energy of FEC (−0.87 eV) compared to EC (−0.38 eV) and other linear carbonates (DEC, 0 eV),<sup>16</sup> FEC can be preferentially reduced and form a compact and stable LiFE-rich SEI layer, thereby improving CE. Similarly, LiNO<sub>3</sub>, possessing low reduction stability, is preferentially reduced, contributing to the formation of a nitrogen-containing interphase on the electrode and enhancing the conductivity of lithium ions within the SEI layer.<sup>48</sup>

Conversely, at a higher concentration (4 M), the influence of FEC addition was minimal, which is likely due to the increase of ion pairs and aggregates at higher concentrations, causing the shift of reductive species from solvent to anion, resulting in the preferential reduction and decomposition of the anion as mentioned earlier. Hence, the incorporation of additives may

not consistently yield favorable outcomes; it can also adversely affect bulk properties. For instance, additive can cause an undesirable increase in viscosity and a decrease in ionic conductivity, distinct from the benefits associated with higher concentrations.<sup>49</sup> However, in the CEs during the first 10 cycles focused in this study, the introduction of a small amount of additives in high-concentration electrolytes, as well as in their derived localized high concentration electrolyte, still plays a crucial role in maintaining robust SEI for the electrolyte's long-term cyclability.<sup>50,51</sup>

## 4. Conclusions

In conclusion, this study exclusively assessed the impact of electrolytes on this fundamental process by employing a separator-free cell to minimize external influences on lithium metal deposition/dissolution. Comprehensively selected 48 electrolytes were prepared by varying solvent type, salt type, concentration, and the presence of additives. Among them, lithium deposition and dissolution tests were conducted on 46 electrolytes. Initially, evaluation focusing on electrolytes at a 1 M concentration revealed a number of free solvent molecules exist at this concentration and CE significantly depends on the type of solvent. Interestingly, carbonate solvents with FEC show very high CEs. In highly concentrated electrolytes, there was transformation in the coordination structure around Li<sup>+</sup>, characterized by an increase of coordinated solvents and CIP and AGGs anions, leading to an enhanced contribution of anions to the SEI formation. The inclusion of easily reducible solvents or salts as additives resulted in anion-derived SEI formation. It is worth mentioning that combining two approaches of increasing concentration and additives did not necessarily yield the highest CE.

Separator-free cells stand as a pivotal guide to amplifying and focusing on the role of electrolyte itself. By enhancing the CE, these insights could better facilitate applications in more practical low-pressure cell systems. These comprehensive lithium deposition/dissolution results underline the potential of optimizing electrolyte to achieve higher efficiency and stability in lithium metal batteries, especially in environments where electrolyte and electrode interactions are critical for overall performance.

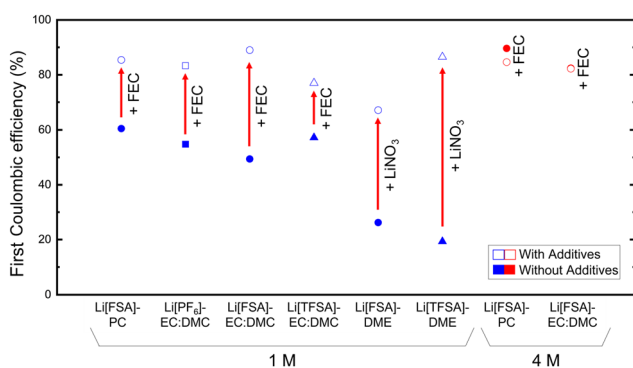


Fig. 8 Effects of additives on the 1st cycle Coulombic efficiency of Li deposition/dissolution tests. Additive: FEC for carbonate electrolytes and LiNO<sub>3</sub> for ether electrolytes.

## Author contributions

Tomoki Takahashi and Di Wang: investigation, data curation, visualization, writing – original draft. Jinkwang Hwang: conceptualization, methodology, investigation, writing – original draft, review & editing supervision. Kazuhiko Matsumoto: validation, supervision, funding acquisition, writing – review & editing, revision & suggestions.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This study was supported by Grant-in-Aid for Scientific Research (B) conducted through the support of the Japan Society for the Promotion of Science (JSPS, KAKENHI Grant Number 19H02811). The authors express their gratitude to Prof. Hagiwara of Kyoto University for engaging in a fruitful discussion.

## Notes and references

- 1 T. Kim, W. T. Song, D. Y. Son, L. K. Ono and Y. B. Qi, *J. Mater. Chem. A*, 2019, **7**, 2942–2964.
- 2 M. Li, J. Lu, Z. Chen and K. Amine, *Adv. Mater.*, 2018, **30**, 1800561.
- 3 M. Winter, B. Barnett and K. Xu, *Chem. Rev.*, 2018, **118**, 11433–11456.
- 4 Q. Liu, X. Su, D. Lei, Y. Qin, J. Wen, F. Guo, Y. A. Wu, Y. Rong, R. Kou, X. Xiao, F. Aguesse, J. Bareño, Y. Ren, W. Lu and Y. Li, *Nat. Energy*, 2018, **3**, 936–943.
- 5 C. Wang, C. Yang and Z. Zheng, *Adv. Sci.*, 2022, **9**, 2105213.
- 6 S. P. Li, F. Lorandi, J. F. Whitacre and K. Matyjaszewski, *Macromol. Chem. Phys.*, 2020, **221**, 1900379.
- 7 R. Van Noorden, *Nature*, 2014, **507**, 26–28.
- 8 J. Betz, G. Bieker, P. Meister, T. Placke, M. Winter and R. Schmuch, *Adv. Energy Mater.*, 2019, **9**, 1803170.
- 9 J. Liu, Z. N. Bao, Y. Cui, E. J. Dufek, J. B. Goodenough, P. Khalifah, Q. Y. Li, B. Y. Liaw, P. Liu, A. Manthiram, Y. S. Meng, V. R. Subramanian, M. F. Toney, V. V. Viswanathan, M. S. Whittingham, J. Xiao, W. Xu, J. H. Yang, X. Q. Yang and J. G. Zhang, *Nat. Energy*, 2019, **4**, 180–186.
- 10 A. Varzi, K. Thanner, R. Scipioni, D. Di Lecce, J. Hassoun, S. Dörfler, H. Altheus, S. Kaskel, C. Prehal and S. A. Freunberger, *J. Power Sources*, 2020, **480**, 228803.
- 11 D. Wang, J. Qiu, N. Inui, R. Hagiwara, J. Hwang and K. Matsumoto, *ACS Energy Lett.*, 2023, **8**, 5248–5252.
- 12 W. Cao, J. Zhang and H. Li, *Energy Storage Mater.*, 2020, **26**, 46–55.
- 13 J. I. Lee, G. Song, S. Cho, D. Y. Han and S. Park, *Batteries Supercaps*, 2020, **3**, 828–859.
- 14 B. Liu, J. G. Zhang and W. Xu, *Joule*, 2018, **2**, 833–845.
- 15 L. Du, B. Zhang, C. Yang, L. Cui, L. Mai and L. Xu, *Energy Storage Mater.*, 2023, **61**, 102914.
- 16 X. Q. Zhang, X. B. Cheng, X. Chen, C. Yan and Q. Zhang, *Adv. Funct. Mater.*, 2017, **27**, 1605989.
- 17 X.-Q. Zhang, X. Chen, L.-P. Hou, B.-Q. Li, X.-B. Cheng, J.-Q. Huang and Q. Zhang, *ACS Energy Lett.*, 2019, **4**, 411–416.
- 18 J. Qian, W. A. Henderson, W. Xu, P. Bhattacharya, M. Engelhard, O. Borodin and J.-G. Zhang, *Nat. Commun.*, 2015, **6**, 6362.
- 19 S. Chen, J. Zheng, D. Mei, K. S. Han, M. H. Engelhard, W. Zhao, W. Xu, J. Liu and J.-G. Zhang, *Adv. Mater.*, 2018, **30**, 1706102.
- 20 A. C. Kozen, C.-F. Lin, O. Zhao, S. B. Lee, G. W. Rubloff and M. Noked, *Chem. Mater.*, 2017, **29**, 6298–6307.
- 21 Y. Liu, D. Lin, P. Y. Yuen, K. Liu, J. Xie, R. H. Dauskardt and Y. Cui, *Adv. Mater.*, 2017, **29**, 1605531.
- 22 L. Zhao, L. Du, H. Xu, J. Deng and L. Xu, *ACS Appl. Energy Mater.*, 2023, **6**, 9523–9531.
- 23 H. Zhao, D. Lei, Y.-B. He, Y. Yuan, Q. Yun, B. Ni, W. Lv, B. Li, Q.-H. Yang, F. Kang and J. Lu, *Adv. Energy Mater.*, 2018, **8**, 1800266.
- 24 L.-L. Lu, J. Ge, J.-N. Yang, S.-M. Chen, H.-B. Yao, F. Zhou and S.-H. Yu, *Nano Lett.*, 2016, **16**, 4431–4437.
- 25 Y. Liu, Q. Liu, L. Xin, Y. Liu, F. Yang, E. A. Stach and J. Xie, *Nat. Energy*, 2017, **2**, 17083.
- 26 H. Jia, C. Zeng, H. S. Lim, A. Simmons, Y. P. Zhang, M. H. Weber, M. H. Engelhard, P. Y. Gao, C. J. Niu, Z. J. Xu, J. G. Zhang and W. Xu, *Adv. Mater.*, 2024, **36**, 2311312.
- 27 S. H. Lee, J.-Y. Hwang, J. Ming, Z. Cao, H. A. Nguyen, H.-G. Jung, J. Kim and Y.-K. Sun, *Adv. Energy Mater.*, 2020, **10**, 2000567.
- 28 M. D. Tikekar, S. Choudhury, Z. Tu and L. A. Archer, *Nat. Energy*, 2016, **1**, 16114.
- 29 Y. Y. Zheng, D. Wang, S. Kaushik, S. N. Zhang, T. Wada, J. Hwang, K. Matsumoto and R. Hagiwara, *Energychem*, 2022, **4**, 100075.
- 30 J. Hwang, H. Okada, R. Haraguchi, S. Tawa, K. Matsumoto and R. Hagiwara, *J. Power Sources*, 2020, **453**, 227911.
- 31 X. Chen and Q. Zhang, *Acc. Chem. Res.*, 2020, **53**, 1992–2002.
- 32 G. M. Hobold, J. Lopez, R. Guo, N. Minafra, A. Banerjee, Y. Shirley Meng, Y. Shao-Horn and B. M. Gallant, *Nat. Energy*, 2021, **6**, 951–960.
- 33 J. Xiao, Q. Li, Y. Bi, M. Cai, B. Dunn, T. Glossmann, J. Liu, T. Osaka, R. Sugiura, B. Wu, J. Yang, J.-G. Zhang and M. S. Whittingham, *Nat. Energy*, 2020, **5**, 561–568.
- 34 B. D. Adams, J. Zheng, X. Ren, W. Xu and J.-G. Zhang, *Adv. Energy Mater.*, 2018, **8**, 1702097.
- 35 R. Rodriguez, R. A. Edison, R. M. Stephens, H.-H. Sun, A. Heller and C. B. Mullins, *J. Mater. Chem. A*, 2020, **8**, 3999–4006.
- 36 J. Ahn, M. Kim, J. Seo, S. Yoon and K. Y. Cho, *J. Power Sources*, 2023, **566**, 232931.
- 37 H. An, Y. Roh, Y. Jo, H. Lee, M. Lim, M. Lee, Y. M. Lee and H. Lee, *Energy Environ. Mater.*, 2023, **6**, e12397.
- 38 L. Su, X. Zhao, M. Yi, H. Charalambous, H. Celio, Y. Liu and A. Manthiram, *Adv. Energy Mater.*, 2022, **12**, 2201911.
- 39 F. Liu, R. Xu, Y. Wu, D. T. Boyle, A. Yang, J. Xu, Y. Zhu, Y. Ye, Z. Yu, Z. Zhang, X. Xiao, W. Huang, H. Wang, H. Chen and Y. Cui, *Nature*, 2021, **600**, 659–663.





- 40 H. Matsumoto, H. Sakaebe, K. Tatsumi, M. Kikuta, E. Ishiko and M. Kono, *J. Power Sources*, 2006, **160**, 1308–1313.
- 41 Y. Yamada, K. Furukawa, K. Sodeyama, K. Kikuchi, M. Yaegashi, Y. Tateyama and A. Yamada, *J. Am. Chem. Soc.*, 2014, **136**, 5039–5046.
- 42 Q. Li, Z. Cao, W. Wahyudi, G. Liu, G.-T. Park, L. Cavallo, T. D. Anthopoulos, L. Wang, Y.-K. Sun, H. N. Alshareef and J. Ming, *ACS Energy Lett.*, 2021, **6**, 69–78.
- 43 J. Alvarado, M. A. Schroeder, M. Zhang, O. Borodin, E. Gobrogge, M. Olguin, M. S. Ding, M. Gobet, S. Greenbaum, Y. S. Meng and K. Xu, *Mater. Today*, 2018, **21**, 341–353.
- 44 Z. Li, L. Wang, X. D. Huang and X. M. He, *Small*, 2023, **20**, 2305429.
- 45 T. Doi, R. Masuhara, M. Hashinokuchi, Y. Shimizu and M. Inaba, *Electrochim. Acta*, 2016, **209**, 219–224.
- 46 R. Okada, Y. Aoki, M. Oda, M. Nakazawa, M. Inaba and T. Doi, *ACS Appl. Energy Mater.*, 2023, **6**, 546–553.
- 47 Y. Zhao, T. Zhou, T. Ashirov, M. E. Kazzi, C. Cancellieri, L. P. H. Jeurgens, J. W. Choi and A. Coskun, *Nat. Commun.*, 2022, **13**, 2575.
- 48 Z. Wang, Y. Wang, C. Wu, W. K. Pang, J. Mao and Z. Guo, *Chem. Sci.*, 2021, **12**, 8945–8966.
- 49 Y. Yamada and A. Yamada, *J. Electrochem. Soc.*, 2015, **162**, A2406.
- 50 H. Jia, J.-M. Kim, P. Gao, Y. Xu, M. H. Engelhard, B. E. Matthews, C. Wang and W. Xu, *Angew. Chem., Int. Ed.*, 2023, **62**, e202218005.
- 51 Q.-K. Zhang, X.-Q. Zhang, J. Wan, N. Yao, T.-L. Song, J. Xie, L.-P. Hou, M.-Y. Zhou, X. Chen, B.-Q. Li, R. Wen, H.-J. Peng, Q. Zhang and J.-Q. Huang, *Nat. Energy*, 2023, **8**, 725–735.

