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Pressure effects on the nanostructure of bicontinuous propane microemulsions with extended surfactants: a SANS study†

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In our recent work, we investigated the influence of pressure on the temperature-dependent phase behavior of symmetric, application-relevant microemulsions containing propane, stabilized by an extended surfactant mixture. By means of high-pressure small-angle neutron scattering, the present study provides further insights by unraveling the impact of pressure and propane on the nanostructure of these microemulsions near their optimum point. Despite the obvious presence of multiple scattering, all recorded scattering curves show the typical characteristics of symmetric bicontinuous microemulsions. Analysis of the scattering data using the Teubner–Strey model and Porod’s law for diffuse interfaces provided the periodicity d_{TS} , the correlation length ξ_{TS} , and the specific interface S/V , as well as the amphiphilicity factor f_a and the effective bending rigidity κ_{eff} of the amphiphilic film. The overall structural order of pure propane microemulsions was found to be markedly lower compared to the *n*-decane microemulsions. While the structure of *n*-decane-rich microemulsions only shows a weak pressure dependence, propane-rich formulations exhibit a significant increase of ξ_{TS} with pressure due to an increasing surfactant monolayer rigidity, caused by enhanced interactions of the compressible propane with the surfactant tails. Microemulsions containing mixtures of the two hydrocarbons behave accordingly, demonstrating that the presence of the short-chain alkane gradually amplifies the sensitivity of the amphiphilic film to pressure changes. Interestingly, the geometric prefactor a of bicontinuous structure models increases from slightly above 7 for *n*-decane microemulsions to $a > 8$ for propane formulations, owing to the increasing disorder.

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1 Introduction

Microemulsions are thermodynamically stable mixtures of water and oil, stabilized by a surfactant monolayer separating polar and non-polar nanodomains. Adsorption of surfactant molecules at the oil/water interface enables to achieve ultra-low interfacial tensions between the immiscible liquids.^{1–4} While microemulsions are optically homogeneous, they exhibit a wide range of nanostructures, including droplet-like, lamellar, or bicontinuous structures.^{5,6} Owing to their unique properties,

conveniently adjustable *via* composition, temperature, or pressure, microemulsions have found their way into many applications such as cleaning, cosmetics, pharmaceuticals and enhanced oil recovery.^{7–11}

Studies on the properties of microemulsions containing gaseous components, such as short-chain alkanes, are scarce, although such formulations can play a central role for instance in chemical-enhanced oil recovery, where the use of microemulsions can improve the exploitation of existing crude oil reservoirs instead of having to explore new oil fields. Reasons for the under-representation of such investigations on microemulsions containing volatile components – which have to be carried out at high pressures in order to solubilize these (liquefied) components and to match reservoir conditions, such as pressures in the range of a few hundred bar – are the necessity for special setups and the experimentally more demanding and time-consuming measurements compared to investigations at ambient pressure.

Just recently, we systematically studied the pressure-dependent phase behavior of application-relevant brine/butyldi-glycol – *n*-decane/propane – alkyl alkoxy sulfate/alkyl sulfonate

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microemulsions containing equal amounts of water and oil for temperatures up to 80 °C and pressures up to 350 bar, which covers reservoir depths of several thousand meters when using pressure gradients of approximately 0.1 bar per meter (depends on fluid density).¹² Due to their long alkyl chains and ionic nature, the surfactants used in our current work exhibit negligible monomeric solubilities in both water and oil, preventing extraction effects. Extended surfactants such as alkyl alkoxy sulfates, which feature groups of intermediate polarity between the hydrophobic tail and hydrophobic head, are characterized by high solubilization capacities and may offer an even stronger reduction of the oil/water interfacial tension compared to conventional surfactants, making them particularly attractive for the recovery of oil trapped within rock pores.^{13,14} We found that the influence of pressure depends on the oil used in the microemulsion: While in *n*-decane-rich microemulsions, pressure moves the system from water-in-oil (w/o) to oil-in-water (o/w) structures, the phase sequence inverts from o/w to w/o in propane-rich formulations, with a bicontinuous structure found during the structural transition.^{15,16} This was explained by the competing effects of headgroup hydration and oil penetration and is thus related to the strength of interactions between surfactant and oil. The first effect outweighs the second in *n*-decane rich formulations, whereas a facilitated oil penetration and a stronger pressure dependence of propane-surfactant interactions result in the opposite behavior in propane-rich formulations.

Motivated by this oil-dependent influence of pressure on the phase behavior of symmetrical microemulsions, the aim of the present study was to systematically investigate the effect of pressure on the nanostructure of these systems. Considering the need for even more specialized setups to perform such investigations, it is not surprising that even fewer publications exist that use methods such as small-angle neutron scattering (SANS), neutron spin echo (NSE) or dynamic light scattering (DLS). In the following, a brief overview of relevant studies is given.

Starting with liquid oils, three studies conducted by Kawabata *et al.*, who utilized a combination of SANS, NSE and DLS, revealed a nearly pressure-independent droplet radius for water-in-decane microemulsions stabilized by different ionic and non-ionic surfactants.^{17–19} The authors report a pressure-induced increase of the bending rigidity, κ , of the surfactant monolayer which is one of the two elastic moduli (alongside the saddle splay modulus $\bar{\kappa}$) in Helfrich's description of the elastic energy of a membrane,²⁰ whereas higher temperatures led to a less rigid amphiphilic film.

Interestingly, almost no pressure dependence of the droplet radii was likewise found in most studies on water-in-oil microemulsions containing more volatile hydrocarbons, revealing no influence of alkane chain length or density.^{21–23} Similar findings were obtained for water-in-CO₂ and CO₂-in-water microemulsions, which are typically solubilized by fluorinated surfactants owing to the stronger affinity to CO₂ compared to conventional hydrocarbon-based surfactants.^{24–27} One of these studies reported a pressure-induced change of the shape of the nanostructure due to a pressure-induced shift of phase behavior, in particular the emulsification failure boundary.²⁶ More notable

deviations of the droplet radius under pressure were only observed for water-in-propane droplets stabilized by the non-ionic surfactant C₁₂E₅, which was explained by its pressure-dependent monomeric solubility.²¹

Just a handful of studies have been conducted on the pressure dependence of the nanostructure of bicontinuous microemulsions.^{28–31} In two works on supercritical CO₂ microemulsions stabilized by a mixture of technical non-ionic fluorinated surfactants,^{29,30} a stiffening of the surfactant monolayer under pressure was found, allowing for a higher structural order, which is in agreement with the works on water-in-decane droplet microemulsions. Minor changes in the periodicity under pressure were again attributed to the monomeric solubility of the surfactant.³⁰ Apart from the SANS study by Pütz *et al.* with a CO₂/cyclohexane mixture,²⁷ systematic investigations on the influence of a varying ratio of volatile and non-volatile oils on the impact of pressure on microemulsion nanostructure are still missing. Equally scarce are high-pressure nanostructure investigations of microemulsions stabilized by application-relevant extended surfactants.

This brief literature review emphasizes the scarcity of insights into the nanostructure of microemulsions containing volatile alkanes, which is even more noticeable when it comes to bicontinuous structures and the use of extended surfactants. Having just recently studied the phase behavior of such microemulsion formulations,^{15,16} this work therefore aims to elucidate the influence of pressure on the nanostructure of balanced microemulsions of the type brine/butyldiglycol – *n*-decane/propane – C_{16–18}-7PO-0.1EO-SO₄Na/C_{14–17}-SO₃Na *via* high-pressure small-angle neutron scattering studies. To the best of our knowledge, no high-pressure SANS studies on extended surfactant microemulsions have been reported in literature to date. We thus conducted bulk contrast SANS experiments to study the influence of pressure and oil composition, systematically adjusted *via* the propane-to-*n*-decane ratio, on microemulsions prepared near their respective optimum point. To quantify the influence of propane and pressure on microemulsion nanostructure, all recorded scattering curves were analyzed using the Teubner-Strey model³² and Porod's law for diffuse interfaces.^{33,34} We demonstrate that propane and pressure significantly and systematically influence the ordering of the nanostructure, quantified *via* the amphiphilicity factor f_a , which depends on the width of scattering peak (\propto correlation length ξ_{TS}) and is related to a systematically changing bending rigidity of the amphiphilic film.

2 Experimental

2.1 Reagents

H₂O was double-distilled, D₂O (Deutero, 99.9%) was used as obtained. Sodium chloride (NaCl, Carl Roth, 99.5%) was used as salt. *n*-Decane (Acros Organics, 99%) and propane (Air Liquide, 99.95%) were used as oils. BASF SE provided the co-solvent butyldiglycol (99%) and aqueous solutions of the anionic surfactants C_{16–18}-7PO-0.1EO-SO₄Na (47–54 wt% active content), an



alkyl alkoxy sulfate (“extended surfactant”), and $C_{14-17}\text{-SO}_3\text{Na}$ (30–32 wt% active content), a secondary alkyl sulfonate. All chemicals were used without further purification, but surfactant homogeneity was ensured before sample preparation.

2.2 High-pressure SANS cell

SANS experiments were performed with a high-pressure setup developed by Strey and coworkers.³⁰ The cell is equipped with two customized sapphire windows ($d_{\text{sapphire}} = 12$ mm) with a sample thickness of $d_{\text{sample}} = 2$ mm (transmission at measurement conditions is $T_{\text{cell}} = 0.89$), allowing for sufficient miscibility and homogeneity of the samples when studying phase behavior *via* visual determination. Regulating pressure mechanically with a piston, thereby adjusting a sample volume of approximately 17 mL, instead of *via* pressurization with gas circumvents changes in the sample composition during measurements. Pressure is measured using a pressure transducer (Burster 81530) connected to a measurement amplifier with an accuracy of ± 3 bar. Calibration is performed with a dead weight tester (WIKA CPB5800) up to a pressure of $p_{\text{max,cal}} = 400$ bar, with the experimental highest pressure being $p_{\text{max,exp}} \approx 350$ bar. The cell is temperature-controlled by a liquid flowing through tubes in the thermal coating around the stainless steel centerpiece of the setup, with temperature regulation taking place with a thermostat connected to the tubing. Temperature can be read off a thermometer in the steel cylinder, offering a precision of ± 0.1 K after temperature equilibration.

2.3 Sample preparation

All investigated microemulsion are pseudo-ternary A–B–C systems recorded in bulk contrast. Here, A = $\text{H}_2\text{O}/\text{D}_2\text{O}/\text{NaCl}/\text{butyldiglycol}$, with a fixed salinity of 4.37 wt% to set the target temperature range. In our previous D_2O -free phase behavior study,¹⁵ the salinity was 4.70 wt%. This change is required to keep the molar salt concentration of the brine constant. With the surfactants containing H_2O by default, we set the highest possible $\text{D}_2\text{O}/\text{H}_2\text{O}$ ratio of 73/27 (w/w). Despite its amphiphilic nature, butyldiglycol, used at 5 wt% of A to facilitate phase behavior studies, is treated as a co-solvent due to its high hydrophilicity. From electrical conductivity measurements, we know that its impact on the phase inversion temperature \bar{T} and therefore on the curvature of the amphiphilic film is marginal at the concentration used here.¹⁵ B is *n*-decane and/or propane, C is the surfactant mixture of $C_{16-18}\text{-7PO-0.1EO-SO}_4\text{Na}/C_{14-17}\text{-SO}_3\text{Na}$, which were used in a 3:1 (w/w) ratio (based on active content) to set the desired temperature range. Stock solutions with surfactant (= stock C) and without (= stock A) were used to adjust the desired surfactant concentration. Samples were prepared with equal volumes of hydrophilic and hydrophobic component ($V_A = V_B$) to obtain symmetric microemulsions, using the propane density at filling pressure and temperature.³⁵ Given the different densities of H_2O and D_2O , surfactant mass fractions (as used in our previous work)^{15,16} were converted to the respective amphiphilic volume ratio, with $\phi_C = V_C/V_{\text{total}}$ (referring to filling conditions), while keeping the equivolumetric oil-to-water ratio. Samples were prepared in proximity to the respective

optimum points \bar{X} of each microemulsion system to adjust the bicontinuous structure while maintaining a sufficient width of the one-phase region to allow for pressure variations. \bar{X} is characterized by ϕ_C , the minimum surfactant volume fraction required to fully solubilize water and oil, as well as the phase inversion (or optimum) temperature \bar{T} .

Samples were prepared directly in the high-pressure cell. Liquid components were added in the order stock C, *n*-decane, stock A. Liquefied propane was inserted subsequently *via* a filling station with a diaphragm accumulator. Since weighing the heavy HP-SANS cell with sufficient precision to account for the small amounts of added propane is not feasible, piston height was calibrated against sample volume. Densities were determined beforehand using an Anton Paar DMA 5000 M density meter. After filling in the liquids, piston height was adjusted to fill in the target amount of propane. Temperature of the HP cell was regulated as describe above. Homogeneity of the sample was achieved under continuous stirring using a special magnetic stirring bar until the temperature equilibrium was reached. The SANS cell was additionally rotated perpendicular to the *z* axis to avoid phase separation above or below the visible scattering volume. Once a measurement was finished, the cell was emptied and cleaned thoroughly with water, acetone and CO_2 . New samples were prepared for each compositional change after air-drying the cell.

2.4 Phase behavior

Phase behavior studies in our previous work were performed as $T(\gamma)$ cuts (“fish cuts”) with H_2O .¹⁵ Given the use of D_2O in the present SANS study, mass fractions were converted to volume fractions (ϕ_C , see above). Phase transition temperatures of the D_2O -containing samples investigated here were checked *via* visual determination in the HP-SANS cell before each measurement, considering that the switch from H_2O to D_2O typically produces a small temperature shift of the phase boundaries.^{34,36,37}

2.5 Small-angle neutron scattering

SANS measurements were conducted during three days of beam time at the D22 diffractometer of the Institut Laue-Langevin (ILL) in Grenoble, France, with a wavelength of $\lambda = 6$ Å ($\Delta\lambda/\lambda = 0.1$). Experiments were performed at a collimation/detector distance of 17.6/17.6 m, providing a q range of $0.0032 < q$ (Å^{−1}) < 0.62 with further use of the side detector of D22. Samples were prepared in the HP-SANS cell ($d_{\text{sample}} = 2$ mm) as discussed above, ensuring sample homogeneity *via* visual inspection before mounting the cell into the beam line. A reference measurement at 1 bar was done in a 1 mm Hellma quartz cuvette. In the ESI,[†] the impact of sample thickness on absolute scattering intensities as well as the influence of multiple scattering are addressed in more detail.

3 Reduction and analysis of SANS data

Raw scattering data, obtainable from the ILL,³⁸ were converted to absolute scattering intensities using direct beam measurements. The GRASP software³⁹ was utilized for data reduction, considering empty cell and background scattering as well as



transmission. Unless stated otherwise, data were radially averaged.

3.1 Teubner–Strey model and Porod's law

The peak region of all scattering profiles was analyzed with the Teubner–Strey model by treating the bicontinuous domains as non-rigid domains characterized by their periodicity d_{TS} and correlation length ξ_{TS} .³² The Teubner–Strey model is derived from Landau theory, for which the Landau free energy, obtained from an order parameter expansion of the free energy density using gradient terms, provides the scattering intensity distribution $I(q)$ under consideration of the free energy change resulting from fluctuations of the order parameter. The typical correlation peak of well-structured microemulsions occurs when the order parameter expansion coefficient $c_1 < 0$ (with $a_2 > 0$ and $c_2 > 0$). Details on the analysis are presented in the ESI.† Expressing these coefficients and thus $I(q)$ with more descriptive fit parameters provides the fitting function used for the scattering data analysis, with

$$I(q) = \frac{I_0}{\left(1 - \frac{I_0}{I_{\text{max}}}\right) \left(\frac{q^2}{q_{\text{max}}^2} - 1\right)^2 + \frac{I_0}{I_{\text{max}}}} \quad (1)$$

where I_0 is the forward scattering intensity and I_{max} is the maximum scattering intensity (at $q = q_{\text{max}}$). The order expansion coefficients a_2 , c_1 and c_2 can be directly determined from the fitting parameters and are further used to calculate the length scales

$$d_{\text{TS}} = 2\pi \left[\frac{1}{2} \left(\frac{a_2}{c_2} \right)^{\frac{1}{2}} - \frac{c_1}{4c_2} \right]^{-\frac{1}{2}} \quad (2)$$

and

$$\xi_{\text{TS}} = \left[\frac{1}{2} \left(\frac{a_2}{c_2} \right)^{\frac{1}{2}} + \frac{c_1}{4c_2} \right]^{-\frac{1}{2}}. \quad (3)$$

The value of the periodicity, d_{TS} , of the structure predominantly depends on the position of the peak (*i.e.*, q_{max}). In a symmetric bicontinuous microemulsion with equal volumes of water and oil, the size, $d_{\text{TS}}/2$, of water and oil domains is therefore equal. The sharpness of the correlation peak characterizes the order of the bicontinuous structure *via* the correlation length ξ_{TS} , which is a measure for the length at which the order of the structure persists. Given that microemulsions do not exhibit long-range order, ξ_{TS} is typically small, roughly of the order of the domain size.^{32,36,40}

In Fig. 3–6, the Teubner–Strey fit is shown as a solid red line. The fit almost quantitatively describes the data around the peak, but it deviates from the scattering data at higher q due to multiple scattering. Even though the q^{-4} decay is mathematically incorporated in the Teubner–Strey fit, the fact that Teubner and Strey's publication explicitly focuses on the origin of the scattering peak³² and to avoid inconsistencies due to multiple scattering contributions (as discussed in the ESI†), it

was considered more adequate to limit the analysis to just the peak region. The entire q range could be described by models such as a fractal scattering-based Beaucage model⁴¹ or the clipped random wave model,⁴² both of which introduce a third length scale (radius of gyration and surface roughness parameter, respectively), or by trying to consider multiple scattering by simply combining multiple Teubner–Strey fits.⁴³

Instead, we analyzed the high q data using Porod's law for diffuse interfaces

$$I(q) - I_{\text{incoh}} = \frac{S}{V} \frac{Q}{\pi \phi_a \phi_b} q^{-4} e^{-q^2 t^2}, \quad (4)$$

which takes into account the diffuseness t of the amphiphilic film by using a Gaussian smoothing function instead of a step profile to describe the variation of the scattering length density across the film.^{33,34} Utilizing the invariant Q and the respective volume fractions of the hydrophilic and hydrophobic domains, ϕ_a and ϕ_b , this analysis provides the specific internal interface S/V of the amphiphilic film, also known as surface-to-volume ratio. The value of I_{incoh} has a strong influence at high q , where the incoherent scattering contribution outweighs the coherent scattering contribution and thus strongly impacts the values of S/V and t . Due to this sensitivity to the absolute intensity, background-corrected coherent scattering intensities $I(q) - I_{\text{incoh}}$ were used for the analysis. For the sake of visualization and to avoid data overlap at extremely low intensities at high q , the incoherent background was subsequently re-added to all plots presented in this work.

3.2 Bending rigidity and amphiphilicity factor

Following Gompper *et al.*'s modification of the random interface model developed by Pieruschka and Safran, d_{TS} and ξ_{TS} can be utilized to determine the bending rigidity κ (*cf.* Fig. 1), which is one of the two elastic moduli employed to describe the elastic properties of amphiphilic membranes alongside the saddle splay modulus $\bar{\kappa}$.^{20,44–46} A higher κ corresponds to a more rigid interfacial film, whose thermal fluctuations lead to its softening and the concomitant decrease of κ . These thermal fluctuations range from small molecular length scales to the order of d_{TS} , which causes a renormalization of κ . Furthermore, they increase the consumption of interface, which affects the domain spacing, *i.e.*, d_{TS} .⁴⁷ Monte Carlo simulations and experimental neutron spin echo (NSE) and small-angle neutron scattering experiments have indicated that κ determined *via* the Teubner–Strey analysis of SANS data is perhaps better understood as a mixture of the actual bending rigidity and the saddle splay modulus.^{48,49} Given that NSE was not available within the scope of this work and an estimation would only be possible using a theoretical value, κ is therefore conceived as an effective bending rigidity, labelled κ_{eff} , as done by other authors.^{43,50–52} This effective bending rigidity of the amphiphilic film is given as

$$\kappa_{\text{eff}} = \frac{10\pi\sqrt{3}}{64} \frac{\xi_{\text{TS}}}{d_{\text{TS}}} k_{\text{B}} T \quad (5)$$

A higher value of κ_{eff} therefore enables the formation of a bicontinuous microemulsion with higher structural order, characterized by a sharper scattering peak and thus a higher



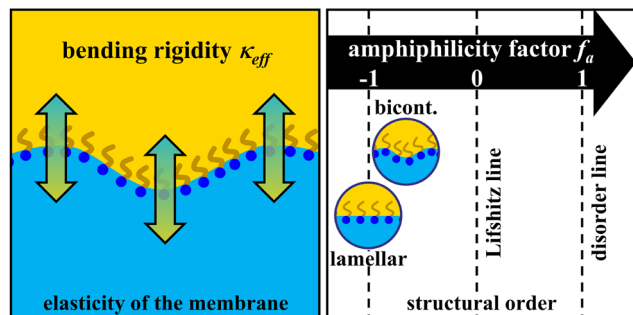


Fig. 1 Left: Schematic illustration of the (effective) bending rigidity κ_{eff} of the surfactant membrane (amphiphilic film). The higher κ_{eff} , the stiffer the membrane. Right: Scale of the amphiphilicity factor between -1 and 1 . Well-structured microemulsions are located at $f_a < -0.6$.⁵³

ratio of $\xi_{\text{TS}}/d_{\text{TS}}$. In this context, a suitable measure for quantifying the influence of propane and pressure on the structural order of the investigated microemulsions is the so-called amphiphilicity factor^{32,53,54}

$$f_a = \frac{c_1}{\sqrt{4a_2c_2}}, \quad (6)$$

which utilizes the order parameter coefficients of the Teubner-Strey model. The main characteristics of the amphiphilicity factor are illustrated in Fig. 1. Disordered solutions with uncorrelated interfaces correspond to more positive f_a values, exceeding the disorder line at $f_a = 1$. Crossing the Lifshitz line at $f_a = 0$ toward negative values corresponds to a change of the sign of the c_1 coefficient and gives rise to the wetting/non-wetting transition of the middle phase microemulsion between the two excess phases as well as the characteristic correlation peak in the scattering profile, located at q_{max} . These negative amphiphilicity factors are found for correlated interfaces, for instance in the case of well-defined microemulsions. The structural order further increases with decreasing f_a , with $f_a = -1$ corresponding to perfectly aligned lamellar sheets.

4 Results and analysis

In the following, we briefly present the most important features of the phase behavior of the investigated extended surfactant microemulsions, serving as the foundation of the subsequent HP-SANS studies. Afterwards, we showcase the scattering profiles obtained from measurements near the respective optimum points. Initial SANS investigations with the microemulsion containing only *n*-decane were performed at the respective pressure-dependent phase inversion temperature. A further set of scattering curves was recorded isothermally as a function of pressure, which was likewise done in the subsequent experiments of the pure propane microemulsion and for two microemulsions containing oil mixtures at different propane-to-*n*-decane ratios. A quantitative analysis utilizing the Teubner-Strey model,³² shown as solid red lines in Fig. 3–6, and Porod's law for diffuse interfaces,^{33,34} represented as dashed blue lines, is provided afterwards. Theoretical foundations are illustrated above and in the ESI.† The analysis is

followed by a comprehensive discussion of the high-pressure data, in which the influence of pressure and propane on the structural order is addressed by the so-called amphiphilicity factor f_a ^{53,54} and their impact on the bending rigidity κ_{eff} of the surfactant monolayer discussed by applying the model of random interfaces.^{44–46}

4.1 Phase behavior

A prerequisite for meaningful studies on the influence of pressure and oil composition on the nanostructure of symmetrical microemulsions is the knowledge of their phase behavior. Detailed $T(\gamma)$ cuts of the D_2O -free microemulsions were measured at constant oil-to-water ratio in one of our recent works,¹⁵ in which we confirmed bicontinuity near the phase inversion temperature through electrical conductivity measurements. Fig. 2 shows the pressure-dependent fish cuts for the microemulsions containing *n*-decane or propane, respectively. The red arrows emphasize the opposite pressure-induced shift of the phase boundaries and the optimum point \tilde{X} . As expected, propane-containing formulations are located at much lower temperatures due to its significantly shorter chain length compared to *n*-decane, although it should be mentioned that the temperature shift for volatile hydrocarbons has been found to be less pronounced than anticipated.^{15,16,55} The value of γ at the \tilde{X} point denotes the minimum surfactant concentration required to form a one-phase microemulsion and thus represents the efficiency of the surfactant mixture to fully solubilize water and oil. As opposed to

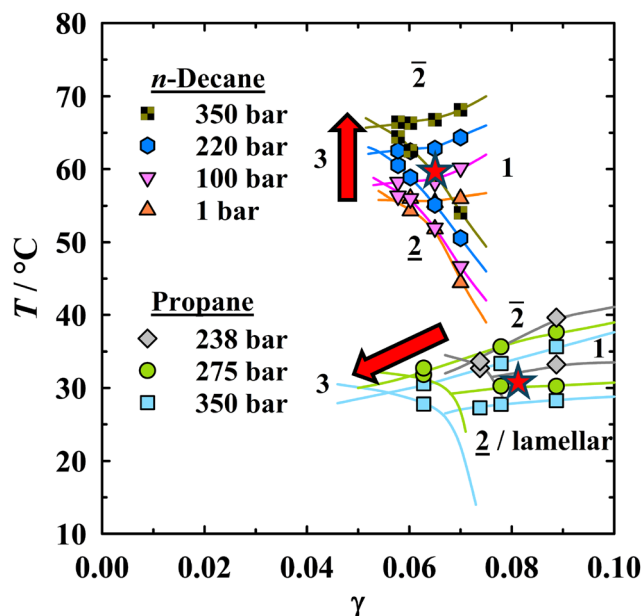


Fig. 2 Influence of pressure on the phase behavior of the microemulsion $\text{H}_2\text{O}/\text{NaCl}/\text{BDG} - n\text{-alkane} - \text{C}_{16-18}\text{-7PO-0.1EO-SO}_4\text{Na}/\text{C}_{14-17}\text{-SO}_3\text{Na}$ containing either *n*-decane or propane. Equal volumes of brine/BDG (salinity of 4.70 wt%) and oil were used. The surfactant ratio is 3:1 (w/w) based on active content. Phase transition temperatures were taken from our previous study.¹⁵ The red arrows indicate the opposite pressure-induced shift of the phase boundaries and \tilde{X} for *n*-decane and propane-rich formulations. Red stars denote the measurement temperature for the isothermal HP-SANS experiments (salinity of 4.37 wt%).

the pure *n*-decane microemulsions, formulations with propane show a pressure-dependent efficiency, explained by the higher compressibility of propane and the related pressure-dependent strength of interactions between propane and the alkyl chains of the surfactant.^{15,56} Considering those weak interactions at low pressures, the limited active content of the commercial surfactants, and that preliminary phase behavior tests indicated a very low solubility of the surfactant mixture in propane at lower pressures, a rather high starting pressure had to be chosen for the propane microemulsion.¹⁵

For the SANS studies, surfactant mass fractions were converted to volume fractions, given that the switch from H₂O to D₂O would otherwise change the volumetric oil-to-water ratio owing to their different densities. All phase transition temperatures with D₂O are compiled in the ESI† (Tables S1–S4). By and large, the influence of pressure and propane on the phase behavior of the D₂O-containing microemulsions corroborates the findings for the D₂O-free systems: pressure shifts phase boundaries upwards for the *n*-decane-rich microemulsions containing 0 and 30 wt% propane. A decrease of the phase transition temperatures is observed for the propane-rich systems with 60 and 100 wt% in the oil phase. The pressure-induced phase boundary shift is less pronounced for the oil mixtures than for the pure alkanes. Furthermore, good agreement between D₂O and H₂O microemulsions regarding the overall temperature range of the phase boundaries is found, with the red stars in Fig. 2 denoting the measurement temperature for the respective isothermal measurements. Small temperature shifts upon deuteration have also been noted by other authors.^{34,36}

4.2 Small-angle neutron scattering

Small-angle neutron scattering was chosen as a powerful, non-destructive technique to obtain information on the length scales of water/oil domains and insights into the impact of pressure and propane on microemulsion nanostructure. SANS experiments discussed in the following were conducted in bulk contrast, setting the highest possible deuteration degree in the hydrophilic component, which was kept constant for all samples. Since all pressure-dependent bulk contrast scattering curves (with one exception discussed later) recorded exhibited isotropic scattering patterns, they were radially averaged over the full azimuthal range to obtain $I(q)$ data. Irrespective of pressure, these scattering curves, which are shown in Fig. 3–6, exhibit certain similar features and trends commonly reported for bicontinuous microemulsions containing comparable amounts of water and oil.

4.2.1 General characteristics. A unique feature of all scattering curves is the pronounced correlation peak defined by the maximum scattering intensity. Toward lower q , the scattering intensity decreases but levels out for $q \rightarrow 0$. Toward higher q , the scattering intensity also decreases, with a weak shoulder occurring at $q \approx 2q_{\text{max}}$ which can be attributed mainly to the influence of multiple scattering, but also thermal fluctuations as well as potential higher-order peak contributions.^{37,41,43,57,58} A detailed discussion on the influence of multiple scattering, including a quantitative analysis using the MuScatt software,^{58,59}

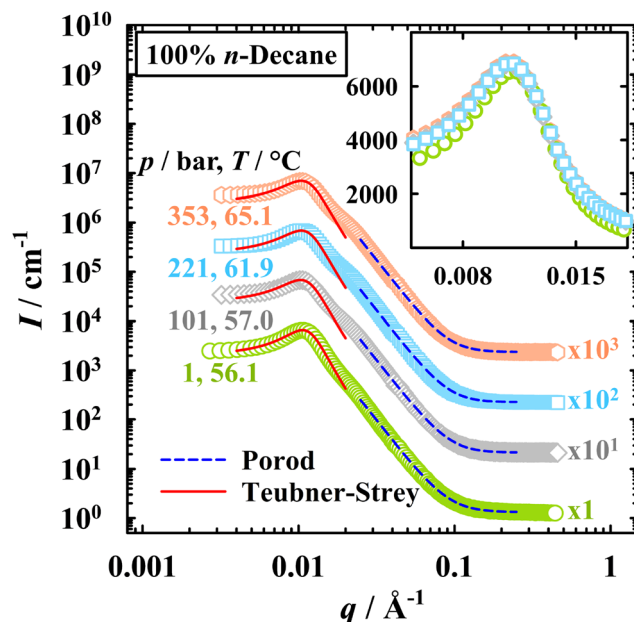


Fig. 3 Pressure-dependent bulk contrast SANS curves for the microemulsion system containing 100 wt% *n*-decane, recorded at $\phi_c = 0.058$ at the respective phase inversion temperature of each pressure. Curves are displaced by a factor of 10 (1 bar unscaled). Peak region analyzed via the Teubner–Strey model³² (red solid lines); high q analyzed with Porod's law, taking into account the diffuseness of the amphiphilic film^{33,34} (blue dashed lines). Inset: Unscaled close-up of the peak region with linear I axis. Fits are omitted for better visibility.

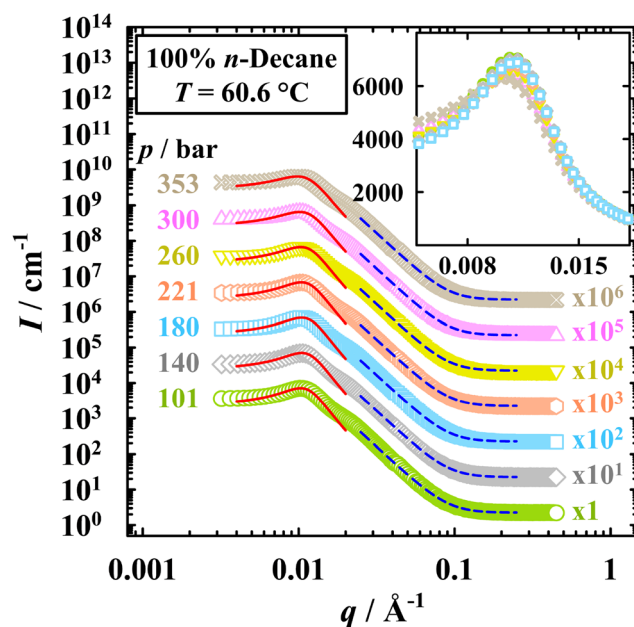


Fig. 4 Pressure-dependent bulk contrast SANS curves for the microemulsion system containing 100 wt% *n*-decane, recorded isothermally at $T = 60.6$ °C and $\phi_c = 0.058$. Curves are displaced by a factor of 10 (101 bar unscaled). Peak region analyzed via the Teubner–Strey model³² (red solid lines); high q analyzed with Porod's law, taking into account the diffuseness of the amphiphilic film^{33,34} (blue dashed lines). Inset: Unscaled close-up of the peak region with linear I axis. Fits are omitted for better visibility.



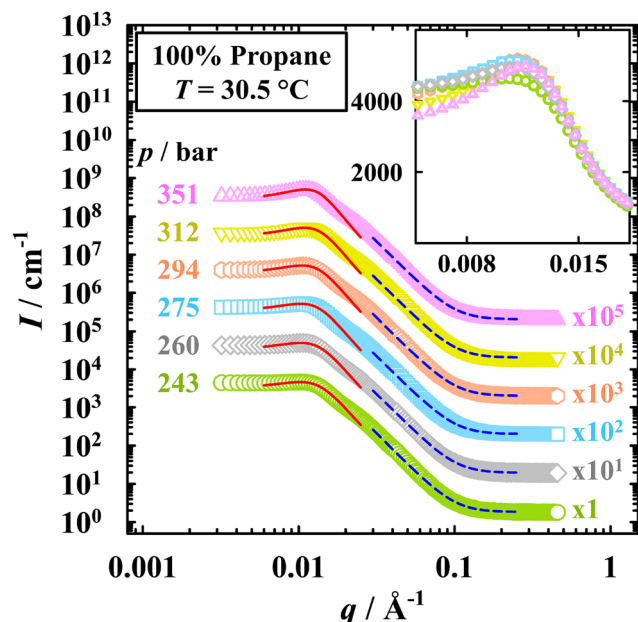


Fig. 5 Pressure-dependent bulk contrast SANS curves for the micro-emulsion system containing 100 wt% propane, recorded isothermally at $T = 30.5\text{ }^{\circ}\text{C}$ and $\phi_C = 0.064$. Curves are displaced by a factor of 10 (243 bar unscaled). Peak region analyzed via the Teubner–Strey model³² (red solid lines); high q analyzed with Porod's law, taking into account the diffuseness of the amphiphilic film^{33,34} (blue dashed lines). The measurement at 200 bar, measured outside of the one-phase region, no longer exhibits the typical features of bicontinuous microemulsions (cf. Fig. S5 and S6, ESI†). Inset: Unscaled close-up of the peak region with linear I axis. Fits are omitted for better visibility.

is provided in the ESI.† The q^{-4} decay at higher q is related to the presence of a specific internal interface in inhomogeneous media, which can be described by Porod's law.³³ Toward the highest experimental q , the scattering intensity levels out, with the remaining intensity resulting from incoherent background scattering I_{incoh} . If the incoherent background is subtracted, the intensity falls off further toward $I \rightarrow 0$, with the decay being even steeper due to the diffuseness of the interfacial film (cf. Fig. S2 and S3, ESI†).³⁴ These distinctive features have also been reported in other works on the nanostructure of bicontinuous microemulsions, both at ambient and high pressure.^{28–30,36,37,43,52,60–62} However, without *a priori* knowledge about the microemulsion structure at specific conditions (e.g., temperature, composition), utilizing SANS as a standalone method might lead to inaccurate assumptions about whether a bicontinuous or droplet-like structure is present.⁶³ Within the scope of the phase behavior studies, given that electrical conductivity measurements confirmed the transition from water- to oil-continuity and that the SANS specimens are prepared using equal volumes of water and oil near the \tilde{X} point, where countless studies have confirmed that the structure is indeed bicontinuous, bicontinuity can be presumed for all experiments, even if there might be slight deviations from a state of zero mean curvature.

4.2.2 *n*-Decane microemulsions. We first investigated the pressure dependence of the nanostructure by means of the microemulsion containing *n*-decane as the oil. For the first set

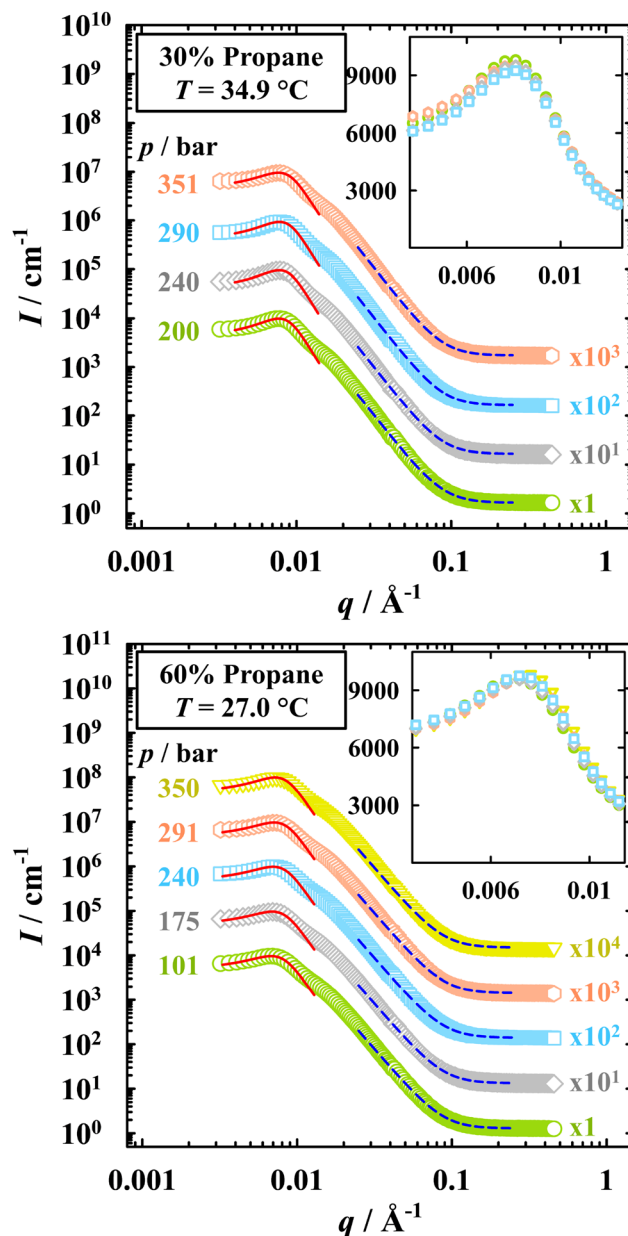


Fig. 6 Pressure-dependent bulk contrast SANS curves for the micro-emulsion system containing (top) 30 wt% propane, recorded isothermally at $T = 34.9\text{ }^{\circ}\text{C}$ and $\phi_C = 0.042$, and (bottom) 60 wt% propane, recorded isothermally at $T = 27.0\text{ }^{\circ}\text{C}$ and $\phi_C = 0.039$. Curves are displaced by a factor of 10 (lowest pressure unscaled). Peak region analyzed via the Teubner–Strey model³² (red solid lines); high q analyzed with Porod's law, taking into account the diffuseness of the amphiphilic film^{33,34} (blue dashed lines). Inset: Unscaled close-up of the peak region with linear I axis. Fits are omitted for better visibility.

of measurements, which also includes the ambient pressure reference measurement, temperature was set close to the respective pressure-dependent phase inversion temperature \tilde{T} , which was found to increase with increasing pressure by approximately 3 K per 100 bar, as visible from Fig. 2.¹⁵

Fig. 3 reveals only negligible changes in the scattering data when pressure is increased from 101 bar to 353 bar at the respective \tilde{T} , with minor differences compared to the 1 bar



measurement performed in a Hellma cuvette. For all pressures, the peak position remains nearly unchanged, indicating that pressure does not significantly affect the size of the water and oil domains. Within experimental and analytical error, the periodicity d_{TS} , obtained from the analysis with eqn (2), is constant with $d_{TS} = (571 \pm 6) \text{ \AA}$ (cf. Table 1). This observation is readily explained by the weak compressibility of water and *n*-decane, illustrated in Fig. S1 (ESI†). Similarly, a nearly pressure-independent radius was reported for water-in-decane droplet microemulsions.^{17,18} A close-up of the peak region, shown in the inset of Fig. 3, demonstrates that the SANS data are almost in quantitative agreement with regard to their forward and maximum scattering intensity, I_0 and I_{\max} . Consequently, the sharpness of the correlation peak is likewise unaffected by pressure, as is thus the correlation length ξ_{TS} .

The somewhat higher I_0 and I_{\max} at elevated pressures, which lead to a broader peak than for the 1 bar measurement, are explained by stronger multiple scattering contributions due to the higher sample thickness of the high-pressure SANS cell (2 mm) compared to the Hellma cell (1 mm). This is also visible in the more pronounced shoulder at $q \approx 2q_{\max}$, which affects the intensity of the high q data. Thus, the differences in the value of the specific internal interface, which is $S/V = (5.3 \pm 0.5) \times 10^{-3} \text{ \AA}^{-1}$ for the 1 bar measurement but $S/V = (6.3 \pm 0.6) \times 10^{-3} \text{ \AA}^{-1}$ for all higher pressures, indicate that the obtained absolute values of S/V should be taken with caution. This is further addressed in the ESI,† including a quantitative analysis *via* the MuScatt software, which could make the “true” absolute value of S/V accessible. Especially the 2 mm sample thickness could render a correction essential given that the low sample transmission (T_{sample} between 0.19 and 0.32); nonetheless, in the main part of the manuscript, we decided to analyze the original 1D scattering curves obtained *via* GRASP from the raw detector data in order to avoid systematic errors. In principle, multiple scattering corrections can be highly useful to maintain comparability under different conditions (sample thickness, wavelength, instrument) and to generate “real” values by eliminating the impact of multiple scattering, which in our case particularly affects I_0 – and thus ξ_{TS} , κ_{eff} and f_a – as well as S/V (cf. discussion in the ESI†). Nevertheless, it is crucial but arguably difficult to ensure that treated data are entirely free of multiple scattering contributions; otherwise, data integrity may be compromised if the fine line between methodical data treatment and questionable data manipulation blurs.

The previous SANS measurements show that the nanostructure of the bicontinuous *n*-decane microemulsion remains almost unchanged near the respective \tilde{T} , regardless of pressure. In the second set of experiments, a constant temperature of 60.6 °C was set, corresponding to \tilde{T} of an intermediate pressure (roughly 180 bar) and conveniently allows to study the impact of pressure isothermally without leaving the one-phase region. The scattering curves shown in Fig. 4 reveal that the peak position and therefore d_{TS} are once more nearly unaffected by pressurization. However, quantitative differences are observed in the low q region, where the forward scattering intensity I_0 and maximum scattering intensity I_{\max} are pressure-dependent. Initially, I_0 decreases with pressure before it increases again,

whereas I_{\max} consistently decreases. Thus, a similar peak sharpness is observed for the lower pressures, while higher pressures exhibit a broader peak. Accordingly, the correlation length ξ_{TS} remains almost constant up to a pressure of 221 bar, *i.e.*, close to where the set temperature corresponds to \tilde{T} , and further decreases considerably with increasing pressure. For these isothermal measurements, a pressure-induced shift away from the phase inversion temperature and thus to a slightly curved structure leads to a less pronounced correlation peak, characterized by a decreasing correlation length. From the analysis of the high q data, a pressure-independent specific internal interface of $S/V = (6.3 \pm 0.9) \times 10^{-3} \text{ \AA}^{-1}$ is found within measurement uncertainty, the same as when studied at the respective phase inversion temperature.

4.2.3 Propane microemulsions. Replacing *n*-decane with the volatile, short-chain propane shifts the phase boundaries to lower temperatures and further affects the pressure-dependent solubilization efficiency.¹⁵ Due to the interference of the lamellar phase (cf. Fig. 2), the pressure-dependent efficiency, the time-consuming experimental routine – around 8 h for sample preparation, measurement, cell-cleaning and phase boundary checks – as well as the limited beam time, we studied the effect of pressure on the nanostructure of propane microemulsions *via* isothermal SANS experiments recorded at $T = 30.5 \text{ °C}$ and $\phi_C = 0.064$, instead of measuring at \tilde{T} .

As shown in Fig. 5, the SANS profiles qualitatively resemble those of the *n*-decane microemulsion. Due to the limited surfactant active content, the low solubility of the surfactant mixture in propane at low pressures, as well as their concomitant weak interactions,⁵⁶ 243 bar was chosen as the starting pressure, as done in the phase behavior studies (cf. Fig. 2).¹⁵ Intriguingly, the peak position is again almost unaffected by pressure, with the periodicity d_{TS} remaining constant at approximately $(526 \pm 10) \text{ \AA}$ – albeit with a slight decrease toward higher pressures. The exact values are listed in Table 1. Given that the volatile propane is more compressible than *n*-decane, this finding appears somewhat counterintuitive. However, the overall density changes in the investigated temperature and pressure range only lead to minor deviations of the actual volumetric water-to-oil ratio of the specimen (cf. Fig. S1, ESI†); consequently, there is no strong trend in the periodicity. For other compressible oils, Eastoe *et al.* likewise report an almost pressure-independent radius of water-in-propane,^{21,23} water-in-*n*-butane,²² and water-in-CO₂ droplets.²⁴ In contrast, a change in the water content of these w/o structures unsurprisingly affects the droplet size.^{22,24} More notable variations of the droplet radius under applied pressure were only observed for water-in-propane droplets stabilized by the non-ionic surfactant C₁₂E₅ as well as balanced CO₂ microemulsions stabilized by fluorinated surfactants, which was in both cases explained by the pressure-dependent monomeric solubility of the surfactant.^{21,30} For the ionic surfactants used in this work, only a very small monomeric solubility in propane is expected, irrespective of pressure.

In the low q part, a rising pressure leads to a lower forward scattering intensity as well as a higher maximum scattering intensity and therefore a sharper peak. As a consequence, the



Table 1. Pressure- and temperature-dependent periodicity d_{TS} , correlation length ξ_{TS} and amphiphilicity factor f_a , determined via the Teubner–Strey model,³² alongside the effective bending rigidity κ_{eff} ,^{44,46} for all investigated microemulsions. Specific internal interface S/V determined via Porod's law, considering the diffuseness of the interface t .^{33,34} Geometric prefactor a determined via eqn (7). Relative errors are estimated as $\Delta d_{TS}/d_{TS} = 0.02$, $\Delta \xi_{TS}/\xi_{TS} = 0.03$, $\Delta f_a/f_a = 0.015$, $\Delta \kappa_{eff}/\kappa_{eff} = 0.035$, $\Delta(S/V)/(S/V) = 0.1$, $\Delta t/t = 0.1$, $\Delta a/a = 0.1$

Oil composition	ϕ_C	p/bar	$T/^\circ\text{C}$	$d_{TS}/\text{\AA}$	$\xi_{TS}/\text{\AA}$	f_a	$\kappa_{eff}/k_B T$	$S/V/10^{-3} \text{\AA}^{-1}$	$t/\text{\AA}$	a
100 wt% <i>n</i> -decane	0.058	1 ^a	56.1	565	295	−0.83	0.44	5.3	4.0	6.0
		101	57.0	576	279	−0.80	0.41	6.3	5.0	7.2
		221	61.9	571	278	−0.81	0.41	6.3	5.2	7.2
		353	65.1	570	273	−0.80	0.41	6.3	5.3	7.2
100 wt% <i>n</i> -decane	0.058	101	60.6	577	284	−0.81	0.42	6.0	5.5	6.9
		141	60.6	568	278	−0.81	0.42	6.2	5.5	7.0
		180	60.6	569	280	−0.81	0.42	6.3	5.8	7.2
		221	60.6	571	278	−0.81	0.41	6.3	5.5	7.2
		260	60.6	574	269	−0.80	0.40	6.4	6.0	7.3
		300	60.6	577	255	−0.77	0.38	6.4	6.0	7.4
		353	60.6	592	246	−0.74	0.35	6.5	6.0	7.7
		200	34.9	758	325	−0.76	0.36	5.0	4.5	7.6
30 wt% propane, 70 wt% <i>n</i> -decane	0.042	240	34.9	754	328	−0.76	0.37	5.0	5.5	7.5
		290	34.9	753	322	−0.76	0.36	5.2	5.5	7.8
		351	34.9	754	303	−0.73	0.34	5.1	5.0	7.7
60 wt% propane, 40 wt% <i>n</i> -decane	0.039	101	27.0	839	318	−0.70	0.32	4.6	4.5	7.7
		175	27.0	828	316	−0.70	0.32	4.7	4.5	7.8
		240	27.0	820	320	−0.71	0.33	4.7	4.0	7.7
		291	27.0	810	318	−0.72	0.33	4.8	4.5	7.8
		350	27.0	803	326	−0.73	0.35	4.8	4.5	7.7
100 wt% propane	0.064	243	30.5	527	162	−0.58	0.26	8.0	5.5	8.4
		260	30.5	530	170	−0.61	0.27	8.0	5.0	8.5
		275	30.5	534	176	−0.62	0.28	7.8	5.0	8.3
		294	30.5	529	181	−0.64	0.29	7.8	4.8	8.3
		312	30.5	516	185	−0.67	0.30	7.8	4.8	8.1
		351	30.5	518	197	−0.70	0.32	7.8	5.0	8.1

^a 1 bar measurement recorded in a Hellma cuvette.

correlation length systematically increases by roughly 20% from $\xi_{TS} = 162 \text{ \AA}$ to 197 \AA within just a little more than 100 bar, in contrast to the trend observed for *n*-decane microemulsions.

In our previous phase behavior studies with propane, we observed demixing when moving to lower pressures, even at higher surfactant concentrations,¹⁵ which could be confirmed when recording phase boundaries for the HP-SANS investigations presented here. We hypothesized that there might be a coexistence of a lamellar phase together with another phase below the lower phase boundary. Therefore, we recorded an additional SANS measurement at 200 bar, shown in Fig. S5 (ESI†). This dataset was excluded from the analysis because its scattering profile no longer exhibits the typical correlation peak at q_{max} , instead showing an increasing forward scattering intensity towards $q \rightarrow 0$ and two smaller local peaks at intermediate q . Even though those peaks are only weakly pronounced, scattering pattern, shown in Fig. S6 (ESI†), and scattering curve give rise to the assumption that a transition towards a lamellar phase has indeed taken place. The presence of such a lamellar phase below the lower phase boundary in gas-rich microemulsions with non-ionic behavior has also been proposed by different authors.⁶⁴ In the ESI†, a detailed discussion of the anisotropic scattering pattern at 200 bar as well as the isotropic scattering patterns of two higher pressures is provided in Fig. S6 (ESI†) by means of an azimuth-dependent analysis of the scattering intensities ($I(\chi)$). To briefly summarize the most important findings, we found that the scattering intensity of the isotropic scattering patterns is unsurprisingly χ -independent, whereas the anisotropic scattering pattern reveals

two intensity peaks in close proximity to 90° and 270° (cf. Table S6, ESI†), proving the presence of lamellar sheets stacked perpendicular to the plane defined by neutron path and z axis. Given that lower pressures limit the solubilization capacity of propane, we assume that this lamellar phase coexists with some oil-rich phase. Consequently, our observations can be attributed to demixing of the sample due to a pressure-induced phase behavior shift outside the one-phase region, whose width was shown to be pressure-dependent for propane-rich microemulsions even at a constant surfactant concentration.¹⁵

4.2.4 *n*-Decane/propane microemulsions. With the two investigations of *n*-decane-free and propane-free microemulsions at hand, the question arises if and how the pressure-dependent scattering profile changes for *n*-decane/propane mixtures. Oil mixtures containing 30 and 60 wt% of propane were thus studied, matching the oil compositions of the phase behavior studies of the H_2O microemulsions.¹⁵ Given that the phase boundaries of the oil mixtures are less affected by pressure, the pressure variation only leads to minor changes of the respective phase inversion temperature. Thus, isothermal high-pressure SANS studies were conducted at 34.9°C (30 wt% propane) and 27.0°C (60 wt% propane), respectively, shown in Fig. 6.

As anticipated, observing an almost unchanged peak position highlights that the periodicity is nearly unaffected by pressure, albeit with a slight decrease of d_{TS} in the propane-rich mixture. Note that in our previous work, we found a higher solubilization efficiency for the microemulsions containing oil



mixtures compared to those with the pure oils.¹⁵ While it is known that the solubilization efficiency of surfactants generally decreases with increasing (non-gaseous) oil chain length,^{62,65,66} the pressure-dependent propane-surfactant tail interactions limit the solubilization potential and yield an efficiency drawback at low pressures. Therefore, the optimum point is located at different surfactant concentrations and we thus need to adjust the surfactant volume fraction ϕ_C to stay in proximity to it. Due to the lower ϕ_C set for the two oil mixtures compared to the pure *n*-decane and propane formulations, the domain sizes are therefore significantly larger, with d_{TS} close to (30 wt% propane) or even above (60 wt% propane) 800 Å. The influence of pressure on peak sharpness and forward scattering intensity is likewise weak and, as expected, somewhat stronger for the formulation with a higher proportion of propane in the oil mixture, which exhibits an increasing peak sharpness under pressurization, as was previously observed for the pure propane microemulsion. The fact that the shoulder at $q \approx 2q_{max}$ appears more prominent for the mixtures confirms an increased multiple scattering contribution due to the stronger scattering caused by larger water/oil domains.

5 Discussion

In this chapter, the influence of propane on the pressure-dependent nanostructure of the investigated microemulsions is discussed in a more general context. We begin by examining whether the prefactor of geometric models of the bicontinuous structure^{67,68} depends on pressure and the propane-to-*n*-decane ratio. Subsequently, we discuss the impact of the aforementioned parameters on the effective bending rigidity κ_{eff} of the surfactant monolayer and on the amphiphilicity factor f_a , which characterizes the structural order of the microemulsion.

5.1 Geometric prefactor of bicontinuous structures

As expected for bicontinuously structured microemulsions, our data analysis clearly shows the inverse proportionality of periodicity and surfactant volume fraction ($d_{TS} \propto \phi_C^{-1}$). In the ESI,[†] this is addressed quantitatively by introducing a normalized periodicity, with Fig. S4 (ESI[†]) proving that changes in d_{TS} can be fully explained by a variation of ϕ_C , further highlighting the low monomeric solubility of the surfactant mixture in both oil and water.

Geometric models of the bicontinuous structure^{67,68} predict that its periodicity d_{TS} is inversely proportional to the specific internal interface S/V according to

$$d_{TS} = 2a \frac{\phi(1-\phi)}{S/V} \quad (7)$$

with geometric prefactors of 5.84 (modeled by a Voronoi tessellation)⁶⁷ and 6 (cubic domains),⁶⁸ while a value of 7.16 was found experimentally.³⁶ An ideal lamellar structure with planar membranes would yield a value of 4.⁶⁹ Given that the symmetric microemulsions contain equal volumes of water and oil ($\phi = 0.5$) the geometric prefactor $a = 2d_{TS}S/V$ can be

determined directly using the d_{TS} and S/V obtained from the SANS data analysis.

In Fig. 7, the determined geometric factors are plotted as a function of pressure for the bicontinuous microemulsions containing different propane-to-*n*-decane ratios. All values are compiled in Table 1. Interestingly, pressure has a minor effect on a for each of the studied microemulsions, which can be explained by the small pressure-induced volume contraction, even for propane-rich specimens. Therefore, the values obtained for the *n*-decane microemulsion are close to the value of $a = 7.16$ (red long dashes) determined for bicontinuous non-ionic model microemulsions.³⁶ With an increasing amount of propane in the sample, the value of the geometric prefactor a increases, with $a > 8$ for the microemulsion containing only propane as the oil. One reason for this interesting systematic trend could be the increasing disorder observed with increasing propane content, which will be further addressed in terms of the amphiphilicity factor later. In Fig. 7, we omitted the value for the *n*-decane microemulsion at 1 bar because the impact of multiple scattering in the Hellma cuvette ($d = 1$ mm) is distinctly lower than for the measurements in the high-pressure cell ($d = 2$ mm), even though it exactly matches $a = 6$ as predicted by de Gennes. Utilizing the MuScatt software to mitigate the impact of multiple scattering, we still observe an increase of the prefactor with increasing propane concentration, albeit somewhat less pronounced. As listed in Table S5 in the ESI,[†] the values of a are around 20% lower, ranging between 5.0 and 6.4.

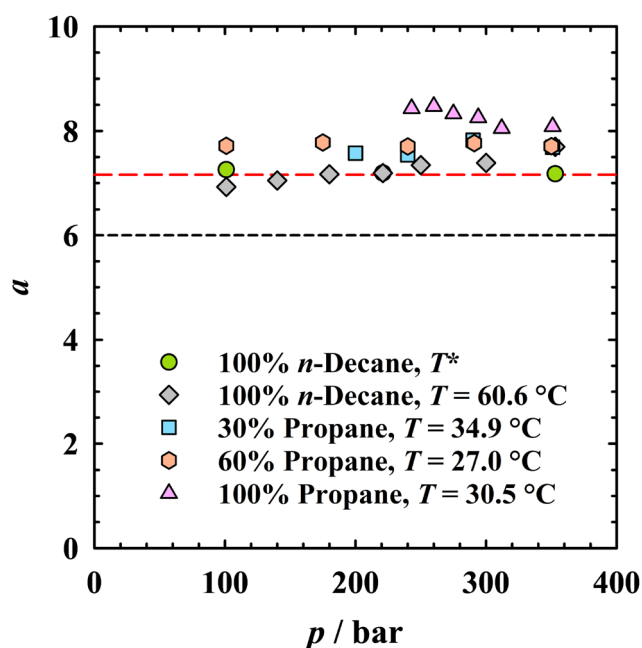


Fig. 7 Geometric prefactor $a = 2d_{TS}S/V$ as a function of pressure for the studied symmetric bicontinuous microemulsions. The black short dashes denote $a = 6$, as theoretically predicted by de Gennes and Taupin.⁶⁸ Red long dashes denote $a = 7.16$, as experimentally determined by Sottmann *et al.*³⁶ The 1 bar measurement is omitted due to a non-comparable impact of multiple scattering in the 1 mm Hellma cuvette.



5.2 Bending rigidity and amphiphilicity factor

The trends observed for the nanostructure of bicontinuous microemulsions as a function of pressure and the propane-to-*n*-decane ratio should be attributable, at least qualitatively, to the influence of these two parameters on the amphiphilic film. Thus, we utilize Gompper *et al.*'s modification of the random interface model developed by Pieruschka and Safran^{44–46} to determine the effective bending rigidity κ_{eff} via eqn (5) and further quantify the amphiphilicity factor via eqn (6) as a measure for the order of the bicontinuous structure (see SANS analysis chapter and Fig. 1 for details). All values of κ_{eff} and f_a are compiled in Table 1 and visualized in Fig. 8 as a function of pressure.

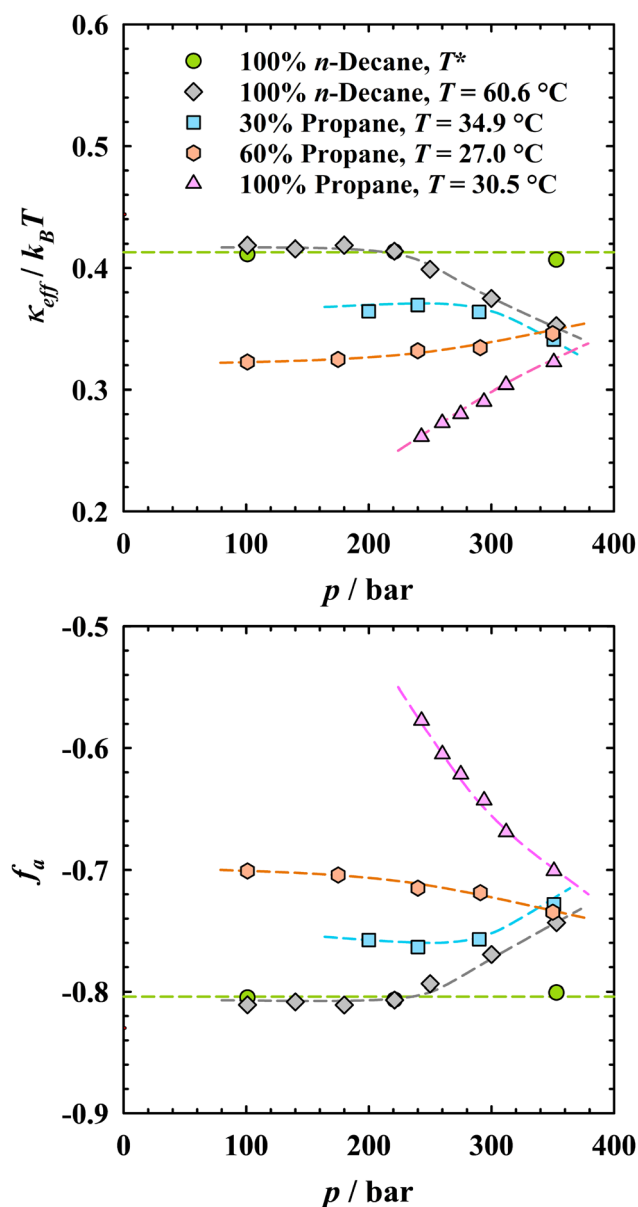


Fig. 8 Pressure dependence of effective bending rigidity κ_{eff} (top) and amphiphilicity factor f_a (bottom) for the investigated microemulsions. Dashed lines to guide the eye. The 1 bar measurement is omitted due to the lower impact of multiple scattering in the 1 mm Hellma cuvette.

Starting with the *n*-decane microemulsions studied at the respective phase inversion temperatures, the pressure independence of d_{TS} and ξ_{TS} leads to a pressure-independent $\kappa_{\text{eff}} \approx 0.41k_{\text{B}}T$, shown in Fig. 8 as green circles. Note that for many well-structured bicontinuous microemulsions, $d_{\text{TS}}/\xi_{\text{TS}} \approx 2$, and similar values of κ_{eff} are thus found at their respective \tilde{X} point, independent of the oil and the alkyl chain length of the surfactant.^{36,62} This is because the higher rigidity of monolayers formed by longer-chain surfactants is compensated by the stronger thermal fluctuations inherent in the larger structures.^{36,44,70} The amphiphilicity factor of $f_a \approx -0.81$ (cf. bottom plot in Fig. 8) indicates a well-structured microemulsion according to the notion of Schubert *et al.*⁵³ This pressure independence is explained by the small temperature changes and the weak compressibility of *n*-decane, and can likewise be anticipated when considering the counteracting influences of temperature and pressure on the bending rigidity as well as macroscopic phase behavior (cf. Fig. 2). Similar findings have been reported in literature, independent on the nature of the surfactant.^{17–19}

Moving to the isothermal measurements at 60.6 °C (gray diamonds in Fig. 8), κ_{eff} and f_a for all pressures up to 221 bar match the values determined from the analysis at the respective pressure-dependent phase inversion temperature (green circles). As pressure is increased further, κ_{eff} decreases slightly, accompanied by a slightly less negative value of f_a , which could be due to the formation of less ordered, elongated structures that are typically present when moving slightly away from \tilde{T} .

For the bicontinuous propane microemulsions, the effective bending rigidity systematically increases from $\kappa_{\text{eff}} = 0.26$ to $0.32k_{\text{B}}T$ within just a little more than 100 bar (pink triangles in Fig. 8). Even at the highest pressure, κ_{eff} is clearly lower than in the *n*-decane microemulsions. A possible explanation for the generally smaller κ_{eff} values and their pressure trend could be related to the lower density of propane, which however noticeably increases with pressure and thus results in stronger pressure-dependent interactions between propane molecules and the alkyl chains of the surfactant. Similarly, a slight increase of the bending rigidity with pressure was found in bicontinuous water/ CO_2 microemulsions stabilized by a commercial fluorinated non-ionic surfactant.^{29,30} In line with these results, the amphiphilicity factor f_a becomes increasingly negative with rising pressure, from -0.58 at 243 bar to -0.70 at 351 bar. In summary, the impact of pressure on the properties of the amphiphilic film in propane microemulsions is considerably stronger than for formulations with the incompressible *n*-decane, whose structural order can no longer be reached, even at the highest investigated pressure.

Attempting a deeper physicochemical understanding of the influence of propane on κ_{eff} based on these observations, we propose that the small and more diffusive propane molecules can interpenetrate the surfactant tails more easily compared to *n*-decane, which increases the local disorder and disrupts tail-tail interactions, leading to a softening of the surfactant monolayer and a reduction of κ_{eff} . Considering further the entropic effect, the vastly different number of molecules per volume unit



could offer more degrees of freedom and hence explain stronger fluctuations of the amphiphilic film in the presence of propane.^{20,71}

For the two microemulsions containing mixtures of *n*-decane and propane, Fig. 8 demonstrates that amphiphilicity factors as well as effective bending rigidities lie in between those of the pure alkane microemulsions. For the *n*-decane-rich mixture (blue squares), κ_{eff} remains almost constant at low and intermediate pressures. However, as in the case of the *n*-decane microemulsion, a decrease in κ_{eff} is observed at the highest pressure, which can again be explained by the increasing distance from \tilde{T} . This trend is corroborated by the pressure dependence of f_a . Increasing the propane content to 60 wt% (coral hexagons) leads to a further softening of the surfactant monolayer. With increasing pressure, κ_{eff} now consistently increases, as found for the pure propane microemulsion. The reason for the weaker increase compared to the pure propane formulation is that the microemulsion with the oil mixture is less compressible, which leads to a lower pressure dependence of the oil-surfactant tail interactions and thus to a smaller change in the nanostructural properties.⁵⁶

5.3 Generalizing the influence of pressure and propane on microemulsion nanostructure

The findings discussed above show how the pressure and the propane-to-*n*-decane ratio systematically affect the bending rigidity of the surfactant film and the order of the bicontinuous nanostructure. It shall be emphasized that these are no run-of-the-mill SANS experiments, but instead rely on time-consuming procedures that allow only for limited experiments during the allocated beam time. We thus summarize the insights into the influence of pressure and propane by interpolating and extrapolating bending rigidity and amphiphilicity factor for currently non-explored measurement conditions, visualized as heat maps. These were calculated *via* second-order polynomials using the isothermal measurement data (*cf.* Table 1). Thus, the trends of κ_{eff} and f_a illustrated by the heat maps correspond to bicontinuous microemulsions having their respective phase inversion temperature at an intermediate pressure for a given oil ratio.

Fig. 9 (top) demonstrates that κ_{eff} systematically reduces when *n*-decane is replaced by the more compressible propane. With an increasing amount of propane, the sensitivity of the amphiphilic film to pressure changes is significantly enhanced. Similar observations can be made for the amphiphilicity factor f_a , shown in the bottom part of Fig. 9. The structural order decreases in propane-rich formulations; however, pressure becomes more decisive and can lead to a significantly higher structural order. Higher pressures could not be investigated due to limitations of the experimental setup, but it stands to reason that the impact of the nature of the oil on the structural order of the microemulsion becomes less crucial when pressure is elevated further. On the other hand, Fig. 9 demonstrates that a combination of low pressures and high propane proportions leads to weakly structured mixtures, although one should keep in mind the uncertainty of extrapolations outside the measurement range toward experimentally inaccessible pressures and temperatures.

The similarity of the heat maps emphasizes that the rigidity of the amphiphilic monolayer is governed by the same factors as the overall structural order of the microemulsion. Expressed from a different perspective, a more rigid monolayer is able to form a well-structured microemulsion. Increasing the proportion of propane in the oil mixture hence always leads to a softening of the amphiphilic film and a loss of structural order. However, the exact impact strongly depends on pressure. At high pressures, the influence of the propane concentration is smaller because the

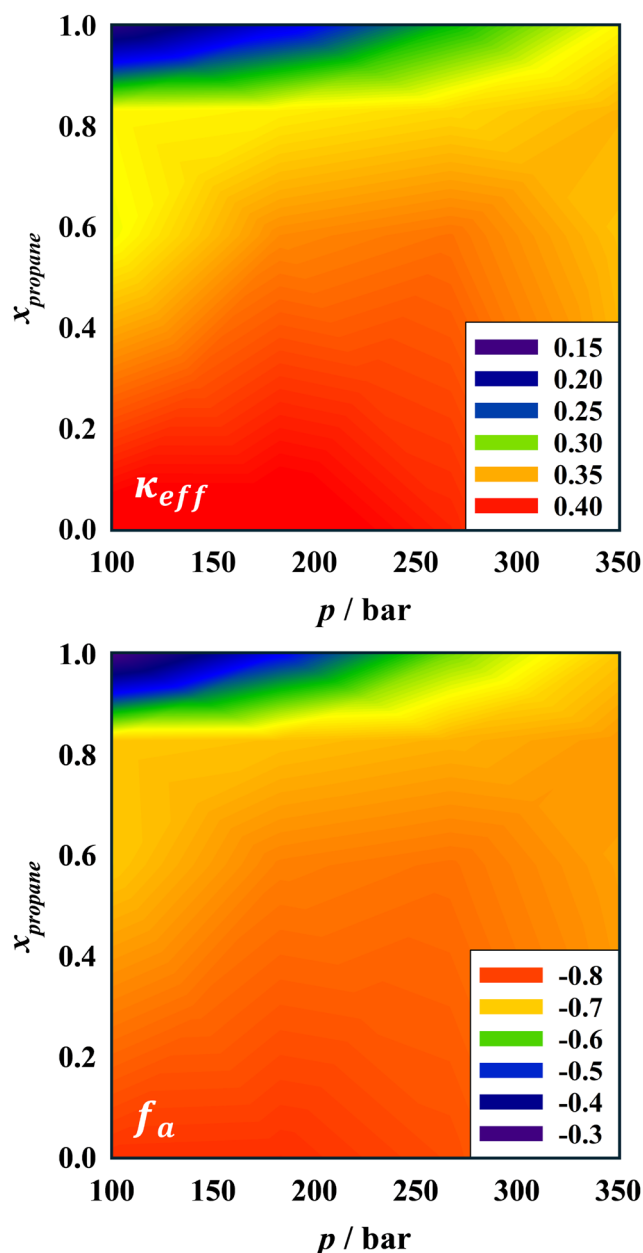


Fig. 9 Heatmaps of the influence of pressure and the propane-to-*n*-decane ratio on the (top) effective bending rigidity κ_{eff} and (bottom) the amphiphilicity factor f_a of bicontinuous microemulsions exhibiting their respective phase inversion temperature at an intermediate pressure for a given oil ratio. The values were inter- and extrapolated *via* second-order polynomials utilizing the respective isothermal measurement data.



interaction strength between surfactant tails and the compressible propane is significantly enhanced⁵⁶ and thus only moderately weaker compared to the surfactant tail-*n*-decane interactions. At low pressures, these interactions are essentially unchanged for the incompressible *n*-decane but substantially weakened for propane. As discussed in our recent work, it was postulated that these altered interactions and their relative magnitude explain changes in curvature as well as the pressure-(in)dependent solubilization capacity of propane (*n*-decane) microemulsions.¹⁵ The high-pressure SANS studies strongly corroborate that this further holds true for the nanostructure of these microemulsions.

6 Conclusions

Even though microemulsions containing volatile alkanes play a central role for instance in chemical-enhanced oil recovery, where the use of microemulsions can improve the exploitation of existing crude oil reservoirs, studies of their properties are scarce. Just recently, we found that the pressure-dependent phase behavior of application-relevant microemulsions of the type H₂O/NaCl/butyldiglycol - *n*-decane/propane - C₁₆₋₁₈-7PO-0.1EO-SO₄Na/C₁₄₋₁₇-SO₃Na strongly depends on the oil used in the microemulsion.¹⁵ Motivated by this intriguing result and the lack of studies on the pressure dependence of the nanostructure of bicontinuous microemulsions containing short-chain alkanes, we performed pressure-dependent bulk contrast small-angle neutron scattering experiments on this type of microemulsions near the respective \bar{X} points.

Scattering curves obtained by radial averaging of the recorded isotropic scattering signals showed a pronounced correlation peak, followed by a $q^{-4} \exp(-q^2 t^2)$ decay according to Porod's law for diffuse interfaces, from which the specific internal interface S/V could be obtained. Despite the noticeable impact of multiple scattering, they exhibit the typical features of symmetrical microemulsions with equal amounts of water and oil being studied close to the phase inversion, where a bicontinuous structure can be expected. Accordingly, the correlation peak was analyzed by means of the Teubner-Strey model, from which two length scales, periodicity d_{TS} and correlation length ξ_{TS} , were obtained, further enabling the determination of the amphiphilicity factor f_a and the effective bending rigidity κ_{eff} of the amphiphilic film.

Studying *n*-decane microemulsions at the respective pressure-dependent phase inversion temperature revealed that the bicontinuous nanostructure is virtually unaffected by pressure due to the weak compressibility of *n*-decane and its nearly pressure-independent interactions with the surfactant. Instead, isothermal measurements showed that a pressure-induced shift away from the phase inversion and thus to a structure with small curvature around water or oil leads to a slightly less pronounced correlation peak, characterized by a decreasing correlation length.

For the pure propane microemulsion investigated at constant temperature, the overall structural order was found to be markedly lower compared to the *n*-decane microemulsion.

While the periodicity turned out to be nearly pressure-independent, the correlation length significantly increased with pressure. Concomitantly, the increase of κ_{eff} indicates a more rigid amphiphilic film due to amplified interactions of the compressible propane with the surfactant tails under pressure. Mixtures of *n*-decane and propane showed intermediate behavior with f_a and κ_{eff} in between those obtained for the pure microemulsions, proving that an increasing concentration of the volatile alkane leads to a reduction of the structural order of the bicontinuous microemulsions, while the pressure dependence steadily increases.

Despite confirming the inverse relationship between periodicity and surfactant volume fraction irrespective of the propane-to-*n*-decane ratio and pressure, it was found by using the d_{TS} and S/V values obtained from the SANS data analysis that the geometric prefactor a of models describing the bicontinuous structure increases from slightly above 7 for *n*-decane microemulsions, matching the experimentally determined a for non-ionic bicontinuous microemulsions,³⁶ to $a > 8$ for propane microemulsions, which is most likely due to the increased consumption of amphiphilic film owing to the increasing disorder.

Utilizing the MuScatt software, it was quantified in the ESI† that the values of ξ_{TS} , S/V , a and f_a are systematically influenced due to multiple scattering. While such a correction could help maintaining comparability under different conditions, original data analysis was prioritized to ensure methodical data reduction in order to guarantee data integrity. In order to elucidate in detail how absolute intensities and the shoulder are affected by multiple scattering, thermal fluctuations, domain size and sample thickness, future systematic studies at high and constant transmission using adjustable sample thickness could be envisioned.

Thus, the findings obtained from our high-pressure SANS experiments proved that the impact of pressure-dependent interactions between (non-)volatile hydrocarbons and surfactant tails is not limited to changes of the macroscopic phase behavior, but likewise affects the nanostructure of the microemulsion. Future studies could target the highly compressible ethane or methane. Expecting weaker interaction strengths with the surfactant tails, it is assumed that such microemulsions would exhibit an even stronger influence of pressure on their nanostructure.

Author contributions

Maximilian Krappel: formal analysis, investigation, visualization, writing – original draft. Christian Bittner: conceptualization, resources. Ralf Schweins: methodology, resources. Thomas Sottmann: conceptualization, investigation, methodology, resources, writing – original draft.

Data availability

Raw scattering data are available under <https://doi.org/10.5291/ILL-DATA.9-10-1745>.³⁸ Further data supporting this article have been included as part of the ESI.†



Conflicts of interest

There are no conflicts to declare.

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Notes and references

- 1 K. Shinoda and S. Friberg, *Adv. Colloid Interface Sci.*, 1975, **4**, 281–300.
- 2 C. Huh, *J. Colloid Interface Sci.*, 1979, **71**, 408–426.
- 3 R. Aveyard, B. P. Binks, S. Clark and J. Mead, *J. Chem. Soc., Faraday Trans.*, 1986, **82**, 125.
- 4 T. Sottmann and R. Strey, *J. Chem. Phys.*, 1997, **106**, 8606–8615.
- 5 W. Jahn and R. Strey, *J. Phys. Chem.*, 1988, **92**, 2294–2301.
- 6 R. Strey, *Colloid Polym. Sci.*, 1994, **272**, 1005–1019.
- 7 *Improved Oil Recovery by Surfactant and Polymer Flooding*, ed. D. O. Shah and R. S. Schechter, Academic Press, New York, 1977.
- 8 B. K. Paul and S. P. Moulik, *Curr. Sci.*, 2001, **80**, 990–1001.
- 9 M. Schwarze, T. Pogrzeba, I. Volovych and R. Schomäcker, *Catal. Sci. Technol.*, 2015, **5**, 24–33.
- 10 E. J. Acosta, J. H. Harwell, J. F. Scamehorn and D. A. Sabatini, *Handbook for Cleaning/Decontamination of Surfaces*, Elsevier, 2007, pp. 831–884.
- 11 F. Garavand, M. Jalai-Jivan, E. Assadpour and S. M. Jafari, *Food Chem.*, 2021, **364**, 130376.
- 12 *Exploring for oil and gas traps*, ed. E. O. Beaumont and N. H. Foster, American Association of Petroleum Geologists, Tulsa, OK, 1999.
- 13 M. Miñana-Perez, A. Graciaa, J. Lachaise and J.-L. Salager, *Colloids Surf., A*, 1995, **100**, 217–224.
- 14 T. Sottmann and C. Stubenrauch, *Microemulsions*, Wiley, Chichester, West Sussex, U.K. and Ames, Iowa, 2009, pp. 1–47.
- 15 M. Krappel, J. Hippele, C. Bittner and T. Sottmann, *Ind. Eng. Chem. Res.*, 2024, **63**, 10041–10053.
- 16 M. Krappel, J. Hippele, S. Kolin, N. Lichterfeld-Weber, R. Schweins, C. Bittner and T. Sottmann, 85th EAGE Annual Conference & Exhibition, 2024.
- 17 Y. Kawabata, M. Nagao, H. Seto, S. Komura, T. Takeda, D. Schwahn, N. L. Yamada and H. Nobutou, *Phys. Rev. Lett.*, 2004, **92**, 056103.
- 18 Y. Kawabata, H. Seto, M. Nagao and T. Takeda, *J. Chem. Phys.*, 2007, **127**, 044705.
- 19 H. Seto, M. Nagao and Y. Kawabata, *Colloids Surf., A*, 2006, **284–285**, 430–433.
- 20 W. Helfrich, *Z. Naturforsch., C*, 1973, **28**, 693–703.
- 21 J. Eastoe, D. C. Steytler, B. H. Robinson and R. K. Heenan, *J. Chem. Soc., Faraday Trans.*, 1994, **90**, 3121.
- 22 J. Eastoe, W. K. Young, B. H. Robinson and D. C. Steytler, *J. Chem. Soc., Faraday Trans.*, 1990, **86**, 2883.
- 23 E. W. Kaler, J. F. Billman, J. L. Fulton and R. D. Smith, *J. Phys. Chem.*, 1991, **95**, 458–462.
- 24 J. Eastoe, B. M. H. Cazelles, D. C. Steytler, J. D. Holmes, A. R. Pitt, T. J. Wear and R. K. Heenan, *Langmuir*, 1997, **13**, 6980–6984.
- 25 M. Klostermann, T. Foster, R. Schweins, P. Lindner, O. Glatter, R. Strey and T. Sottmann, *Phys. Chem. Chem. Phys.*, 2011, **13**, 20289–20301.
- 26 A. Müller, Y. Pütz, R. Oberhoffer, N. Becker, R. Strey, A. Wiedenmann and T. Sottmann, *Phys. Chem. Chem. Phys.*, 2014, **16**, 18092–18097.
- 27 Y. Pütz, L. Grassberger, P. Lindner, R. Schweins, R. Strey and T. Sottmann, *Phys. Chem. Chem. Phys.*, 2015, **17**, 6122–6134.
- 28 M. Nagao, H. Seto, S. Komura, T. Takeda and M. Hikosaka, *Formation and Dynamics of Self-Organized Structures in Surfactants and Polymer Solutions*, Steinkopff, Darmstadt, 1997, vol. 106, pp. 86–90.
- 29 O. Holderer, M. Klostermann, M. Monkenbusch, R. Schweins, P. Lindner, R. Strey, D. Richter and T. Sottmann, *Phys. Chem. Chem. Phys.*, 2011, **13**, 3022–3025.
- 30 M. Klostermann, R. Strey, T. Sottmann, R. Schweins, P. Lindner, O. Holderer, M. Monkenbusch and D. Richter, *Soft Matter*, 2012, **8**, 797–807.
- 31 M. Berghaus, M. Paulus, P. Salmen, S. Al-Ayoubi, M. Tolan and R. Winter, *J. Phys. Chem. B*, 2016, **120**, 7148–7153.
- 32 M. Teubner and R. Strey, *J. Chem. Phys.*, 1987, **87**, 3195–3200.
- 33 G. Porod, *Small Angle X-ray Scattering*, Academic Press, London, 1982.
- 34 R. Strey, J. Winkler and L. Magid, *J. Phys. Chem.*, 1991, **95**, 7502–7507.
- 35 E. W. Lemmon, I. H. Bell, M. L. Huber and M. O. McLinden, *NIST Chemistry WebBook, NIST Standard Reference Database 69*, National Institute of Standards and Technology, Gaithersburg, MD, 2023.
- 36 T. Sottmann, R. Strey and S.-H. Chen, *J. Chem. Phys.*, 1997, **106**, 6483–6491.
- 37 M. Laupheimer, T. Sottmann, R. Schweins and C. Stubenrauch, *Soft Matter*, 2014, **10**, 8744–8757.
- 38 T. Sottmann, C. Bittner, J. Fischer, M. Krappel, N. Schnabel, R. Schweins, F. Trummer and D. Sottmann, Influence of Pressure on the Microstructure of Bicontinuous Propane Microemulsions, Institut Laue-Langevin (ILL), 2023, DOI: [10.5291/ILL-DATA.9-10-1745](https://doi.org/10.5291/ILL-DATA.9-10-1745).
- 39 C. D. Dewhurst, *J. Appl. Crystallogr.*, 2023, **56**, 1595–1609.
- 40 D. Langevin, *Acc. Chem. Res.*, 1988, **21**, 255–260.
- 41 C. Frank, H. Frielinghaus, J. Allgaier and H. Prast, *Langmuir*, 2007, **23**, 6526–6535.
- 42 S. M. Choi, S. H. Chen, T. Sottmann and R. Strey, *Phys. A*, 2002, **304**, 85–92.
- 43 K. Schneider, P. Verkoyen, M. Krappel, C. Gardiner, R. Schweins, H. Frey and T. Sottmann, *Langmuir*, 2020, **36**, 9849–9866.



- 44 G. Gompper, H. Endo, M. Mihailescu, J. Allgaier, M. Monkenbusch, D. Richter, B. Jakobs, T. Sottmann and R. Strey, *EPL*, 2001, **56**, 683–689.
- 45 P. Pieruschka and S. A. Safran, *EPL*, 1993, **22**, 625–630.
- 46 P. Pieruschka and S. A. Safran, *EPL*, 1995, **31**, 207–212.
- 47 D. Byelov, H. Frielinghaus, O. Holderer, J. Allgaier and D. Richter, *Langmuir*, 2004, **20**, 10433–10443.
- 48 M. Peltomäki, G. Gompper and D. M. Kroll, *J. Chem. Phys.*, 2012, **136**, 134708.
- 49 O. Holderer, H. Frielinghaus, M. Monkenbusch, M. Klostermann, T. Sottmann and D. Richter, *Soft Matter*, 2013, **9**, 2308.
- 50 B. Jakobs, *Amphiphile Blockcopolymer als Efficiency Booster für Tenside: Entdeckung und Aufklärung des Effekts*, Cuvillier, Göttingen, 2002.
- 51 H. F. M. Klemmer, J. Allgaier, H. Frielinghaus, O. Holderer and M. Ohl, *Colloid Polym. Sci.*, 2017, **295**, 911–923.
- 52 J. Fischer, L. Porcar, J. T. Cabral and T. Sottmann, *J. Colloid Interface Sci.*, 2023, **635**, 588–597.
- 53 K.-V. Schubert, R. Strey, S. R. Kline and E. W. Kaler, *J. Chem. Phys.*, 1994, **101**, 5343–5355.
- 54 K.-V. Schubert and R. Strey, *J. Chem. Phys.*, 1991, **95**, 8532–8545.
- 55 M. C. Puerto and R. L. Reed, *Soc. Pet. Eng. J.*, 1983, **23**, 669–682.
- 56 D. G. Peck and K. P. Johnston, *J. Phys. Chem.*, 1991, **95**, 9549–9556.
- 57 J. A. Silas and E. W. Kaler, *J. Colloid Interface Sci.*, 2003, **257**, 291–298.
- 58 H. Frielinghaus, *Nucl. Instrum. Methods Phys. Res., Sect. A*, 2018, **904**, 9–14.
- 59 S. Jaksch, V. Pipich and H. Frielinghaus, *J. Appl. Crystallogr.*, 2021, **54**, 1580–1593.
- 60 M. Nagao, H. Seto, T. Takeda and Y. Kawabata, *J. Chem. Phys.*, 2001, **115**, 10036–10044.
- 61 H. Endo, M. Mihailescu, M. Monkenbusch, J. Allgaier, G. Gompper, D. Richter, B. Jakobs, T. Sottmann, R. Strey and I. Grillo, *J. Chem. Phys.*, 2001, **115**, 580–600.
- 62 K. Schneider, T. M. Ott, R. Schweins, H. Frielinghaus, O. Lade and T. Sottmann, *Ind. Eng. Chem. Res.*, 2019, **58**, 2583–2595.
- 63 N. Freiburger, C. Moitzi, L. de Campo and O. Glatter, *J. Colloid Interface Sci.*, 2007, **312**, 59–67.
- 64 M. Schwan, L. G. A. Kramer, T. Sottmann and R. Strey, *Phys. Chem. Chem. Phys.*, 2010, **12**, 6247–6252.
- 65 M. Kahlweit, R. Strey, P. Firman, D. Haase, J. Jen and R. Schomaecker, *Langmuir*, 1988, **4**, 499–511.
- 66 S. Queste, J. L. Salager, R. Strey and J. M. Aubry, *J. Colloid Interface Sci.*, 2007, **312**, 98–107.
- 67 Y. Talmon and S. Prager, *J. Chem. Phys.*, 1978, **69**, 2984–2991.
- 68 P. G. de Gennes and C. Taupin, *J. Phys. Chem.*, 1982, **86**, 2294–2304.
- 69 P. Debye, H. R. Anderson and H. Brumberger, *J. Appl. Phys.*, 1957, **28**, 679–683.
- 70 D. C. Morse, *Curr. Opin. Colloid Interface Sci.*, 1997, **2**, 365–372.
- 71 G. Porte and C. Ligoure, *J. Chem. Phys.*, 1995, **102**, 4290–4298.

