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The chemical industry is a significant driver of fossil fuel consumption and has the largest energy consumption of all industrial sectors. Sustainability targets therefore necessitate alternative and sustainable methodologies for chemical production. Simultaneously, polymeric waste, including lignocellulosic materials, non-lignocellulosic food waste, and plastics is increasing annually and current recycling technologies are insufficient to mitigate an environmental pollution.

Synthetic biology can address these challenges by facilitating waste-to-chemical conversion through microbial metabolic engineering. This approach supports the development of a circular economy while aligning with United Nations Sustainable Development Goal 11 (Sustainable Cities and Communities), 12 (Responsible Consumption and Production) and 13 (Climate Action). Developing and embracing these novel technologies will enable the chemical industry to realise a step-change towards net-zero.

View Article Online  
DOI: 10.1039/D5SU00013K



## Chemical bio-manufacture from diverse C-rich waste polymeric feedstocks using engineered microorganisms

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DOI: 10.1039/D5SU00013K

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### Abstract

Sustainability targets are driving the chemicals industry away from reliance upon finite fossil fuel resources for chemical synthesis. Biotechnology holds huge promise in this area and methods to convert renewable feedstocks, such as glucose, into a myriad of value-added chemicals are well-known. Metabolic engineering and synthetic biology have been transformational in enabling microbial cells to perform non-native chemistry, increasing product yields and the scope of chemical space accessible through bio-based approaches. While the development of the bioeconomy using virgin renewable feedstocks (e.g., glucose) has been a significant milestone, we propose that the next major breakthrough towards a sustainable future lies in utilizing waste feedstocks through engineered microbes. In particular, C-rich polymeric materials such as lignocellulosic and plastic waste hold vast untapped potential for the circular bioeconomy. This mitigates land-use conflicts with the food industry and aligns with principles of the circular economy. This Perspective highlights progress and challenges in this emerging field of using biotic and abiotic polymers as a feedstock for chemical biomanufacturer.

**Keywords:** Sustainable chemistry; waste upcycling; biocatalysis; biomanufacturing; circular bioeconomy.

### Introduction

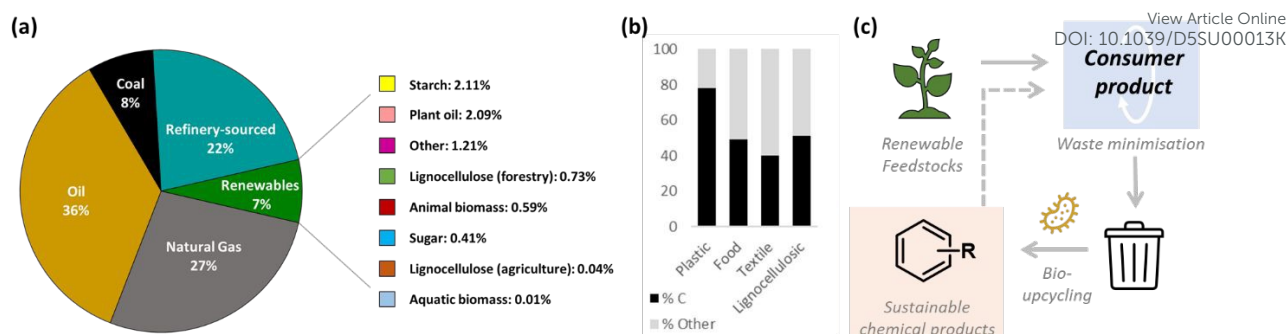
Synthetic chemicals are deeply integrated into modern day society and form the cornerstone of the pharmaceuticals, plastics, agrochemicals, flavours, fragrances and cosmetics industries. Cumulatively, the chemicals industry was valued at approximately \$5.7tn in 2022<sup>1</sup>, with 93% of this accounted for by the petrochemicals industry, which uses finite fossil fuel resources (e.g. crude oil and natural gas) as its primary feedstock (Figure 1a). Petrochemical synthesis accounts for 14% and 8% of all oil and gas consumption globally, with the remainder used for fuel for the transport and energy sectors<sup>2</sup>. This reliance upon finite feedstocks to support a vast and growing array of chemical supply chains is not sustainable and has prompted a shift towards alternative raw materials.

As such, the remaining 7% of the global market comprises renewable chemicals, or

those wholly or partially derived from materials of biological origin, such as plants, animals and microorganisms (Figure 1a)<sup>2,3</sup>. These renewable feedstocks may be processed via chemical or biological methods to produce the synthetic chemical of interest with life-cycle analysis studies to date often showing a reduction in greenhouse gas (GHG) emissions and energy usage for many biobased routes<sup>4</sup>.

Beyond use of virgin renewable feedstocks, there is an emerging field of valorising underutilized C-rich by-products and waste streams from industrial and municipal settings as a feedstock for chemical production. This trend is further incentivized by high feedstock costs, land-use conflicts with the food industry<sup>5,6</sup> and circular economy policy drivers. In particular, polymeric waste streams are increasingly accessible for valorisation due to significant advances in depolymerisation





2 **Figure 1.** (a). Current feedstocks for the chemicals industry. (b) Percentage carbon content by mass of four major  
4 waste streams. (c) Proposed future materials flow for a circular chemicals economy based on renewable and waste  
4 inputs

technologies. In this Perspective, we will refer to these materials collectively as 'C-rich waste feedstocks'. In contrast to virgin renewable feedstocks, waste feedstocks are typically low-cost and therefore hold potential for significant value to be added via processing into second generation chemical products. These 'upcycling' strategies are anticipated to generate new value chains for industry. Figure 1b shows an estimation of the carbon content of four major waste streams which contain high proportions of polymeric content (plastic, food, textiles and non-food lignocellulosic materials). Whilst the majority of this waste is currently sent to landfill or used for energy recovery, a growing body of evidence suggests that this carbon could be diverted instead towards 'upcycling' processes that would yield second generation chemical products.

## 26 Biotechnological approaches to polymer upcycling

28 Whilst chemical approaches to polymeric waste upcycling is acknowledged as an important and active field of research<sup>7,8</sup>, bio-based upcycling technologies hold particular advantages. Biological 'funneling' of variable and mixed waste feedstocks into single chemical products presents a unique advantage over chemical processes and 'smart' bioprocesses could respond in real-time to feedstock variability<sup>9</sup>. Bio-processes are also inherently suited to mesophilic and aqueous conditions, with LCA studies

consistently showing sustainability advantages over chemical routes<sup>4,10–12</sup>. In addition, enabling technologies in synthetic biology allow augmentation, adaptation or 're-wiring' of microbial metabolism, including *in situ* depolymerisation of the polymeric feedstock into fermentable monomers<sup>13</sup>. The result is an impressive array of engineered microbial cell factories capable of new-to-Nature enzymatic cascades<sup>14–17</sup> and increased product titres<sup>16,18</sup>. This will enable a paradigm shift in the synthetic chemicals industry, which transitions away from finite, petrochemical feedstocks. Rather, raw materials could be sourced from renewable, biological origin and converted into a consumer product. Aligning with the principles of the circular economy, C-rich materials would be kept in circulation for as long as possible and waste minimised<sup>19</sup>. Unavoidable waste would then serve as the primary feedstock for bio-based upcycling processes using engineered microbial metabolism to convert industrial waste products into synthetic chemicals (Figure 1c). This framework holds synergistic benefits of sustainable chemical production and waste valorisation which adds new value streams to established industrial processes. This Perspective highlights illustrative examples of progress in this emerging field and provides a critical evaluation of outstanding challenges. We focus on the use of C-rich polymeric feedstocks for the production of platform and fine chemicals using engineered microbial metabolism.



Transition towards a circular economy is vital to achieving a net-zero society and alignment with the UN Sustainable Development Goals (SDGs), in particular SDG 11 (Sustainable cities and communities), 12 (Responsible consumption and production) and 13 (Climate action)<sup>20</sup>. This is driven by a staggering volume of waste materials being generated from industrial and domestic settings, including ~2 billion tonnes of municipal solid waste produced globally pa, which is predicted to increase to ~3.4 billion tonnes by 2050<sup>21</sup>. An increasing proportion of this (13% - 274,800 tonnes in 2020)<sup>22</sup> is currently used for 'waste-to-energy' incineration, however this ultimately releases waste-embedded carbon into the atmosphere as greenhouse gasses and substantial sustainability advances could be made through instead of diverting the flow of carbon into second generation chemical products, whilst investing in 'clean' energy solutions in the long term<sup>23</sup>.

Two approaches have been taken to polymer waste bio-upcycling. The first is direct fermentation of waste or depolymerisation products, where these serve as the sole or primary carbon source for microbial growth and metabolism, from which the target chemical is over-produced. The second involves use of whole-cell biocatalysis (WCB) to convert a waste feedstock into the chemical of interest. This usually employs microbial cells as catalysts which metabolise a renewable feedstock (e.g. glucose) as the primary C-source for growth and heterologous enzyme and/or pathway expression. Whilst WCB can afford higher product titres, input costs tend to be higher due to the increased number of steps and nutrient broth requirements. In both cases, feedstocks typically require pre-processing into fermentable monomers prior to upcycling. The following section discusses examples of both strategies in the context of upcycling polymeric waste feedstocks into industrially important chemicals.

### Lignocellulosic waste

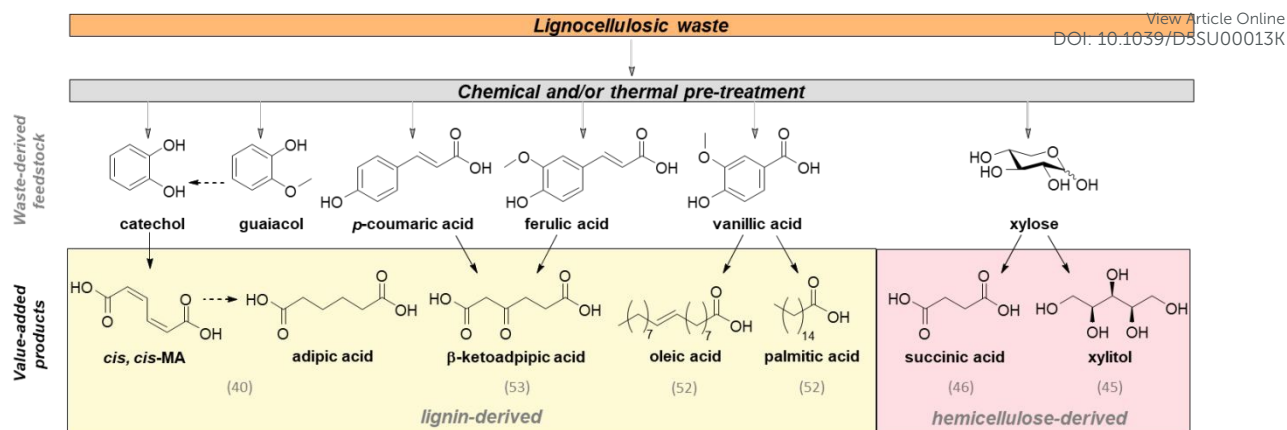
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DOI: 10.1039/D5SU00013K

Lignocellulosic waste is produced at an estimated volume of 140 gigatons per year<sup>24</sup> from agricultural and forestry residues, the food industry and municipal solid waste<sup>25,26</sup>. It primarily comprises cellulose, hemicellulose and lignin, the proportions of which vary according to the biomass type<sup>27,28</sup>. Despite the chemical potential of these materials as a rich and abundant source of fixed carbon, widespread application is limited by slow and energy intensive degradation into fermentable small molecules (e.g. glucose) due to the high crystallinity of cellulose and chemical stability of high-molecular weight lignin<sup>29</sup>. Lignin also exhibits significant interspecies and intraspecies structural variability between different growth stages<sup>30</sup>, tissues<sup>31,32</sup>, and environmental conditions<sup>33,34</sup>. This feedstock variability poses challenges for widespread valorisation<sup>35,36</sup>.

Lignocellulosic waste bio-valorisation efforts therefore normally employ two-step processes comprising (1) generation of fermentable small molecules through lignin degradation<sup>37,38</sup> and (2) bio-conversion of degradation products into chemical targets of interest via engineered metabolism<sup>39</sup>. Exemplar chemical transformations demonstrated through this approach are shown in Figure 2 and briefly described below.

Utilisation of phenol derivatives in lignin hydrolysates has been well described. Kohlstedt *et al.* developed a metabolic pathway to convert pine lignin-derived catechol into *cis-cis* muconic acid (ccMA), a nylon precursor. A *de novo* metabolic pathway was constructed to convert catechol into ccMA using two native catechol 1,2-dioxygenases CatA and CatA2, and the heterologous expression of phenol hydroxylase in *P. putida* KT2440. A catechol and phenol-rich lignin hydrolysate from a softwood hydrothermal pre-treatment was supplemented with glucose as the carbon source for central metabolism of the engineered strain, which accumulated 13 g L<sup>-1</sup> ccMA in a fed-batch process. The authors demonstrated production of the ccMA by chemically





**Figure 2.** Chemicals accessed from lignin-rich waste feedstocks using engineered microbial metabolism. Grey arrows denote pre-processing steps; black arrows denote chemical transformations mediated by an engineered microorganism or microbial consortium; references shown in parentheses.

reducing the isolated product to adipic acid (AA) and polymerising into nylon-6,6<sup>40</sup>. Reduction of ccMA into AA can also be achieved enzymatically using the enolate reductase from *Bacillus coagulans* (BcER)<sup>41</sup>, as demonstrated in *E. coli* BL21 (DE3) in the context of lignin-derived guaiacol upcycling to AA, giving 61% conversion to AA via co-expression of chaperone proteins<sup>42,43</sup>. In comparison to the current industrial chemical route and assuming 100% efficiency of all steps, the guaiacol to AA route has 83% atom economy (vs 77% for the chemical route) and crucially eliminates the production of the potent greenhouse gas N<sub>2</sub>O as a major by-product.

The hemicellulose fraction of lignocellulosic biomass contains 5 and 6-carbon monosaccharide units (e.g. arabinose, rhamnose and xylose)<sup>44</sup>, which can be fermented by engineered yeast and fungi for chemical production. For example, Meng *et al.* engineered an *Aspergillus niger* strain to convert lignocellulosic waste into xylitol, a sweetener ubiquitous in the food industry, currently produced industrially by chemical hydrogenation of xylose<sup>45</sup>. Deletion of *ladA*, *xdhA*, and *sdhA*, which encode key enzymes in the pentose catabolic pathway, resulted in biomass-derived xylose degradation through batch fermentation and enabled up to 0.26 g/L of xylitol from cotton seed hulls.

Waste paper also represents a rich source of lignocellulosic waste and has been valorised for chemical production. For

example, succinic acid (SA) is currently synthesised industrially from oil-derived benzene or *n*-butane at 70,000 tonne scale<sup>46</sup>. Using engineered microorganisms, a recent bioprocess achieved >51 g/L SA from waste paper using *E. coli* KJ122 in a fed-batch system with simultaneous saccharification and fermentation<sup>47</sup>. This process has an estimated atom economy of 95%, process mass intensity (PMI) of 20.5 and E-factor of 19.7 (calculated from paper-derived glucose and xylose to SA), which whilst higher than competing petrochemical processes (which normally fall in the PMI range of 1-5 for bulk chemicals), is an encouraging demonstration that early stage bioprocesses could be competitive with their petrochemical alternatives upon further optimisation and scale-up.

Microbial co-cultures have also been explored to mitigate high metabolic burden placed on cells through overexpression of large heterologous pathways<sup>48-51</sup>. For example, a co-culture of a wild type and engineered *Rhodococcus* strain showed higher lipid biosynthesis from corn stover, a residual product of corn harvest, compared to monocultures. An engineered strain of *R. jostii* modified lignin-derived feedstocks through the native  $\beta$ -ketoadipate pathway and accumulated vanillic acid, which was used as a sole carbon source for growth and production of lipids by *R. opacus* PD630. The co-fermentation approach enabled ~40% lignin degradation and accumulation



of 0.29 g lipid/g of cell dry weight (CDW) after 5 days, compared to 34% and 21% degradation in monoculture experiments<sup>52</sup>.

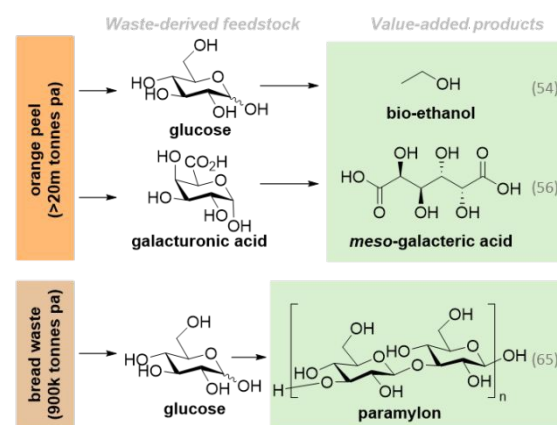
Alkaline pre-treated corn stover has also been valorised for  $\beta$ -keto adipic acid production using engineered *P. putida* KT2440 in a fed-batch fermentation.

Overexpression of vanillate O-demethylase (VanAB), replacement of endogenous *p*-hydroxybenzoate hydroxylase (PobA) with heterologous Pral<sub>JJ-1b</sub> from *Paenibacillus* sp. JJ-1b and deletion of global regulator Crc, allowed for the conversion of *p*-cumarate and ferulate from lignin into  $\beta$ -keto adipic acid, yielding 25 g/L in 48 hours at 30 °C from glucose-supplemented media<sup>53</sup>.

An inherent challenge to the valorisation of polymeric waste is the requisite depolymerisation to release fermentable sugars. Synthetic biology offers a unique opportunity for simultaneous feedstock depolymerisation and upcycling through surface-display or secretion of degradative enzymes. For example, Yang *et al.* extracellularly expressed three heterologous cellulases (endo-1,4- $\beta$ -glucanase, exo-1,4- $\beta$ -glucanase, and  $\beta$ -xylanase) via genomic integration in *S. cerevisiae*<sup>54</sup>. This enabled the production of glucose from orange-peel waste, a prolific by-product of the juice industry produced at >20 million tonne scale every year (Figure 3)<sup>55</sup>. Bioprocessing under anaerobic conditions gave 7.53 g/L ethanol, an important biofuel<sup>54</sup>. Other studies have demonstrated the use of citrus peel waste for chemical bioproduction under aerobic fermentation conditions, such as production of *meso*-galactaric acid from industrial orange peel waste. Here, *S. cerevisiae* was engineered to co-utilize peel waste-derived D-galacturonic acid and D-glucose, producing 8 g/L product from an 80 h batch-fermentation<sup>56</sup>.

The potential for these preliminary studies to yield bioprocesses with genuine sustainability advantages over current petrochemical routes remains a critical area of investigation. Whilst a limited number of LCA studies have been reported, there is clear evidence of potential for genuine environmental

benefits. In one study, bio-based adipic acid production was estimated to reduce greenhouse gas (GHG) emissions by 62–78% compared to petrochemical processes, which emit nitrous oxide (N<sub>2</sub>O), a greenhouse gas with 273-fold the global warming potential of CO<sub>2</sub>. However, this work also identified lignin pre-treatment energy demands and base inputs as major environmental burdens<sup>10</sup>. A broader review of LCA studies on lignin valorisation gave a more nuanced picture<sup>11</sup>. While lignin bioprocessing often resulted in reduced GHG emissions, fossil fuel depletion, and ecotoxicity relative to petrochemical methods, environmental burdens could increase across several impact categories and were primarily attributed to solvent and energy-intensive lignin pre-treatment and depolymerisation steps<sup>11,57</sup>. Further, lack of standardisation in LCA methodology can hinder direct comparison between studies. This underscores the ongoing need for development of standardised LCA methodologies, and innovation to improve the release of fermentable monomers from lignin at mesophilic conditions, for example via bio- or abiotic catalysis<sup>58</sup>.



**Figure 3.** Examples of chemicals accessed from lignocellulosic and non-lignocellulosic food waste feedstocks using engineered microbial metabolism. The figures quoted represent the approximate volume of each waste feedstock generated each year. References shown in parentheses.

### Non-lignocellulosic food waste

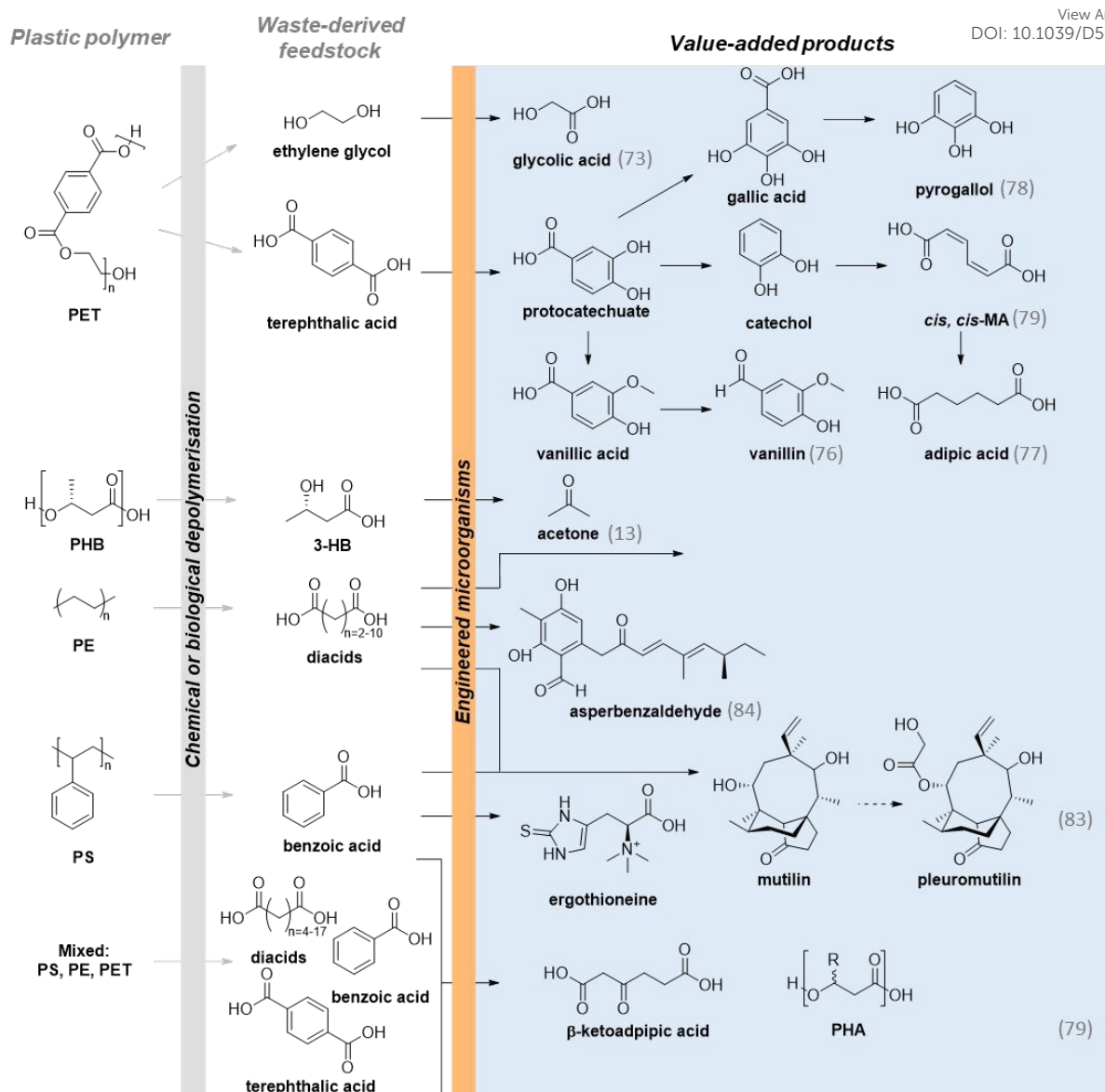
Food and garden waste account for more than 50% of global municipal solid waste production, presenting a significant opportunity for the circular bioeconomy which aligns with SDG 12 (food waste and



losses)<sup>20,23</sup>. Biotechnology is well  
2 established in this field, with anaerobic  
digestion (AD) widely demonstrated as a  
4 cost-effective method for treatment of  
agricultural, industrial and food waste for  
6 the production of methane<sup>59</sup>, biofuels<sup>60</sup> and  
other useful products<sup>61</sup>. Coupling AD  
8 systems with production of high-value  
chemical products could have additional  
10 cost benefits whilst providing new  
sustainable chemical manufacturing  
12 routes<sup>62,63</sup>.







**Figure 4.** Chemicals accessed from plastic waste feedstocks using engineered microbial metabolism. Grey arrows denote depolymerisation steps (chemical or biological); black arrows denote chemical transformations mediated by an engineered microorganism or microbial consortium; references shown in parentheses.

For example, bread waste is an abundant source of polymeric glucose, with bread being the second most wasted food item in the UK<sup>64</sup>. In a recent study, bread waste was used as a feedstock for paramylon and syngas production, using biological and chemical approaches, respectively. Bread was enzymatically hydrolysed to yield glucose, which fuelled the synthesis of paramylon by fermentation of the algae *Euglena gracilis*, while H<sub>2</sub> was generated via catalytic pyrolysis of the solid hydrolysis residue using CO<sub>2</sub> and Ni/SiO<sub>2</sub> catalysis<sup>65</sup>. This demonstrates the promising application of two complementary technologies to valorise all fractions of a processed waste stream.

**Plastic waste**

Plastic production currently exceeds 400 million tonnes of plastic each year, of which only 9% is recycled, 57% sent to landfill and 29% incinerated<sup>66–68</sup>. Although traditionally considered as recalcitrant, a growing body of evidence shows that many plastics can be degraded under biologically relevant conditions into small molecules which can support microbial metabolism<sup>69–75</sup>. These degradation products can further be ‘upcycled’ into higher-value, second generation products through engineering microbial metabolism to favour C-flux towards the product of interest. Many studies have reported innovative methods



to upcycle single-use, post-consumer plastic waste, as summarised in Figure 4. For example, poly(ethylene terephthalate) (PET)-derived terephthalic acid (TA) was upcycled into the industrially valuable small molecule vanillin through the introduction of a novel pathway in engineered *Escherichia coli* for whole-cell biocatalysis, giving 79% conversion of terephthalic acid into vanillin, which was sequestered via *in situ* product removal to mitigate product toxicity<sup>76</sup>. Whilst we note that the theoretical (assuming 100% conversion at each step) atom efficiency of the TA to vanillin route is the same as the industrial chemical guaiacol to vanillin process, a full LCA will be required to determine whether it holds tangible sustainability benefits in other categories. In another study, TA from PET was upcycled into adipic acid (115 mg/L), a key precursor to nylon, by optimization of a six-enzyme *de novo* biosynthetic pathway using calcified alginate bead-encapsulated *E. coli*<sup>77</sup>. To valorise both PET monomers, Kim *et al.* demonstrated biological valorisation of both TA and ethylene glycol (EG). Gallic acid, pyrogallol, catechol, muconic acid, and vanillic acid were obtained from whole-cell biocatalysis using plastic-derived TA as feedstock, while glycolic acid was obtained from EG conversion using a *Gluconobacter oxydans* strain<sup>78</sup>. Simultaneous TA and EG consumption were also demonstrated by Bao *et al.*, who highlighted the advantages of a division of labour approach to fully upcycling PET hydrolysate. Two strains of *P. putida* were designed for the respective degradation of TA and EG from a PET hydrolysate and upcycled into medium chain length PHA and *cis,cis*-muconic acid (ccMA) with titres of 0.64 g/L and 4.73 g/L respectively<sup>79</sup>. Collectively, these examples offer considerable evidence that post-consumer PET offers a promising C-feedstock for chemical biomanufacture.

However, many 'real-world' waste streams comprise complex mixtures of polymeric materials. This so called 'mixed plastic waste' is a significant challenge for upcycling and chemical approaches can result in complex product mixtures of low value<sup>80,81</sup>. However, the plasticity of microbial metabolism has been

demonstrated to be a powerful tool for 'funneling' these mixed feedstocks into a target value-added product. A seminal example of this is from Sullivan *et al.* who reported a tandem chemical oxidation and bioconversion of mixed waste models comprising PET, high-density polystyrene (HDPS) and polystyrene (PS) into  $\beta$ -ketoadipate and polyhydroxyalkanoates (PHA)<sup>82</sup>. Mixed plastics were first depolymerised via metal-catalysed autoxidation using O<sub>2</sub>, Co(II), Mn(II) and *N*-hydroxyphthalimide in acetic acid at elevated temperatures to generate a mixture of dicarboxylic acids, benzoic acid and terephthalate. This mixture was then funnelled into the TCA cycle of *P. putida*, which was engineered for production of the target molecules. This approach enabled a 75.5% molar yield of  $\beta$ -ketoadipate from mixed PET, PS and HDPS.

A further challenge in plastic upcycling is valorisation of non-hydrolysable plastics, typically comprising C-C or C-O-C linked polymer backbones, yet here again engineered microbial metabolism has demonstrated potential. For example, Rabot *et al.* developed a hybrid chemical and biological approach to convert post-consumer PS into high value fungal secondary metabolites. PS was oxidatively depolymerised using metal catalysis, generating benzoic acid (BA) that served as sole carbon source for three engineered *Aspergillus nidulans* strains. A six-day fermentation produced ergothioneine, a natural anti-oxidant; mutilin, an antibiotic precursor; and its active derivative pleuromutilin<sup>83</sup>. *Aspergillus nidulans* has also been used for polyethylene (PE) upcycling. In this application, catalytic digestion in anaerobic conditions allowed for depolymerization of PE into a mixture of characterized carboxylic diacids that served as sole carbon source for the growth of engineered *A. nidulans* strains. Background strain engineering coupled with overexpression of the biosynthetic cluster genes *afuG*, *afuE* and *afuC*, provided 4.23 g/L asperbenzaldehyde in a batch fermentation. In a second system, heterologous expression of genes from *A. terreus var. aureus* and *Clitopilus passeckerianus* enabled the production of mutilin and citreoviridin, respectively<sup>84</sup>.



2 Whilst most plastic upcycling studies to  
4 date have focussed on petrochemical-  
6 derived polymers, bio-based and  
8 biodegradable plastics such as  
10 poly(hydroxyalkanoates) (PHAs) and  
12 poly(lactic acid) (PLA) are gaining  
14 popularity for single-use applications.  
16 Whilst widely marketed as biodegradable,  
18 there are growing concerns over 'pollution  
20 swapping' due to unknown effects of  
22 degradation products and microplastics on  
24 the environment, and greenhouse gas  
26 emissions through their biodegradation<sup>85-  
28 89</sup>. To address this, our laboratory has  
30 recently demonstrated the potential of  
32 waste next-generation plastics as a  
34 feedstock for the circular bioeconomy  
through conversion of PHB waste into  
acetone, a solvent widely used in the  
chemical industry and cosmetics which is  
currently produced at 8 million tonne scale  
annually from oil via the cumene process.  
In this one-pot approach, a single strain of  
*E. coli* BL21 (DE3) was engineered to  
simultaneously secrete a PHB hydrolase  
for feedstock depolymerisation into 3-  
hydroxybutyrate (3-HB) whilst  
intracellularly expressing 3-HB  
dehydrogenase and acetoacetate  
decarboxylase for conversion of 3-HB into  
acetone. This strategy enabled acetone  
titres of up to 7 g/L from 24 h fermentation  
at 30 °C<sup>13</sup>.

36 Compared to lignocellulosic waste  
38 streams, the field of plastic bio-upcycling is  
40 relatively new and as such, detailed LCA  
42 studies to determine sustainability  
44 advantages are lacking. However, based  
46 on LCA studies on closed-loop plastic  
48 (bio)degradation and recycling, it is  
50 anticipated that feedstock  
52 depolymerisation will be a driver of  
54 environmental burden. We therefore  
reiterate that methods to depolymerise  
these materials at low temperature under  
biocompatible conditions to enable direct  
interfacing with biological upcycling  
processes will be critical in enabling  
ultimate success of novel upcycling  
technologies<sup>90-92</sup>. Whilst plastic bio-  
upcycling cannot solve the vast and  
complex issue of plastics pollution alone,  
we propose that it will be an important part

56 of a suite of technologies and policies that  
58 embed circularity into the lifecycle of  
unavoidable plastic waste of the future<sup>93</sup>.

#### 4. Outlook and future perspectives

60 Waste bio-upcycling using engineered  
62 microorganisms holds vast potential for  
64 sustainable chemical production, and  
66 indeed preliminary life-cycle assessments  
68 in this field indicate sustainability  
70 advantages over existing petrochemical  
72 routes<sup>91,92,94</sup>. Additionally, ambitious policy  
74 drivers are further motivating industry to  
both de-fossilise product supply chains,  
and seek opportunities for waste  
valorisation to generate additional revenue  
and meet sustainability targets. This is  
driving end-user engagement with  
engineering biology technologies to bridge  
waste generation and chemical  
bioproduction.

76 Whilst feedstock pre-treatment and  
78 depolymerisation has been discussed  
above, further outstanding challenges  
remain<sup>95</sup>. First, successful process scale-  
80 up to technology readiness level (TRL) >4  
82 is also crucial to navigating the infamous  
84 'valley of death'. This is non-trivial as key  
86 process indicators (e.g. dissolved oxygen,  
88 pH, growth rate, feedstock consumption  
90 and product distribution) often do not scale  
92 linearly with fermentation volume<sup>96,97</sup>.  
94 Earlier integration of LCA and TEA into  
96 bioprocess development may help to  
98 mitigate this, such that strains are  
engineered from the outset for scale up.  
For example, this could include greater  
focus on genomic integration of pathway  
genes to decrease costs associated with  
antibiotic usage, and use of constitutive or  
self-inducible promoter systems to  
decrease process costs. Additionally,  
transparent and comprehensive waste-  
mapping by region, incentivised by policy  
changes, could vastly accelerate transition  
to a more sustainable circular chemicals  
industry. This would enable rapid  
identification of potential feedstocks and  
matching by the academic and industrial  
biotechnology community to suitable



**Table 1.** Summary of key examples of solid waste upcycling into industrially important molecules using engineered microorganisms.

Feedstock	Process	Chassis	Chemical	Scale	Time	Titre	Reference
<b>Lignocellulosic waste</b>							
Pine lignin	Fed-batch fermentation	<i>Pseudomonas putida</i> KT2440	Muconic acid	50 mL	54 h	13 g/L	40
Corn stover lignin	Batch co-fermentation	<i>Rhodococcus opacus</i> PD630, <i>Rhodococcus jostii</i> RHA1 VanA <sup>-</sup>	Fatty acids (C13-C24)	100 mL	120 h	0.29 g/g CDW (Cell Dry Weight)	52
Corn stover-derived lignin-related aromatic compounds	Fed-batch fermentation	<i>Pseudomonas putida</i> KT2440	$\beta$ -Ketoadipic acid	150 mL	48 h	25 g/L	53
Mixed waste office paper	Fed-batch fermentation	<i>E. coli</i> KJ122	Succinic acid	2.5 L	54 h	51.38 g/L	46
Wheat bran, cotton seed hulls	Batch fermentation	<i>Aspergillus niger</i> N593	Xylitol	50 mL	48 h	0.22 g/L and 0.26 g/L	45
Waste orange peel	Batch fermentation	<i>Saccharomyces cerevisiae</i> BY4741	meso-Galactaric Acid	50 mL	80 h	8 g/L	56
Waste orange peel	Anaerobic batch fermentation	<i>Saccharomyces cerevisiae</i>	Ethanol	200 mL	48 h	7.53 g/L	54
<b>Non-lignocellulosic food waste</b>							
Bread waste	Batch fermentation	<i>Euglena gracilis</i>	Paramylon	2.5 L	72 h	5.79 g/L	65
<b>Plastic waste</b>							
PET	Whole cell biocatalysis	<i>Escherichia coli</i> MG1655 RARE	Vanillin	40 mL	24 h	0.01 g/L	76
PET	Whole cell biocatalysis	<i>Escherichia coli</i> BL21(DE3)	Terephthalic acid	3 mL	24 h	0.11 g/L	77
PET	Whole cell biocatalysis	<i>Escherichia coli</i> XL1- Blue, <i>Escherichia coli</i> MG1655(DE3)	Gallic acid		24 h	0.34 g/L	78
			Pyrogallol		24 h	0.07 g/L	
			Muconic acid	4-20 mL	6 h	0.38 g/L	
PET	Division of labour fed-batch	<i>Pseudomonas putida</i> EM42, <i>Pseudomonas putida</i> M31	Vanillic acid		48 h	0.23 g/L	79
			Glycolic acid		12 h	~ 0.76 g/L	
			Medium chain length polyhydroxyalkanoates	50 mL	96 h	0.64 g/L	
PHB	Batch fermentation	<i>Escherichia coli</i> BL21 (DE3)	Muconic acid			4.73 g/L	13
PS	Catalytic oxidative cleavage, then batch fermentation	<i>Aspergillus nidulans</i> FGSC A4 (LO10050)	Acetone	5 mL	24 h	7 g/L	83
PE	Aerobic catalytic digestion, then batch fermentation	<i>Aspergillus nidulans</i> FGSC A4	Ergothioneine, pleuromutilin, mutilin	30 mL	144 h	0.17 g/L, ~0.02 g/L, ~0.4 g/L	84
			Asperbenzaldehyde	10 mL	144 h - 72 h	4.23 g/L	
Mixed plastics (PS, HDPE, PET)	Oxidative cleavage, then batch fermentation	<i>Pseudomonas putida</i> KT2440 strains	$\beta$ -ketoadipate, polyhydroxyalkanoates (PHA)	50 mL	9 h	75.5% molar yield	82



chemical targets<sup>13</sup>. Finally, mixed and variable feedstocks remain a central challenge. Costs of their pre-treatment to release fermentable substrates and removal of potential microbial inhibitors. A range of technologies are emerging for this, including polymeric resins<sup>98</sup> and solvent extraction<sup>99,100</sup>, however solutions are likely to be developed and scaled on a case-by-case basis as appropriate to the specific chemistry of the system.

Despite sustainability advantages inherent to a biological waste upcycling process, some metrics of sustainability such as PMI E-factor (e.g. ~8535 and 8533, respectively, for biological upcycling of PET into vanillin based on 79% conversion of 1 mM TA) remain high for very early proof-of-concept bio-upcycling studies performed at low substrate loading and high cell density. Development of workflows to rapidly optimise these bioprocesses towards higher product titres with lower process inputs (e.g. lower cell densities, higher feedstock loading and improved product recovery) in a single fermentative step is therefore a research priority to improve their sustainability profile and bring these technologies closer to commercialisation.

The scope of molecules accessible via engineered microbial metabolism is inherently limited to chemical transformations known to nature, or which can be catalysed by new-to-nature, engineered or evolved enzyme<sup>101–104</sup>. This precludes bioproduction of a multitude of industrially important molecules, prompting the emerging field of biocompatible chemistry, which directly interfaces abiotic chemistry with microbial metabolism to leverage the ‘best of both worlds’<sup>105–108</sup>. We propose that biocompatible chemistry will be an important addition to the biotechnology toolbox for waste upcycling for sustainable chemical production. An early example of this has recently been reported by Valenzuela-Ortega *et al.* in the conversion of PET-derived terephthalic acid into the nylon 6,6-precursor adipic acid. The bottleneck double reduction of ccMA to AA using BcER was alleviated

through addition of a H<sub>2</sub>-producing strain of *E. coli*, in combination with a Pd catalyst for chemical reduction of TA-derived ccMA to the target molecule adipic acid with 80% conversion<sup>77</sup>. As this field continues to expand over the coming decade we anticipate these hybrid chemo-biological processes becoming increasingly prevalent in the field of waste upcycling.

This Perspective has focussed on waste streams for which upcycling via engineered microbial metabolism has been reported. However, other abundant C-rich solid waste streams also hold promise for sustainable chemical manufacture, including flower waste<sup>109</sup>, textiles<sup>110,111</sup> and potato waste<sup>112–115</sup>, although opportunities to merge these with engineered microbial metabolism remain under-exploited.

## 5. Conclusions

Microbial metabolism has been generating functional molecules from diverse C-rich feedstocks for millions of years in a staggering range of environments. This remarkable ability for microbes to perform complex chemistry from basic building blocks continues to inspire the discovery, characterisation and application of biological machinery for the production of synthetic chemicals. In this Perspective, we have demonstrated how engineering biology can be applied to engineer microbial metabolism to enable valorisation of C-rich waste feedstocks from industry and municipal solid waste. We propose that this approach holds vast untapped potential to address sustainability issues inherent to the petrochemicals industry. In particular, lignocellulosic by-products from industry, plastic waste and food waste have all been demonstrated to be promising alternatives to virgin renewable feedstocks for the industrial biotechnology sector. We highlight the current need for future work in this field to focus on low-cost polymer depolymerisation technologies, bio-process scale up and identification and valorisation of novel C-rich waste polymeric feedstocks to realise the vast potential this



- technology holds for the future of a sustainable chemicals industry. 44
- Conflicts of Interest** 46
- The authors declare no conflicts of interest. (6) 48
- Acknowledgements** 50
- JCS and MFP acknowledge a PhD studentship from IBioIC (Scottish Funding Council H19001). 52
- References** 54
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## Data availability

No primary research results, software or code have been included and no new data were generated or analysed as part of this review.

