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Al-SBA-15 catalysed cross-esterification and acetalisation of biomass-derived platform chemicals

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Abstract.

Al-SBA-15 exhibited excellent catalytic activities in acid-catalysed glycerol transformation including esterification and acetalisation reactions. Quantitative conversion and good selectivities to mono- and diacetylglycerides could be obtained in the esterification of glycerol with levulinic acid. The catalyst also proved to be very effective in the acetalisation of glycerol with aldehydes and acetone, with an interesting selectivity switch from the 6-membered acetal (using paraformaldehyde as aldehyde source) to a 5-membered acetal (when benzaldehyde or furfural were employed). Al-SBA-15 materials were also proved to be highly stable and reusable in most glycerol transformations under the investigated reaction conditions.

Keywords: Glycerol, esterification, acetalisation, levulinic acid, acetone, formaldehyde, benzaldehyde and furfural, Al-SBA-15.

1. Introduction

Biomass valorization has been increasingly recognized to be the way forward in order to provide future alternatives for the production of energy and chemicals from sustainable resources.^{1,2} Biomass as widely available and renewable feedstock can in principle provide access to similar chemical entities, energy and materials to those currently obtained from crude oil. A number of biomass deconstruction strategies have been proposed in recent years to break down complex feedstocks into useful starting compounds (e.g. platform molecules). The chemistries of such biomass-derived platform chemicals will play a major future role in terms of a better understanding in biomass transformations. In 2004, the US Department of Energy (DOE) provided a number of key biomass-derived molecules for further transformations,³ recently revisited by Bozell and Petersen.⁴ These platform chemicals include sugars (glucose, xylose), polyols (sorbitol, xylitol, glycerol), furans (furfural, 5-hydroxymethylfurfural) and acids (succinic, levulinic, lactic acids), which will be key to provide routes towards useful chemicals, fuels and materials from renewable resources.

Glycerol, generally synthesized from propylene oxide derived from fossil fuel resources,⁵ can be obtained from renewable resources as by-product from soap manufacture, biodiesel production^{5,6} and/or microbial fermentation.⁷ With glycerol having low value as by-product, its conversion into value-added chemicals is of great industrial importance due to the large production of glycerol derived from the biodiesel industry.^{8,9}

Comparatively, levulinic acid (LA) is another biomass-derived key platform chemical which repeated in both lists^{3,4} due to its possibilities to be produced from lignocellulosic feedstocks at low cost. LA is a versatile building block for the synthesis of various organic chemicals including levulinate esters, γ -valerolactone, acrylic acid,

1,4-pentanediol, β -acetylacrylic acid, methyl THF and δ -amino levulinic acid.^{10,11} Several of these levulinic acid derivatives have been used as monomers for the synthesis of different polymers including levulinic acid-glycerol oligomers.¹²

Furfural has also been considered a promising chemical which can be derived from sugars dehydration (e.g. hemicelluloses) and further converted into fuel additives, monomers and intermediates for fine chemistry such as 2-methylfuran and 2,5-dimethylfuran.¹³

With the advent of green chemical technologies for more sustainable processes, protocols have attempted a shift from the use of toxic heavy metals and stoichiometric quantities of reagents into novel, benign, and recyclable heterogeneous catalysts for different processes. As part of our research endeavors towards the utilization of greener catalysts for industrially relevant transformations, we report herein the utilization of highly active, stable and versatile Al-SBA-15 in a series of glycerol transformations to valuable compounds including esterification with levulinic acid and acetalysation with furfural and a range of carbonyl compounds.

2. Experimental

2.1. Materials

Pluronic (P123), sodium metasilicate, tetraethyl orthosilicate (TEOS), aluminium isopropoxide, glycerol, levulinic acid, formaldehyde, benzaldehyde, furfural, acetone, deuterium oxide, hexane, diethyl ether and ethanol employed in this work were purchased from Aldrich, Scharlau and Panreac. All chemicals were used without further purification, except furfural which was purified by column chromatography.

2.2. Preparation of Al-SBA-15

The catalysts were prepared according to a previous reported methodology.¹⁴ Around 20 g of P123 template, 700 mL of HCl solution and the desired quantity of Al precursor (aluminium isopropoxide, in order to reach a Si/Al 30 ratio in the synthesis gel) were added (pH 1.5) and then mixed until all P123 was dissolved. The silica precursor (TEOS) was then added dropwise to the solution. The mixture was then stirred for 24 hours at 100°C (aging) until a white solid was formed. The material was then filtered off, dried in the oven and eventually calcined for 24 h at 550°C under air.

2.3. Preparation of Zr-SBA-16

Zr-SBA-16 materials were synthesized according to a previous literature report.¹⁵ In a typical synthesis, 16 g of a 10% aqueous solution P123 (EO₁₀₆PO₇₀EO₁₀₆), 26 g distilled water and 4.71 g sodium metasilicate (Na₂SiO₃•9H₂O) were stirred together at 40°C until the formation of a clear solution. 13.6 g HCl (35%) with the target amount of zirconyl chloride (ZrOCl₂•8H₂O, to achieve a Si/Zr ratio of 25 in the gel) were subsequently added under vigorous stirring. The molar composition of the gel mixture was 1.0 SiO₂: x Zr: 3.17•10⁻⁴ P123: 6.68 HCl: 137.9 H₂O. The solution was continuously stirred for 120 min (optimum conditions)^{15a} and subsequently microwave-irradiated in a microwave digestion system (Milestone Corporation, ETHOS-1) for 120 min at 100°C. The solid product was eventually filtered off, dried at 120°C overnight and calcined at 500°C. The material was prepared with a Si/Zr ratio of 25 and denoted as Zr-SBA-16 (25).

2.4. General procedure for catalytic experiments

2.4.1. Esterification of glycerol with levulinic acid

In a typical experiment, the catalyst (0.025 to 0.05 g), levulinic acid and glycerol (4:1 molar ratio) were placed inside an ampoule and the mixture was then heated at different temperatures (100, 120 or 140 °C) under continuous stirring for 8h. Upon reaction completion, the resulting mixture was filtered, extracted with ethanol and subsequently analyzed using GC-MS. The products mono-, di- and tri-acetylglycerides were identified by GC-MS (and their corresponding ratios). The response factors of the starting material and products were determined using naphthalene as external standard.

2.4.2. *Glycerol acetalisation with aldehydes*

2.4.2.1. *Formaldehyde (source: paraformaldehyde)*

In a typical acetalisation reaction, the catalyst (0.005-0.01 g) was suspended in a mixture of glycerol (1 mmol) and paraformaldehyde (1 mmol) inside an ampoule under stirring at 100°C for 8h. The resulting mixture was then filtered, ethanol-extracted and analyzed by GC-MS. Reaction products including 5-hydroxy-1,3-dioxane and 4-hydroxymethyl-1,3-dioxolane were identified by GC-MS.

2.4.2.2. *Benzaldehyde*

In a typical acetalisation reaction with benzaldehyde, the catalyst (0.05-0.1 g) was suspended in a mixture of glycerol (1 mmol) and benzaldehyde (1 mmol) inside an ampoule under stirring at 100°C for 8h. Upon reaction completion, the resulting mixture was then filtered off, extracted using ethanol and analyzed by GC-MS. Several reaction products could be observed including (2-phenyl-1,3-dioxolan-4-yl)methanol and 2-phenyl-1,3-dioxane-5-ol using GC-MS and ¹H NMR (D₂O) studies.

2.4.2.3. *Furfural*

Reactions were carried out as in the case of benzaldehyde described above, but the time of reaction for this particularly process was 12h. Reaction products included (2-(furan-2-yl)-1,3-dioxolan-4-yl)methanol and 2-(furan-2-yl)-1,3-dioxan-5-ol and were again identified using GC-MS and ^1H NMR (D_2O).

2.4.3. *Glycerol acetalisation with acetone*

The formation of solketal from glycerol (1 mmol) and acetone (1 mmol) was carried out in an ampoule at 100 °C for 8h under continuous stirring. Products (2,2-dimethyl-1,3-dioxolan-4-yl)methanol and 2,2-dimethyl-1,3-dioxan-5-ol and their ratios were identified by GC-MS.

2.5. *Recyclability tests*

To determine the stability of the catalysts under the investigated conditions, recyclability studies were performed. The catalysts were reused upon reaction completion by simple centrifugation, separation and vacuum drying, followed by subsequent washing (three times) with ethanol and drying prior to their reuse in another catalytic run.

2.6. *Analytical methods*

Upon reaction completion, the quantitative analysis of products was performed by GC-MS. Chromatograms were recorded on a GS-MS turbo system (5975-7820A) model equipped with a HP-5MS capillary column (30 m x 0.25 mm x 0.25 μm), under the following conditions:

Esterification and acetalisation (benzaldehyde and furfural): injector temperature 230°C, detector temperature 250°C, 50°C ramp 10°C/min. until 230°C (held 20min).

Retention times (levulinic acid): peak at 6.73 min. levulinic acid, at 12.50 min. naphthalene, at 12.66 min. monoacetylglyceride, at 19.61 min. diacetylglyceride and at 32.21 min. triacetylglyceride.

Retention times (benzaldehyde): peak at 5.20 min. benzaldehyde, at 12.66 and 12.89 min. two diastereomers of (2-phenyl-1,3-dioxolan-4-yl)methanol, and at 13.54 min. the two diastereoisomers of 2-phenyl-1,3-dioxan-5-ol.

Retention times (furfural): peak at 3.48 min. furfural, at 10.32 and 10.60 min. the two diastereomers of (2-(furan-2-yl)-1,3-dioxolan-4-yl)methanol, at 10.39 and 11.32 min. the other two diastereomers of 2-(furan-2-yl)-1,3-dioxan-5-ol.

Acetalisation (paraformaldehyde and acetone): injector temperature 230°C, detector temperature 250°C, oven temperature program: 40°C (10 min.) ramp 5°C/min. until 100°C and another ramp 9°C/min. until 200°C.

Retention times (paraformaldehyde): peak at 1.54 min. aldehyde, at 10.54 min. 4-hydroxymethyl-1,3-dioxolane, at 11.40 min. 5-hydroxy-1,3-dioxane and at 22.90 min. glycerol (broad peak).

Retention times (acetone): at 14.75 min. (2,2-dimethyl-1,3-dioxolan-4-yl)methanol, at 16.26 min. 2,2-dimethyl-1,3-dioxan-5-ol and at 22.90 min. glycerol (broad peak).

NMR spectra were recorded using Varian Mercury 300 spectrometer. Chemical shifts (δ) are reported in ppm and were measured relative by the internal referencing to the D₂O (¹H).

3. Results and discussion

Al-SBA-15 (Si/Al 30 ratio) possessed typical textural and structural properties as compared to previously reported analogous materials.¹⁴ The material possessed a surface area of 720 m² g⁻¹, a pore size of ca. 8 nm and a pore volume of 0.8 mL g⁻¹. Surface acidity measurements by means of titration with pyridine (PY) and 2,6-dimethylpyridine (DMPY) showed the catalyst contained a good balance between Lewis and Brønsted acid sites (Table 1), in good agreement with previous surface acidity results.¹⁴ Relatively similar results were found for Zr-SBA-16, although a higher total acidity and larger proportion of Lewis acid sites were determined in this material (Table 1). Structural characteristics of analogous mesoporous Al-SBA-15 materials (XRD, TEM and N₂ physisorption) have also been previously reported.¹⁴

In view of such measured acidity, Al-SBA-15 materials have a promising potential as solid acid catalysts for various acid-catalysed processes. The catalytic activity of Al-SBA-15 was subsequently investigated in a range of esterification and acetalisation processes for glycerol valorization to useful polymer-intermediates and fuel oxygenated additives.

Table 1. Textural and surface acid properties of Al-SBA-15 and Zr-SBA-16 materials

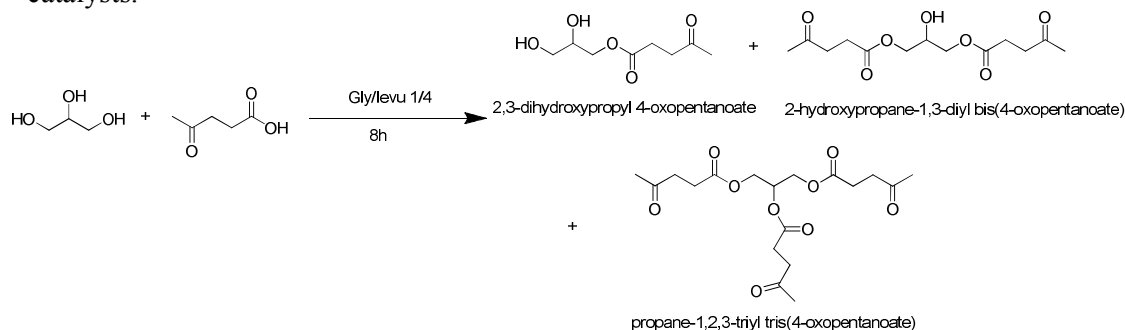
Catal.	Surface area (m ² g ⁻¹)	Pore size/volume (nm/mL g ⁻¹)	Surface acidity at 300°C/μmolg ⁻¹		
			PY (total acidity)	DMPY (Brønsted acidity)	Lewis acidity
Al-SBA-15 (30)	720	8.0/0.8	140	75	65
Zr-SBA-16 (25)	> 600	6.0/0.6	233	33	200

3.1. *Esterification of glycerol with levulinic acid*

Traditionally, mineral acids have been used as catalysts in the esterification of glycerol to prepare mono-, di- and triglycerides that find a number of applications in the food industry.¹⁶ However, heterogeneous catalysts have various advantages in terms of simple recovery and/or recycling, with structures or textural properties potentially influencing reaction selectivities (e.g. porous network). Different solid acids including zeolites and acidic mesoporous materials have been recently reported in glycerol esterification¹⁷⁻²⁰ which can render a range of value-added products including pharmaceutical intermediates, foodstuffs, plasticisers and insecticides.²¹⁻²³

The esterification of glycerol with levulinic acid was carried out using Al-SBA-15. The effect of various parameters in the reaction including temperature and catalyst loading were studied to optimize the reaction conditions (Table 2). Blank runs (in the absence of catalyst) provided negligible glycerol conversion even at temperatures above 120°C and longer times of reaction (Table 2). Al-SBA-15 exhibited a good conversion to products at 120°C, with high selectivity to monoacylglycerides (Table 2, entry 2). Diacylglycerides became major products at reaction temperatures of 140 °C, with quantitative conversion of starting material (Table 2, entry 3). Interestingly, product selectivity remained unchanged at high conversion values when decreasing catalyst loadings in the esterification reaction (Table 2, entry 4). A higher catalytic activity was comparably obtained for Zr-SBA-16 (Table 2, entry 5). Clearly, Zr-SBA-16 possesses a superior Lewis acidity as compared to Al-SBA-15 (i.e. DMPY-PY value is a rather accurate measure of Lewis acidity; this was found to be 65 for Al-SBA-15 as compared to 200 for Zr-SBA-16). These findings therefore suggest that the proposed esterification reaction was largely promoted by Lewis acid sites.

Table 2. Esterification of glycerol with levulinic acid using mesoporous solid acid catalysts.^a



Entry	Catalyst	μmol of acid groups per mmol of glycerol	Mono/Di/Tri Selectivity (mol %)	Temperature ($^{\circ}\text{C}$)	Conversion (%)
Blank	-	-	-	140	<10
1	Al-SBA-15	7	-	100	-
2	Al-SBA-15	7	94/5/1	120	78
3	Al-SBA-15	7	0/85/15	140	>99
4	Al-SBA-15	3.5	6/85/9	140	85
5	Zr-SBA-16 (25) ^b	5.82	77/23/0	100	70

^a Reaction conditions: 1 mmol glycerol, 4 mmol levulinic acid, catalyst, solventless, 8h. ^b Zr-SBA-16 (Si/Zr 25 ratio).

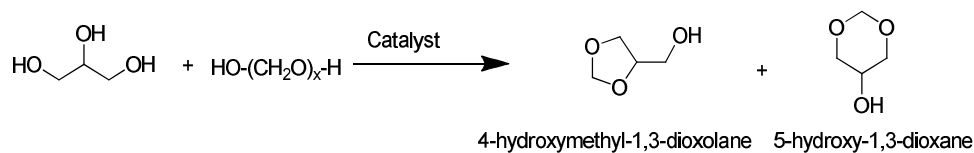
3.2. Acetalisation of glycerol with aldehydes

The acetalisation of glycerol is an important reaction for the synthesis of six- and five-membered cyclic products that find a wide range of industrial applications. Glycerol acetals and ketals have been extensively utilized as additives fuels, binders as well as in formulations of water-based inks.²⁴⁻²⁶ A variety of heterogeneous catalysts have been studied in glycerol acetalisation including exchanged resins,²⁷ heteropolyacids,²⁸ mesoporous materials,^{29, 20} and zeolites.³⁰

3.2.1. Paraformaldehyde

The results obtained in the acetalisation of glycerol with paraformaldehyde have been summarised in Table 3. The reaction conditions (molar ratio of glycerol to formaldehyde, temperature and time) were selected based on our experience and results obtained by Ruiz *et al.*³⁰ The condensation of glycerol with paraformaldehyde as aldehyde generally leads to the formation of a six-membered cyclic acetal as stable product (Table 3), even more remarkable for Al-SBA-15 as compared to Zr-SBA-16 (Table 3, entry 4). Results seem to point to a Brønsted-acid promoted reaction taking into account the low Brønsted acidity of Zr-SBA-16 and compared to Al-SBA-15, which was proved to be highly active even at low catalyst loadings (Table 3, entries 1, 2 and 3).

Table 3. Catalytic activity of Al-SBA-15 and Zr-SBA-16 (25) in the acetalisation of glycerol with paraformaldehyde.^a



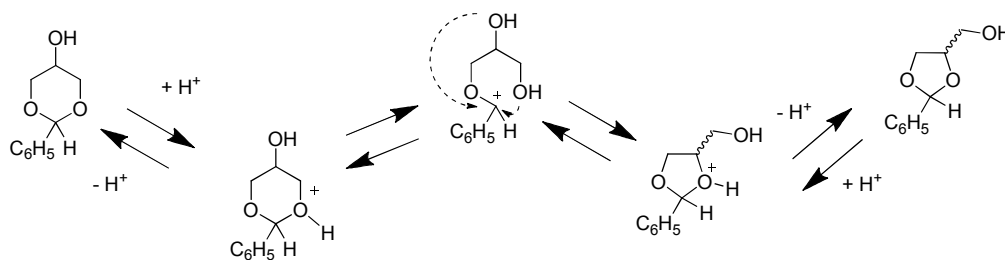
Entry	Catalyst	μmol of acid groups	Selectivity (dioxolane/dioxane)	Conversion
		per mmol of glycerol		(%)
1	Al-SBA-15	2.8	34/66	96
2	Al-SBA-15	1.4	36/64	93
3	Al-SBA-15	0.7	31/68	43
4	Zr-SBA-16 (25) ^b	23.3	26/74	44

^a Reaction conditions: 1 mmol glycerol, 1 mmol paraformaldehyde, solventless 100°C, 8h.

^b Zr-SBA-16 (Si/Zr 25 ratio).

3.2.2. Benzaldehyde.

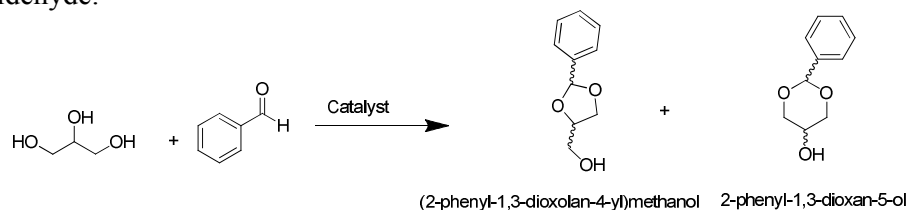
Selectivity comparably changes from dioxane to dioxolane (from a 6-membered ring to a 5-membered ring) in the acetalisation of glycerol with benzaldehyde, in good agreement literature results.^{27, 31} However, the evolution of five- to six-membered rings at longer times of reaction was reported by Deustch *et al.*²⁷ To further prove the stability of the dioxolane product under the investigated reaction conditions (Scheme 1), the reaction mixture was subsequently reacted overnight. After 24 h+ reaction, the five-membered was still preferentially obtained as major reaction product, in contrast with results from Deustch *et al.* The effect of Al-SBA-15 loading on glycerol conversion was subsequently investigated (Table 4). Catalytic experiments were conducted by varying the catalyst amount (0.05 and 0.1 g, 7 and 14 μmol of acid groups in the catalyst per mmol of glycerol, respectively) under identical reaction conditions. No significant improvements on glycerol conversion or selectivity were observed as evidenced in Table 4.



Scheme 1. Acid-catalysed equilibrium between C6 and C5 products obtained in glycerol acetalisation with benzaldehyde.

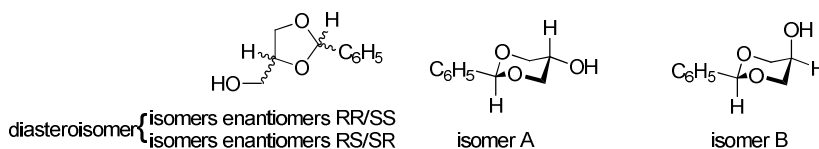
The synthesised product mixture contained two pairs of diastereomers, each of which is formed by two C5 enantiomers and two C6 diastereomers (Scheme 2) as identified by GC-MS and ^1H -RMN.

Table 4. Catalytic activity of Al-SBA-15 in the acetalisation of glycerol with benzaldehyde.^a



Entry	Catalyst	μmol of acid groups per mmol of glycerol	Selectivity (dioxolane/dioxane)	Conversion (%)
1	Al-SBA-15	7	83/17	72
2	Al-SBA-15	14	83/17	82

^a Reaction conditions: 1 mmol glycerol, 1 mmol benzaldehyde, solventless, 100°C, 8h.



Scheme 2. Conformational isomers of (2-phenyl-1,3-dioxolan-4-yl)methanol and 2-phenyl-1,3-dioxane-5-ol.

Chromatograms showed three distinctive products, with mass spectra revealing C5 diastereomers (first two peaks) and C6 diastereomers (third peak, Figure 1A). ¹H NMR spectra exhibited four peaks corresponding to OCH(C₆H₅)O, C5 [5.82 and 5.71 ppm] and C6 [5.58 and 5.45 ppm] (Figure 1B). All chemical shifts were found to be in agreement with literature results.²⁷

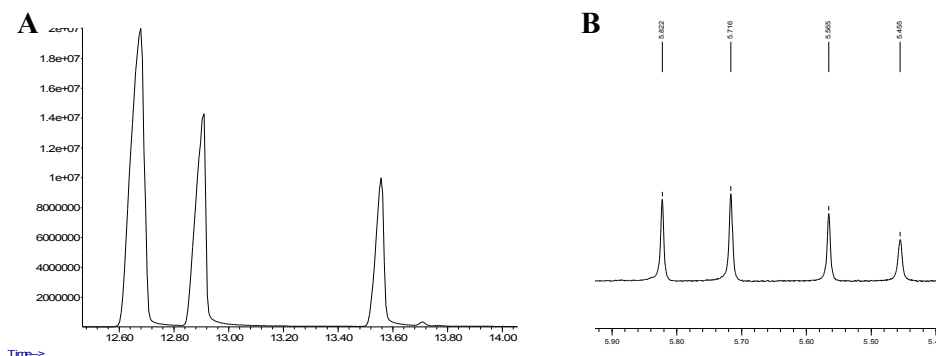
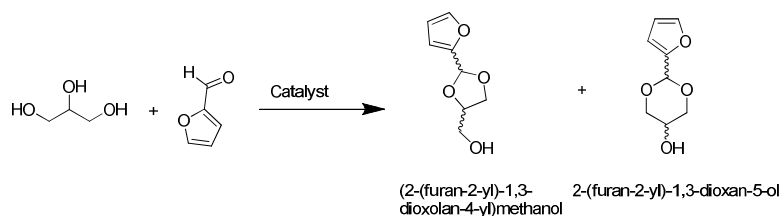


Figure 1. Product mixture from glycerol acetalisation with benzaldehyde. **A)** GC Chromatogram. **B)** ¹H NMR Spectrum.

3.2.3. Furfural

Similar product and catalytic activity trends could be observed in the acetalisation of glycerol with furfural as aldehyde source. The reaction was found to be kinetically controlled, with the catalytic formation of five-membered cyclic acetals proceeding at a higher rate with respect to those of six-membered cyclic acetals. Such behavior might be attributed to the increasing torsional effect in 6-membered rings with cyclic and aromatic substrates.

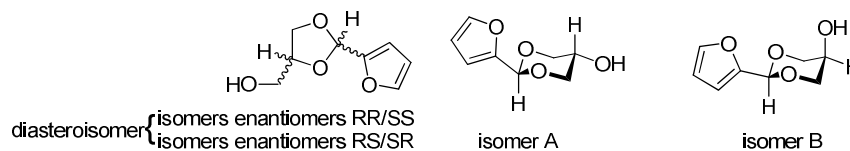
Table 5 summarises results for the acetalisation reaction of glycerol with furfural. Good conversions in the systems (ca. 70%) could be achieved at 100°C after 12 h reaction, in agreement with literature reports.^{32,33} Importantly, an increase in catalyst loading did not significantly influence the conversion under the investigated reaction conditions.

Table 5. Catalytic conversion of glycerol and furfural to cyclic acetals.^a

Entry	Catalyst	μmol of acid groups per		Selectivity (dioxolane/dioxane)	Conversion (%)
		mmol of glycerol			
1	Al-SBA-15	7		67/33	69
2	Al-SBA-15	14		68/32	74

^a Reaction conditions: 1 mmol glycerol, 1 mmol furfural, solventless 100°C, 12h.

Different 5- and 6-membered stereoisomers were again obtained as depicted in Scheme 3. Products identification by GC-MS pointed to the presence of four peaks (Figure 2), further confirmed by mass spectrometry as two C5 and C6 isomers, respectively. The mixture was subsequently purified by column chromatography using a silica column (eluted with 1:2 hexane/diethyl ether³²) and attempted to identify individual products by GC-MS and ¹H-RMN. A 2-(furan-2-yl)-1,3-dioxan-5-ol diastereomer could be isolated as pure compound.



Scheme 3. Conformational isomers of (2-(furan-2-yl)-1,3-dioxolan-4-yl)methanol and 2-(furan-2-yl)-1,3-dioxan-5-ol.

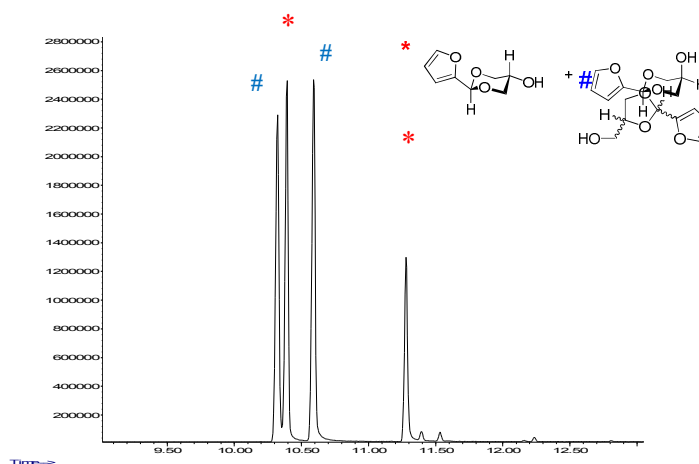
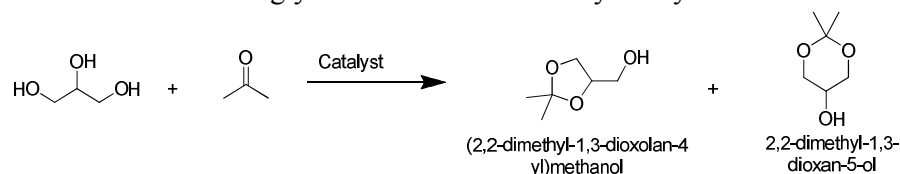


Figure 2. Chromatogram reaction with Al-SBA-15, 1 mmol glycerol, 1 mmol furfural, 8h, 100°C (selectivity 68/32).

3.3. Acetalisation of glycerol with acetone

The acetalisation of glycerol with acetone is another relevant process for glycerol valorization to produce solketal (2,2-dimethyl-1,3-dioxolan-5-ol) (Table 6). This molecule constitutes an excellent product as additive in gasoline formulations as well as diesel and biodiesel fuels. The catalyst loading was found to be critical in the conversion of the systems (Table 6, entries 1 vs 2), with Al-SBA-15 exhibiting comparable activities to those previously reported using Amberlyst-15.²⁷

Table 6. Acetalisation of glycerol with acetone catalyzed by Al-SBA-15.^a



Entry	Catalyst	μmol of acid groups per mmol of glycerol	Selectivity (dioxolane/dioxane)	Conversion (%)
1	Al-SBA-15	7	99/1	6
2	Al-SBA-15	14	99/1	75

^a Reaction conditions: 1 mmol glycerol, 1 mmol acetone, solventless 100°C, 8h.

3.4. Reusability of Al-SBA-15

The reusability and stability of the catalyst are crucial features of catalysts besides the activity and selectivity for practical applications. The possibility to reuse Al-SBA-15 in all conducted reactions (esterification and acetalisation) was subsequently explored, with results discussed in Figures 3 to 7. Al-SBA-15 was fairly stable and reusable in most cases, preserving most initial catalytic activity after several uses. In the case of the esterification of glycerol with levulinic acid, results from Figure 3 prove the high stability and possibility to recycle the catalyst up to five uses without any noticeable decrease in activity. The selectivity was also preserved in reused Al-SBA-15 material.

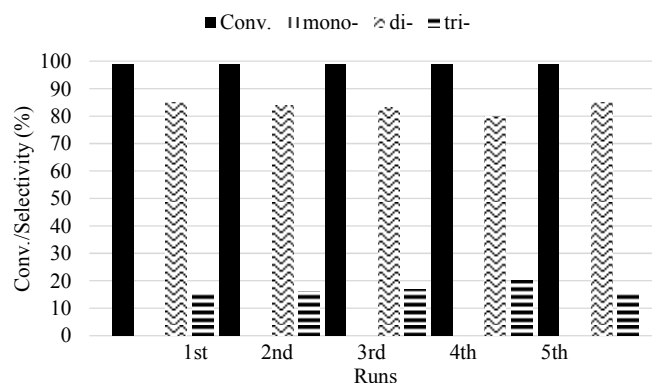


Figure 3. Reusability of Al-SBA-15 in the esterification of glycerol with levulinic acid. Reaction conditions: 1 mmol glycerol, 4 mmol levulinic acid, 0.05 g catalyst (7 μ mol of acid groups in the catalyst per mmol of glycerol), solventless 140°C, 8h reaction.

Figure 4 comparably shows that Al-SBA-15 exhibited a poor reusability in the acetalisation of glycerol with paraformaldehyde. The activity was preserved in the first reuse but over 40% of its initial activity was already lost after three reuses (Figure 4). Interestingly, the observed significant drop in activity was also accompanied by a change in selectivity towards a favoured production of 6-membered acetal products. The

observed reduction may be caused by the formation of physisorbed species and/or carbonaceous deposits on the surface of the catalyst.

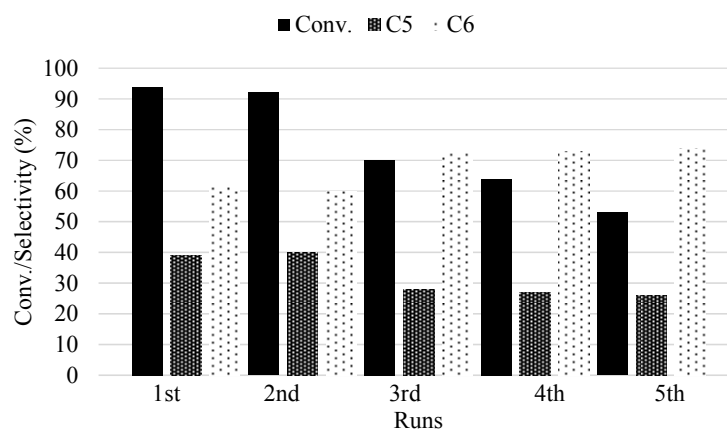


Figure 4. Experiments of catalyst recycling in the acetalization of glycerol with paraformaldehyde. Reaction conditions: 1 mmol glycerol, 1 mmol paraformaldehyde, 100°C, 0.01 g catalyst (1.4 μmol of acid groups per mmol glycerol), solventless, 8h reaction.

In contrast with glycerol acetalisation using paraformaldehyde, Al-SBA-15 was found to also lose activity in the acetalisation of glycerol with benzaldehyde (around 20% of initial activity, Figure 5) but only after the first reuse. Subsequent reuses of the catalyst provided essentially identical activities, with also analogous selectivities to the major C5 cyclic product (Figure 5). A similar behaviour was also observed in the acetalisation of glycerol with furfural (Figure 6). The observed activity drop after the first run could be due to deactivation of strong Brønsted acid sites in the reaction (i.e. by coking) in a similar way to that observed in the acetalisation of glycerol with paraformaldehyde (Figure 4). Selectivity remained unchanged after several reuses, with a preferential formation of 5-membered acetal products.

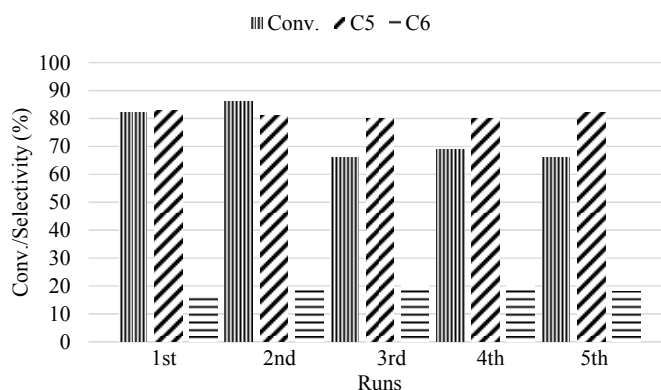


Figure 5. Al-SBA-15 recycling experiments in the acetalisation of glycerol with benzaldehyde.

Reaction conditions: 1 mmol glycerol, 1 mmol benzaldehyde, 100°C, 0.1 g catalyst (14 μ mol of acid groups per mmol glycerol), solventless, 8h reaction.

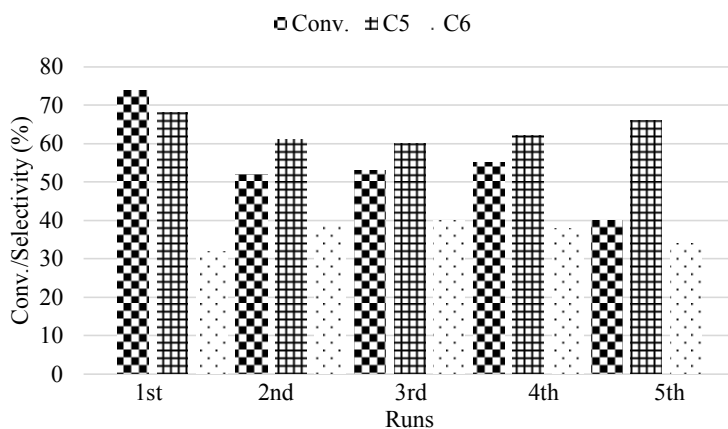


Figure 6. Reuse experiments for Al-SBA-15 in the acetalisation of glycerol with furfural.

Reaction conditions: 1 mmol glycerol, 1 mmol furfural, 100°C, 0.1 g catalyst (14 μ mol of acid groups per mmol glycerol), solventless, 12h reaction.

An interesting recycling behavior was observed for Al-SBA-15 in the acetalisation of glycerol with acetone (Figure 7). The stability of the catalyst was remarkably improved as compared to previous acetalisation with paraformaldehyde, benzaldehyde or furfural up to 4 cycles. Interestingly, the activity significantly dropped after the fourth cycle (70% of the initial activity) which could be related to a partial

deactivation of the catalyst due to formation of carbonaceous deposits. Solketal was selectively obtained in all runs as major product.

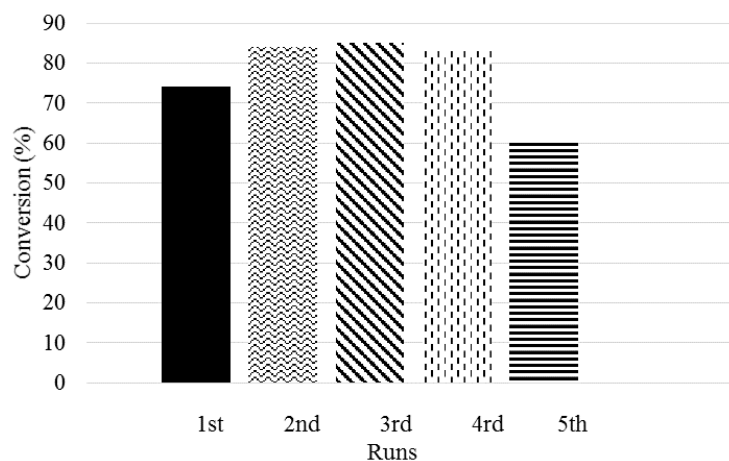


Figure 7. Reusability study for the acetalisation of acetone with glycerol using Al-SBA-15 as catalyst. Reaction conditions: 1 mmol glycerol, 1 mmol acetone, 100°C, 0.1 g catalyst (14 μmol of acid groups per mmol glycerol), solventless, 8h reaction.

Conclusion

A highly stable, recyclable and efficient Al-SBA-15 catalyst was utilized as heterogeneous catalyst in two important industrial reactions (esterification and acetalisation). Both Al-SBA-15 and Zr-SBA-16 exhibited very good conversions to monoacylglycerides, with a reaction promoted by Lewis acid sites. Comparably, Al-SBA-15 provided improved yields to products in acetalisation reactions promoted by Brönsted acid sites. Interestingly, the use of linear chain aldehyde precursors tend to favor the preferential production of 6-membered ring isomers, while the use of cyclic substrates lead to the formation of 5-membered isomers. The simplicity of the methodology and the catalyst make this protocol potentially useful to related glycerol and polyol chemistries with advanced functional materials (e.g. supported nanoparticles on Al-SBA-15) to be reported in due course.

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