

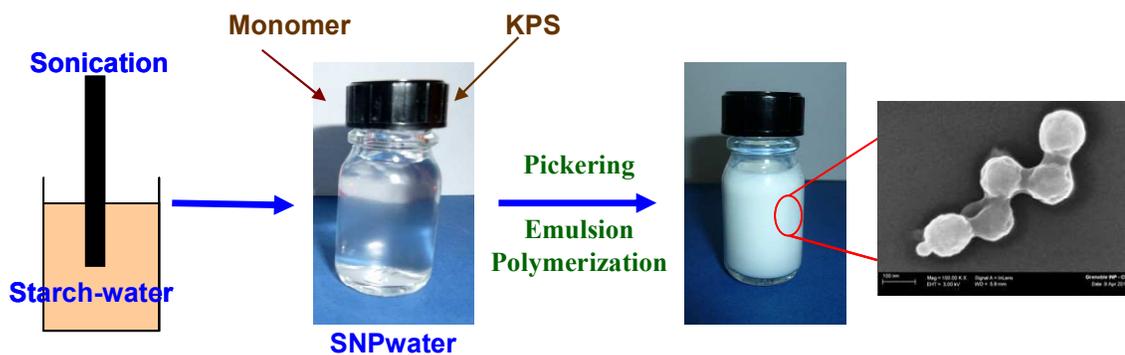


Starch Nanoparticles produced via ultrasonication as a sustainable stabilizer in Pickering Emulsion polymerization

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A facile and effective method for the Pickering emulsion polymerization of acrylate monomer was reported, using SNPs as a sole stabilizer. The SNPs were produced via ultrasonication in water without any chemical additives



21

22 **Abstract**

23

24 Pickering emulsion polymerizations using starch nanoparticles (SNPs) as a sole stabilizer and
25 persulfate as an initiator have been successfully accomplished. The SNPs were prepared in
26 water via high-power ultrasonication without the addition of any chemical reagent. The
27 polymer dispersion stabilized by SNPs proved to be stable for several months, when the SNP
28 content was above 4 wt% relative to the monomer phase. As the SNP loading increased, the
29 particle sizes of the polymer dispersion decreased steadily, confirming the key role of the
30 SNPs in the stabilization process. On the basis of the zeta-potential measurement and change
31 in polymer particle size during emulsion polymerization, a mechanistic aspect of the
32 Pickering emulsion polymerization is proposed. The film-formation properties of the
33 nanocomposite dispersion and the optical properties of the ensuing films are also discussed. It
34 was shown that nanocomposites formed prepared via the Pickering emulsions route displayed
35 better optical transparency than that obtained by ex-situ mixing route.

36

37 *Key words:* Pickering, starch nanoparticles, emulsion polymerization.

38

39 Introduction

40

41 In recent years, the production of nanoparticles from naturally occurring biopolymers such as
42 cellulose¹, chitin² and starch³ has drawn considerable attention because they combine the
43 advantageous properties of biopolymers, namely the broad range of chemical modifications,
44 renewability and sustainability, with the specific attributes of nanosized materials, which in
45 turn has expanded the spectrum of potential applications.

46 Although much less studied than nanocellulose or cellulose nanocrystals, the extraction and
47 uses of starch nanoparticles (SNP) have been the subject of numerous reports^{4,5}. Current
48 potential use of SNP is as a reinforcing phase in a polymeric matrix to improve the
49 mechanical and barrier properties of the materials⁶. SNP can be produced via the acid
50 hydrolysis route, leading to starch nanocrystals with a well defined platelet-like shape and a
51 highly crystalline structure. It can be also produced via a physical disintegration process
52 without the need to implement any chemical treatment or to add any chemical reagent. This
53 latter route affords environmentally friendly approaches and is arousing increasing interest. In
54 this context, we have described an efficient approach for the preparation of nano-sized starch
55 particles using the purely physical method of high-intensity ultrasonication⁷. The process is
56 based on the high-power ultrasonication of a suspension of starch granules in water at 1 to 2%
57 consistency and at a temperature of 8-10°C. It was shown that complete conversion of the
58 starch granules from a micronic to a nanometric scale is achieved after 75 min ultrasonication,
59 generating nanoparticles from 20 to 100 nm in size. This process constitutes a green approach
60 to the production of SNP with a high yield and without the need to undertake any post
61 purification treatment.

62 Currently, SNPs are mainly used as a nanofiller in polymer matrixes, where an improvement
63 in the barrier properties and mechanical properties has been reported⁸. In most processing

64 routes for preparing SNP-based nanocomposite, two-pot mixing involving an SNP suspension
65 with waterborne polymer dispersion remained the most commonly used and most efficient
66 approach, ensuring the preservation of the individualized state of the nanoparticles. However,
67 this approach is time-consuming and involves multiple steps.

68 *In situ* polymerization in the presence of SNPs could be envisaged as an alternative way to
69 produce a one-pot nanocomposite dispersion ready for use and with good dispersion of the
70 nanofiller within the matrix. Preparation of the emulsion with the nanoparticles present (*in-*
71 *situ* approach) has the further advantage of: (i) creating the formulation in one step rather than
72 through the so-called *ex-situ* approach requiring the nanoparticles to be blended with the
73 polymer latex after polymerization has taken place, (ii) reducing the necessary processing
74 steps, and (iii) avoiding the dilution and mixing phase. In addition, this strategy results in a
75 more efficient binding of the nanoparticles onto the polymer particles. This allows improved
76 tailoring of the nanocomposite characteristics on the nanoscale level, favoring nanoparticle
77 individualization⁹.

78 The presence of nanoparticles during emulsion polymerization might be further exploited to
79 induce what is known as Pickering stabilization. Using solid particles, conventional
80 emulsifying agents can be omitted and hazardous surfactants may be replaced by less harmful
81 materials and more environmentally-friendly components¹⁰. The use of surfactants is known
82 to have an adverse effect on the mechanical and water-resistance properties of the resulting
83 films¹¹, and also contribute to generating foams and fine bubbles. All of these attributes make
84 the Pickering polymerization approach of great interest.

85 In Pickering emulsions, solid particles of intermediate wettability with dimensions ranging
86 from several nanometers to several micrometers attach to liquid-liquid interfaces and provide
87 emulsion stability. Emulsions stabilized by solid particle emulsions are known to display
88 higher stability against coalescence compared to systems stabilized by surfactants. The

89 stabilization has been explained by the volume exclusion created by the adsorbed particles
90 preventing contact between neighboring oil–water interfaces and by the Gibbs free energy
91 penalty incurred by removing the adsorbed solid particles away from the interface¹².

92 The use of polysaccharide-based nanoparticles, such as cellulose nanofibrils¹³, cellulose
93 nanocrystals¹⁴ and, recently, starch nanocrystals¹⁵ and cellulose as solid-emulsifiers has
94 received increasing attention in a broad field of applications such as food technology,
95 cosmetic formulation, and pharmaceutical products. The wide availability of these particles,
96 their relative ease of production, combined with their biodegradability and non-toxic
97 character, are all factors driving the use of this class of nanoparticle as a stabilizer to replace
98 synthetic surfactant.

99 The use of SNPs as a Pickering stabilizer for the *in situ* emulsion polymerization to elaborate
100 SNP-based nanocomposite has not yet been explored. In a recent work, starch nanoplatelets
101 were found to provide a synergistic effect with cationic surfactant in stabilizing butyl
102 methacrylate mini-emulsions during polymerization¹⁶. The emulsion polymerization strategy
103 using SNPs as a stabilizing agent is expected to result in better attachment of the
104 nanoparticles onto the polymer particles, which in turn would lead to improved tailoring of
105 the nanocomposite characteristics on the nanoscale level and favor nanoparticle
106 individualization¹⁷, and possibly even promote the formation of chemical linkages between
107 the polymer and the nanofiller. This, in turn, is expected to lead to higher film transparency,¹⁸
108 with a higher nanoparticle reinforcing potential. The use of water as a dispersion medium also
109 has environmental benefits and gives a direct one-pot route to waterborne film-forming
110 nanocomposite dispersions ready for use as water-based coatings and adhesives.

111 In this research, we report the successful Pickering emulsion polymerization of acrylic
112 monomers using SNPs prepared via ultrasonication as a sole stabilizer. The effect of the SNP

113 content on the particle size, the colloidal properties of the polymer dispersion and the optical
114 properties of the ensuing nanocomposites were investigated.

115 **Experimental set-up**

116 *Materials*

117 Butyl methacrylate (BMA, Aldrich, 99 wt%) was distilled under vacuum and kept refrigerated
118 until use. Potassium persulfate (KPS) was supplied by Sigma Aldrich and used without
119 further purification. Distilled water was used for all the polymerization and treatment
120 processes. Waxy maize (WaxyliTM, > 99% amylopectin) was provided by Roquette S.A.
121 (Lesterm, France).

122 *Starch nanoparticle preparation*

123 The SNPs were prepared by adopting the procedure described in our previous work⁷. More
124 specifically, 1.5 g of starch was added to 100 ml of water and sonicated at 80% power output
125 for 75 min using a 20kHz Branson digital Sonifier S-450D (Germany) coupled with a horn
126 with a tip diameter of 13 mm. The ultrasonication treatment was conducted at a temperature
127 below 10°C. The temperature was reached by immersing the starch suspension in a
128 thermostated bath maintained at a temperature of $8 \pm 1^\circ\text{C}$. At the end of the ultrasonication
129 treatment, the starch suspension turned from turbid white to transparent.

130 *Emulsion polymerization*

131 The emulsion polymerization of BMA was carried out in the presence of SNP suspension at
132 70°C using KPS as an initiator. The typical formulation is the following: Water (17 g),
133 monomers MBA (3g) and KPS (0.12 g) and SNPs (from 0.05 up to 0.3 g).

134 The following procedure was adopted to implement the emulsion polymerization reaction: the
135 appropriate amount of SNPs in water (with a solid content of 2%) was weighed first, then
136 BMA monomer and KPS initiator were added and kept under magnetic stirring for several
137 minutes to create the monomer emulsion. The resulting emulsion was then flushed with N₂

138 and the polymerization started by heating the emulsion to 70°C. Polymerization occurred
139 within 3h.

140 ***Particle size determination***

141 The emulsion droplet diameters were measured at 25°C using a Malvern Nano-Zetasizer ZS
142 instrument at a fixed scattering angle of 173°. The dispersion was diluted to about 5 wt% with
143 distilled water before starting the measurements. The cumulative average determined from the
144 dynamic light scattering (DLS) correlation curve was fitted with a single exponential decay to
145 determine the particle size distribution. Each measurement was performed in triplicate and the
146 values obtained averaged to obtain the mean particle size.

147 ***Zeta-Potential Measurement***

148 The zeta-potentials were measured at 25°C using a laser Doppler electrophoresis apparatus
149 (Malvern Nano-Zetasizer ZS, UK). The sample consistency in water was set at 0.01% (w/v).
150 The measurements were performed three times for each sample.

151 ***FE-SEM microscopy***

152 Field Emission Scanning Electron Microscope (FE-SEM) images were obtained with a Zeiss
153 Supra40. Images were created by the SMARTSEM software. A drop of a diluted suspension
154 of starch (with a solid content of about 0.02wt.%) was deposited on a silicon wafer,
155 evaporated at room temperature and then coated with a thin carbon layer limited to 3 nm
156 applied by sputtering. In the case of the polymer dispersion, the drop of diluted dispersion
157 (0.01%) was deposited on a silicon wafer and freeze-dried to prevent the polymer particles
158 from coalescing.

159 ***Dynamic mechanical analysis (DMA)***

160 Dynamic mechanical analysis (DMA) experiments were conducted in tension mode using a
161 PYRIS Diamond DMA (Perkin- Elmer, Waltham, MA, USA). Temperature scans were run
162 from -50°C to 100°C at a heating rate of 2°C min⁻¹, a frequency of 1 Hz and an amplitude of

163 10 μm . The storage (E') as well as the loss factor $\tan \delta$ were measured as a function of
164 temperature. Sample dimensions were about 20mm (length), 5 mm (width) and 0.1– 0.3 mm
165 (thickness).

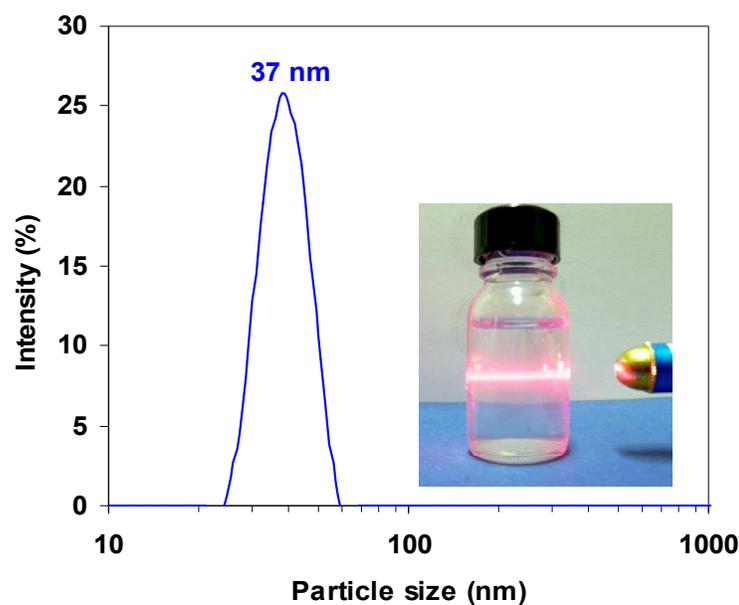
166 The nanocomposite films were prepared via casting of the nanocomposite dispersion in a
167 Teflon mold and storing 40°C until water evaporation was completed.

168 **Results and discussion**

169 *SNP properties*

170 The nano-sized starch particles were prepared via high-intensity ultrasonication without any
171 chemical additives. The process is based on the high-power ultrasonication of a suspension of
172 starch granules in water at 2% consistency for 75 min at a temperature of 8-10°C. After
173 ultrasonication, the suspension became transparent without any change in the fluidity of the
174 solution, which is a good indication of the small size of the starch nanoparticles. This is
175 further confirmed from the Tyndall scattering effect when the suspension is illuminated by a
176 laser beam (see inset Figure 1). It is worth noting that the optical appearance of the dispersion
177 did not change with time and no trace of settling was noted after storing over a period
178 exceeding one month at 8-10°C. This physical method for producing fine starch NPs
179 involving ultrasonication without any chemical additive has been recently developed in our
180 group and has proved to be efficient in reducing the size of starch granules from the micronic
181 to the nanometric scale. The particle size distribution determined from DLS showed a
182 monomodal narrow distribution centered at 37 nm. FE-SEM observation of the particles after
183 depositing a drop of diluted suspension of NPS and drying at room temperature showed
184 nanosized particles 35 to 50 nm in size (Figure 2). The apparent tendency of the nanoparticles
185 to self-associate is inherent to their chemical structure (i.e. high density of surface hydroxyl
186 groups), their nanosized scale and the mode of sample preparation (water evaporation at room
187 temperature). Although it is hard to have a clear-cut indication about the exact morphology of

188 the SNPs, the FE-SEM observation revealed the presence of both a granular, as well as a
189 platelet-like shape. The zeta-potential of the SNP from waxy maize was -3 mV over a pH
190 ranging from 4 to 9, which indicates that the SNPs did not hold any surface charge. The
191 reason for choosing waxy starch lies in its high amylopectin content and the quasi absence of
192 amylose in the starch backbone, which is likely to leach out from the SNPs. Another reason is
193 the insensitivity of SNPs to water, even after prolonged heating at 70°C . Actually, as shown
194 in Figure 3, the particle size remained unchanged at around 37 nm when the SNP suspension
195 was heated for more than 4h at 70°C . This aspect is essential for the following work, in which
196 SNPs were used as a Pickering stabilizer in the emulsion polymerization of acrylic monomer.



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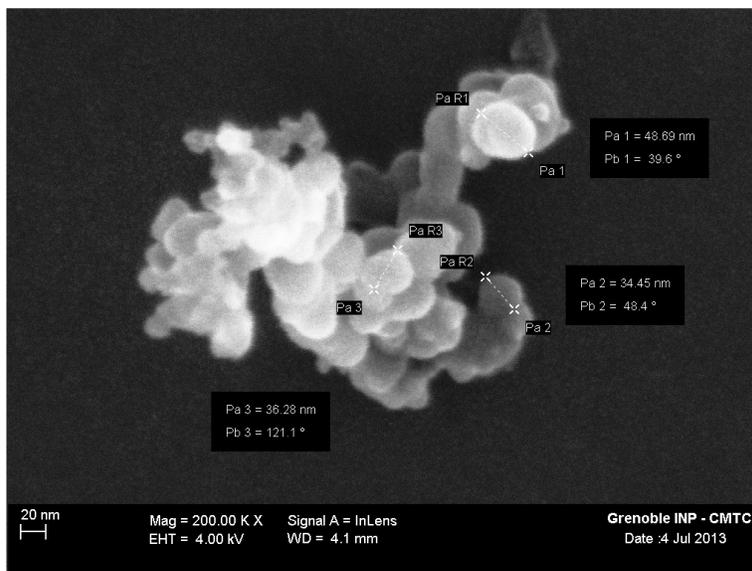
198 **Figure 1: Particle size distribution of SNP from waxy maize and the appearance of the**
199 **SNP suspension (at 1.5 wt.% solid content). Photo showing the Tyndall scattering effect**
200 **(He–Ne laser, 632.8 nm) confirming the presence of colloidal SNPs.**

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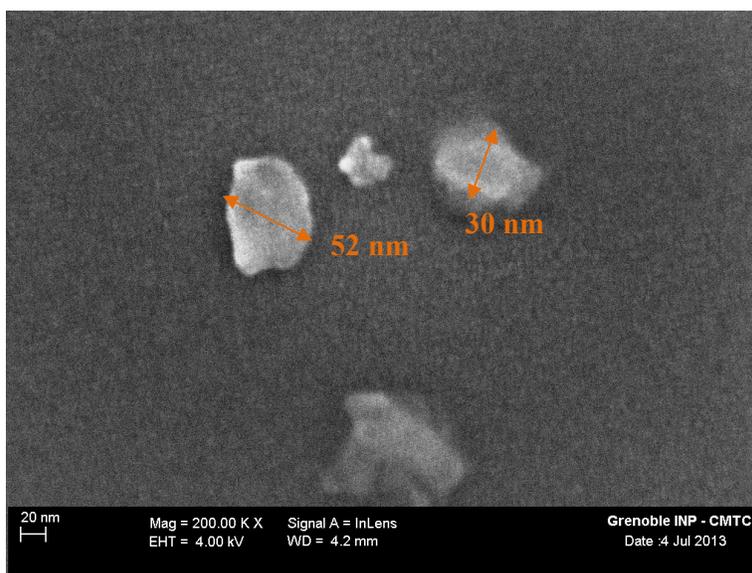
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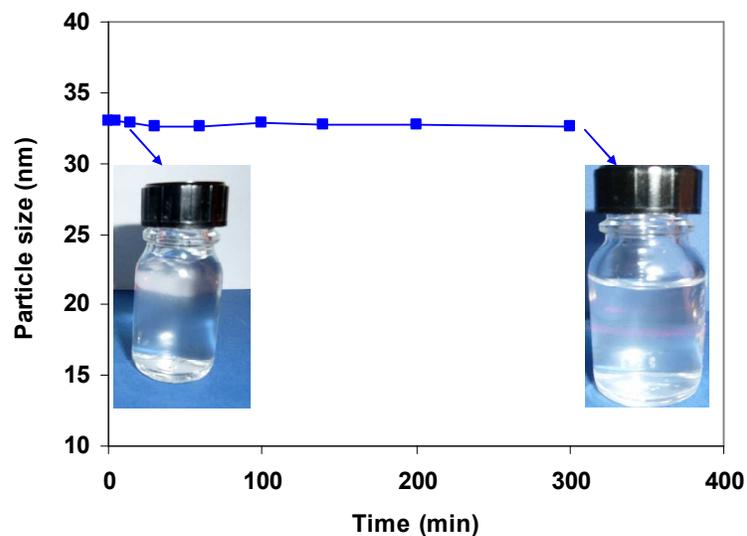
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210 **Figure 2: FE-SEM images of SNPs from waxy maize used in the present work.**

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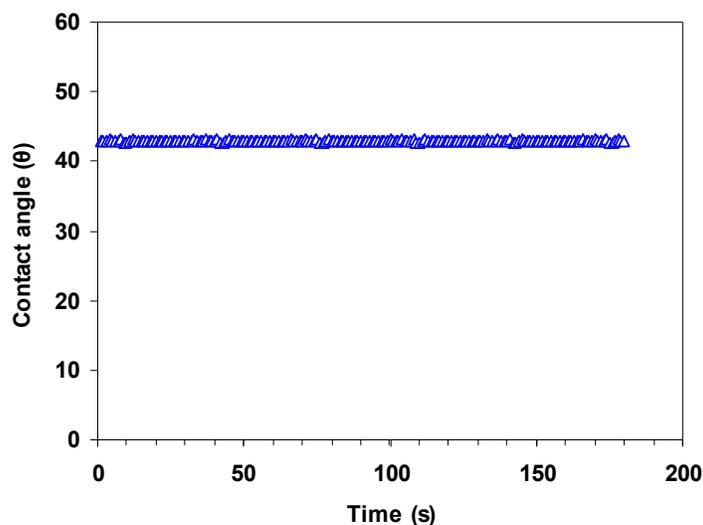


212

213 **Figure 3: Particle size change in SNPs vs time as the suspension with 2% solid content**
214 **was exposed to a temperature of 70°C.**

215

216 To determine the water contact angle on the SNPs, a thin transparent film was formed on a
217 glass slide. The film was prepared by depositing drops of the SNP suspension containing 10%
218 of isopropanol to improve the complete wetting of the glass. A thin, transparent and
219 homogenous film was obtained after drying at 50°C for several hours. This approach has been
220 proven to be effective in determining the water contact angle of SNP, giving a constant angle
221 around 43° (Figure 4).



222

223 **Figure 4. Water contact angle changes vs. time of SNPs from waxy maize films**
224 **deposited on a glass slide.**

225

226 ***Pickering emulsion polymerization***

227

228 The first experiment run in the emulsion polymerization of BMA was carried out in the
229 presence of 6% SNP as sole stabilizer. It was conducted by adding the initiator to the mixture
230 of BMA and the aqueous suspension of SNP, followed by heating at 70°C. Progressively, the
231 dispersion turned from a translucent to a white emulsion with increasing polymerization,
232 giving stable polymer latex free from any coagulum after 3h of reaction at 70°C. A
233 monomodal size distribution centered at 195 nm was obtained and the polymer dispersion
234 remained stable without any change in particle size during storage at room temperature for
235 over 8 months. The same polymerization reaction carried out without SNPs was found to be
236 too slow (conversion limited to about 70% after 6h at a temperature of 70°C) and the polymer
237 dispersion proved to be unstable, resulting in the formation of coarse lumps of polymer
238 particles swollen with monomer after several hours at 70°C. This proves that SNPs were
239 essential in achieving the successful emulsion polymerization of BMA in the absence of any

240 surfactant. We presume that the stabilization process during the formation and growth of the
241 polymer particles was the result of the attachment of the SNPs on to the polymer particles,
242 promoting what it is known as a Pickering stabilization process. Actually, as opposed to the
243 molecular surfactant, which is usually in rapid dynamic equilibrium at the oil/water interface,
244 with the shape and chemical properties of the surfactant molecules determining the
245 emulsifying behavior, in the Pickering emulsions, the oil droplet is stabilized by the reduction
246 of the bare oil-water interface due to the adsorption of the small particles. The adsorbed solid
247 particles provide an efficient steric barrier that hinders the close approach of the droplets and
248 their likely aggregation. In fact, the energetic penalty incurred by removing the adsorbed
249 particles from the interface provides the energetic barrier against coalescence. This has been
250 confirmed in this present study. Indeed, the energy required to remove the particles from the
251 interface can be estimated from Eq. (1)¹⁹:

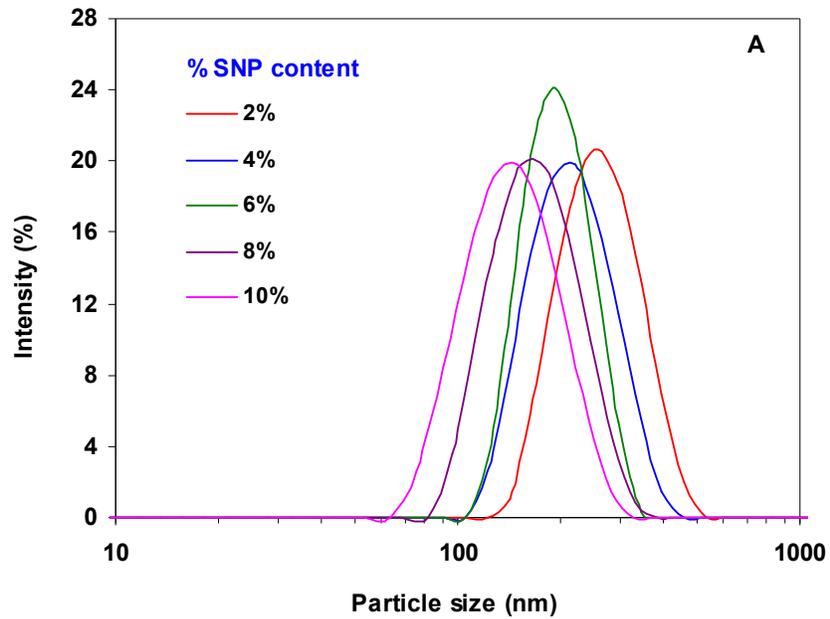
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$$253 \quad E = \gamma_{wp} R^2 (1 - \cos \theta)^2 \quad (1)$$

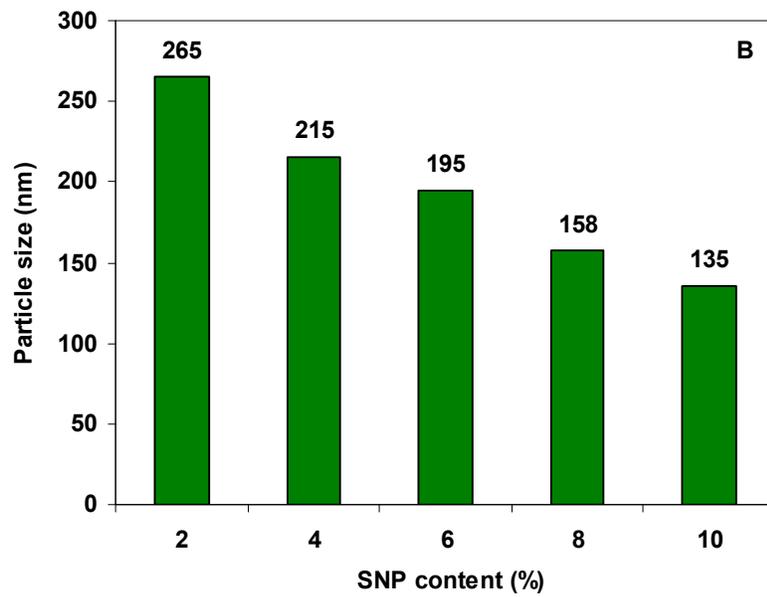
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255 Where R , γ_{wp} , θ represent the particle radius, oil-water interfacial tension and three-phase
256 contact angle respectively: ($R = 37 \text{ nm}$, $\theta = 43^\circ$ for waxy maize, $\gamma_{wp} = 35 \text{ mN.m}^{-1}$)

257 This gives an energy for the SNP of $740 (k_B T)$, which is much greater than the thermal motion
258 energy of a colloidal particle $k_B T$ ($8.5 \times 10^{-21} \text{ J}$ at 363°C : the temperature of the polymerization
259 reaction). This means that once the SNPs are attached to the polymer-water interface,
260 desorption is very difficult because the energy of desorption per particle is of the order of
261 several hundred $k_B T$.



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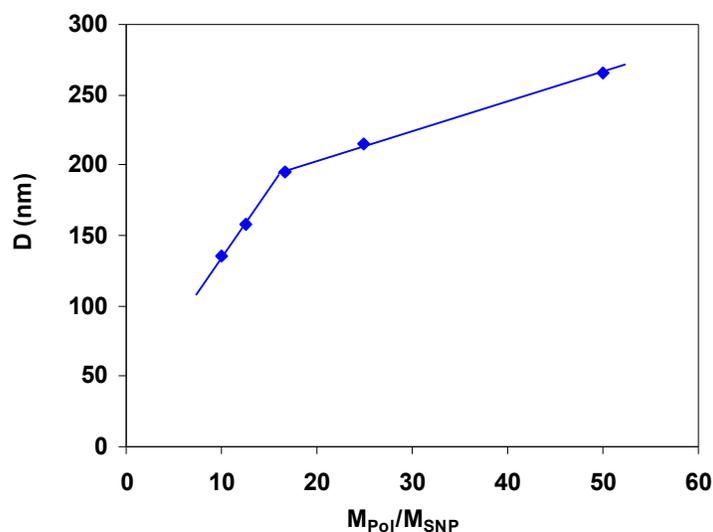


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264

265 **Figure 4: Change in (a) particle size distribution and (b) mean particle size of the**
266 **polymer latex as a function of SNP content.**

267



268

269 **Figure 5: Diameter of the polymer particle (D) vs. the polymer to SNP weight ratio**
 270 **(M_{pol}/M_{SNP}) content during the Pickering emulsion polymerization.**

271

272 In order to further highlight the key role of SNPs in the stabilization process, we performed a
 273 series of Pickering emulsion polymerization experiments in which we varied the SNP content
 274 from 2 up to 10%. As shown in Figure 4, by increasing the SNP content, a steady decrease in
 275 the polymer particle size can be seen over the whole SNP loading range. The strong
 276 dependence of the particle size on SNP content further emphasizes the key role of SNPs in the
 277 stabilization process. Actually, in the Pickering stabilization process, the amount of stabilizing
 278 solid particles controls the size of the droplets because the extent of the stabilized interfacial
 279 area is proportional to the stabilizer content. If it is assumed that all available SNPs become
 280 adsorbed at the polymer particle-water interface, then the interfacial area would increase
 281 linearly with respect to the SNP content and the diameter of the polymer particle would be
 282 proportional to the polymer to SNP weight ratio (M_{pol}/M_{SNP}) according to Eq. (2):

$$283 \quad D = \frac{6}{\rho_{Poly} \cdot S_{snp}} \cdot \frac{M_{poly}}{M_{snp}} \quad (2)$$

284

285 where D is the average polymer diameter, M_{snp} and M_{pol} is the total mass of solid particles and
286 polymer particles in the system, ρ_{pol} is the polymer density and S_{snp} is the specific surface area
287 per unit mass of SNP at full coverage, i.e., the polymer particle surface covered per unit gram
288 of SNP.

289 As shown in figure 5, the linear behavior predicted by Eq. (2) was not observed over the full
290 polymer/SNP range, and two domains were noted. The first one extended from 2 to 6% SNP
291 and the second one from 6 to 10%. This behavior is put down to the involvement of two
292 modes of stabilization during the growth of the polymer particle, according to the SNP. In the
293 first domain, between 2 to 6%, electrostatic stabilization is expected to contribute to the
294 stabilization process in addition to the Pickering mode. On the other hand, over 6% SNPs, the
295 stabilization process occurs essentially via the Pickering mode. This hypothesis is supported
296 by analyzing the change in the zeta-potential of the polymer particles vs. the SNP content
297 after the complete emulsion polymerisation. The results in Figure 6 show a negative zeta-
298 potential around -20 mV as the SNP content is lower than 6%; this grows abruptly to a value
299 of around -5 mV as the SNP content exceeds 8%. Taking account the fact that the SNPs were
300 not charged (zeta-potential around -3 mV), the negative zeta-potential in the first domain
301 where the SNP content is lower than 6%, is indicative of the fact that the polymer particles
302 bear negative charges. On the other hand, with an SNP content of over 8%, the ensuing
303 polymer latex particles are not charged, as their zeta-potential is close to 0. According to the
304 colloidal stability rules, particles with a zeta-potential of around -20 mV are considered to be
305 moderately charged and should aggregate within a short period, and with a zeta-potential
306 lower than ± 5 mV, they should immediately aggregate if no physical barrier stands against
307 this irreversible process. The exceptional colloidal stability of the polymer dispersion with an
308 SNP content of more than 4%, and more specifically above 8%, where the zeta-potential is
309 close to zero, is a good indication that the stabilization process during the emulsion

310 polymerization is driven by the Pickering process. It is worth noting that the polymer
311 dispersion prepared with 8 and 10% SNPs (results not shown) did not experience any change
312 in particle size with the addition of KCl electrolyte up to a concentration of 0.1 M, which
313 further emphasizes the high colloidal stability of the polymer dispersion even at high ionic
314 strength.

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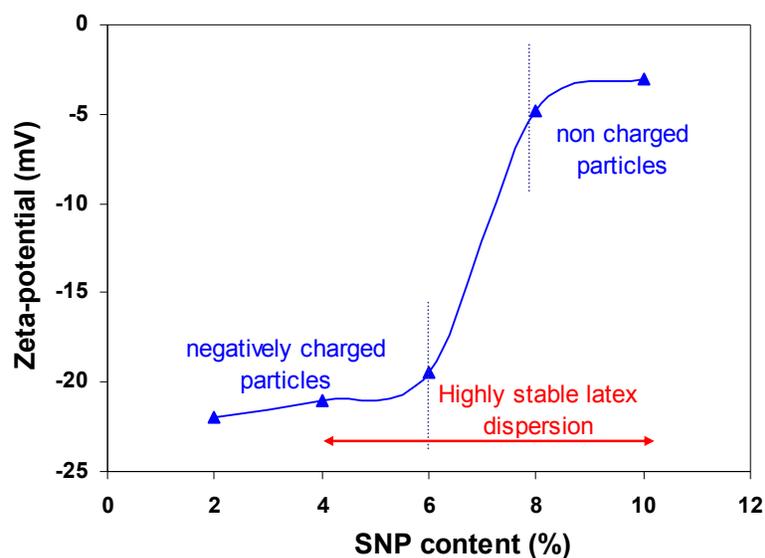
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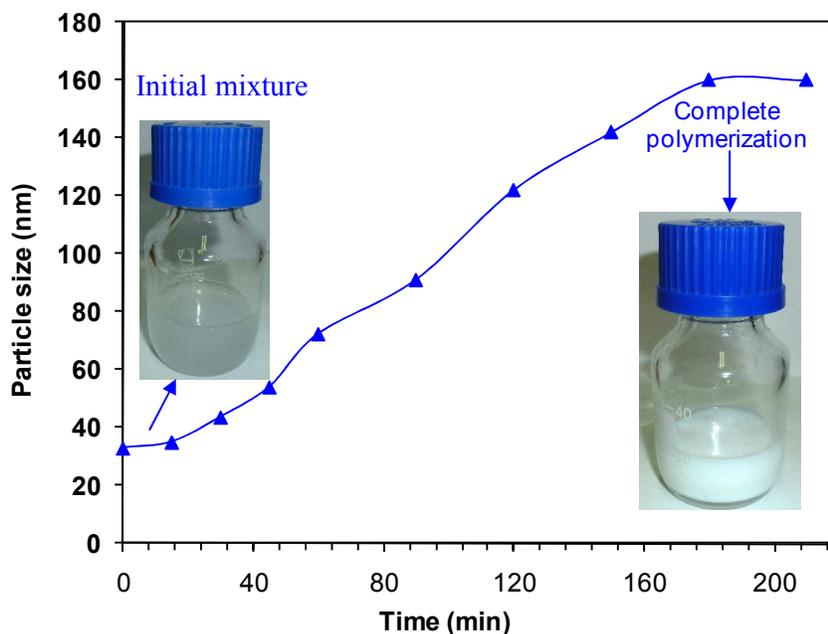


325 **Figure 6: Change in zeta-potential of the polymer dispersion according to SNP content**
326 **after emulsion polymerization**

327 The presence of negative charges in the domain where SNP is lower than 6% is most probably
328 due to the initiator residue (SO_4^-) accumulating on the uncovered part of the polymer
329 particles. The presence of these negative charges is likely to contribute to the stabilization
330 process as the SNP content is lower than 8%. On the other hand, above this level, the polymer
331 particles are fully covered by SNPs and their surface properties will be controlled by those of
332 the anchored solid nanoparticles.

333

334 The change in apparent particle size during the emulsion polymerization was monitored by
335 DLS, as shown in Figure 7. As polymerization proceeded, the particle size increased
336 continuously until the monomer droplet and the dissolved monomer were depleted.
337 Furthermore, it can also be seen that the polymerization reaction is completed within 3 h,
338 which is an acceptable kinetic with regard to the emulsion polymerization.



339

340 **Figure 7: Change in particle size vs. time during the course of Pickering emulsion**
341 **polymerization in the presence of 8% SNPs**

342

343 Based on the above data, the following mechanism by which the Pickering emulsion
344 polymerization of BMA takes place in the presence of SNP might be proposed upon the
345 addition of the water-soluble KPS and the temperature raising to 70°C, the decomposition of
346 the initiator produced generated free radicals free radicals in the aqueous phase, that initiated
347 the polymerization of monomer dissolved in water, forming oligomer with a terminal sulfate
348 group. When the growing macroradical reaches a critical length, it is no longer soluble in the
349 aqueous phase and precipitates to form a nucleated polymer particle. The nucleated polymer

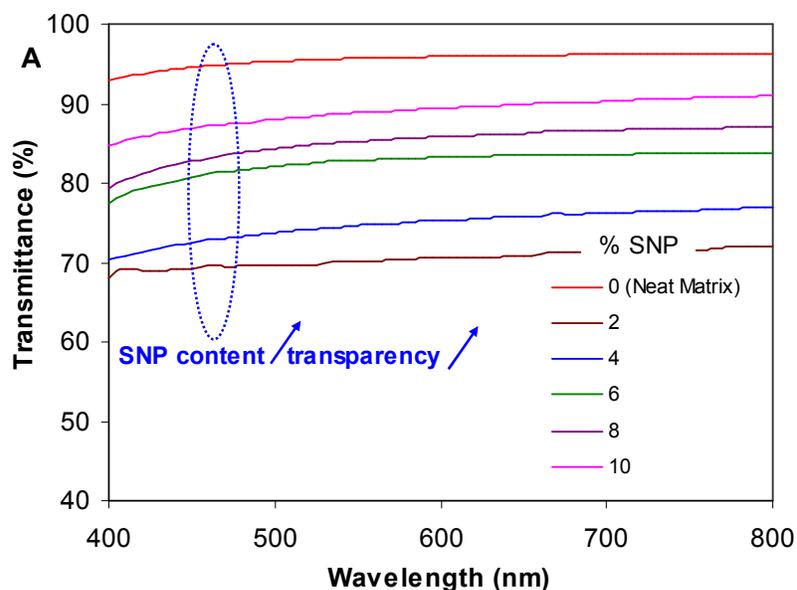
350 particles are then adsorbed on the SNP and continue to grow by monomer diffusion from the
351 monomer droplet and the entry of radical into the polymer particle.. The primary particles are
352 then stabilized by SNP adsorbed onto the monomer droplet or free SNP from the aqueous
353 phase and will grow through the monomer diffusion from the droplets, which act as reservoirs
354 to supply the necessary monomer to the growing polymer particles. As the particles grow,
355 their interfacial area increases and additional solid particles are needed to ensure stabilization
356 and prevent particle aggregation. These are supplied by the direct adsorption of SNPs on the
357 grown polymer particle or result from the aggregation of the nucleated polymer particles until
358 optimum surface coverage is achieved. The polymer particles continue to grow until all the
359 monomer droplets are consumed. During this final stage, the number of particles also remains
360 constant and the polymerization rate decreases until the monomer is completely converted.
361 Two reasons might explain the preferential attachment of SNP onto the growing polymer
362 particles; first, the higher number of polymer particles compared to that of monomer droplet
363 which is the result of the difference in the size between the monomer and the nucleated
364 polymer particles (1-10 μ m for the former against 50-200 nm for the later), and second, the
365 higher interfacial energy of the polymer particles compared to that of the of the monomer
366 droplets.

367 *Optical properties*

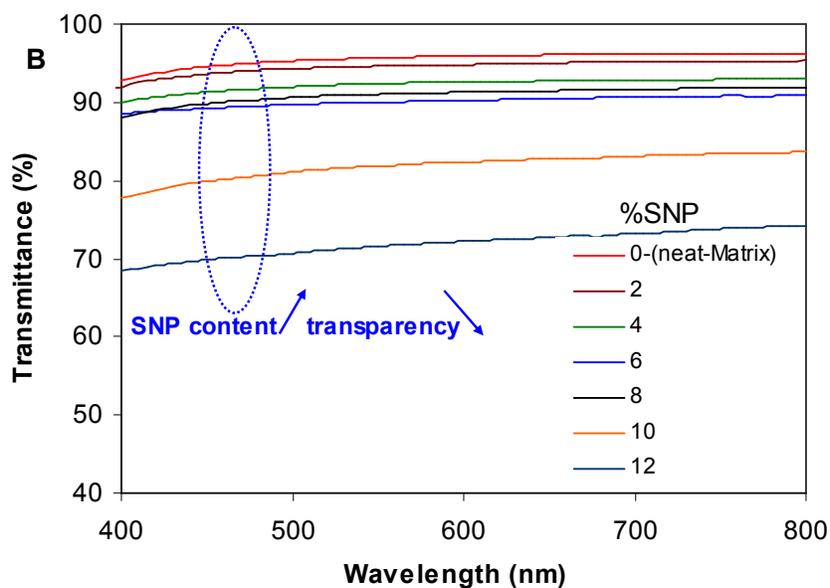
368 In nanocomposite-based material, it is extremely desirable to preserve the transparency of the
369 host matrix after the incorporation of NPs. However, even in the case of NPs measuring less
370 than 40 nm, this property is not readily achieved and a much greater drop in transparency is
371 often observed. The higher the NPs content, the greater this is.

372

373



374



375

376 **Figure 8: Transmittance spectra recorded in the visible wavelength range (thickness**
 377 **normalized to 200 nm) for nanocomposite film prepared via (A) the Pickering emulsion**
 378 **route and (B) mixing with already prepared latex dispersion**
 379

380

381 In fact, in the case of nanocomposite materials, transparency is reduced by light scattering
 382 against the randomly dispersed particles. This phenomenon is dependent on both the
 383 difference in refractive index between the nanoparticles and the polymer matrix, and also on

384 the particle size of the dispersed phase. In general, 50 nm is the upper limit for nanoparticle
385 diameter to avoid any loss in the intensity of transmitted light due to light scattering. At
386 present, due to the mismatch between the refractive index (RI) of starch (1.58)²⁰ and the host
387 matrix (1.48)²¹ and the low particle size of the SNPs, the critical factor controlling the
388 transparency of the nanocomposites is dispersion/agglomeration of nanoparticles within the
389 host polymer matrix.

390 The optical transparency of the SNP-PBMA nanocomposite films was assessed using UV–vis
391 in the visible wavelength range of 400–800 nm (Figure 8). For the sake of comparison, the
392 nanocomposite films were prepared either via the *in situ* method using the dispersion prepared
393 through Pickering emulsion polymerisation, or through an *ex-situ* approach by mixing SNP
394 suspension with already prepared PBMA dispersion. To avoid the effect of a variation in film
395 thickness, the film transmittance was normalized to a 200 µm-thickness using the Beer–
396 Lambert law. The neat PBMA matrix was an optically transparent sheet with light
397 transmittance above 90% in the visible light wavelength range (400–800 nm). The change in
398 film transmittance with nanofiller content differs according to the preparation route. Using the
399 *in-situ* Pickering approach, the change in transmittance according to SNP content displays a
400 particular type of behavior; at 2 and 4% SNP, a meaningful drop in transmittance from about
401 95% for the neat matrix to about 70% for the nanocomposite. However, as the SNP content
402 increases, an upward shift in transmittance is observed; this is indicative of an improvement
403 in the transparency as the nanofiller loading increases. At 10% SNP content, the film
404 transmittance is close to that of the neat matrix. This indicates that, above 8% SNP, the
405 presence of the nanoparticles did not affect the high transparency of the PBMA film. In
406 contrast, when the nanocomposite films are prepared via the *ex-situ* mixing process, the
407 transmittance is maintained up to a content of 6% SNP and appreciably decreases over 8%
408 SNP, which is probably the result of aggregation or clustering of the SNPs, as their content

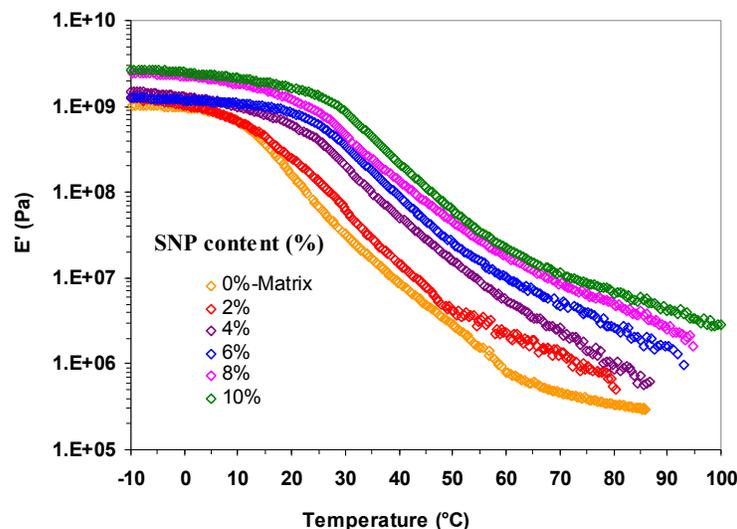
409 exceeds a critical threshold. This did not seem to be the case when the film was prepared via
410 the *in-situ* Pickering approach, and good dispersion of the SNPs was ensured by this method.
411 It is likely that the efficient and irreversible binding of SNPs were on to the polymer particles
412 during Pickering emulsion polymerization immobilized the NPs and accordingly prevented
413 their likelihood aggregation during the film-formation process.

414 However, as the SNPs content is lower than 8%, the film transmittance of the film from ex-
415 situ approach is higher than that of the in-situ route. The relatively high particle size of the
416 polymer dispersion as SNPs were lower than 8% might hinder the film-formation process and
417 reduce the polymer particles coalescence. This led to surface roughness that contributed to
418 reduce the transmittance via light diffusion.

419 **Reinforcing effect**

420

421 Polysaccharide based nanofiller arouse much interst because of their huge reinforcing
422 potential when incorporated into a ductile polymer matrix. However, the reinforcing potential
423 of the nanofiller is strongly affected by the dispersion degree of nanoparticles and their
424 homogeneity within the polymer matrix. Accordingly, the processing route of the
425 nanocomposite is a key step that determines the reinforcing effectiveness of the nanofiller.
426 This is particularly the case for polysaccharide based nanoparticles, where their inherent
427 polarity and hydrogen-bonding tendency complicates homogeneous dispersion in a
428 hydrophobic polymer matrix. This explains why the most common route for the processing of
429 polysaccharide nanoparticle composites relies on the mixing of an aqueous suspension of
430 polysaccharide NPs with a waterborne polymer, followed by solvent casting and water
431 evaporation. Evidently this approach is time-consuming and limits their commercial potential,
432 despite their well-recognized exceptional reinforcing potential.



433

434 **Figure 9:** Storage tensile modulus, E' , versus temperature at 1 Hz for nanocomposites film
 435 obtained from Pickering emulsion polymerization.

436

437

438

439 The reinforcing effectiveness of SNPs was investigated by DMA carried out on

440 nanocomposite films prepared by solvent casting of the nanocomposite dispersion prepared

441 via Pickering emulsion polymerization. The temperature dependence of the storage tensile

442 modulus, E' as a function of temperature at 1Hz for nanocomposite films with different SNP

443 contents is shown in Figure 9. Two behaviors are observed; below the glass transition

444 temperature, no significant variation in the storage modulus is detected upon the incorporation

445 of SNPs. On the other hand, above the glass transition the storage modulus is more sensitive

446 to the presence of the nanofiller and increased significantly with SNP addition, in line with

447 the well-known reinforcing effect of nanobased polysaccharide nanoparticles.²² This means

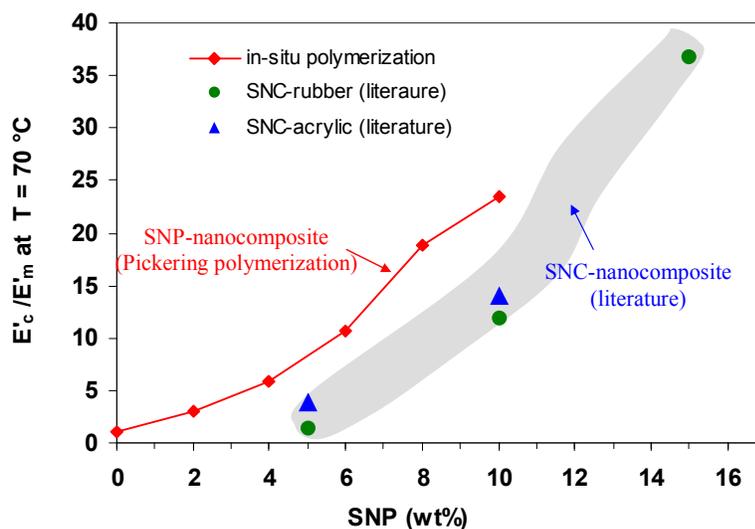
448 that SNPs are most effective in restricting the mobility of the polymers chains above T_g .

449 To further highlight the stiffening effect imparted by the addition of SNPs the evolution of the

450 relative modulus $E_r = \frac{E_c}{E_{mat}}$ (with E_c and E_{mat} the storage modulus of the nanocomposite and

451 unfilled matrix respectively measured in the rubbery region taken here at 70°C) versus the

452 SNP content was drawn for the nanocomposite films prepared via Pickering emulsion
 453 polymerization (Figure 10). For sake of comparison, data collected from literature for
 454 nanocomposite prepared from starch nanocrystals (SNC) and latex polymer via a mixing route
 455 was also shown. Even though, SNPs were not prepared via the same approach than that used
 456 for SNC, the enhancement in the stiffness brought by the presence of SNPs was higher than
 457 that imparted by SNC at the same loading. For instance, at 10 wt% SNPs, the modulus is 23
 458 times higher than the modules of the neat matrix when Pickering emulsion polymerization
 459 was adopted, while the increment is about 11-14 fold that of the neat matrix modules when
 460 *the two-pots* mixing mode was used to prepare the nanocomposite film. This higher
 461 reinforcing potential is a likely the result of the good dispersion of the SNPs within the
 462 polymer matrix after film-formation process.



475 **Figure 10:** Relative storage modulus $E_r = \frac{E_c}{E_{mat}}$ versus SNP content at 70 °C for
 476 nanocomposite films prepared via Pickering emulsion polymerization. Data for starch
 477 nanocrystals (SNC) were extracted from literature^{6, 23}.
 478

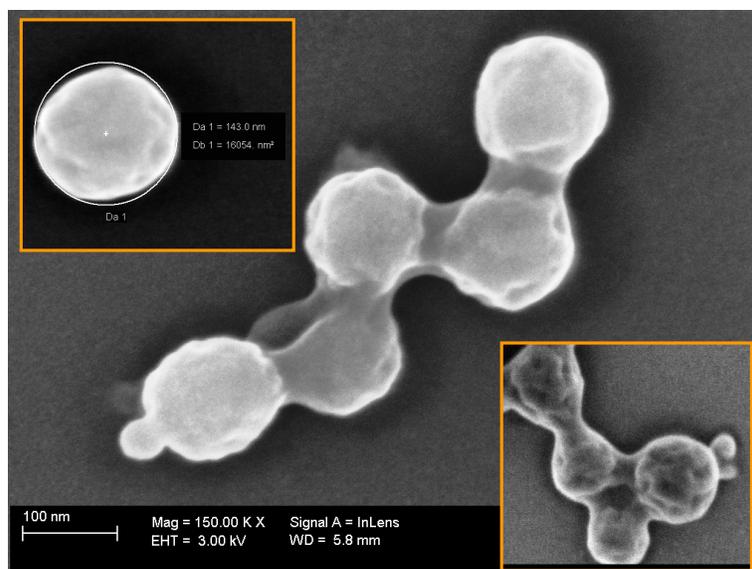
479

480

481 ***Morphology of the polymer particles***

482

483 As shown in Figure 11, nearly spherical particles with a uniform size and raspberry-like
484 morphology could be seen. The size of the polymer particles was around 145 nm, which is in
485 agreement with the DLS data. No free SNPs were visible on the analyzed surface, which
486 might be a confirmation that all the SNPs were attached onto the polymer particles. The
487 raspberry-like morphology, along with the imperfect spherical shape, indicate that the surface
488 of the polymer particles is rough and is surrounded by densely packed nanosized SNPs,
489 confirming the role of SNPs as a stabilizer. The apparent connection between the polymer
490 particles observed during FE-SEM is probably due to their interwinding a result of the high-
491 voltage electron beam causing local heating.. This typical morphology may be attributed to
492 the mechanistic aspect of the emulsion polymerization in the presence of SNPs. As previously
493 proposed, once the nucleated particle is formed and its size increases, partial aggregation
494 among the nucleated particles stabilized by SNPs might take place to ensure enough surface
495 coverage by the SNP particles. This aggregation behavior may lead to the polymer particle
496 surface observed.



497

498 **Figure 11 : FE-SEM micrographs of freeze-dried poly(butyl methacrylate) dispersion**
499 **stabilized with 8 wt% SNP from waxy maize.**

500 **Conclusions**

501 To summarize, an easy and effective method for surfactant-free emulsion polymerization of
502 methacrylate monomer was reported, using SNPs as a Pickering stabilizer. The SNPs were
503 prepared from waxy maize using the purely physical method of high-intensity ultrasonication
504 without any chemical additives. The SNP suspensions, with a particle size of around 40 nm,
505 were used as prepared without any additional purification.

506 Pickering emulsion polymerization was easy to implement and involved mixing the monomer
507 with the SNP suspension containing the persulfate initiator, and keeping the mixture stirred
508 magnetically at 70°C for 3h. A polymer dispersion, free from any coagulum, stable for more
509 than six months, and with a particle size ranging from 250 to 150 nm, was obtained without
510 the need for additional surfactant or any non-aqueous co-solvent. It was shown that the SNP
511 content plays a key role in the stabilization process and determines the polymer particle size.

512 After the film-formation process at room temperature, the nanocomposites formed displayed
513 higher optical transparency than could be obtained by blending the polymer emulsion with an
514 SNP suspension, showing that the present approach led to a highly transparent nanocomposite
515 based on SNPs and a film-forming methacrylate monomer.

516 Overall, the present procedure demonstrates a green chemistry approach for the preparation of
517 nanocomposite dispersions based on SNPs, giving rise to high optical transparency after the
518 film-formation process. Moreover, this approach may be applicable to a wide variety of
519 vinylic and acrylic monomers, which expands its potential application to a wide range of uses
520 such as adhesives, coatings, nanocomposites and the like.

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