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1     **Mechanistic insight into active chlorine species mediated electrochemical**  
2                     **degradation of recalcitrant phenolic polymers**

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10 **ABSTRACT**

11 Degradation of recalcitrant phenolic syntan by electro-oxidation was investigated. The  
12 kinetics of mineralization of phenolic syntan was followed both in terms of TOC and COD  
13 measurements. The generation of oxidants such as  $\text{Cl}_2$ , HOCl and free radicals of oxychloride  
14 in the presence of NaCl electrolyte was also monitored and their role in the oxidation of  
15 organics was discussed. The generation of  $^*\text{ClO}$  free radical was ascertained by electron spin  
16 resonance (ESR) spectroscopy coupled with spin trapping technique. The effect of pH,  
17 electrolyte concentration and current density on the degradation of phenolic syntan was  
18 discussed. Also, the current efficiency (CE) and energy consumption (EC) was estimated. It  
19 was observed that the oxidation of phenolic syntan was proportional to the current density  
20 and electrolyte concentration. The kinetics of the degradation of phenolic syntan was found to  
21 follow first order rate equation with an  $R^2$  value of 0.9966. The intermediate compounds  
22 formed during electrooxidation were characterised using AOX, FT-IR and NMR techniques  
23 and the degradation pathway was proposed. These results clearly suggest the effectiveness of  
24 electrochemical technique for the treatment of wastewater containing high concentration of  
25 phenolic syntan.

26

27 **Keywords:** Phenolic syntan; electro-oxidation; degradation; ESR study; free radicals; nuclear  
28 magnetic resonance; degradation kinetics.

## 29 Introduction

30 The impact of leather processing on environment is considered to be very significant (Ludvik,  
31 2000). About 30-35 m<sup>3</sup> of water and 700 kg of chemicals are used for converting 1 tonne of  
32 hide/skin into leather.<sup>1</sup> Though the pre-tanning operations contribute 70% of pollution load,  
33 the pollutants generated are simple and easy to treat. Conversely, the complex chemicals used  
34 in post-tanning process also called as wet-finishing process renders the wastewater highly  
35 complex and difficult to treat. Wide range of chemical products such as synthetic tannins  
36 (syntans), fat-liquors and dyes are used during wet-finishing processes.<sup>2</sup> The syntans are  
37 complex synthetic phenolic polymers synthesized using phenol as basic molecule. The  
38 unutilized / unadsorbed phenolic syntans in wastewater poses serious challenge to  
39 environment because of their poor biodegradability. The concentration of phenolic resin in  
40 tannery wastewater varies from 200 to 1500 mg/L and depends on the degree of uptake.

41 The phenol and phenolic products are environmentally hazardous and toxic to aquatic  
42 organisms and mankind.<sup>3</sup> Many techniques such as coagulation and flocculation, biological  
43 treatment, adsorption, ultrafiltration, ozonation and sonochemical degradation had been  
44 attempted for the treatment of phenolic wastewater.<sup>4-8</sup> The biodegradation of phenolic  
45 compounds is difficult because phenols are toxic to common microorganism. Though the  
46 advanced oxidation techniques such as photochemical degradation, ozonation and sonication  
47 are effective, the operating costs are high.<sup>9,10</sup> The electrochemical treatment is effective for  
48 the treatment of wastewater containing organic compounds. It has been extensively studied  
49 for the treatment of various pollutants generated from tanneries, textile industries, olive oil  
50 mills and other organic chemicals such as nonyl phenol ethoxylates, benzoquinone and  
51 chlorophenols.<sup>11-18</sup> Recently several attempts have been made to treat the phenol by  
52 electrochemical methods.<sup>19-23</sup> The electrochemical degradation of phenol using Ti/ RuO<sub>2</sub>-Pt  
53 was studied and reported that the phenol could be completely degraded by electrooxidation.

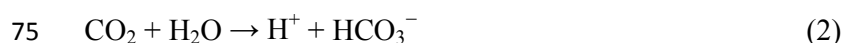
54 In the present study, degradation of synthetic phenolic resin (syntan) by electro-  
55 oxidation technique using IrO<sub>2</sub>/RuO<sub>2</sub>/TiO<sub>2</sub> coated titanium as electrodes was reported. The  
56 generation of active chlorine especially the free radicals during electro-oxidation was  
57 examined by ESR technique and FT-IR & NMR techniques are used to identify the  
58 intermediate compounds. The oxidation kinetics of phenolic syntan and its degradation path  
59 was attempted.

60

## 61 **Results and discussion**

### 62 **Effect of pH, electrolyte concentration and current density of Electro-oxidation**

63 The effect of initial pH on the degradation of phenolic polymer was studied by varying the  
64 pH between 2.0 to 10.0. Electro-oxidation of phenolic syntan prepared in 2% NaCl solution  
65 was carried out at a constant current density of 0.015 A/cm<sup>2</sup>. The results in terms of TOC  
66 with respect to time at different pH values are shown in Fig. 2. From the results, it is  
67 apparent that the degradation of syntan within 120 minutes of electro-oxidation was found to  
68 be hardly 45% and the effect of pH on the degradation is very marginal. Though the cell  
69 voltage remained almost constant during electrolysis, the final pH of the solution was found  
70 to shift to 7.8-8.5 irrespective of its initial value. This may be attributed to the production of  
71 CO<sub>2</sub> during electro-oxidation of syntan which intern dissolve in water and generates H<sup>+</sup> and  
72 HCO<sub>3</sub><sup>-</sup>. The H<sup>+</sup> ions thus generated are cathodically reduced to hydrogen gas whereas HCO<sub>3</sub><sup>-</sup>  
73 acts as buffering agent.



77 The insitu generation of chlorine and its role in electrooxidation was investigated at  
78 different NaCl concentrations by keeping the current density and pH at 0.015 A/cm<sup>2</sup> and 10.0

79 respectively. The initial pH was kept at 10.0 as the degradation is slightly better in alkaline  
80 medium. The results presented in Fig. 2 clearly illustrate the effect of NaCl on the  
81 degradation of organics. It was observed that the TOC decreases by increasing the  
82 concentration of NaCl. However, the decrease in TOC is very marginal beyond the salt  
83 concentration of 3%. The concentration of  $\text{Cl}^-$  in the reactor was measured and found to  
84 decrease 1450 ppm within half an hour. The  $\text{Cl}_2$  discharge from the anode in the presence of  
85 NaCl can be represented as



87 The chlorine gas thus generated is soluble in water to form HOCl according to the  
88 following reaction. It is also known that chlorine is soluble in water to the extent of 6g/L.

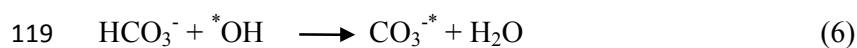


90 The change in pattern of UV-Visible spectrum of syntan solution during  
91 electrooxidation was monitored over a wavelength range of 200-800 nm. The maximum  
92 absorbance noticed around 280 nm (Fig. 3) may be attributed to  $n-\pi^*$  transitions of syntan  
93 molecule.<sup>24</sup> After 30 minutes of electro-oxidation, the peak at 280 nm was found to disappear  
94 and the colour of the wastewater turned to dark brown. The dark brown colour also ultimately  
95 disappears over a period of time. The change in colour could be attributed to various of  
96 intermediate products. The peak at 290 nm could be attributed to the presence of  $\text{OCl}^-$ . This  
97 spectrum is consistent with that of hypochlorite solution in basic medium (Fig.3, inset). Thus  
98 the generation of hypochlorite can be confirmed during electrooxidation. The shoulder  
99 around 350 nm may be due to the presence of  $\text{ClO}_2$  formed as a result of reaction between  $\text{Cl}_2$   
100 and  $\text{O}_3$  generated due to secondary electrochemical reactions. The broad peak between 275-  
101 350 nm may be interpreted due to merger of spectra of syntan molecule,  $\text{OCl}^-$  and  $\text{ClO}_2$ .

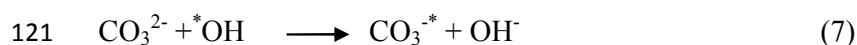
102 The generation of  $^*\text{OCl}$  and  $^*\text{OH}$  during electrooxidation of syntan was also  
103 continuously monitored using electron spin resonance spectroscopy (ESR) coupled with spin

104 trapping technique.<sup>25</sup> Electron spin resonance spectroscopy (ESR) is used to identify free  
105 radicals. A free radical is a paramagnetic species containing an unpaired electron which  
106 exerts a magnetic moment that is detected by ESR. The free radicals are highly reactive with  
107 a life time of less than 20 s and hence their direct detection by ESR would be difficult to  
108 achieve. In order to overcome this difficulty, spin trap agents were used. The spin trapping  
109 agent reacts with a specific free radical to produce a more stable radical or spin adduct which  
110 is detected by ESR. In the presence of  $^*\text{OH}$  radicals in the reaction mixture, the DMPO-OH  
111 adduct should yield a spectrum with characteristic intensity of 1:2:2:1. The ESR spectrum of  
112 DMPO-OCl adduct exhibit seven characteristic peaks (Fig. 4(a) and 4(b)).<sup>25</sup> In the present  
113 case, the ESR data confirm the generation of  $^*\text{OCl}$  during electrooxidation of syntan. Though,  
114 the generation of  $^*\text{OH}$  radicals during electrolysis was well established by previous  
115 researchers,<sup>26,27</sup> the absence of  $^*\text{OH}$  radicals in this case may be explained due to co-  
116 generation of carbonate and bicarbonate ions which act as scavenging agents for hydroxyl  
117 radicals as shown in the following reactions.

118 In acidic pH



120 Under alkaline pH



122 Though the exact mechanism of the formation of carbonate radical is not fully  
123 established, it is known that the carbonate radical thus generated is further decayed to carbon  
124 dioxide

125 Therefore it is clear that the oxidation of phenolic syntan in the presence of NaCl is  
126 mediated predominantly by hypochloride ion and its free radical  $^*\text{OCl}$ .

127 The low degradation of organics (70% of TOC) in the presence of  $\text{RuO}_2/\text{IrO}_2/\text{TiO}_2$   
128 coated titanium may be explained by the competition between the oxidation of organics and

129 the oxygen evolution reaction at the anode surface. The oxide coated electrodes have low  
130 over-potential for oxygen evaluation and hence the secondary reaction is favoured in  
131 comparison with oxidation of organic matter.<sup>28</sup> The oxidation of organics on noble oxide  
132 anode was attributed to the formation of “higher oxides” via adsorption of the hydroxyl / oxy  
133 chloride radical and its interaction with the oxygen already present in the oxide with a  
134 possible transition to higher oxide as mentioned below.



137

138 Since the solubility of chlorine in water is very high (6g/L) compared to oxygen (8  
139 ppm), high concentration of oxidant with high oxidation reduction potential (ORP) would  
140 built up in the aqueous solution. Consequently even the refractory organics can be easily  
141 oxidized and degraded during electrooxidation. From the present study it is evident that  
142 oxidation of organics in the presence of chloride ion proceeds via adsorption of  $\cdot\text{OCl}$  on  
143 metal oxide and the transition of oxygen atom to metal oxide, forming higher metal oxide as  
144 suggested in the above equation.

145 The cell voltage was found to decrease when the salt concentration was increased.  
146 This is due to increase in conductivity of the solution. The energy consumption (Fig. 5) was  
147 decreased from 8.06 kWh/kg of COD to 2.01kWh/kg of COD, when chloride concentration  
148 was increased from 1% w/v to 4% w/v. The inverse proportionality relationship between salt  
149 concentration and energy consumption may be attributed to increase in active chloro species  
150 and decrease in cell voltage when the salt concentration was increased. General current  
151 efficiency was found to increase with increase in NaCl concentration due to the formation of  
152 chlorine and hypochlorous acid/hypochlorite ion in very high concentrations.



153 The influence of current density on degradation was also studied by varying the  
 154 current density from 0.005 A/cm<sup>2</sup> to 0.0025 A/cm<sup>2</sup>. The NaCl concentration and the initial  
 155 pH was maintained at 3% at 10.0 respectively. From results it is evident that the degradation  
 156 rate was increased with increase in current density (Fig. 2). It could be attributed the  
 157 formation of more oxidizing agents. There was no significant change in COD beyond 0.020  
 158 A/cm<sup>2</sup>.

159

### 160 **Energy consumption (EC) and General Current Efficiency (GCE)**

161 Further the energy consumption (EC) and general current efficiency (GCE) were also  
 162 calculated using the following equations and the results are given as in Fig. 5.

163 Total Current Efficiency (TCE)

164

$$165 \quad TCE = \frac{[COD_t - COD_{t+\Delta t}]}{8I\Delta t} \quad (10)$$

166

167 Where COD<sub>t</sub> and COD<sub>t+Δt</sub> are chemical oxygen demands in gram of O<sub>2</sub> per dm<sup>3</sup> at times t and  
 168 t+Δt respectively; F is Faraday constant (96487 C mol<sup>-1</sup>); V is the volume of electrolyte in  
 169 litre and I is the current in Ampere and 8 is the equivalent mass of oxygen (g/eq<sup>-1</sup>).

170

171 Energy consumption for the removal of one Kg of COD was calculated. It is  
 172 expressed in kWh.kg<sup>-1</sup> of COD or TOC.

173

$$174 \quad \text{Energy consumption} = \frac{[tVA/S_v] / 1 \times 10^3}{\Delta COD / 1 \times 10^6} \text{ Kwh / kgCOD} \quad (11)$$

175

176 Where,  $t$  is the time of electrolysis in hours,  $V$  is the average cell voltage,  $A$  is Ampere,  $S_v$  is  
177 sample volume in litres and  $\Delta\text{COD}$  is the difference in COD in time  $t$  in mg/L.

178

179 The current efficiency was found to decrease when the current density was increased.  
180 This may be explained due to higher rate of oxygen evolution compared to oxidation of  
181 organics at the anode surface. In general, if the applied current is more than the limiting  
182 current, the oxidation will be invariably under mass transport control and the oxygen  
183 evolution dominates the oxidation.

184

#### 185 **Fourier Transform - Infrared Spectroscopy (FT-IR) study**

186 The FT-IR spectra of the syntan and the sample resulting from the electrooxidation (obtained  
187 by lyophilisation) was recorded and shown in Fig.6. The broad absorption band around 3350  
188  $\text{cm}^{-1}$  observed in the FT-IR spectrum of phenolic syntan could be assigned to -OH stretching  
189 vibrations. The peak with medium intensity at 1568  $\text{cm}^{-1}$  may be assigned to C=C stretching  
190 vibrations and the high intensity peak at 1116  $\text{cm}^{-1}$  could be attributed to -C=O stretching  
191 vibrations. The sharp peak with medium intensity around 1035  $\text{cm}^{-1}$  may be assigned to S=O  
192 stretching vibrations of  $\text{SO}_3\text{H}$  attached to phenol ring. The broad peak around 3435  $\text{cm}^{-1}$   
193 observed in the spectrum of oxidized syntan sample could be assigned to O-H stretching  
194 vibrations. The sharp peak with high intensity at 1635  $\text{cm}^{-1}$  is a characteristic  $\nu(\text{C}=\text{O})$   
195 vibration of quinone functional group. The peak with medium intensity at 1391  $\text{cm}^{-1}$  may be  
196 assigned to C-O-H bending. The low intensity peak at 996  $\text{cm}^{-1}$  could be assigned to COOH  
197 bending vibrations. Thus the FT-IR spectrum of the electrooxidation sample clearly indicates  
198 the presence of carboxylic acids. It is apparent that the polymer is ultimately mineralized to  
199  $\text{CO}_2$  and  $\text{H}_2\text{O}$  via low molecular weight carboxylic acids like formic acid and oxalic acid. The  
200 presence of these acids in oxidized sample was established by NMR spectroscopy.

## 201 **Nuclear Magnetic Resonance (NMR) study**

202 In order to have better clarity on the oxidation of syntan during electrooxidation, NMR  
203 spectrum was taken to identify the compounds formed during oxidation. Fig. 7(a) shows the  
204  $^{13}\text{C}$ -CP/TOSS spectrum of phenolic syntan run in solid state at room temperature. It shows  
205 characteristics peaks arising from the constituents of phenolic syntan. The peak with  
206 moderate intensity at 40 ppm is assigned to methylene bridge of phenolic syntan. Six peaks  
207 are seen with varying intensity in the range of 115-161 ppm. The chemical shift value and  
208 their assignment are shown in Table 1. The presence of two peaks at 160.4 and 156.55 ppm  
209 is attributed to carbons to which OH functionality is attached. The phenyl ring carbons show  
210 peaks in the range of 115-140 ppm. The individual assignment ring carbons are arrived by  
211 comparing the literature data are listed in Table 1. These features are consistent with the  
212 structure of phenolic syntan as shown in Fig.7(a).

213 Fig. 7(b) shows the  $^{13}\text{C}$ -CP/TOSSNMR of oxidized sample of phenolic syntan during  
214 electro-oxidation. Remarkably, the spectrum shows only one intense peak at 164.35 ppm  
215 with few shoulders. In contrast to phenolic resin where more than six peaks are seen the  
216 appearance of one peak for the electro-oxidized (120 min) phenolic syntan clearly suggests  
217 that the aromatic moieties are broken. The high intense peak seen at 164.35 ppm of electro-  
218 oxidized phenolic syntan is attributed to formic acid/oxalic acid residual moiety. This is  
219 based on the fact that the carbonyl region of the acid is 160-165 ppm. Further, the  
220 disappearance of peaks arising from phenyl ring and methylene bridge supports oxidation of  
221 the phenolic syntan leading to the formation of oxalic acid and formic acid.

222

## 223 **Adsorbable Organic Halogens (AOX)**

224 The samples collected at different time intervals of electrooxidation was analysed for the  
225 presence of chloro-organic compounds. The results of AOX analysis have revealed the

226 absence of chloro-organics at any point of time during electro-oxidation. The results  
227 demonstrate that the electrooxidation is a cleaner and promising process compared to other  
228 processes.

229

### 230 **Kinetics of degradation**

231 In indirect electrochemical treatment, degradation of organic compound is predominantly due  
232 to electrically generated chlorine/hypochlorite. Therefore, COD removal rate is directly  
233 proportional to the concentration of organic compound (phenolic syntan) and the  
234 chlorine/hypochlorite. The data of  $\ln C/C_0$  was fitted for zero order, first order and second  
235 order equations. The equations for the orders zero, first and second are  $y=-0.2098x+1.08$ ,  $y=-$   
236  $0.5025x+0.4633$  and  $y=1.5962x+1.1956$  with  $R^2$  values 0.878, 0.996 and 0.943 respectively.  
237 The best fit ( $R^2$ ) was obtained for first order reaction. The first order rate constant calculated  
238 from the slope of the plot is  $16.70 \times 10^{-3} \text{ min}$  (Fig. 8). Therefore it could be concluded that  
239 the process of electrolytic degradation is dependent solely on the concentration of phenolic  
240 resin.

241

### 242 **Degradation pathway**

243 The possible degradation pathway of electro-oxidation of phenolic syntan is shown in figure  
244 (Fig. 9). Initially, the polymer is degraded to hydroquinone and benzoquinone during  
245 electrooxidation. Breakdown of quinone compound as progresses is also evident from FT-IR  
246 and NMR spectra. The polymeric syntan is finally degraded to formic acid before converting  
247 to  $\text{CO}_2$ .

248

249

250 **Study on passivation of electrodes by Scanning Electron Microscope/Energy Dispersive**  
251 **Sperctroscopy (SEM/EDAX)**

252 The problem of passivation of electrodes and the formation of polymeric films on the  
253 electrodes during electro-oxidation of phenolics was reported.<sup>29</sup> Blocking polycrystalline  
254 platinum Pt and boron-doped diamond BDD electrodes by 20 phenolic compounds was  
255 studied by means of chronoamperometric and theoretical methods.<sup>30</sup> The polymerization  
256 process was studied as a function of the methyl substitution in the phenolic structure.  
257 Electrochemical quartz crystal microbalance studies show that the polymer formed from  
258 substituted phenols is more passivating than that from the non-substituted phenol. In any  
259 case, the largest amount of mass was deposited during the first voltammetric cycle and the Pt  
260 electrode was more active than the Au electrode for the organic electrooxidation process.<sup>30</sup>  
261 The process of passivation is governed by many factors such as electrode material, current  
262 density, type of phenolic compound and electrolyte concentration. Therefore studies to verify  
263 the possible passivation is equally essential while evaluation the oxidation process. The  
264 electrode surface was investigated using scanning electron microscope with EDAX facility.  
265 The micrographs shown in Fig.10, indicated that there was no coating or passivation on the  
266 electrode surface. Major elements detected by EDAX and the composition of the electrodes  
267 were presented in Table 2. It is evident that atomic weight % of the elements present in the  
268 electrodes is more or less same even after the electro-oxidation of phenolic syntan. Thus it is  
269 evident that there is no change in the electrode composition due to deposition of organic  
270 matter during electrolysis. It is also evident that there is no passivation of electrodes due to  
271 deposition of syntan polymer on the electrode surface.

272

273

274

## 275 **Conclusions**

276 The Degradation of recalcitrant phenolic syntan by electrooxidation was investigated using  
277 RuO<sub>2</sub>/IrO<sub>2</sub>/TiO<sub>2</sub> coated titanium electrodes. The generation of oxidants such as Cl<sub>2</sub>, HOCl  
278 and free radicals of oxychloride were found to play a major role in the oxidation of organics.  
279 The generation of <sup>\*</sup>ClO free radical was ascertained using electron spin resonance (ESR)  
280 spectroscopy coupled with spin trapping technique. The intermediate compounds formed  
281 during electrooxidation were characterised using AOX, FT-IR and NMR techniques and the  
282 possible degradation pathway was suggested. The polymeric syntan was initially converted to  
283 benzoquinone which inturn is oxidized to low molecular weight compounds such as oxalic  
284 and formic acids. It was observed that the oxidation of phenolic syntan was proportional to  
285 the current density and electrolyte concentration. The kinetics of the degradation of phenolic  
286 syntan was found to follow first order rate equation with an R<sup>2</sup> value of 0.9966. It was also  
287 observed that chloroorganic compounds were not formed during electro-oxidation of phenolic  
288 syntan. Further it was found that there was no passivation of electrodes.

289

## 290 **Experimental**

### 291 **Materials**

292 The phenolic syntan (phenolic polymer) viz., Basyntan DI was obtained from M/s BASF  
293 India Ltd., Chennai, India. The syntan was quantitatively analysed for C, H, N, and S and  
294 found to be 32.24%, 3.25%, 1.81% and 11.90% respectively. The characteristic UV-Visible  
295 absorbance ( $\lambda_{\text{max}}$ ) was noticed around 280 nm. The other chemicals used were of analytical  
296 grade and procured from M/s Sigma-Aldrich, India.

297

298

299

### 300 **Electro-oxidation setup**

301 The schematic diagram of experimental setup is shown in Fig.1. Reactor with a working  
302 volume of 2.0 litres was fitted with titanium electrodes coated with  $\text{TiO}_2/\text{RuO}_2/\text{IrO}_2$ . The  
303 working surface area of the electrode was estimated to be  $380 \text{ cm}^2$ . Both the anode and  
304 cathode were placed vertically and parallel to each other with a gap of 1.0 cm between anode  
305 and cathode to minimize the ohmic losses. A D.C regulated current ranging from 0 to 25A was  
306 used. A peristaltic pump was used for circulating the sytan solution under constant flow of  
307 300 mL/min.

308 The phenolic polymer (Basytan DI) solution with a concentration of 1000 mg/L was  
309 prepared using distilled water. Required quantity of NaCl was added and the pH was  
310 adjusted using dilute HCl and NaOH solutions.

311

### 312 **Analysis**

313 The degradation of sytan was followed by measuring the total organic carbon (TOC) / and  
314 chemical oxygen demand (COD). During the experiment, samples were drawn at different  
315 intervals and analysed. TOC was determined using ELEMENTER - Vario TOC Select  
316 analyzer. The COD was determined by the standard procedure reported by American public  
317 health association.<sup>31</sup> In order to eliminate the interference of chloride ion, mercuric sulphate  
318 was added in the COD estimation. Elements present in phenolic polymer were analyzed by  
319 Elemental analyzer (Model: Vario Micro Cube; Make: M/s Elementer, Japan). The pH of the  
320 solution was measured using pH meter (HACH model HQ40d). The UV-Vis  
321 spectrophotometer (JASCO-V600) and FT-IR (JASCO-4200) were used to follow the  
322 degradation of sytan during electrooxidation. All the results reported are the arithmetic  
323 mean of three samples.

324

**325 Characterization of free radicals**

326 Electron Spin Resonance (ESR) spectrometry coupled with spin trapping technique was  
327 employed to identify the free radicals generated during electro-oxidation. 5,5,-dimethyl-1-  
328 pyrroline-N-oxide (DMPO) was used as spin trapping agent. Prior to using, the DMPO was  
329 purified using activated charcoal to avert the free radicals. ESR spectra were recorded using  
330 BRUKER spectrometer operating at the X band and flat cell assembly. For each sample six  
331 scans were recorded at a modular frequency of 10 kHz. Data acquisition and instrument  
332 control were performed by Bruker software. All the experiments were carried out at room  
333 temperature and ambient air.

334

**335 NMR study**

336 NMR analysis was carried out in 400MHz Bruker WB Avance III NMR spectrometer <sup>13</sup>C  
337 frequency = 100 MHz) and 4 mm probe head were used. The NMR spectrum was recorded  
338 using Zpgg 30 pulse sequence. Processing and plotting was done using Top Spin NMR  
339 software.

340

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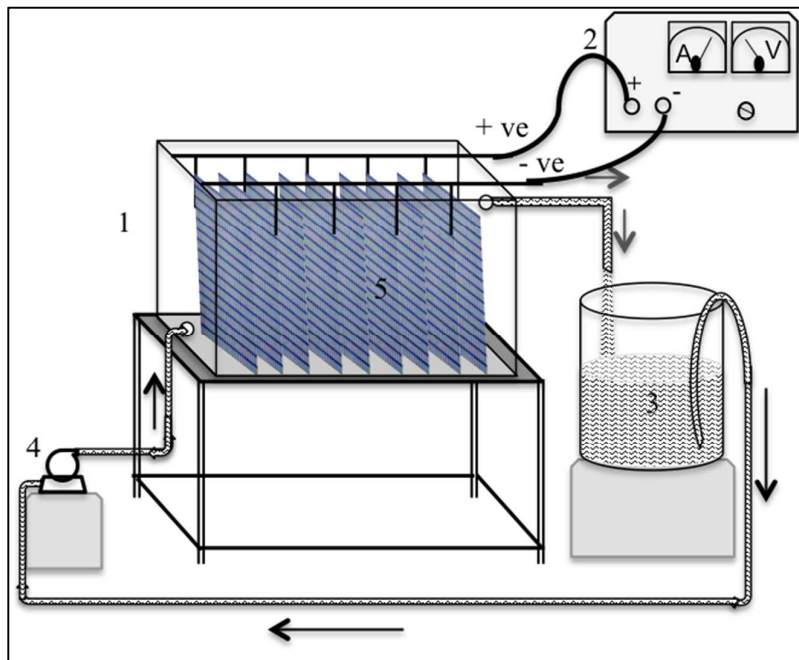


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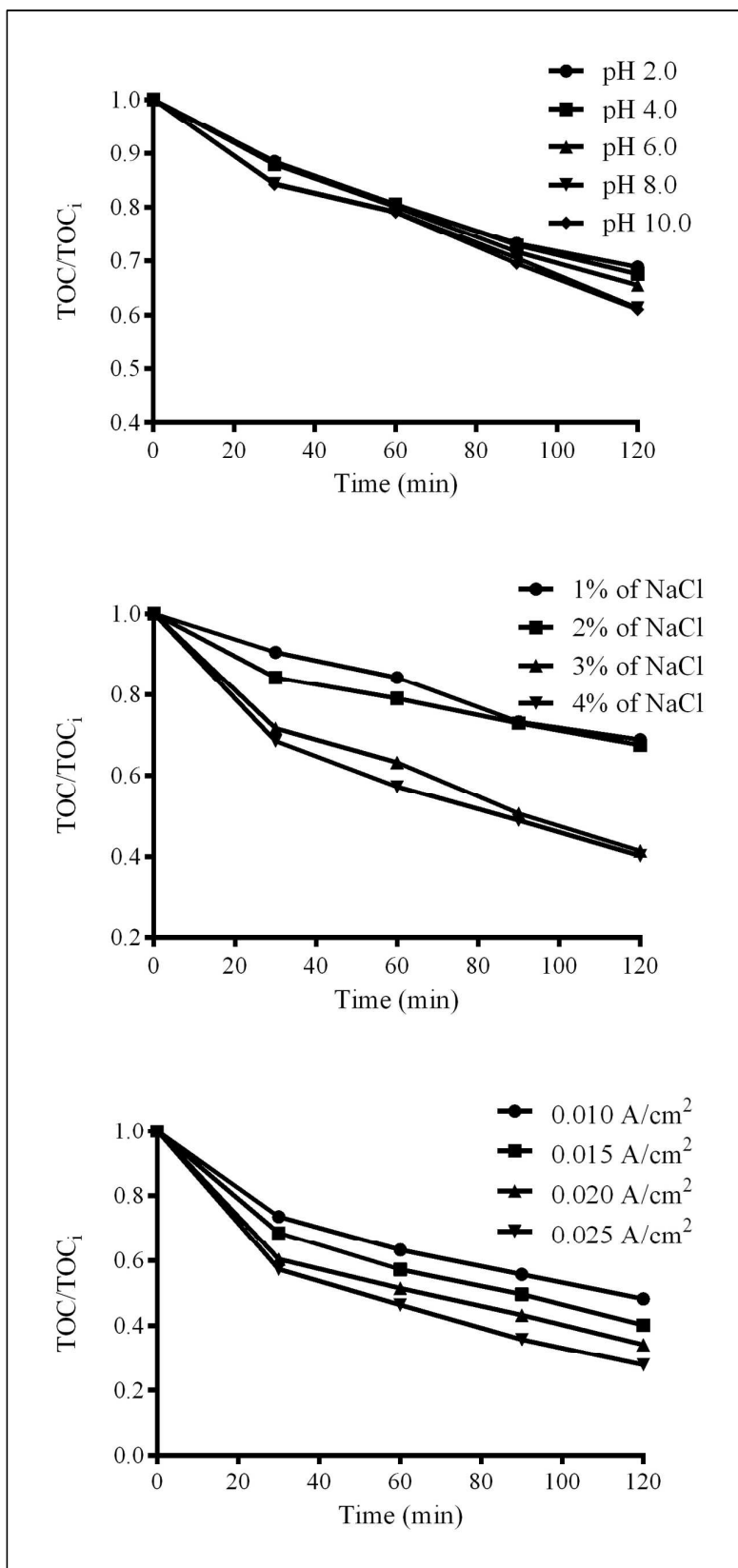
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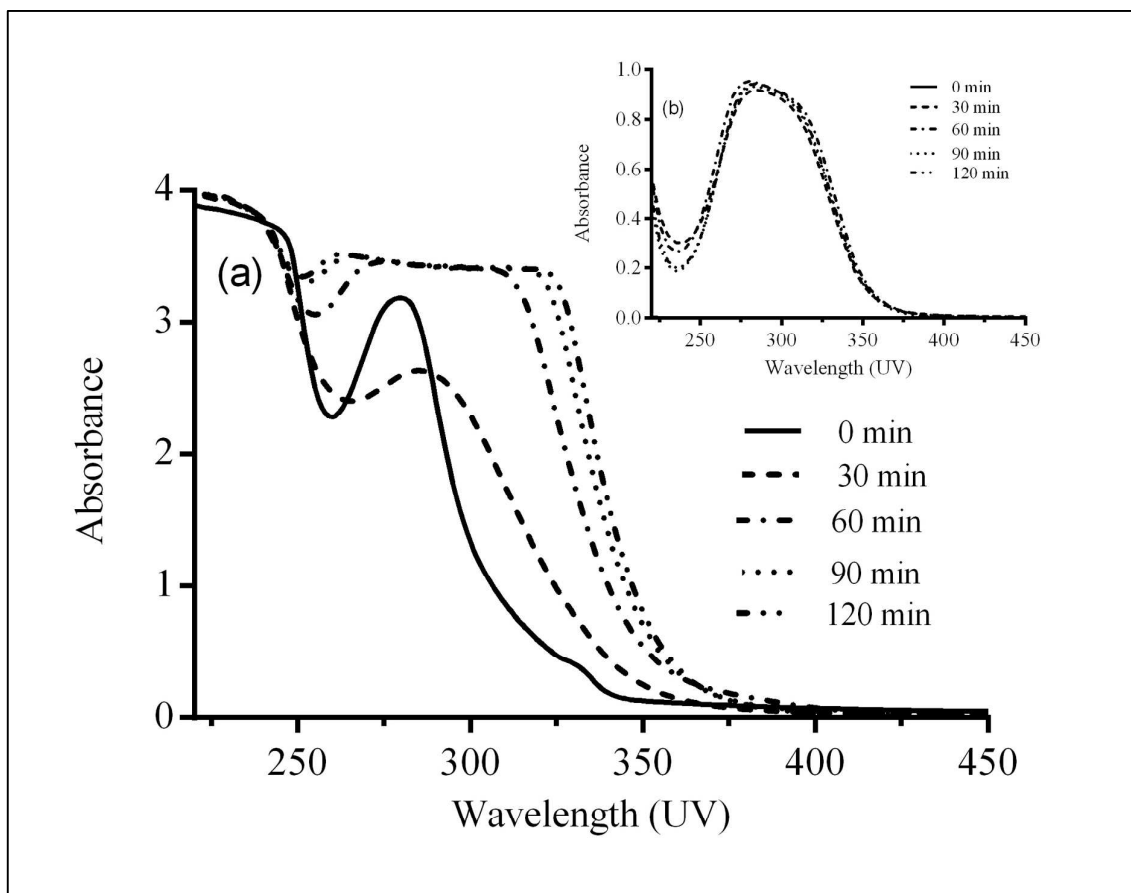
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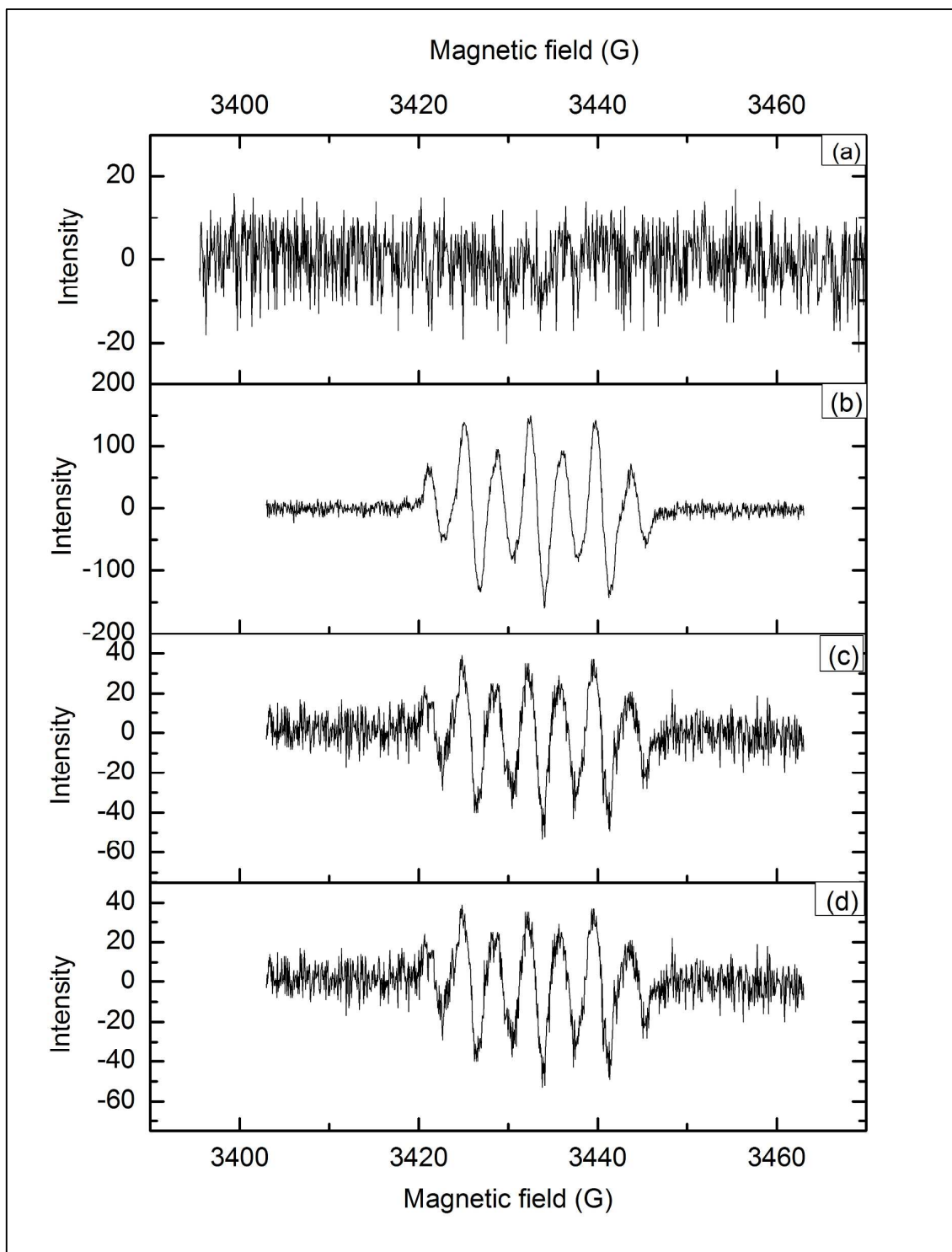
**Fig. 1** Schematic diagram of electro-oxidation setup: 1. Electro-oxidation Tank; 2. DC power source; 3. Phenolic sytan solution; 4. Peristaltic pump; 5. Anodes and cathodes



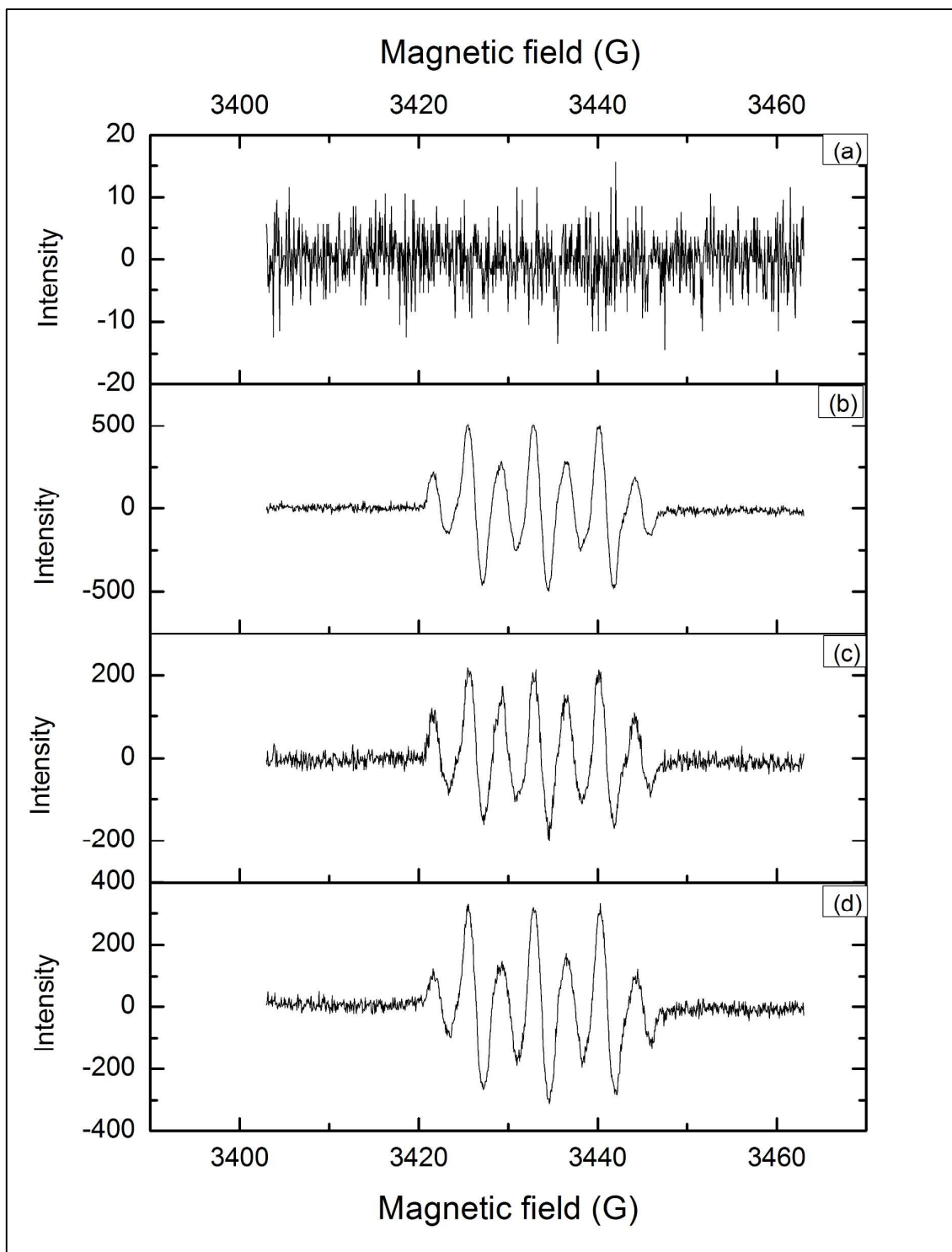
**Fig. 2** Effect of operational parameters (a) pH, (b) Electrolyte concentration (c) Current density on COD and TOC reduction rate with electrolysis time



**Fig. 3** UV-Vis spectrum for electro-oxidation of (a) phenolic resin and (b) in the absence of phenolic syntan at different time of electro-oxidation (Current density  $0.015 \text{ A/cm}^2$ , pH 9.0, concentration of electrolyte 3.0% and duration of electrolysis: 120 min).

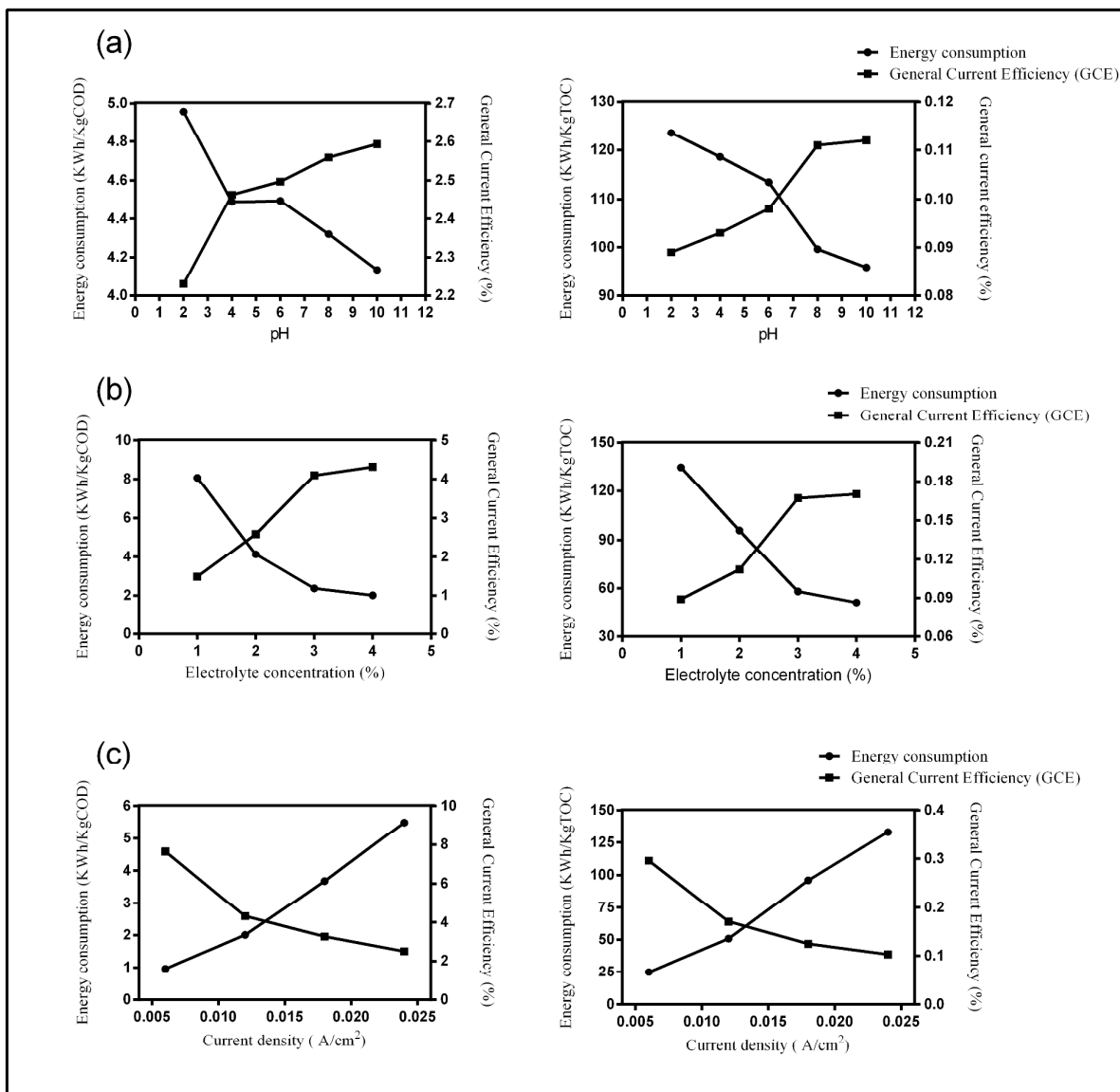


**Fig. 4(a)** ESR spectra of phenolic syntan samples collected at different time intervals of electro-oxidation (a) 0 min, (b) 10 min, (c) 20 min and (d) 30 min. (Current density  $0.015 \text{ A/cm}^2$ , pH 9.0 and concentration of electrolyte 3.0%).

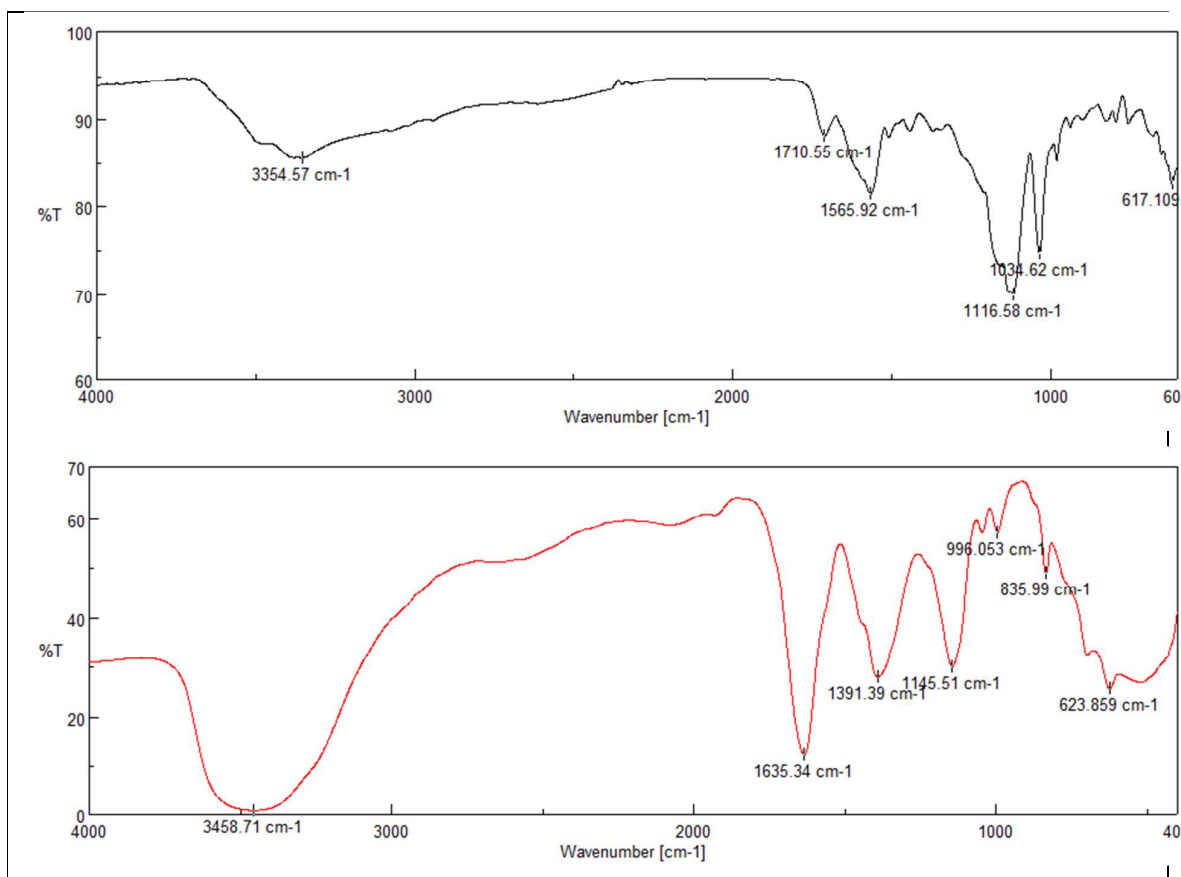


**Fig. 4(b)** ESR spectra of samples collected during electrolysis of NaCl in the absence of phenolic syntan at (a) 0 min, (b) 10 min, (c) 20 min and (d) 30 min. (Current density  $0.015 \text{ A/cm}^2$ , pH 9.0 and concentration of electrolyte 3.0%).





**Fig. 5** Comparison of energy consumption and General Current Efficiency at various conditions of electro-oxidation (a) pH; (b) Electrolyte Concentration; (c) Current density; (Electrolysis time: 120 min).



**Fig. 6** FT-IR spectrum of phenolic sytan, (a) before electro-oxidation and (b) at the 120 min of electro-oxidation (Current density 0.015 A/cm<sup>2</sup>, pH 9.0, concentration of electrolyte 3.0% and electrolysis time 120 min).

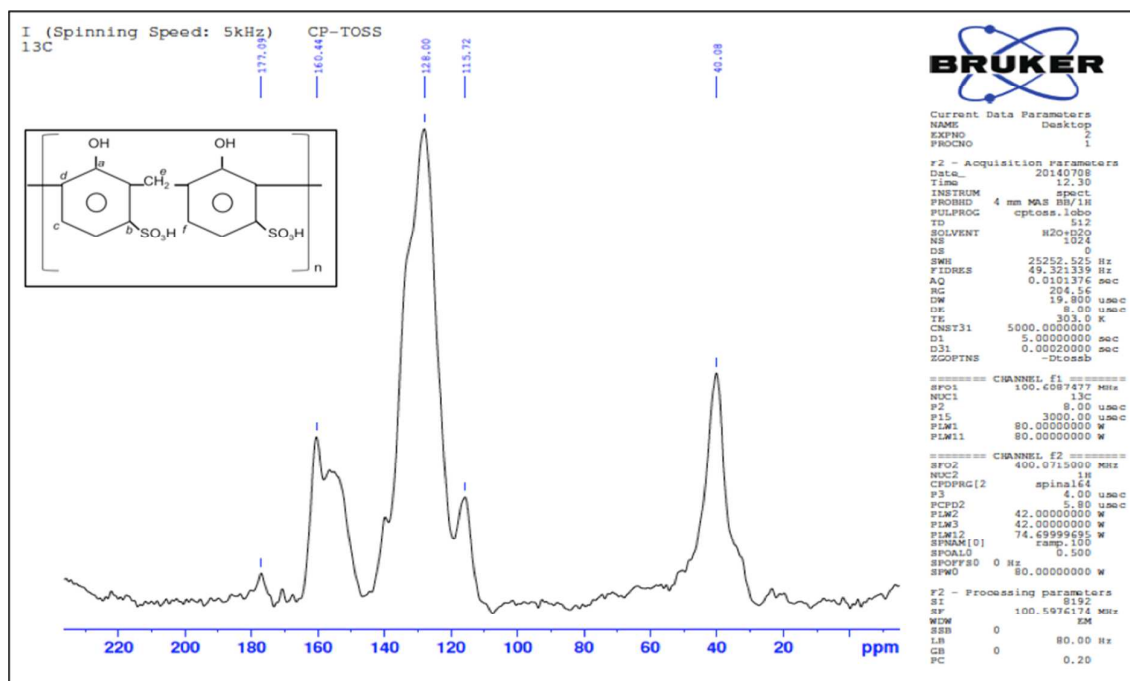
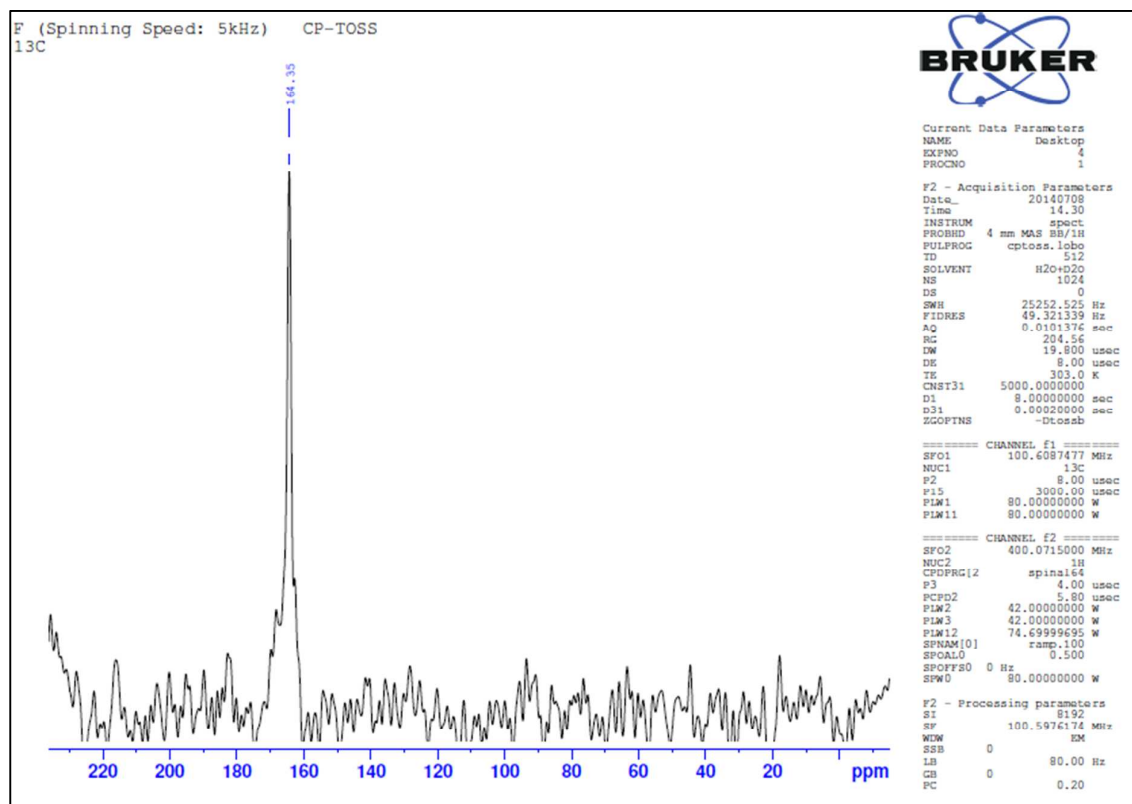
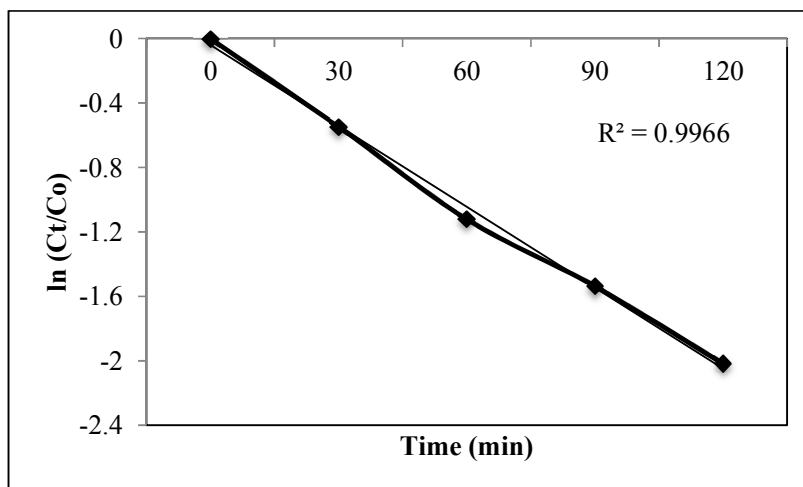


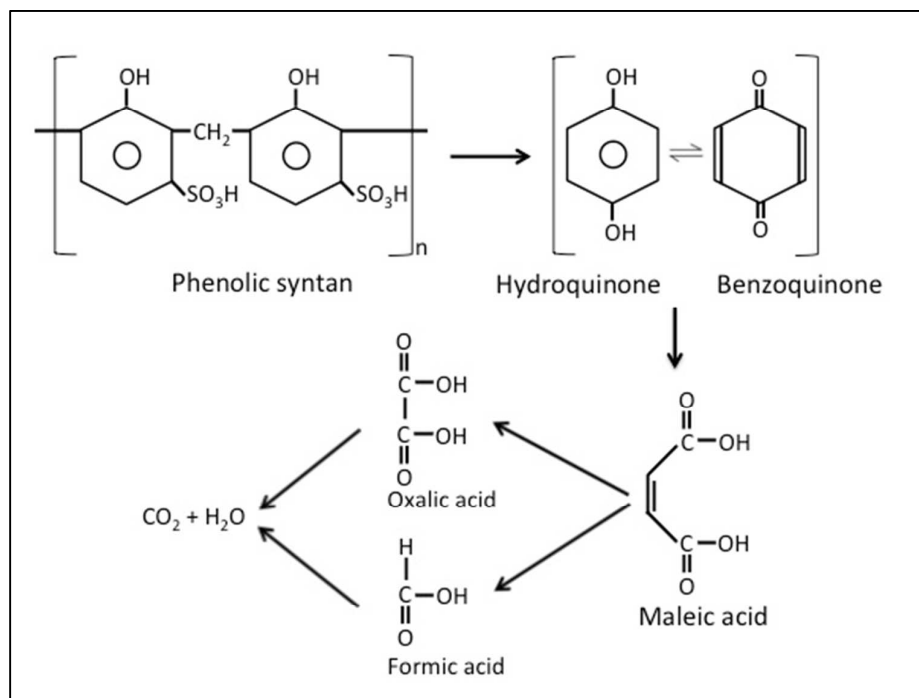
Fig. 7(a) <sup>13</sup>C-CP/TOSS spectrum of phenolic syntan before electrochemical degradation



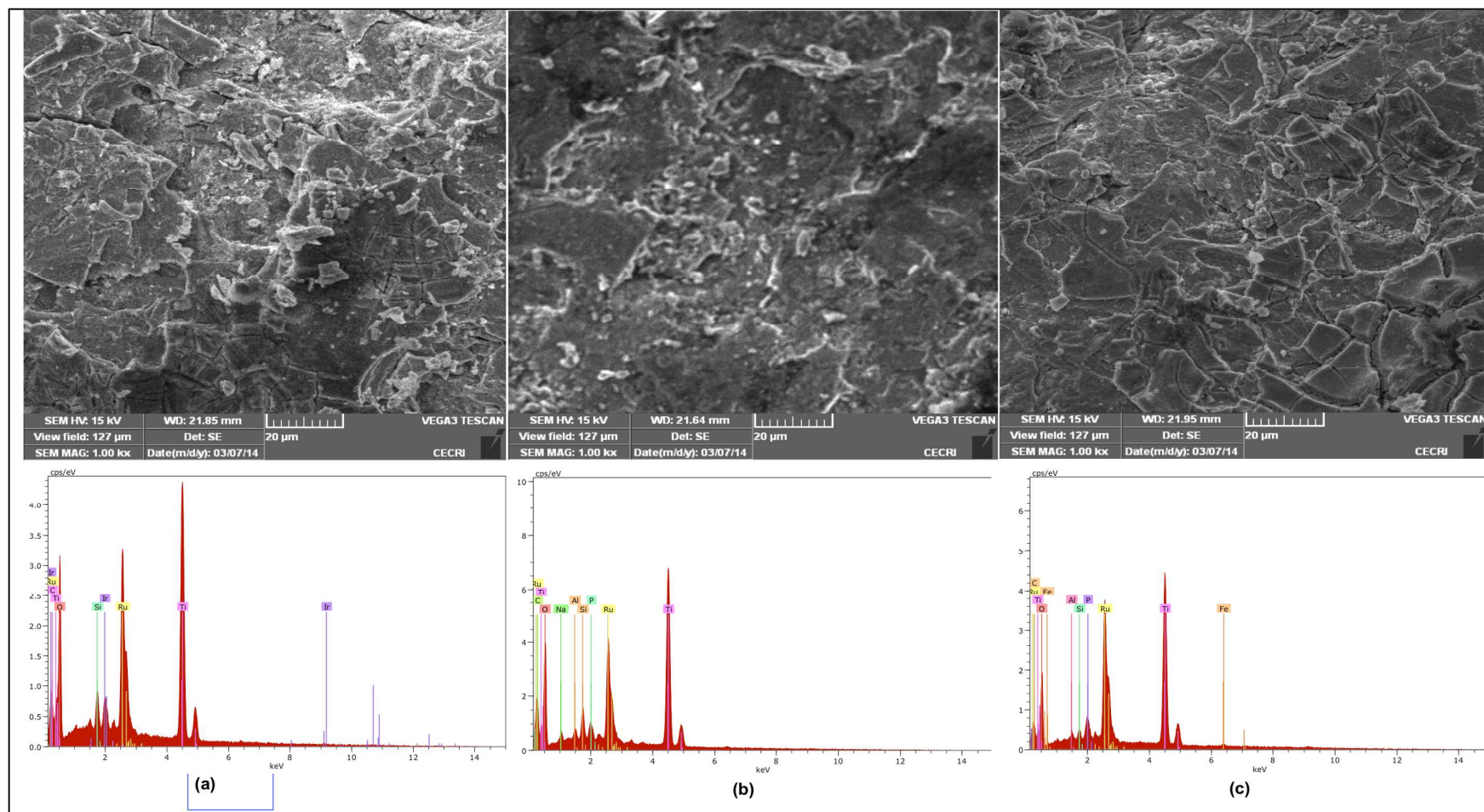
**Fig. 7(b)** <sup>13</sup>C-CP/TOSS spectrum of phenolic sytan after electrochemical degradation (Current density 0.015 A/cm<sup>2</sup>, pH 9.0, concentration of electrolyte 3.0% and duration 120 min).



**Fig. 8** Kinetics for electrochemical degradation of phenolic syntan ( $A=0.015A/cm^2$ ); Electrolyte concentration = 3%; pH = 9.0 and time = 120 min)



**Fig. 9** Possible degradation pathway of phenolic syntan during electrochemical degradation



**Fig. 10** SEM-EDAX micrographs and spectra presenting the chemical composition of the electrodes surface of (a) Before oxidation, (b) After oxidation: Anode and (c) After oxidation: Cathode

**Table 1. Chemical shift values  $^{13}\text{C}$  NMR of phenolic syntan (Before and after electrochemical degradation)**

Assignment	Chemical shift (ppm)	Assignments of carbons
a	156.55	Phenoxy region
b	139.70	C-SO <sub>3</sub> H
c	131.90	Meta, substituted <i>ortho</i> , substituted <i>para</i>
d	115.70	Unsubstituted <i>ortho</i> position
e	40.80	Para-para methylene bridges
f	128.00	Meta, substituted <i>ortho</i> , substituted <i>para</i>



**Table 2. Elemental composition (weight % and Atomic Weight %) of electrodes surfaces from EDAX spectrum**

Elements	Before Electro-oxidation		After Electro-oxidation			
			Cathode		Anode	
	Weight (%)	Atomic weight (%)	Weight (%)	Atomic weight (%)	Weight (%)	Atomic weight (%)
<b>Ti</b>	31.50	21.97	28.92	27.12	32.22	21.26
<b>O</b>	31.20	65.10	29.28	57.62	29.65	58.55
<b>Ru</b>	16.45	5.44	17.57	7.80	13.90	4.34
<b>C</b>	1.91	5.30	1.52	2.17	4.81	12.64
<b>Si</b>	0.99	1.18	ND	ND	1.23	1.38
<b>P</b>	0.95	1.02	0.78	1.13	0.73	0.75