

RSC Advances



This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

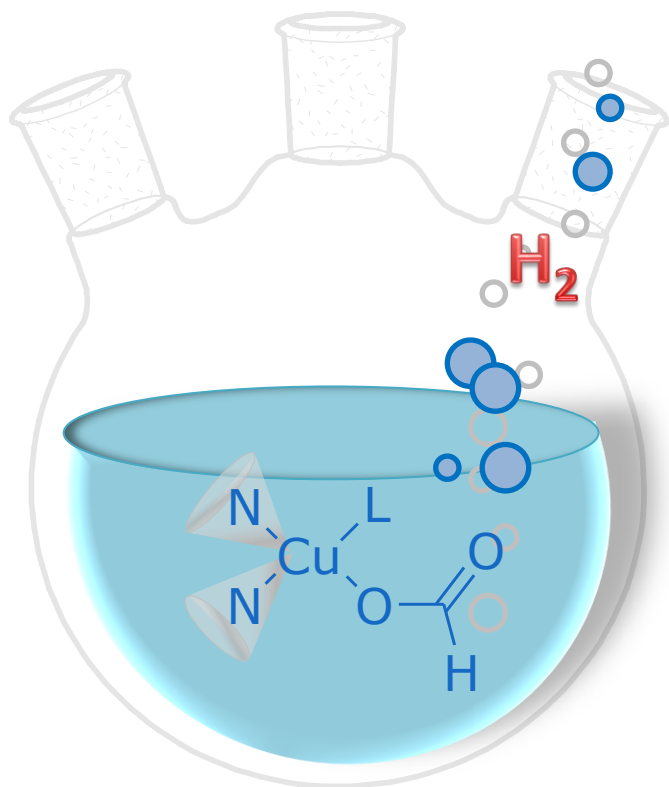
Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. This *Accepted Manuscript* will be replaced by the edited, formatted and paginated article as soon as this is available.

You can find more information about *Accepted Manuscripts* in the [Information for Authors](#).

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard [Terms & Conditions](#) and the [Ethical guidelines](#) still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.

A new Cu-based system for formic acid dehydrogenation

Nicola Scotti, Rinaldo Psaro, Nicoletta Ravasio* and Federica Zaccheria



The production of H₂ from HCOOH was achieved using simple Cu compounds and different HCOOH/amine adducts.

COMMUNICATION

A new Cu-based system for formic acid dehydrogenation

Cite this: DOI: 10.1039/x0xx00000x

Nicola Scotti, Rinaldo Psaro, Nicoletta Ravasio* and Federica Zaccheria

Received 00th January 2012,

Accepted 00th January 2012

DOI: 10.1039/x0xx00000x

www.rsc.org/

The production of H₂ from HCOOH was achieved by using simple Cu compounds and different HCOOH/amine adducts. The activity is strongly dependent on the amine, more basic and bulky ones giving better results whereas the use of chelating amines is detrimental.

New catalytic systems for the hydrogenation of CO₂ to formic acid followed by its decomposition to give back CO₂ and H₂ are extremely interesting as the combination of the two reactions would allow one to valorize CO₂ by its transformation in a highly useful instrument for hydrogen storage.

The development of improved technologies for H₂ generation and H₂ storage in a safe and reversible manner is a prerequisite for the utilization of hydrogen as fuel¹. Moreover formic acid is one of the major by-products of levulinic acid production with the Biofine process.² Compared to H₂, formic acid is liquid and easy to store, transport and handle.³ Besides, HCOOH is considered less hazardous than methanol (its first competitor as hydrogen carrier) and therefore a valuable alternative in spite of its lower hydrogen density (43 vs 125 g/kg).⁴

In the last years some papers, especially from Beller and Laurency groups, on formic acid dehydrogenation have been published, reporting promising results, but using expensive catalysts based on noble metals, such as [{RuCl₂(p-cymene)}₂] or proton-switchable Ir complexes.⁵ Others works report an interesting activity using various heterogeneous system mainly based on Pd, Au and Ag.^{5b,6} As far as non-noble metals are concerned, only a few homogeneous iron catalysts are reported to be active in the reaction, in the presence or in the absence of visible light^{1,7,8} while the potential of Cu based system is still largely unexplored.

In this paper we wish to report our results in the production of H₂ from formic acid by using simple copper complexes and a HCOOH/amine adduct.

In the absence of catalyst a 5:2 HCOOH/NEt₃ adduct (NEt₃=triethylamine) gave no gas evolution, but as soon as Cu(OAc)₂ is added formation of H₂ and CO₂ starts giving in 3 h a total volume of 20 ml. GC analysis of the gas phase of all the experiments showed that H₂ and CO₂ were formed in a 1:1 ratio, together with traces of CO (<150 ppm).

By decreasing the HCOOH/NEt₃ ratio we observed the same trend reported by Beller and coworkers^{5a,d}, the higher the

amine concentration, the higher the conversion, although for ratio lower than 1 the increase was quite limited (Table 1).

Table 1. Decomposition of formic acid using different HCOOH/NEt₃ ratio and different Cu precursors

Cu precursor	HCOOH/NEt ₃ Ratio	V (ml)			C (%)	TON	TOF
		3 h	6 h	22 h			
Cu(OAc) ₂	5/2	20	28	56	4.1	4.4	0.20
Cu(OAc) ₂	1/1	58	103	234	17.2	18.6	0.85
Cu(OAc) ₂	2/5	63	112	273	20.1	21.6	0.98
Cu(OOCH) ₂	1/1	47	88	229	16.8	18.4	0.84
Cu(acac) ₂	1/1	64	121	253	18.6	20.3	0.92
Cu(NO ₃) ₂	1/1	66	116	231	17.0	18.6	0.85
CuCl ₂	1/1	17	26	71	5.2	5.7	0.26
CuO	1/1	47	66	249	19.6	19.6	0.89
Cu powder	1/1	8	9	21	1.5	1.7	0.08

Reaction conditions: Cu=0.26 mmol, 95 °C, HCOOH=28 mmol (1.31 g)

On the contrary the use of different copper compounds for the reaction did not lead to important differences in conversion and total volume produced. This could be due to the rapid replacement of pristine ligands by formate and amine, due to their high concentration in the reaction medium. Only CuCl₂ was significantly less performant while Cu powder was almost inactive.

A more interesting and evident effect was observed by changing the amine (Table 2). Here the basicity plays an important role. In particular, the lower the basicity of the amine, the lower the activity. Aniline and pyridine, e.g., with high pK_b (9.37 and 8.75) gave negligible conversion after 22 h (0.6% and 2%) whereas highly

COMMUNICATION

basic dibutylamine and triethylamine, allowed to reach a conversion around 17% in 22 h (V=221).

Table 2. Decomposition of formic acid with $\text{Cu}(\text{OAc})_2$ using different amines: effect of basicity

Amine	pK_b	V (ml)			C (%)
		3 h	6 h	22 h	22 h
Dibutylamine	2.75	53	94	221	16.2
Piperidine	2.88	59	99	164	12.0
Triethylamine	2.99	58	103	234	17.2
Tributylamine	3.11	115	186	349	25.6
Ethylendiamine	3.29 ^[a]	8	8	8	0.6
Tripropylamine	3.35	160	241	312	22.9
Benzylamine	4.67	13	17	28	2.1
Pyridine	8.75	24	26	28	2.1
Aniline	9.37	11	10	10	0.7
Diphenylamine	13.21	4	5	5	0.4

Reaction conditions: Cat=0.26 mmol, 95°C, HCOOH =28 mmol (1.31 g, 99 wt%), $\text{HCOOH}/\text{Amine}$ =1; [a] pK_{b1}

However, Fig 1 shows that there is no linear dependence of the activity on basicity. On the contrary a very narrow range of pK_b grants high activity while outside this range activity collapses. Moreover there is no linearity even in the pK_b range ensuring activity, e.g. piperidine is more basic than triethylamine or tributylamine (pK_b =2.88 vs 2.99 and 3.11) but the volume of gas produced is much lower (t =22h, 156 ml vs 221 and 349). The particular case of ethylendiamine is worth noting: notwithstanding its high basicity the reaction does not almost proceed. This behavior suggests a coordination effect of the amine on the copper center. Ethylendiamine is well known for its chelating properties and could strongly coordinate the Cu atom blocking all the four square planar coordination sites with its bite angle⁹ of $\sim 85^\circ$ and thus inhibiting coordination of the HCOO^- species and forming a very stable and inactive complex.

Therefore we took into consideration other parameters such as nucleophilicity and steric hindrance that can play a role in the coordination chemistry involved in this reaction. Table 3 reports catalytic data related with the nucleophilic constant, n^{10} and with the conic angle¹¹ of the amines. It is apparent from this comparison that activity increases by increasing steric hindrance and by decreasing nucleophilicity, thus suggesting that the role of the amine is not limited to HCOOH deprotonation.

A reaction mechanism may be suggested in which the presence of two bulky amines could favour the elimination of hydrogen and CO_2 from a square planar intermediate.

The catalytic system tends to deactivate with time, as shown by the solution discolouring and by the formation of a reddish precipitate. Reduction of Cu (II) in basic medium by means of weak reducing agents such as reducing sugars, citric and ascorbic acid¹² is well known.

However the catalyst could be easily reactivated, before complete reduction to metallic phase, simply by opening the reactor to air. After a few minutes (5 min) the mixture turns back to blue (Cu(II)) and an increase in activity is observed (Fig.2).

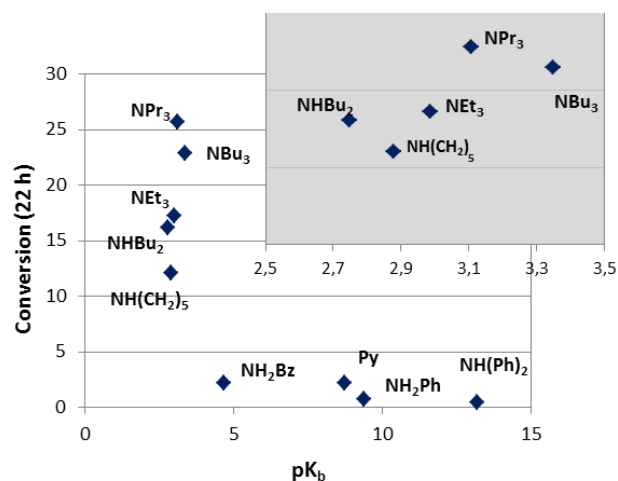


Fig. 1. Conversion vs pK_b for the different amines. The inset shows the region between 2.5-3.5 pK_b

Table 3. Decomposition of formic acid: effect of nucleophilicity

Amine	$n^{[a]}$	pK_b	$\theta^{[b]}$	V (ml)		C (%)
				6 h	22 h	22 h
Piperidine	5.59	2.88	121	99	164	12.0
Dibutylamine	4.77	2.75	158	94	221	16.2
Triethylamine	4.09	2.99	150	103	234	17.2
Tripropylamine	-	3.35	160	241	312	22.9

Reaction conditions: Cat=0.26 mmol, 95 °C, HCOOH =28 mmol (1.31 g, 99 wt%), $\text{HCOOH}/\text{Amine}$ =1; [a] n = nucleophilic constant; [b] conic angle

To stabilize copper in solution we tried to exploit the chelating ability of ethylendiamine, as we already observed that in the presence of such amine neither decomposition of HCOOH nor discoloring of the solution or separation of solids took place. Results reported in Table 4 show that in fact a stoichiometric amount of ethylendiamine with respect to Cu gave a significant improvement in the performance of the $\text{HCOOH}/\text{NEt}_3$ adduct. On the contrary, Cu/en ratio other than 1 or a different diamine such as TMEDA had no effect.

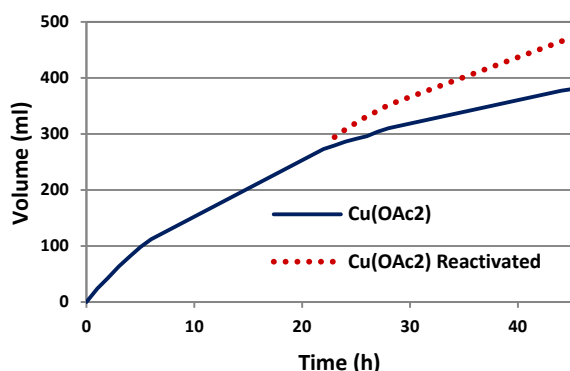


Figure 2. Re-activation of $\text{Cu}(\text{OAc})_2$, by exposing the reaction mixture to air after 22 h.

Another chance is to avoid alkalization of the medium as reduction of copper to form $\text{Cu}(0)$ nanoparticles only occurs under basic conditions. Therefore we added an acid other than HCOOH to keep a low pH during the reaction, without affecting the $\text{HCOOH}/\text{amine}$ ratio. Addition of acetic acid to the $1\text{HCOOH}/1\text{NEt}_3$ mixture did not modify the reaction profile during the first hours of reaction, but the long term stability increased very much ($V=320$ vs 220 , $C=24.5$ vs 16.4) as shown in Fig.3.

Table 4. Stabilization of Cu catalyst using stoichiometric amount of Ethylenediamine or TMEDA

Cu/en Ratio	3 h		6 h		22 h	
	V (ml)	C (%)	V (ml)	C (%)	V (ml)	C (%)
Cu/en=1/2	60	4.4	105	7.7	234	17.2
Cu/en=1/1	121	8.9	189	13.9	299	22.0
Cu/en=2/1	59	4.3	98	7.2	223	16.4
Cu/TMEDA=1/1	70	5.2	111	8.2	224	16.4

Reaction conditions: $\text{Cu}(\text{OAc})_2=0.26$ mmol, 95°C , $\text{HCOOH}=28$ mmol (1.31 g, 99 wt%), $\text{HCOOH}/\text{NEt}_3=1$

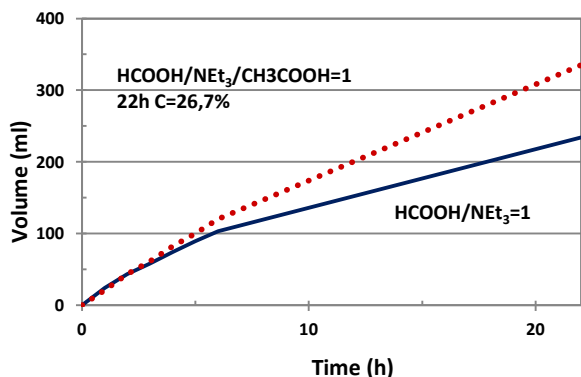


Figure 3. Stabilization of the Cu catalyst by the addition of CH_3COOH to the starting mixture

Finally we tested some precursor with very low potential reduction to metallic copper (Table 5).

Table 5. Decomposition of formic acid using different Cu precursors

Cu precursor	$\text{HCOOH}/\text{NEt}_3$ Ratio	V (ml)			C (%)
		3 h	6 h	22 h	22 h
CuCl	1/1	32	59	189	14.9
Cu_2O	1/1	79	124	217	16.0
CuI	1/1	110	209	493	36.2
$[(\text{PPh}_3)\text{CuH}]_6$	1/1	28	47	59	4.3

Reaction conditions: $\text{Cu}=0.26$ mmol, 95°C , $\text{HCOOH}=28$ mmol (1.31 g)

Cu_2O showed high initial activity but it slowed down reaching at 22 h a conversion comparable to the Cu species reported in Table 1.

On the contrary CuI showed very high activity and stability allowing to reach 36% conversion at 22 h and 66% at 45 h. This matches with a TON value of 72 which is far away from the values obtained with Fe^8 or Ru^{5a} that are up to 4 order of magnitude higher.

In conclusion, copper compounds appear as promising catalysts for H_2 production from $\text{HCOOH}/\text{amine}$ adducts although, so far, neglected by the scientific community.

Their activity can be finely tuned through the choice of the amine while deactivation may be controlled. Work is in progress to get a deeper insight into the mechanism and particularly into the coordination geometry of the active site in order to develop an effective system for hydrogen production from HCOOH in the presence of a non-noble metal.

The Italian Ministry for University and Research (MIUR) is acknowledged for funding the project: „Mechanisms of CO_2 activation for the design of new materials for energy and resource efficiency“ PRIN 2010A2FSS9_001.

Notes and references

Dr. N. Scotti, R. Psaro, Dr. N. Ravasio*, Dr. F. Zaccheria
Institute of Molecular Science and Technology CNR, Via Golgi, 19,
20133 Milano (Italy)

E-mail: n.ravasio@istm.cnr.it

Electronic Supplementary Information (ESI) available: experimental conditions (apparatus, catalytic experiments and gas-phase analysis) and reaction profiles. See DOI: 10.1039/c000000x/

1 a) A. Boddien, B. Loges, F. Gärtner, C. Torborg, K. Fumino, H. Junge, R. Ludwig, M. Beller, *J. Am. Chem. Soc.*, 2010, **132**, 8924; b) I. Mellone, M. Peruzzini, L. R. D. Mellmann, H. Junge, M. Beller, L. Gonsalvi, *Dalton Trans.*, 2013, **42**, 2495.

2 D.J. Hayes, S.W. Fitzpatrick, M.H.B. Hayes, J.R.H. Ross, in: B. Kamm, P.R. Gruber, M. Kamm (Eds.), *Biorefineries: Industrial Processes and Products*, vol. 1, Wiley, Weinheim, Germany, 2005, p. 139.

COMMUNICATION

- 3 B. Loges, A. Boddien, F. Gärtner, H. Junge, M. Beller, *Top. Catal.*, 2010, **53**, 902.
- 4 Y. Yang, M. G. White, P. Liu, *J. Phys. Chem. C*, 2012, **116**, 248.
- 5 a) B. Loges, A. Boddien, H. Junge, M. Beller, *Angew. Chem. Int. Ed.*, 2008, **47**, 3962; b) M. Grasmann G. Laurencyzy, *Energy Environ. Sci.*, 2012, **5**, 8171; c) C. Fellay, P. J. Dyson, G. Laurencyzy, *Angew. Chem. Int. Ed.* 2008, **47**, 3966; d) A. Boddien, B. Loges, H. Junge, M. Beller, *ChemSusChem*, 2008, **1**, 751; e) C. Fellay, N. Yan, P. J. Dyson, G. Laurencyzy, *Chem. Eur. J.*, 2009, **15**, 3752; f) H. Junge, A. Boddien, F. Capitta, B. Loges, J. R. Noyes, S. Gladiali, M. Beller, *Tetrahedron Lett.*, 2009, **50**, 1603; g) J. F. Hull, Y. Himeda, W.-H. Wang, B. Hashiguchi, R. Periana, D. J. Szalda, J. T. Muckerman, E. Fujita, *Nat. Chem.*, 2012, **4**, 383; h) Y. Manaka, W.-H. Wang, Y. Suna, H. Kambayashi, J. T. Muckerman, E. Fujita, Y. Himeda, *Catal. Sci. Technol.*, 2014, **4**, 34; i) W-H Wang, S. Xu, Y. Manaka, Y. Suna, H. Kambayashi, J. T. Muckerman, E. Fujita, Y. Himeda, *ChemSusChem*, 2014, **7**, 1976; j) K. Sordakis, M. Beller, G. Laurencyzy, *ChemCatChem* 2014, **6**, 96; k) D. Mellmann, E. Barsch, M. Bauer, K. Grabow, A. Boddien, A. Kammer, P. Sponholz, U. Bentrup, R. Jackstell, H. Junge, G. Laurencyzy, R. Ludwig, M. Beller, *Chemistry - A European Journal* 2014, **20**, 13589; l) A. Thevenon, E. Frost-Pennington, G. Weijia, A. F. Dalebrook, G. Laurencyzy, *ChemCatChem*, article in press DOI: 10.1002/cctc.201402410
- 6 a) M. Ojeda, E. Iglesia, *Angew. Chem. Int. Ed.*, 2009, **48**, 4800; b) X. Gu, Z.-H. Lu, H.-L. Jiang, T. Akita, Q. Xu, *J. Am. Chem. Soc.*, 2011, **133**, 11822; c) K. Tedsree, T. Li, S. Jones, C. W. A. Chan, K. M. K. Yu, P. A. J. Bagot, E. A. Marquis, G. D. W. Smith, S. C. E. Tsang, *Nature Nanotech.*, 2011, **6**, 302; d) X. Zhou, Y. Huang, W. Xing, C. Liu, J. Liao, T. Lu, *Chem. Commun.*, 2008, 3540; e) K. Mori, M. Dojo, H. Yamashita, *ACS Catal.*, 2013, **3**, 1114.
- 7 a) S. Enthaler, B. Loges, *ChemCatChem*, 2012, **4**, 323; b) A. Boddien, F. Gärtner, R. Jackstell, H. Junge, A. Spannenberg, W. Baumann, R. Ludwig, M. Beller, *Angew. Chem. Int. Ed.*, 2010, **49**, 8993.
- 8 a) E. A. Bielinski, P. O. Lagaditis, Y. Zhang, B. Q. Mercado, C. Würtele, W. H. Bernskoetter, N. Hazari, S. Schneider, *J. Am. Chem. Soc.* 2014, **136**, 10234–10237; b) A. Boddien, D. Mellmann, F. Gärtner, R. Jackstell, H. Junge, P. J. Dyson, G. Laurencyzy, R. Ludwig, M. Beller, *Science* 2011, **333**, 1733
- 9 C.-C. Su, Y.-I. Lin, S.-J. Liu, T.-H. Chang, S.-L. Wang, F.-L. Liao, *Polyhedron*, 1993, **12**, 2687.
- 10 a) H. K. Hall Jr., R. B. Bates, *Tetrahedron Lett.*, 2012, **53**, 1830; b) J. W. Bunting, J. M. Mason, C. K. M. Heo, *J. Chem. Perkin Trans.*, 1994, **2**, 2291.
- 11 A. L. Seligson, W.C. Trogler, *J. Am. Chem. Soc.*, 1991, **113**, 2520.
- 12 a) L. Gou, C. J. Murphy, *Nano Lett.*, 2003, **3**, 231; b) H. Bao, W. Zhang, Q. Hua, Z. Jiang, J. Yang, W. Huang, *Angew. Chem. Int. Ed.*, 2011, **50**, 12294; c) Q. Hua, D. Shang, W. Zhang, K. Chen, S. Chang, Y. Ma, Z. Jiang, J. Yang, W. Huang, *Langmuir*, 2011, **27**, 665.