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## COMMUNICATION

## Surface roughness-induced speed increase for active Janus micromotors

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Udit Choudhury,<sup>‡a</sup> Lluís Soler,<sup>‡a,b</sup> John Gibbs,<sup>a,c</sup> Samuel Sanchez,<sup>\*a,d,e</sup> and Peer Fischer<sup>a,f</sup>Received 00th January 2012,  
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**We demonstrate a simple physical fabrication method to control surface roughness of Janus micromotors and fabricate self-propelled active Janus microparticles with rough catalytic platinum surfaces that show a four-fold increase in their propulsion speed compared to conventional Janus particles coated with a smooth Pt layer.**

The use of catalytic reactions for self-propulsion of micro and nanoparticles is a well-established means to move colloidal particles in solution at low-Reynolds number.<sup>1, 2</sup> The colloids must be anisotropic in their material properties for them to generate any active propulsion. For that purpose, Janus spheres with two different faces have been fabricated, including platinum/insulator Janus microspheres, platinum/gold bimetallic nanoparticles and nanorods, and platinum-coated microtubular jets<sup>2-9</sup> The propulsion in these micromotors arises from the decomposition of hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) at the platinum (Pt) surface. While a number of studies have focussed on developing new propulsion systems,<sup>10-12</sup> there have been only a few studies examining the effect of the surface morphology on catalytic self-propulsion.<sup>13-15</sup>

It is well known that the catalytic activity is directly related to the surface area of the catalyst and can thus be influenced by introducing nanoscale surface-features to increase the effective surface area.<sup>16</sup> This is commonly used to increase the surface area of conducting electrodes in electrochemical reactions.<sup>17</sup> Hence, one could expect that the incorporation of nanoscale features on the catalytic face of catalytic micro/nanomotors should also lead to a higher effective area. This should consequently lead to a higher net turn-over and thus higher propulsion speeds.

Ozin *et al.* studied the motion of electrochemically fabricated rough bimetallic rods produced by incorporating Ludox® silica nano-particles in the electroplating solution for bimetallic nanorods.<sup>13</sup> Wang *et al.* included carbon nanotubes into the Pt plating solution and obtained much faster speeds of the Au-CNT/Pt nanowires compared with Au-Pt ones.<sup>14</sup> For polystyrene/Pt Janus microspheres a shift in the propulsion mechanism from diffusiophoresis to bubble propulsion was observed after chemically roughening the surface.<sup>15</sup> Increasing the surface roughness of Pt in Pt/insulator Janus particles is, however, not straightforward. First, insulating particles do not lend themselves to direct electrochemical

fabrication and typical physical vapour deposition (PVD) methods usually yield smooth surfaces. Further, bimetallic micromotors grown electrochemically have limitations in propulsion in high ionic media. This necessitates exploring different material configurations for studying micro scale propulsion for which physical vapour deposition is a simple and widely used scheme.

Here, we present a facile method to obtain roughness using PVD. Commonly, Janus particles are grown by sputtering or evaporating a layer of Pt onto silica or polystyrene beads. Pt by itself does not, in general, form rough surfaces. Here we show that by first depositing an under-layer of silica before depositing the Pt introduces nanoscale roughness on the Janus particles and that this then automatically yields a rough Pt surface. We demonstrate that this leads to a four-fold speed increase compared to particles with a smooth surface. The reaction rates for catalytic propulsion was derived assuming a diffusiophoretic model of propulsion which shows a similar two to four fold increase in turnover rates for rough micromotors. The effect of roughness on catalytic activity was further verified by oxygen evolution tests and observation of the surface topology by SEM.

The morphology of thin films grown by glancing angle deposition (GLAD), a variant of PVD, where the substrate is tilted relative to the vapour flux to induce shadowed film growth, whilst permitting azimuthal rotation, depends on the deposition rate, the angle of the incident vapour and the material properties. Nanoscale morphology on a plane substrate can be introduced by tilting the substrate at a high angle relative to the vapour flux to induce self-shadowing during the growth.<sup>18, 19</sup> Substrate rotation under glancing angle deposition can promote columnar growth of nanostructures.<sup>18</sup> However, metals have higher surface mobilities than (metal) oxides and will therefore diffuse on the substrate easily to form smoother surfaces compared to oxides. This effectively inhibits pure metal thin films, including Pt, from forming rough surfaces.

In this work, we have explored two different growth techniques to introduce roughness on smooth silica spheres. We first prepared a dense monolayer of silica beads (5 µm diameter) by drop-casting a diluted suspension of beads onto a clean silicon wafer. After drying, we placed the wafer in a vacuum PVD system. Two types of rough Pt Janus particles were grown, named R<sub>1</sub> and R<sub>2</sub>. Both preparation methods are described below:

R<sub>1</sub> : Preparation of Pt Janus micromotors under nominally

normal incidence: 80 nm of SiO<sub>2</sub> was deposited by an e-beam evaporator at 0° (normal incidence) as the first layer onto the silica beads followed by 7 nm of titanium (Ti) and 20 nm of Pt (Fig. 1a). Ti serves as an adhesion layer. The vapour flux necessarily impinges on the curved surfaces of the silica beads with varying angles of incidence: 90° at the equator to 0° at the pole. This procedure promotes patchy growth on the particle surface (as can be seen in Fig. 1c).

**R<sub>2</sub>** : Preparation of Pt Janus micromotors under nominally oblique angles: To stimulate growth of columnar structures on the surface of the microspheres the deposition of SiO<sub>2</sub> was performed by tilting the substrate inside the e-beam evaporation chamber. This resulted in high angles of incidence ( $\alpha = 87^\circ$  at the pole, Fig. 1b). In addition, the substrate was rotated about the azimuth at five revolutions per minute (Fig 1b). Keeping the azimuthal rotation speed constant, the substrate tilt angle  $\alpha$  was continuously swept from  $87^\circ$  to  $0^\circ$  to ensure even hemispherical coverage of the surface of the microsphere (Fig. 1b). The SiO<sub>2</sub> deposition is followed by a 7 nm layer of Ti and then a 20 nm layer of Pt, both at nominally normal (0°) incidence. It is important to note that the same amount of SiO<sub>2</sub> is deposited in both fabrication procedures R<sub>1</sub> and R<sub>2</sub>.

To facilitate the direct comparison with conventional fabrication of spherical Janus micromotors, we fabricated two different types of Janus particles for control purposes, named S<sub>1</sub> and S<sub>2</sub>, which are described below:

**S<sub>1</sub>** : 7 nm Ti and 20 nm Pt were evaporated keeping the substrate fixed at 0° on a monolayer of silica beads (see Fig. 1a).

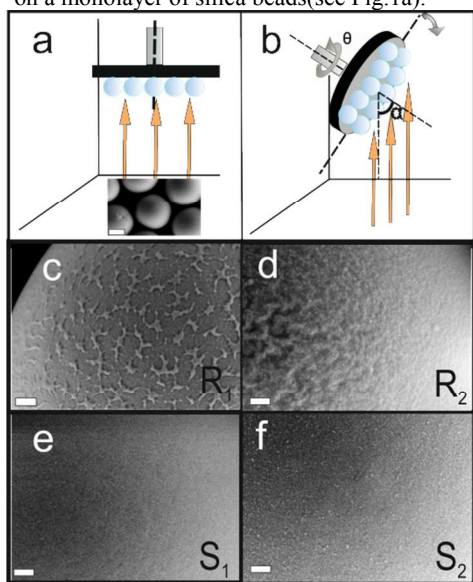


Fig.1 Schematic of the PVD fabrication method and images of Janus micromotor surfaces. 1a) Particles R<sub>1</sub>, S<sub>1</sub> and S<sub>2</sub> were fabricated by keeping the substrate at fixed position. SiO<sub>2</sub> was initially deposited for R<sub>1</sub> and subsequently Ti and Pt were deposited. Orange arrows indicate the direction of the incoming vapour flux. 1b) Particle R<sub>2</sub> was fabricated by continuously rotating the substrate at 5 rpm and changing  $\alpha$  from  $87^\circ$  to  $0^\circ$  while SiO<sub>2</sub> was evaporated, while keeping the azimuthal angle  $\theta$  constant. Subsequently, titanium and platinum was evaporated by keeping the substrate fixed at 0°. The scale bar in the image 1a is 2  $\mu\text{m}$ . c,d,e,f : Morphology of particles R<sub>1</sub>, R<sub>2</sub>, S<sub>1</sub> and S<sub>2</sub>, respectively. The SEM images are captured by an SE2 detector. The scale bar for the images (c,d,e,f) is 200nm.

**S<sub>2</sub>** : 80 nm of Ti and 20 nm of Pt was evaporated while keeping the substrate fixed at 0° to ensure that the particles exhibit a diameter comparable to the Janus particles of R<sub>1</sub> and R<sub>2</sub>. However, here the Pt

surface is smoother than for the particles in R<sub>1</sub> and R<sub>2</sub> due to the higher surface mobility of the Ti adatoms. The surface-smoothness is comparable to the particles in S<sub>1</sub>.

To determine the surface morphology of the silica spheres qualitatively, the samples were examined by scanning electron microscopy (SEM). The images in Figs. 1c, 1d, 1e and 1f suggest the topological differences between the coated surfaces. While the top surface of R<sub>1</sub> shows small patches of silica on the surface of the microsphere, the surface of R<sub>2</sub> shows a wrinkled surface texture caused by self-shadowing. The coated surfaces of particles S<sub>1</sub> and S<sub>2</sub> have in contrast a smoother topology.

To estimate the influence of the surface roughness on the catalytic activity of the Pt decomposition of H<sub>2</sub>O<sub>2</sub>, we have performed oxygen (O<sub>2</sub>) evolution experiments. In order to permit quantitative measurements we chose to perform the O<sub>2</sub> evolution tests on Si wafer-pieces (1 cm x 2cm) coated with smooth and rough Pt surfaces, rather than surfaces covered with the silica particles. Silica particles do not form completely close-packed monolayers causing high variability in the particle covered surface and hence the total surface area. The smooth wafers were prepared by depositing Ti (7 nm) and Pt (20 nm) at 0° as shown in Fig. 1a. The rough wafer was prepared by first depositing SiO<sub>2</sub> under glancing angle (as shown in Fig. 1b) and subsequently coated with Ti (7 nm) followed by Pt (20 nm) at 0°. The wafers therefore mimic the surface morphology of particles R<sub>2</sub> (rough) and particles S<sub>1</sub> and S<sub>2</sub> (smooth). The roughness for the particle R<sub>1</sub> is due to the surface curvature of the silica spheres and hence cannot be mimicked by a planar wafer.

After the deposition, each wafer piece was immersed in a 100 cm<sup>3</sup> Pyrex glass reactor containing 75 mL of 10% H<sub>2</sub>O<sub>2</sub> at room temperature. The detailed experimental setup to measure the evolution of gases from reactions in aqueous solutions is described elsewhere.<sup>20</sup> Here we only give a brief description of the experimental details. The generation of O<sub>2</sub> started as soon as the wafer covered with catalytically-active Pt came into contact with the H<sub>2</sub>O<sub>2</sub> solution. Oxygen produced by the decomposition of H<sub>2</sub>O<sub>2</sub> escapes from the reactor via a silicone tube, which was then passed through a water bath at room temperature and collected in an inverted burette filled with water. The volume of the generated oxygen was deduced (at 298 K and 1 atm) from the water level change in the burette. The maximum rates of O<sub>2</sub> evolution were determined from the maximum slope of the experimentally determined O<sub>2</sub> generation curves. The maximum O<sub>2</sub> evolution rate for rough Pt was found to be 1.8 mmol O<sub>2</sub> cm<sup>-2</sup> Pt min<sup>-1</sup> and for smooth Pt was 0.6 mmol O<sub>2</sub> cm<sup>-2</sup> Pt min<sup>-1</sup>.

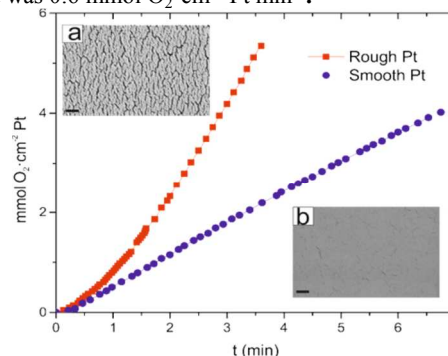


Fig. 2 Evolution of O<sub>2</sub> from Pt layers (thickness 20 nm) deposited onto a Si wafer piece (1 cm x 2 cm) reacting with 10% H<sub>2</sub>O<sub>2</sub>. The upper left inset (a) shows a SEM image of rough Pt (as deposited by the deposition method used for particle R<sub>2</sub>). The lower right inset (b) shows an SEM image of smooth Pt (as deposited by the deposition method used for particle S<sub>1</sub>). The rough surface mimics the topology

of particle  $R_2$  and the smooth surface that of particles  $S_1$  and  $S_2$ . The scale bar is 200 nm.

After verifying the higher catalytic rates for the rough surfaces, we investigated the different swimming characteristics of the Janus microparticles. The Janus particles were released from the wafer into deionized water by sonication and the suspension was washed and purified by centrifugation. Aqueous suspensions of Janus micromotors were pipetted onto a silicon wafer piece, which was previously cleaned with  $O_2$  plasma, and increasing amounts of  $H_2O_2$  were added sequentially to obtain the desired  $H_2O_2$  concentration. The videos of the self-propelled particles were recorded with a Leica optical microscope coupled to a CCD camera recording at 30 fps. The particles were tracked for 20 s. (Fig.3) and the trajectories of 10 particles were combined to determine the average speed and the mean squared displacement (MSD) (see Fig. 4 and supporting videos R1, R2, S1 and S2).

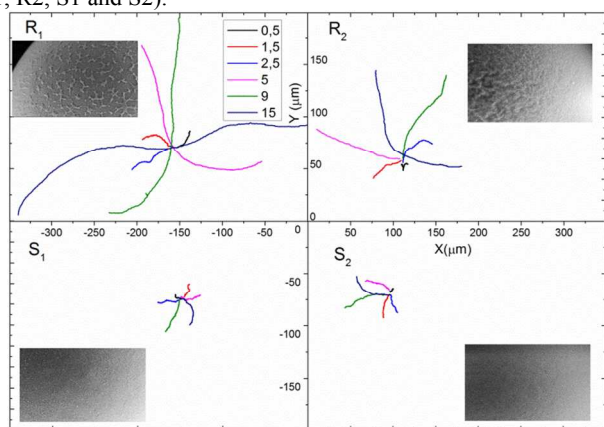


Fig.3 Examples of tracking trajectories of a single Janus particle of type  $R_1$ ,  $R_2$ ,  $S_1$  and  $S_2$  at different peroxide concentrations tracked for 20 s. Particle  $R_1$  in 15%  $H_2O_2$  covers a correspondingly largest distance

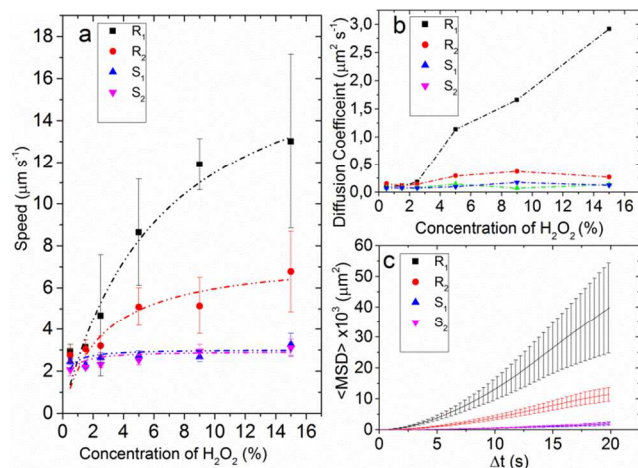


Fig. 4a: Speed of Janus particles at different  $H_2O_2$  concentrations. Smooth Particles  $S_1$  and  $S_2$  show a maximum mean speed of  $3 \mu\text{m s}^{-1}$  while particles  $R_1$  and  $R_2$  have a maximum mean speed of  $7 \mu\text{m s}^{-1}$  and  $13 \mu\text{m s}^{-1}$ , respectively, for a 15%  $H_2O_2$  concentration. Fig.4b: Translational diffusion coefficient  $D_{diff}$  of Janus particles  $R_1$ ,  $R_2$ ,  $S_1$  and  $S_2$  obtained by fitting eq. (1) for to the mean squared displacement of the trajectory (from 0 to 2 s) with the error bars as weights (see supplementary Fig.S1). Fig 4c: MSD plot with error bars for the 15%  $H_2O_2$  concentration for different particles.

At low  $H_2O_2$  concentration (0.5%) the speeds of all particles are low and within the experimental accuracy no differences can be observed. For higher concentrations the speed of the smooth particles  $S_1$  and  $S_2$  compare well to the literature value for  $5 \mu\text{m}$  particles<sup>21</sup> and are comparable for all measured  $H_2O_2$  concentrations. At 5%  $H_2O_2$  the mean velocities between the smooth and the rough particles diverge with  $R_1$  ( $9 \mu\text{m s}^{-1}$ ) and  $R_2$  ( $5 \mu\text{m s}^{-1}$ ) showing, respectively a 3 and a 1.5 fold increase over particles  $S_1$  ( $3 \mu\text{m s}^{-1}$ ) and  $S_2$  ( $2.5 \mu\text{m s}^{-1}$ ). At 15%  $H_2O_2$  particle  $R_1$  propels at a mean speed of  $13 \mu\text{m s}^{-1}$  compared to the  $3 \mu\text{m s}^{-1}$  of particle  $S_1$ .

The mean squared displacements ( $\Delta L^2$ ) as a function of the time interval ( $\Delta t$ ) were analyzed for individual concentrations to obtain the diffusion constant,  $D_{diff}$ . For time scales shorter than the rotational diffusion time ( $\tau_r$ ),  $\Delta L^2$  can be approximated as<sup>1,21</sup>

$$\Delta L^2 = 4 D_{diff} \Delta t + V^2 \Delta t^2 \quad (1)$$

which is fitted for  $\Delta t = 2\text{s}$  ( $\Delta t \ll \tau_r = 50\text{s}$ ), where  $D_{diff}$  is the diffusion constant and  $V$  is the propulsion speed (Electronic Supplementary Information Fig. S1). The diffusion constant  $D_{diff}$  is calculated by fitting equation (1) to data of Fig. for  $S_1$  using the error bars as weights.

The translational diffusivities of the smooth particles  $S_1$  and  $S_2$  remain close to the theoretically calculated value  $0.1 \mu\text{m}^2\text{s}^{-1}$  for a  $5 \mu\text{m}$  particle

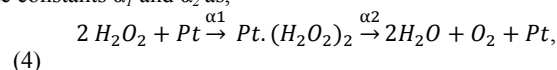
$$D_{diff} = k_B T / 6\pi\eta R \quad (2)$$

where  $k_B$  is the Boltzmann constant,  $T$  is Temperature,  $\eta$  is the viscosity and  $R$  is the radius of the particle). The particles  $R_1$  and  $R_2$  show a higher mean  $D_{diff}$  for higher  $H_2O_2$  concentrations reaching  $3 \mu\text{m}^2\text{s}^{-1}$  for particle  $R_1$  (see Fig. 4b).

The self-diffusiophoretic speed can be expressed in terms of surface reaction rate  $k$  as<sup>1</sup>

$$V = \frac{3\pi}{2} k a \lambda^2 \quad (3)$$

where  $a$  is the hydrodynamic radius of the solute,  $k$  is the reaction rate and  $\lambda$  is the interaction zone between the solute and the particle. The breakdown of  $H_2O_2$  can be modeled as a two-step reaction with rate constants  $\alpha_1$  and  $\alpha_2$  as,<sup>1,21</sup>



with,

$$k = \alpha_2 \frac{[H_2O_2]_{vol}}{[H_2O_2]_{vol} + \alpha_2 / \alpha_1} \quad (5)$$

We can solve the unknown reaction rate constants  $\alpha_1$  and  $\alpha_2$  as a function of the  $H_2O_2$  concentration by fitting equation (3) and equation (5) to the speed of particles  $R_1$ ,  $R_2$ ,  $S_1$  and  $S_2$  in Fig.4a. We assume  $a = 1 \text{ \AA}$  and  $\lambda = 5 \text{ \AA}$ ,<sup>1</sup> and obtain the best fit line for Eqn. (3) to the speed data (see supplementary Fig S2). The experimentally determined reaction rates for different particles at 10%  $H_2O_2$  concentrations are summarized in Table 1.

	$\alpha_1 (\mu\text{m}^2\text{s}^{-1})$	$\alpha_2 (\mu\text{m}^2\text{s}^{-1})$	$k \text{ at } 10\% (\mu\text{m}^2\text{s}^{-1})$
$R_1$	$2.49 \times 10^{10}$	$1.6 \times 10^{11}$	$9.75 \times 10^{10}$
$R_2$	$2.42 \times 10^{10}$	$6.40 \times 10^{10}$	$5.06 \times 10^{10}$
$S_1$	$1.19 \times 10^{11}$	$2.57 \times 10^{10}$	$2.51 \times 10^{10}$
$S_2$	$9.32 \times 10^{10}$	$2.50 \times 10^{10}$	$2.43 \times 10^{10}$

Table 1: Experimental reaction rates  $\alpha_1$  and  $\alpha_2$  for  $R_1$ ,  $R_2$ ,  $S_1$  and  $S_2$  Janus particles calculated by fitting Eqn. (3) and Eqn. (4) to the speed of the micromotors for 10%  $H_2O_2$  concentration (Fig S2). We used  $a=1 \text{ \AA}$  and  $\lambda=5 \text{ \AA}$  and solved for  $\alpha_1$  and  $\alpha_2$ . We calculate the reaction rate  $k$  from Eqn. (4) at 10%  $H_2O_2$  concentration to compare the surface reaction rate of the different micromotors. (see supplementary text S4 for detailed discussion)

Since the difference between the different particles is primarily due to a change in surface area, the change in reaction rate and speed can serve as an indirect measure for the surface area. Further, the speed

as a function of the  $\text{H}_2\text{O}_2$  concentration saturates at higher  $\text{H}_2\text{O}_2$  concentrations.<sup>1, 5</sup> Therefore we can choose a concentration of 10% to calculate the reaction rate and estimate the surface area enhancement effects from it. Furthermore, particle  $\text{S}_2$  with a 80 nm Ti under-layer is of the same dimension as particles  $\text{R}_1$  and  $\text{R}_2$ . Hence, we can conclude that the increased reaction rate in particles  $\text{R}_1$  and  $\text{R}_2$  is caused by the surface roughness due to the nanoscale features introduced by the PVD process. From Fig. 2, we find the  $\text{O}_2$  evolution for the rough Pt surface prepared using the deposition protocol for  $\text{R}_2$  is three times higher than for the smooth surface prepared by the deposition protocol for  $\text{S}_1$ , suggesting that the surface area is also three times larger for the particle  $\text{R}_2$  compared with the smooth particles  $\text{S}_1$  and  $\text{S}_2$ . The reaction rate at 10%  $\text{H}_2\text{O}_2$  concentration shows a similar increase of four and two times for particles  $\text{R}_1$  and  $\text{R}_2$ , respectively, compared to particles  $\text{S}_1$  and  $\text{S}_2$ . Hence, we find that the increase in catalytic activity as observed *via* the speeds as well as the  $\text{O}_2$  evolution tests on the rough surfaces are in agreement and of the same order of magnitude. This suggests that the increase in the effective surface area by the deposition of a  $\text{SiO}_2$  under-layer applies both at the macroscopic wafer-scale and at the microscale of individual particles.

The difference in the speeds of  $\text{R}_1$  and  $\text{R}_2$  can be qualitatively explained by observing the morphology of the particles. While  $\text{R}_1$  has random rough patches on its surface,  $\text{R}_2$  has a more creased topology indicating denser growth of  $\text{SiO}_2$  patches. Subsequently, the deposition of Ti and Pt under normal incidence yields larger coverage of the catalyst Pt on the patchy surface of  $\text{R}_1$  than for  $\text{R}_2$ , since it is easier for the metal to diffuse uniformly on the patchy morphology of  $\text{R}_1$ , while self-shadowing only covers the tips of the structures in  $\text{R}_2$ . Hence, the effective area of the catalyst will be higher in  $\text{R}_1$  than in  $\text{R}_2$  which will lead to increased propulsion speed of  $\text{R}_1$ , as is experimentally observed.

## Conclusions

In conclusion, we have presented a fabrication scheme for making rough Pt surfaces on microsphere surfaces with PVD. We have shown that this results in a four-fold increase in the speed of the self-propelled particles compared to Janus particles that have a smooth Pt surface. Furthermore, we have characterized the surface morphology of the rough spheres and theoretically estimated the increase of surface area of the particles fabricated by glancing angle growth. The simple fabrication strategy and a high increase in catalytic surface area and propulsion speed open up a new way to control the locomotion of micro-scale active swimmers. It also shows the range of speed increases that are available with PVD methods. It will be interesting to apply these techniques to rolled-up tubular micromotors where the roughness may also influence the formation of bubbles.

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## Notes and references

- <sup>a</sup>Max-Planck Institute for Intelligent Systems. Heisenbergstr.3, 70569 Stuttgart, Germany.
- <sup>b</sup>Institute of Energy Technologies, Universitat Politècnica de Catalunya, Diagonal 647, 08028 Barcelona, Catalonia, Spain.
- <sup>c</sup>Department of Physics and Astronomy, Northern Arizona University, S. San Francisco Street, Flagstaff, Arizona 86011, United States
- <sup>d</sup>Institució Catalana de Recerca i Estudis Avançats (ICREA), Passeig Lluís Companys 23, 08010, Barcelona, Spain
- <sup>e</sup>Institut de Bioenginyeria de Catalunya (IBEC), Baldiri I Reixac 10-12, 08028 Barcelona, Spain
- <sup>f</sup>Institute for Physical Chemistry, University of Stuttgart, Pfaffenwaldring 55, D-70569 Stuttgart, Germany
- \*Email: [sanchez@is.mpg.de](mailto:sanchez@is.mpg.de), [sanchez@ibecbarcelona.eu](mailto:sanchez@ibecbarcelona.eu)
- ‡These authors contributed equally to the work.
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