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1 **Biocatalytic Perchlorate Reduction: Kinetics and Effects of Groundwater Characteristics**

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11 **Water Impact Statement**

12 Perchlorate, an endocrine disrupter, is toxic to sensitive populations at low concentrations. This
13 manuscript investigated biocatalytic removal of perchlorate for use in drinking water treatment.
14 Robust biocatalytic activity was observed in groundwater samples over a range of conditions.
15 Measured perchlorate removal rates in groundwater samples provide a basis for reactor design.
16 The results support the potential for biocatalytic perchlorate removal.

18 **Abstract**

19 Biocatalytic reduction of perchlorate can minimize the effects of competitive electron acceptors
20 and completely reduce perchlorate into chloride and oxygen, but to date has only been
21 demonstrated under idealized laboratory conditions. This work investigated biocatalytic
22 perchlorate reduction in two groundwater drinking water sources, under a range of conditions and
23 with a variety of electron donors. The biocatalysts, perchlorate reductase and chlorite dismutase
24 from *Azospira oryzae*, had a maximum activity of $162.5 \pm 8.4 \text{ U } (\mu\text{g Mo})^{-1}$ in buffered solution
25 and retained 82-94% of their activity in groundwater samples. The half saturation concentration
26 for perchlorate was $92.0 \mu\text{M}$. Perchlorate reduction rates were higher than nitrate reduction rates,
27 with nitrate as the sole electron acceptor having reduction rates 7.5 to 9.7 % of the maximum
28 perchlorate reduction rates in groundwater. Activity was consistent from pH 6.5 to 9.0. The
29 temperature dependence of biocatalytic perchlorate reduction was well defined by the Arrhenius
30 equation. No significant difference in biocatalytic activity was observed with calcium and
31 magnesium concentrations over the tested range of 0 to 400 mg L^{-1} or with natural organic matter
32 up to 6 mg L^{-1} . Ascorbic acid with addition of an electron shuttle resulted in reduction of more
33 than 99% of perchlorate in less than 6 hours, an order of magnitude loss in activity compared to

34 methyl viologen. These results suggest the potential of the biocatalysts for treating perchlorate
35 over a range of concentrations and conditions representative of industrial and groundwater
36 perchlorate contamination.

37

38 **Keywords**

39 *Azospira oryzae*

40 Perchlorate

41 Groundwater

42 Biocatalyst

43 Perchlorate reductase

44 Chlorite dismutase

45 Enzyme Based Remediation

46 **1. Introduction**

47 Widespread perchlorate contamination of drinking water has been found in over 20 U.S.
48 states, resulting in advisory or regulatory limits in several states and a pending regulatory limit of
49 $15 \mu\text{g L}^{-1}$ from the United States Environmental Protection Agency.¹⁻³ These regulations are
50 intended to prevent developmental defects in fetuses and young children arising from preferential
51 uptake of perchlorate in the thyroid.⁴⁻⁶

52 To remove perchlorate from drinking water, municipalities primarily use non-selective or
53 selective ion exchange.¹ Whole-cell biological processes have also been shown to reduce
54 perchlorate.¹ However, these technologies have significant drawbacks. Non-selective ion
55 exchange produces brine waste with elevated perchlorate concentrations and is less effective for
56 perchlorate removal in the presence of high concentrations of competing anions such as nitrate
57 and sulfate.⁷ Specialized, bi-functional resins target perchlorate more specifically, reducing the
58 impact of competing anions.⁸ The disadvantage is that these specialized resins are not easily
59 regenerated and are generally incinerated after saturation,⁸ increasing costs and environmental
60 impacts. Whole cell biological reduction has been explored in a number of configurations
61 including fixed beds,^{9, 10} bioelectrochemical reduction,¹¹ and membrane biofilm reactors.¹²
62 However, biological reduction of perchlorate also performs poorly in the presence of co-
63 contaminating nitrate, sulfate, and oxygen, since these are preferred electron acceptors for many
64 microorganisms.¹³⁻¹⁵ Other challenges associated with biological perchlorate removal include the
65 potential for hydrogen sulfide production, the possible growth of pathogenic organisms, and
66 public perception.

67 Because co-contaminating nitrate and sulfate are common in drinking water sources,¹⁶
68 these problems necessitate advances in perchlorate treatment. To that end, a wide variety of

69 approaches are being investigated, including chemical¹⁷ and biological¹⁸ processes to treat
70 perchlorate in waste brines, direct biological regeneration of perchlorate-selective resins,^{19,20} ion
71 exchange membrane bioreactors,²¹ and two stage membrane biofilm reactors that minimize
72 sulfate reduction.²² We recently proposed a system that selectively reduces perchlorate into
73 innocuous chloride and oxygen using cell-free biocatalysts, specifically perchlorate reductase
74 (PR) and chlorite dismutase (CD) from *Azospira oryzae*, and provided proof of concept for this
75 approach in buffered, laboratory solutions.²³ PR is a soluble, periplasmic protein with similarity
76 to nitrate reductases.²⁴ CD is also a soluble protein and catalyzes an intramolecular electron
77 transfer to form the final products of chloride and oxygen.²⁵

78 Biocatalytic treatment is generally attractive due to high substrate affinities and reaction
79 rates, specificity, and optimal activities under ambient conditions of temperature, pressure, and
80 pH. However, to date biocatalysts have largely been used only for high value products such as
81 pharmaceuticals.²⁶ A prominent exception is the extracellular biocatalyst laccase, which has been
82 used to treat phenolic compounds in industrial wastewater (e.g. forest products industry²⁷ and
83 textile and dye-making industry²⁸). Laccase has also been proposed for oxidation of phenolic
84 compounds such as pharmaceuticals in wastewater effluent.²⁹

85 For treatment of perchlorate and other chlorine oxyanions, a biocatalytic approach shares
86 with biological treatment processes the advantage of completely degrading the contaminant, but
87 avoids some of the challenges associated with whole-cell reduction of perchlorate. Specifically,
88 unlike whole cells, which preferentially use nitrate, the biocatalysts target perchlorate even in the
89 presence of excess nitrate and have no activity with sulfate, reducing the amount of electron
90 donor that would be required to treat perchlorate in the presence of competing anions.²³
91 Furthermore, because the biocatalysts are non-living, the process can operate under nutrient

92 limited conditions, avoiding formation of hydrogen sulfide, mitigating any hazard posed by
93 pathogenic organisms, and minimizing the formation of biofilms. In addition, these biocatalysts
94 showed good stability, maintaining perchlorate reduction up to 23 days.²³ While promising, this
95 initial proof-of-concept study did not determine kinetic parameters for perchlorate reduction. It
96 was further limited by its exclusive use of buffered laboratory solutions and ideal electron
97 donors.

98 To better understand the potential advantages and limitations of the biocatalytic system
99 for perchlorate removal, this work measured the biocatalysts' kinetic activities in two real world
100 groundwater samples and laboratory buffered conditions. The effects of temperature, pH, natural
101 organic matter (NOM), calcium, and magnesium were specifically investigated, and a variety of
102 potential electron donors were tested. The results provide a basis for evaluating the practical
103 potential for biocatalytic removal of perchlorate during drinking water treatment.

104 **2. Materials and Methods**

105 **2.1 Biocatalyst Preparation, Media, and Chemicals.**

106 Biocatalysts were obtained from the perchlorate-reducing *A. oryzae* strain PS (ATCC
107 number BAA-33). The anaerobic growth media was as previously described,²³ with 14.7 mM
108 acetate as electron donor and 7 mM perchlorate as electron acceptor. Preparation of *A. oryzae*
109 soluble protein fraction containing PR and CD was also as previously described, including
110 addition of glycerol to a final concentration of 10% before storage.²³

111 To normalize activity across different preparations, two measurements were used:
112 molybdenum content, as an indirect measure of PR concentration, and total protein. To determine
113 molybdenum content, aliquots of each soluble protein fraction were taken prior to addition of
114 glycerol and dialyzed to remove salts and free molybdenum using 3,000 Dalton molecular

115 weight cut off dialysis cassettes (Thermo Scientific) with three 50mM phosphate buffer
116 exchanges. Original volume of sample was maintained. Samples were analyzed with inductively
117 coupled plasma-optical emission spectrometry (ICP-OES) (PerkinElmer Optima 2000DV,
118 Waltham, MA). To facilitate comparison to the literature, activity was also normalized to total
119 protein concentrations in the soluble protein fractions, as determined using the Bicinchoninic
120 acid (BCA) assay (Pierce, Rockford, IL). Soluble protein fractions produced in this work
121 contained an average of 21.22 ± 1.76 mg mL⁻¹ protein and 357 ± 39 μ g L⁻¹ molybdenum.

122 All solutions were prepared with Nanopure water (18 M Ω cm), produced from deionized
123 water in an EMD Millipore Milli-Q (Model Number: Z00QSV0US) System (Billerica, MA).
124 Unless otherwise specified, chemicals were purchased from Fisher Scientific (Pittsburgh, PA).
125 Anaerobic solutions were prepared by degassing with N₂:CO₂ for 30 minutes, and headspace was
126 degassed with the same mixture for 5 minutes. The ratio of N₂:CO₂ was varied in the range of
127 80:20 to 100:0 to maintain the desired pH.

128 **2.2 Groundwater Sampling and Characterization**

129 Groundwater was collected from two sources. The Illinois groundwater (Illinois GW)
130 was harvested from a depth of 46.3 meters in the Illinoisian Formation above the Mahomet
131 Aquifer. This water was known to have high amounts of iron and manganese and was therefore
132 pretreated in a manganese greensand filter. Water was also collected in Eastern Iowa (Iowa GW),
133 from a depth of 151 meters in the Silurian-Devonian Aquifer, without pretreatment. Five gallon
134 samples were collected and stored in polypropylene jerricans in the dark at 4°C.

135 The groundwater samples were characterized after equilibration with the atmosphere and,
136 for the Illinois sample, after pretreatment, corresponding to the expected placement of the
137 biocatalysts in the treatment train for drinking water prior to disinfection. Oxygen concentration

138 was measured using a rugged dissolved oxygen (RDO) probe (Thermo Scientific, 087020MD).
139 pH was measured using a Thermo Orion 8172 BN ROSS Sure-Flow pH electrode. Bicarbonate
140 concentration was estimated from alkalinity pH titration measurement using 0.1, 0.01 and 0.001
141 M HCl. Hardness was tested by titration (Hach Total Hardness Kit, HA-71A). Selected metals
142 were analyzed with inductively coupled plasma-optical emission spectrometry (ICP-OES)
143 (PerkinElmer Optima 2000DV). Total ammonia (NH_3/NH_4 mg L⁻¹ NH-N) was analyzed by
144 colorimetric analysis (Hach salicylate kit). Halides were measured using Thermo Scientific Ion
145 Selective Electrodes. Perchlorate was quantified using ion chromatography (IC) with
146 conductivity detection (IC-CD; Dionex ICS-2000) on an Ion Pac AG-16 and AS-16,³⁰ and
147 nitrate, sulfate, chlorate and chlorite were analyzed on an Ion Pac AG-18 and AS-18 Hydroxide-
148 Selective Anion Exchange Column as previously described.²³

149 **2.3 Colorimetric Biocatalytic Activity Assays**

150 Biocatalytic activities were analyzed using a standard colorimetric assay for perchlorate
151 reduction, which uses methyl viologen (MV) as an electron donor.²⁴ As previously described,²³
152 the assays were performed in stoppered anaerobic cuvettes (Absorption Cells 117.104, Hellma
153 USA, Inc., Plainview, NY) at room temperature. In brief, the methyl viologen was first reduced
154 with sodium dithionite, twenty μL soluble protein fraction was added and monitored until the
155 absorbance (578 nm) slope stabilized, and then electron acceptor (perchlorate, chlorate, nitrate,
156 sulfate, or anion combinations as specified) was added and the reaction was followed by
157 absorbance measurements. The background activity of the soluble protein fraction (measured
158 without electron acceptor) was subtracted. An extinction coefficient of 13.1 mM⁻¹ cm⁻¹ was
159 used.³¹ Units (U) represent one μmole of MV oxidized per minute. Because MV donates
160 electrons for perchlorate reduction and can also react with the oxygen that is produced, up to

161 eight moles of MV could be oxidized per mole of perchlorate reduced to chloride. Activity
162 measurements were performed in triplicate from independent growths (biological replicates) and
163 reported with standard deviation. Data was fit to the single substrate Michaelis-Menten Kinetic
164 equation:

$$165 \quad v = V_{\max} * [S] / (K_m + [S])$$

166 where v is the activity of the biocatalysts at a given substrate concentration, V_{\max} is the maximum
167 activity for the biocatalysts, S is the substrate concentration and K_m is the substrate concentration
168 at half V_{\max} . Kinetic parameters, V_{\max} and K_m , reported with standard error were calculated using
169 the Marquardt-Levenberg algorithm in the Enzyme Kinetic Module in SigmaPlot 13 from
170 triplicate biological replicates.

171 Using the MV assay, biocatalytic activity was tested over a range of conditions. The pH
172 was varied from 6 – 9 in increments of 0.5 in assays conducted with 1mM perchlorate and Iowa
173 GW. Iowa GW pH was adjusted with hydrochloric acid or sodium hydroxide prior to degassing.
174 pH was maintained during the degassing process by determined ratios of carbon dioxide and
175 nitrogen.

176 Biocatalytic activity was also determined over a temperature range from 5°C to 30°C in
177 increments of 5°C, again using the MV assay, 1mM perchlorate, and Iowa GW. Temperature was
178 controlled by putting the spectrophotometer (Thermo Scientific Genesys 20) in an incubator
179 (Thermo Scientific MaxQ 6000). Solutions were allowed to equilibrate to the specified
180 temperature before measurement. The data was fit to the Arrhenius' equation shown:

$$181 \quad k = A e^{-E_a/(RT)}$$

182 where k is the rate constant, A is the pre-exponential factor, E_a is the activation energy, R is the
183 universal gas constant and T is the temperature.

184 The effects of calcium, magnesium, and NOM were determined in 50mM Tris Cl⁻ (pH
185 7.5) buffered conditions. Calcium chloride and magnesium chloride were tested individually at
186 concentrations up to 400mg L⁻¹. Suwanee River NOM (IHSS, St. Paul, MN) was tested from 1 to
187 6 mg L⁻¹.

188 **2.4 Alternative Electron Donors**

189 To characterize the range of electron donors that can be used by the biocatalysts, a variety
190 of organic electron donors were tested in buffered solutions. Based on previous work with
191 NADH,³² each of these potential donors was tested with and without the electron shuttle 5-
192 methylphenazinium methyl sulfate (PMS) (Acros Organics, New Jersey). Twenty μ L of soluble
193 protein fraction were incubated in 10 mL samples containing 5mM electron donor, 0 or 100 μ M
194 PMS, and 1 mM perchlorate. Initial assays were incubated on the benchtop (approximately
195 22°C) for 24 hours and then frozen at -80°C to halt enzyme activity. Perchlorate removal was
196 monitored by IC as detailed in section 2.2. Controls included no soluble protein fraction and no
197 perchlorate samples for each reaction mixture. The initial reaction rate was quantified for one
198 promising candidate, ascorbic acid, by scaling the reaction up to 100mL with 1mL of soluble
199 protein fraction in stoppered anaerobic media bottles and withdrawing 3mL samples hourly for
200 perchlorate measurements.

201 **2.5 Preliminary Design Calculations**

202 Initial calculations for perchlorate treatment in a batch reactor system were determined
203 using an influent perchlorate concentration of 100 μ g/L and an effluent concentration of 10 μ g/L.
204 The reactor was modeled using an integrated form of the Michaelis-Menten equation and a
205 hydraulic retention time (HRT) of two hours. For initial calculations, nitrate was not included as
206 an inhibitory effect.

207 **2.6 Statistical Analysis**

208 The assumption of equal variance was tested using F-test. Statistical analysis was
209 performed using the independent-samples t-test with equal variance. Samples were considered
210 significantly different with an alpha of less than 0.05.

211 **3. Results**

212 **3.1 Characterization of Groundwater**

213 The two groundwater samples were similar in composition (Table 1). The hardness and
214 alkalinity measurements are characteristic of very hard water in the United States.³³ The
215 alkalinity of the samples nevertheless represents a decrease in buffering capacity as compared to
216 the laboratory buffered system. Other than hardness, the groundwater characteristics were within
217 typical ranges (Table 1). No perchlorate, chlorate or nitrate were detected, and the levels of
218 sulfate were below the EPA regulatory and advisory limits.³⁴

219 **3.2 Biocatalytic Activity in Groundwater**

220 To determine activities of the biocatalysts at realistic perchlorate concentrations and in
221 groundwater, the soluble protein fractions were assayed in real groundwater over a range of
222 perchlorate concentrations. Although the biocatalysts were not purified, throughout this work the
223 measured activity is attributed to PR and CD. This assumption is supported by the high
224 expression of PR in *A. oryzae* cells grown on perchlorate²⁴ and by the unique activity of CD. It is
225 however possible that some of the measured activity was due to a nitrate reductase, which can
226 also show activity for perchlorate.²⁴ To account for variation in biocatalyst content across
227 different preparations, activities were normalized to molybdenum concentration, because subunit
228 A of PR has one molecule of molybdenum.²⁴ The biocatalysts showed good activity in
229 groundwater (Fig. 1), maintaining 82% (Illinois GW) and 94% (Iowa GW) of their activity in

230 laboratory solutions. To facilitate comparison to previously published results,^{23, 24} the
231 biocatalysts' activity was also normalized to total protein content. The activity values were 2.49
232 ± 0.22 U mg total protein⁻¹ in buffer, 2.22 ± 0.38 U mg total protein⁻¹ in the Illinois GW, and
233 2.28 ± 0.12 U mg total protein⁻¹ in Iowa GW. The background activity in groundwater was less
234 than 0.1% of the maximum perchlorate reducing rates. The maximum reaction rates (V_{\max}) and
235 half saturation constants (K_m) of the soluble protein fractions were calculated using the single
236 substrate form of Michaelis Menten kinetic equation (Table 2). Kinetic values for Illinois GW
237 and Iowa GW were not statistically different from buffer.

238 When chlorate was supplied instead of perchlorate, the maximum activity was higher
239 (658.3 ± 36.8 U ($\mu\text{g Mo}$)⁻¹ versus 152.4 ± 6.3 U ($\mu\text{g Mo}$)⁻¹), and the half saturation constant was
240 lower (50 ± 12 μM versus 105 ± 16 μM) in Iowa GW. This suggests the system will also be
241 effective for chlorate remediation and that chlorate will not accumulate during perchlorate
242 removal. The activity with chlorite could not be tested in this assay because it reacts with MV.

243 Because a key advantage of the biocatalytic system is the specificity it exhibits for
244 perchlorate,²³ the specificity was confirmed in groundwater. Assays with 1mM nitrate as the sole
245 electron acceptor showed slow reduction, with rates only $9.7 \pm 0.4\%$ of perchlorate reduction
246 rates in Iowa GW and $7.5 \pm 2.3\%$ in Illinois GW. These results are slightly better than previous
247 results in a buffered system, where nitrate had $24.9 \pm 3.6\%$ of perchlorate activity.²³ Nitrate
248 activity could be due to the presence of a putative nitrate reductase³⁵ in the soluble protein
249 fractions or to the similarity between PR and nitrate reductase.³⁶ Simultaneous addition of 1 mM
250 nitrate and 1 mM perchlorate lowered the observed reduction rates to $72.1 \pm 1.1\%$ of perchlorate
251 reduction rates in Iowa GW and $71.8 \pm 3.2\%$ in Illinois GW. This rate is difficult to interpret,
252 since the colorimetric response could come from either electron acceptor. However, by

253 quantifying perchlorate in endpoint assays, prior work demonstrated that the biocatalysts showed
254 good perchlorate removal even in the presence of 100-fold excess nitrate.²³ There was no
255 observed sulfate activity in either groundwater or in previous work.²³

256 3.3. Effects of Groundwater Characteristics on Activity

257 In addition to rapid and selective perchlorate reduction in real world waters, application
258 of biocatalysts requires an understanding of their response to common variables. Several
259 important factors: pH, temperature, calcium, magnesium, and NOM, were tested here for their
260 impact on the perchlorate reducing activities of the biocatalysts. pH and temperature were tested
261 in Iowa GW, while calcium, magnesium, and NOM were tested in buffered conditions.

262 Over the pH range tested here (6.0-9.0), the biocatalysts showed robust perchlorate
263 reduction (Fig. 2). Activity decreased only at pH 6.0, with a 48% loss of activity, but even at pH
264 6.0, the values were not significantly different ($P=0.10$) from pH 7.0. A stronger response to
265 temperature was observed, with a gradual decrease in activity as temperature decreased,
266 culminating in a 68% decrease in activity when comparing activity at 10°C to 25°C. Using the
267 Arrhenius equation, the activation energy of the biocatalysts was 45.6 kJ mole⁻¹, and the pre-
268 exponential factor was $\ln(21.6) \text{ s}^{-1}$. Data fit the equation with a coefficient of determination of
269 .970 (Fig 3).

270 No statistically significant differences in biocatalyst activity were observed over calcium
271 and magnesium concentrations from 0 to 400 m L⁻¹, although a slight decreasing trend might be
272 occurring for calcium (Fig. 4), culminating with a drop in activity of 24.2%. Suwanee River
273 NOM also had no statistically significant impact on perchlorate reducing activity over the range
274 from 1-6 mg L⁻¹ of NOM tested (Fig. 4). Slight differences in the zero-point reference activities
275 are due to fluctuations in room temperature.

276 3.4. Alternative Electron Donors

277 Previous studies on perchlorate reduction have used either MV or NADH/PMS as
278 electron donors (e.g. ^{23, 24, 32}). However, these compounds are relatively expensive. MV and PMS
279 are also oxygen-sensitive. We therefore tested a variety of alternative organic electron donors:
280 sodium acetate, ascorbic acid, citric acid, ethanol, formic acid, and sodium pyruvate. The
281 electron donors tested in this study are common metabolites. In conditions without an additional
282 electron shuttle, there was no detectable perchlorate removal.

283 However, with the addition of 100 μ M PMS as an electron shuttle, the results were more
284 promising. Ascorbic acid showed the most potential to act as an electron donor for the
285 perchlorate reducing enzymes, achieving a statistically significant $32.0 \pm 15.7\%$ decrease as
286 compared to the initial concentration of perchlorate ($P=.028$). With formic acid $14.3 \pm 9.7\%$ of
287 the perchlorate was reduced as compared to the initial perchlorate concentration; however, the
288 results were not statistically significant ($P=0.086$). Citric acid and pyruvate also were able to
289 reduce perchlorate; however, these results were inconsistent across replicates, perhaps due to the
290 involvement of an additional component from the soluble protein fraction. No perchlorate
291 reduction was detected with acetate or ethanol. No perchlorate reduction was observed in
292 controls without biocatalysts.

293 As ascorbic acid with PMS demonstrated the most promise for perchlorate reduction, the
294 rate of perchlorate reduction was tested for this system. Robust perchlorate reduction was
295 observed, with $52.3 \pm 8.4\%$ perchlorate reduced within the first hour (Fig. 5). This initial
296 perchlorate reduction rate corresponds to 2.2 μ mol perchlorate reduced per min per μ g of
297 molybdenum. For comparison to MV assay results, assuming the methyl viologen reaction
298 consumes 8 electrons for each perchlorate molecule, the perchlorate reduction rate for methyl

299 viologen at 1mM perchlorate would be $19.6 \mu\text{mol min}^{-1} \mu\text{g}^{-1}$. Using ascorbic acid with PMS as
300 an electron donor system therefore results in approximately an order of magnitude loss in
301 activity. After six hours, over 99% of the perchlorate had been reduced.

302 4. Discussion

303 This work demonstrates the activity of the perchlorate-reducing biocatalysts under
304 application-appropriate conditions. Activities in real groundwater were only slightly lower than
305 in laboratory buffered solutions, comparing to buffered values measured here and in previous
306 reports.^{23, 32} Considering a broader range of typical groundwater conditions, the activity was
307 relatively insensitive to pH, hardness, and NOM, and showed a gradual decrease with decreasing
308 temperature. Substitution of ascorbic acid and electron shuttle PMS for MV resulted in
309 approximately an order of magnitude drop in activity. Here we discuss these findings in the
310 context of the literature and describe their implications for process design.

311 The half saturation constants measured here (91-105 μM) were within the range of
312 reported values for PR and perchlorate, which span a bacterial consortium reported at $0.28 \mu\text{M}$ ¹³
313 to $4700 \mu\text{M}$ for *Dechlorosoma* sp KJ with the electron donor acetate.³⁷ They are higher than that
314 published for purified PR from another *A. oryzae* strain, GR-1, which was $27 \mu\text{M}$ K_m for
315 perchlorate.²⁴ This discrepancy could reflect differences in the PR encoded by these two strains,
316 or it could be due to our use of soluble protein fractions rather than purified protein. Another
317 component in the soluble protein fractions could cause some type of interference or competition
318 that raises the apparent K_m . If the affinity for perchlorate becomes a limiting factor for
319 technology development, it should be possible to improve it by removing interfering factors
320 and/or using a higher-affinity homolog.

321 The effects of groundwater characteristics reported here are generally consistent with the
322 limited information available in prior publications. Our soluble protein fraction has shown
323 perchlorate reducing activity as low as 5°C, with the highest activity at the highest temperature
324 tested, 30°C. Purified PR from strain perclace has perchlorate reducing activity in the range of
325 20 to 40°C with optimal activity at 25 to 35°C.³⁸ To our knowledge, no prior reports of activation
326 energy for PR or CD exist, but a related enzyme, nitrate reductase, has activation energies of 41-
327 42 kJ mol⁻¹,^{39,40} very similar to the value of 45.6 kJ mol⁻¹ reported here for perchlorate reduction.
328 Work with strain perclace showed consistent PR activity over a pH range from 7.0 to 9.0, in
329 agreement with our results.³⁸ For strain GR-1, optimal CD activity is achieved at a pH of 6.0 and
330 drops precipitously below 6.0.²⁵ A direct comparison of our results with these CD results is,
331 however, not possible, because the colorimetric assay used in our experiments measures the
332 combined effects of PR and CD. To our knowledge, the effects of magnesium, calcium, and
333 NOM on perchlorate reduction have not been previously studied.

334 The electron donors tested in this study were selected based on their occurrence in
335 bacterial metabolism, which was anticipated to increase the likelihood of successful interaction
336 with PR. However, these common electron donors were unable to donate electrons directly for
337 perchlorate reduction; the addition of a shuttle was required. While the biocatalysts are able to
338 reduce perchlorate in the presence of oxygen, at this point, the known options for supplying
339 reducing power (MV or a shuttle with NADH or ascorbic acid) for biocatalytic perchlorate
340 reduction all involve an oxygen-sensitive component. Biocatalytic treatment of perchlorate for
341 drinking water therefore would require anaerobic operation of the system. Alternatively,
342 development of an oxygen-stable electron donor or shuttle would provide a broader range of
343 potential operational conditions.

344 In comparison to ligand-enhanced rhenium complex/palladium catalysts under
345 development for perchlorate reduction,⁴¹ the biocatalysts show much higher activity. To
346 correspond as nearly as possible to the chemical convention of normalizing to active site, we
347 used the Mo-normalized values for the biocatalysts. Comparing perchlorate reduction rates at 1
348 mM initial perchlorate, these chemical catalysts reduced 0.317 mmol perchlorate min⁻¹ (mmol
349 Rh)⁻¹, compared to the biocatalysts' rate of 1900 mmol min⁻¹ (mmol Mo)⁻¹. This represents a
350 6000 fold higher activity for the biocatalysts. Another option is to compare the k_{cat} for the
351 biocatalysts (1716 min⁻¹) to these chemical catalysts' k_{obs} value of 0.0415 min⁻¹ value: a 41,000
352 fold larger turnover number for the biocatalysts. For large-scale application, the biocatalysts'
353 activity at neutral pH is also a significant advantage, as the chemical catalysts' activities were
354 reported at pH 3, where they are most active.

355 Considering the implications of the kinetics reported here for practical application of the
356 biocatalysts, the best available basis for comparison is a recent life cycle analysis (LCA) of
357 perchlorate treatment options. For traditional rhenium/palladium catalysts, this LCA projected
358 that a 20-fold increase in activity was required for the technology to be competitive versus ion
359 exchange and biological reduction.^{42, 43} Considering that the ligand-enhanced catalysts used as a
360 comparison here already represent an approximately 140-fold increase in activity over the values
361 used in the LCA,⁴¹ and that the biocatalytic activities reported in this work are orders of
362 magnitude higher than the enhanced catalysts, suggests that a biocatalytic process will be
363 competitive with existing technologies. However, a comprehensive evaluation of the costs and
364 environmental impacts of the biocatalysts is needed to guide continued progress towards
365 application. The results presented here provide a solid basis for conducting such an evaluation.

366 This work also provides a basis for preliminary design calculations. For treatment of
367 groundwater-sourced drinking water, in their current soluble form, the biocatalysts could be
368 applied in batch reactors. Based on the kinetic results, a batch reactor operating at 25°C and an
369 average HRT of 2 hours would require a dosing rate of 0.1 µg molybdenum equivalence of
370 biocatalyst for each liter of water treated. This dosage corresponds to 280 µL of biocatalysts for
371 each liter of water treated. If the pH were at or below pH 6.5, the dosage would be 0.15 µg
372 molybdenum equivalence of biocatalyst each liter of water treated. Operating at 5°C would
373 require dosing rates of 0.38 µg molybdenum equivalence of biocatalyst each liter of water
374 treated. From prior applications of enzymes industrially, there are also a variety of methods for
375 immobilizing enzymes, which could be applied to PR and CD to reduce the dosage, costs and
376 environmental impacts. Finally, it is important to note that while molybdenum is an essential
377 trace element, it can also contribute to copper deficiency and cause toxic effects at high levels of
378 consumption. However, even if all of the molybdenum was released from PR, these dosage
379 values are approximately two orders of magnitude lower than the reference dose limits for
380 molybdenum of 5 µg kg⁻¹ day⁻¹ recommended by the US EPA.⁴⁴

381 5. Conclusions

382 This work demonstrates the potential of biocatalysts for perchlorate reduction in drinking
383 water treatment. The biocatalysts showed effective perchlorate reduction over a perchlorate
384 range from 0.5µM to 1 mM, representing perchlorate contamination found in municipal drinking
385 water to industrial/military industrial sites, in real groundwater and under typical ranges of
386 groundwater characteristics. Preliminary design calculations suggest that perchlorate could be
387 removed to concentrations less than the likely EPA regulation limit of 15 ppb with hydraulic

388 retention times of 2 hours, supporting its practical potential, although a detailed economic and
389 environmental assessment is still needed.

390 The biocatalysts have advantages compared to traditional treatment technologies. As
391 compared to the industry standard of ion exchange, the biocatalysts completely reduce
392 perchlorate to innocuous chloride and oxygen and show minimal interference from competing
393 anions nitrate and sulfate. In comparison to whole-cell based biological perchlorate remediation,
394 the biocatalysts have a lower demand for electron donor, because they show specificity for
395 perchlorate over nitrate. Because the biocatalysts are non-living, they should pose lower risk and
396 be more widely accepted for use in drinking water treatment.

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403

Table 1 - Constituent Values for Groundwater Samples from Illinois and Iowa GW.

| Component | Units | Illinois GW | Iowa GW | MCL ^a or NSDWR ^b | Typical Values ^c |
|-------------|---|-----------------|---------|--|-----------------------------|
| pH | | 7.34 | 7.19 | 6.5-8.5 ^b | 6.0-8.5 |
| Alkalinity | mg L ⁻¹ as HCO ₃ ⁻ | 393.0 | 378.9 | -- | -- |
| Hardness | mg L ⁻¹ of CaCO ₃ | 342.0 | 376.2 | -- | 121-180 |
| Ca | ppm | 66.8 | 70.5 | -- | >15 |
| Fe | ppb | 0.5 | 480 | 300 ^b | <10,000 |
| K | ppm | 1.62 | 0.78 | -- | <10 |
| Mg | ppm | 26.9 | 28.5 | -- | <300 |
| Mn | ppb | 68 | 37 | 50 ^b | <200 |
| Mo | ppm | 0 | 0 | 0.03-1 | -- |
| Na | ppm | 26.2 | 12.08 | 0.2 | <1000 |
| P | ppm | 0.16 | 0.13 | -- | -- |
| S | ppm | 1.24 | 1.03 | -- | -- |
| Ammonia | mg L ⁻¹ NH ₃ -N | <0.4 | <0.4 | | |
| Fluoride | ppm | 0 | 0 | 4 ^a /2 ^b | <10 |
| Chloride | ppm | 61 | 52 | 250 ^b | <10 |
| Bromide | ppm | 2 | 0 | -- | -- |
| Iodide | ppm | 0 | 0 | -- | -- |
| Perchlorate | ppm | ND ^d | ND | -- | -- |
| Chlorate | ppm | ND | ND | -- | -- |
| Chlorite | ppm | ND | ND | 1.0 | -- |
| Nitrate | ppm | ND | ND | 44 ^a | <50 |
| Sulfate | ppm | 9.5 | 9.7 | 250 ^b | <1000 |
| TOC | ppm | 1.74 | 1.22 | -- | 0.1 - 6 |
| Temperature | °C | | | -- | 2.78 – 25 ^e |
| DO | mg L ⁻¹ | 9.66 | 10.06 | -- | -- |

^a Maximum Contaminant Level ³⁴

^b National Secondary Drinking Water Regulations ³⁴

^c ³³

^d ND – Not Detected, Detection Limits NO₃⁻ (10ppb), ClO₃⁻ (10ppb), ClO₄⁻ (5ppb)

^e Temperatures were determined for near surface groundwater from mean annual temperature.

Table 2. Kinetic parameters of perchlorate reducing biocatalytic system in buffered and groundwater sample matrices.

| Component | Illinois GW | Iowa GW | Buffer System |
|--|---------------|---------------|---------------|
| Maximum Velocity ^a (V _{max}) (U (μg Mo) ⁻¹) ^b | 132.9 ± 9.8 | 152.4 ± 6.3 | 162.5 ± 8.4 |
| Half Saturation Constant ^a (K _m) (mM) | 0.091 ± 0.026 | 0.105 ± 0.016 | 0.092 ± 0.019 |

405 ^a average ± standard error

406 ^b Units (U) are defined as 1 μmol MV oxidized per minute and are normalized to molybdenum as an indirect measure of PR
 407 concentration.

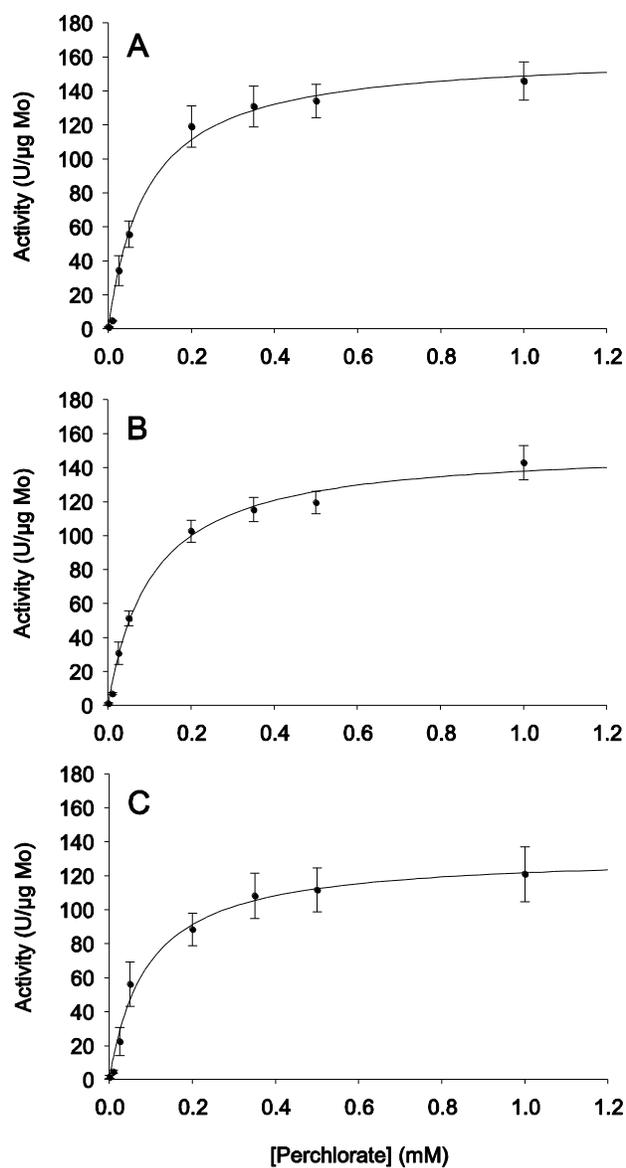


Fig. 1. Biocatalytic perchlorate reduction in buffered systems (a) and groundwater (b, Iowa GW; c, Illinois GW). Results of MV activity assays conducted on triplicate independent soluble protein fractions at perchlorate concentrations from .0005 – 1 mM. Activity is given in Units (U), defined as 1 μmol MV oxidized per minute, and are normalized to molybdenum as an indirect measure of PR concentration. Solid line represents Michaelis-Menten Kinetics model. Error bars represent Standard Error.

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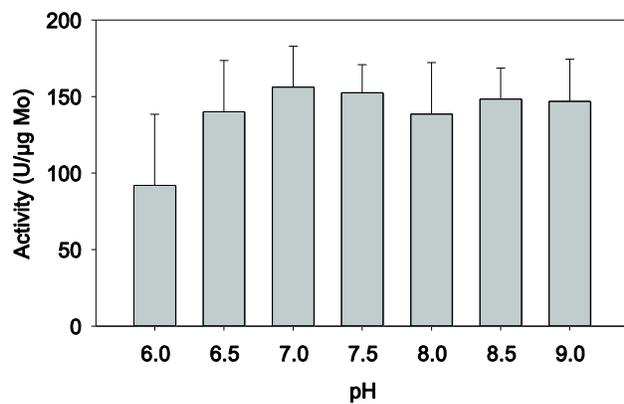


Fig 2. Effect of pH on biocatalytic perchlorate reduction. Results of MV assays conducted in Iowa GW with 1mM perchlorate. Activity is given in Units (U), defined as 1 μmol MV oxidized per minute, and are normalized to molybdenum as an indirect measure of PR concentration. Average and standard deviation of triplicate independent soluble protein fractions are presented.

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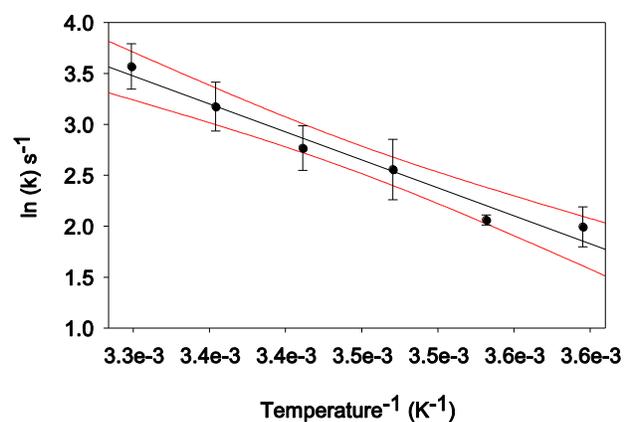


Fig 3 – Effect of temperature on biocatalytic perchlorate reduction. Results of MV assays conducted in Iowa GW with 1mM perchlorate at specified temperature. Average and standard deviation of triplicate independent soluble protein fractions are presented. Black line indicates Arrhenius equation fit, and red lines indicate 95% confidence interval.

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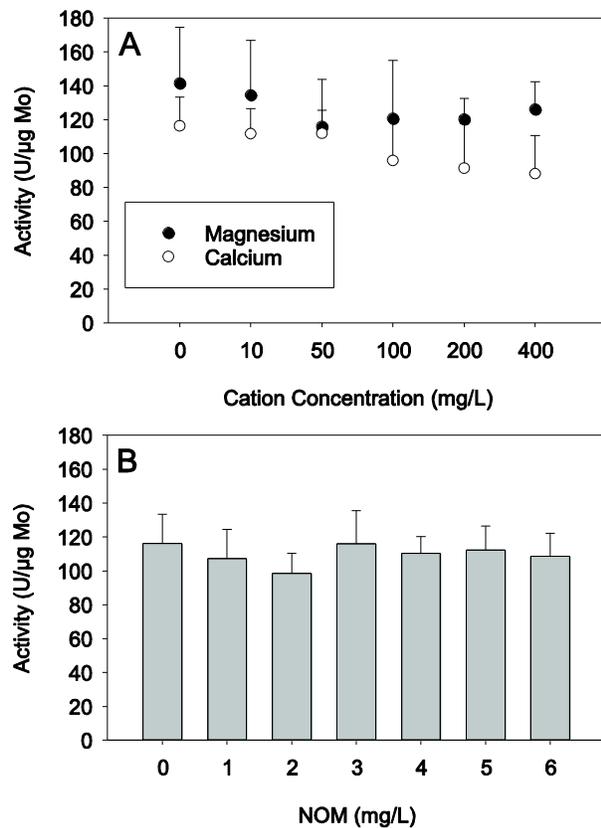


Fig 4. Effect of calcium and magnesium (a) and NOM (b) on biocatalytic perchlorate reduction. Results of MV assays conducted in buffered system with 1 mM perchlorate. Activity is given in Units (U), defined as 1 μmol MV oxidized per minute, and are normalized to molybdenum as an indirect measure of PR concentration. Average and standard deviation of triplicate independent soluble protein fractions are presented.

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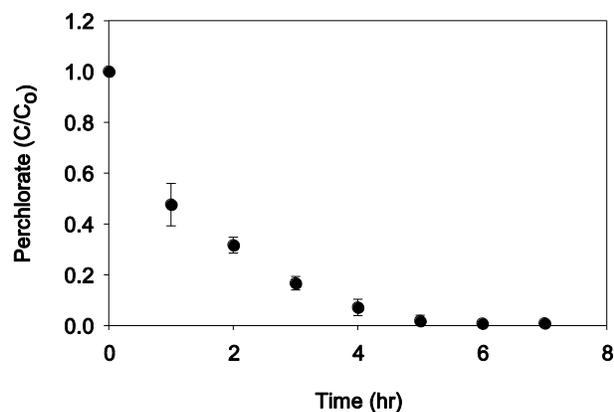


Fig 5. Biocatalytic perchlorate reduction with ascorbic acid and PMS. Reactions were conducted in buffer with an initial concentration of 1 mM perchlorate, and reaction progress was monitored by quantification of perchlorate. Average and standard deviation of triplicate independent soluble protein fractions are presented.

412

- 413 1. *Perchlorate Treatment Technology Update* U.S. Environmental Protection Agency, 542-R-
414 05-015, Washington, D.C., 2005,
- 415 2. *Drinking Water: Preliminary Regulatory Determination on Perchlorate*, US Environmental
416 Protection Agency, Federal Register 73 FR 60262, 2008, 60262-60282
- 417 3. *EPA Seeks Advice on Perchlorate in Drinking Water - Agency Issues Interim Health*
418 *Advisory*, US Environmental Protection Agency, EPA-HQ-OW-2009-0297-0675,
419 Washington, D.C., 2009,
- 420 4. R. J. Brechner, G. D. Parkhurst, W. O. Humble, M. B. Brown and W. H. Herman, *J. Occup.*
421 *Environ. Med.*, 2000, **42**, 777-782.
- 422 5. M. A. Greer, G. Goodman, R. C. Pleus and S. E. Greer, *Environ. Health Perspect.*, 2002,
423 **110**, 927-937.
- 424 6. T. Zewdie, C. M. Smith, M. Hutcheson and C. R. West, *Environ. Health Perspect.*, 2010,
425 **118**, 42-48.
- 426 7. A. R. Tripp and D. A. Clifford, *J. Am. Water Works Assoc.*, 2006, **98**, 105-114.
- 427 8. B. H. Gu, G. M. Brown and C. C. Chiang, *Environ. Sci. Technol.*, 2007, **41**, 6277-6282.
- 428 9. J. C. Brown, R. D. Anderson, J. H. Min, L. Boulos, D. Prasifka and G. J. G. Juby, *J. Am.*
429 *Water Works Assoc.*, 2005, **97**, 70-81.
- 430 10. S. K. De Long, X. Li, S. Bae, J. C. Brown, L. Raskin, K. A. Kinney and M. J. Kirisits, *J.*
431 *Appl. Microbiol.*, 2012, **112**, 579-592.
- 432 11. C. S. Butler, P. Clauwaert, S. J. Green, W. Verstraete and R. Nerenberg, *Environ. Sci.*
433 *Technol.*, 2010, **44**, 4685-4691.
- 434 12. K. J. Martin and R. Nerenberg, *Bioresour. Technol.*, 2012, **122**, 83-94.
- 435 13. M. R. London, S. K. De Long, M. D. Strahota, L. E. Katz and G. E. Speitel Jr, *Water Res.*,
436 2011, **45**, 6593-6601.
- 437 14. J. C. Brown, V. L. Snoeyink, L. Raskin and R. Lin, *Water Res.*, 2003, **37**, 206-214.
- 438 15. S. G. Lehman, M. Badruzzaman, S. Adham, D. J. Roberts and D. A. Clifford, *Water Res.*,
439 2008, **42**, 969-976.
- 440 16. E. T. Urbansky, *Perchlorate in the Environment*, Kluwer Academic/ Plenum Publishers, New
441 York, 2000.
- 442 17. J. Liu, J. K. Choe, Z. Sasnow, C. J. Werth and T. J. Strathmann, *Water Res.*, 2013, **47**, 91-
443 101.
- 444 18. B. E. Logan, J. Wu and R. F. Unz, *Water Res.*, 2001, **35**, 3034-3038.

- 445 19. A. K. Venkatesan and J. R. Batista, *Biorem. J.*, 2011, **15**, 1-11.
- 446 20. M. Sharbatmaleki and J. R. Batista, *Water Res.*, 2012, **46**, 21-32.
- 447 21. C. T. Matos, S. Velizarov, J. G. Crespo and M. A. Reis, *Water Res.*, 2006, **40**, 231-240.
- 448 22. A. Ontiveros-Valencia, Y. Tang, R. Krajmalnik-Brown and B. E. Rittmann, *Water Res.*,
449 2014, **55**, 215-224.
- 450 23. J. M. Hutchison, S. K. Poust, M. Kumar, D. M. Cropek, I. E. MacAllister, C. M. Arnett and
451 J. L. Zilles, *Environ. Sci. Technol.*, 2013, **47**, 9934-9941.
- 452 24. S. W. Kengen, G. B. Rikken, W. R. Hagen, C. G. van Ginkel and A. J. Stams, *J. Bacteriol.*,
453 1999, **181**, 6706-6711.
- 454 25. C. G. van Ginkel, G. B. Rikken, A. G. M. Kroon and S. W. M. Kengen, *Arch. Microbiol.*,
455 1996, **166**, 321-326.
- 456 26. A. J. J. Straathof, S. Panke and A. Schmid, *Curr. Opin. Biotechnol.*, 2002, **13**, 548-556.
- 457 27. P. Widsten and A. Kandelbauer, *Enzyme Microb. Technol.*, 2008, **42**, 293-307.
- 458 28. D. T. D'Souza, R. Tiwari, A. K. Sah and C. Raghukumar, *Enzyme Microb. Technol.*, 2006,
459 **38**, 504-511.
- 460 29. S. Ba, A. Arsenault, T. Hassani, J. P. Jones and H. Cabana, *Crit. Rev. Biotechnol.*, 2013, **33**,
461 404-418.
- 462 30. D. Shuai, B. P. Chaplin, J. R. Shapley, N. P. Menendez, D. C. McCalman, W. F. Schneider
463 and C. J. Werth, *Environ. Sci. Technol.*, 2010, **44**, 1773-1779.
- 464 31. R. N. F. Thorneley, *Biochim. Biophys. Acta: Bioenergetics*, 1974, **333**, 487-496.
- 465 32. M. Heinnickel, S. C. Smith, J. Koo, S. M. O'Connor and J. D. Coates, *Environ. Sci. Technol.*,
466 2011, **45**, 2958-2964.
- 467 33. American Water Works Association, *Groundwater*, American Water Works Association,
468 Denver, CO, 3 edn., 2003.
- 469 34. *Drinking Water Contaminants*, US Environmental Protection Agency, EPA 819-F-09-0004,
470 2009,
- 471 35. K. G. Byrne-Bailey and J. D. Coates, *J. Bacteriol.*, 2012, **194**, 2767-2768.
- 472 36. M. J. Oosterkamp, F. Mehboob, G. Schraa, C. M. Plugge and A. J. Stams, *Biochem. Soc.*
473 *Trans.*, 2011, **39**, 230-235.
- 474 37. B. E. Logan, H. Zhang, P. Mulvaney, M. G. Milner, I. M. Head and R. F. Unz, *Appl.*
475 *Environ. Microbiol.*, 2001, **67**, 2499-2506.

- 476 38. B. C. Okeke and W. T. Frankenberger, Jr., *Microbiol. Res.*, 2003, **158**, 337-344.
- 477 39. J. R. Mahan, T. D. Sherman and E. A. Funkhouser, *Plant and Cell Physiology*, 1988, **29**,
478 735-737.
- 479 40. B. Lledo, R. M. Martinez-Espinosa, F. C. Marhuenda-Egea and M. J. Bonete, *Biochim.*
480 *Biophys. Acta*, 2004, **1674**, 50-59.
- 481 41. J. Liu, J. K. Choe, Y. Wang, J. R. Shapley, C. J. Werth and T. J. Strathmann, *ACS Catalysis*,
482 2015, **5**, 511-522.
- 483 42. J. K. Choe, M. H. Mehnert, J. S. Guest, T. J. Strathmann and C. J. Werth, *Environ. Sci.*
484 *Technol.*, 2013, **47**, 4644-4652.
- 485 43. K. D. Hurley, Y. Zhang and J. R. Shapley, *J. Am. Chem. Soc.*, 2009, **131**, 14172-14173.
- 486 44. US Environmental Protection Agency, IRIS - Molybdenum,
487 <http://www.epa.gov/iris/subst/0425.htm#oralrfd>, (accessed March, 2015).
488
489