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## L-Lactide Polymerization Studied by <sup>1</sup>H NMR with **Diffusion Ordered Spectroscopy (DOSY). "One NMR Tube Experiment" Providing: Conversion, Polymer** Structure, $M_n$ and $M_w$ .

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L-lactide polymerization has been studied by "One NMR Tube Experiment". Traditional <sup>1</sup>H NMR, providing structure, conversion and number average molar mass  $(M_n)$ has been combined with Diffusion Ordered Spectroscopy (DOSY), yielding mass averaged molar mass  $(M_w)$ . Thus, complete kinetic experiment could be performed without sampling, in one NMR tube.

Diffusion Ordered Spectroscopy (DOSY) has been elaborated above fifty years ago and today every NMR spectrophotometer has capability to conduct DOSY experiments. DOSY gives the dependence of the intensity of the peak ascribed to the given nuclei on its diffusion coefficient (D) and magnetic field gradient.<sup>1</sup> The physical principle of DOSY has been explained clearly in literature and various aspects of experimental set-up have been discussed.<sup>2</sup> An exhaustive review of original papers devoted to the method and its applications in various areas of organic chemistry, including polymer chemistry, has also been published.<sup>5</sup> In polymer chemistry DOSY has mostly been used in determination of  $M_{\rm w}$ . This method has also been applied in our present work on L-lactide polymerization, to complement our kinetic work.

The detailed description of the theoretical bases of the method, eventually related to the Stokes-Einstein relation-ship (1) of the size of molecules and their diffusion coefficients has been given in several papers.6-9

$$D = \frac{Tk_B}{6\pi\eta R_H} \tag{1}$$

Where T is the absolute temperature,  $k_{\rm B}$  is the Boltzmann constant,  $\eta$  is viscosity of the medium, and  $R_{\rm H}$  is hydrodynamic radius of the studied molecule.

On the basis of the mean field theory molar mass M is related to  $R_{\rm H}$  and leads to the dependence of M on D according to the simple equation (2), resembling the Mark-Houwink-Sakurada equation.<sup>1</sup> (2)  $R_{\mu} = KM^{\nu}$ 

K is proportionality constant and v is scaling exponent.

Finally, the relation between M and diffusion coefficient has a relatively simple form (3). (3)

 $D = K'M^{-\nu}$ 

The K' and v coefficients have been determined for a few polymer-solvent systems.7,11-13

Recently Grubbs et al. in a paper entitled "Application of <sup>1</sup>H DOSY for Facile Measurement of Polymer Molecular Weights" applied DOSY for the first time in studies of controlled polymerization of styrene and of 1,5-cyclooctadiene (ROMP).<sup>13</sup> The conversion and mass average molar mass  $(M_w)$  data have been determined in the Grubbs' paper by sampling the reaction mixture.

We decided to follow the Grubbs' approach and study the L-lactide (LA) polymerization in this way, although in place of sampling the reaction mixture we performed polymerization in a sealed NMR tube, acquiring all the information "on-line" without taking samples. This was possible because the rate of the studied process is sufficiently slow at the measurement temperature, assuring that neither the measurements nor the polymerization were disturbed.

This work is divided into three parts. In the first one the dependence of diffusion coefficient on  $M_w$  for poly(L-Lactide) (PLA) is given. In the second this dependence is verified in a kinetic experiment with sampling the polymerization mixture. The third is devoted to the actual "One NMR Tube Kinetic Experiment".

All experimental details, analytical procedures, results of characterization of the synthesized samples are described in the Electronic Supplementary Information (ESI).

Five samples of PLA were prepared (polymerization with Sn(2ethylhexanoate)<sub>2</sub> (Sn(Oct)<sub>2</sub>)/benzyl alcohol (BzOH) catalytic system) and precipitated from the polymerization solution.  $M_{\rm w}$  were measured by SEC and D using DOSY. In addition, number average molar masses  $M_n$  were determined by <sup>1</sup>H NMR and SEC and compared with  $M_{\rm p}$  calculated from the conditions of polymerization. The tabulated (Table 1) data were used to determine the analytical dependence of D on  $M_w$  (Figure 1). Then the relative difference (called "error") between  $M_w$  determined by SEC and  $M_w$  calculated from D, using the established analytical dependence is given in the last column of Table 1.

id	$M_{\rm n}({ m th})^{ m a}$	${M_{\mathrm{n}}}^{\mathrm{b}}$	$M_{\rm n}^{\rm c}$	$M_{ m w}{}^{ m c}$	$D^{c}$	$10^{11} \cdot D^{d}$ (m <sup>2</sup> · s <sup>-1</sup> )	${M_{ m w}}^{ m d}$	error <sup>e</sup> (%)
А	3 200	4 000	4 100	4 200	1.03	20.301	4 207	-0.6
В	4 660	6 450	6 300	6 700	1.05	14.977	6 601	3.5
С	10 500	13 100	13 500	13 900	1.03	9.857	13 861	0.2
D	20 100	20 100	21 000	21 600	1.03	7.301	22 065	6.3
Е	29 700	30 100	31 000	33 700	1.09	5.838	33 056	-1.1

Table 1 Characteristics of PLA samples

As seen from the data collected in Table 1, the  $M_n$  determined by SEC with MALLS detector and from integrations of signals in the <sup>1</sup>H NMR spectra are consistent with the theoretical ones, based on the ratio 144.13x[LA]<sub>0</sub>/[BzOH]<sub>0</sub>. Differences noted for the calculated and measured smallest masses could be ascribed to the fractionation-removal of the lower mass molecules during precipitation of the crude samples. Low dispersities (D) (ranging from 1.03 to 1.09), indicate controlled behaviour of the applied polymerization process.

The DOSY spectra for PLA solutions were acquired according to the protocol used by Grubbs et al. (details given in ESI).<sup>13</sup> A novel ITAMeD algorithm and the Matlab® script provided recently by Urbańczyk et al. have been used for extraction of D values from attenuation decay curves.<sup>6</sup> Comparing with other methods, ITAMeD does not require any assumptions on composition of the analysed sample.

The NMR signal decay curves and obtained diffusion coefficient distributions are presented in the ESI. The numerical values of D and  $M_w$  are given in Table 1.



**Fig. 1** Weight-averaged molecular mass  $(M_w)$  vs. diffusion coefficient (*D*) log-log plot for PLA in benzene-d6.

In Figure 1 the dependence of the diffusion coefficients on the corresponding mass average molar masses is given. A straight line fits the experimental data with correlation coefficient  $r^{2}=0.9997$  and passes closely to points obtained for benzene and LA. The proportionality constant K' is equal to  $10^{-7.53(\pm0.03)}$  and value of the scaling exponent  $v = 0.598(\pm0.006)$ . The value of the scaling exponent indicates that benzene is a good solvent for PLA, as it was established earlier on the basis of viscosity measurements.<sup>14</sup> The *D* values extracted from DOSY spectra using the T1/T2 TopSpin module yield nearly identical result as the ITAMeD method:  $K'=10^{-7.53(\pm0.03)}$  and  $v = 0.597(\pm0.006)$  (cf. Figure S5 in ESI).

The  $M_{\rm w}$  values, calculated from analytical relationship (cf. Figure 1), were then compared with  $M_{\rm w}$  determined by SEC. The highest noticed difference was equal to 6.3 %.

Even though the established dependence is valid only for the polymer concentration of 0.5 g·l<sup>-1</sup>, after determining correction factors it has been successfully applied in studies of polymerization kinetics with changing concentration of the formed polymer. Polymer concentration's changes may also influence the diffusion coefficient by aggregation phenomena or simply by increasing solution viscosity. In order to correctly analyse the experimental data the dependence of *D* on polymer concentration (from 0.5 to 30 g·l<sup>-1</sup>) has been determined and plotted as in Figure 2.



Fig. 2 Dependence of the D on  $M_w$  and concentration of polymer. Open marks: data used for determining of plot slopes. Crosses: data used for confirmation of linearity of the concentration dependence. Stars illustrate a correction introduced by equation 4. Numbers indicate  $M_w$  of samples.

The dependencies are linear and slopes do not depend on molar masses. It follows that the mean value of the slope (S) is equal to  $(1.3\pm0.2)\cdot10^{-12} \text{ m}^2\cdot1 \text{ s}^{-1} \text{ snd}$  it is common for all molar masses within the studied range. Thus, the corrected value of the diffusion coefficient can be calculated from equation (4):  $D_{corr} = D_{ava} - S(C_{ava} - C_{corr})$  (4)

 $D_{corr} = D_{exp} - S(c_{exp} - c_{corr})$  (4) Where: *c* is concentration; indices "exp" and "corr" mean experimental and corrected value, respectively.

Finally the  $M_{\rm w}$  values were calculated from the  $D_{\rm corr}$  using equation given in Fig. 1.

After having established the dependence of D on  $M_w$  and polymer concentration, it had been necessary to verify the correctness of this relationship before performing the "One NMR

Journal Name

Tube Experiment". Therefore a kinetic experiment on L-lactide polymerization was first performed with sampling of the polymerization mixture (protocol and conditions of experiments are given in ESI). The determined molar masses are given in Table 2.

**Table 2**  $M_n$ ,  $M_w$ , D and D as determined by SEC, <sup>1</sup>H NMR and DOSY measurements in the kinetic experiment with sampling

id	$M_{\rm n}^{\ \rm a}$	$M_{ m w}{}^{ m a}$	$D^{\mathrm{a}}$	$M_{\rm n}^{\rm b}$	$M_{ m w}^{\  m c}$	$D^{\mathrm{d}}$	$10^{11} \cdot D^{c}$ (m <sup>2</sup> ·s <sup>-1</sup> )
1	6 500	6 800	1.03	6 800	6 780	1.00	1 5042
2	8 4 5 0	8 600	1.02	8 600	8 620	1.01	1 3048
3	9 400	9 700	1.04	9 800	10 100	1.03	1.1846
4	10 200	10 600	1.03	9 400	10 100	1.07	1.1840
<sup>a</sup> SEC with MALLS detection. <sup>b</sup> Integration of <sup>1</sup> H NMR spectra.							
<sup>c</sup> From DOSY. <sup>d</sup> $M_n$ ( <sup>1</sup> H NMR)/ $M_w$ (DOSY)							

Data collected in Table 2 (as well as Figure S8 in ESI) show, that for the dead macromolecules both the DOSY and SEC methods give almost identical  $M_n$  and  $M_w$ . This additionally indicate that the relationship between  $M_w$  and D has been correctly determined. Moreover,  $\mathcal{D}$  of polymer samples range from 1.00 to 1.07, as expected for chains formed in the controlled-living polymerization.



**Fig. 3** <sup>1</sup>H NMR 500 MHz spectrum of the living PLA in C<sub>6</sub>D<sub>6</sub> initiated by Sn(Oct)<sub>2</sub>/BzOH system. Temperature 353 K, reaction time 12 h,  $[LA]_0 = 0.226 \text{ mol}\cdot l^{-1}$ ,  $[BzOH]_0 = 2.99 \cdot 10^{-3} \text{ mol}\cdot l^{-1}$ ,  $[Sn(Oct)_2]_0/[BzOH]_0 \approx 1.0$ . Integrations (proton number): **d'** = 1.0, **e** = 134.0, monomer = 25.0.

Application of DOSY for studies of the polymerization kinetics of L-Lactide using the "One NMR Tube Experiment" approach is illustrated by polymerization conducted in sealed NMR tubes (experimental details are given in ESI). Polymerization mixture, containing  $C_6D_6$ , LA, and initiating-catalytic system  $Sn(Oct)_2/BZOH$ , was prepared and transferred into NMR tube under vacuum. The tube was then sealed-off and kept in a thermostat at 353 K. At predetermined time intervals the tube was cooled and <sup>1</sup>H NMR as well as DOSY spectra of the polymerizing mixture were acquired at 298 K. At this temperature, during the time of measurements (20 min), polymerization practically does not take place.

**Table 3** Conversion,  $P_n$ ,  $M_n$ , D,  $M_w$  and  $\overline{D}$  determined from <sup>1</sup>H NMR and DOSY measurements for the "One NMR Tube Experiment"

Experiment								
time s	conv.	$P_n^{a}$	$M_n^{b}$	$10^{10} \cdot D$ m <sup>2</sup> s <sup>-1</sup>	$M_{ m w}$	$D^{c}$		
3 600	0.115	11.5	2 0 3 0	2.780	2 4 3 0	1.20		
7 200	0.296	21.6	3 490	1.947	4 4 1 0	1.26		
10 800	0.413	30.9	4 820	1.494	6 870	1.43		
21 600	0.650	47.2	7 200	1.144	10 700	1.49		
32 400	0.777	61.0	9 200	1.007	13 300	1.45		
43 200	0.844	65.8	9 900	0.9972	13 500	1.36		
129 600	0.924	72.9	10 900	0.9017	16 000	1.47		
129 600 <sup>d</sup>	0.918	71.5	10 700	1.072	12 000	1.12		
<sup>a</sup> number of LA units. <sup>b</sup> BzOH and –SnOct end grups. <sup>c</sup> $M_n/M_w$								
<sup>d</sup> quenched								

The monomer conversion and degree of polymerization  $P_n$  have been determined from integrations of the standard <sup>1</sup>H NMR spectrum (Figure 3). The spectrum shows the structure of active macromolecules being in equilibrium with the temporarily inactive chains with –OH end groups, in agreement with ref. 15. The monomer conversion was calculated from the ratio of integration of the methine protons of the lactoyl units **e** signal (overlapped quartets at  $\delta = 5.0 - 5.1$  ppm) to integration of the monomer signal (quartet centred at  $\delta = 3.75$  ppm). Signals **e**' and **g** are broadened due to equilibrium between active and inactive chains and therefore cannot be used for calculations of  $P_n$  of living macromolecules.  $P_n$  and  $M_n$ were calculated from the ratio of integrations of signals **e** and **d'** (the latter at  $\delta = 4.89$  ppm).



**Fig. 4** Kinetic plot of the polymerization of LA in  $C_6D_6$  initiated by  $Sn(Oct)_2/BzOH$  system. Temperature 353 K,  $[LA]_0 = 0.226 \text{ mol}\cdot l^{-1}$ ,  $[BzOH]_0 = 2.99 \cdot 10^{-3} \text{ mol}\cdot l^{-1}$ ,  $[Sn(Oct)_2]_0/[BzOH]_0 \approx 1.0$ .

Figure 4 presents the experimental plot of the left hand side of equation 5 as function of time.

$$-\ln\left(1 - \frac{\left[\mathbf{I}\right]_{0} P_{n}}{\left[\mathbf{M}\right]_{0} - \left[\mathbf{M}\right]_{e}}\right) = k_{p} \left[\mathbf{I}\right]_{0} t$$

$$\tag{5}$$

The corresponding equation has been derived for living irreversible polymerization in one of our previous works by combining  $\ln([M]_0/[M]_t) = -k_p[I]_0t$  and  $P_n = ([M]_0 - [M]_t)/[I]_0$ .<sup>16</sup> Equation 5, after introduction of  $[M]_e$ , is valid for the reversible

Page 4 of 5

polymerization and can be used for determination of the propagation rate constant. The linearity of the plot (as in Figure 4) means that termination and irreversible transfer are simultaneously absent.  $[I]_0$ in Equation 5 is equal to the invariant concentration of the living growing chains. However, in the system studied in this work, the concentration of the growing chains, being invariant, is neither equal to  $[Sn(Oct)_2]_0$  nor to  $[BzOH]_0$ . As the major aim of this work is demonstration of the "One NMR Tube Experiment", it suffices to estimate the  $[I]_0$  value using an approach presented in the work from our laboratory as well as the kinetic studies by Morbidelli.<sup>17,18</sup>

It has been determined in our work, that the instantaneous concentration of the active centres is a function of [ROH] for an invariant  $[Sn(Oct)_2]_0$ .<sup>17</sup> For the conditions used in the present work  $[P^*] \approx [ROH]/3$  (where  $[P^*]$  is the concentration of the momentarily active species. This results from formation of active species in the reversible reaction of  $Sn(Oct)_2$  and BzOH, followed by the propagation step with reversible inter-conversion of active chains into the temporarily inactive ones.

The slope in Figure 4 ( $k_p[I]_0$ ) is equal to 5.76·10<sup>-5</sup> s<sup>-1</sup> and it follows that  $k_p \sim 0.058 \text{ l}\cdot\text{mol}^{-1}\cdot\text{s}^{-1}$  ([I]<sub>0</sub> = 1.134 10<sup>-2</sup> mol·1<sup>-1</sup>) which is close to 0.091 l·mol<sup>-1</sup>·s<sup>-1</sup>, calculated taking into account the temperature coefficient for  $k_p$  as determined by Morbidelli in bulk for the temperature range from 403 to 483 K.<sup>18</sup>

The values of diffusion coefficients for the instantaneous polymer concentrations were extracted from the on-line acquired DOSY spectra and corrected to the proper concentration (eq. (4)).  $M_{\rm w}$  values were obtained from equation given in Figure 1.



**Fig. 5** Dependence of  $M_n$ ,  $M_w$  and D on conversion in living polymerization of LA in C<sub>6</sub>D<sub>6</sub> at 353 K, initiated by Sn(Oct)<sub>2</sub>/BzOH. [LA]<sub>0</sub> = 0.226 mol·l<sup>-1</sup>, [BzOH]<sub>0</sub> = 2.99·10<sup>-3</sup> mol·l<sup>-1</sup>, [Sn(Oct)<sub>2</sub>]<sub>0</sub>/[BzOH]<sub>0</sub>  $\approx$  1.0. Solid line is the least square fit to the  $M_n$  data. Numerical data in Table 3.

In Figure 5 the dependences of  $M_n$  and  $M_w$  on conversion are given. *D* values shown in the figure were calculated as equal to the ratio  $M_w/M_n$ .

The determined values of  $M_w$  (and therefore also D) are higher than expected for controlled-living polymerization. There are several possible reasons: aggregation of the living chains, reversibility of propagation, particularly important at higher conversion, and interconversion of the active and temporarily inactive chains. All these phenomena vanish for quenched samples. Indeed,  $M_w$  (and therefore also D) drop to the level characteristic for macromolecules formed in the controlled–living conditions. Corresponding results obtained from <sup>1</sup>H NMR/DOSY and SEC analyses of the "killed" polymers are shown in Table 2. A decrease of  $M_w$  and D was noticed also after quenching the polymerization in the "One NMR Tube Experiment" (cf. Table 3 and Figure 5). Hence, the described metodology gives also an insight into the subtle phenomena in the polymerizing systems.

#### Conclusions

It has been shown, in the controlled polymerization of L-lactide, that combination of different NMR techniques (standard and DOSY) allows studying on-line the kinetics of polymerization together with determination of  $M_n$ ,  $M_w$  and D. Moreover, in the same experiment carried out in a single NMR tube, the poly(L-lactide) structure analysis has been possible.

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## Notes and references

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Electronic Supplementary Information (ESI) available: experimental procedures, NMR and SEC data. See DOI: 10.1039/c000000x/

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