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1 Novelty of work: Development and characterization of non-oxidative biodiesels to improve 2 engine performance and exhaust emissions 3 Evaluation of the characteristics of non-oxidative biodiesel- A FAME composition, 4 thermogravimetric and IR analysis I. Shancita¹, M.A. Kalam², H.H. Masjuki, S.S. Reham, A.M. Ruhul, I.M. Monirul 5 6 Centre for Energy Sciences, Department of Mechanical Engineering, Faculty of Engineering, 7 University of Malaya, 50603 Kuala Lumpur, Malaysia. 8 Abstract 9 This experiment evaluates the effect of non-oxidative biodiesels (low oxygen content biodiesels) 10 characteristics and their engine performances. Biodiesel produce from different feedstocks 11 typically contains 10 to 15% of oxygen by weight which enhance the combustion quality and reduce the emissions of hydrocarbons (HCs), Carbon monoxide (CO). However, it produces 12 higher amount of oxides of nitrogen (NOx) due to increasing number of combustion products 13 14 resulting higher cylinder temperature. In addition, lean air-fuel mixture can contribute to higher NO_x emissions because biodiesel is more oxygenated than diesel. In this study, biodiesels 15 16 produced from different feedstocks by transesterification process were induced to reduce the 17 oxygen content by using iron bar dipping in those biodiesels, which absorbs oxygen from

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18 biodiesels and get oxidized. Then, oil characteristics, such as, the percentage of saturated and 19 unsaturated fatty acid of, thermal degradation, stability and existing functional groups by using 20 Fatty acid methyl ester (FAME) composition analysis, thermogravimetric analysis (TGA), 21 Differential scanning calorimetry (DSC) and Fourier transform infrared (FT-IR) spectroscopy 22 analysis of neat biodiesel and non-oxidative biodiesel are analyzed. Here, the pongamia and 23 moringa biodiesels were used to evaluate the experiment containing normal and reduced weight 24 percentage of oxygen to improve the quality and stability of biodiesels to be used in the diesel 25 engine which will also reduce the NOx emissions. Non-oxidative biodiesels had some positive 26 effect on their properties which can further reduce the NO_x emissions. Here, Non-oxidative 27 pongamia and moringa had quite similar characteristics and non-oxidative pongamia was 28 observed to perform better according to its property in the reduction of NO_x and other emissions 29 as well.

30 Keywords: Biodiesel, transesterification, non-oxidative, FAME, thermo gravimetric analysis, FT
31 - IR analysis.

32 **1.0 Introduction**

Nowadays, biodiesel is one of the most suitable alternative energy provider for industrial, transportation and domestic consumption as being renewable, eco-friendly, readily available, biodegradable and non-toxic resource. Biodiesel can be used as pure or mixed with diesel by any volume percentage and also it is feasible to use in the diesel engine without any modification of the engine ^{1, 2}. Although, biodiesel accounts for emitted almost zero sulfur oxides, 14.2% HC, 26.8% PM and 9.8% CO₂ emissions by replacing the use of diesel fuel its negative impact on NO_x emissions arising several questions in case of environmental pollutions ^{3, 4}. Biodiesel is

40 typically produced by transesterification reaction in which triglycerides of vegetable oils or 41 animal fats are reacted with short chain alcohol like methanol or ethanol to produce 42 corresponding mono-alkyl esters and glycerin. So mainly biodiesel is a mixture of different fatty 43 acid methyl esters (FAME) containing of long chain, high concentrated mono and poly 44 unsaturated compounds ^{5, 6}.

Typically, neat biodiesel consists of 11-15 wt% oxygen that is the main cause for the 45 46 improvement of combustion efficiency of biodiesel. On the other hand, it degrades the biodiesel 47 stability and also makes less efficient than fossil fuel and not to be used in the airplane. 48 Moreover, it increases the emissions of NO_x although decreasing HC and CO emissions. These 49 results in products of combustion is triggered by the higher oxygen content which raises the 50 combustion chamber temperature improving combustion efficiency and consequently promoting NO_x formation ^{4, 7, 8}. In this study, the oxygen percentage in biodiesel is being decreased in an 51 52 optimum amount which termed as a non-oxidative biodiesel with an aim to reduce NOx 53 emissions. These reformed biodiesels were obtained from low temperature oxidation process in 54 an iron-oxygen bath. The iron bar absorbed the oxygen molecule from biodiesels. Those 55 biodiesels were characterized by FAME composition, TGA, DSC and FT-IR analysis.

Thermal degradation, FAME composition and IR characteristics of biodiesel are important quality assessment sources for biodiesel to be used in diesel engine commercially. Thermal characteristics give the information about thermal stability and volatility of biodiesel by measuring heat capacity, enthalpy, activation energy and melting point ^{2, 7}. Thermogravimetric analysis (TGA) is considered as thermoanalytical technique which measures the change in mass of a substance as a function of increasing temperature at a constant rate. The loss in mass of a substance with the increase in temperature may be caused by decomposition, oxidation or

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vaporization. A derivative of the weight loss curve is normally used to get the decomposition or 63 64 vaporization temperature for pure as well as mixed compounds. On the other hand, differential 65 scanning calorimetry (DSC) is used together with TGA and also is a thermoanalytical technique. 66 It typically measures the energy required for the temperature increase of the substance that 67 studied. DSC curve provides important information about enthalpy of boiling, melting, oxidation 68 and decomposition. An endothermic weight loss is accounted for endothermic decomposition or 69 boiling and exothermic weight loss is attributed for exothermic oxidation or decomposition of the substance 9, 10. Many studies used thermogravimetric analysis for the measurement of 70 stability and production rate of biodiesels. Jain et al.¹¹ reported their study about the effect of 71 72 antioxidants on the thermal degradation of Jatropha curcas biodiesel. By varying the concentration and type of antioxidants various thermodynamic properties of biodiesel such as 73 activation energy (E_a), onset temperature (T_{on}) and offset temperature (T_{off}) were measured by 74 75 TGA analysis. This study helped to improve the biodiesel thermal stability by selecting the suitable additives in engine fuel. On the other hand, Vega-Lizama et al.¹ conducted their 76 77 research on the measurement of thermal degradation degree of soy biodiesel using the residual 78 mass obtained from the decomposition curve. The obtained results showed that, TGA analysis is an efficient method to find the oxidation degree of biodiesel without knowing the biodiesel 79 oxidation process. Moreover, Niu et al.² studied the thermal degradation of different biodiesels 80 81 produced from different feedstocks through transesterification process by TGA analysis. Also, 82 the combustion characteristics of palm and rapeseed biodiesels by thermogravimetric analysis in 83 the furnace of thermogravimetry - differential scanning calorimetry (TGA- DSC) thermal analyzer instead of diesel engine was studied by Yuan et al.⁷. This study was focused on 84

- 85 comparing the suitability of non-oxidative biodiesels with neat biodiesels and diesel which will
- 86 affect the engine performance and exhaust emissions characteristics.

87 **2.0 Materials and methods**

88 2.1 Materials

Crude moringa and pongamia oil were collected from India. The characteristics of those crude
oils are listed in table 3. The diesel fuel (B0) was purchased from PETRONAS. Other materials,
reagents, and chemicals, such as methanol, H₂SO₄, KOH, and Na₂SO₄, were obtained from LGC
Scientific Sdn. Bhd. (Malaysia).

93 **2.2 Production of pongamia and moringa biodiesels**

94 The production of pongamia and moringa biodiesels from their corresponding crude oils was 95 performed in the energy laboratory of the University of Malaya. A 1L batch reactor equipped 96 with flux condenser, magnetic stirrer, thermometer, and sampling outlet were used to produce 97 biodiesels. Crude moringa oil was transesterified to produce biodiesel from it as the acid value 98 was less than 4 mg KOH/g. On the other hand, for pongmia biodiesel production, to reduce the 99 high acid value of feedstocks, a two-step process, involving esterification and transesterification 100 was performed. Firstly, moringa oil was reacted with 25% (v/v oil) of methanol (6:1molar ratio) 101 and 1% (w/w oil) of potassium hydroxide (KOH) and maintained at 60°C and 600 rpm for 2 h. 102 After the reaction, the mixture was deposited in a separation funnel for 12 h to separate glycerol 103 from the produced biodiesel. The lower layer containing glycerol and impurities was drained. In 104 the post-treatment process, the methyl ester formed from the previous process was washed with 105 hot distilled water at 60° C to remove glycerol and impurities. The upper layer was poured into a 106 control rotary evaporator (IKA) to remove water and excess methanol from methyl ester,

107 whereas the lower layer was drained. Methyl ester was dried using Na₂SO₄. The produced 108 biodiesel was filtered using a qualitative filter paper to obtain the final product. For, pongamia 109 oil, in the esterification process, the molar ratio of methanol was maintained at 12:1 (50% v/v110 oil) and 1%(v/v oil) of sulfuric acid (H₂SO₄) were added to the pre-heated oils at 60 °C and 600 111 rpm for 3 h in a glass reactor to refine the crude oils. After reaction completion, the product was 112 transferred to a separation funnel, in which the esterified oil (lower layer) was separated from the 113 upper layer. The upper layer included excess alcohol, sulfuric acid, and impurities. The lower 114 layer was then loaded into a control rotary evaporator (IKA) and heated at 60 °C under vacuum 115 conditions for 1 h to remove methanol and water from the esterified oil. Then, during 116 transesterification, the esterified oils were reacted with 25% (v/v oil) of methanol and 1% (m/m 117 oil) of potassium hydroxide (KOH) and maintained at 60°C and 600 rpm for 2 h. After reaction 118 completion, the produced biodiesels were deposited in a separation funnel for 12 h to separate 119 glycerol from the biodiesels. The upper layer was washed three times with hot distilled water. 120 The formed methyl ester was poured into a control rotary evaporator (IKA) to remove water and 121 excess methanol and then dried using Na₂SO₄. The lower layer containing impurities and glycerol 122 was drained. The produced methyl ester was filtered with qualitative filter paper to obtain the 123 final products as biodiesel.

124 **2.3 Oxygen reducing process from produced biodiesels**

125 The oxygen reducing process was conducted by using a commercial grade iron bar of length 3 126 cm, width 1.5 cm and thickness 0.3 cm, which was dipped in the produced biodiesel. The iron 127 bar was dipped in 10-20 ml biodiesels at 60°C and 100 rpm after cleaning. All the biodiesels 128 with iron bars were kept in airtight glass bottle at room temperature for 6 weeks. All the iron bars 129 were weighted before and after the test period balanced by Scaltec SBA 31 (0.0001g resolution). 130 There was a change of weight of iron bars which was observed 1.04% and 0.7% for pongamia 131 and moringa biodiesels respectively. The iron bars were get oxidized by reacting with oxygen 132 from biodiesels, which was the main cause for reduced oxygen weight percentage in non-133 oxidative biodiesels than neat biodiesels.

134 **2.4 Iron oxidation and elemental composition**

The oxidation of iron bars due to dipping in biodiesels was observed using SEM (Scanning electron microscope) model Hitachi TM3030 at 150x magnification with acceleration voltage of the microscope of 5 KV while operating. Elemental composition of normal and oxidized iron bars has been analyzed by Bruker Quantax 70 EDX (energy dispersive system) at 150x magnification attached with the microscope. Each bars was scanned at three different spots and their average result is reported in this article.

141 **2.5 Fatty acid methyl ester (FAME) composition**

142 The fatty acid methyl ester composition of neat and non-oxidative pongamia and moringa 143 biodiesels were measured by using gas chromatography (GC) analysis in an Agilent 7890A 144 model equipped with a flame ionization detector with HP- INNOWax column (30 m \times 0.25 mm, 145 0.25 µm of thickness). The flow rate of carrier gas Helium was 3.5mL/min. The oven 146 temperature was held at 50°C for 5 min initially and then programmed to increase at a rate of 20 147 °C/min to 210°C and held for 18 min. Then another increase was made to 230°C at a rate of 20 148 °C/min which was held for 13 min. Both the injector and detector temperature was maintained at 149 250°C. A sample was injected at a spilt ratio of 50:1 of 0.3µL volume.

150 **2.6 Property analysis of neat and non-oxidative biodiesels**

151 Biodiesels can be characterized by several important physicochemical properties that determine 152 the quality and suitability of those biodiesels in order to be used in the unmodified diesel engine 153 as a blend with diesel or in a pure form. In this study, some key characterization properties of 154 neat and non-oxidative coconut, pongamia and moringa biodiesels are measured and compared 155 which include kinematic viscosity, density, calorific value, cetane number, oxidation stability 156 and flash point. These physicochemical properties were measured according to the international 157 standard specifications of ASTMD6751 or EN14214, then compared between neat and non-158 oxidative biodiesels and also with conventional diesel.

159 2.7 Thermogravimetric (TGA) analysis

The TGA analysis test of neat, non-oxidative biodiesels and diesel was performed by using TGA
 Q500 V20.13 Build 39 thermal analyzer at a constant heating rate of 50 °C/min under nitrogen

atmosphere at a flow rate of 40 ml/min. About 10-20 mg of samples were used in a 40μL
platinum pan at temperature interval from 4.0°C- 950°C.

164 **2.8 Differential scanning calorimetry (DSC) analysis**

165 The DSC analysis test for neat, non-oxidative biodiesels and diesel was performed in a 166 instrument named DSC Q200 V24.11 Build 124 DSC analytical module in standard cell under 167 inert (nitrogen) atmosphere with gas flow rate of 50 ml/min and at a 10°C/min heating rate to 168 130 °C to heat the samples. DSC cell was loaded with one sample and one reference pans. About 169 10 mg of sample was put in sealed in an aluminum pan and one identical empty pan was set as a 170 reference to perform the test. For heating scans, samples were cooled rapidly and held 171 isothermally for 2 min at -60°C and then heated to 130°C and then the samples were held 172 isothermally for 2 min at 130°C, then cooled to -80°C for cooling scans.

173 **2.9** Fourier transform infrared (FT-IR) spectroscopy analysis

The FT-IR spectroscopy analysis of neat, non-oxidative biodiesels and diesel was done in a Perkin Elmer biodiesel FAME analyzer connected with an MIR TGS detector. The range of spectrum was 4000-450 cm⁻¹ and the resolution and scans were 4 cm⁻¹ and 16 scans, respectively. This spectrum was processed by e-spectrum software.

178 **3.0 Results and discussions**

179 **3.1 Oxidation of iron bars to reduce the oxygen content of biodiesels**

Figure 1 (a), (b) and (c) presents the SEM images of normal, oxidized iron bars from pongamia and moringa biodiesel, respectively. From the SEM images we can observe the change in the iron bars from normal to oxidized mode due to reacting with oxygen in biodiesels, which in turns confirmed that the iron bars were oxidized. Moreover, it can be comprehended from the image

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that, the iron bar from pongamia biodiesel was oxidized higher than iron bar from moringa biodiesel. As a result, there was a higher reduction of oxygen content from pongamia biodiesel than moringa. As biodiesels were kept in an airtight opaque bottle and they were examined before and after the oxygen reduction process.



188

189

(a)



190

191



(c)

192	Fig 1: SEM images of (a) Normal iron (b) Oxidized iron (Pongamia) and (c) Oxidized iron
193	(Moringa)

194 **3.1.1 Elemental composition analysis of normal and oxidized iron bars**

195 The elemental composition of normal and oxidized iron bars was analyzed to see the main 196 components of those bars before and after the oxidation process. Results were obtained from 197 three different spots and the atomic percentage of elements were presented in figure 2. The 198 elements presented in the bars were oxygen, iron and carbon. From the figure 2 (a), (b) and (c) it can be seen that the atomic percentage of oxygen of normal and oxidized iron bars were different 199 200 and the iron bar from pongamia biodiesel had higher oxygen molecule than the iron bar from 201 moringa biodiesel. However, the elemental composition also confirmed the oxidation of iron bars 202 due to reacting with oxygen from the biodiesels as the oxygen percentage increases from normal 203 to oxidized mode and therefore, higher oxygen reduction from pongamia biodiesel.





210 **3.2 FAME composition of neat and non-oxidative biodiesels**

211 In Table 1, the FAME composition of neat and non-oxidative pongamia and moringa biodiesels are presented. The saturated and

212 unsaturated fatty acid composition of both the neat and non-oxidative biodiesels are compared to find the most suitable one for better

213 performance.

214

Table 1: Fatty acid composition of neat and non-oxidative pongamia and moringa biodiesels

				Neat bi	odiesels	Non-oxidative biodiesels		
FAME	Structure	Molecular	Formula	Pongamia	Moringa	Pongamia	Moringa	
		weight		(wt%)	(wt%)	(wt%)	(wt%)	
Methyl hexanoate	6:0	130.18	CH ₃ (CH ₂) ₄ COOCH ₃	-	< 0.1	< 0.1	< 0.1	
Methyl octanoate	8:0	158.24	CH ₃ (CH ₂) ₆ COOCH ₃	< 0.1	< 0.1	< 0.1	< 0.1	
Methyl decanoate	10:0	186.29	CH ₃ (CH ₂) ₈ COOCH ₃	< 0.1	< 0.1	< 0.1	< 0.1	
Methyl laurate	12:0	214.34	CH ₃ (CH ₂) ₁₀ COOCH ₃	< 0.1	< 0.1	0.1	< 0.1	
Methyl myristate	14:0	242.39	CH ₃ (CH ₂) ₁₂ COOCH ₃	< 0.1	< 0.1	0.1	0.1	
Methyl palmitate	16:0	270.45	CH ₃ (CH ₂) ₁₄ COOCH ₃	9.7	10.8	10.2	10.9	
Methyl palmitoleate	16:1	268.43	CH ₃ (CH ₂) ₅ CH=CH(CH ₂) ₇ COOCH ₃	< 0.1	0.1	< 0.1	0.2	
Methyl heptadecanoate	17:0	284.48	CH ₃ (CH ₂) ₁₅ COOCH ₃	-	-	0.1	0.1	
methyl (Z)-heptadec-10-	17:1	282.46	CH ₃ (CH ₂) ₅ CH=CH(CH ₂) ₈ COOCH ₃	-	-	< 0.1	0.1	
enoate								
Methyl stearate	18:0	298.50	CH ₃ (CH ₂) ₁₆ COOCH ₃	6.8	4.4	6.9	4.0	
Methyl Oleate	18:1	296.49	$CH_3(CH_2)_7CH=CH(CH_2)_7COOCH_3$	50.9	25.2	50.8	32.1	
Methyl Linoleate	18:2	294.47	CH ₃ (CH ₂) ₄ CH=CHCH ₂ CH=CH(CH ₂) ₇ COO	18.2	52.1	17.0	44.1	
			CH_3					
Methyl Linolenate	18:3	292.46	CH ₃ CH ₂ CH=CHCH ₂ CH=CHCH ₂ CH=CH(C	4.0	6.0	3.6	4.6	
			H ₂) ₇ COOCH ₃					
Methyl archidate	20:0	326.56	CH ₃ (CH ₂) ₁₈ COOCH ₃	1.6	0.4	1.7	0.4	
Methyl eiosenoate	20:1	324.54	$CH_3(CH_2)_7CH=CH(CH_2)_9COOCH_3$	1.2	0.3	1.3	0.2	
Methyl Behenate	22:0	354.61	CH ₃ (CH ₂) ₂₀ COOH	5.6	0.4	5.6	0.4	
Methyl erucate	22:1	352.59	CH ₃ (CH ₂) ₇ CH=CH(CH ₂) ₁₁ COOH	-	0.2	-	-	
Methyl Lignocerate	24:0	382.66	CH ₃ (CH ₂) ₂₂ COOH	1.6	0.1	1.6	0.2	
Other				0.4	-	1.0	2.6	
			Saturation	25.3	16.1	26.3	16.1	

Mono-unsaturated	52.1	25.8	52.1	32.6
Poly-unsaturated	22.2	58.1	20.6	48.7
Total	99.6	100	99	97.4

215 The monounsaturated fatty acid was same for both neat and non-oxidative pongamia biodiesel, 216 whereas it was increased for moringa biodiesel from neat to non-oxidative mode. These were 217 consisted of mainly oleic acid C 18:1 (50.9%) and (50.8%) for neat and non-oxidative, and 218 eicosenoic acid C 20:1 (1.2%) and (1.3%) for neat and non-oxidative pongamia biodiesel 219 respectively. Meanwhile, for moringa biodiesel it was consisted of oleic acid C 18:1 and 220 eicosenoic acid C 20:1 as (25.2% and 32.1%) and (0.3% and 0.2%) for neat and non-oxidative 221 mode respectively. Other unsaturation percentage was completed by polyunsaturated fatty acid 222 which was due to the presence of linoleic C 18:2 and linolenic acid C 18:3. For both pongamia 223 and moringa biodiesel the percentage of linoleic (18.2% to 17.0% and 52.1% to 44.1%) and 224 linolenic (4.0% to 3.6% and 6.0% to 4.6%) acid were decreased from neat to non-oxidative 225 mode respectively, which resulted the total decreased in polyunsaturation of both biodiesels from 226 neat to non-oxidative mode. High monounsaturated fatty acid resulted in high oxidation stability 227 of pongamia biodiesel which was also confirmed from the test. Moreover, low amount of 228 polyunsaturated fatty acid develops higher cetane number and also produces lower emissions of NO_r ¹²⁻¹⁵. On the other hand, the saturated fatty acid composition was same for moringa but 229 230 increases for pongamia biodiesel from neat to non-oxidative mode. The highest saturated fatty 231 acid was palmitic C 16:0 (9.7% to 10.2% and 10.8% to 10.9%), followed by stearic C 18:0 (6.8% 232 to 6.9% and 4.4% to 4.0%), behenic C 22:0 (5.6% to 5.6% and 0.4% to 0.4%) and arachidic C 233 20:0 (1.6% to 1.7% and 0.4% to 0.4%) for pongamia and moringa biodiesel from neat to non-234 oxidative mode, respectively. High saturated fatty acids contained biodiesels have low quality cold flow properties and also they have high melting points ^{12, 14}. In this study, both the 235 236 biodiesels had low amount of saturated fatty acids and high amount of monounsaturated fatty

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acid with a higher value in pongamia biodiesel for both neat and non-oxidative mode. These
 results are comparable with the previous literatures ¹⁶⁻²².

239 **3.3 Elemental composition of neat and non-oxidative biodiesels**

240 **Table 2** presents the elemental composition of neat and non-oxidative pongamia and moringa 241 biodiesels. Generally, biodiesel contains carbon, hydrogen and oxygen content whereas diesel 242 contains only carbon and hydrogen. Although high oxygen content in biodiesel helps to reduce 243 CO and HC emissions by complete combustion process that influences the oxidation of unburned 244 hydrocarbons, which in turns increase the NO_x emissions by raising the combustion chamber 245 temperature. On the other hand, for reducing the NO_r emissions from produced biodiesels non-246 oxidative pongamia and moringa biodiesels contain optimum amount of oxygen that helps to 247 reduce the CO and HC emissions as well as decreases the NO_x emissions unlike the typical 248 biodiesels. From the table, it can be seen that, neat pongamia biodiesel contained higher oxygen 249 and hydrogen content whereas had lower carbon content than moringa biodiesel. So, pongamia 250 biodiesel had more complete combustion characteristics which also increase the NO_x emissions 251 higher. The reduction of oxygen weight percentage was observed 1.9% and 1.4% for pongamia 252 and moringa biodiesels respectively. Moreover, the carbon percentage increases for both 253 biodiesels from neat to non-oxidative mode, which can be from the iron bar that had lower 254 carbon percentage from normal to oxidized mode. From the table, it can be concluded that, non-255 oxidative moring had the lowest oxygen content hence more suitable for NO_x reduction, 256 although the reduction percentage was higher for pongamia biodiesel.

257

258

259 Table 2: Elemental composition of neat and non-oxidative pongamia and moringa

260

biodiesels

		Neat bi	odiesels	Non-oxidati	ve biodiesels	
Wt%	Test Method	pongamia	moringa	pongamia	moringa	Diesel
Carbon	ASTM D5291	74.0	75.8	76.1	77.1	85.2
(C)						
Hydrogen	ASTM D5291	12.4	12.3	12.2	12.4	14.8
(H)						
Oxygen	ASTM D5291	13.6	11.9	11.7	10.5	0
(0)						
C/H	-	5.97	6.16	6.24	6.22	5.76
Empirical	-	C _{6.17} H _{12.3} O _{0.85}	$C_{6.32}H_{12.2}O_{0.74}$	C _{6.34} H _{12.1} O _{0.73}	C _{6.43} H _{12.3} O _{0.66}	$C_{7.1}H_{14.68}$
formula						

261

262 **3.4 Characterization of neat and non-oxidative biodiesels**

The major physicochemical properties of neat and non-oxidative pongamia and moringa biodiesels are listed in **Table 3** to compare with no. 2 diesel (B0). All the properties were compared with the ASTM D6751 standards. Cetane number was determined three times using fatty acid methyl ester composition with several empirical equations ²³⁻²⁶ presented below:

267
$$CN = 46.3 + (5458/SV) - (0.225*IV)$$
 (1)

268 SV =
$$\sum (560^* A_i)/M_{wi}$$
 (2)

269 IV =
$$\sum (254*A_i*D)/M_{wi}$$
 (3)

where A_i is the weight percentage of each fatty acid component, D is the number of double bonds in each fatty acid, M_{wi} is the molecular mass of each fatty acid component SV is the saponification value and IV is the iodine value.

				ASTM D6	751 B100	Crud	e oil	Neat bio	odiesels	Non-oxi	idative	ASTM D9	75 Diesel
										biodi	esels		
Property	Units	Equipment	Accuracy	Test	Limits ^b	Pongamia	Moringa	Pongamia	Moringa	Pongamia	Moringa	Limits ^c	Results
				Method									
Kinematic	mm²/s	SVM 3000	0.1%	ASTM	1.9-6	44.17	33.26	5.13	4.43	6.50	4.33	1.3-4.1	3.85
viscosity at				D445									
40°Č													
Density at	Kg/m ³	SVM 3000	± 0.1	ASTM	860-894	941.2	921.3	894.7	883.2	909.5	885.2	850	839.1
15°Č	•		kg/m ³	D1298									
Oxidation	h	873	±0.01 h	EN ISO	3 h min ^a	13.47	6.27	6.70	4.99	11.98	0.88	-	19.89
stability		Rancimat		14112									
Calorific	MJ/kg	C2000 basic	± 0.001	ASTM	-	38.85	39.60	38.19	39.97	39.45	39.90	42-46	45.67
value	U	calorimeter	MJ/kg	D240									
Cetane	-			ASTM	47 min	-	-	56.13	45.97	56.60	49.28	40-55	48
number				D613									

273 Table 3: Physicochemical properties of crude oil, neat and non-oxidative pongamia and moringa biodiesels

^aLimit according to EN-14214

275 ^b Ref. ^{27, 28}

^c Ref. ²⁷

277 **3.4.1 Kinematic viscosity**

In table 3, there is fluctuation in the change of the property for neat and non-oxidative biodiesels. The kinematic viscosity decreases for moringa biodiesel from neat to non-oxidative, but increases for pongamia biodiesel. However, both the biodiesels had higher viscosity than diesel for both neat and non-oxidative mode. Moreover, in case of crude oil, pongamia had higher viscosity than moringa. As, viscosity influences the fuel injection system specially the spray atomization, penetration of the injected jet, air-fuel mixture combustion quality at low temperatures, it is very important for combustion quality. Biodiesels have higher viscosity than

diesel fuel because of the presence of electronegative oxygen which makes the biodiesels more polar than diesel ²⁸⁻³⁰. Hence, the reduction of oxygen from biodiesels can improve the viscosity.

285 **3.4.2 Density**

The changes in density are almost similar to the changes in kinematic viscosity except in the case of moringa biodiesel, as shown in table 3. The density increases for pongamia and moringa biodiesels from neat to non-oxidative mode. However, all the neat and nonoxidative biodiesels had a higher density than diesel, among them moringa biodiesel had lower density range for both neat and nonoxidative mode. Crude pongamia oil had higher density than moringa similar as the neat and non-oxidative biodiesels. Density is an important parameter for fuel property as it affects the fuel atomization and combustion as well as Other engine properties are also related to fuel density such as heating value, cetane number and viscosity. The density of biodiesel is normally higher than diesel as the density of biodiesel depends on its fatty acid composition, molar mass, water content and purity ^{28, 29}.

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293 **3.4.3 Oxidation stability**

294 The oxidation stability increases for pongamia biodiesel from neat to non-oxidative mode, 295 whereas decreases for moringa biodiesel from neat to non-oxidative mode which was under the 296 minimum requirement. This decrease indicates the lower oxidation stability of moringa biodiesel 297 from neat to non-oxidative mode. However, diesel had the highest oxidation stability among all 298 crude oils, neat and non-oxidative biodiesels. Meanwhile, non-oxidative pongamia biodiesel had 299 higher oxidation stability after diesel among all other neat and non-oxidative biodiesels due to 300 high monounsaturated fatty acid. oxidation stability affects biodiesel quality by oxidizing it 301 during storage for distribution or in the fuel system. Biodiesels are fatty acid methyl ester which 302 oxidize automatically to form aldehydes, ketons and resins and makes the fuel useless to run the 303 engine. The oxidization rate of biodiesel depends on temperature, fatty acid composition, 304 reaction catalyst, radiation intensity, light etc. and it can be delayed by adding different antioxidants^{28, 29}. 305

306 **3.4.4 Calorific value**

307 It can be inferred from the table 3 that, for moringa biodiesel the calorific value decreases from 308 neat to non-oxidative mode but increases for pongamia biodiesel. However, among all the 309 biodiesels moringa had the highest calorific value for both neat and non-oxidative mode. 310 Meanwhile, all the biodiesels and crude oils had lower calorific value than diesel. Biodiesels 311 have lower heating value than diesel fuel because of the deviation in the hydrogen and carbon 312 content and presence of high oxygen molecule that decreases the heating value about 10-13 313 percent in biodiesel than diesel. Heating value of biodiesel increases with its number of carbon atoms and decreases with its number of double bonds ^{28, 29}. So, it can be shown that, in pongamia 314

biodiesel the calorific value increases with increasing carbon molecules and decreasing oxygenmolecules.

317 **3.4.5 Cetane number**

318 The cetane number for all biodiesels was increased from neat to non-oxidative mode, as seen in 319 table 3. However, Pongamia biodiesel had higher cetane number than moringa for both neat and 320 non-oxidative mode. Moreover, all the biodiesels had higher cetane number than diesel except 321 neat moringa and also the non-oxidative moringa had almost similar value with diesel. Cetane 322 number is defined as the dimensionless measure of the ignition quality of diesel fuel during 323 combustion of a compression ignition engine. It describes the fuel quality based on the ease of 324 self-ignition of the particular fuel. Ignition delay (ID) period of diesel fuel is also indicated by it 325 during the ignition period of injected diesel fuel in combustion chamber. The higher ignition 326 time lag indicates the lower cetane number and vice versa. The range of cetane number in ASTM 327 D6751 standards is based on the two experimental measured fuels named hexadecane ($C_{16}H_{34}$) 328 with cetane number 100 and 2.2.4.4.6.8.8- heptamethylnonane with cetane number 15. The first 329 one is easily ignited fuel and the other one is highly resistive to ignite. Typically, biodiesels have 330 higher cetane number than diesel fuel. 41-56 is the usual range of cetane number for no. 2 diesel and it should not be higher than 65^{28, 29}. So in that case, moringa biodiesel had the more suitable 331 332 cetane number but as indicated earlier that lower polyunsaturated fatty acid indicates high cetane 333 number and thus a low level of NO_x emissions, so non-oxidative pongamia can perform better 334 than moringa biodiesel. Moreover, all the neat and non-oxidative pongamia and moringa 335 biodiesels satisfied the requirements according, which ensures the suitability of use of those 336 biodiesels in the diesel engine without any modification by blending with diesel or in a pure 337 form.

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By analyzing all the properties, it can be observed that all the neat and non-oxidative pongamia and moringa biodiesels satisfied the requirements according to the ASTM D6751 standards, which ensure the suitability of use of those biodiesels in diesel engine without any modification by blending with diesel or in a pure form.

342 **3.5** Thermogravimetric analysis of neat and non-oxidative biodiesels

343 Thermogravimetric analysis of neat, non-oxidative biodiesels and diesel were conducted to344 understand the decomposition, thermal degradation behavior and volatility of those biodiesels.

345 In Figure 3, the TGA curves of neat, non-oxidative pongamia, moringa biodiesels and diesel 346 were compared. In this figure 3, all the curves had the similar trend. Firstly, the TGA curves 347 achieve ascending trend due to buoyancy and molecular adsorption effect but not in a distinct 348 way and all of the neat and non-oxidative biodiesels and diesel were decomposed in only one step which was clearly observed². The decomposition temperature decreases from neat to non-349 350 oxidative biodiesels. Neat pongamia and moringa biodiesels had almost similar thermal stability 351 range. Pongamia and moringa biodiesels were thermally stable up to 170.16 °C and 172.20 °C 352 respectively. However, non-oxidative pongamia and moringa biodiesels were thermally stable up 353 to 158.28°C and 171.78°C, respectively. On the other hand, diesel was thermally stable up to 354 129.04°C. Hence, moringa biodiesel is thermally more stable than pongamia biodiesel and diesel 355 at both neat and non-oxidative mode. Then, with the increasing temperature the TGA curves 356 were descending due to volatilization of weak chemical bonds and small molecules. Around 99% 357 of weight loss took place at the temperature ranges from 95 °C to 279 °C, 107 °C to 317 °C and 358 61 °C to 302 °C for neat pongamia, moringa biodiesels and diesel, respectively. On the other 359 hand, for non-oxidative biodiesels the 99% weight loss range increases than the neat biodiesels. 360 Then, the final thermal degradation was observed with the 0.09%, 0.006% and 0.02024% carbon

361 residue at the end of decomposition for neat pongamia, moringa biodiesels and diesel, 362 respectively. However, in case of non-oxidative biodiesels there were negative percentage of 363 carbon residue observed at the end of the decomposition ^{2, 31, 32}.



Fig 3: TGA curves of neat, non-oxidative pongamia, moringa biodiesels and diesel at 50
 °C/min heating rate

In **Figure 4**, the derivative of thermogravimetric curves (DTG) are also presented. This curves showed the temperature at its peak point where the maximum rate of change of thermal decomposition (dm/dT_{max}) took place for all of the neat and non-oxidative biodiesels and diesel. From the figure, it can be seen that, the peaks of the DTG curves occurred at 177 °C, 179 °C and 203 °C for neat pongmia, moringa biodiesels and diesel, respectively. For non-oxidative moringa

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biodiesel the peak was increased but it decreased for pongamia biodiesel. So, moringa biodiesel had the highest temperature for the maximum rate of change of thermal decomposition (dm/dT_{max}) for both neat and non-oxidative mode, but lower than that of diesel ^{10, 33}.

10 Oxidative Pongamia E **Oxidative Moringa** Non-oxidative Pongamia Diese 8 6 Deriv. Weight (%/°C) 2 0 -2+ 0 200 400 600 800 Universal V4.7A TA Instruments Temperature (°C)

Fig 4: DTG curves of neat, non-oxidative pongamia, moringa biodiesels and diesel at 50

°C/min heating rate

From the two figures it can be concluded that, almost all the biodiesels and diesel had the similar
TGA and DTG curves and thermal characteristics with slight variations. In Table 4, all the
results are summarized.

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375

377

382 Table 4: Thermal characteristics (TGA) of neat and non-oxidative pongamia, moringa

383

biodiesels and diesel

Parameters	Neat	biodiesels	Non-oxidat	Non-oxidative biodiesels		
-	Pongamia	Moringa	Pongamia	Moringa		
Product weight	18.07	19.72	14.04	20.56	19.89	
(mg) Decomposition	170.16	172.20	158.28	171.78	129.04	
temperature (°C)						
Volatility (%)	Not found	Not found	Not found	Not found	Not found	
1 st weight loss (%mg/mg)	99.3	99.4	101.8	99.67	99.5	
1 st weight loss temperature	95 - 279	107 - 317	57 - 444	95 - 353	61 - 302	
range (° C)						
Lost weight at 1st	17.95	19.60	14.29	20.49	19.79	
weight loss (mg)						
Residue	0.08	0.006	-2.48	-0.3379	0.02024	
(%mg/mg)						
Weight at residue	0.0156	0.0013	-0.3481	-0.06946	0.004	
(mg)						
Peak	177	179	169	180	203	
temperature (°C)						

384

385 **3.6 DSC analysis of neat and non-oxidative biodiesels**

386 Differential scanning calorimetry (DSC) is one of the measurement methods for determining the 387 thermal stability of biodiesels. It determines the differential heat flow of biodiesel samples either 388 endothermic or exothermic in respect with a reference as a function of temperature. In other words, DSC measures the energy absorbed or released by a sample as it is heated or cooled 34 . In 389 390 the DSC curves, heat flow (W/g) was plotted against temperature (°C). In the curves, there were 391 variations in transitions and in the inert nitrogen atmosphere the transitions was endothermic 392 which means to be cracked the molecules of the samples were taking heat from surrounding. 393 The melting point and the corresponding enthalpy for those temperatures can be determined from 394 the heating curves and from the cooling curves crystallization point and corresponding enthalpy can be obtained. There was no glass transition found for all of the biodiesel samples ³⁵⁻³⁹. 395

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In **Figure 5 (a) and (b)**, DSC curves of neat pongamia biodiesel for heating and cooling are shown respectively. It represents all the parameters that are important to analysis the curves. The curves showed that, there was no glass transition phase only melting and freezing phases were visible. So, it was clear from the curves that, in heating curve only endothermic and in cooling curve only exothermic reactions occurred. Moreover, the enthalpy change for melting and freezing were also presented in the curves including the reaction temperature range and heat flow range.

403 In Figure 6and 7, the DSC curves for heating and cooling are presented for neat, non-oxidative 404 pongamia, moringa biodiesels and diesel to compare their changes. For diesel and both neat and 405 non-oxidative biodiesels only cracking reactions occurred and there is no distillation region for 406 both diesel and neat, non-oxidative biodiesels as per the figure. From the heating curves, the 407 melting point of both neat and non-oxidative pongamia were higher than both neat and non-408 oxidative moringa biodiesels but lower than that of diesel. However, the melting point decreases 409 for moringa biodiesel from neat to non-oxidative mode but increases for pongamia biodiesel. On 410 the other hand, the enthalpy of melting decreases for all of the biodiesels from neat to non-411 oxidative mode. It was the highest for both neat and non-oxidative moringa biodiesels and the lowest for diesel. 412

413 On the other hand, from the cooling curves, it is clearly comprehended that, diesel had the 414 highest and moringa had the lowest crystallization temperature for both neat and non-oxidative 415 mode, among all the biodiesels. However, the crystallization temperature decreases from neat to 416 non-oxidative mode for both pongamia and moringa biodiesels. Meanwhile, for the enthalpy of 417 crystallization it was highest for moringa biodiesel for both neat and non-oxidative mode and

- 418 lowest for diesel among all other biodiesels. Moreover, the enthalpy of crystallization decreases
- 419 for all of the biodiesels from neat to non-oxidative mode.



421



Fig 5: DSC curves analysis of pongamia biodiesel at 10 °C/min heating rate for (a) heating 424

scans (b) cooling scans



427 Fig 6: DSC heating curves of neat, non-oxidative pongamia, moringa biodiesels and diesel

428

at 10 °C/min

429



432 Fig 7: DSC cooling curves of neat, non-oxidative pongamia, moringa biodiesels and diesel 433 at 10 °C/min

434 In Table 5, all the results for heating and cooling curves of DSC for diesel and neat, non-435 oxidative pongamia and moringa biodiesels are summarized to be clearly understand the 436 comparison among them.

437

438

440 Table 5: Thermal characteristics (DSC) of neat and non-oxidative pongamia, moringa

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441
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biodiesels and diesel

Parameter	Neat bi	odiesels	Non-oxidati	Diesel	
	Pongamia	Moringa	Pongamia	Moringa	
Product mass (mg)	17.7	14	11.2	5.8	15.8
Melting temperature (T _m) (°C)	-32.95	-48.49	-32.31	-49.52	-8.36
Onset temperature for melting (°C)	-39.02	-52.59	-36.84	-53.62	-39.03
Enthalpy of melting (∆H) (J/g)	34.40	43.58	29.16	41.53	22.82
Temperature range of melting (°C)	-47.27 ~ -22.91	-70.81 ~ -33.34	-54.78 ~ -20.24	-70.90 ~ -25.62	-57.89 ~ -19.60
Heat flow range for melting (W/g)	-0.31 ~ -0.25	-0.09 ~ -0.16	-0.14 ~ -0.19	-0.04 ~ -0.11	-0.26 ~ 0.28
Crystallization temperature (T _c) (°C)	-47.14	-58.65	-53.97	-60.32	-16.49
Onset temperature for crystallization	-47.00	-58.24	-51.43	-59.02	1.67
(°C)					
Enthalpy of crystallization (ΔH) (J/g)	40.35	40.81	28.68	36.73	21.04
Temperature range of crystallization	-65.30 ~ -36.48	-74.33 ~ -46.69	$-70.46 \sim -42.03$	-73.02 ~ -48.12	-58.33 ~ 12.70
(°C)					
Heat flow range for crystallization	$0.2674 \sim 0.2669$	$0.09 \sim 0.18$	$0.13\sim 0.22$	$0.11 \sim 0.16$	0.28 ~ 0.29
(W/g)					
442					70

443 3.7 Fourier transform infrared spectroscopy (FT-IR) analysis of neat and non-oxidative 444 biodiesels

In this study, the FT-IR characteristics of all neat and non-oxidative biodiesels are presented to compare with diesel fuel and also to confirm that the functional groups presented in nonoxidative biodiesels were similar to neat biodiesels and diesel. This proofs the suitability of those biodiesels in the diesel engine without any modification.

In **figure 8** and **9** the IR spectrum of neat and non-oxidative pongamia and moringa biodiesels are shown in comparison to diesel fuel. **Table 6** summarized all the frequency range, functional groups, absorbance peaks and percent transmittance (%T) for all neat and non-oxidative biodiesels along with diesel fuel. There is slight difference in the functional group presents between neat and non-oxidative biodiesels. All the neat and non-oxidative biodiesels contained esters and the absence of any broad peaks of O-H stretching vibration of carboxylic acids in the



456 Moreover, the %T decreases from neat to non-oxidative mode for all biodiesels ^{19, 31, 40}.



459 Fig 8: FT-IR spectrum of neat pongamia and moringa biodiesels compared with diesel



			Neat biodiesels		Non-oxidati		
Frequency	Bond	Functional	Pongamia	Moringa	Pongamia	Moringa	Diesel
range (cm ⁻¹)	type	group	U	0	U U	C C	
2850-3000	C-H stretching	Alkanes	Present (2922.97 cm ⁻¹ , 65.92 %T) (2853.55 cm ⁻¹ , 74.08 %T)	Present (2923.49 cm ⁻¹ , 67.48 %T) (2853.98 cm ⁻¹ , 75.26 %T)	Present (2923.07 cm ⁻¹ , 61.90 %T) (2853.62 cm ⁻¹ , 69.8 %T)	Present (2923.56 cm ⁻¹ , 64.06 %T) (2854.07 cm ⁻¹ , 71.82 %T)	Present (2954.89 cm ⁻¹ , 81.75 %T) (2922.9 cm ⁻¹ , 64.65 %T) (2853.41 cm ⁻¹ , 75.18 %T)
1735-1750	C=O stretching	Esters	Present (1741.66 cm ⁻¹ , 66.58 %T)	Present (1741.53 cm ⁻¹ , 63.84 %T)	Present (1740.96 cm ⁻¹ , 64.33 %T)	Present (1741.66 cm ⁻¹ , 61.03 %T)	Absent
1350-1480	-C-H bending	Alkanes	Present (1462.97 cm ⁻¹ , 85.31 %T) (1435.92 cm ⁻¹ , 83.55 %T)	Present (1461.95 cm ⁻¹ , 85.47 %T) (1435.71 cm ⁻¹ , 83.09 %T)	Present (1436.12 cm ⁻¹ , 77.95 %T)	Present (1435.64 cm ⁻¹ , 79.04 %T)	Present (1462.24 cm ⁻¹ , 92.94 %T) (1377.22 cm ⁻¹ , 88.7 %T)
1000-1300	C-O stretching	Esters	Present (1195.72 cm ⁻¹ , 79.93 %T) (1168.30 cm ⁻¹ , 75.44 %T)	Present (1244.40 cm ⁻¹ , 84.92 %T) (1195.63 cm ⁻¹ , 78.25 %T) (1169.46 cm ⁻¹ , 74.28 %T) (1120.07 cm ⁻¹ , 90.71 %T)	Present (1169.09 cm ⁻¹ , 70.48 %T)	Present (1169.62 cm ⁻¹ , 71.69 %T)	Absent
700-725	C-H rock	Alkanes	Absent	Present 722.52 cm ⁻¹ , 84.14 %T)	Present (722.82 cm ⁻¹ , 82.33 %T)	Present (722.64 cm ⁻¹ , 81.10 %T)	Present 722.04 cm ⁻¹ , 95.87 %T)
2500-3300	O-H stretching	Carboxylic acids	Absent	Absent	Absent	Absent	Absent

468 Table 6: IR characteristics region for neat, non-oxidative biodiesels with diesel fuel

All the non-oxidative biodiesels satisfied the minimum requirements and had some improvements in their properties with very few exceptions, to be used as an alternative fuel mixed with diesel instead of neat biodiesels. This new form of biodiesels will affect the performance of engine by reducing the NO_x emissions as well as maintain the other performance and exhaust emissions similar to neat biodiesels. However, the non-oxidative biodiesels is an alternative fuel source of the future for commercial use in large scale.

475 **4.** Conclusions

476 In this study, non-oxidative biodiesels were characterized by fuel physicochemical properties, 477 FAME composition, thermogravimetric and IR analysis to compare with neat biodiesels and 478 diesel fuel and find the suitability of those biodiesels to be used in the diesel engine according to 479 stability and quality remarked by that analysis. By considering and optimizing all the properties, 480 it can be said that non-oxidative pongmia has the higher suitability to be used in diesel engine 481 although it has higher viscosity and density than its neat biodiesel but had an improvement on 482 oxidation stability and calorific value. Further research can be done on the improvement of those 483 properties. The findings of this study are summarized here-

- The oxidation of iron bars was higher for pongamia biodiesel than moringa biodiesel.
- The oxygen reduction percentage was higher for pongamia than moringa biodiesel.
- The kinematic viscosity of moringa biodiesel was decreased due to reduction of oxygen
 content but it increases for pongamia biodiesel. Density increases for both pongamia and
 moringa biodiesels for the reduction of oxygen content.
- Non-oxidative pongamia had the highest oxidation stability after diesel among other
 biodiesels.
- Pongamia biodiesel had increased calorific value due to the reduction of oxygen.

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- Non-oxidative pongamia had the highest cetane number among other neat and non-oxidative biodiesels and diesel. Lower polyunsaturated fatty acid indicates high cetane number and thus low level of NO_x emissions. Hence, non-oxidative pongamia can reduce more NO_x compared to moringa biodiesel.
- TGA and DSC analysis confirmed the thermal, oxidation and storage stability for both
 the non-oxidative biodiesels compared with neat biodiesels and diesel. For all biodiesels
 and diesel, no volatile characteristics were found.
- FT-IR analysis confirmed the suitability of all non-oxidative biodiesels to be used with
- 500 diesel fuel replacing the neat biodiesels by defining the esters content and transmittance
- 501 rate of those biodiesels.

502 **5. Acknowledgement**

- 503 The authors would like to acknowledge University of Malaya for financial support through High
- 504 Impact Research grant UM.C/HIR/MOHE/ENG/07. Thanks to Mr. Solaiman and Mr. Ismail for
- 505 their help in oxygen reduction process and thermogravimetric analysis test, respectively.

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