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| 1 | Cubic and Tetragonal Ferrite Crystal Structures for Copper Ion Immobilization | | |
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| 2 | in Iron-rich Ceramic Matrix | | |
| 3 | | | |
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| 17 | | | |
| 18 | Abstract | | |
| 19 | | | |
| 20 | This study proposed a strategy by reusing the incineration ash of municipal wastewater | | |
| 21 | sludge as ceramic materials to immobilize copper. After sintering the mixture of CuO | | |
| 22 | and sludge ash, hematite (α -Fe ₂ O ₃ , one major component) incorporated copper into | | |

| 23 | cubic CuFe ₂ O ₄ . To observe copper incorporation mechanisms, mixtures of |
|----|---|
| 24 | CuO+ α -Fe ₂ O ₃ were sintered from 650 to 1050 °C, and different copper incorporation |
| 25 | behavior was detected. A low temperature CuFe ₂ O ₄ phase with tetragonal structure |
| 26 | was detected at 750 $^{o}\text{C},$ and the cubic CuFe_2O_4 developed at 1000 $^{o}\text{C}.$ The |
| 27 | incorporation efficiencies were first quantitatively determined by Rietveld refinement |
| 28 | analysis of the X-ray diffraction data. The maximum copper incorporation into |
| 29 | tetragonal and cubic $CuFe_2O_4$ reached around 80% and 73%, respectively. The |
| 30 | leachability analysis pointed to superiority of both copper ferrites in stabilizing copper, |
| 31 | suggesting a promising technique for incorporating copper into the iron-rich ceramic |
| 32 | matrix. Both tetragonal and cubic CuFe ₂ O ₄ were observed with incongruent leaching |
| 33 | behavior, but the lower copper concentrations and higher [Cu]/[Fe] ratio in tetragonal |
| 34 | CuFe ₂ O ₄ leachates indicates its higher capacity for copper stabilization. With high |
| 35 | transformation ratio into CuFe ₂ O ₄ phases and dramatic reduction in metal leachability, |
| 36 | the beneficial use of sludge ash to immobilize hazardous metal contaminated soil may |
| 37 | be potentially succeeded. |
| | |

38

39 Keywords

40

41 Municipal wastewater sludge; Copper ferrite; Quantification; Ceramics; Leaching;
42 Immobilization

43

45 **1. Introduction**

46

The release of metals from mine activities to the surrounded sites can pose severe soil 47 contamination, and may last for a long time without remediation.^{1,2} Once in the soil, 48 the metal pollutants may disperse mechanically and undergo weathering reactions, 49 leading to metal ion distribution within the soil system in forms more mobile than the 50 original ones.³ Remediation approaches such as soil flushing, vacuum extraction, 51 electro reclamation, bioremediation, and soil washing⁴ are employed for 52 metal-contaminated soil, but methods above are highly challenging and expensive for 53 a large scale remediation.^{5,6} Other investigators have also attempted to immobilize 54 hazardous metals in contaminated soil by adding amendments that are able to adsorb, 55 complex, or (co)precipitate elements in the soil.⁷⁻⁹ The suggested copper 56 immobilization mechanisms were reported to precipitate as copper carbonates and 57 oxy-hydroxides, and formation of SO_4^{2-} or PO_4^{3-} complexes.⁸ However, the mobility 58 of heavy metals such as copper in soil is strongly pH dependent, and usually reaches 59 the lowest value at slightly alkaline.⁸ Once in acidic conditions, the immobilization 60 effect of copper will be destroyed.^{8,10} 61

62

By adding aluminum-rich materials into hazardous metal waste, the metals can be stabilized through well-controlled thermal treatment schemes.¹¹⁻¹⁴ By thermally reacting with alumina and kaolinite precursors, the nickel and copper in the spinel-type crystalline structure were found to have substantial reduction in their 67 leachability under acidic environments.

68

Sewage sludge (municipal wastewater sludge) is generated with huge quantity in 69 urban environments, resulting from the accumulation of solids through wastewater 70 treatment.¹⁵ With complex and variable organic and inorganic substances, sewage 71 sludge may contain viable pathogens and parasites as well as a variety of potentially 72 toxic elements and compounds.¹⁶ The amount of sludge produced annually is keeping 73 dramatic increase all over the world.¹⁷ In Europe, the production of dry sewage sludge 74 is in average 90 g per person per day,^{18,19} and there will be an increase of 50% by 75 year.¹⁸ While in Hong Kong, the amount of sludge will increase from the current 76 77 quantity of about 800 tons per day to some 1,500 tons per day by 2014, and subsequently over 2,000 tons per day in 2020.²⁰ The disposal of sewage sludge is one 78 79 of the most difficult problems to be solved, and the need to achieve a sustainable sludge management strategy has become of global concern.²¹ Incineration has become 80 81 an alternative to largely reduce the sludge volume, destruct pathogen agents, and remove organic pollutants for easier and safer handling and disposal.¹⁷ Sludge 82 83 incineration technology, as one of the most attractive disposal methods in the world,^{18,22} was also chosen by Hong Kong government as the core treatment 84 technology to resolve sludge problems.²⁰ Nevertheless, approximately 30% of the 85 solids remain as residues after sludge incineration.²³ With further development of the 86 incineration technology, the subsequent disposal of incineration residues is becoming a 87 serious concern.^{24,25} 88

89

Since sewage sludge ash always contains aluminum, silicon, and iron as the main 90 components,^{26,27} as a waste-to-resource technology, the use of sludge resulting from 91 wastewater treatment processes has attracted much attention.²⁸ More than 70% of the 92 93 total amount of sewage sludge generated in Hong Kong is through the chemically enhanced primary treatment (CEPT).²⁹ CEPT involves the use of chemical coagulants 94 95 (such as alum, lime, ferric chloride, and polyaluminum chloride) to induce coagulation or flocculation of the suspended particles.^{28,30} Once the incineration 96 technology was adopted, iron and/or aluminum might become the main components 97 98 in the ash after sludge incineration process. Therefore, it is predicted that the sludge 99 ash may be potentially used to stabilize metals in contaminated soils. In this study, the 100 sewage sludge ash will be reused and its potential for effectively stabilizing hazardous 101 copper during the sintering process will be evaluated. Furthermore, to quantify the 102 reaction mechanisms and immobilization efficiencies, the simulated system will also 103 be analyzed to assist in the exploration of metal incorporation processes. A prolonged 104 leaching experiment will be carried out to examine the copper stabilization effect, and 105 the leaching behavior of the sintered products will be further discussed.

106

107 **2. Experimental**

108

The collected CEPT sludge sample was first dried at 105 °C, and the weight loss of
the sludge calcined at a temperature range of 200-1000 °C was illustrated in Figure S1.

The weight of the dried sludge significantly reduced from 200 to 500 °C, and kept 111 stable afterwards. The ash from 900 °C and 30 min fired sludge was ground into 112 113 powder for elemental composition analysis by X-ray fluorescence spectroscopy (XRF) 114 (JEOL JSX-3201Z). Normalization into metal oxides (Figure S2) shows Si, Fe, Ca 115 and Al to be the major constituents in the ash. The XRD pattern (Figure S3) further 116 indicates predominant iron-containing crystalline phase as hematite (Fe_2O_3), while Si, 117 Ca and Al are mainly contained in hauyne (Na₆Ca₂Al₆Si₆O₂₄(SO₄)₂), anhydrite (CaSO₄), and a type of zeolite (Na₆(AlSiO₄)₆). Works by others³¹ also reported the 118 119 existence of aluminosilicate and anhydrite phases in the sewage sludge ash.

120

121 The 900 °C and 30 min fired sludge was used as soil amendment, and mixed with 122 copper oxide (Sigma Aldrich) which was simulated as the predominant pollutant of 123 the contaminated mining areas. Since both aluminum and iron will potentially react 124 with copper in the system, samples were first prepared by mixing CuO and the sludge 125 ash with the molar value of Al and Fe together as two times of Cu. The mixture was then sintered at 950 °C, and the XRD pattern (Figure S4) shows Fe₂O₃ as the only 126 127 component reacting with copper and forming CuFe₂O₄ product phase. Therefore, the 128 CuO was further mixed with the sludge ash at a Cu:Fe molar ratio of 1:2 to guarantee 129 the maximum production of CuFe₂O₄ in the sludge ash system. To explore the 130 detailed mechanisms of copper incorporation, the Fe₂O₃ was used as iron-rich 131 material to react with CuO at a Cu:Fe molar ratio of 1:2. All mixing processes were 132 carried out by ball milling the powder in water slurry for 18 h. The slurry samples

were dried and homogenized by mortar grinding, pressed into 20-mm pellets at 480
MPa, and then fired. A sintering scheme with a 3-h dwelling time at the targeted
temperature in a high-temperature furnace (LHT 02/16 LB, LBR, Nabertherm Inc.)
was used for temperatures ranging from 650 to 1050 °C with furnace-controlled
cooling.

138

Phase transformation during sintering was monitored using the powder X-ray 139 140 diffraction (XRD) technique. The step-scanned XRD pattern of each powder sample 141 was recorded by a Bruker D8 Advance X-ray powder diffractometer equipped with 142 Cu K α 1,2 X-ray radiation source (40 kV 40 mA) and a LynxEye detector. The 2 θ 143 scanning range was 10 to 90°, and the step size was 0.02° with a scan speed of 0.8 s step⁻¹. Qualitative phase identification was executed by matching powder XRD 144 145 patterns with those retrieved from the standard powder diffraction database of the 146 International Centre for Diffraction Data (ICDD PDF-2, Release 2008). In hematite 147 series, the crystalline phases in the products are all subjected to quantitative phase analysis using Topas 4-2, which employs the Rietveld refinement method.³² The 148 149 refinement quality was monitored by the reliability values provided in Table S1.

150

As one objective of this study was to distinguish the leaching characteristics of different copper-hosting phases, single-phase samples were considered preferable in the leaching experiment. The leaching experiments for CuO and copper-containing product phase(s) were conducted by a method modified from the U.S. Environmental

| 155 | Protection Agency's SW-846 Method 1311: Toxicity Characteristic Leaching |
|-----|--|
| 156 | Procedure (TCLP), with an acetic acid solution (extraction fluid #2, pH 2.9) used as the |
| 157 | leaching fluid. Each leaching vial was filled with 10 mL of leaching fluid and 0.5 g of |
| 158 | the powder sample and rotated end-over-end at 60 rpm for 0.75 to 22 days. At the end |
| 159 | of each agitation period, the leachates were filtered using 0.2- μ m syringe filters, the pH |
| 160 | was determined, and the concentrations of all metals were derived by inductively |
| 161 | coupled plasma atomic emission (Perkin-Elmer Optima 3300 DV). |
| 162 | |
| 163 | 3. Results and discussion |
| 164 | |
| 165 | 3.1. Potential of reusing municipal wastewater sludge ash for copper stabilization |
| 166 | |
| 167 | XRD patterns in Figure 1a demonstrate the phase transformation when the mixtures of |
| 168 | sludge ash and CuO were sintered at temperatures ranging from 650 to 1050 $^{\rm o}{\rm C}$ for 3 |
| 169 | h. The peaks of CuFe ₂ O ₄ spinel were detected after the 3-h sintering process at 750 $^{\circ}$ C, |
| 170 | even with very complicated compositions in the system. When the sintering |
| 171 | temperature increased to 850 $^{\rm o}\text{C},$ the CuFe_2O_4 spinel phase developed substantially |
| 172 | while peaks of CuO and Fe ₂ O ₃ diminished accordingly. Further heating increased the |
| 173 | crystallinity and production of the CuFe ₂ O ₄ spinel phase. Besides the formation of |
| 174 | CuFe ₂ O ₄ spinel, other major components such as hauyne and zeolite kept |
| 175 | continuously growing, while anhydrite and quartz eventually decreased with elevated |
| 176 | temperatures. Although the decomposition temperature for anhydrite is usually higher |

| 177 | than 1000 °C, ³³ the disappearance of anhydrite at temperature ≤ 850 °C in this |
|-----|--|
| 178 | experiment may be due to the conversion of calcium into the growing phases: hauyne |
| 179 | and zeolite. Apart from phases discussed above, anorthite $(CaAl_2Si_2O_8)$ — a main |
| 180 | crystalline phase in glass-ceramics ³⁴ kept relatively stable through out the sintering |
| 181 | mechanism. |

182

From the standard diffraction pattern of CuFe₂O₄ spinel (PDF#77-0010), the highest 183 peak is at $2\theta \sim 35.5^{\circ}$ but was overlapped by peaks of other phases. Therefore, the 184 second highest peak at $2\theta \sim 62.7^{\circ}$ was selected for further observation of the CuFe₂O₄ 185 186 spinel in the sintered products (Figure 1b). The peak intensity of the CuFe₂O₄ spinel 187 kept increasing after its first appearance at 750 °C, and a significant growth was 188 observed when the sintering temperature increased from 750 to 850 °C. With further 189 heating (≥ 950 °C), the spinel phase kept stable through out the sintering process. 190 From the phase transformation during the sintering process of CuO + sewage sludge 191 ash, iron was observed as the only component to incorporate copper, and the $CuFe_2O_4$ 192 spinel was identified as the only copper-hosting product phase. It seems that other 193 complicated compositions are not involved in the formation of $CuFe_2O_4$ spinel, and 194 their existence might influence the efficiency of copper transformation. Therefore, the 195 hematite (Fe₂O₃) without any other impurities was used as amendment to incorporate 196 copper, and to further analyze the mechanisms of copper transformation in iron-rich 197 systems.

199 *3.2.* The mechanisms of copper incorporation in simulated iron-rich systems

200

XRD patterns in Figure 2 illustrate the phase changes in $CuO + Fe_2O_3$ systems when 201 202 the mixture was sintered from 650 to 1050 °C for 3 h. After being sintered at 750 °C 203 for 3 h, the observable peaks show that the $CuFe_2O_4$ with tetragonal structure 204 $(t-CuFe_2O_4)$ was first generated. Spinel-type ferrites usually display cubic symmetry 205 but some show tetragonal distortion in which one of the lattice edges differs in length in relation to the other two.³⁵ Generally, in the normal AB_2O_4 spinel structure, B^{3+} 206 ions occupy some of the octahedral sites and A²⁺ ions locate on tetrahedral sites.³⁶ But 207 for an ideal inverse spinel, the Cu²⁺ ions occupy octahedral sites, whereas Fe³⁺ ions 208 are found on octahedral and tetrahedral sites with approximately equal occupancy.^{35,37} 209 The t-CuFe₂O₄ is a stable low temperature phase, and its crystal lattice exhibits a 210 tetragonal distortion from the ideal inverse CuFe₂O₄ spinel.³⁵ From Figure 3, the 211 212 t-CuFe₂O₄ phase kept developing with elevated sintering temperatures, while peaks of 213 CuO and Fe_2O_3 diminished eventually. However, when the temperature reached 1000 214 ^oC, the CuFe₂O₄ phase mainly crystallized with cubic spinel structure with very strong 215 peak intensities, and the peaks of t-CuFe₂O₄ reduced dramatically. In cubic CuFe₂O₄ (c-CuFe₂O₄) crystal structure, a few of the Cu²⁺ ions occupy tetrahedral sites.³⁷ When 216 the sintering temperature kept increasing to 1050 °C, the orthorhombic compound 217 CuFeO₂ was detected. The formation of CuFeO₂ under air atmosphere was also 218 reported at a temperature range of 1000 to 1100 °C.^{38,39}. 219

| 221 | The copper-hosting crystalline phases together with the other iron-hosting phases |
|-----|---|
| 222 | were all subjected to quantitative analysis via Rietveld refinement, and the weight |
| 223 | fractions were shown in Figure 3a. Sintering the sample at 750 °C for 3 h generated |
| 224 | around 75% of the t-CuFe ₂ O ₄ phase, and the weight fractions of CuO and Fe ₂ O ₃ |
| 225 | reduced to values lower than 15%. With elevated temperatures, the weight percentage |
| 226 | of t-CuFe ₂ O ₄ phase increased to about 90% and kept stable around this value until the |
| 227 | temperature reaching 950 °C. Further heating at 1000 °C cause the significant |
| 228 | reduction of t-CuFe ₂ O ₄ phase and substantial formation (about 70%) of the c-CuFe ₂ O ₄ |
| 229 | phase as observed in Figure 2. At 1050 $^{\circ}$ C, the c-CuFe ₂ O ₄ developed with the weight |
| 230 | percentage of higher than 80%, and about 20% of the $CuFeO_2$ was generated as |
| 231 | another copper-hosting product phase. |

232

233 Therefore, reactions derived from both XRD and quantitative results are listed below:

234

235
$$\operatorname{CuO} + \operatorname{Fe}_2 O_3 \xrightarrow{\leq 950 \ ^{\circ}C} \operatorname{CuFe}_2 O_4 \text{ (tetragonal)}$$
(1)

236
$$\operatorname{CuO} + \operatorname{Fe}_2 \operatorname{O}_3 \xrightarrow{1000 \, {}^{\circ} \operatorname{C}} \operatorname{CuFe}_2 \operatorname{O}_4 (\operatorname{cubic}) + \operatorname{CuFe}_2 \operatorname{O}_4 (\operatorname{tetragonal})$$
(2)

237
$$\operatorname{CuO} + \operatorname{Fe}_2 \operatorname{O}_3 \xrightarrow{1050 \, ^{\circ} \mathrm{C}} \operatorname{CuFe}_2 \operatorname{O}_4 (\operatorname{cubic}) + \operatorname{CuFeO}_2$$
(3)

238

To indicate copper transformation efficiencies into different product phases, the transformation ratio (TR) is used. Taking M_n (n = 1, 2, 3,...) as copper-hosting product phases, the TR (n = 1, 2, 3,...) is calculated as follows:

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244
$$= \frac{a_{n} \frac{\text{wt\% of } M_{n}}{\text{MW of } M_{n}}}{a_{1} \frac{\text{wt\% of } M_{1}}{\text{MW of } M_{1}} + a_{2} \frac{\text{wt\% of } M_{2}}{\text{MW of } M_{2}} + a_{3} \frac{\text{wt\% of } M_{3}}{\text{MW of } M_{3}} + \dots + a_{n} \frac{\text{wt\% of } M_{n}}{\text{MW of } M_{n}}}$$
(4)

245

where MW = molecular weight; a_n (n=1, 2, 3,...) is the number of the target copper atom contained in the corresponding phase; and wt% is the weight fraction of its corresponding phase obtained through Rietveld refinement.

249

Therefore, the TR index for copper transforming into $t-CuFe_2O_4$ (TR_t), $c-CuFe_2O_4$ (TR_c) and CuFeO₂ (TR_d) can be calculated according to Eq (4). And the total transformation of copper (TR) into new crystal structures can be expressed as

253

254
$$TR(\%) = TR_t(\%) + TR_c(\%) + TR_d(\%)$$
 (5)

255

The copper incorporation into t-CuFe₂O₄ reached around 70% at 750 °C and increased to about 80% at the temperature range of 850-950 °C. The copper transformation into c-CuFe₂O₄ increased significantly to around 60% after being sintered at 1000 °C for 3 h. At the highest temperature (1050 °C) of this sintering mechanism, about 73% of copper distributed in c-CuFe₂O₄ with 27% in CuFeO₂. The total TR value kept stable around 80% at temperature ≤ 1000 °C, and reached 100% at 1050 °C, indicating the complete transformation of copper into product phases.

263

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| When the transformation behavior of copper in Fe_2O_3 and sewage sludge system is | | |
|--|--|--|
| compared, it can be found that the tetragonal $CuFe_2O_4$ never appeared in sewage | | |
| sludge system. Since a small amount of dopant ions can change structural properties | | |
| of ferrites, ⁴⁰ and the site preference of dopant ions might lead to transfer Fe^{3+} from | | |
| A-sites to B-sites and cause a crystallographic transformation from tetragonal to cubic | | |
| structure. ⁴¹ Therefore, the structure of the as formed CuFe ₂ O ₄ in sewage sludge | | |
| system will predominantly crystallize as cubic structure due to the existence and | | |
| influence of Al, ⁴² Si, ⁴³ or other minor compositions. | | |
| 3.3. Leaching behavior of product phases | | |

phases in the sintered products, their capacity in metal stabilization must be taken into account and compared with the initial copper-containing phase (CuO). Thus, this study prepared single-phase samples to determine their intrinsic leachability and leaching behavior in a prolonged (22-d) leaching experiment. The as-received CuO powder was used as the single-phase sample after phase confirmation by XRD. The single-phase t-CuFe₂O₄ and c-CuFe₂O₄ sample were obtained by sintering the CuO + Fe₂O₃ mixture at 950 °C for 60 h and at 1000 °C for 72 h, respectively. The purpose of such prolonged sintering processes is to ensure the complete reaction at grain boundaries/surface. The XRD patterns of single-phase products are provided in Figure S5.

Because t-CuFe₂O₄ and c-CuFe₂O₄ are the potential and predominant copper-hosting

| 2 | Q | 6 |
|---|---|---|
| 4 | 0 | U |

The pH value of the CuO leachate (Figure S6) underwent a significant increase in the 287 288 first few days and then held steady at around pH 4.8. For c-CuFe₂O₄ and t-CuFe₂O₄ 289 leachates, in contrast, were very close to the initial pH value of the leaching fluid 290 throughout the leaching period. As an increase in leachate pH may be accompanied by 291 the destruction of the sample crystal structure, the increase in the CuO leachate's pH 292 may indicate that the CuO phase is more vulnerable to proton-mediated dissolution 293 than the copper ferrite phases. Since the compositions of different metal-hosting 294 phases will affect the contact between solid and solution, the total metal content 295 should be normalized for comparison of the leachability. The normalized copper 296 concentrations in both the CuO and copper ferrites leachates are presented in Figure 297 4a, which shows that the leached copper from the CuO sample is two orders greater 298 than those from the CuFe₂O₄ samples. When the metal leachability of both ferrites is 299 compared, the c-CuFe₂O₄ phase performed both higher copper and iron leaching than 300 the lower temperature phase $(t-CuFe_2O_4)$ as demonstrated in Figure 4a & b. At the end 301 of the leaching period, a four-time higher copper concentration in $c-CuFe_2O_4$ leachate 302 than that in t-CuFe₂O₄ leachate indicates the tetragonal CuFe₂O₄ phase as a more 303 promising structure for copper stabilization. Moreover, the iron concentrations in 304 t-CuFe₂O₄ leachate are lower than those in c-CuFe₂O₄ leachate, which confirms the 305 higher resistance to acidic attack of the tetragonal structure.

306

307 With the proceeding of leaching process, the congruent dissolutions of these

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308 crystalline phases in an acidic solution may be expressed as follows: 309 $CuO_{(s)} + 2H^{+}_{(aq)} \rightarrow Cu^{2+}_{(aq)} + H_2O$ 310 311 $CuFe_2O_{4(s)} + 8H^+_{(aq)} \rightarrow Cu^{2+}_{(aq)} + 2Fe^{3+}_{(aq)} + 4H_2O$ 312 313 The concentrations of both $[Cu^{2+}]$ and $[Fe^{3+}]$ may also be limited by the potential 314 precipitation/dissolution of the Cu(OH)₂ and Fe(OH)₃ solid, respectively,^{44,45} as listed 315 316 in followings:

317

318
$$Cu(OH)_2 \leftrightarrow Cu^{2+} + 2OH^- (K_{spCu} = 10^{-19.3})$$
 (8)

319

320
$$Fe(OH)_3 \leftrightarrow Fe^{3+} + 3OH^- (K_{spFe} = 10^{-37.4})$$
 (9)

321

322 The pH value of the leachate at the end of the leaching process was measured as 4.9. According to Eq (8), the permitted $[Cu^{2+}]$ value was calculated to be $10^{-1.1}$ M, which 323 is higher than the measured total copper concentration of ~ 2090 mg L^{-1} (~ 10^{-1.5} M). 324 325 Thus, copper ions might not be precipitated during the leaching process. Since the pH 326 value of copper ferrite leachates kept stable at pH around 2.9, the system was 327 maintained in a more acidic environment and the copper concentration was much lower than that of the CuO leachate. The copper concentrations in the leachates of 328 329 c-CuFe₂O₄ and t-CuFe₂O₄ were all considerably under-saturated regarding to the

(6)

(7)

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| 330 | $Cu(OH)_{2(s)}$ phase. At pH 2.9, the permitted concentration of total Fe ³⁺ ions is |
|-----|--|
| 331 | calculated as $10^{-4.1}$ M (4.45 mg L ⁻¹) according to Eq (9). From Figure 4b, the iron ion |
| 332 | concentrations were observed as 2.3 and 0.7 mg $L^{\text{-1}}$ for c-CuFe_2O_4 and t-CuFe_2O_4, |
| 333 | respectively. The lower iron concentrations in both leachates than the permitted |
| 334 | maximum value shows that iron ions were also not subject to reprecipitation from the |
| 335 | leachates. Theoretically, if the c-CuFe ₂ O ₄ and t-CuFe ₂ O ₄ solid displayed a congruent |
| 336 | dissolution, the [Cu]/[Fe] molar ratios would be at 1:2 which is coincident with the |
| 337 | stoichiometry of Cu and Fe ions in their original phase. However, the observed |
| 338 | [Cu]/[Fe] molar ratios (> 1:2) in Figure 4c illustrate that both c-CuFe ₂ O ₄ and |
| 339 | t-CuFe $_2O_4$ leachates are incongruent solutions, where the majority of the Fe-O bonds |
| 340 | still remained on copper ferrite surfaces. |

341

342 Although c-CuFe₂O₄ and t-CuFe₂O₄ displayed incongruent leaching, the behavior in 343 both leachates is different from each other. Firstly, the [Cu]/[Fe] molar ratio decreased 344 from about 18.0 to around 8.0 and kept stable around 8.0 in t-CuFe₂O₄ leachates, 345 whilst the ratio in c-CuFe₂O₄ leachates kept stable from 4.3 to 5.0. Since both the 346 leaching of copper and iron increased with the prolong leaching time, the decrease of 347 [Cu]/[Fe] ratio might indicate the moderate leaching of copper from the tetragonal 348 structure. Secondly, although the [Cu]/[Fe] molar ratio kept decreasing within the first 349 10 days in t-CuFe₂O₄ leachates, the value of this ratio is still much higher than that in 350 c-CuFe₂O₄ leachates throughout the whole leaching process. The higher ratio means 351 that there might be more Fe-O bonds remained on the solid surface, which may inhibit

- further leaching of copper from the product phase. Therefore, it might explain much
 lower copper leachability observed in t-CuFe₂O₄ leachates.
- 354

355 Even though with different treatment methods and leaching conditions, the effect of 356 copper immobilization in this study was further compared with what have been reported in other studies. Kumpiene et al.⁴⁶ used coal fly ash and natural organic 357 358 matter (peat) as the amendments to stabilize the metal contaminated soil, and reached a 98.2% decrease in the amount of leached copper. Solpuker et al.⁴⁷ investigated the 359 360 potential of using pervious concrete to immobilize copper, and detected the degree of 361 copper immobilization (the ratio of leached copper to initial copper amount) to be around 0.19. Furthermore, a recent study⁴⁸ reported that the combination treatment of 362 363 calcined oyster shells (COS) and steel slag (SS) was sufficient enough to significantly decrease copper leachability (96% reduction). While in our study, a 99.7% and 99.4% 364 decrease of the amount of leached copper was monitored for t-CuFe₂O₄ and 365 c-CuFe₂O₄ phases compared to CuO, even with very fine milled powders and after a 366 367 22-d leaching period.

368

4. Conclusions

371 Copper ferrites were generated with two different crystal structures (cubic and 372 tetragonal) when α -Fe₂O₃ was used as the ceramic precursor to incorporate copper, 373 while the cubic CuFe₂O₄ was found as the only copper-containing product phase in

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| iron-rich municipal wastewater ash systems. The incorporation mechanisms of | |
|---|---|
| hazardous copper were explicated with the combination of quantitative and qualitative | |
| XRD technique. About 90% of the tetragonal CuFe ₂ O ₄ phase was generated when | |
| samples of CuO+ α -Fe ₂ O ₃ were sintered at 850 °C for 3 h, while the weight percentage | |
| of cubic CuFe ₂ O ₄ phase increased to 70% with a significant decrease of tetragonal | |
| $CuFe_2O_4$ when the samples were further heated at 1000 °C. Both copper ferrites | 1 |
| exhibited good performance in copper ion immobilization, and the low-temperature | |
| tetragonal CuFe ₂ O ₄ phase was further confirmed as a more promising structure for | |
| copper stabilization when copper concentrations in both cubic and tetragonal $CuFe_2O_4$ | |
| leachates were compared. Although with different metal leachability, both cubic and | |
| tetragonal CuFe ₂ O ₄ displayed incongruent leaching behavior. In conclusion, through | |
| reliably reusing iron-rich materials (the municipal wastewater sludge ash and iron | 1 |
| oxide), this study does not only show the potential to thermally stabilize the simulated | |
| copper-polluted soils, but also realize the feasibility of achieving "waste-to-resource" | |
| for a more sustainable environment. | |
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hazardous copper were explicated with the combination o 375 376 XRD technique. About 90% of the tetragonal CuFe₂O₄ 377 samples of CuO+ α -Fe₂O₃ were sintered at 850 °C for 3 h, 378 of cubic CuFe₂O₄ phase increased to 70% with a signif 379 $CuFe_2O_4$ when the samples were further heated at 100 380 exhibited good performance in copper ion immobilization 381 tetragonal CuFe₂O₄ phase was further confirmed as a n 382 copper stabilization when copper concentrations in both c 383 leachates were compared. Although with different metal 384 tetragonal CuFe₂O₄ displayed incongruent leaching beha 385 reliably reusing iron-rich materials (the municipal wast 386 oxide), this study does not only show the potential to ther 387 copper-polluted soils, but also realize the feasibility of ac 388 for a more sustainable environment.

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390 Acknowledgements

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398 Supporting Information

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400 One table and eight figures demonstrating the characterization of municipal 401 wastewater sludge, powder XRD patterns of raw materials and pure phase products 402 for leaching experiments, and two examples of Rietveld refinement results are 403 available free of charge via the Internet at http://pubs.acs.org. 404

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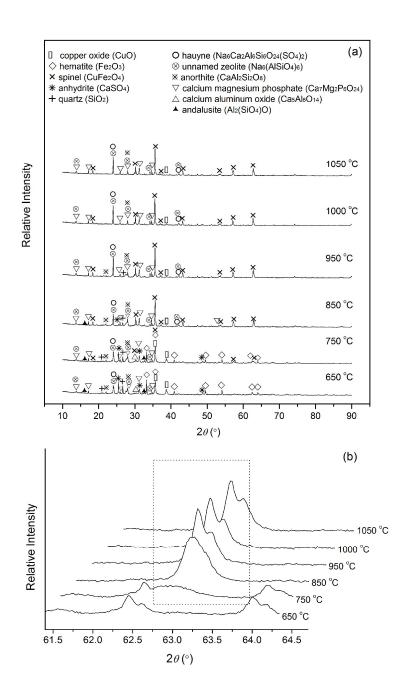
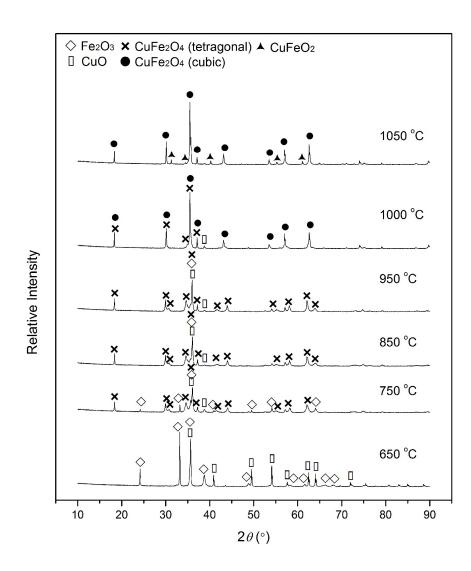


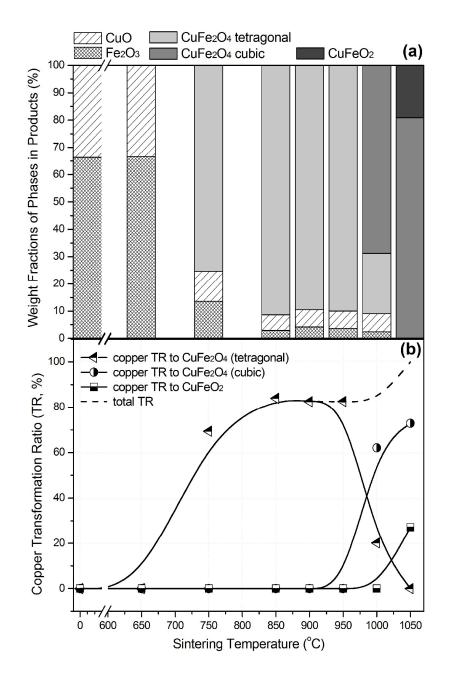
Figure 1. (a) XRD patterns of the sludge ash + CuO system, and (b) the comparison of 486 XRD peak intensities (between $2\theta = 61.5$ and 64.5°) for sludge ash + CuO samples 487 sintered at 650-1050 °C for 3 h. The crystalline phases are identified as: CuO 488 (PDF#80-1268), Fe₂O₃ (PDF#85-0599), CuFe₂O₄ (PDF#77-0010), anhydrite (CaSO₄, 489 PDF#37-1496), (PDF#79-1910), hauyne 490 quartz $(Na_6Ca_2Al_6Si_6O_{24}(SO_4)_2,$ PDF#73-1920), zeolite $(Na_6(AlSiO_4)_6,$ PDF#42-0217), 491 unnamed anorthite (Ca(Al₂Si₂O₈), PDF#89-1473), calcium magnesium phosphate (Ca₇Mg₂P₆O₂₄, 492 PDF#20-0348), calcium aluminum oxide (Ca₅Al₆O₁₄, PDF#11-0357), andalusite 493 (Al₂(SiO₄)O, PDF#39-0376). 494



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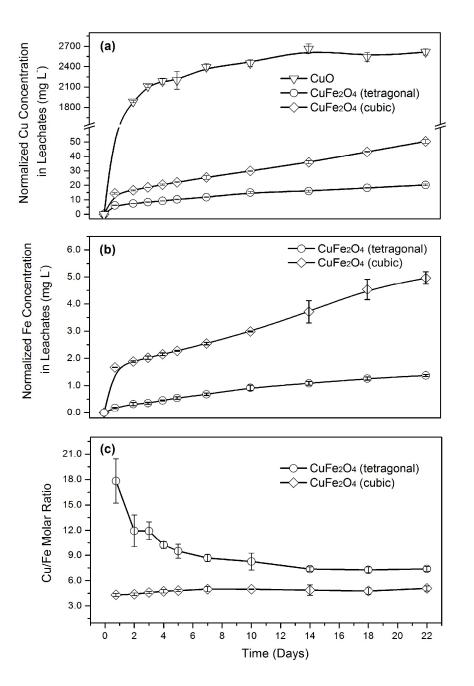
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Figure 2. XRD patterns of 650-1050 °C and 3 h sintered $Fe_2O_3 + CuO$ samples. The standard patterns include CuO (PDF#80-1268), tetragonal CuFe₂O₄ (PDF#34-0425), cubic CuFe₂O₄ (PDF#77-0010), CuFeO₂ (PDF#75-2146), and hematite (α -Fe₂O₃, PDF#85-2599).



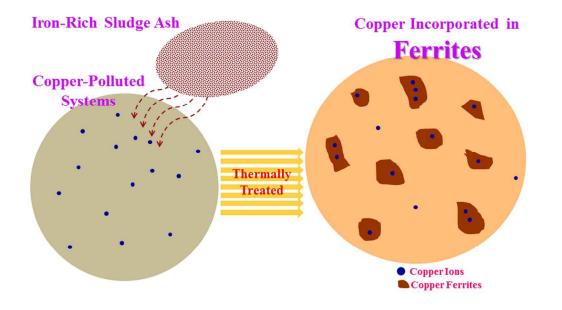
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Figure 3. (a) Variations of weight fractions of Cu- and Fe-containing crystalline phases obtained from the CuO sintering reactions with Fe_2O_3 precursor, and (b) the transformation ratios (TR_t, TR_c. TR_d, and total TR, %) of Cu into the product phases.



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Figure 4. (a) Normalized copper concentrations of the CuO, tetragonal CuFe₂O₄, and cubic CuFe₂O₄ leachates, (b) normalized iron concentrations and (c) [Cu]/[Fe] molar ratios of tetragonal CuFe₂O₄ and cubic CuFe₂O₄ leachates. The leaching solution was TCLP extraction fluid no. 2 (acetic acid solution) with a pH of 2.9. Each leaching vial was filled with 10 ml of extraction fluid and 0.5 g of powder samples, and then rotated end-over-end between 0.75 and 22 d.



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