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1 **Utilization of a pyrrole derivative based antimicrobial functionality impregnated onto**
2 **CaO/g-C₃N₄ for dyes adsorption**

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11

Abstract

A novel functionalization of CaO/g-C₃N₄ based nanocomposite using 4,5-diphenyl-2-thioxo-2,5-dihydro-1H-pyrrole-3-cabonitrile (P3C@CaO-HCN) was performed for wastewater remediation from organic dyes and microbial pollutants. Adsorption performance of multiple mixtures of basic and acidic dyes by P3C@CaO-HCN was investigated and optimized using three-level Box–Behnken design of experiment (BBD-DOE). The quadratic Box-Behnken polynomial equation showed best fitted with the experimental adsorption capacities of crystal violet (CV), methylene blue (MB), and methyl orange (MO) model dyes. The simultaneous influence of adsorption conditions was tested based on the developed Box-Behnken equation, 3D contour plots, and ANOVA analysis. Nonlinear regression analysis of kinetics and isotherm constants were computed and validated to propose the adsorption mechanism. Adsorption is found within the ranges of endothermic physical adsorption ($\Delta H^\circ = 6.17$ to 8.58 KJ/mol) and controlled by both π - π and electrostatic forces depending on the pH level beside film diffusion mechanism. The maximum adsorption affinity can arrange in the order of MB > CV \geq MO with q_e ($\mu\text{mol/g}$) of 1915.8, 1227.8, and 1221 $\mu\text{mol/g}$, respectively. At 500 mg/l P3C@CaO-HCN as minimum inhibitory dose, the inhibition rate (I%) were 87.9%, 46.9%, and 72.5% for *E. coli*, *P. aeruginosa*, and *C. albicans*, respectively. The antimicrobial effect can result from the free cyanide (C \equiv N) functionality of a pyrrole-3-cabonitrile and protonated g-C₃N₄ (HCN) sheet, which depend on the P3C@CaO-HCN concentration and pathogen types.

Keywords: 4,5-diphenyl-2-thioxo-2,5-dihydro-1H-pyrrole-3-cabonitrile; protonated carbon nitride; CaO nanoparticle; adsorption; antimicrobial activity; Box–Behnken design of experiment (BBD-DOE).

34

35 1. Introduction

36 Many kinds of water pollutions have already become existed, including organics,
37 inorganic, microorganism, and so on. Dyes contaminated water environments have been
38 generated ever since the dyestuffs were fabricated and recently become one of the largest water
39 defilers in the world. At present, over one hundred thousand of the dyestuffs are daily consumed
40 in industry to color various kinds of materials¹⁻³. Crystal violet (CV) and methylene blue (MB),
41 basic dyes, are used a lot for coloring paper, dyeing cotton, and wools^{2,4,5}. Methyl orange (MO),
42 an acidic dye containing the azo group (N=N), is quite used in the printing, food, pharmaceutical,
43 paper, and textile industries^{2,6}. Both basic and acidic dyes have significant concerns because of
44 their toxicity to aquatic creatures and human beings^{6,7}. But, the basic dyes are more toxic than the
45 acidic dyes, because of their easily interact with negative cell membrane, and/or entrance into
46 living cells and concentrate in the cytoplasm to cause mitotic poison^{4,7}.

47 Adsorption is shown the most effective technique for dye removal because of its easy
48 operation and the ability to treat concentrated dyestuffs with the possibility of regeneration^{1,2,4,7-}
49 ¹⁰. Most of the developed adsorbents in the literature do not have an effective treatment
50 performance for the effluents have multi-dyes (basic and acidic) constituents as industrial cases.
51 More recently, regarding increasing types of water pollutions, the exploitation of multifunctional
52 materials has received enormous attention in research communities. To date, there are a few
53 literature on the preparation of multifunctional materials for dye adsorption and microbial
54 purification. For example, Jiang et al. (2016) studied the application of magnetic chitosan-
55 graphene oxide (MCGO) composite as adsorbent for MO dye (398.08 mg/g) and antibacterial
56 towards *Escherichia coli*. Al-Sagheer et al. (2014) investigated the uptake of different dyes (EBT,
57 MV, and MB) and cytotoxicity against different bacteria and fungi using chitosan-g-poly (N-
58 acryloyl morpholine) copolymer and they noted that the copolymer exhibits greater affinities of
59 acid dye adsorption and antibiological activity towards *E. coli*. However, to the best of our
60 survey, there is no literature to explore the antimicrobial and dye adsorption performance of 4, 5-
61 diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-3-cabonitrile, and protonated carbon nitride (HCN).

62 In view of the above facts, the aim of this work is to fabricate a new multifunctional
63 material for the effective wastewater remediation from multi-dyes (CV, MB, and MO) pollutants
64 with simultaneous antimicrobial properties. As a result, P3C@CaO-HCN multifunctional
65 nanomaterial prepared by the reaction of 4, 5-diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-3-
66 cabonitrile hetero-aromatic with CaO nanoparticles impregnated onto protonated carbon nitride
67 sheet (HCN) was obtained and characterized. Four variables, three-level Box-Behnken design of
68 experiment (BBD-DOE) was applied to investigate the linear and nonlinear influence of the

69 adsorption variables and provides a mathematic equation for optimization of dye adsorption.
70 Kinetic, isotherm, and thermodynamic theories were investigated and statistically validated to
71 understand the rate-controlling steps involved in the adsorption process. The antimicrobial
72 activity of the P3C@CaO-HCN nanocomposite was further tested against three selected
73 microorganisms, including *Escherichia coli*, *Pseudomonas aeruginosa* and *Candida albicans*
74 strains, as widely distribution pathogens in water environments.

75 2. Experimental

76 2.1. Synthesis of 4, 5-diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-3-cabonitrile (P3C)

77 A mixture of 10 mmol 4, 5-diphenyl-2-oxo-2, 5-dihydro-1H-pyrrole-3-cabonitrile ¹² and
78 20 mmol P₂S₅ in 30 ml dry toluene was refluxed for 8h. After that, the solvent was decanted
79 under reduced pressure and the solid obtained was filtered off, washed and then recrystallized
80 from benzene in dark red needles. The obtained reddish crystals of 4, 5-diphenyl-2-thioxo-2, 5-
81 dihydro-1H-pyrrole-3-cabonitrile (yield 60% and m.p 476- 478 K) was labeled as P3C. The
82 characteristics structure of the obtained P3C (thioxo pyrrole derivative) were presented as follow.
83 FTIR (KBr) cm⁻¹: 3350 (NH), 1250 (C=S), 2360 (C≡N). ¹H-NMR (DMSO-d₆): δH (ppm) 2.51
84 (br.s, 1H, NH, exchangeable with D₂O), 4.63 (s, 1H, -CHPh), 7.02-7.77 (m, 10H, ArH). MS, m/z
85 (%): 278 (M⁺, 72), 260 (45), 248 (15), 231 (17), 105 (30), 74 (90), 59 (100). Anal. Calcd. For
86 C₁₇H₁₂N₂S (276.36): C, 73.88; H, 4.38; N, 10.14; S, 11.60. Found: C, 74.01; H, 4.47; N, 9.98;
87 S, 11.82.

88 2.2. Synthesis of g-C₃N₄ and CaO nanomaterials

89 The g-C₃N₄ was prepared by microwave thermal condensation of 20 g urea (99%,
90 Aldrich) in a covered alumina crucible for 1h at 700 watts. The resulting yellow product was then
91 HCl-treated in a quartz reactor containing 1 mol HCl at 348 K under vigorous stirring for 12 h.
92 The protonated product was collected, washed with hot deionized water, and then vacuum dried
93 at 373K and coded as protonated carbon nitride (HCN).

94 Calcium oxide nanoparticles were prepared from eggshells substrate. Typically, the free
95 membrane eggshells were grounded and then purified by dichloromethane in an ultrasonic bath
96 for 2 h at 333 K then filtered and dried at 393K. The powder was then calcined in a microwave
97 oven at 700 watts for 90 minutes and the obtained white powder was coded as CaO nanoparticles.

98 2.3. Fabrication of P3C@CaO-HCN nanocomposite adsorbent

99 The P3C@CaO-HCN nanocomposite was prepared according to the procedure described
100 hereinafter, which was also depicted in Scheme (1). In the first step, a mixture of CaO and HCN
101 (1:3) were completely dispersed in 100 ml ethanol/water solutions placed in 60 Hz ultrasonic bath
102 for 1 h, then aged overnight at 363K under stirring. The CaO-HCN nanocomposite obtained was

103 then collected by centrifugation and calcined at 553K for 2h. In the next step, the CaO-HCN
104 sample was dispersed in 50 mL ethanol/acetic acid anhydrous (1:0.2) solutions and sonicated for
105 30 minutes. To this dispersion, 15 ml ethanol solution of P3C heteroaromatic functionalities was
106 added over 3h, after that, aging for another 36 h at 363 K and stirring speed of 700 rpm. After the
107 reaction stopped, the obtained powder of P3C@CaO-HCN nanocomposite, with nominal ratios of
108 1: 3: 0.5 was collected, washed, and vacuum dried at 363 K.

109 **2.4. Analytical procedures**

110 Melting points were measured on a Gallen Kamp electric melting point apparatus. The
111 ¹H-NMR spectra were run at 300 MHz on a GEMINI 300 BB NMR spectrometer using
112 tetramethylsilane (TMS) in DMSO-d₆ as the internal standard. The mass spectra were recorded on
113 a Shimadzu GC-MS QP-1000EX mass spectrometer operating at 70 eV. FTIR spectra were
114 obtained using KBr disc on a spectrum one Perkin Elmer FT-IR spectrophotometer. The phase
115 structural was determined by X-ray powder diffraction (XRD, Xpert PRO, PAN analytical,
116 Netherlands) at 1.54056° A Cu K α radiation and a D8 Bruker diffractometer (40 kV and 30 mA).
117 A high-resolution transmission electron microscopy (HR-TEM) images were recorded on a JEOL
118 JEM-2, 100 electron microscope at 200 kV accelerating voltage.

119 **2.5. Batch adsorption tests**

120 A stock water solutions of 2000 $\mu\text{mol/l}$ of CV, MB, and MO multi-dyes was first
121 prepared in synthetic wastewater containing 1055 mg/L inorganic dissolved solids similar to the
122 characteristic of previously collected dyestuff industrial wastewater in Egypt (data not shown).
123 All batch adsorption runs were conducted in a 125 mL closed shaking flasks at 150 rpm fixed
124 shaking speed.

125 **2.5.1. Box-Behnken design of experiment (BBD-DOE)**

126 The optimum variables for optimizing P3C@CaO-HCN adsorbent for the adsorption of
127 CV, MB, and MO multi-dyes were set by a rotatable, four-variables, three-level Box–Behnken
128 design (BBD). The three-level independent variables were set as solution pH (X_{pH} =3, 6, 9),
129 composite dose (X_D = 0.5, 1.0, 1.5 g/l), initial dyes concentrations (X_{Co} =200, 600, 1000 $\mu\text{mol/l}$),
130 and solution temperature (X_T =288, 308, 328 K). The levels of independent variables were
131 selected based on our assessment of Al-Gharbia textile industries in Egypt (data not shown). The
132 adsorption capacities (q_e , $\mu\text{mol/g}$) of CV (Y_{CV}), MB (Y_{MB}) and MO (Y_{MO}) dyes by P3C@CaO-
133 HCN were selected as response factors. Based on BBD-DOE design matrix, a total 29 batch
134 experimental runs (runs= $2^4+2*4 + 5$ controlled points) were studied. The 29 BBD-DOE
135 responses results obtained were then analyzed using the MINITAB (v. 17) and Design-Expert (v.

136 7.0.1) software to develop a numerical regression equation to express the relation between the
137 dyes responses and the independent variables under tested conditions.

138 2.5.2. Adsorption studies

139 For statistical BBD-DOE adsorption design, 29 series of lab flasks with the desired level
140 of the variables combination were placed on an orbital shaker and agitated for 24 h. At the
141 optimum BBD-DOE conditions: kinetic, thermodynamic and isotherm studies were conducted.
142 The kinetic and thermodynamic studies were carried out at $X_{Co} = 1000 \mu\text{mol/l}$ initial dyes
143 concentrations with varying temperatures (288 K to 328 K) for ten intervals time up to 24 h. The
144 isotherm test was performed using 10 series of initial dyes concentrations ranging from 50 to
145 1600 $\mu\text{mol/l}$. The other adsorption conditions were set on the basis of the optimum BBD-DOE
146 results obtained. After adsorption processes, the residual dyes concentrations were determined by
147 a double beam UV-visible spectrophotometer in the clear water solutions after centrifugation.
148 Dyes concentrations in the treated wastewater were calculated from the corresponding linear
149 calibration curves for each dye at their λ_{max} values of 586 nm, 668 nm, and 464 nm for CV, MB,
150 and MO, respectively. The dyes removal percentage (Y%) and adsorption capacities ($\mu\text{mol/g}$)
151 were calculated using the following equations (Eqs. 1 -2):

$$152 \quad Y\% = \frac{(C_o - C_t)}{C_o} \times 100 \text{ (Eq. 1)}$$

$$153 \quad q_t = \frac{C_o - C_t}{m} V \text{ (Eq. 2)}$$

154 Where C_o and C_t ($\mu\text{mol/l}$) are the dyes concentrations at initial and t time, respectively, V
155 (L) is the water volume and m (g) is the adsorbent dose.

156 2.6. Statistical models validation and error analysis

157 The adequacy of the simulated models and their validation were assessed using different
158 descriptive statics including a non-parametric Mann–Whitney U-test and a parametric two-sample
159 (unpaired) t-test in accordance with the analysis of variance (ANOVA) at a probability level of
160 0.05⁴. Error statics; including the root mean square error of prediction (RMSEP), the relative
161 standard error of prediction (RSEP), chi-square (X^2) tests, and the average relative error (ARE%)
162 were also calculated to reflect the suitability of the simulated mathematical models to predict the
163 adsorption responses^{4,13,14}. The statistical validation and error studies were checked by using the
164 solver add-in with Microsoft Excel[®]2013, MINITAB (v.17) and IBM-SPSS (v. 21) statistical
165 package for the verification of the results obtained.

$$166 \quad RMSEP = \sqrt{\frac{\sum_{i=1}^N (Y_{pred,i} - Y_{exp,i})^2}{N}} \text{ (Eq. 3)}$$

$$RSEP = \sqrt{\frac{\sum_{i=1}^N (Y_{pred,i} - Y_{exp,i})^2}{\sum_{i=1}^N (Y_{exp,i})^2}} \times 100 \text{ (Eq. 4)}$$

$$X^2 = \sum_{i=1}^N \left| \frac{Y_{exp,i} - Y_{pred,i}}{Y_{exp,i}} \right|^2 \text{ (Eq. 5)}$$

$$ARE\% = \frac{100}{N} \sum_{i=1}^N \left(\frac{Y_{exp,i} - Y_{pred,i}}{Y_{exp,i}} \right) \text{ (Eq. 6)}$$

Where $Y_{pred,i}$ and $Y_{exp,i}$ are the model predicted and experimental response values and N is the number of experimental runs.

3. Results and discussion

Pyrrole is an important heterocycle because its structure is incorporated into many natural products e.g., heme, chlorophyll, vitamin B12, and the bile pigment. Also, the pyrrole ring is present in various drugs, including immunosuppressant, analgesic, anti-tubercular agents, and COX-2 inhibitors. In our earlier investigation¹², 4,5-diphenyl-2-oxo-2,5-dihydro-1H-pyrrole-3-carbonitrile preparation was reported by our research group. In the present work, we have modified the pyrrolone derivatives into its thioxo derivative through converting the oxocarbonyl group (C=O) at position-2 into the thiocarbonyl group (C=S) by reaction with P_2S_5 in dry toluene (Scheme 1) (cf. experimental part). The thiocarbonyl group, which is known to be more electron rich and polarizable than C=O group, existing as a thione/thiol tautomers with the N-H group in the 1H-pyrrole derivative. The presence of the two active functionalities of thiol (-SH) and cyanide (-CN) obtained in the 4, 5-diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-3-carbonitrile (P3C) promoted our interest to construct an active functional component onto CaO-HCN nanocomposite through thiol group. This resulting in the formation of a strong S-O bond on the CaO-HCN nanocomposite surface and free cyanide (-C≡N) group as confirmed by the FTIR (cf. 3.1 part). The developed P3C@CaO-HCN showed multifunctional application for the adsorption of CV, MB, and MO organic dyes and wastewater purification from microbial pathogens because of the free cyanide group as described hereinafter and depicted in Scheme (1).

3.1. Structure characterization of the P3C@CaO-HCN

XRD spectra are used to test the phase structures and purity of the samples. The set of XRD diffraction peaks (Fig. 1a) shows the pure crystal phases of CaO NPs ($2\theta=18.10^\circ$, 32.3° , 37.4° , 53.90° , 64.20° , and 67.40°) and g- C_3N_4 (HCN) ($2\theta=13^\circ$ and 27.4°) with no more other impurities peaks. For CaO-HCN hybrid nanocomposite, the XRD patterns assigned for both CaO NPs and g- C_3N_4 were beside a minor amount of $Ca(OH)_2$ phase resulted during CaO impregnation in the water atmosphere. The HCN peak at 27.4° (0 0 2) become weaker, which was the result from restraining the stacking of HCN perpendicular to the 0 0 2 directions, the graphitic

198 stacking of the conjugated aromatic system, owing to introducing CaO NPs¹⁵. These results
199 imply that CaO NPs deposit on the surface of HCN sheet and not incorporate into the HCN lattice
200^{15,16}. Also, The XRD data showed that microwave thermal method is sufficient to achieve
201 complete thermal decomposition of carbonate in eggshells to pure CaO phase and thermal
202 condensation of urea to graphitic carbon nitride (g-C₃N₄). The determined crystallite size of the
203 prepared CaO/g-C₃N₄ sample using the Scherrer formula¹⁷ at 2 Θ = 37.4° computed as 65.6 nm
204 compared to CaO NPs crystal size of 58.42 nm.

205 The FTIR of functional P3C@CaO-HCN nanocomposite (Fig. 1b) showed similar
206 characteristic features to their starting components with a slight red shift to a higher wavenumber
207 compared to HCN, CaO NPs, and P3C materials. A band ranging from 3000-3600 cm⁻¹ is
208 originated from the vibration modes of the free N-H (pyrrole group) and the O-H of adsorbed
209 H₂O by CaO NPs. The sharp breathing vibration band at ca. 810 cm⁻¹ is assigned to the g-C₃N₄
210 tri-s-triazine units¹⁸. Absorption bands in the region between 1200–1700 cm⁻¹ are corresponding
211 to the skeletal C–N heterocycles stretches, comprising trigonal (N–(C)₃) and bridging C–NH–C
212 units of the extended C-N-C network at g-C₃N₄¹⁸. In contrary, the decreased of the intensive
213 bands at ca. 3600 cm⁻¹ (O-H) and ca. 500 cm⁻¹ (Ca-O vibration) in P3C@CaO-HCN compared to
214 starting components is a sign for P3C formation complexation on the CaO NPs surface rather
215 than HCN. The disappear of C=S thiocarbonyl stretch band at ca. 1250 cm⁻¹ (P3C) and appear of
216 the band at ca.760 cm⁻¹ and 1015 cm⁻¹ ascribed to S-O stretching bonds (P3C@CaO-HCN)
217 between P3C functionalities and Ca-O through thiol groups. Observation results suggest that the
218 strengthening interaction bonds in the resultant P3C@CaO-HCN nanocomposite sample during
219 self-assembly preparation approach.

220 The P3C@CaO-HCN morphological structure was examined using HRTEM image
221 shown in Fig. 2a. HRTEM image showed spherical CaO NPs incorporated with both de-
222 agglomerated and agglomerated distribution on the smooth surface of HCN with an average
223 diameter of 60.7 nm. Also, HCN displayed a platelet-like morphology and a two-dimensional
224 sheet structure. The pH zero point charge (pH_{ZPC}) of HCN, CaO NPs, and P3C@CaO-HCN
225 samples were determined by both potentiometric mass titration and salt addition methods after 24
226 h of equilibration¹⁹. The resultant pH values using a pH meter model Mettler Toledo (Seven Go,
227 IP67) are plotted in Fig. 2b. A significant change in the pH_{ZPC} surface charge properties was
228 observed, which is calculated as 5.09, 10.52, and 5.82 for HCN, CaO NPs, and P3C@CaO-HCN,
229 respectively.

230 3.2. Statistical modeling and optimization of the adsorption variables by RSM method

231 3.2.1. Statistical model simulation

232 The three-level BBD-DOE approach was adopted for studying the linear and
 233 simultaneous effects of the four adsorption variables to enhance the adsorption properties of
 234 P3C@CaO-HCN. Based on BBD-DOE experiments, the obtained minimum and maximum
 235 responses were found to be between 110.8-1013.9 $\mu\text{mol/g}$, 116.5-1455.8 $\mu\text{mol/g}$, and 69.7-1007.9
 236 $\mu\text{mol/g}$ for MB, and MO dyes, respectively. The BBD coupled with DOE analysis suggests the
 237 nonlinear polynomial regression model (Eq. 8) as the best-fitted expression between the dyes
 238 responses and the coded variables (X_{pH}, X_D, X_{Co}, X_T) with β as the regression coefficient term.

$$239 Y = \beta_0 + \beta_1 X_{pH} + \beta_2 X_D + \beta_3 X_{Co} + \beta_4 X_T + \beta_{12} X_{pH} X_D + \beta_{13} X_{pH} X_{Co} + \beta_{14} X_{pH} X_T + \beta_{23} X_D X_{Co} + \\ 240 \beta_{24} X_D X_T + \beta_{34} X_{Co} X_T + \beta_{11} X_{pH}^2 + \beta_{22} X_D^2 + \beta_{33} X_{Co}^2 + \beta_{44} X_T^2 \text{ (Eq. 7)}$$

241 The quality of the polynomial equation (Eq. 7) was confirmed by the high correlation
 242 coefficients (R_{Adj}^2 0.997-0.991 and R_{Pred}^2 0.996-0.989), which are close to unity with high
 243 accuracy of approximation ($R^2=0.998$). A low significant error deviation in the conducted design
 244 further confirmed the suitability of the developed equation to fit the CV, MB, and MO adsorption
 245 responses. The RMSEP of 9.1, 14.04, and 11.83, RSEP of 18.63%, 25.36%, and 32.89% and
 246 calculated χ^2 values of 7.68, 15.29 and 16.07 less than critical χ^2 ($\chi_{\alpha,(n-1)}^2$)41.34) were calculated
 247 for CV, MB, and MO adsorption responses, respectively. The statics low coefficient of variation
 248 (C.V. of 2.92%-3.72%) and adequate precision ratio of 82.65-97.99 greater than 4⁴, show an
 249 adequate signal for the polynomial equation (Eq. 7) to predict the dyes responses data. Moreover,
 250 the ANOVA results listed in Table (1) also indicated that the polynomial equation is significant.
 251 This is evident from the Student t-test ($t_{model}=56.76-75.81 >> t_{crit}$ 2.049) and Fisher's F-test
 252 ($F_{model} = 447.33-626.28 >> F_{crit} = F_{0.05,df,(n-df+1)} = 2.484$) with a low probability value (p_{model}
 253 < 0.0001). Thus, the simulated model can be efficiently used in optimization of dyes adsorption.

254 3.2.2. Effects of model components on dyes adsorption efficiencies

255 The influence of the model components and their coefficient terms (β) on the studied
 256 dyes adsorption were tested by ANOVA tools listed in Table 1. Statistical F_{Calc} , t_{Calc} and p-tools
 257 adopted that the linear model components showed high significant effects on dyes responses than
 258 their respective interactive and quadratic effects (Table 1). The results were reflected also by the
 259 estimated β values and the percent contribution (PC %) tabulated in Table 2. As seen, the linear
 260 components represented the highest influence level with a total PC% of 90.1%, 86.2%, and
 261 85.2%; but, the quadratic components showed the lowest contribution with a total PC% of 4.2%,
 262 4.6% and 4.8% for the CV, MB, and MO dyes adsorption, respectively. In general, the influential
 263 level of linear components can arrange as initial dyes concentrations ($X_{Co}=44.8\%$, 46.2%, and
 264 42.6%) > composite dose ($X_D=35.4\%$, 36.97%, and 29.5%) > solution pH ($X_{pH}=8.2\%$, 2.7%, and

265 12.6%) > temperature ($X_T=1.7\%$, 0.36%, and 0.47%) on the dyes adsorption responses. Among
266 the equation components, the interaction term of $X_D * X_T$ (PC%=0.001-0.05%; $p=0.071-0.541$)
267 and quadratic temperature term (X_T^2 , PC%=0.001-0.02%; $p=0.236-0.984$) showed the lowest
268 influential effect on the dyes adsorption. As a fact, the coefficient sign determines the effect
269 direction on the studied responses^{4,13,20}. The estimated coefficient values (Table 2) showed that
270 the X_D exhibited unfavorable or antagonistic effect (negative sign) on the dyes responses and pH
271 variable (X_{pH}) on MO response. But the other variables showed positive coefficients terms
272 (synergistic effect) along with X_{pH} on both CV and MB adsorption responses.

273 3.2.3. BBD-DOE optimization of adsorption process

274 The three-dimensional (3D) response surface contour plots are more helpful in
275 facilitating the straightforward investigation of the experimental variables on the dyes responses
276^{4,20}. Based on the simulated polynomial equation (Eq. 7), the 3D contour plots for the CV, MB
277 and MO responses (q_e , $\mu\text{mol/g}$) are visualized in Fig (3). The 3D plots of $X_{pH} * X_D$ interactive
278 term (Fig. 3a) showed that the P3C@CaO-HCN dose (X_D) exhibits an inverse influential effect
279 on adsorption capacity, whereas the effect of solution pH is depends on the adsorbed dyes type.
280 The q_e ($\mu\text{mol/g}$) of the basic CV and MB dyes increase with an increase in the entire pH range up
281 to pH 7.5. While acidic MO dye adsorption capacity is higher at the median pH level of ≈ 6 and
282 decreased at both very low and high pH levels. The pH-adsorption dependent suggested that the
283 P3C@CaO-HCN adsorption mechanism is a complex interplay between electrostatic and non-
284 electrostatic forces based on solution pH, pH_{ZPC} of the adsorbent and pka of dyes molecules
285 (Scheme 1& cf. adsorption mechanism hereinafter). Because of hydrogen and hydroxyl ions are
286 quite adsorbed on the surface sites and therefore the adsorption of dyes molecules is affected by
287 the pH of the water. In addition, the solution pH affects the degree of adsorbent surface charge
288 through protonation or deprotonation of functional groups on the adsorbent surface active sites
289 and ionization of organic dyes pollutants.

290 The interactive effect of $X_{Co} * X_D$ on dyes adsorption (Fig. 3b) showed that the X_{Co} has a
291 synergetic effect on the q_e ($\mu\text{mol/g}$) responses with decreasing the X_D level^{4,20}. This trend is
292 explained by assuming that the saturation of the all binding sites on the P3C@CaO-HCN surface
293 is attained at the low X_D level of 0.5 g/l. However, with increase X_D level, a higher number of
294 binding sites would generate that decrease the q_e ($\mu\text{mol/g}$) responses due to a vacant surface site
295 that still unoccupied (equilibrium state not reached). The combined effect of $X_{Co} * X_T$ (Fig. 3c)
296 showed that the temperature variable has a low synergetic influence on the dyes responses with
297 parallel contour lines and no interaction with X_{Co} . This finding suggests that the experimental

298 temperature levels possess lower significant influence on dyes responses (q_e , $\mu\text{mol/g}$), which is
299 confirmed by its lowest linear effect ratio of 91.59, 55.23 and 54.63 for CV, MB, and MO
300 adsorption, respectively (Table 2).

301 In general, the results above revealed that the prepared P3C@CaO-HCN adsorbent has
302 higher dyes adsorption capacities. Which is evident from an increase of q_e to 869.18, 1215.1, and
303 905.8 $\mu\text{mol/g}$ for CV, MB, and MO, respectively at the adsorbent dose <0.75 g/l and increase X_{Co}
304 up to 900 $\mu\text{mol/l}$. Consequently, the maximum operating conditions for the applied application
305 were set by solving the developed polynomial regression model (Eq. 7) on the basis of BBD-DOE
306 and the input variables levels with their linear, quadratic and interaction terms obtained. The
307 predicted optimal variables levels at $X_{Co}=1000$ $\mu\text{mol/l}$ were then computed as 5.9 pH, 0.5g/l
308 P3C@CaO-HN sorbent, and 307 K solution temperature with desirability level of 0.96. At those
309 optimum conditions, the maximum CV, MB, and MO predicted $q_e(\mu\text{mol/g})$ were 1013.9, 1418,
310 and 1062.1, which are close to the experimental $q_e(\mu\text{mol/g})$ of 1018.2, 1429.5, and 1053.8,
311 respectively.

312 3.3. Adsorption kinetics and thermodynamics

313 The effect of adsorption contact times on the dyes adsorption performance of P3C@CaO-
314 HCN at temperature ranges from 288K to 328 K are shown in Fig (4). As seen, the dyes
315 adsorption appear rapid rising at the first 4 h followed by gradual decrease up to equilibrium
316 flattening rates starting at 6 h. Temperature also showed a low synergetic influence in the
317 adsorbed amount ($q_{e,exp}$, entire set of Fig. 4a) with calculated t_{calc} value of 15.62-8.01, 7.18-
318 5.38, and 8.21-5.62 and p-value range from 0.034 to 0.043 for CV, MB, and MO, respectively. To
319 determine the adsorption mechanism, five kinetic models including pseudo-first-order model
320 (PFOM), pseudo-second-order model (PSOM), Elovich, fractal like-pseudo first order (FL-
321 PFOM), and mixed first and second-orders (MOE) kinetic models²¹⁻²⁴ were applied to simulate
322 the dyes adsorption curvatures. Kinetic results and their corresponding mathematical model
323 formula are listed in Table 3. According to the coefficients (R^2) and the resemblance between
324 $q_{e,theo}$ and $q_{e,exp}$ values in Table (3), the dye adsorption data can be interpreted by FL-PFOM and
325 MOE kinetic expressions. A good fit mathematical equation does not depend only on the R^2 , but it
326 should be also accurate in predicting the experimental data. The good fitness to the FL-PFO and
327 MOE mathematical models (Fig.4a) imply that the overall rate of dyes adsorption is time
328 dependent on heterogenous sites on P3C@CaO-HCN surface that changing the adsorption
329 behavior with the lapse of time^{22,24}.

330 The surface diffusion and intra-particle diffusion models such as the Boyd model and
331 Weber and Morris (WMM) theory were further studied to determine the diffusion mechanism
332 ^{23,25}. Application of WMM model (Fig. 4b) showed two-linearity adsorption stages. In the initial
333 macro-pore diffusion phase I (R_1^2 0.902-0.991), most obtainable P3C@CaO-HCN adsorbing sites
334 were utilized by 80- 90% of adsorbed dyes within $2.45h^{0.5} \approx 6$ h. The second micro-pore
335 diffusion phase II (R_2^2 0.857-0.983) is attributed to a slow diffusion generated with the lapse of
336 time. As seen in (Fig. 4b), the WMM empirical relationship stated that the intra-particle diffusion
337 is not the rate-factor due to the two phases (I and II) lines do not pass through the origin.
338 Diffusion rate constant of K_t ($\mu\text{mol g}^{-1} \text{h}^{0.5}$) were found to be exhibit a low significant dependent
339 on the studied temperature ranges. Additionally, the Boyd model also showed that the calculated
340 B_t points, the time coordinate of Boyd's expression, were scattered around the linear lines with
341 good correlations values R^2 of 0.85-0.97 for dye adsorption (Fig. 4c). But, the linear lines of
342 Boyd's curves (Fig. 4c) for the adsorbed dyes passing through the origin, which ascertained that
343 the adsorption rates on P3C@CaO-HCN are governed by an initial boundary layer resistance and
344 film diffusion mechanism.

345 The low significant effect of temperature levels (288 to 328 K) above was confirmed by
346 the calculated thermodynamic constants using the Van't Hoff formula ^{21,26,27} at $C_0=1000$ $\mu\text{mol/l}$.
347 The calculated positive enthalpy changes ($\Delta H^\circ=8.58, 6.43, \text{ and } 6.17$ KJ/mol) and entropy changes
348 ($\Delta S^\circ=0.034, 0.034 \text{ and } 0.027$ KJ/mol) for CV, MB, and MO adsorbed dye show endothermic
349 adsorption, which is consistent with the kinetics and BBD-DOE results. The low magnitude of
350 calculated ΔH° , less than 20.9 kJ/mol, reveal that the adsorption is non-electrostatic physical type
351 at optimum conditions ^{21,26}. In addition, the determined Gibb's free energy changes (ΔG°) for CV,
352 MB, and MO dyes are $\leftarrow 1.26$ to $\leftarrow 2.62$ KJ/mol, $\leftarrow 3.46$ to $\leftarrow 4.49$ KJ/mol, and $\leftarrow 1.70$ to $\leftarrow 2.51$
353 KJ/mol at 288 K to 328 K, respectively. The negative values of ΔG° suggests spontaneity and
354 feasibility of favorable adsorption by P3C@CaO-HCN. This kind of low significant temperature
355 dependence of the adsorbed dyes by P3C@CaO-HCN adsorbent reflect the film diffusion
356 mechanism of dye into the adsorbent.

357 3.4. Equilibrium isotherm studies

358 The isotherm provides information on how dyes adsorption and the commercial viability
359 of the P3C@CaO-HCN materials for the adsorption application. A nonlinear regression solving
360 of Langmuir, Tempkin, Freundlich, Redlich–Peterson, and Dubinin–Radushkevich isotherm
361 models ^{21,26,27} were applied to simulate the equilibrium dyes adsorption results. The simulated
362 nonlinear isotherm expressions for the adsorbed dyes by P3C@CaO-HCN and their coefficients

363 R^2 values are tabulated in Table 4. According to the determined coefficient R^2 value, R-P
364 isotherm ($R^2 > 0.99$) showed best-fitting of dye adsorption data and poorest-fitting to D-R model
365 ($R^2 = 0.92 - 0.87$). The R-P isotherm is a mix of Langmuir–Freundlich equations, and the R-P
366 exponent constant ($0 < b < 1$) can characterize the adsorption isotherm favorability²⁶. Tabulated
367 isotherm expressions (Table 4) and their graphical representations in Fig. 4d showed that the
368 Langmuir is the preferable isotherm ($R^2 = 0.99$) for CV and MO adsorption ($b = 0.86$ and 0.95);
369 whereas MB adsorption obeys the Freundlich isotherm ($R^2 = 0.99$ and $b = 0.59$). The dimensionless
370 separation factor, R_L of 0.06–0.15 at $C_o = 1000 \mu\text{mol/l}$, and Freundlich n exponent factor ($n = 2.32$ –
371 3.03) further confirmed favorable adsorption isotherm by P3C@CaO-HCN. Isotherm data shows
372 that the P3C@CaO-HCN characterized by a certain degree of a heterogeneity binding sites
373 ($B_T = 239.02$ – 259.14 J/mol) as further revealed by Tempkin model ($R^2 = 0.94$ – 0.98)^{26,27}. Fig. (4d)
374 also shows that the adsorption capacity of dye sharply increase to reach a plateau of maximum
375 equilibrium trend at initial concentrations of $1200 \mu\text{mol/l}$ CV, $1450 \mu\text{mol/l}$ MB, and $1100 \mu\text{mol/l}$
376 MO dye. At these concentration points, the maximum experimental q_e ($\mu\text{mol/g}$) were recorded as
377 1227.8 , 1915.8 , and $1221 \mu\text{mol/g}$ for CV, MB, and MO dye, respectively.

378 3.5. Adsorption Mechanism

379 Regarding the resultant data above, it can be suggested that the high performance of the
380 P3C@CaO-HCN adsorbent toward both basic and acidic dyes (CV, MB and MO) adsorbates may
381 be ascribed to a complex adsorption interactions. In addition, the adsorption interactions showed
382 low B_T and ΔH° binding energy with a heterogeneity binding sites including electrostatic and
383 non-electrostatic mechanisms, and its rate-controlling is a pH-dependent.

384 Herein, the potential mechanism involved was expected to be related to the electrostatic
385 interaction as the predominant force at high and low pH levels. With increase $\text{pH} > \text{pH}_{ZPC}$ (5.82),
386 the CV and MB basic dyes adsorption were enhanced due to electrostatic forces developed
387 between acidic surface sites of P3C@CaO-HCN and positive charge density of CV and MB
388 cations, which is unfavorable for the adsorption of MO acidic dye due to the electrostatic
389 repulsion^{4,28–30}. In this case, it can be said that the adsorption of cationic dyes is fine and can more
390 easily take place when usage of alkaline pH. At high acidic condition ($\text{pH} < 4$), the adsorption
391 capacities of basic (CV and MB) and acidic (MO) dyes decreased, because of the higher number
392 of protonation H^+ levels. The high concentrations of positive H^+ ions associate to the
393 P3C@CaO-HCN surface and form positively protonated surface sites. The developed protonated
394 surface generate electrostatic repulsion with basic CV and MB cations and hydronium counter
395 ions around acidic MO anions (SO_3^-) in the bulk water solution, leading to decrease their

396 adsorption capacity. Similar observation was recorded at a high alkaline pH ($\text{pH} > 8$) because of a
397 relatively higher number of HO^- groups in solution. In fact, such electrostatic interaction
398 mechanism is possible between the electron pairs of N-H group in the 1H-pyrrole derivative of
399 the P3C functionalities or tri-s-triazine units (bridging C–NH–C units) of HCN. Otherwise, at
400 near neutral $\text{pH} \approx 6$ approximately equal pH_{ZPC} (5.82) $>$ pK_a of CV ($\text{pK}_a=5.31$), MB ($\text{pK}_a=3.8$)
401 and MO ($\text{pK}_a=3.47$), the main predominant mechanism could be controlled by non-electrostatic
402 attraction forces. Such non-electrostatic interactions could including π - π stacking interaction and
403 hydrophobic-hydrophobic mechanisms, which could be more favored for MO anionic dye. At
404 which, the π - π adsorption mechanism can developed between the π -orbitals in the aromatic ring
405 of dye molecules and delocalized π -electrons of the C=C double bonds of HCN nanosheets or
406 aromatic binding sites on the P3C functional surface of adsorbents. P3C@CaO-HCN can also
407 interact with dye molecules via hydrophobic-hydrophobic mechanism between the di-phenyl
408 groups in the pyrrolone derivatives of P3C functionality at positions 4 and 5 of 1H-pyrrole
409 derivative and aromatic rings of dye molecules. This is worthwhile to point out that the
410 P3C@Cao-HCN is effective adsorbent in the adsorption removal of both cationic and anionic
411 organic dyes with counter charges.

412 3.6. Models validation and error analysis

413 Statistical error parameters for the best-fitted models were computed in this work to
414 confirm the suitability of the overall simulated kinetic (FL-PFO and MOE) and isotherm
415 (Langmuir, Freundlich, and R-P) mathematical expressions to the experimental results. First, a
416 non-parametric Mann–Whitney U-test, a parametric (unpaired) t-test and one-way ANOVA were
417 conducted to test significance difference between the experimental (Y_{exp}) and the predicted
418 (Y_{pred}) dyes adsorption capacities⁴. The calculated Mann–Whitney z-score of 0.75-0.04, less
419 than unity, associated with the two-tailed p-value of 0.59-0.987 greater than the chosen level of
420 $p=0.05$ (95% confidence) imply the suitability of the above selected fitted expressions. Also, the
421 calculated statistic tools from one-way ANOVA were found to be in the range of $t_{\text{cal}}=0.001-0.39$
422 and $F_{\text{cal}}=0.0001-0.31$, which are lower than the critical values of $t_{\text{crit}}=\pm 2.41$, and $F_{\text{crit}}= 3.73$.
423 Second, the experimental and predicted output response variables (q_e , $\mu\text{mol/g}$) for each set of
424 validation points were used to compute the Chi-square (χ^2), RSEP, RMSEP, and %ARE error
425 values. Notably, a low error results were recorded using RMSEP (2.08 -2.81), RSEP (1.12- 2.13),
426 % ARE (2.17%-4.65%), and χ^2 (0.13-0.15 \ll critical $\chi_{\alpha, (df=n-1)}^2$ of 16.92) with a high
427 correlation ($R^2 = 0.992$ to 0.999) between Y_{exp} and Y_{pred} . In this case, at 95% certainty, the
428 experimental dyes adsorption results by P3C@CaoO-HCN were well described by the fitted

429 mathematical expressions above under the calculated statics with the lowest error and the
430 significant difference between the two set of output responses (Y_{pred} and Y_{exp})⁴.

431 3.7. Antimicrobial activity

432 The synthesized P3C@CaO-HCN nanocomposite was further screened for its in vitro
433 antimicrobial activity against three free-living pathogenic strains of *Escherichia coli* and
434 *Pseudomonas aeruginosa* bacterial and *Candida albicans* yeast. Luria-Bertani (LB) broth
435 containing different concentrations of P3C@CaO-HCN (C_o = 100, 250, 500, 1000, and 2500
436 mg/l) and 10^5 CFU/ml initial pathogenic cell was used to test the antimicrobial activity at 310 K
437 and 150 rpm shaking speed. An inhibitory percentage rate (I%, Eq. 9) at the mid-exponential
438 microbial growth was measured against microbial culture blank as a positive control.

439

$$440 \quad I\% = \frac{(CFU_{PC} - CFU_{ACo})}{CFU_{PC}} \times 100 \text{ (Eq. 9)}$$

441 Where, CFU_{PC} and CFU_{ACo} are the total strains colony forming unit (CFU/ml) in the
442 absence and presence of composite, respectively. The inhibitory rate (I%) of P3C@CaO-HCN
443 against *E. coli*, *P. aeruginosa* and *C. albicans* pathogens is shown in Fig (5). It is seen that the
444 cytotoxicity effect toward the three pathogens was increased with the increasing concentration of
445 P3C@CaO-HCN. The visualized reduced of cell viability was escalated with *E. coli* compared to
446 *P. aeruginosa* and *C. albicans* at given concentrations, which implied that the antimicrobial
447 activity of P3C@CaO-HCN was not only P3C@CaO-HCN dependent but also microbial
448 dependent. As shown in Fig (5), the P3C@CaO-HCN loaded cultures also exhibited a high
449 significant antimicrobial activity with reduction percentage on *E. coli* (93.5%) and *C. albicans*
450 (85.8%) compared to a moderate I% against *P. aeruginosa* (61.54%) at C_o of 2500 mg/l
451 P3C@CaO-HCN. Also, the P3C@CaO-HCN showed minimum inhibitory concentration (MIC)
452 at 500 mg/l with I% of 87.9%, 46.9%, and 72.5% for *E. coli*, *P. aeruginosa*, and *C. albicans*,
453 respectively. Lossing microbial viability may result from the free cyanide ($C\equiv N$) group on 4, 5-
454 diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-3-carbonitrile functionality and protonated g- C_3N_4
455 (HCN) sheet. The composite provide electrostatic adsorption of a negatively charged microbial
456 surface onto positive HCN sheet, and subsequently, the free $C\equiv N$ functionalities tightly bound to
457 ubiquinone whole cells (Scheme 1). This may lead to induce microbial membrane stress and
458 hence disrupting their metabolic system that leading to cell death^{10,11}.

459 4. Conclusions

460 In this work, P3C@Cao-HCN nanocomposite, a new multi-functional nanomaterial, was
461 fabricated for wastewater remediation from organic dye and microbial contaminants. The

462 P3C@Cao-HCN was prepared by the reaction of 4, 5-diphenyl-2-thioxo-2, 5-dihydro-1H-pyrrole-
463 3-cabonitrile with CaO nanoparticles impregnated onto protonated carbon nitride (HCN).
464 Adsorption experiment of CV, MB, and MO organic dye using Box-Behnken design outlined that
465 the adsorption mechanism of P3C@Cao-HCN depends on the molecular dye structure and the
466 adsorbate surface aspect, which varies with solution pH level. The adsorption data was fitted with
467 both the fractal like-pseudo first-order (FL-PFOM), and mixed first and second-orders (MOE)
468 kinetic models and Redlich–Peterson (R-P) isotherm well. The validation data confirmed the high
469 suitability of the selected models to simulate the adsorption data ($R^2 > 0.99$, RMSEP ≤ 2.81 , RSEP
470 ≤ 2.13 , % ARE $\leq 4.65\%$, and $x^2 \leq 0.15$ less than critical $x_{\alpha, (df=n-1)}^2$ of 16.92) at the probability
471 level of 0.05. P3C@CaO-HCN proved to be a suitable novel antimicrobial nanomaterial against
472 *E. coli* and *P. aeruginosa* and *C. albicans* pathogens in this work for the first time. The inhibition
473 rates (I%) of 87.9%, 46.9%, and 72.5% were attained at MIC of 500 mg/l P3C@CaO-HCN for *E.*
474 *coli*, *P. aeruginosa*, and *C. albicans*, respectively due to damaging of microbial membrane by the
475 free cyanide (C≡N) functionality and protonated g-C₃N₄ (HCN) sheet. The notable high dye
476 adsorption capacity and antimicrobial activity by P3C@CaO-HCN offers its promising
477 applications for industrial wastewater remediation and management.

478 5. References

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528 Figure Captions

529 Fig. 1: a) XRD patterns (CaO NPs, HCN, and CaO-HCN) and (b) FT-IR spectra of (i) P3C, (ii)
530 CaO NPs, (iii) HCN, (iv) CaO-HCN, and (v) P3C@CaO-HCN.

531 Fig. 2: a) TEM image of P3C@CaO-HCN composite, and b) The pH_{ZPC} determination by
532 potentiometric and salt addition methods.

533 Fig. 3: 3D response surface contour plots of CV, MB, and MO dyes adsorption capacities versus
534 interaction of: (a) pH and adsorbent dose ($X_{pH}X_D$), (b) initial dyes concentrations and adsorbent
535 dose ($X_{Co}X_D$), and (c) initial dyes concentrations and temperature ($X_{Co}X_T$).

536 Fig. 4: (a) Effect of contact time on P3C@CaO-HCN adsorption capacities (b) Intra-particle
537 diffusion model; (c) Boyed surface diffusion model; and (d) isotherm models of CV, MB, and
538 MO adsorptions.

539 Fig. 5: Antimicrobial activity of P3C@CaO-HCN against *E. coli*, *P. aeruginosa* and *C. albicans*
540 microbial pathogen

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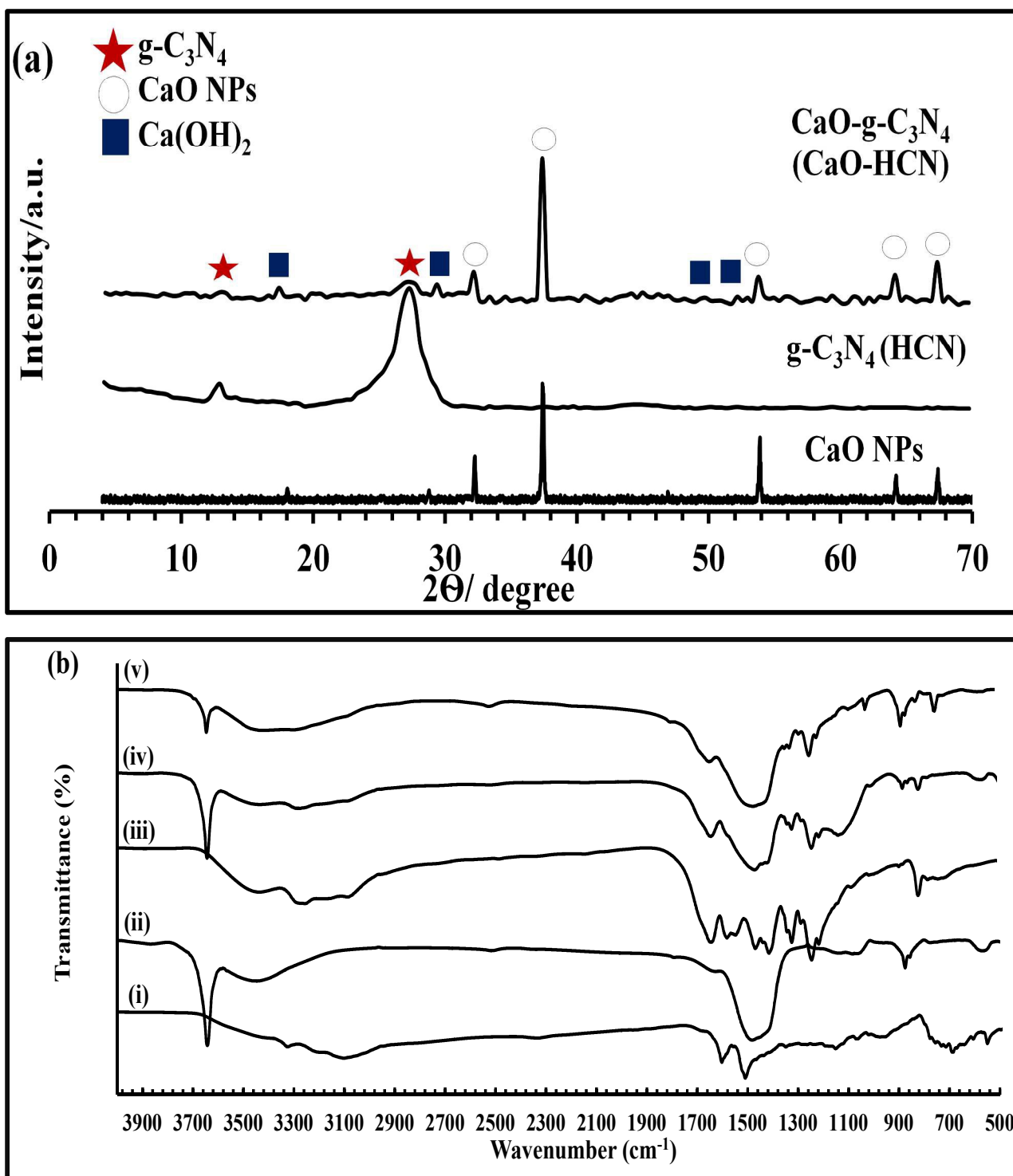


Fig. 1: a) XRD patterns (CaO NPs, HCN, and CaO-HCN) and (b) FT-IR spectra of (i) P3C, (ii) CaO NPs, (iii) HCN, (iv) CaO-HCN, and (v) P3C@CaO-HCN.

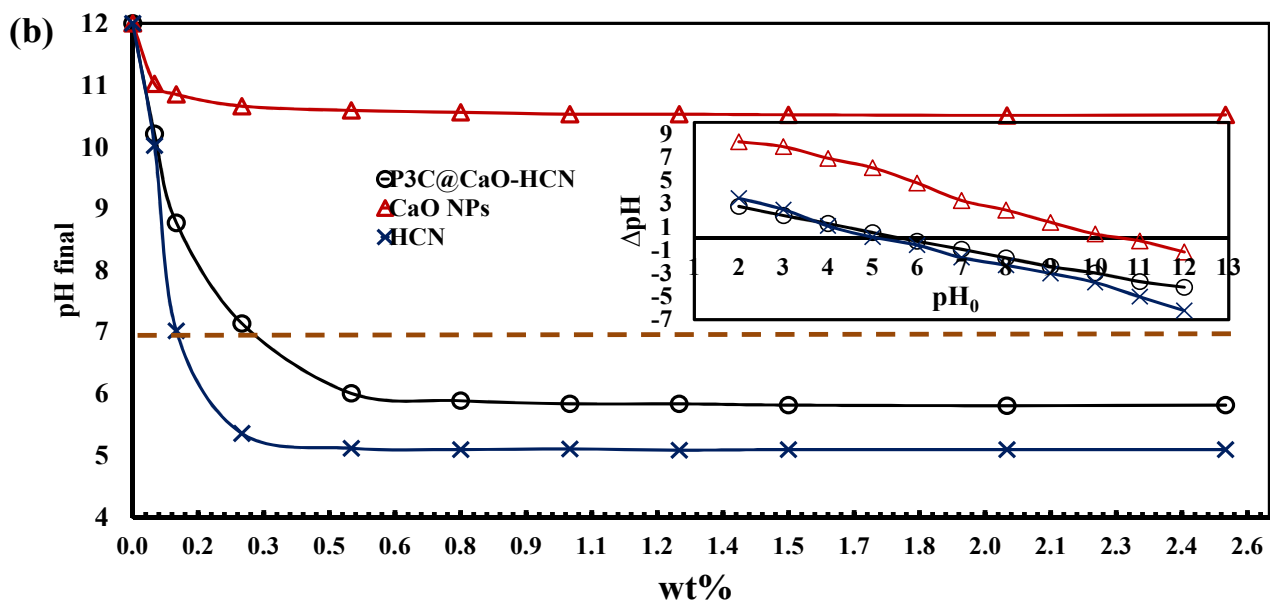
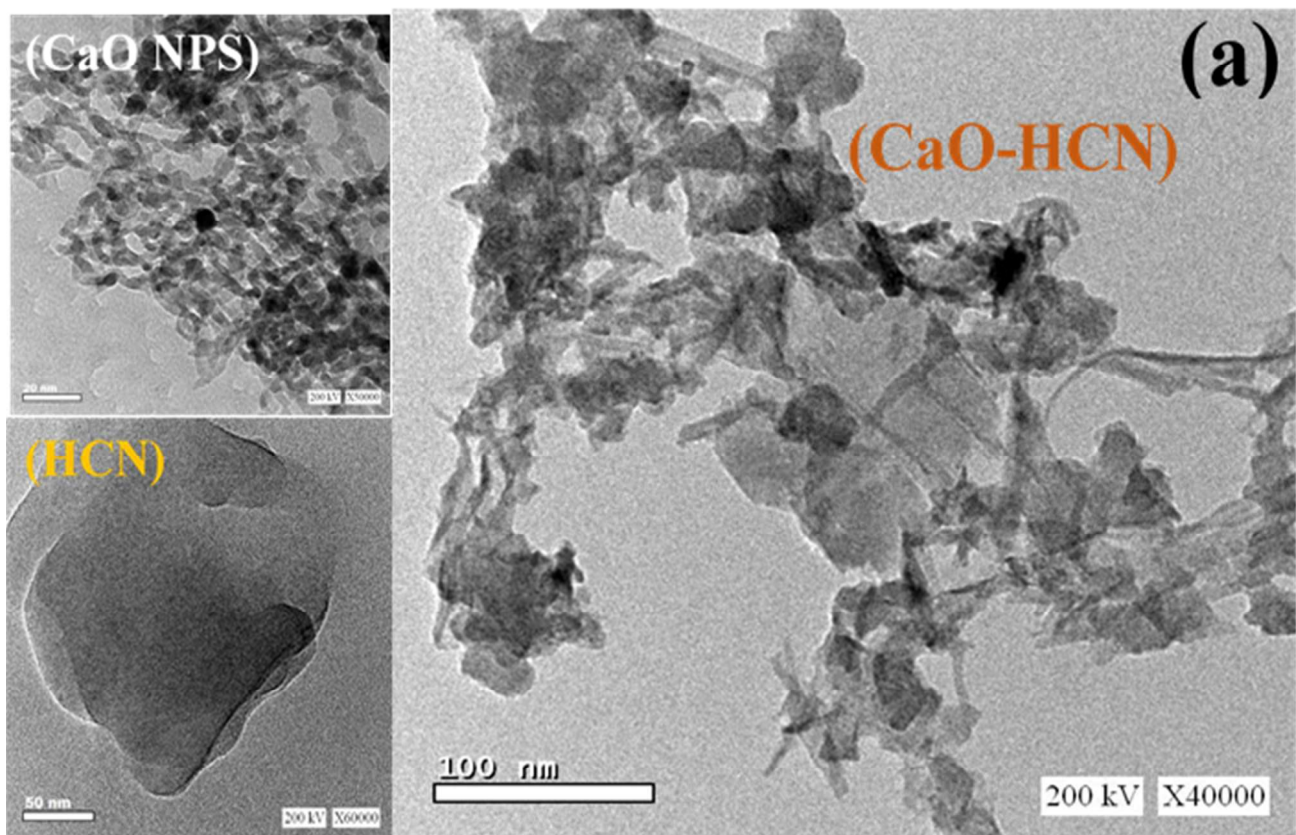


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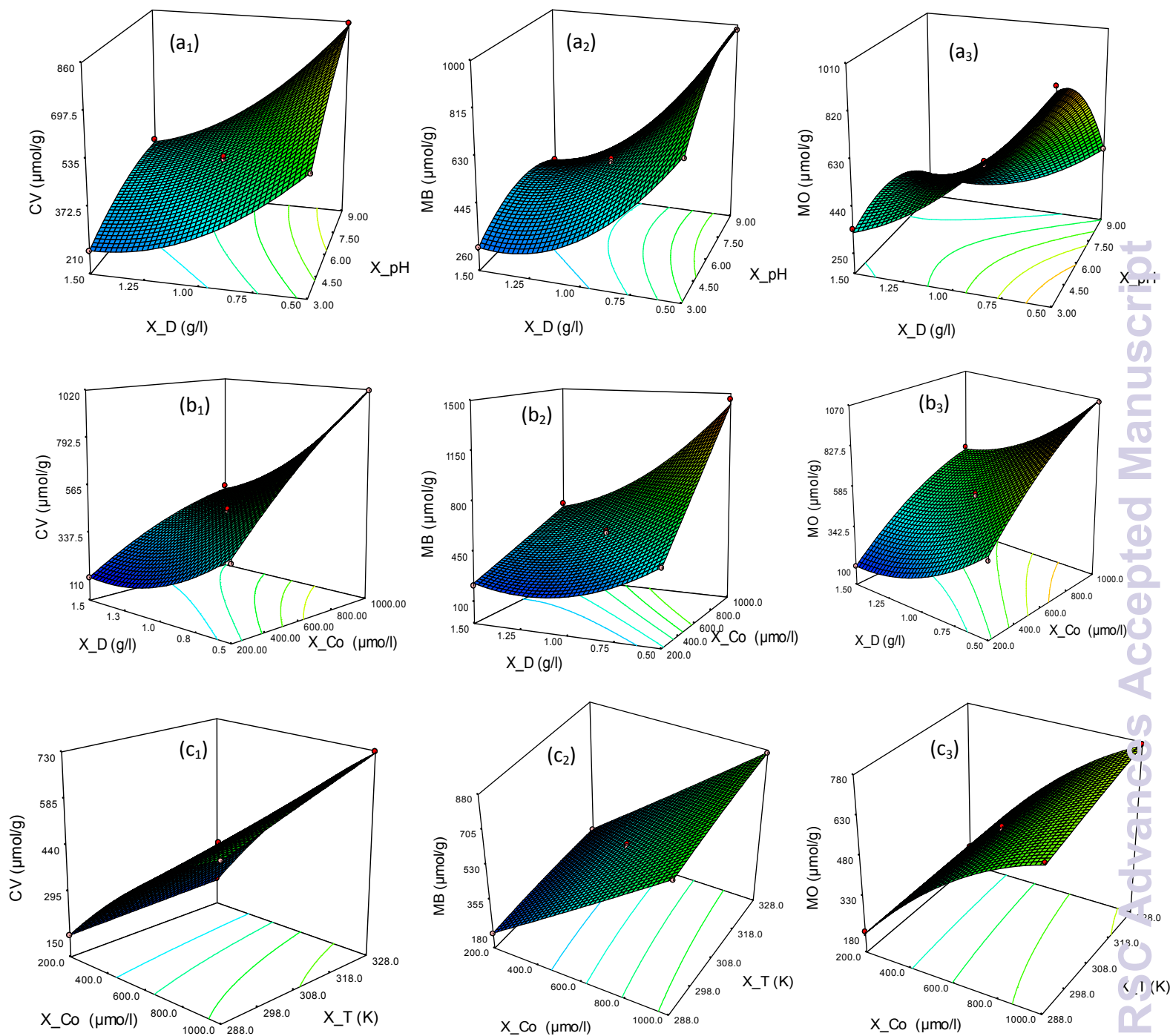


Fig. 3: 3D response surface contour plots of CV, MB, and MO dyes adsorption capacities versus interaction of: (a) pH and adsorbent dose ($X_{pH}X_D$), (b) initial dyes concentrations and adsorbent dose ($X_{Co}X_D$), and (c) initial dyes concentrations and temperature ($X_{Co}X_T$).

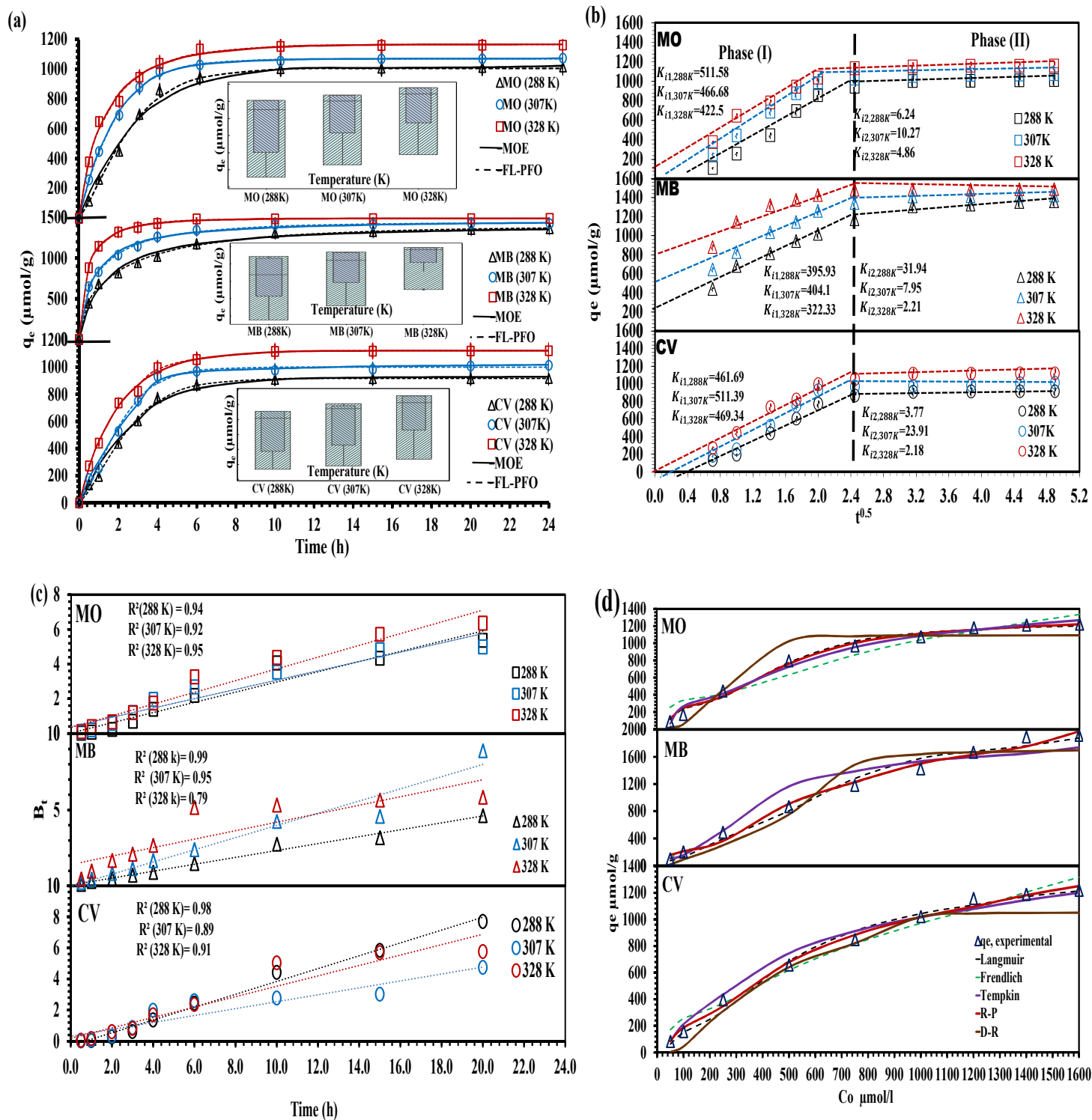


Fig. 4: (a) Effect of contact time on P3C@CaO-HCN adsorption capacities (b) Intra-particle diffusion model; (c) Boyed surface diffusion model; and (d) isotherm models of CV, MB, and MO adsorptions.

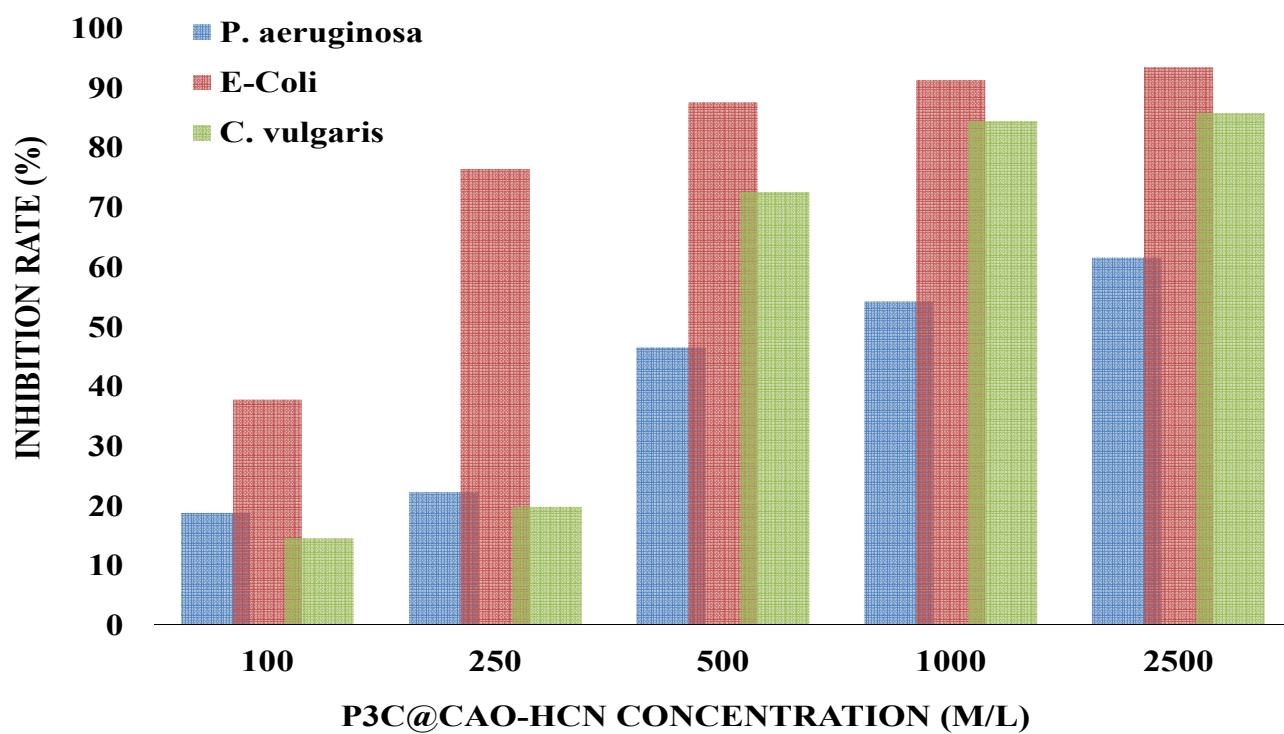
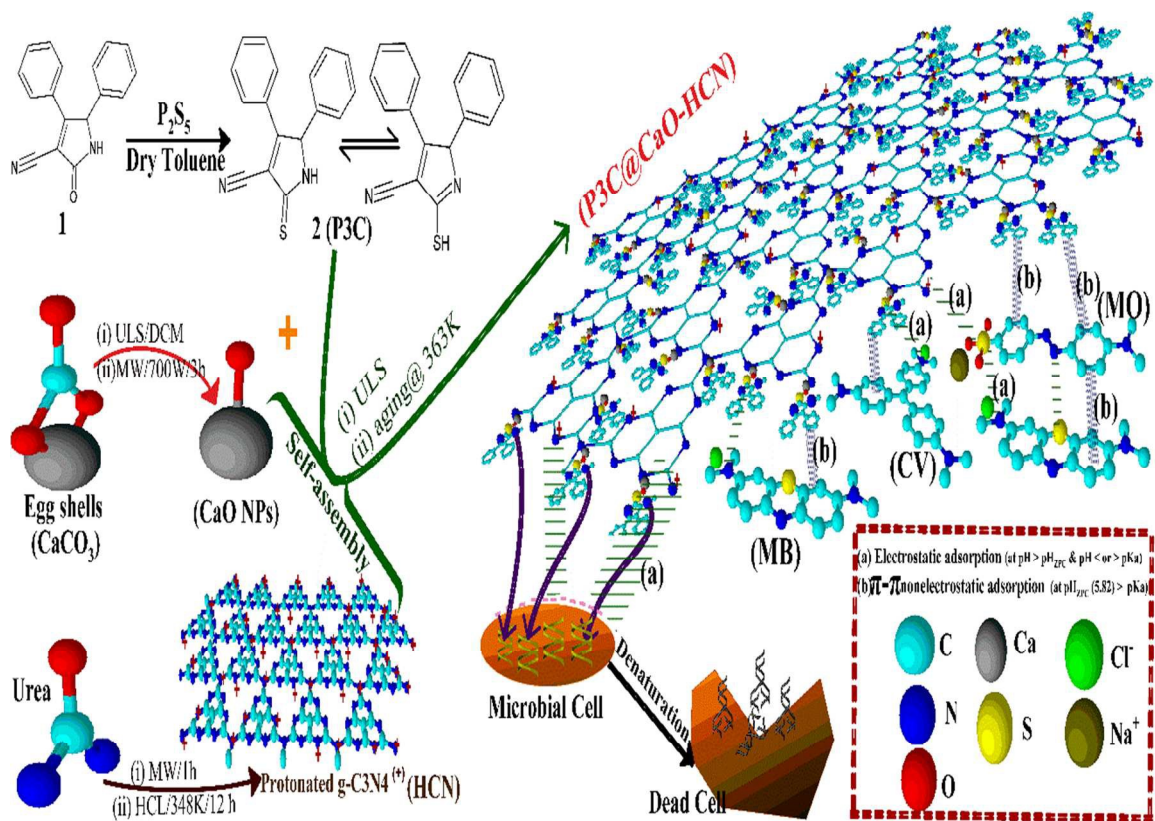


Fig. 5: Antimicrobial activity of P3C@CaO-HCN against *E. coli*, *P. aeruginosa* and *C. albicans* microbial pathogen.



Scheme 1: diagram of P3C@CaO-HCN nanocomposite preparation procedure, and proposed adsorption and antimicrobial mechanisms.

Table 1: ANOVA¹ results of the CV, MB, and MO responses by P3C@CaO-HCN.

Source	df	SS			F-value			Prob>F		
		CV	MB	MO	CV	MB	MO	CV	MB	MO
Model	14	1504132.8	2553355.5	1912533.8	626.3	532.5	467.0	< 0.0001	< 0.0001	< 0.0001
X_{pH}	1	123848.6	68927.1	242111.8	721.9	201.3	827.7	< 0.0001	< 0.0001	< 0.0001
X_D	1	533950.1	945749.9	565372.2	3112.5	2761.5	1932.8	< 0.0001	< 0.0001	< 0.0001
X_{Co}	1	674328.3	1180919.0	816988.7	3930.8	3448.1	2793.1	< 0.0001	< 0.0001	< 0.0001
X_T	1	25167.8	9150.5	8954.0	146.7	26.7	30.6	< 0.0001	0.0001	< 0.0001
$X_{pH}X_D$	1	6048.7	9096.6	45405.4	35.3	26.6	155.2	< 0.0001	0.0001	< 0.0001
$X_{pH}X_{Co}$	1	18413.6	9108.9	37073.9	107.3	26.6	126.7	< 0.0001	0.0001	< 0.0001
$X_{pH}X_T$	1	4175.6	1253.0	221.5	24.3	3.7	0.8	0.0002	0.0765	0.3741
X_DX_{Co}	1	28218.4	97195.0	4961.1	164.5	283.8	17.0	< 0.0001	< 0.0001	0.0007
X_DX_T	1	67.3	522.5	999.7	0.4	1.5	3.4	0.5413	0.2371	0.0714
$X_{Co}X_T$	1	6300.1	892.8	3100.0	36.7	2.6	10.6	< 0.0001	0.1287	0.0040
X_{pH}^2	1	7428.3	46226.8	62815.4	43.3	135.0	213.0	< 0.0001	< 0.0001	< 0.0001
X_D^2	1	48461.4	142760.8	62708.5	282.5	416.8	216.1	< 0.0001	< 0.0001	< 0.0001
X_{Co}^2	1	11976.8	75.5	30338.0	69.8	0.2	102.5	< 0.0001	0.6459	< 0.0001
X_T^2	1	0.1	526.1	69.4	0.04	1.5	0.2	0.9841	0.2356	0.6154
Residual	14	2401.7	4794.7	3679.3						
Lack of Fit	10	2281.9	4493.7	3449.2	7.6	6.0	2.1	0.0326	0.0499	0.0496
Pure Error	4	119.8	301.0	230.2						
Cor Total	28	1506534.5	2558150.2	1916213.2						

Table 2: Multiple regression² and BBD-DOE coefficients results.¹ ANOVA: analysis of variance determined by Design-Expert (v. 7.0.1) software.

Model components	Model terms	Effect			Estimated coefficient			t-value			PC ³ (%)		
		CV	MB	MO	CV	MB	MO	CV	MB	MO	CV	MB	MO
Intercept	β_0	----	----	----	444.1	519.4	522.1	75.81	62.76	72.01	----	----	----
X_{pH}	β_1	203.18	151.58	-284.08	101.6	75.8	-142.0	26.87	14.19	-30.35	8.22	2.69	12.63
X_D	β_2	-421.88	-561.47	-434.12	-210.9	-280.7	-217.1	-55.79	-52.55	-46.38	35.44	36.97	29.50
X_{Co}	β_3	474.11	627.41	521.85	237.1	313.7	260.9	62.7	58.72	55.76	44.76	46.16	42.64
X_T	β_4	91.59	55.23	54.63	45.8	27.6	27.3	12.11	5.17	5.84	1.67	0.36	0.47
$X_{pH}X_D$	β_{12}	-77.77	-95.38	213.09	-38.9	-47.7	106.5	-5.94	-5.15	13.14	0.40	0.36	2.37
$X_{pH}X_{Co}$	β_{13}	135.7	95.44	-192.55	67.8	47.7	-96.3	10.36	5.16	-11.88	1.22	0.36	1.93
$X_{pH}X_T$	β_{14}	64.62	35.4	-14.88	32.3	17.7	-7.4	4.93	1.91	-0.92	0.28	0.05	0.01
X_DX_{Co}	β_{23}	-167.98	-311.76	-70.44	-84.0	-155.9	-35.2	-12.83	-16.85	-4.34	1.87	3.80	0.26
X_DX_T	β_{24}	-8.2	-22.86	-31.62	-4.1	-11.4	-15.8	-0.63	-1.24	-1.95	0.001	0.02	0.05
$X_{Co}X_T$	β_{34}	79.37	29.88	55.68	39.7	14.9	27.8	6.06	1.61	3.43	0.42	0.03	0.16
X_{pH}^2	β_{11}	-67.68	-168.84	-196.82	-33.8	-84.4	-98.4	-6.58	-11.62	-15.46	0.74	2.98	3.82
X_D^2	β_{22}	172.87	296.71	196.65	86.4	148.4	98.3	16.81	20.42	15.45	3.99	6.01	4.34
X_{Co}^2	β_{33}	-85.94	6.82	-136.78	-43.0	3.4	-68.4	-8.36	0.47	-10.74	0.82	0.01	1.61
X_T^2	β_{44}	-0.21	-18.01	-6.54	-0.1	-9.0	-3.3	-0.02	-1.24	-0.51	0.001	0.02	0.001

² Multiple regression analysis calculated by MINITAB (v. 17) software.

³ The percent contribution (PC %) = $SS/\sum SS \times 100$.

Table 3: Kinetics constants for the adsorption of CV, MB, and MO by P3C@CaO-HCN at different temperatures (288 K, 307 K, and 328 K).

Kinetic parameters	CV			MB			MO			Kinetic equations
	288 K	307 K	328 K	288 K	307 K	328 K	288 K	307 K	328 K	
Experimental q_e ($\mu\text{mol. g}^{-1}$)	915.40	1014.00	1120.32	1360.07	1421.99	1487.54	1014.01	1073.90	1161.79	
PFOM										
q_o ($\mu\text{mol. g}^{-1}$)	933.72	1017.57	1118.02	1298.28	1368.71	1452.65	1024.15	1070.77	1145.34	$q_t = q_o(1 - \exp(-K_1 t))$
K_1 (h^{-1})	0.35	0.42	0.51	0.52	0.87	1.66	0.35	0.55	0.68	
R^2	0.98	0.97	0.99	0.91	0.91	0.94	0.98	0.99	0.97	
FL-PFO										
q_o ($\mu\text{mol. g}^{-1}$)	916.1	1009.69	1121.61	1365.52	1436.59	1486.35	1010.34	1068.95	1166.77	$q_t = q_o(1 - \exp(-K_1 t^\alpha))$
K_1 (h^{-1})	0.26	0.32	0.52	0.61	0.87	1.41	0.28	0.54	0.72	
α	1.34	1.37	0.96	0.59	0.59	0.62	1.27	1.04	0.79	
R^2	0.996	0.99	0.995	0.993	0.996	0.997	0.992	0.998	0.991	
PSOM										
q_o ($\mu\text{mol. g}^{-1}$)	1080.16	1157.38	1243.37	1409.54	1470.08	1512.28	1186.13	1187.42	1249.21	$q_t = \frac{K_2 q_o^2 t}{1 + K_2 q_o t}$
K_2 ($\text{g. } \mu\text{mol}^{-1} \cdot \text{h}^{-1}$)	0.0004	0.0004	0.0005	0.001	0.001	0.002	0.0003	0.0006	0.001	
$t^{1/2}$ (h)	2.46	1.96	1.46	0.70	0.68	0.33	2.48	1.34	1.00	
R^2	0.94	0.93	0.97	0.98	0.98	0.99	0.95	0.96	0.98	
Elovich										
β ($\mu\text{mol. g}^{-1} \cdot \text{h}^{-1}$)	226.39	232.11	225.72	242.61	204.65	137.59	250.01	211.05	196.67	$q_t = \beta \ln(\alpha \beta t)$
α ($\text{g. } \mu\text{mol}^{-1} \cdot \text{h}^{-2}$)	0.02	0.02	0.05	0.07	0.35	29.77	0.02	0.06	0.14	
R^2	0.90	0.86	0.90	0.94	0.92	0.80	0.92	0.87	0.88	
MOE										
q_o ($\mu\text{mol. g}^{-1}$)	913.94	1016.59	1121.24	1389.87	1433.29	1488.42	1021.18	1071.78	1167.17	$q_t = q_o \frac{1 - \exp(-K_1 t)}{1 - F \exp(-K_1 t)}$
K_1 (h^{-1})	0.35	0.42	0.45	0.01	0.03	0.36	0.35	0.55	0.33	
F	0.001	0.001	0.154	1.000	0.975	0.866	0.001	0.001	0.640	
R^2	0.981	0.973	0.995	0.982	0.988	0.998	0.982	0.998	0.990	

Table 4: Isothermal equations and determination coefficients of CV, MB, and MO dye adsorption onto P3C@CaO-HCN adsorbent.

Isotherm models	Simulated mathematical isotherm equations			R^2		
	CV	MB	MO	CV	MB	MO
Langmuir	$q_e = 1449.40 \frac{0.005C_e}{1 + 0.005C_e}$ $R_L=0.154$	$q_e = 2221.56 \frac{0.008C_e}{1 + 0.008C_e}$ $R_L=0.11$	$q_e = 1284.37 \frac{0.015C_e}{1 + 0.015C_e}$ $R_L=0.06$	0.99	0.95	0.99
Freundlich	$q_e = 67.192C_e^{1/2.32}$	$q_e = 203.26C_e^{1/2.84}$	$q_e = 137.33C_e^{1/3.03}$	0.97	0.99	0.94
Tempkin	$q_e = 259.14 \ln(0.103C_e)$	$q_e = 253.69 \ln(0.147C_e)$	$q_e = 239.02 \ln(0.2C_e)$	0.98	0.94	0.98
Redlich–Peterson (R-P)	$q_e = \frac{11.399C_e}{1 + 0.027C_e^{0.86}}$	$q_e = \frac{1395.09C_e}{1 + 6.38C_e^{0.59}}$	$q_e = \frac{21.28C_e}{1 + 0.02C_e^{0.95}}$	0.99	0.99	0.99
Dubinin–Radushkevich (D-R)	$q_e = 1053.88 \exp(-0.001\varepsilon^2)$	$q_e = 1713.38 \exp(-0.0006\varepsilon^2)$	$q_e = 1092.61 \exp(-0.0001\varepsilon^2)$	0.87	0.87	0.92

