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# Improved high-current-density hydrogen evolution reaction kinetics on single-atom Co embedded in an order pore-structured nitrogen assembly carbon support†

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Single-atom catalysis is a subcategory of heterogeneous catalysis with well-defined active sites. Numerous endeavors have been devoted to developing single-atom catalysts for industrially applicable catalysis, including the hydrogen evolution reaction (HER). High-current-density electrolyzers have been pursued for single-atom catalysts to increase active-site density and enhance mass transfer. Here, we reasoned that a single-atom metal embedded in nitrogen assembly carbon (NAC) catalysts with high single-atom density, large surface area, and ordered mesoporosity, could fulfil an industrially applicable HER. Among several different single-atom catalysts, the HER overpotential with the best performing Co-NAC reached a current density of 200 mA cm<sup>-2</sup> at 310 mV, which is relevant to industrially applicable current density. Density functional theory (DFT) calculations suggested feasible hydrogen binding on single-atom Co resulted in the promising HER activity over Co-NAC. The best-performing Co-NAC showed robust performance under alkaline conditions at a current density of 50 mA cm<sup>-2</sup> for 20 h in an H-cell and at a current density of 150 mA cm<sup>-2</sup> for 100 h in a flow cell.

## New concepts

This work demonstrates a novel approach to a high-current-density hydrogen evolution reaction (HER) using single-atom cobalt sites embedded in ordered porous nitrogen assembled carbon (Co-NAC). The concept addresses key challenges in single-atom catalysis for industrial-scale water electrolysis by combining a high density of active sites with enhanced capabilities of mass transfer in one catalyst. Using a hard-template synthetic method, we achieved atomically dispersed cobalt sites within a high-surface-area, ordered mesoporous carbon structure. This unique design enabled rapid current increase from 50 to 200 mA cm<sup>-2</sup> with a minimal overpotential increase of 18 mV. Density functional theory calculations revealed that different Co-N co-ordinations in the NAC structure moderated Co-H binding, with CoN<sub>3</sub>C<sub>1</sub> sites showing particularly favorable energetics for the HER. The stability of the catalyst under alkaline conditions and high current densities for extended periods demonstrated its potential for practical applications. This work demonstrates a new concept of designing single-atom catalysts that can meet the demands of industrial-scale hydrogen production. Our method could bridge the gap between fundamental research and practical implementation of HER in renewable-energy technologies.

## Introduction

To achieve net-zero carbon emissions, clean and renewable energy resources have drawn extensive attention for sustainable development and deployment. “Green” hydrogen generated from water electrocatalytic splitting is recognized as one of the most promising clean fuels if the electricity comes from renewable sources such as wind, solar, and hydropower. To accommodate both hydrogen and oxygen evolution reactions in the same electrolyte solution, the hydrogen evolution reaction (HER) under alkaline conditions is more desirable to simplify the water-splitting process due to the sluggish kinetics of the oxygen evolution reaction (OER) under acidic conditions.<sup>1</sup> Under alkaline conditions, Pt-based catalysts are superior for the HER, but the high cost with limited supply restricts their large-scale applications.<sup>2–6</sup> Alternatively, earth-abundant metal catalysts such as Ni, Co, and Mo<sub>2</sub>C have gained significant attention for the HER.<sup>7–11</sup>

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Numerous efforts have been devoted to developing single-atom catalysts because of their high atomic utilization and unique activity in contrast to nanomaterials.<sup>12,13</sup> The kinetics of single-atom catalysts are critically dependent on the loading of active sites, the interaction between the metal and support, and the support structure. In particular, porous supports with high surface area usually lead to reduced mass transfer and, hence, improved catalytic kinetics.<sup>14</sup> In electrocatalytic reactions, the conductivity of the catalyst is another essential factor affecting activities. Some single-atom catalysts with 3d transition metals, such as Fe-N-C, Co-TiO<sub>2</sub>, and Co-N-C, have shown promising activity for the HER with low onset potentials that are comparable with those of precious metal catalysts.<sup>15–19</sup> Nevertheless, atomically dispersed non-precious metal HER catalysts remain to be investigated to suit industrial applications, especially under large currents.

Herein, we designed single-atom catalysts with nitrogen assembly carbon (NAC) as an ordered porous support to study the HER at high current density under alkaline electrolyte conditions.<sup>20</sup> The high nitrogen content of a NAC support enables the regulated anchoring of five 3d to 4d metals (*e.g.*, Co, Fe, Ni, Cu, and Ru) generally with high metal site loading. The high surface area combined with the ordered mesoporous structure ensures high surface exposure of metal sites and facilitates mass transfer under large currents and fast reaction kinetics for the alkaline HER. Among all studied catalysts, Co-NACs exhibited the best performance with the smallest overpotential followed by rapid current increase. The synthesis of Co-NAC was optimized further by varying the Co loading and carbonization temperature. Co-100-NAC-800, prepared at 800 °C with the highest Co single atom loading (1.9 wt%), reached 200 mA cm<sup>−2</sup> at an overpotential of 310 mV during linear sweep voltammetry (LSV) test. The Tafel slope of Co-NAC materials was >130 mV dec<sup>−1</sup>, indicating that the Volmer step was rate-determining. The density functional theory (DFT)-calculated free energy diagram suggested that the outstanding HER activity was due to moderate binding of hydrogen over Co-NAC with various levels of nitrogen coordination. The high robustness of Co-100-NAC-800 was further demonstrated by stable potential over a 100-h test at a current density of 150 mA cm<sup>−2</sup> in a membrane electrode assembly (MEA).

## Results and discussion

### Synthesis and characterization of single-atom NAC

Single-atom metal-NAC catalysts were prepared following a reported hard-template method (Scheme S1, ESI†).<sup>21,22</sup> First, ethylenediamine was coordinated with metal precursors as the acetylacetonate salt (for Co, Ni, Fe, Cu, and Ru) and polymerized with tetrachloride carbon using SBA-15 silica with a long-range ordered mesopore structure as the template. The resulting mixture was carbonized under Ar at different temperatures ranging from 600 to 800 °C. The single-atom NAC was obtained after removing the SBA-15 template upon etching. We designated the as-prepared single-atom NAC samples as “M-*x*-NAC-*y*”, where M represents the metal type, *x* denotes the mass of metal precursor added during synthesis in milligrams, and *y*

indicates the carbonization temperature in degrees Celsius. For instance, “Co-100-NAC-800” stands for a cobalt single-atom catalyst embedded in NAC prepared using 100 mg of cobalt precursor and carbonized at 800 °C.

Using Co-NAC as an example, the powder X-ray diffraction (PXRD) patterns in Fig. S1 (ESI†) show primarily two peaks at 25° and 44° assigned to a graphitic carbon structure, while no peak is observed for metallic Co particles. N<sub>2</sub> physisorption studies showed that the surface area of the prepared Co-NACs was typically larger than 600 m<sup>2</sup> g<sup>−1</sup> (Fig. 1 and Table S2, ESI†). The mesoporous structures were indicated by a type-IV hysteresis loop observed from N<sub>2</sub> adsorption/desorption isotherm curves (Fig. 1(a) and (c)). Pore distribution simulated with the BJH model confirmed the ordered mesoporous structure of Co-NAC with an average pore size of ~4.0 nm (Fig. 1(b), (d) and Table S2, ESI†). The large surface area and ordered mesoporous morphology hold the promise of improved mass transfer, which could facilitate the high current density electrochemical applications at the industrial scale. Additionally, scanning electron microscopy (SEM) and transmission electron microscopy (TEM) images showed the synthesized Co-NAC preserved the morphology and aligned pore structure of the SBA-15 template (Fig. S2 and S3, ESI†).

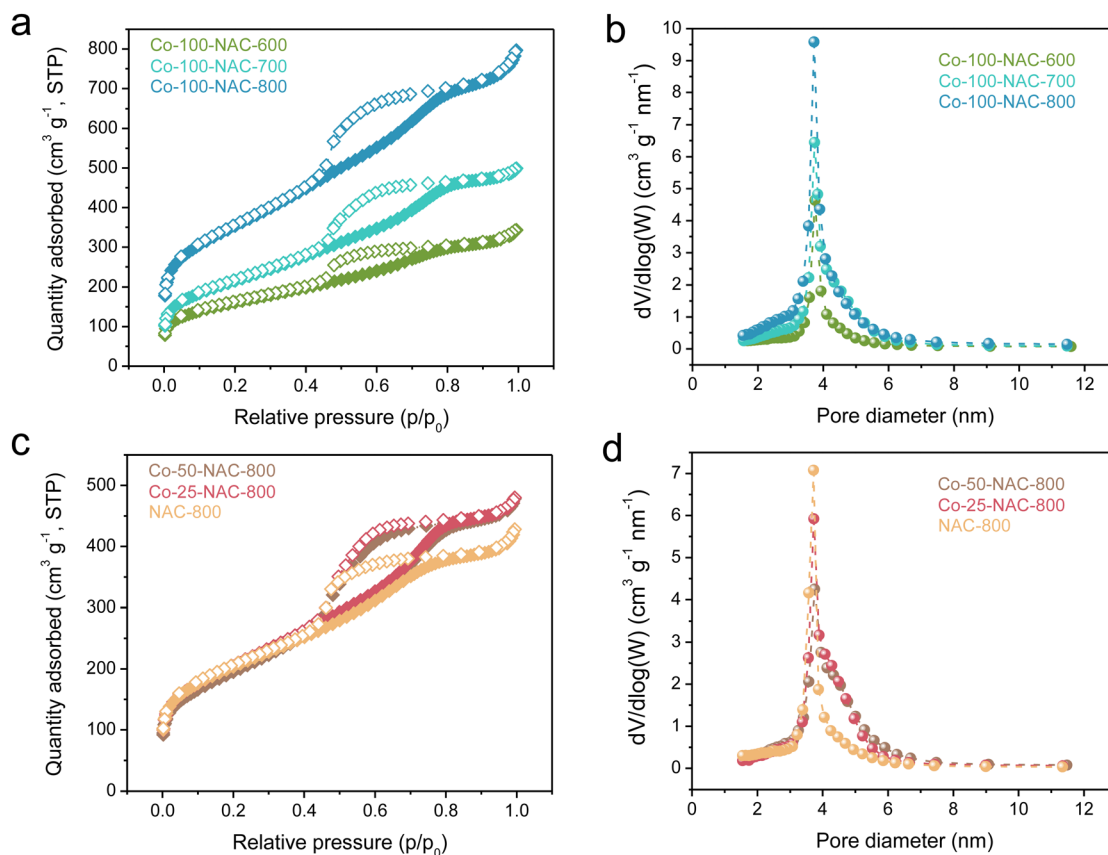
High-resolution scanning transmission electron microscopy (HR-STEM) study of the representative Co-100-NAC-800 revealed single Co atoms embedded on NAC, with no observable nanoparticles or clusters (Fig. 2(a); Co single atoms are indicated by blue arrows). The uniform distribution of Co on the NAC substrate was confirmed through energy dispersive X-ray spectroscopy (EDS) elemental mapping (Fig. 2(b)–(e)), indicating the successful preparation of the single-atom Co-NAC catalyst.

X-ray absorption experiments of the Co K-edge were carried out for representative Co-NAC samples. As shown in Fig. S5a (ESI†), X-ray absorption near-edge structure (XANES) spectra of all three samples present a higher energy pre-edge and a more intense white line than those of Co foil, suggesting oxidized Co species. The XANES spectra of Co-NAC catalysts are consistent with 4-coordinate cobalt atoms reported in the literature.<sup>23–25</sup> In the extended X-ray absorption fine structure (EXAFS) spectra, only one main peak was observed for the first shell (Fig. S5b, ESI†). Fittings of the EXAFS spectra with defined coordination numbers of 4 for all samples gave bond lengths of 1.94, 1.94 and 1.99 Å (Fig. S6 and Table S3, ESI†) for Co-NAC-800, Co-NAC-700, and Co-NAC-600, respectively, best assigned as Co-N bonds.<sup>26,27</sup> There was no detection of Co-Co at 2.49 Å (after phase correction) in the second shell. Consequently, the results of XANES and EXAFS suggested that cobalt atoms were atomically dispersed and bonded with most likely four nitrogen atoms on the NAC support. X-ray photoelectron spectroscopy (XPS) suggested that the Co species in the Co-NAC were mainly Co<sup>2+</sup>, while there were several N species, including graphitic, pyrrolic, and pyridinic N, existing in the Co-NAC (Fig. S7, ESI†).

### Electrocatalytic HER

Screening of the HER activity over different metal-NACs was carried out under alkaline electrolyte (1 M KOH) in a H-cell.

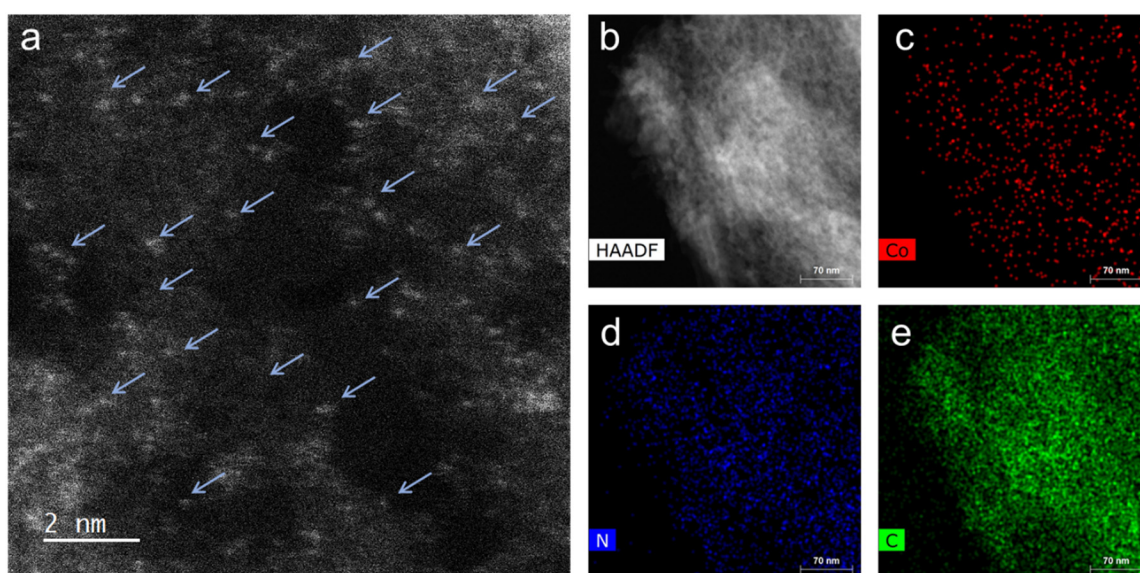




**Fig. 1**  $\text{N}_2$ -sorption isotherm (a) and (c) and pore-size distribution (b) and (d) of Co-NAC catalysts carbonized at 600, 700, and 800 °C with different metal loadings. The samples are named as "Co- $x$ -NAC- $y$ ", which are prepared with  $x$  mg of added  $\text{Co}(\text{acac})_2$  and under a carbonization temperature of  $y$  °C. The actual Co loadings are summarized in Table S1 (ESI†). NAC-800 is a sample prepared using the same method but without addition of a Co precursor.

Carbon fiber paper ( $1 \text{ cm}^2$ ) with single-atom catalyst deposition,  $\text{Hg}/\text{HgO}$  (1 M KOH), and Pt mesh were used as the working, reference, and counter electrodes, respectively. Nafion 117

membrane was used to separate the cathode and anode. LSV was performed from 0 to  $-0.5 \text{ V}$  versus the reverse hydrogen electrode (RHE) to monitor the HER performance of metal-NACs



**Fig. 2** Electron-microscopy characterization of Co-100-NAC-800. (a) HR-STEM image of Co-NAC, the arrows indicate the single-atom Co on the NAC support. (b)–(e) EDS elemental mapping images of Co-NAC: (b) HAADF-STEM image; (c) Co mapping; (d) C mapping; (e) N mapping.



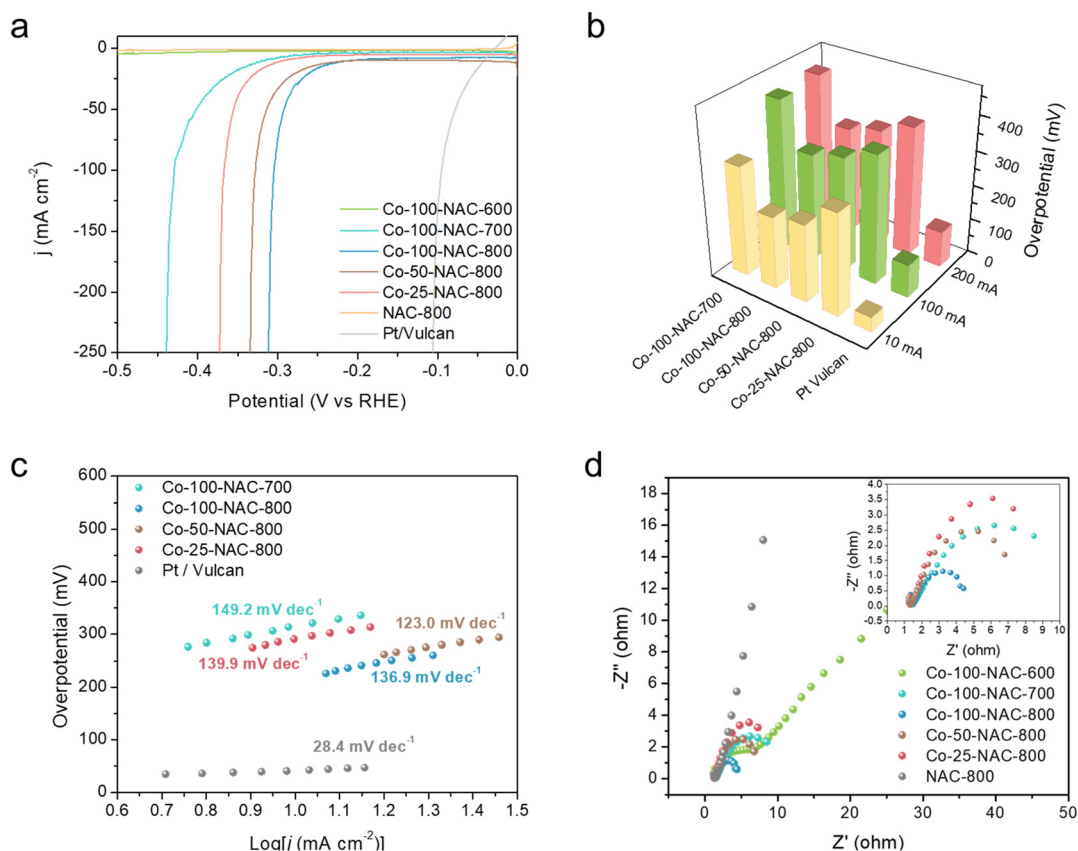


and compared with metal-free NAC-800 support and commercial Pt/Vulcan. Fe-100-NAC-800, Co-100-NAC-800, and Ni-100-NAC-800 showed similar current change behavior with larger overpotential than Pt/Vulcan but rapid current increase, while Cu-NAC and Ru-NAC showed a sluggish HER over the test range (Fig. S8, ESI†). Among these catalysts, Co-100-NAC-800 demonstrated the smallest overpotential, 207 mV at  $10 \text{ mA cm}^{-2}$  and 292 mV at  $50 \text{ mA cm}^{-2}$ . The rapid current increase for Co-NAC permitted a high-current-density HER under relatively small overpotential compared with the single-atom catalysts reported in the literature.<sup>12,14,17</sup>

We further performed HER in a single cell with Co-NAC catalysts to test the effect of different synthetic parameters. The single-cell setup helped to eliminate the cation exchange limitation on the Nafion membrane at a high current density. Synthetic parameters, particularly the carbonization temperature, can directly impact the physiochemical properties of catalysts, including the N content of the NAC support (Table S4, ESI†), local coordination of metal sites, conductivity, and surface area. Besides, the density of catalytically active sites is essential for a high-current HER application. Therefore, Co-NAC catalysts were prepared and examined for the large-current HER with different amounts of Co precursors and carbonization at different temperatures. The exact Co loading was measured using inductively coupled plasma mass spectrometry (ICP-MS) (Table S1, ESI†).

From the LSV profile of Co-NACs shown in Fig. 3(a), Co-100-NAC-800 prepared at  $800^\circ\text{C}$  with the highest Co loading showed the smallest overpotential (310 mV) at a current density of  $200 \text{ mA cm}^{-2}$ . Co-NAC catalysts prepared at lower temperatures had a larger onset overpotential; in contrast, Co-100-NAC-600 showed negligible activity in the HER within the tested potential range. Like Co-100-NAC-800, Co-100-NAC-700 also enabled a rapid current increase but started at a larger overpotential after a considerable window of the sluggish current response. As summarized in Fig. 3(b), the trend of change in the HER overpotential with respect to Co loadings of Co-NAC-800 catalysts aligned with our prediction that catalysts with high Co loading provide more active sites for the HER, improve the overall kinetics, and lower the HER overpotential at a high current density.

The Tafel plots of Co-NAC catalysts provided insight into the HER mechanism, as shown in Fig. 3(c).<sup>28</sup> In the region of low current density, Co-NAC catalysts presented a Tafel plot larger than  $120 \text{ mV dec}^{-1}$ , indicating the Volmer step to be the rate-determining step.<sup>28</sup> It is generally accepted that the good conductivity of electrodes is more desirable in the electrocatalytic process to maximize the efficiency of electron utilization.<sup>29</sup> Electrochemical impedance spectroscopy (EIS) was conducted to study the conductivity properties of Co-NACs under an overpotential of 300 mV. As shown from the Nyquist plot in Fig. 3(d), the resistances of the Co-100-NAC-800 were better



**Fig. 3** HER evaluation on Co-NAC. (a) LSV; (b) overpotential at 10, 100, and  $200 \text{ mA cm}^{-2}$ ; (c) Tafel plots; (d) Nyquist plots at  $-0.3 \text{ V}$ ; insert: zoom-in Nyquist plot. Co-100-NAC-600 overlaps with NAC-800 in (a).



than Co-100-NAC-600 and Co-100-NAC-700. With better conductivity, the Joule loss of Co-100-NAC-800 at a high current density was smaller than those of Co-100-NAC-600 and Co-100-NAC-700.

The surface area of the electrode can affect mass transfer, especially under large-current conditions. Large electrode surface areas are therefore pursued to eliminate the limitation of mass transfer. The electrochemical surface areas (ECSA) of Co-NACs were estimated using double-layer capacitance ( $C_{dl}$ ), as shown in Fig. S9–S14 (ESI<sup>†</sup>). Cyclic voltammetry (CV) was performed at different scanning rates in a potential range without any faradaic process. The slope of current density *versus* scanning rate is the double-layer capacitance of the Co-NAC electrode, and the ECSA can be calculated using the ratio between  $C_{dl}$  and specific capacitance ( $C_s$ ), as shown in eqn (1). Measuring the  $C_s$  of a material involves an unachievable flat electrode with this single-atom porous material. However, researchers have measured a series of materials for their specific capacitance, which typically ranges between 0.022 to 0.130 mF cm<sup>-2</sup> in alkaline electrolytes.<sup>30,31</sup> In this case, we estimated the ECSA of Co-NAC using  $C_s = 0.06$  mF cm<sup>-2</sup>. As mentioned above, the NAC support has a large surface area and ordered mesoporous structure; as a result, the corresponding ECSA of NAC catalysts was calculated to be from 531.7 to 2455 cm<sup>2</sup> (per cm<sup>2</sup> geometric electrode surface). The large ECSA maximizes exposure to active sites and thus minimizes the mass-transfer limitation, which makes the HER at a high current density feasible.

$$\text{ECSA} = \frac{C_{dl}}{C_s} \quad (1)$$

The durability of electrodes is a crucial parameter for industrial applications. Enhancing durability under a high current density is challenging because the large current could change the structure of the electrode, leading to site deactivation or metal leaching. A 20-h stability test was performed at a current density of 50 mA cm<sup>-2</sup> in 1 M KOH electrolyte with stirring. As shown in Fig. 4(a), the potential remained unchanged over the 20-h test with the Co-100-NAC-800 catalyst. At the same time, a hydrogen bubble was continuously generated from the electrode (shown in Fig. S15 and Supplementary Video, ESI<sup>†</sup>). No structure evolution of Co-100-NAC-800 was observed from the XRD pattern after the 20-h stability test (Fig. S16, ESI<sup>†</sup>).

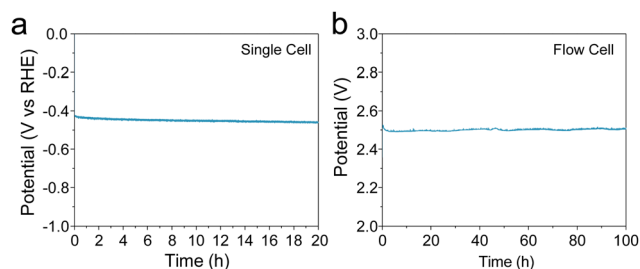


Fig. 4 Stability test of Co-100-NAC-800. (a) Chronopotentiometry (CP) plot showing the stability test at 50 mA cm<sup>-2</sup>; (b) 100-h water-splitting test at 150 mA cm<sup>-2</sup> current density in flow cell with Co-100-NAC-800 as the cathode catalyst and Pt on carbon as the anode catalyst.

To evaluate the long-term stability of the Co-NAC under practical conditions, we conducted a continuous flow test. A membrane electrode assembly (MEA) was built with Co-100-NAC-800 as the cathode catalyst and Pt/Vulcan as the anode catalyst to test the stability of the Co-NAC catalyst. As shown in Fig. 4(b), the initial voltage of the water-splitting was 2.50 V at a current density of 150 mA cm<sup>-2</sup>. Despite the observed overpotential of water-splitting being compromised by the sluggish OER on the Pt electrode, the cell voltage remained stable at 2.50 V during the 100-h stability test with no voltage increase.

### Theoretical insights

DFT calculations were performed to provide insights into the atomic structure of the potential active sites for the HER. Gibbs free energy of H adsorption was used as a descriptor for the HER activity, as shown in the literature.<sup>32,33</sup> Fig. 5 shows that the H binding energy on the CoN<sub>4</sub> is 0.18 eV. As indicated in our previous study, the binding configuration between the single metal atom and the substrate atom (nitrogen or carbon) could be altered among the coordination (N<sub>x</sub>C<sub>4-x</sub>) of the NAC.<sup>22</sup> Thus, DFT calculations were carried out on Co-NAC with these possible coordinations (Fig. 5). To compare their metal-substrate binding configuration, the values with different bond lengths between the Co and N (or C) atoms are provided in Table S5 (ESI<sup>†</sup>). The shorter metal-support bond and the increased number of N coordinations enabled the CoN<sub>4</sub> structure to have a stronger metal-substrate interaction, in agreement with the EXAFS results (Fig. S5 and S6, ESI<sup>†</sup>). The HER energy profiles of Co-NACs were further investigated for different Co-N<sub>x</sub>-NAC structures. The different N coordinations moderated the Co–H binding, with CoN<sub>3</sub>C<sub>1</sub> showing the least difference in free energy for H

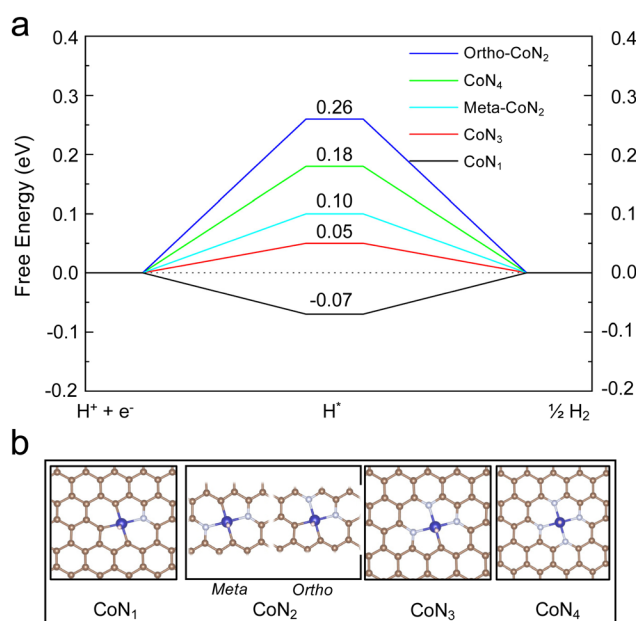


Fig. 5 DFT calculations of hydrogen adsorption. (a) Calculated HER free-energy diagram over different configurations of Co-N<sub>x</sub>-NAC. The H binding energy is labeled on top of each configuration. (b) Atomic structures of H adsorbed on Co-N<sub>x</sub>-NAC.



adsorption on the metal centre, indicating the lowest overpotential based on the computational hydrogen electrode (CHE) model.<sup>34</sup> The thermodynamic calculations in Fig. 5 thus suggest that Co-NACs, possibly with the CoN<sub>3</sub> site, could also show promising HER activity. Our DFT calculations could not unambiguously determine the exact local binding configuration of Co (*e.g.*, N<sub>4</sub> vs. N<sub>3</sub>C<sub>1</sub>) in Co-NAC, and in the real samples, different metal-coordination likely coexist. Nevertheless, the calculations reveal that single-atom Co with various Co–N coordination displayed favorable hydrogen binding that was close to thermoneutral at the metal centre.

## Conclusions

We systematically studied the single-atom Co materials, Co-NACs, which efficiently catalyzed the HER under a high current density. The synthetic parameters, including Co metal loading and carbonization temperature, were varied as critical parameters for HER-performance studies. High Co loading and a high carbonization temperature led to low overpotential and high current density. On the contrary, a low carbonization temperature resulted in high resistance, which limited the achievable current density in the HER. Both kinetic analysis and theoretical calculations suggested that the Volmer step was the rate-limiting step. The high surface area of the NAC support boosted the HER current by maximizing exposed active species and minimizing mass-transfer limitations. With a combination of high Co loading and large electrode surface area, enhanced kinetics enabled Co-100-NAC-800 to overcome a large HER onset potential and access a high current density (200 mA cm<sup>−2</sup>) at a moderate overpotential (310 mV) in LSV tests. In addition, Co-NAC-800 demonstrated stability in the HER over 100 h under strong alkaline conditions and at a high current density, making it feasible for scalable industrial applications.

## Methods

### Materials

Iron(III) acetylacetonate (purity ≥ 99.5%, trace metal), cobalt(II) acetylacetonate (≥ 99%), nickel(II) acetylacetonate (95%), copper(II) acetylacetonate (≥ 99.9%, trace metal), Ruthenium(III) acetylacetonate (97%), carbon tetrachloride (≥ 99.9%), ethylenediamine (≥ 99.5%), tetraethyl orthosilicate (TEOS, 98%), and pluronic P123 (*M<sub>n</sub>* ~ 5800) were purchased from Millipore-Sigma. Hydrofluoric acid (trace metal), hydrochloric acid (trace metal), and nitric acid (trace metal) were purchased from Thermo Fisher. All chemicals were used as received.

### Synthesis of transition metal single-atom on NAC

**Synthesis of the SBA-15 template.** SBA-15 with ordered pore structure was synthesized using P123 as the soft template.<sup>35</sup> In a 500-mL polypropylene bottle, 4.0 g of P123 was added to HCl–H<sub>2</sub>O solution (120 mL of 2 M HCl solution and 30 mL of H<sub>2</sub>O) and stirred at 36 °C in an oil bath for 1 h to dissolve P123. Then, 8.5 g of TEOS was added to the solution with stirring. The

transparent solution slowly changed to milky white, indicating the nucleation and growth of porous silica. After 20 h in an oil bath at 36 °C, the mixture was transferred to an oven at 100 °C and left for another 24 h to age the formed silica. The mixture was then allowed to cool down to room temperature naturally. SBA-15 was separated by filtration and washed with water until the pH was neutral. After drying the solid at 75 °C overnight, the templating P123 was removed by calcination at 550 °C for 5 h to enable the exposure of pore structures.

**Synthesis of single-atom NAC.** The desired amount of metal acetylacetonate was first dissolved in a solution of ethylenediamine (1.80 g). Next, 4.0 g of carbon tetrachloride was added, followed by the addition of 0.80 g of SBA-15. The mixture was heated in an oil bath at 90 °C for 16 h for condensation. The oil-bath temperature was then increased to 120 °C for 4 h to remove the uncondensed ethylenediamine and carbon tetrachloride. The obtained brown powders were carbonized under Ar flow, with temperature raised at a ramping rate of 3 °C min<sup>−1</sup> to 600, 700, or 800 °C and maintained for 2 h. After carbonization, the black powder was treated with 5 wt% HF and 10 wt% HCl aqueous solution for 2 days to remove the SBA-15 template and excess metals. The products were recovered *via* centrifugation, washed with deionized water until the pH reached 7, and dried at 100 °C. The prepared single-atom NAC was named “M-*x*-NAC-*y*”, where M is the type of metal, *x* is the amount of metal acetylacetonate added in milligrams, and *y* is the calcination temperature in degrees Celsius.

**Synthesis of NAC.** NAC was synthesized using the same method as the synthesis of single-atom NAC, but without adding metal acetylacetonate precursors.

### Characterization

Powder X-ray diffraction (XRD) was performed using a Bruker D8A25 diffractometer with Cu K $\alpha$  radiation ( $\lambda$  = 1.54184 Å). N<sub>2</sub> physisorption was performed using an auto-adsorption analyzer (3Flex; Micromeritics) at −196 °C. Inductively coupled plasma mass spectroscopy (ICP-MS) for metal loadings was measured with a spectrometer (X Series 2; Thermo Scientific). HAADF-STEM imaging was performed on a Titan Themis 300 equipped with a gun monochromator and probe spherical aberration (*C<sub>s</sub>*) corrector operated at 200 kV. EDS mapping data were collected with a Super-X EDX detector. CHNS analysis was conducted using an Elementar Unicube Analyzer. X-ray adsorption spectroscopy (XAS) experiments, including X-ray absorption near edge structure (XANES) and extended X-ray absorption fine structure (EXAFS), were conducted at 7-BM QAS beamline in National Synchrotron Light Source II at Brookhaven National Laboratory. The Co K-edge of Co-NAC samples was collected in fluorescence mode at room temperature and ambient pressure. Co foil was also collected to act as a reference for energy calibration and drift correction of the monochromator.

“Athena” and “Artemis” from the Demeter software package were used to analyze the data of each sample.<sup>36,37</sup> The FEFF program was used for the calculation and appropriate fitting of EXAFS spectra. A *k* range between 2.5 to 8.5 Å<sup>−1</sup> was used for Fourier-transformed (FT) EXAFS spectra.



## HER

**Preparation of the working electrode.** First, 1 mg of prepared NAC or metal-NAC catalyst was dispersed in 0.49 mL of acetone and 10  $\mu\text{L}$  of Nafion solution through sonication for 30 min. The suspension was drop-cast onto  $1 \times 2 \text{ cm}^2$  carbon fiber paper to form a  $1 \times 1 \text{ cm}^2$  catalyst patch. The electrode was dried at room temperature in a fume hood overnight.

**H-cell HER test.** The HER was tested in a three-electrode system using an electrochemical potential station (Biologic). Catalyst-loaded carbon fiber paper, Hg/HgO (1 M KOH), and Pt mesh were used as the working, reference, and counter electrodes, respectively. The working and counter electrodes were separated with Nafion 212 membrane. The potential was converted from Hg/HgO to the RHE using eqn (2). LSV was performed to evaluate the HER properties of NAC catalysts from 0 to  $-0.5 \text{ V}$  vs. RHE at a scan rate of  $2 \text{ mV s}^{-1}$  with 85% IR compensation.

$$E_{\text{RHE}} = E_{\text{Hg/HgO}} + E_{\text{Hg/HgO}}^0 + 0.059\text{pH} \quad (2)$$

**HER tests at a high current density.** Large-current HER was tested in a three-electrode, one-component cell using the electrochemical potential station (biologic) with a booster. NAC-loaded carbon fiber paper, Hg/HgO, and the Pt plate were used as working, reference, and counter electrodes, respectively. The same LSV was performed with a scanning rate of  $2 \text{ mV s}^{-1}$  and 85% IR compensation.

**Stability test.** A stability test was performed in the one-component cell. Chronopotentiometry (CP) under constant current ( $50 \text{ mA cm}^{-2}$ ) was applied, and the potential change was recorded for 20 h. During the stability test, a stir bar was added with stirring (800 rpm) to minimize the limitation of external mass transfer.

**MEA test.** The flow electrolyzer contained two stainless-steel flow-field plates with serpentine channels, PTFE and silicone gaskets. The MEA, which contained two electrodes and a membrane, was formed after assembling the cell hardware. Pt/C ( $0.5 \text{ mg}_{\text{catalyst}} \text{ cm}^{-2}$ ) and Co-NAC ( $1 \text{ mg}_{\text{catalyst}} \text{ cm}^{-2}$ ) were spray-coated on  $\text{HNO}_3$ -treated carbon-cloth substrates as the anode and cathode, respectively. The mass ratio of nanoparticles and ionomer was 4:1. The catholyte and anolyte of 1 M KOH were circulated by a peristaltic pump (Masterflex<sup>®</sup> L/S<sup>®</sup>) at  $20 \text{ mL min}^{-1}$ . The applied current was controlled by a SP-300 potentiostat/galvanostat (biologic). The membrane used to separate the catholyte and anolyte was an anion exchange membrane (A201; Tokuyama). The test was performed at room temperature.

## Computational details

DFT calculations were performed using the VASP package.<sup>38</sup> The Perdew–Burke–Ernzerhof (PBE) functional within the generalized gradient approximation (GGA) was used for the exchange–correlation energy.<sup>39</sup> The electron–ion interaction was described by the projector augmented wave (PAW) approach.<sup>40,41</sup> The van der Waals interaction was included using the DFT-D3 method.<sup>42</sup> All electronic energies were converged to  $10^{-5} \text{ eV}$ , and the atomic force on each atom was minimized to be  $<0.02 \text{ eV \AA}^{-1}$ . The structures of single-atom

NACs were taken from a previous work.<sup>22</sup> A  $(3 \times 3 \times 1)$  Monkhorst–Pack  $k$ -point was used to sample the first Brillouin zone. The Gibbs free energy of adsorption was computed using the computational hydrogen electrode model where the chemical potential of  $(\text{H}^+ + \text{e}^-)$  at  $\text{pH} = 0$  equalled the chemical potential of 1-bar  $\text{H}_2$  in the gas phase at 298 K.<sup>32,34</sup> We added 0.24 eV onto the DFT-calculated total energies to take into account the entropy lost and zero-point energy change for the adsorbed state.<sup>32</sup>

## Author contributions

All authors contributed to the conceptualization of this study. JY conducted the electrochemical evaluation and part of the materials characterization under the supervision of WH. YY performed the theoretical study under the supervision of BW. YL synthesized the materials and conducted part of the characterization under the supervision of ZZ, LQ, and WH. HL assisted with electrochemical tests under the supervision of WL. SS assisted with the electrochemical tests under the supervision of WH. YL, SX, and FL conducted the XAS study. JSO and LZ conducted the HR-STEM characterization of catalysts. JY and YY drafted the manuscript under the supervision of BW and WH. YL and LQ drafted the XAS part of the manuscript. All authors contributed to the revision and finalization of this manuscript.

## Data availability

All data are available in the main text and the ESI.<sup>†</sup>

## Conflicts of interest

There are no conflicts to declare.

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