

Cite this: *J. Mater. Chem. A*, 2024, 12, 32735

# From pollution to energy storage: leveraging hydrogen sulfide with SU-101 cathodes in lithium–sulfur batteries†

Raul A. Marquez,<sup>id</sup>\*<sup>a</sup> Juan L. Obeso,<sup>id</sup>‡<sup>bc</sup> Rinish Reddy Vaidyula,<sup>id</sup>‡<sup>a</sup> Valeria B. López-Cervantes,<sup>id</sup>‡<sup>b</sup> Ricardo A. Peralta,<sup>id</sup><sup>d</sup> Pablo Marín Rosas,<sup>d</sup> José Antonio de los Reyes,<sup>e</sup> C. Buddie Mullins<sup>id</sup>\*<sup>afg</sup> and Ilich A. Ibarra<sup>id</sup>\*<sup>bh</sup>

Despite growing interest in developing metal–organic frameworks to capture toxic emissions, the potential for revalorizing these emissions has largely been overlooked. Captivated by the unique ability of SU-101 to transform H<sub>2</sub>S into polysulfides spontaneously, here we demonstrate how this remarkable capability can be leveraged to power lithium–sulfur batteries. Our proof-of-concept demonstrates how hydrogen sulfide emissions, efficiently captured by the SU-101 metal–organic framework, can be directly converted and utilized in a lithium–sulfur battery. Despite demonstrating a modest initial capacity of about 85 mA h g<sup>−1</sup> and capacity retention of approximately 54%, analogous to other MOF-based Li–S batteries reported in the literature, the SU-101-Sat cathode delivered a durable and stable performance across 1000 cycles and maintained 99.87% coulombic efficiency. The stable response is credited to the controlled release of polysulfides generated from captured hydrogen sulfide. Such resilience is advantageous for developing compact batteries for extended use in special applications, including wearable technology, satellite components, and weather monitoring instruments. These findings open new pathways for waste valorization by employing metal–organic frameworks designed to spontaneously convert toxic gas emissions into valuable feedstocks, serving as potential candidates for more sustainable electrochemical energy conversion and storage devices.

Received 24th May 2024  
Accepted 11th June 2024

DOI: 10.1039/d4ta03620d

rsc.li/materials-a

## Introduction

Air quality is an important environmental concern.<sup>1</sup> In addition to greenhouse gases, carbon monoxide (CO), ozone (O<sub>3</sub>), ammonia (NH<sub>3</sub>), sulfur dioxide (SO<sub>2</sub>), volatile organic

compounds (VOCs), particulate matter (PM), and hydrogen sulfide (H<sub>2</sub>S) represent some of the most predominant and hazardous air pollutants.<sup>2</sup> H<sub>2</sub>S is a colorless, flammable gas, particularly corrosive (*i.e.*, H<sub>2</sub>S is associated with acid rain), and is cataloged as a hazardous chemical. H<sub>2</sub>S is frequently found in biogas and natural gas and is produced by different chemical processes at industrial levels, such as in oil refineries.<sup>3</sup>

H<sub>2</sub>S is highly toxic to humans since it can be rapidly absorbed through inhalation,<sup>4</sup> causing illnesses of the respiratory, cardiovascular, and nervous systems, and specifically, it is related to laryngitis, pneumonia, bronchitis, and pulmonary edema.<sup>5</sup> Even at relatively low concentrations, H<sub>2</sub>S is lethal, causing severe nervous system failure.<sup>6</sup> Therefore, the effective sequestration of H<sub>2</sub>S is crucial for numerous industrial procedures before it is released into the atmosphere. Despite recent advances in H<sub>2</sub>S capture, current technologies (*e.g.*, alkanolamines, ionic liquids, cryogenic sequential distillation, and physisorption in zeolites, activated carbons, and metal oxides) have encountered difficulties such as corrosion of pipelines, large amounts of wastewater, low capture and recovery of H<sub>2</sub>S, and high costs of re-use.<sup>7</sup> Furthermore, there is a pressing need to develop further waste valorization strategies for exploiting these captured emissions.

<sup>a</sup>Department of Chemistry, The University of Texas at Austin, Austin, Texas 78712, USA. E-mail: raul.marquez@utexas.edu

<sup>b</sup>Laboratorio de Fisicoquímica y Reactividad de Superficies (LaFReS), Instituto de Investigaciones en Materiales, Universidad Nacional Autónoma de México, Ciudad de México 04510, Mexico

<sup>c</sup>Laboratorio Nacional de Ciencia, Tecnología y Gestión Integrada del Agua (LNAgua), Instituto Politécnico Nacional, CICATA, U. Legaria, Ciudad de México 11500, Mexico

<sup>d</sup>Departamento de Química, División de Ciencias Básicas e Ingeniería, Universidad Autónoma Metropolitana-Iztapalapa, Ciudad de México 09340, Mexico

<sup>e</sup>Laboratory of Environmental Catalysis, Universidad Autónoma Metropolitana-Iztapalapa, Ciudad de México 09340, Mexico

<sup>f</sup>McKetta Department of Chemical Engineering, The University of Texas at Austin, Austin, Texas 78712, USA

<sup>g</sup>Texas Materials Institute, The University of Texas at Austin, Austin, Texas 78712, USA

<sup>h</sup>On Sabbatical as “Catedra Dr. Douglas Hugh Everett” at Departamento de Química, Universidad Autónoma Metropolitana-Iztapalapa, Ciudad de México 09310, Mexico

† Electronic supplementary information (ESI) available: Experimental details and procedures, supporting figures and tables, additional characterization data. See DOI: <https://doi.org/10.1039/d4ta03620d>

‡ These authors contributed equally to this work.

Chemically-stable metal–organic frameworks (MOFs) have recently been investigated for the efficient capture of  $\text{H}_2\text{S}$ , and promising results have been reported.<sup>8</sup> However, once  $\text{H}_2\text{S}$  is captured (by a reversible physisorption process) in MOFs, what steps are needed to convert  $\text{H}_2\text{S}$  chemically to a different inert chemical molecule? Catalytic conversion of  $\text{H}_2\text{S}$  within MOFs is a novel concept that was only recently demonstrated. Our research group reported the spontaneous chemical transformation of  $\text{H}_2\text{S}$  inside the micropores of MOFs to generate polysulfides *in situ* at room temperature and atmospheric pressure.<sup>9</sup> Based on this premise, we conceive a significant potential for the use of MOF adsorbents containing irreversibly chemisorbed sulfur species (polysulfides) as feedstocks for electrochemical energy conversion and storage technologies, such as sulfur-based batteries.<sup>10</sup>

Lithium–sulfur (Li–S) batteries are promising candidates for the next generation of energy storage systems due to their high theoretical capacity, low cost, and environmentally friendly fabrication.<sup>11</sup> Li–S batteries show promise for overcoming dependence on fossil fuels, reducing exhaust emissions, and paving the way to produce batteries for the next generation of electric vehicles. Certainly, the commercial application of Li–S batteries faces many different challenges, such as (i) poor electrical conductivity of elemental sulfur and its final discharge product of  $\text{Li}_2\text{S}$ ; (ii) large volume expansion of sulfur during the lithiation process resulting in fast capacity decay; (iii) diffusion of soluble polysulfide intermediates affording to irreversible loss of active materials and corrosion of the lithium anode and (iv) the use of a metallic lithium anode can produce safety concerns due to the formation of uninhibited lithium dendrites.<sup>12</sup> To solve these problems, different efforts have focused on designing cathode materials, improving novel electrolytes, adapting separators, and protecting the lithium anode.<sup>13</sup>

Previous studies have utilized MOFs as potential cathode materials for Li–S batteries, given their customizable pore and cage structures and pore dimensions that can effectively encapsulate sulfur.<sup>14</sup> Typically, the MOF material is calcined at high temperatures (500–600 °C) and then subjected to sulfur impregnation. Some materials, such as MIL-101(Cr)@rGO/S (335 mA g<sup>−1</sup> after 50 cycles),<sup>15</sup> HKUST-1 (240 mA g<sup>−1</sup> after 50 cycles),<sup>16</sup> and Mn-MOF (190 mA g<sup>−1</sup> after 50 cycles),<sup>17</sup> have demonstrated high reversible capacities. However, these approaches have reported low cyclability, raising concerns about the lifetime of sulfur-enriched MOF cathodes.

The decreased lifetime is often associated with the detrimental effects of polysulfide intermediates that shuttle between the electrodes and react with the Li anode, resulting in the depletion of active material and manifesting as a capacity decay over time.<sup>18,19</sup> Only a few MOFs have demonstrated effective confinement of polysulfides through physical encapsulation and chemical adsorption.<sup>10</sup> Therefore, identifying the optimal chemical compositions that can effectively suppress polysulfide release is crucial. Furthermore, the additional calcination and sulfur impregnation steps increase both the cost and energy demand of the production process, factors that become critical for commercialization and environmental valorization. To

streamline synthesis and leverage the waste valorization potential of MOF adsorbents, the intrinsic formation of polysulfides following  $\text{H}_2\text{S}$  adsorption presents new possibilities for enhancing Li–S battery technologies.

Herein, we report a proof-of-concept strategy that leverages MOF adsorbents designed to permanently capture toxic  $\text{H}_2\text{S}$ , repurposing them as feedstocks for electrochemical energy storage applications. We show that cathodes containing SU-101 MOF (the polysulfide host) as the active material in a conventional Li–S battery deliver modest capacities, high coulombic efficiencies, and substantial cycling stability for 1000 cycles. These results open promising avenues for using MOFs in sustainable energy applications and waste valorization.

## Experimental

### Synthesis of SU-101 and $\text{H}_2\text{S}$ uptake

SU-101 was synthesized following a previously reported procedure.<sup>20</sup> A total of 15 mg of ellagic acid and 38 mg of  $\text{Bi}(\text{CH}_3\text{CO}_2)_3$  were dissolved in 30 mL of water and acetic acid (6% vol. acetic acid). First, the solution was stirred strongly at room temperature for 48 hours. Later, the recovered powder was washed three times with water and ethanol. Subsequently, it was dried overnight at 60 °C.  $\text{H}_2\text{S}$  saturation experiments were conducted using a custom-designed saturation chamber (Fig. S1†). A detailed description of this procedure is available in the ESI.†

### Material characterization

$\text{H}_2\text{S}$  adsorption measurements were conducted using an HP 5890 gas chromatograph. X-ray diffraction (XRD) patterns were recorded using a Rigaku MiniFlex 600 diffractometer equipped with a Cu K $\alpha$  radiation source. Scanning electron microscopy (SEM) images and energy-dispersive X-ray spectroscopy (EDX) elemental maps were captured using a Thermo Scientific Apreo 2 microscope at a 10 kV accelerating voltage. Elemental mass fractions were quantified through total-reflectance X-ray fluorescence (TXRF) using an S2 PICOFOX spectrometer. XPS characterization was carried out with a PHI VersaProbe 4 instrument using a nonmonochromatic Al K $\alpha$  source (1486.6 eV) using the charge neutralizer. The base pressure of the instrument was  $\sim 10^{-9}$  torr. High-resolution spectra were collected over an analysis area of  $\sim 250 \times 250 \mu\text{m}^2$  using a pass energy of 10 eV. Binding energy calibration was carried out using the C 1s peak for adventitious hydrocarbons at 284.8 eV. Data analysis was performed using CasaXPS software. The spectral fitting parameters for the C 1s, O 1s, Bi 4f, and S 2p peaks were adopted from previous studies.<sup>21–23</sup> Fitting components were modeled using a combination of Gaussian (70%) and Lorentzian (30%) profiles, denoted as GL(30) in CasaXPS, and a standard Shirley-type baseline.

### Electrode preparation and cell assembly

Battery performance tests were performed using LIR2032 coin-type cells following previous cathode and electrolyte compositions.<sup>14,19</sup> For cathode preparation, slurries were prepared by mixing 40 wt% of the MOF powder ( $\sim 50$  mg) with 50 wt% of



carbon black (Super P, TIMCAL) and 10 wt% of polyvinylidene fluoride (PVDF) binder, for a total batch size of 125 mg. The mixture was carefully dissolved in  $\sim 955 \mu\text{L}$  of *N*-methyl-2-pyrrolidone (NMP, density:  $1.03 \text{ g cm}^{-3}$ ) and stirred over 80 minutes using a small magnetic stir bar within 10 mL glass vials. The slurry was then spread onto aluminum foil current collectors using a compact film coater (Xiamen Tmax Battery Equipments Ltd, Model TMAX-TMH). Cathodes were cut into discs with a diameter of 13 mm. The thickness of the film was measured using a digital thickness gauge (Mitutoyo 543-400). A typical cathode contained approximately 0.6 mg of active material with a thickness of  $8 \mu\text{m}$ , excluding the current collector. Coin cells were assembled using the MOF-containing cathode as the working electrode, lithium metal discs as the counter electrode, and a polypropylene microporous separator (Celgard 2400, thickness:  $25 \mu\text{m}$ ). The electrolyte ( $\sim 300 \mu\text{L}$ ) consisted of a mixture of 1,3-dioxolane (DOL) and dimethoxyethane (DME) in a 1:1 volume ratio, 1 M lithium bis(trifluoromethane)sulfonimide (LiTFSI), and 0.2 M  $\text{LiNO}_3$ . For carbonate-based electrolyte tests, the electrolyte consisted of a mixture of ethylene carbonate (EC) and diethyl carbonate (DEC) in a 1:1 volume ratio, 1 M  $\text{LiPF}_6$  as the supporting electrolyte, and 10 vol% of fluoroethylene carbonate (FEC) as an additive. Cell assembly was conducted inside an Ar-filled glovebox (MBRAUN UNILab 2000), maintaining  $\text{O}_2$  and  $\text{H}_2\text{O}$  contents below 0.1 ppm.

### Electrochemical measurements

Tests were conducted using a Gamry Reference 620 potentiostat/galvanostat. The open-circuit potential (OCP) was measured 30 minutes before and after electrochemical measurements. Cyclic voltammetry (CV) scans were conducted within a potential window of 1.5 to 3.0 V vs.  $\text{Li/Li}^+$  at a scan rate of  $0.1 \text{ mV s}^{-1}$ . Electrochemical impedance spectroscopy (EIS) measurements were conducted at stable OCP values at an AC amplitude of 10 mV over a frequency range from 100 kHz to 0.5 Hz. Galvanostatic charge-discharge (GCD) cycling was conducted by charging and discharging the cell at a constant current of 0.18 mA (equivalent to a  $C/2$  rate or  $0.5 \text{ A g}^{-1}$ ) between 1.5 and 3.0 V vs.  $\text{Li/Li}^+$ .

## Results and discussion

Our previous study demonstrated that the SU-101(Bi) MOF achieves a significant uptake of  $\text{H}_2\text{S}$  ( $15.95 \text{ mmol g}^{-1}$ ) from an  $\text{N}_2$  mixture.<sup>20</sup> This uptake exceeds that of other MOF adsorbents such as MIL-47(V) ( $14.6 \text{ mmol g}^{-1}$ )<sup>24</sup> and Ni-CPO ( $12.0 \text{ mmol g}^{-1}$ ),<sup>25</sup> and is comparable to other MOFs examined by our group, including MIL-53(Al)-TDC ( $18.1 \text{ mmol g}^{-1}$ ),<sup>26</sup> and MFM-300(Sc) ( $16.5 \text{ mmol g}^{-1}$ ).<sup>9</sup> The high  $\text{H}_2\text{S}$  uptake has previously been attributed to the strong chemisorption of  $\text{H}_2\text{S}$ , which results in the formation of low-order polysulfides.<sup>9,20</sup> Building upon these reports, we synthesized samples of SU-101, saturated them with  $\text{H}_2\text{S}$  gas, and used them as the active cathode material in Li-S batteries.

The powder X-ray diffraction (PXRD) pattern of the pristine SU-101 MOF corroborates its phase purity (Fig. S2†). Next, a SU-101 sample was activated at 423 K for 10 h under vacuum ( $1.4 \times 10^{-3}$  torr), and the BET surface area was calculated at  $414 \text{ m}^2 \text{ g}^{-1}$ . These parameters are in good correlation with previously reported characterization.<sup>20</sup> Two freshly synthesized samples of SU-101 were exposed to concentrated  $\text{H}_2\text{S}$  (approximately 1500 ppm) in our custom *in situ* adsorption system (Fig. S1†) at different times. The first SU-101 sample was activated at 423 K for 10 h under vacuum and exposed to  $\text{H}_2\text{S}$  for 4 h (labeled as SU-101-4h).  $\text{H}_2\text{S}$  adsorption measurements reveal a complete uptake of about 4.3 mL after 13 minutes (Fig. S3†).

PXRD measurements were carried out to examine the integrity of the crystalline structure after exposure to a diluted  $\text{H}_2\text{S}$  atmosphere (4.3 vol%  $\text{H}_2\text{S}$  with 95.7 vol% of  $\text{N}_2$ , approximately 50 000 ppm). The crystalline structure of SU-101 remains largely unchanged after 4 h of exposure (Fig. S4†), in line with our previous findings.<sup>20</sup> Another SU-101 sample was activated (*vide supra*) and exposed to  $\text{H}_2\text{S}$  for 12 h (labeled as SU-101-Sat). Interestingly, the PXRD pattern indicates a significant change in the crystalline structure, likely due to the amorphization of the SU-101-Sat sample (Fig. S5†). However, the SU-101-Sat sample exhibits distinct diffraction peaks corresponding to the (220), (111), (060), and (002) planes of the simulated SU-101 structure and peak splitting at  $28.7^\circ$ .<sup>27,28</sup> This amorphization phenomenon has been attributed to the de-coordination of the Bi-O bonds, as previously observed for other MOF materials.<sup>8</sup> Therefore, two different SU-101 samples were tested to compare the Li-S battery performance: crystalline SU-101 (SU-101-4h) and partially amorphous SU-101 (SU-101-Sat).

Elemental analysis conducted *via* TXRF revealed sulfur mass fractions of 6.6 and 11.3% for the SU-101-4h and SU-101-Sat samples, respectively (Fig. S6 and Table S1†). SEM images of the Bi(III)-based MOF particles reveal agglomerates of approximately  $15 \mu\text{m}$  in diameter (Fig. 1a). A closer inspection of these particles reveals a spike-like morphology (Fig. 1b), while EDX elemental mappings reveal uniform bismuth, oxygen, and sulfur distribution across the particles (Fig. 1c). Notably, the EDX analysis confirms the presence of sulfur in the MOF particles. Furthermore, the formation of polysulfides was confirmed by Raman spectroscopy (Fig. S7†), with bands at 243 and  $445 \text{ cm}^{-1}$  assigned to  $\text{S}_n^{2-}$  and  $\text{S}_4^{2-}$  species, respectively.<sup>20</sup>

X-ray photoelectron spectroscopy (XPS) characterization was conducted to examine the chemical composition and bonding of the SU-101-Sat MOF. As shown in Fig. 2a, the XPS survey reveals signals for C, S, O, and Bi, which align with the EDX analysis. The C 1s, O 1s, Bi 4f, and S 2p regions were inspected closely, and components were fit accordingly. The C 1s peak exhibits clear components for C-C, C-H, C-OH, and O-C=O functional groups (Fig. 2b), which are present in the building unit of SU-101, ellagic acid.<sup>20</sup> Furthermore, a small component originating from the (C=O)-O-Bi interaction in the SU-101 MOF can be seen at  $\sim 291 \text{ eV}$ .<sup>21</sup> The O 1s region also shows components characteristic of ellagic acid and its interaction with the metallic Bi center (Fig. 2c). The main two signals are caused by oxygen atoms in the carboxylic group interacting with the Bi center, namely (C=O)-O-Bi and (C=O)-O-Bi at around





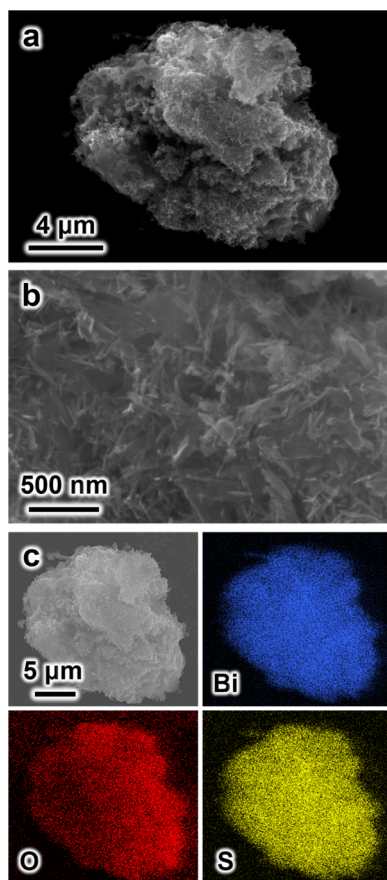


Fig. 1 SEM images of the as-synthesized SU-101-Sat MOF at (a) low and (b) high magnifications. (c) EDX mapping for Bi, O, and S elements in the SU-101-Sat sample.

533.4 and 531.8 eV, respectively. Moreover, a contribution from O–Bi–O bonds can be seen at approximately 530.3 eV.<sup>21</sup> There are no signals ascribable to adsorbed O, confirming the absence of water molecules in the MOF.<sup>22</sup>

As shown in Fig. 2d, the Bi 4f region exhibits two asymmetric peaks at 159.3 and 164.6 eV, corresponding to the Bi 4f<sub>7/2</sub> and 4f<sub>5/2</sub> peaks of Bi<sup>3+</sup> species with a spin–orbit splitting of 5.3 eV.<sup>21,22</sup> In contrast to the typical symmetric peaks of Bi<sub>2</sub>O<sub>3</sub>, the presence of a shoulder at higher binding energies is attributed to the Bi–O–C interaction, typically seen in carboxylic groups coordinating Bi<sup>3+</sup>.<sup>21</sup> Furthermore, a small component was added at approximately 161.7 eV, attributed to terminal sulfur atoms (*n*-S<sub>T</sub><sup>−1</sup>) in polysulfide species.<sup>23,29,30</sup> Note, however, that there are no additional peaks at higher binding energies, which are typically ascribed to bridging S<sup>0</sup> species (−S<sub>B</sub><sup>0</sup>, ~163.9 eV), and oxidized products such as thiosulfate (167.2 eV), polythionate (168.2 eV), and sulfate (169.5 eV).<sup>23,29–32</sup> This result suggests that sulfur is present as a short-chain polysulfide or sulfide species in the SU-101-Sat MOF material after saturation.

Additional XPS analyses were performed on the pristine SU-101 and SU-101-4h samples to examine the effects of H<sub>2</sub>S saturation. The pristine sample exhibits a composition featuring oxygen- and carbon-based functional groups similar to those observed in the SU-101-Sat sample. Bismuth is

predominantly involved in Bi–O–C interactions and has no components related to sulfur species (Fig. S8†). In contrast, the SU-101-4h sample reveals a small contribution from an additional component attributed to terminal sulfur (Fig. S9†). Furthermore, the O–Bi–O component, absent in the pristine sample, becomes more pronounced with increasing saturation times (see Fig. 2d, S8d, and S9d†). In contrast, the same component in the O 1s region decreases in intensity (see Fig. 2c, S8c, and S9c†). These results indicate that the Bi–O interaction is likely affected by the incorporation of sulfur. It is also conceivable that the O–Bi–O component in the Bi 4f region might represent a combination of Bi–O and Bi–S interactions. However, this is challenging to confirm due to the complex overlap of Bi 4f and S 2p signals.

The interference between Bi and S species complicates the analysis of sulfur interactions in the S 2p region. Therefore, we also probed the S 2s region to determine the composition of sulfur in the SU-101 MOFs. While the pristine SU-101 samples exhibit no peaks in the S 2s region, both the SU-101-4h and SU-101-Sat samples display clear signals, with the signal for the SU-101-Sat sample being more intense (Fig. S10†). The peaks were fitted into two components at approximately 225.8 and 227.8 eV. Given that the S 2p and S 2s peaks are separated by about 64.0 ± 0.2 eV,<sup>33</sup> the sulfur species data in the S 2p region (SO<sub>4</sub><sup>2−</sup>: 169.5 eV; SO<sub>3</sub><sup>2−</sup>: 166.8 eV; S<sub>n</sub>: 164.0 eV; −S<sub>B</sub><sup>0</sup>: ~163.9 eV; S<sub>2</sub><sup>2−</sup>: 162.9 eV; S<sub>2</sub><sup>−</sup>: 161.9 eV; *n*-S<sub>T</sub><sup>−1</sup>: ~161.7 eV) enable us to assign the observed components in the S 2s region.<sup>23,29,30,33</sup> More reduced species are present at lower binding energies, while more oxidized species appear at higher ones. Consequently, the stronger component at the lower binding energy (~225.8 eV) can be attributed to either terminal sulfur (*n*-S<sub>T</sub><sup>−1</sup>, ~225.7 eV) or S<sup>2−</sup> (225.9 eV), while the less intense peak at higher binding energy may correspond to either bridging sulfur (−S<sub>B</sub><sup>0</sup>, ~227.9 eV) or elemental sulfur (S<sub>n</sub>, ~228.0 eV). Consistent with previous studies,<sup>33,34</sup> these results suggest that sulfur within the MOF is predominantly reduced, likely as short-chain polysulfides, with only a small fraction of sulfur existing as S<sub>n</sub> species.

Building on previous studies of SU-101,<sup>9,10,20,35</sup> and based on the physical and chemical characterization results from this study, we propose a reaction mechanism for the formation of polysulfides (illustrated in Fig. S11†). First, the SU-101 MOF is activated by the removal of water molecules. Subsequently, H<sub>2</sub>S molecules adsorb onto exposed Bi<sup>3+</sup> sites. These coordinated H<sub>2</sub>S molecules then undergo a dissociation step where protons are removed. Given the proximity (3.78 Å) between adjacent Bi<sup>3+</sup> sites, the sulfur atoms are oxidized, forming an S–S bond and the concurrent release of H<sub>2</sub>. Finally, the resultant sulfur species are released, completing the reaction cycle.

To evaluate the battery performance, we prepared cathodes from SU-101 slurries (Fig. S12a†) and paired them with Li metal anodes to assemble coin cells (Fig. S12b†). A detailed battery composition checklist is shown in Table S2.† Cyclic voltammetry tests were conducted to characterize the redox processes of these MOF-containing Li–S batteries. The batteries comprised an MOF-containing cathode encapsulated with a separator and a Li metal anode in a commercial coin cell setup (Fig. 3a). As shown in Fig. 3b, the cathodes containing the SU-



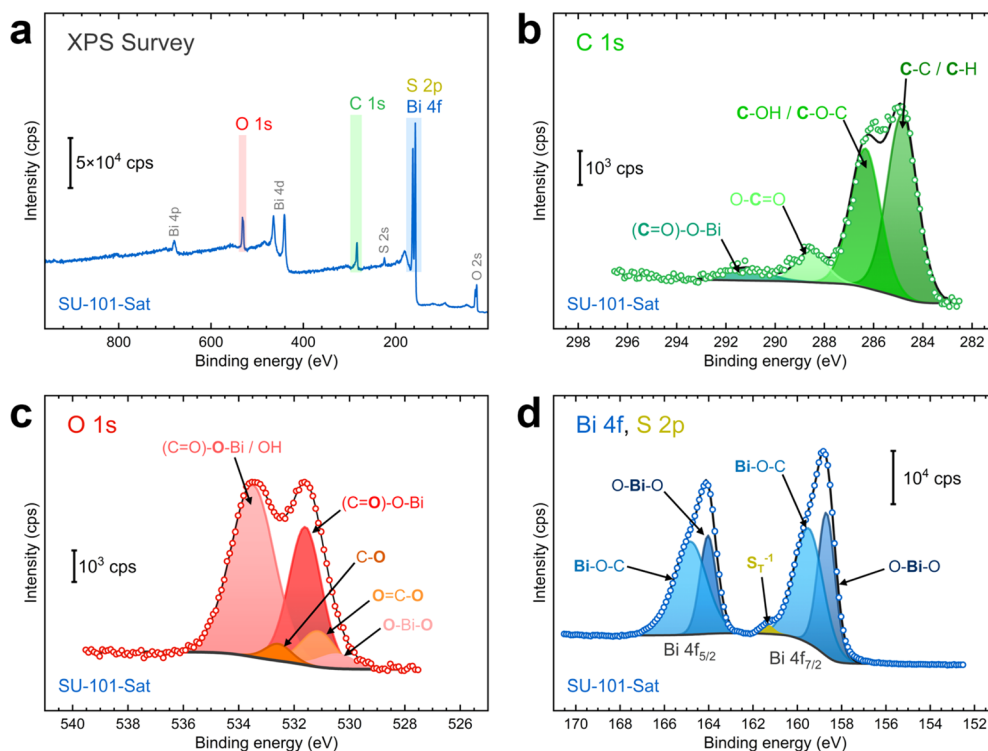


Fig. 2 XPS characterization of the SU-101-Sat sample: (a) XPS survey, (b) C 1s region, (c) O 1s region, and (d) Bi 4f/S 2p regions. The labels indicate the specific bonds of the functional groups related to each component fitted to the spectra. Green, red, yellow, and blue tones refer to carbon-, oxygen-, sulfur-, and bismuth-based groups.

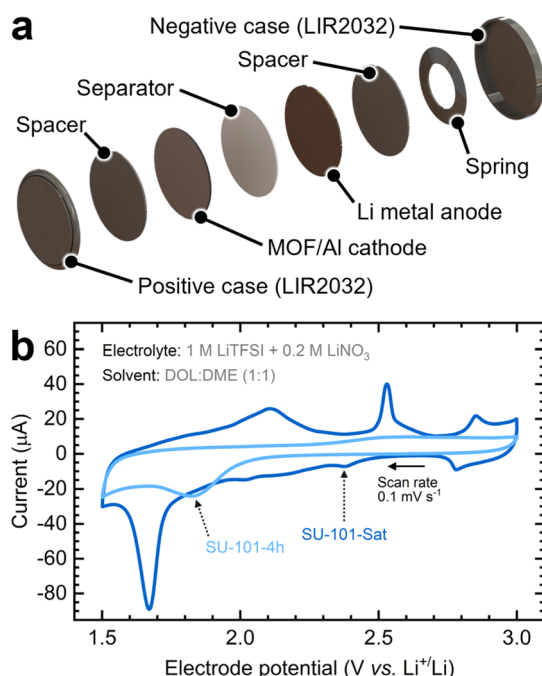


Fig. 3 (a) Exploded-view 3D rendering of the Li-S battery coin cell and its components. (b) Cyclic voltammograms of SU-101-4h and SU-101-Sat cathodes assembled into coin cells. The second CV scan is shown for each cathode. The arrow indicates the scan direction at the specified scan rate.

101 MOFs show clear reduction and oxidation signals. During the reduction scan, sulfur species within SU-101-Sat reduce to  $\text{Li}_2\text{S}$  sequentially, transitioning through various polysulfide intermediates. In the case of the SU-101-Sat, the cathode exhibits multiple subtle peaks and plateaus between 2.5 and 1.9 V vs.  $\text{Li}/\text{Li}^+$ , indicative of the transformation from  $\text{S}_8$  to longer-chain intermediates ( $\text{Li}_2\text{S}_x$  where  $x \geq 4$ ) at relatively higher potentials and to shorter-chain intermediates ( $\text{Li}_2\text{S}_x$  where  $x < 4$ ) at lower potentials.<sup>18,36,37</sup> These transformations align with the XPS results (Fig. S10<sup>†</sup>), suggesting that the initial fraction of  $\text{S}_n$  species is converted into intermediates during cycling. A pronounced peak appears around 1.7 V, associated with the strong confinement of sulfur within the partially amorphous MOF (SU-101-Sat). The sharpness of this peak has been attributed to strong chemical adsorption and rapid conversion.<sup>14</sup>

During the oxidation scan, two peaks emerge at approximately 2.1 V and 2.5 V, corresponding to the gradual oxidation of short-chain polysulfides back to longer chains and ultimately to  $\text{S}_8$ .<sup>14</sup> A pair of redox peaks, observed at around 2.8 V and 2.9 V, exhibit some degree of reversibility and persistence over successive cycles. These peaks, previously unreported in the literature on MOF-based Li-S batteries,<sup>14,19,36</sup> can be attributed to the high potential polarization of polysulfide peaks influenced by the interaction of the metal center ( $\text{Bi(III)}$ ) with polysulfides of short length as also demonstrated by XPS.<sup>37–39</sup>

Interestingly, the SU-101-4h cathode displays more subdued redox signals, suggesting that the polysulfide intermediates



undergo gradual reactions, resulting in broader redox peaks and extended plateaus.<sup>18</sup> This diminished intensity might also stem from less sulfur participating in the reactions, unlike the SU-101-Sat cathode material, which was saturated with H<sub>2</sub>S for an extended period, and the crystalline structure of SU-101 was partially lost (Fig. S5†).

The cycling performance of the MOF-containing cathodes was further examined through galvanostatic charge/discharge tests at a  $C/2$  rate using an identical coin cell setup. Typical potential *versus* time curves depicting the charge and discharge profiles at a constant current were used to extract the capacity for each cycle (Fig. S13†). The SU-101-Sat cathode exhibits distinct plateaus aligning with the redox signals identified in CV scans. The charge profile is characterized by a notable slope change at approximately 2.1 V and a more pronounced plateau at  $\sim 2.7$  V, while the discharge profile presents a sharp slope transition at  $\sim 2.7$  V and a prolonged plateau below 1.9 V, indicative of the sequential reduction of short-chain polysulfides to insoluble Li<sub>2</sub>S.<sup>18</sup> As shown in Fig. 4a, this pattern is also discernible when examining the charge/discharge profiles based on the capacity after 100 cycles. The SU-101-Sat cathode achieves the highest capacity at  $\sim 66$  mA h g<sup>-1</sup>, followed closely by the SU-101-4h cathode at  $\sim 48$  mA h g<sup>-1</sup>. As shown in Fig. 4b, the cycling performance tests indicate an initial capacity reduction for the SU-101-Sat cathode, which stabilizes after 80 cycles. In contrast, the SU-101-4h cathode demonstrates a more consistent cycling performance. These observations suggest that while the SU-101-Sat possesses a more abundant sulfur content available for cycling, a portion is depleted during the cycles until a stable composition is attained. On the other hand, the SU-101-4h cathode contains a lower amount of sulfur available, slightly below the stable composition threshold. The decreased sulfur content accounts for the  $\sim 22\%$  capacity reduction compared to the SU-101-Sat cathode. Capacity measurements over cycling show that both SU-101 compositions (SU-101-4h and SU-101-Sat) maintain average coulombic efficiencies of 99.88% and 99.76%, respectively, confirming the reversibility of the Li-S battery (Fig. S14†).

EIS analysis was conducted to study the influence of the electrochemical processes on the ionic and electronic resistances of the cells. Fig. 4c shows Nyquist plots for SU-101 cathodes (SU-101-4h and SU-101-Sat), revealing distinct characteristics. A modified equivalent circuit model was applied to derive parameters such as the ohmic resistance ( $R_s$ ), charge-transfer resistance ( $R_{ct}$ ), double-layer capacitance ( $C_{dl}$ ), and the Warburg impedance ( $Z_w$ ) from the Nyquist plots (Table S3†). The  $R_s$  values for the SU-101-Sat and SU-101-4h cathodes after cycling are  $\sim 2.6$  and  $\sim 6.8$   $\Omega$ , respectively, aligning with expectations for this electrolyte composition.<sup>37–40</sup> A similar pattern emerges for the  $R_{ct}$  values, with the SU-101-Sat cathode demonstrating the lowest resistance at 74.9  $\Omega$ . Note, however, that the  $R_{ct}$  values increase slightly after cycling, which can be attributed to the formation of Li<sub>2</sub>S<sub>2</sub> and Li<sub>2</sub>S films on the cathode surfaces. These films act as barriers, being ionically and electronically insulating.<sup>18</sup> The intrinsic low electrical conductivity of SU-101-4h and SU-101-Sat, coupled with other polysulfide species dissolved in the electrolyte, further explains this increase in  $R_{ct}$ .<sup>18,41</sup> However, this increase does not

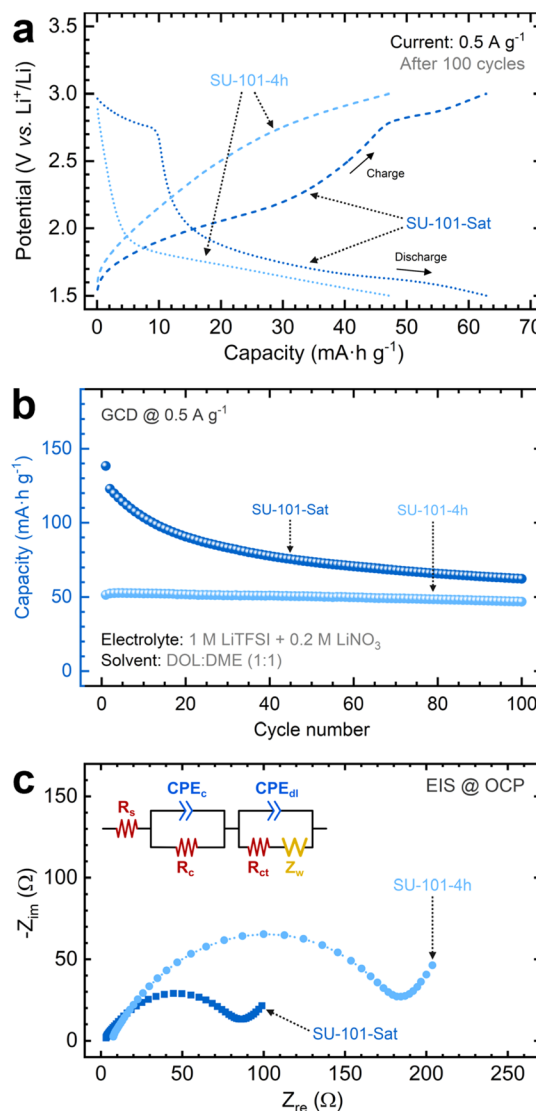


Fig. 4 (a) Galvanostatic charge–discharge curves of the SU-101-4h and SU-101-Sat cathodes after cycling at a  $C/2$  rate ( $0.5 \text{ A g}^{-1}$ ) between 1.5 and 3.0 V vs. Li/Li<sup>+</sup>. Charge profiles are depicted with dashed lines, while discharge profiles are depicted with dotted lines. Arrows indicate the charge and discharge directions. (b) Capacity decay tests of SU-101-4h and SU-101-Sat cathodes for 100 cycles. Each sphere represents the capacity measured from one charge–discharge cycle. (c) Nyquist plots after cycling performance tests measured at the open circuit potential (OCP). The inset depicts the equivalent circuit model used to fit Nyquist plots.

lead to complete battery failure after 100 cycles. Furthermore, the data in Table S3† reveals that both SU-101-4h and SU-101-Sat exhibit comparably similar  $C_{dl}$  values, suggesting similar surface areas, independently of the crystallinity grade of SU-101 (*i.e.*, crystalline *vs.* amorphous). Finally, both cathodes experience increased  $Z_w$  values after cycling, indicating higher resistance towards Li ion diffusion and aligning with the  $R_{ct}$  trend explained by the surface passivation of insoluble, short-chain polysulfides. However, the SU-101-Sat cathode exhibits a lower  $Z_w$  value, indicating decreased lithium ion diffusion resistance compared to SU-101-4h.<sup>38</sup>



Given the superior performance of the SU-101-Sat cathode compared to SU-101-4h, we extended the cycling performance tests to 1000 cycles. CV scans illustrate a marked decrease in intensity for the reduction and oxidation peaks with prolonged cycling, as depicted in Fig. 5a. The peak at  $\sim 1.7$  V attributed to confined sulfur decreases after cycling, indicating the consumption of some initially retained sulfur within the amorphous SU-101. Nonetheless, persistent redox signals between 2.3 and 2.0 V denote the ongoing and reversible presence of intermediate polysulfide species during cycling. Fig. 5b

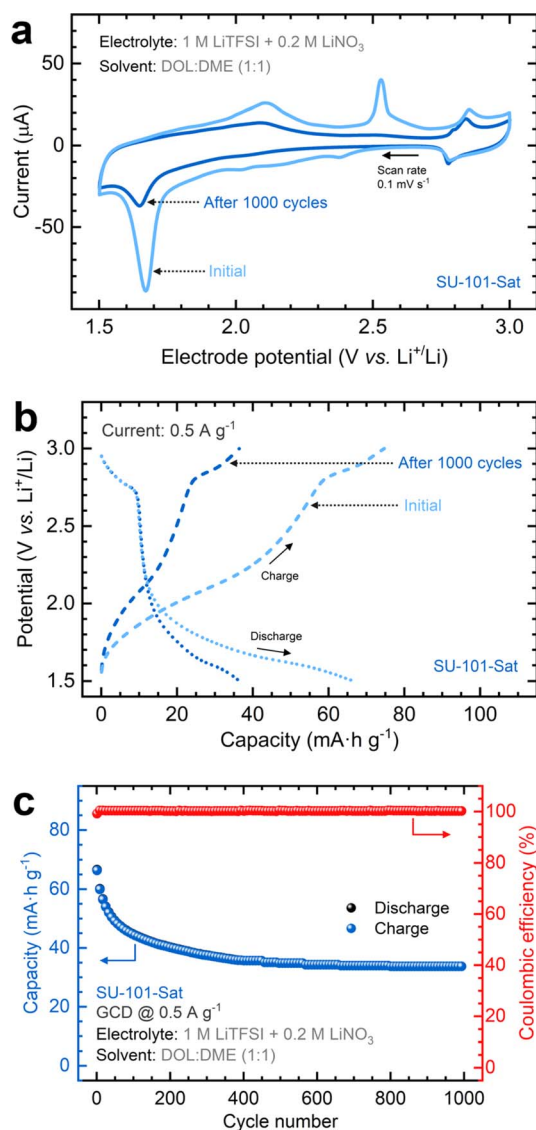
demonstrates that prolonged cycling of the SU-101-Sat cathode results in a capacity reduction of approximately 52%. However, charge and discharge plateaus remain distinctly visible. The cycling performance curves shown in Fig. 5c reveal that most capacity decay occurs in the initial 400 cycles without losing coulombic efficiency until the coin cell achieves a stable response (capacity:  $34 \text{ mA h g}^{-1}$ ). Further EIS analysis (Table S4†) reveals a slight increase in the  $R_{ct}$  and the  $Z_w$  values, aligning with the same trend observed after 100 cycles to the formation of insulating films during cycling.

To evaluate the performance variability of cathodes prepared in different batches, replicate experiments were conducted, with the results included in the ESI (Fig. S15).† Despite the variation in capacity values, particularly in the initial capacity ( $84.6 \text{ mA h g}^{-1}$  on average), all three cells displayed similar decay patterns, resulting in an average final capacity of  $45.6 \text{ mA h g}^{-1}$  after 1000 cycles, corresponding to an average capacity retention of about 54%.

These findings suggest that an excess uptake of polysulfides is initially consumed during the early cycles until a stable solid-electrolyte interphase is formed. Although the SU-101-Sat cathode exhibited an initial capacity decay, it ultimately achieved the highest final capacity and the lowest charge-transfer and diffusion resistances compared to SU-101-4h. However, both materials demonstrated satisfactory reversibility, maintaining average coulombic efficiencies of about 99.8%. This finding is attributed to the control over and release of polysulfide species facilitated by the unique architecture and chemistry of SU-101, which preserved the crystalline structure, particularly achieving only partial amorphization. It is worth noting that, in contrast to conventional practices, the sulfur in the cathode is not deliberately introduced during synthesis. Instead, it is sequestered by SU-101 from the spontaneous transformation of  $\text{H}_2\text{S}$  to polysulfides (at room temperature and atmospheric pressure) and subsequently serves as the electro-active element in the Li-S battery.

We also explored using carbonate-based electrolytes, which require specialized sulfur cathodes designed to limit polysulfide formation to short-chain species.<sup>42</sup> Coin cells were assembled using the configuration detailed in Table S2,† substituting the ether-based electrolyte with a mixture of EC:DEC (1:1 in volume) in 1 M  $\text{LiPF}_6$  and FEC as an additive. Fig. S16† illustrates the battery performance results of the SU-101-Sat cathode operating with the carbonate-based electrolyte.

CV scans of the SU-101-Sat cathode in the carbonate electrolyte are quite similar to those in the ether-based electrolyte (Fig. S16a†), particularly with notable peaks between 2.5 and 1.9 V vs.  $\text{Li/Li}^+$  attributed to the formation of shorter-chain sulfur intermediates and the distinct peak at 1.7 V attributed to sulfur confinement. However, the absence of an oxidation peak at 2.5 V suggests that the gradual oxidation of polysulfides back into  $\text{S}_8$  was limited. Despite exhibiting similar ohmic resistance, capacitance, and Warburg impedance values to those in the ether electrolyte, EIS analysis reveals a significant increase in the charge-transfer resistance when operating in the carbonate electrolyte (Fig. S16b and Table S5†). Cycling performance tests for over 1000 cycles revealed a battery capacity nearly five times



**Fig. 5** Extended cycling performance tests for the SU-101-Sat MOF cathode: (a) cyclic voltammograms and (b) galvanostatic charge-discharge profiles before and after 1000 cycles. (c) Cycling performance plot showing the capacity on the left axis and the coulombic efficiency on the right axis. Each sphere represents the capacity measured during charge (blue) and discharge (black). Discharge and charge profiles are plotted concurrently. Red spheres represent the coulombic efficiency measured for each charge-discharge cycle. Cycling was conducted at a rate of  $C/2$  ( $0.5 \text{ A g}^{-1}$ ) between 1.5 and 3.0 V vs.  $\text{Li/Li}^+$ . Electrolyte: 1 M LiTFSI + 0.2 M  $\text{LiNO}_3$  in DME : DOL 1 : 1 solvent.



lower than that observed in the ether electrolyte. After an initially higher discharging step (Fig. S16c†), the capacity quickly stabilized around  $7 \text{ mA h g}^{-1}$  (Fig. S16d†). Thus, despite a lower experimental capacity, the SU-101-Sat cathode in the carbonate electrolyte displays stable performance over 1000 cycles, with a coulombic efficiency of 99.7%.

The abrupt drop in capacity and subsequent stabilization, along with a significantly lower initial coulombic efficiency (approximately 89.9%, see Fig. S16d†), suggest that the cathode material undergoes an initial chemical transformation that drastically reduces the capacity in carbonate electrolytes. In line with the observed increase in charge-transfer resistance and the absence of a strong oxidation peak at 2.5 V, it seems that not all sulfur intermediates participate in the reaction, and operation in carbonate electrolytes restricts the battery's reversibility. The chemistry and associated transformations in this environment are beyond the scope of our study, and we encourage future investigations to examine the interaction of carbonate electrolytes with MOF cathodes more thoroughly.

Finally, the capacity of the SU-101-Sat cathode ( $45.6 \text{ mA h g}^{-1}$ ) is relatively modest compared to other examples of Li-S batteries in the literature (Table S6†). Although this capacity does not set new records, the high cycle life and coulombic efficiency over 1000 cycles offer a valuable opportunity for creating low-energy batteries with long cyclability. These batteries could be suitable for powering small portable devices, satellite components, and weather station sensors.<sup>43,44</sup> Hence, this proof-of-concept Li-S battery not only showcases the potential of MOF materials in capturing toxic gas emissions but also demonstrates a successful example of sustainable waste valorization and its successful application in electrochemical energy technologies.

A major concern regarding the use of MOFs in energy technology applications is their economic viability and scalability. Although there is a clear need for more robust and specific techno-economic assessments in the future, using these specific MOF materials could prove competitive for industrial applications. For instance, a bio-derived MIL-160(Al) MOF costs about \$55 per kg at a production scale of 100 tons per year, which could be further reduced to \$29.5 per kg at 1 kton per year.<sup>45</sup> The SU-101 MOF is synthesized from ellagic acid, a linker abundant in strawberries, raspberries, grapes, walnuts, pecans, and pomegranates.<sup>46,47</sup> Thus, a bio-derived SU-101 material could potentially be synthesized at a large scale using a similar approach to MIL-160(Al).<sup>20</sup> Given the biocompatibility of ellagic acid and the low toxicity of bismuth, the synthesis of bio-derived SU-101 offers a competitive and environmentally friendly approach for commercializing MOF-based technologies.

The waste valorization strategy proposed in our study offers critical environmental benefits. A significant challenge with adsorbent materials used for toxic gas capture is that they merely transfer pollutants into a solid residue, failing to remove them effectively from the environment.<sup>48</sup> Our approach not only captures  $\text{H}_2\text{S}$  but also repurposes the resulting solid waste into useful materials for energy technology applications, thereby fostering a circular economy where materials are reused rather than discarded, minimizing additional waste generation.<sup>49</sup>

Furthermore, life cycle assessment (LCA) studies have enhanced our understanding of the environmental impact of MOFs and Li-S battery technologies. LCA studies have identified solvent use during MOF synthesis as a critical hotspot for environmental impact,<sup>50</sup> particularly with organic solvents like DMF and THF. In contrast, solvents like ethanol and methanol are considered more environmentally friendly.<sup>51,52</sup> Our synthesis approach for SU-101, which occurs in aqueous media, supports the sustainability of our method.

Regarding the environmental impact of Li-S batteries, the electricity source, cycle life, and specific energy density are critical factors in the cradle-to-grave LCA impacts. The cyclability is particularly relevant, as longer lifetimes mean cells need replacing less frequently, which reduces environmental impacts across all categories. The LCA study by Wickerts and coworkers assumes a baseline of 1500 cycles, aligning closely with our reported lifespan of 1000 cycles, which is significantly higher than previous studies (<500 cycles, see Table S6†).<sup>53</sup> Moreover, compared to traditional Li-ion batteries, which often contain toxic metals like nickel, cobalt, and manganese, Li-S batteries have a lower environmental footprint.<sup>54,55</sup> Given the proven biocompatibility and lower toxicity of the Bi-based SU-101,<sup>20</sup> our approach is also expected to have a lower environmental impact than other conventional battery technologies containing more toxic metals.

Following the demonstration of our proof-of-concept study, we encourage the community to explore further the potential of these promising materials in electrochemical energy storage and conversion. There is a substantial opportunity to enhance our understanding of battery performance, economic viability, and the environmental impacts of waste valorization strategies using toxic gas adsorbents and MOF-based cathode materials.

## Conclusions

We present an experimental proof-of-concept SU-101-Sat MOF cathode exhibiting remarkable performance similar to standard Li-S batteries reported in the literature. Despite an initial capacity reduction, commonly observed in MOF-derived Li-S batteries during the initial conditioning phase, this cathode exhibited a stable performance and maintained nearly 99.8% coulombic efficiency across 1000 cycles. This resilience is attributed to the controlled release of polysulfides, a characteristic feature facilitated by the chemical composition of SU-101 (*i.e.*, Bi(III) metal centers) and the unique chemical transformation of  $\text{H}_2\text{S}$  to polysulfides at room temperature and atmospheric pressure by the SU-101 MOF. These findings highlight the potential of MOF materials to spontaneously transform toxic  $\text{H}_2\text{S}$  emissions into polysulfides independently of fully maintaining the crystalline structure of the framework. This approach is a promising candidate for implementing toxic waste valorization strategies and subsequent applications in electrochemical energy storage applications.

## Author contributions

R.A. Marquez: conceptualization, investigation, methodology, formal analysis, visualization, writing – original draft, project





administration. J. L. Obeso: investigation, methodology, formal analysis, visualization, writing – original draft. R. R. Vaidyula: investigation, methodology, writing – review & editing. V. B. López-Cervantes: investigation, methodology, writing – review & editing. R. A. Peralta: conceptualization. P. Marín Rosas: investigation. J. A. de los Reyes: resources, funding acquisition. C. B. Mullins: writing – review & editing, resources, funding acquisition, project administration. I. A. Ibarra: writing – original draft, resources, funding acquisition, project administration. All authors have approved the final version of the manuscript.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

The authors acknowledge PAPIIT-UNAM (Grant IN202820), Mexico and the Welch Foundation (Grant F-1436), United States, for their generous financial support. R. A. M., V. B. L.-C., and J. L. O. acknowledge CONAHCYT for their PhD scholarship award (919871, 1005649, 1003953). Thanks to U. Winnberg (Pharma View Consulting SC) for scientific discussions and G. Ibarra-Winnberg for conceptualizing the design of this contribution.

## References

- 1 A. Cincinelli and T. Martellini, *Int. J. Environ. Res. Public Health*, 2017, **14**, 1286.
- 2 Z. Jianwen, L. Da and F. Wenxing, *J. Hazard. Mater.*, 2014, **264**, 350–362.
- 3 S. Çetinyokuş, *Process Saf. Prog.*, 2023, **42**, 469–480.
- 4 S. L. Malone Rubright, L. L. Pearce and J. Peterson, *Nitric Oxide*, 2017, **71**, 1–13.
- 5 D. H. Truong, M. A. Eghbal, W. Hindmarsh, S. H. Roth and P. J. O'Brien, *Drug Metab. Rev.*, 2006, **38**, 733–744.
- 6 A. A. Khan, M. M. Schuler, M. G. Prior, S. Yong, R. W. Coppock, L. Z. Florence and L. E. Lillie, *Toxicol. Appl. Pharmacol.*, 1990, **103**, 482–490.
- 7 M. S. Shah, M. Tsapatsis and J. I. Siepmann, *Chem. Rev.*, 2017, **117**, 9755–9803.
- 8 E. Martínez-Ahumada, A. López-Olvera, V. Jancik, J. E. Sánchez-Bautista, E. González-Zamora, V. Martis, D. R. Williams and I. A. Ibarra, *Organometallics*, 2020, **39**, 883–915.
- 9 J. G. Flores, J. A. Zárate-Colín, E. Sánchez-González, J. R. Valenzuela, A. Gutiérrez-Alejandre, J. Ramírez, V. Jancik, J. Aguilar-Pliego, M. C. Zorrilla, H. A. Lara-García, E. González-Zamora, G. Guzmán-González, I. González, G. Maurin and I. A. Ibarra, *ACS Appl. Mater. Interfaces*, 2020, **12**, 18885–18892.
- 10 J. L. Obeso, D. R. Amaro, C. V. Flores, A. Gutiérrez-Alejandre, R. A. Peralta, C. Leyva and I. A. Ibarra, *Coord. Chem. Rev.*, 2023, **485**, 215135.
- 11 R. Fang, S. Zhao, Z. Sun, D. Wang, H. Cheng and F. Li, *Adv. Mater.*, 2017, **29**, 1606823.
- 12 M. Zhao, B. Li, H. Peng, H. Yuan, J. Wei and J. Huang, *Angew. Chem., Int. Ed.*, 2020, **59**, 12636–12652.
- 13 S. Ponnada, M. S. Kiai, D. B. Gorle, S. Rajagopal, S. Andra, A. Nowduri and K. Muniasamy, *Energy Fuels*, 2021, **35**, 11089–11117.
- 14 Z. Wang, X. Li, Y. Cui, Y. Yang, H. Pan, Z. Wang, C. Wu, B. Chen and G. Qian, *Cryst. Growth Des.*, 2013, **13**, 5116–5120.
- 15 W. Bao, Z. Zhang, Y. Qu, C. Zhou, X. Wang and J. Li, *J. Alloys Compd.*, 2014, **582**, 334–340.
- 16 Z. Zhang, Y. An, J. Feng, L. Ci, B. Duan, W. Huang, C. Dong and S. Xiong, *Mater. Lett.*, 2016, **181**, 340–344.
- 17 Z. Zhang, H. Yoshikawa and K. Awaga, *Chem. Mater.*, 2016, **28**, 1298–1303.
- 18 X. Huang, T. Qiu, X. Zhang, L. Wang, B. Luo and L. Wang, *Mater. Chem. Front.*, 2020, **4**, 2517–2547.
- 19 X. Liu, S. Wang, A. Wang, Z. Wang, J. Chen, Q. Zeng, P. Chen, W. Liu, Z. Li and L. Zhang, *J. Mater. Chem. A*, 2019, **7**, 24515–24523.
- 20 E. S. Grape, J. G. Flores, T. Hidalgo, E. Martínez-Ahumada, A. Gutiérrez-Alejandre, A. Hautier, D. R. Williams, M. O'Keeffe, L. Öhrström, T. Willhammar, P. Horcajada, I. A. Ibarra and A. K. Inge, *J. Am. Chem. Soc.*, 2020, **142**, 16795–16804.
- 21 J. Rodríguez-Pereira, S. A. Rincón-Ortiz and R. Ospina, *Surf. Sci. Spectra*, 2020, **27**, 024001.
- 22 V. H. Nguyen, T. D. Nguyen and T. Van Nguyen, *Top. Catal.*, 2020, **63**, 1109–1120.
- 23 M. Fantauzzi, B. Elsener, D. Atzei, A. Rigoldi and A. Rossi, *RSC Adv.*, 2015, **5**, 75953–75963.
- 24 L. Hamon, C. Serre, T. Devic, T. Loiseau, F. Millange, G. Férey and G. D. Weireld, *J. Am. Chem. Soc.*, 2009, **131**, 8775–8777.
- 25 P. K. Allan, P. S. Wheatley, D. Aldous, M. I. Mohideen, C. Tang, J. A. Hriljac, I. L. Megson, K. W. Chapman, G. D. Weireld, S. Vaesen and R. E. Morris, *Dalton Trans.*, 2012, **41**, 4060–4066.
- 26 J. A. Zárate, E. Sánchez-González, T. Jurado-Vázquez, A. Gutiérrez-Alejandre, E. González-Zamora, I. Castillo, G. Maurin and I. A. Ibarra, *Chem. Commun.*, 2019, **55**, 3049–3052.
- 27 Y.-H. Zou, X. Wang, F. Ning, J. Yi and Y. Liu, *Sep. Purif. Technol.*, 2023, **317**, 123806.
- 28 Q. Zhang, Y. Liu, Z. Wang, P. Wang, Z. Zheng, H. Cheng, X. Qin, X. Zhang, Y. Dai and B. Huang, *J. Colloid Interface Sci.*, 2022, **617**, 578–584.
- 29 F. Liu, Q. Xiao, H. B. Wu, F. Sun, X. Liu, F. Li, Z. Le, L. Shen, G. Wang, M. Cai and Y. Lu, *ACS Nano*, 2017, **11**, 2697–2705.
- 30 X. Liang, C. Hart, Q. Pang, A. Garsuch, T. Weiss and L. F. Nazar, *Nat. Commun.*, 2015, **6**, 5682.
- 31 Z. Zhang, J.-N. Wang, A.-H. Shao, D.-G. Xiong, J.-W. Liu, C.-Y. Lao, K. Xi, S.-Y. Lu, Q. Jiang, J. Yu, H.-L. Li, Z.-Y. Yang and R. V. Kumar, *Sci. China Mater.*, 2020, **63**, 2443–2455.
- 32 Y. Wu, T. Momma, S. Ahn, T. Yokoshima, H. Nara and T. Osaka, *J. Power Sources*, 2017, **366**, 65–71.



- 33 G. A. Bukhtiyarova, V. I. Bukhtiyarov, N. S. Sakaeva, V. V. Kaichev and B. P. Zolotovskii, *J. Mol. Catal. A: Chem.*, 2000, **158**, 251–255.
- 34 R. Malakooti, L. Cademartiri, Y. Akçakir, S. Petrov, A. Migliori and G. A. Ozin, *Adv. Mater.*, 2006, **18**, 2189–2194.
- 35 A. López-Olvera, J. G. Flores, J. Aguilar-Pliego, C. K. Brozek, A. Gutiérrez-Alejandre and I. A. Ibarra, *Chem. Mater.*, 2021, **33**, 6269–6276.
- 36 R. Demir-Cakan, M. Morcrette, F. Nouar, C. Davoisne, T. Devic, D. Gonbeau, R. Dominko, C. Serre, G. Férey and J.-M. Tarascon, *J. Am. Chem. Soc.*, 2011, **133**, 16154–16160.
- 37 K. Zou, X. Chen, W. Jing, X. Dai, P. Wang, Y. Liu, R. Qiao, M. Shi, Y. Chen, J. Sun and Y. Liu, *Energy Storage Mater.*, 2022, **48**, 133–144.
- 38 Z. Li, K. Hu, J. Guo, Y. Zhang, M. Zhang and J. Lian, *J. Mater. Sci.*, 2023, **58**, 2234–2248.
- 39 T. Li, C. Ma, Y. Li, F. Tu, C. Jiao, Z. Li and S. Yao, *Ionics*, 2022, **28**, 1701–1711.
- 40 X. Zhou, X. Luo, H. Wang, J. Yang, H. Xu, M. Jia and J. Tang, *J. Mater. Sci.*, 2019, **54**, 9622–9631.
- 41 S. Suriyakumar, G. J. Rani and A. M. Stephan, *Ionics*, 2020, **26**, 2201–2210.
- 42 X. Li, M. Banis, A. Lushington, X. Yang, Q. Sun, Y. Zhao, C. Liu, Q. Li, B. Wang, W. Xiao, C. Wang, M. Li, J. Liang, R. Li, Y. Hu, L. Goncharova, H. Zhang, T.-K. Sham and X. Sun, *Nat. Commun.*, 2018, **9**, 4509.
- 43 S. Dörfler, S. Walus, J. Locke, A. Fotouhi, D. J. Auger, N. Shateri, T. Abendroth, P. Härtel, H. Althues and S. Kaskel, *Energy Technol.*, 2021, **9**, 2000694.
- 44 A. Fotouhi, D. J. Auger, L. O'Neill, T. Cleaver and S. Walus, *Energies*, 2017, **10**, 1937.
- 45 M. I. Severino, E. Gkaniatsou, F. Nouar, M. L. Pinto and C. Serre, *Faraday Discuss.*, 2021, **231**, 326–341.
- 46 K. R. Määttä-Riihinen, A. Kamal-Eldin and A. R. Törrönen, *J. Agric. Food Chem.*, 2004, **52**, 6178–6187.
- 47 M. N. Clifford and A. Scalbert, *J. Sci. Food Agric.*, 2000, **80**, 1118–1125.
- 48 E.-S. M. El-Sayed and D. Yuan, *Green Chem.*, 2020, **22**, 4082–4104.
- 49 S. Geisendorf and F. Pietrulla, *Thunderbird Int. Bus. Rev.*, 2018, **60**, 771–782.
- 50 P. G. Jessop and A. R. MacDonald, *Green Chem.*, 2023, **25**, 9457–9462.
- 51 C. A. Grande, R. Blom, A. Spjelkavik, V. Moreau and J. Payet, *Sustainable Mater. Technol.*, 2017, **14**, 11–18.
- 52 H. U. Escobar-Hernandez, Y. Quan, M. I. Papadaki and Q. Wang, *ACS Sustainable Chem. Eng.*, 2023, **11**, 4219–4225.
- 53 S. Wickerts, R. Arvidsson, A. Nordelöf, M. Svanström and P. Johansson, *ACS Sustainable Chem. Eng.*, 2023, **11**, 9553–9563.
- 54 G. Benveniste, A. Sánchez, H. Rallo, C. Corchero and B. Amante, *Resour. Conserv. Recycl. Adv.*, 2022, **15**, 200086.
- 55 Y. Deng, J. Li, T. Li, X. Gao and C. Yuan, *J. Power Sources*, 2017, **343**, 284–295.

