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Titanosilicate zeolite precursors for highly efficient oxidation reactions†

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Titanosilicate zeolites are catalysts of interest in the field of fine chemicals. However, the generation and accessibility of active sites in titanosilicate materials for catalyzing reactions with large molecules is still a challenge. Herein, we prepared titanosilicate zeolite precursors with open zeolitic structures, tunable pore sizes, and controllable Si/Ti ratios through a hydrothermal crystallization strategy by using quaternary ammonium templates. A series of quaternary ammonium ions are discovered as effective organic templates. The prepared amorphous titanosilicate zeolites with some zeolite framework structural order have extra-large micropores and abundant octahedrally coordinated isolated Ti species, which lead to a superior catalytic performance in the oxidative desulfurization of dibenzothiophene (DBT) and epoxidation of cyclohexene. It is anticipated that the amorphous prezeolitic titanosilicates will benefit the catalytic conversion of bulky molecules in a wide range of reaction processes.

Introduction

Zeolites are crystalline microporous silica-based materials with well-defined pores and cavities that play a fundamental role in ion-exchange, adsorption, and separation, as well as petrochemical and fine-chemical catalytic applications.^{1–7} The uniform micropores with sizes of molecular dimensions (*ca.* 0.25–1 nm) endow zeolites with unrivalled catalytic properties, especially shape selectivity.^{8,9} However, such microporous zeolites cannot process bulky molecules with kinetic diameters larger than 1.0 nm. Only the active sites located on the crystal surface or at the pore mouths are accessible for those bulky molecules. Besides, such confined environments in microporous zeolites also dramatically decrease the transport efficiency of reactants and products.¹⁰

In recent years, extra-large pore zeolites have shown interesting potential as efficient catalysts in the field of fine chemicals and petrochemicals, but suffer from high product cost and low (hydro)thermostability.^{11,12} Nano-sized zeolites

are expected to greatly lower the transport limitations, but are obstructed by the separation processes from the zeolite synthesis liquid or the catalytic reaction system.^{13,14} Creating hierarchical structures in the microporous zeolites has proven to be an efficient method for increasing the mass transport efficiency, but leads to the intrinsic limited ability to process bulky molecules as well as complicated and time/energy-consuming procedures.^{15–17} Seeking alternative materials that better combine the intrinsic shape selectivity of zeolites and the accessibility towards the active site is of great significance in zeolite catalysis.

With the deepening of research on the crystallization mechanism in recent years, in both clear synthesis gels and dense synthesis gels, it is generally accepted that the crystallization of zeolites proceeds *via* the following steps: (1) induction period, (2) nucleation, and (3) crystal growth.^{18–20} The mixed synthesis reactants, referred to as the primary amorphous phase, can transform into the secondary amorphous phase by equilibrating with the solution phase.¹⁸ The secondary amorphous phase is a pseudo-steady-state intermediate, exhibiting some short-range order of the zeolite framework structures, and can be converted to crystalline zeolites with long-range order zeolite frameworks. Tsuruta *et al.* presented that the short-range order of Si and Al atoms in the amorphous aluminosilicate is similar to that in crystalline zeolite crystals in the zeolite A system by using X-ray and electron diffraction.⁵⁶ With extended X-ray absorption-fine structure (EXAFS) and X-ray absorption near edge structure (XANES) spectroscopies, Walton *et al.* found that the structure of the amorphous gallium silicates is similar to the structure of the finally crystallized gallium hydrox-osodalite zeolite.⁵⁷ Although the secondary amorphous phases

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demonstrate some spectroscopic and size-exclusive characteristics of zeolites, the lack of long-range periodicity of a crystalline zeolite lattice makes it amorphous and unsuitable for X-ray diffraction (XRD).^{21–24} Therefore, these zeolite precursors are also regarded as X-ray amorphous zeolites or embryonic zeolites.

Corma *et al.* constructed amorphous zeolite precursors of ITQ-7, ITQ-21, ITQ-30, ZSM-12, Beta, and NU-87, which exhibited pore dimensions and topologies very close to their corresponding crystalline zeolites, through the self-assembling of organic templates and silica.²¹ Inagaki *et al.* regulated the crystal growth kinetics of zeolite Y (FAU) and found that the X-ray amorphous zeolite phase, taken at the end of the induction period, showed the highest catalytic activity toward the Knoevenagel condensation of benzaldehyde with ethyl cyanoacetate.²⁵ Recently, Haw *et al.* prepared X-ray amorphous ZSM-5 precursors with tetrapropylammonium hydroxide (TPAOH) as the structure directing agent, which presented superior catalytic performances in the dealkylation of 1,3,5-triisopropylbenzene, which cannot penetrate through the micropores of zeolites.²³ The above demonstrated high catalytic activities of the amorphous titanosilicate zeolites were ascribed to the more open structure of X-ray amorphous zeolites, which dramatically increased the accessibility towards the catalytic active sites and enhanced the mass transport efficiency.

Heteroatom-containing zeolites (*e.g.* Ti, Sn, B, *etc.*) with isolated active sites in the zeolite framework exhibit unique catalytic performances in numerous important processes.^{26–31} Titanosilicate zeolites, as a typical family of heteroatom-containing zeolites, have been widely used in oxidation reactions with H₂O₂ as the oxidant under mild conditions, such as alkene epoxidation, phenol hydroxylation, cyclohexanone ammoxidation, and deep oxidative desulfurization.^{32–35} The catalytic activity of titanosilicate zeolites strongly correlates with the lattice Ti contents and the Ti coordination states.^{36,37} The length difference between the Ti–O bond (1.80 Å) and Si–O bond (1.61 Å) distorts the local structure around Ti in the titanosilicate zeolites, requiring high framework flexibility for the isomorphous substitution of Ti ions for Si.^{36,38,39}

In addition, Guo *et al.* thoroughly investigated the active titanium species in TS-1 zeolite, and identified a new titanium species with a characteristic Raman band at 695 cm^{−1} when excited at the 266 nm laser line, confirmed by DFT calculations.⁴⁰ The newly discovered octahedrally coordinated titanium species showed superior catalytic performance in the epoxidation reactions in comparison to the tetrahedrally coordinated one. Very recently, Xu *et al.* constructed a mononuclear TiO₆ species in TS-1 zeolite *via* seed-assisted microwave irradiation.⁴¹ The octahedrally coordinated titanium species was identified with UV-Raman (excited at the 266 nm laser line) and X-ray absorption spectroscopy. The obtained TS-1 zeolite catalyst with mononuclear TiO₆ species displayed outstanding catalytic performance and stability in the epoxidation of 1-hexene. Increasing the accessibility towards the Ti sites and the mass transport efficiency, improving the Ti contents, and constructing Ti catalytic species with higher activity have been widely

considered to be key for improving the catalytic efficiency of titanosilicate catalysts.

In this work, with the understanding of zeolite formation processes, we prepared a series of amorphous titanosilicate zeolites (ATZ) with a short-range order structure as well as tunable Si/Ti ratio and pore sizes by using quaternary ammonium ions as the organic structure directing agents (OSDAs). The OSDA used in the zeolite synthesis system not only provides shape commensurate with the cages and channels in zeolites but also is in charge of the nucleus formation and the crystal growth process; the lower the charge density of the OSDA, the higher the requirement for nucleation.^{42,43} A series of commercialized and low charge density home-made quaternary ammonium cations have been employed to obtain amorphous titanosilicate zeolites, which are characterized by specific porosities, open structures, and abundant octahedrally coordinated Ti species. The obtained amorphous titanosilicate zeolite catalysts show enhanced catalytic performance in the oxidative desulfurization of dibenzothiophene (DBT) and the epoxidation of cyclohexene, with respect to the final zeolite structures.

Results and discussion

A series of amorphous titanosilicate zeolites (ATZ) with short-range order were synthesized with a molar composition of 1.0 SiO₂: 0.025–0.2 TiO₂: 0.25–0.50 OSDA: 10–30 H₂O under hydrothermal conditions (170 °C for 6 h) by using TEA⁺, TMAda⁺, PhHE²⁺, DPhHE²⁺, and PhDC²⁺ as the structure directing agents (Scheme 1), and the obtained amorphous titanosilicates were named ATZ-TEA, ATZ-TMAda, ATZ-PhHE, ATZ-DPhHE, and ATZ-PhDC, respectively. The detailed synthesis conditions of ATZ samples are presented in Table 1. Notably, the Si/Ti ratio of the successfully prepared ATZ samples can be as low as 5, demonstrating the high plasticity of the ATZ samples.

All the harvested titanosilicate samples are X-ray amorphous (Fig. 1a). Infrared spectroscopy (IR) was used to characterize the short-range orders of the ATZ samples (Fig. 1b). The absorption bands in the IR spectra at around 1080 and 800 cm^{−1} correspond to the asymmetric and symmetric Si–O stretching motions; the band at 460 cm^{−1} is ascribed to a bending Si–O–Si mode.⁴⁴ A small absorption band, that can be observed at 550



Scheme 1 Organic cations utilized as structure directing agents (OSDA).



Table 1 Syntheses and textural porosities of the ATZ samples

Sample	x^a	y^a	Si/Ti ^c	S_{BET}^d (m ² g ⁻¹)	S_{micro}^d (m ² g ⁻¹)	S_{ext}^d (m ² g ⁻¹)	V_{total}^e (cm ³ g ⁻¹)	V_{micro}^d (cm ³ g ⁻¹)	V_{meso}^f (cm ³ g ⁻¹)	$I_{960/800}^g$
ATZ-TEA	0.50	10	40.8	605	352	253	1.89	0.14	1.75	2.17
ATZ-TEA-5 ^b	0.50	10	4.9	623	283	340	2.05	0.12	1.93	2.97
ATZ-TMAda	0.50	10	40.7	747	319	428	1.93	0.13	1.80	1.93
ATZ-PhHE	0.25	30	41.3	537	318	219	1.40	0.14	1.26	2.31
ATZ-DPhHE	0.25	30	41.2	730	628	102	0.41	0.25	0.16	2.13
ATZ-PhDC	0.25	30	40.5	498	299	199	1.76	0.13	1.63	1.89

^a Initial gel: SiO₂: 0.025TiO₂: xOSDA: yH₂O. ^b Prepared with TiO₂/SiO₂ = 0.2. ^c Measured by inductively coupled plasma (ICP). ^d Specific surface area calculated from the nitrogen adsorption isotherm using the BET method. S_{micro} (micropore area), S_{ext} (external surface area), and V_{micro} (micropore volume) calculated using the *t*-plot method. ^e Total pore volume at $P/P_0 = 0.995$. ^f $V_{\text{meso}} = V_{\text{total}} - V_{\text{micro}}$. ^g FT-IR relative intensity of the bands at 960 and 800 cm⁻¹.



Fig. 1 (a) XRD patterns, (b) FT-IR spectra, (c) N₂ adsorption and desorption isotherms, and (d) pore size distributions of the ATZ samples.

cm⁻¹, is assigned to the bending vibrations of external Si–O, and also is generally attributed to the stretching vibration of double rings in the MFI structure.⁴⁵ The absorption band at 960 cm⁻¹ is attributed to the vibration of the Si–O–Ti or Si–O bond perturbed by Ti atoms in the framework.^{46,47} The intensity ratio between the absorption bands at 960 cm⁻¹ and 800 cm⁻¹ ($I_{960/880}$) is usually used to evaluate the relative content of Ti in the framework.⁴⁸ Generally, a larger $I_{960/880}$ value means a higher framework titanium content. As summarized in Tables 1 and S1,[†] ATZ samples exhibited larger $I_{960/880}$ values than the conventional TS-1 zeolite sample (1.16), which was added as a benchmark, indicating outstanding ability to incorporate framework titanium species.

The nitrogen adsorption–desorption isotherms of the ATZ samples show combined type I–IV isotherms (Fig. 1c). The significant uptakes at low relative pressure demonstrate the existence of abundant microporous structures; and the

hysteresis loops at a relative pressure of $0.8 < P/P_0 < 0.99$ are ascribed to the aggregation of small particles and the existence of mesopores. ATZ samples exhibit similar micropore volumes and higher total pore volumes in comparison to the crystallized TS-1 zeolite sample (Table S1 and Fig. S1[†]). Taking into account the comparison of the detailed data of the samples obtained from PhHE, and DPhHE that have been summarized in Table 1, it can be found that the Brunauer–Emmett–Teller (BET) area and micropore volume are positively correlated with the size of the utilized organic template (S_{BET} : 537, and 730 m² g⁻¹, respectively; V_{micro} : 0.14, and 0.25 cm³ g⁻¹, respectively). It is worth noting that TEA⁺ usually directs the zeolite structure through a clustered mode, presenting a clustered/aggregated conformation, thus resulting in a sample with comparable surface areas and micropore volumes to PhHE²⁺ which exhibits a bulkier molecule size (605 vs. 537 m² g⁻¹, and 0.14 vs. 0.14 cm³ g⁻¹, respectively).⁴⁹ The micropore surface area of ATZ-TEA-5 is smaller than that of the ATZ-TEA (283 vs. 352 m² g⁻¹), indicating that the structural order decreases with increasing Ti content. The pore diameter of ATZ samples, determined according to nonlocal density functional theory, ranges from 0.5–2 nm, showing a strong correlation with the size of the OSDAs and verifying the existence of microporous structures (Fig. 1d). It is widely accepted that the quaternary ammonium cations could order the surrounding (alumino)silicate species by progressively displacing water molecules in the hydration sphere, thus forming the inorganic–organic composite species. Therefore, the utilized organic templates are closely related to the textural properties of the prepared ATZ samples.

The transmission Electron Microscopy (TEM) images of the obtained ATZ samples illustrate that all the samples exhibit a branched worm-like morphology, with sizes ranging from 10 to 20 nm (Fig. 2). The worm-like morphology is the typical morphological feature of the amorphous zeolite material. It is notable that the ATZ-DPhHE sample, prepared by using DPhHE²⁺ as the OSDA, exhibits a larger particle size (50–100 nm) than the others. The two phenyl groups in the DPhHE²⁺ provide stronger hydrophobicity to the template, which dramatically facilitates the overlap of the hydration sphere of the OSDA and the raw Si and Ti species, enhancing the polymerization and evolution processes. Notably, all these ATZ samples exhibit plentiful intra- and inter-particle mesopores,



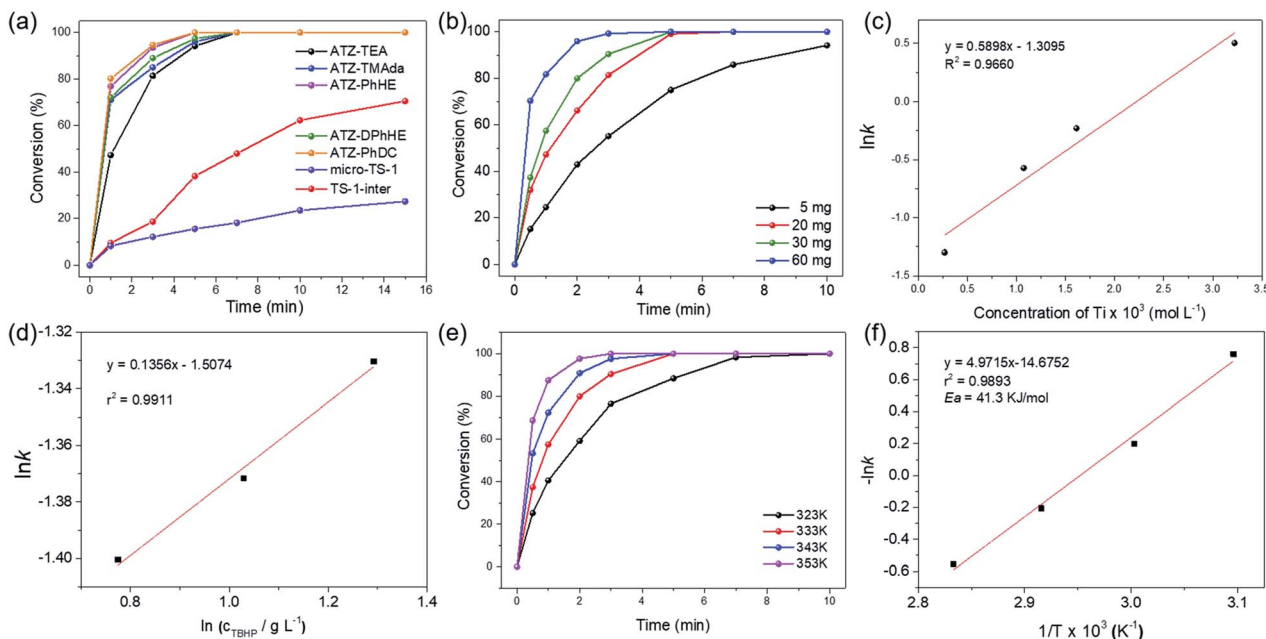


Fig. 5 (a) Time-course variation of DBT conversion over 20 mg of the series of ATZ catalysts at 333 K; (b) time-course variation of DBT conversion with various Ti concentrations and (c) pseudo first-order rate constant for different concentrations of the ATZ-TEA catalyst at 333 K; (d) pseudo zero-order rate constant for different concentrations of TBHP; (e) time-course variation of DBT conversion at different reaction temperatures and (f) Arrhenius plot for the conversion of DBT over the 30 mg ATZ-TEA catalyst. Reaction conditions: 10 mL of 500 ppm model fuels, $n(\text{sulphide})/n(\text{TBHP}) = 0.5$.

pseudo first-order kinetics (Fig. 5f and S10[†]). The apparent activation energy (E_a) of the ATZ-TEA catalyst is 41.3 kJ mol⁻¹, which is calculated from the Arrhenius plot, and indicates that the reaction is kinetically controlled (Fig. 5f).

We have measured external and internal diffusion and have found that the reaction is not controlled by diffusion. The potential external diffusion control was investigated by performing the oxidative desulfurization of DBT at different stirring speeds (400 rpm, 600 rpm, and 800 rpm). When the stirring speed was over 400 rpm, there was no significant enhancement in the rate of the reactions (Fig. S11[†]). We measured the rate of the reaction for two reactants with different molecular sizes: thiophene (Th) and dibenzothiophene (DBT). Th could penetrate, at least some, within TS-1, while DBT cannot penetrate within the pores of MFI. Then we measured the initial rate for the oxidative desulfurization of the two molecules with the microporous TS-1 and the amorphous titanosilicate zeolite precursor (ATZ-TEA) that contains extra-large pores. The results show that with the larger DBT molecule, the ratio of the initial reaction rate, with respect to thiophene, is much larger with the amorphous titanosilicate zeolite precursor with extra-large pores than with TS-1 (21.7 vs. 8.9 at the reaction time of 1 min). This indicates the benefit of the zeolite precursor with extra-large pores, also from the point of view of reactant and product diffusion.

Furthermore, to get a deeper insight into the nature of the active Ti sites, we treated the ATZ-TEA catalyst with acid leaching, which removed most of the octahedrally coordinated Ti species, as evinced by the UV-vis spectrum and the UV-Raman spectrum excited at a wavelength of 266 nm (Fig. S13[†]). ICP

suggested that the acid treatment removed ~30% titanium species (Si/Ti increased from 40.8 to 58.0). The catalytic activity of the acid treated ATZ-TEA catalyst was also evaluated with the oxidation of DBT. Fig. S14[†] shows that the acid treatment dramatically deactivated the catalyst, implying that the octahedrally coordinated Ti species was responsible for the catalytic activity.

The durability tests for the oxidation of DBT over the ATZ-TEA catalyst were also conducted. The used catalyst was regenerated by calcination in air. As presented in Fig. S15[†], 91% of the initial catalytic activity remained after 10 runs. UV-vis spectroscopy, N₂ adsorption-desorption isotherms, and TEM imply that the microenvironment of Ti and microporosity of the open structure are well maintained, showing high catalytic stability (Fig. S16, S17 and Table S1[†]).

Moreover, the catalytic activity of ATZ-TEA was also evaluated by the epoxidation of cyclohexene with TBHP as the oxidant and with nano-sized TS-1 and Ti-Beta (Si/Ti = 25) as the reference catalysts, which were proved to mainly exhibit tetrahedrally coordinated Ti by UV-vis spectroscopy (Fig. S5 and S18–S20[†]). The conversion of cyclohexene over the ATZ-TEA catalyst is 42% of the maximum theoretical value, which is much higher than that over the TS-1 zeolite catalyst (around 16% of the maximum theoretical value) and Ti-Beta zeolite catalyst (around 28% of the maximum theoretical value) (Fig. 6 and Tables S5–S7[†]). The efficiency of TBHP is higher than that for the Ti-Beta catalyst (95 vs. 92%). The epoxide selectivity over ATZ-TEA is also higher than that of the Ti-Beta catalyst (69 vs. 44%). The superior catalytic performance of the ATZ catalyst can be ascribed to the open structure and the active octahedrally coordinated Ti



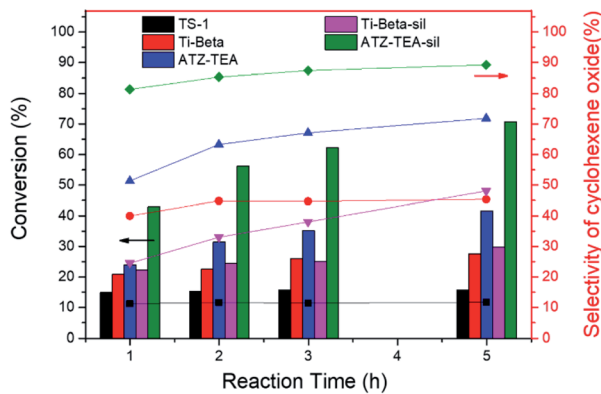


Fig. 6 Epoxidation of cyclohexene over TS-1, Ti-Beta, Ti-Beta-Sil, ATZ-TEA, and ATZ-TEA-Sil catalysts. Reaction conditions: cat., 30 mg; cyclohexene, 56 mmol; TBHP (80 wt%), 14 mmol; temp., 333 K, and 3 bar of N_2 .

species. Due to the wettability of titanosilicate catalysts influencing the activity and selectivity largely, we silylated Ti-Beta and ATZ-TEA catalysts with dimethoxydimethylsilane to increase the hydrophobicity. Fig. S20 and S21[†] indicated that the silylation transformed most of the octahedrally coordinated Ti species into a tetrahedrally coordinated form. As summarized in Fig. 6 and Table S8,[†] the silylated ATZ-TEA sample (named ATZ-TEA-Sil) showed dramatically enhanced catalytic activity and epoxide selectivity in comparison to the non-silylated ATZ-TEA (71% and 86% vs. 42% and 69%, respectively). But the silylated Ti-Beta (Ti-Beta-Sil) exhibited slightly improved catalytic performance in comparison to the fresh one (with the conversion of cyclohexene: 30% vs. 28%) (Fig. 6 and Table S9[†]). The briefly increased activity over the Ti-Beta-Sil catalyst can be ascribed to the hindrance effect aroused by the silylated methyl groups, which is almost negligible in the case of the ATZ-TEA sample due to the large external surface area.

Conclusions

In summary, a series of prezeolitic long-range amorphous titanosilicates but with an open structure of zeolite units and high amounts of catalytically active titanium species were prepared by using quaternary ammonium cations as the organic structure directing agents under hydrothermal conditions. Comprehensive characterization indicated that the amorphous titanosilicates exhibited some open structure of the zeolite units with pore dimensions ranging from 0.5 to 2 nm. Besides, the textural properties of ATZ samples strongly correlated with the utilized organic template. UV-vis, UV-Raman, and X-ray absorption spectra evidenced the presence of octahedrally coordinated isolated titanium species, which remained stable upon calcination. The outstanding catalytic performance over ATZ catalysts in the oxidative desulfurization of dibenzothiophene and the epoxidation of cyclohexene could be attributed to the highly active octahedrally coordinated isolated titanium sites and the abundant open structure of zeolite units, which

dramatically enhanced the transport efficiency and active site accessibility. This work opens a new avenue for expanding the catalytic applications of current microporous titanosilicate zeolites for processing bulky molecules.

Experimental methods

Preparation of titanosilicate zeolite precursors

Titanosilicate zeolite precursors were prepared with the following molar composition: 1.0 SiO_2 : 0.025–0.200 TiO_2 : 0.25–0.50 OSDA: 10–30 H_2O under hydrothermal conditions (170 °C for 6 h), in which OSDA can be tetraethylammonium (TEA^+), trimethyladamantylammonium ($TMAA^+$), N,N,N,N',N',N' -hexaethyl-1,4-benzenedimethanaminium, ($PhHE^{2+}$), N,N,N,N',N',N' -hexaethyl-[1,1'-biphenyl]-4,4'-dimethanaminium ($DPhHE^{2+}$), and N,N' -dicyclohexyl- N,N,N',N' -tetramethyl-1,4-benzenedimethanaminium, ($PhDC^{2+}$). The typical synthesis procedure is as follows: the organic template was mixed with distilled water and stirred for 15 min. Afterward, tetrabutyl titanate (TBOT) and tetraethyl orthosilicate (TEOS) were added into the system and stirred for 6 h to achieve complete hydrolysis. Then the synthesis gel was introduced into a teflon-lined stainless-steel autoclave. Crystallization was carried out at 170 °C under static conditions for 6 h. After centrifugation, washing, and drying, the products were calcined at 550 °C for 6 h under an air atmosphere to remove the organic template.

Preparation of conventional TS-1 zeolites TS-1-inter and micro-TS-1

With tetrapropylammonium hydroxide (TPAOH) as the organic template and TBOT as the titanium source, the conventional TS-1 zeolite samples were synthesized with a molar composition of 1.0 SiO_2 : 0.025 TiO_2 : 0.3 TPAOH: 30 H_2O under hydrothermal conditions at 170 °C for 6–24 h. The samples crystallized for 6 h and 24 h were named TS-1-inter and micro-TS-1, respectively. A typical preparation procedure is similar to that of the ATZ samples.

Preparation of the nano-sized Ti-Beta zeolite

The Ti-Beta zeolite was synthesized in basic medium from a gel of the following molar composition: SiO_2 : 0.067 TiO_2 : 0.56 TEOH: 0.35 H_2O_2 : 7 H_2O : 5 wt% Seed. The gel preparation involved the hydrolysis under stirring of TEOS in an aqueous solution containing TEA^+ and H_2O_2 . Later, tetraethyl orthotitanate (TEOT) was added and the solution was kept under stirring until the ethanol formed in the hydrolysis of TEOS was evaporated. Dealuminated zeolite Beta seeds were also added and the mixture was loaded into teflon-lined stainless-steel autoclaves and heated at 140 °C under rotation (60 rpm) for 20 days. The solid was recovered by centrifugation, washed with distilled water and calcined in static air at 580 °C for 3 h.

Acid treatment

Typically, 1 g ATZ-TEA sample was treated with 50 mL 2 M HNO_3 water solution at 60 °C for 2 h, and then thoroughly washed with distilled water.



Silylation conditions

The silylation process was performed using a standard procedure under a N₂ flow. Calcined ATZ-TEA or Ti-Beta zeolite (1 g) previously dehydrated at 300 °C under vacuum was brought into contact with a solution of the silylating agent (dimethoxydimethylsilane, 2.8 mmol) in dry toluene (10 mL) at 80 °C under reflux for 1 hour. Then, a solution of triethylamine (2.8 mmol) in toluene (5 mL) was also added and the mixture was refluxed for an additional hour at 80 °C. The zeolite was washed with toluene and dried at 100 °C. The silylated ATZ-TEA and Ti-Beta samples were named ATZ-TEA-Sil and Ti-Beta-Sil, respectively.

Conflicts of interest

There are no conflicts to declare.

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