



Cite this: *Green Chem.*, 2024, **26**, 7579

# A review on sustainable iron oxide nanoparticles: syntheses and applications in organic catalysis and environmental remediation

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Iron oxide nanoparticles have been intensively investigated owing to their huge potential as diagnostic, therapeutic, and drug-carrier agents in biomedicine, sorbents in environmental technologies, sensors of various inorganic and organic/biological substances, energy-generating and storing materials, and in assorted biotechnological and industrial processes involving microbiology, pigment industry, recording and magnetic media or (bio)catalysis. An eminent interest in exploring the realm of iron oxides is driven by their chemical and structural diversity, high abundance, low cost, non-toxicity, and broad portfolio of chemical procedures enabling their syntheses with desirable physicochemical features. The current review article centers its attention on the contemporary advancements in the field of catalysis and environmental technologies employing iron oxides in various chemical forms (e.g., hematite, magnetite, maghemite), sizes (~10–100 nm), morphology characteristics (e.g., globular, needle-like), and nano architecture (e.g., nanoparticles, nanocomposites, core-shell structures). In particular, the catalytic applications of iron oxides and their hybrids are emphasized regarding their efficiency and selectivity in the coupling, oxidation, reduction, alkylation reactions, and Fischer–Tropsch synthesis. The deployment of iron oxides and their nanocomposites in environmental and water treatment technologies is also deliberated with their roles as nanosorbents for heavy metals and organic pollutants, photocatalysts, and heterogeneous catalysts (e.g., hydrogen peroxide decomposition) for oxidative treatment of various contaminants. The associated challenges and potential progress in iron-oxide-based catalytic and environmental technologies are highlighted as well. Young chemists, researchers, and scientists could find this review useful in enhancing the usefulness of nano iron oxides in their investigations and developing sustainable methodologies.

Received 16th April 2024,  
Accepted 10th May 2024  
DOI: 10.1039/d4gc01870b  
rsc.li/greenchem

## 1. Introduction

For several decades, iron oxides have been intensively examined and manufactured for a broad scale of applications. An eminent interest in exploring the realm of iron oxides has been nourished by comprehension of their remarkable physical behaviors and their inherent physicochemical properties, most of which have been found appealing for various appli-

cations. Until now, iron oxides have been successfully applied in many branches of human activities comprising first media to store information, tools for diagnostic,<sup>1–3</sup> therapeutic,<sup>4,5</sup> and drug-delivery purposes in medicine,<sup>6–9</sup> agents enhancing photocatalytic/catalytic performances in diverse chemical processes, materials improving efficiency of energy-generating cells (e.g., cells for the direct solar splitting of water and hydrogen generation),<sup>10</sup> key components in spintronic/electronic devices and energy-storing units (e.g., Li-ion batteries),<sup>11,12</sup> sorbents removing toxic inorganic and organic/biological pollutants from the environment,<sup>13,14</sup> among many others.<sup>15–17</sup> Such a broad portfolio of iron oxide applications is attributed to their high abundance, low cost, and diversity of chemical procedures to synthesize them with desirable physicochemical features. Moreover, once synthesized in the nano-dimension form, they are endowed with unique properties driven by finite-size (*i.e.*, quantum, confinement-related) effects and surface effects. Iron oxides also exhibit favorable biochemical

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properties such as non-toxicity, biodegradability, and biocompatibility<sup>18</sup> placing them among the most appropriate (nano) materials in various biomedical<sup>19,20</sup> and biotechnological areas especially in view of their encounter with living organisms. The examples include contrast agents in NMR imaging, carriers for drugs and biomolecules, tools providing immobilization of proteins and cell separation, and therapeutic agents in magnetically-assisted hyperthermia, among others. Furthermore, in the context of sustainability and environmental consciousness, the utilization of abundant iron as a key element in various applications holds significant value. According to the ACS Green Chemistry Institute's Periodic Table of Endangered Transition Elements, iron stands out as the only 'white space' among the transition metals of consequence, thus aligning with the principles of green chemistry and sustainable practices (Fig. 1a). The unique position of iron in the periodic table not only reinforces its virtues but also underscores its importance in promoting environmentally friendly solutions. Fig. 1b indicates constantly high interest of scientific community in research of "Iron Oxide, nanoparticles" with nearly 3000 publications per year.

Till date, seventeen crystalline iron oxide phases have been found and described in detail. They are commonly categorized into two important classes, *i.e.*, hydrated and non-hydrated iron oxide phases. Hydrated iron oxides of mineral nature contain water in their crystal structure, and comprise goethite ( $\alpha$ -FeOOH), akaganeite ( $\beta$ -FeOOH), lepidocrocite ( $\gamma$ -FeOOH), ferroxhyte ( $\delta$ -FeOOH), ferrihydrite ( $5\text{Fe}_2\text{O}_3 \cdot 9\text{H}_2\text{O}$ ), high-pressure FeOOH, schwertmannite ( $\text{Fe}_8\text{O}_8(\text{OH})_6(\text{SO}_4)_n \cdot n\text{H}_2\text{O}$ ),

and green rust/green-rust-like compounds.<sup>21</sup> Formally, they were frequently used as precursors for the synthesis of non-hydrated iron oxide forms as upon thermal treatment, they readily undergo phase transformations with molecular water leaving their crystal structure. In the realm of non-hydrated iron oxides, three classes have been acknowledged with respect to the degree of oxidation of Fe identified in their crystalline arrangement:<sup>22–24</sup> (i) FeO (wüstite) with only  $\text{Fe}^{2+}$  ions; (ii)  $\text{Fe}_2\text{O}_3$  (ferric oxide) with only  $\text{Fe}^{3+}$  ions, and (iii)  $\text{Fe}_3\text{O}_4$  (magnetite) containing both  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$  ions. While FeO and  $\text{Fe}_3\text{O}_4$  each exhibit only one crystal pattern, iron(III) oxide demonstrates extensive polymorphism, *i.e.*, indicating the presence of multiple crystal phases that possess identical chemical composition, however having distinct physical characteristics revealing their various crystal structures. Other than amorphous phase, five distinct polymorphs of ferric oxide, stable under ambient conditions, have been described so far: (i)  $\alpha$ - $\text{Fe}_2\text{O}_3$  (mineralogically known as hematite); (ii)  $\beta$ - $\text{Fe}_2\text{O}_3$ ; (iii)  $\gamma$ - $\text{Fe}_2\text{O}_3$  (mineralogically known as maghemite); (iv)  $\epsilon$ - $\text{Fe}_2\text{O}_3$ , and (v) recently reported  $\zeta$ - $\text{Fe}_2\text{O}_3$ . The crystal structures of non-hydrated iron oxide phases are shown in Fig. 2.<sup>23</sup> As the present review deals with the systematic description of the most important catalytical and environmental applications of nanocrystalline non-hydrated iron oxides, it is thus timely to briefly summarize their fundamental structural and physico-chemical properties.

$\alpha$ - $\text{Fe}_2\text{O}_3$ ,  $\gamma$ - $\text{Fe}_2\text{O}_3$ , and  $\text{Fe}_3\text{O}_4$  are naturally-occurring non-hydrated iron oxide phases, and a various synthetic pathways have been documented to produce both nanoscale and bulk



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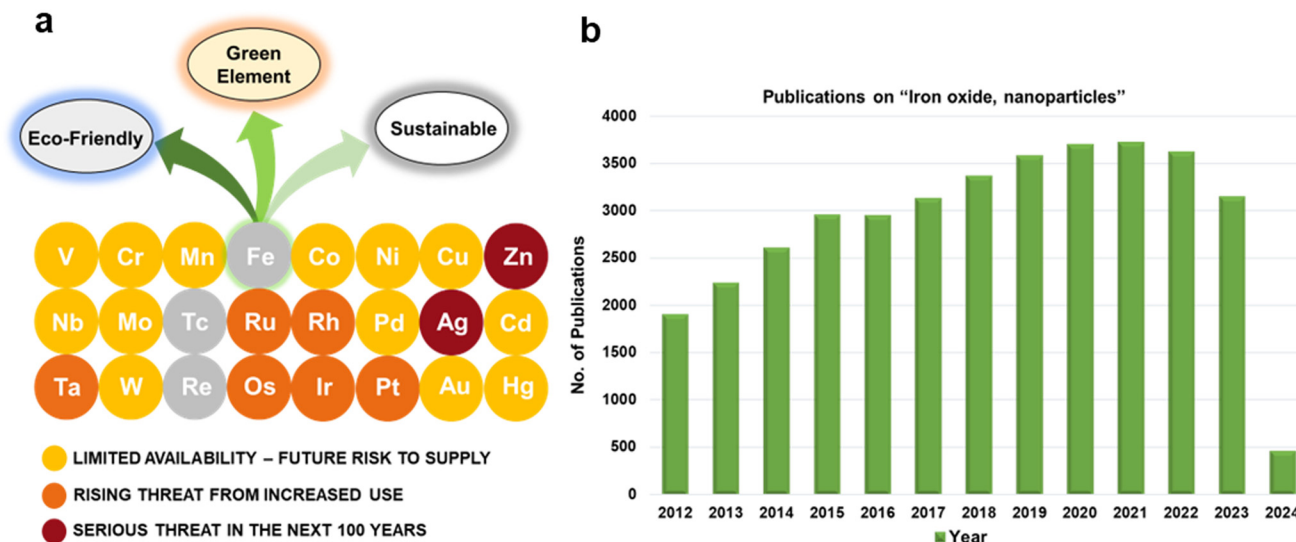
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**Fig. 1** (a) Periodic table of endangered transition elements (source: ACS Green Chemistry Institute, Endangered Elements). (b) The number of publications for the keyword search "iron oxide, nanoparticles" as uncovered in Web of Science (dated: March 27, 2024).

forms with sophisticated control of particle size, particle size distribution (PSD), structure, surface modification, and hence, physicochemical features. Conversely,  $\beta$ - $\text{Fe}_2\text{O}_3$  and  $\epsilon$ - $\text{Fe}_2\text{O}_3$  are viewed as rare non-hydrated  $\text{Fe}_2\text{O}_3$  phases which barely exist

naturally, and are challenging to prepare in the laboratory as single phases without contamination by other  $\text{Fe}_2\text{O}_3$  admixtures. By virtue of being low surface energy and thermodynamical stability, they exist only as nanosized objects (e.g., as



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nanoparticles, nanotubes, thin films). To date, only a few reaction pathways are known for the production of  $\beta$ -Fe<sub>2</sub>O<sub>3</sub> and  $\epsilon$ -Fe<sub>2</sub>O<sub>3</sub> phases and most of them deliver lower yields without proper control on attaining precise particle size and morphology.

Among all iron(III) oxide polymorphs,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> phase possess the highest degree of thermodynamic stability.<sup>22,23</sup> Notably,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> shows a corundum-type crystal structure (similar to ilmenite (FeTiO<sub>3</sub>) and corundum) with hexagonally-closed packed oxygen (O) lattice wherein Fe<sup>3+</sup> ions occupy two-thirds of the octahedral positions (see Fig. 2c). The crystalline arrangement of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> is represented within the  $R\bar{3}c$  space group with lattice parameters  $a = 5.034$  Å and  $c = 13.752$  Å.  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> exhibits two magnetic transitions, ( $\sim 950$  K Néel temperature) and ( $\sim 265$  K, Morin transition temperature MTT). The strong magnetic dipolar anisotropy competes with local ion anisotropy which shows different thermal dependencies to drive the Morin transition. Upon cooling past the MTT, the spins undergo a 90° spin reorientation from the basal plane to the  $c$ -axis. Nonetheless, above MTT, due to effective spin-orbit coupling, the spins deviate slightly from the basal plane as a result slight canting is observed, inducing feeble magnetic moment pointing along the  $c$ -axis. The tilting of the spins arises due to Dzyaloshinsky–Moriya antisymmetric interaction prompted by the crystal fields arising from favorable positioning of O<sup>2-</sup> anions within the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystal lattice. The temperature of Morin transition is influenced by many factors like lattice defects, exchange by foreign cations, divergences from stoichiometry, surface effects, structures, and particle size. In a weakly ferromagnetic state,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> shows very small net magnetization, which limits its exploitation in magnetism-

based applications. However, the n-type semiconductor ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>) exhibit the wide band gap ( $\sim 2.1$  eV) among all the polymorphs of iron(III) oxide reported so far;  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> possesses very low hole mobility. Both empirical and theoretical investigations proven that the photoelectrochemical characteristics of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> can be notably improved through modifying the morphology, particle size, doping, and substrate type during the growth of nanoscale  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> thin films, opening the entry to effectively apply iron(III) oxide polymorphs for the fabrication of electrodes in the photo electrolysis of H<sub>2</sub>O to produce H<sub>2</sub>.<sup>16</sup> Besides,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> has been found as a promising constituent in gas and humidity sensors and electrodes in lithium-ion batteries.<sup>25</sup> In geophysics, hematite-ilmenite solid solutions have been used as a model system for description and explanation of the essence of lamellar magnetism, a phenomenon behind strong remanent magnetization imprinted by a planet's internal magnetic field and stable for hundreds of millions of years.<sup>26</sup>

$\beta$ -Fe<sub>2</sub>O<sub>3</sub>, discovered in 1956, is metastable crystalline polymorph of Fe<sup>3+</sup> oxide<sup>22,23</sup> which adopts a cubic-body-centered (CBC) crystalline morphology of a bixbyite type with  $Ia\bar{3}$  space group (see Fig. 2d). Owing to the distinct crystallographic atmospheres, two distinct cation positions in the  $\beta$ -Fe<sub>2</sub>O<sub>3</sub> crystal structure can be clearly recognized and are assigned as b-sites and d-sites. In the cubic unit cell with  $a = 9.393$  Å, 24 Fe<sup>3+</sup> ions fill the d-sites with the  $C_2$  symmetry and 8 Fe<sup>3+</sup> ions occupy the b-sites with the  $C_{3i}$  symmetry leaving no vacant cation position. Unlike other ferric oxide polymorphs,  $\beta$ -Fe<sub>2</sub>O<sub>3</sub> is paramagnetic at room temperature (RT) while at 110 K, it is magnetically ordered, and below that it becomes antiferromagnetic, most probably of canted nature.<sup>27</sup> Moreover, it



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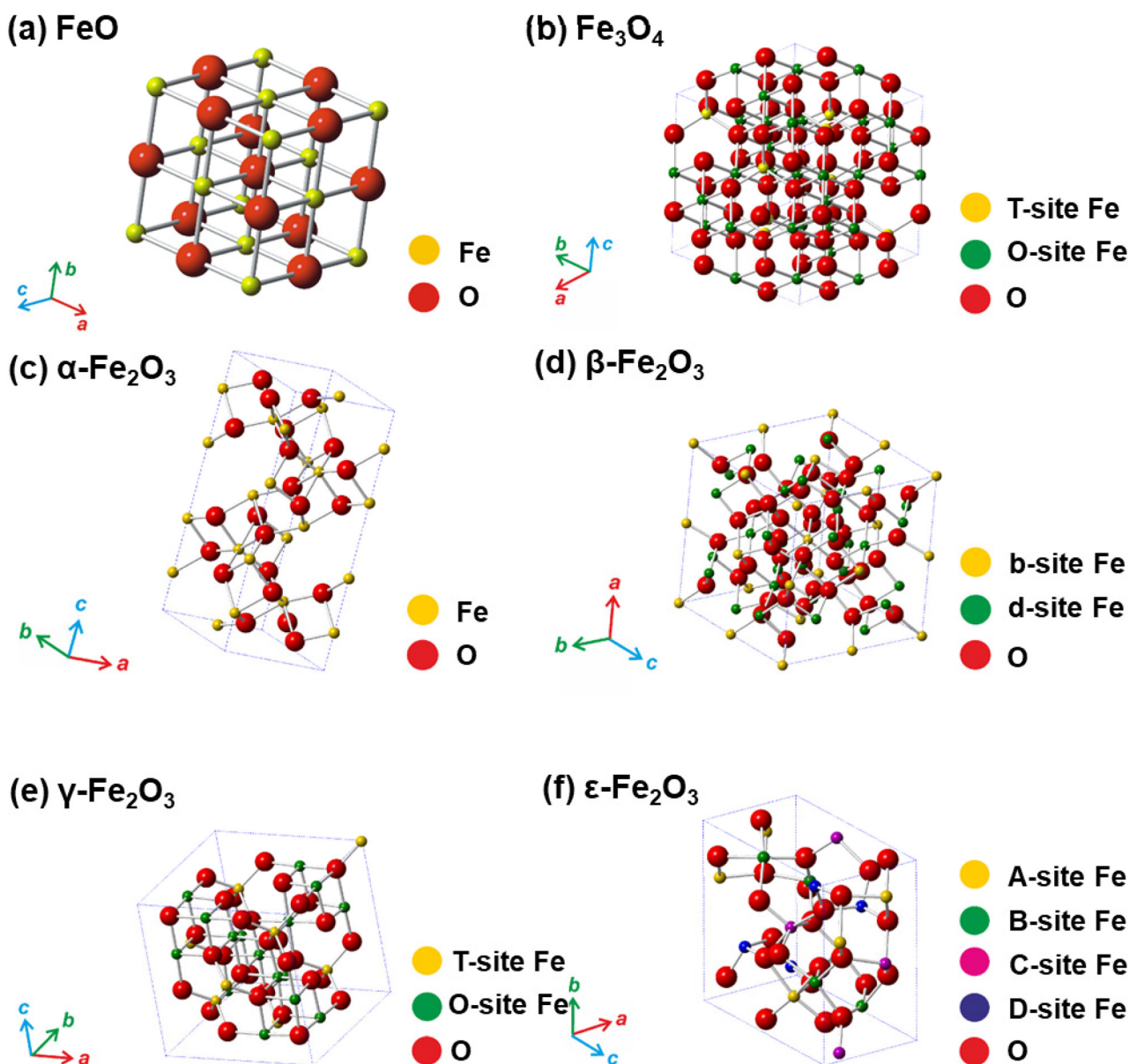
*He is a member of the editorial advisory board of several international journals, published over 985 papers, and awarded 17 U. S. Patents, 11 books, 31 book chapters, and 3 encyclopedia contributions with 77 600 citations.*



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**Fig. 2** Crystal structures of non-hydrated iron oxides. In panel (a), Fe represents octahedral position in the framework of  $\text{FeO}$ . In panel (b), T-site Fe (tetrahedral) and O-site Fe (octahedral) in the  $\text{Fe}_3\text{O}_4$  crystal structure. In panel (c), Fe represents octahedral position in the framework of  $\alpha\text{-Fe}_2\text{O}_3$ . In panel (d), b-site Fe and d-site Fe represents octahedral b-sites and d-sites, respectively, with different polyhedra distortion in the crystalline arrangement of  $\beta\text{-Fe}_2\text{O}_3$ . In panel (e), T-site Fe and O-site Fe represents tetrahedral and octahedral position, respectively, in the  $\gamma\text{-Fe}_2\text{O}_3$  crystalline arrangement. In panel (f), A-site Fe, B-site Fe, and C-site Fe stand for the octahedral sites with different polyhedra distortion and D-site Fe stands for the tetrahedral position in the crystalline framework of  $\epsilon\text{-Fe}_2\text{O}_3$ . In all the panels, O stands for oxygen positions in the respective crystal structures. Panels (c), (d), (e), and (f) Reproduced with permission from ref. 23 Copyright 2011, American Chemical Society.

undergoes a polymorphic transformation to  $\alpha\text{-Fe}_2\text{O}_3$  at  $\sim 500^\circ\text{C}$ ; however, if  $\beta\text{-Fe}_2\text{O}_3$  nanoparticles are endowed with a hollow morphology,  $\beta\text{-Fe}_2\text{O}_3$ -to- $\gamma\text{-Fe}_2\text{O}_3$  transformation has been observed. Despite being a non-attractive magnetic material, the  $\beta\text{-Fe}_2\text{O}_3$  phase offers itself a prospective contender within the realm of optoelectronics,<sup>28</sup> serving as a viable option for chloroform sensing<sup>29</sup> and enhancement of lithium-ion battery performance when employed as an anode.<sup>30</sup> In

view of the band gap width of  $\sim 1.9$  eV,  $\beta\text{-Fe}_2\text{O}_3$  phase, prepared as a thin film has been successfully deployed for the photo-assisted  $\text{H}_2$  production as an alternative iron oxide photocatalysts.<sup>31</sup>

$\gamma\text{-Fe}_2\text{O}_3$ , initially identified in 1925, has an inverse spinel-type cubic crystal arrangement with a lattice parameter of  $a = 8.351 \text{ \AA}$  and is formed by the topo tactic oxidation of  $\text{Fe}_3\text{O}_4$ .<sup>22,23</sup> Two crystallographically distinctive cation sites



(octahedral and tetrahedral) are established in its crystal structure (see Fig. 2e). To develop a neutral charge within the  $\gamma\text{-Fe}_2\text{O}_3$  crystalline arrangement, certain octahedral sites are left unoccupied. Thus,  $\gamma\text{-Fe}_2\text{O}_3$  is described with a stoichiometric formula specified as  $[(\text{Fe}^{3+})^T(\text{Fe}_{5/3}^{3+}\text{O}_{1/3})^{\text{O}}\text{O}_4]_{3/4}$ , where o denotes vacancies. The vacancies within the octahedral sites can be divided randomly in accordance with cubic  $Fd3m$ , cubic  $P4_132$  or fully ordered tetragonal  $P4_32_12$  space groups. This modulation affects the  $\gamma\text{-Fe}_2\text{O}_3$  crystal symmetry, transitioning from higher (cubic) to lower (tetragonal) symmetrical configurations. In addition, the ordering of vacancies over the octahedral sites is believed to minimize the electrostatic energy of the crystal, occurring dominantly under conditions of elevated temperatures and pressures and at reduced dimensions. Similarly, as in the case of  $\alpha\text{-Fe}_2\text{O}_3$  and  $\beta\text{-Fe}_2\text{O}_3$ ,  $\gamma\text{-Fe}_2\text{O}_3$  is a semiconductor with a bandgap of  $\sim 2$  eV. From the perspective of magnetism,  $\gamma\text{-Fe}_2\text{O}_3$  is a strong ferrimagnet with two magnetic sublattices (*i.e.*, tetrahedral and octahedral) and where a range of 780 to 980 K is estimated for the Curie temperature. The precise determination of Curie temperature is impossible due to the  $\gamma\text{-Fe}_2\text{O}_3$  to  $\alpha\text{-Fe}_2\text{O}_3$  polymorphic conversion upon heating. The net magnetic moment of stoichiometric  $\gamma\text{-Fe}_2\text{O}_3$  per formula unit is offered by the unequal occupancies of  $\text{Fe}^{3+}$  ions in the tetrahedral and octahedral magnetic sub lattices, oriented in the direction of the octahedral  $\text{Fe}^{3+}$  magnetic moments and amounting to  $2.5\mu_B$ . When the size of  $\gamma\text{-Fe}_2\text{O}_3$  NPs falls down to a specific value ( $\sim 30$  nm), it exhibits superparamagnetic through a robust magnetic reactivity under minor external magnetic fields and intense relaxation phenomenon. Moreover, in the nanoworld,  $\varepsilon\text{-Fe}_2\text{O}_3$  is frequently identified as midway phase upon thermal processing on the  $\gamma\text{-Fe}_2\text{O}_3$ -to- $\alpha\text{-Fe}_2\text{O}_3$  route.<sup>22,23</sup>  $\gamma\text{-Fe}_2\text{O}_3$  is considered as the first model and commonly explored nanomaterials deployed to construct the groundwork for superparamagnetic relaxation theory and other characteristics magnetic phenomena prevalent in the nanoscale domain such as emergence of collective magnetic excitations in the blocked state, theory of spin tilting and spin defeat, *etc.*<sup>22,23</sup> Apart from theoretical studies, nanosized  $\gamma\text{-Fe}_2\text{O}_3$  is the most significant form of ferric oxide, which has previously been used in assorted magnetism-based technologies (*e.g.*, information storage pigments, magnetic fluids, gas sensors, magneto-optical devices, magneto-caloric refrigeration, *etc.*) and medical appliances (*e.g.*, NMR imaging agent, medical diagnosis, cell labeling, and separation, targeted drug delivery, *etc.*).<sup>6–8,15</sup>

Similar to  $\beta\text{-Fe}_2\text{O}_3$ ,  $\varepsilon\text{-Fe}_2\text{O}_3$  is rare, metastable crystalline form of iron(III) oxide; initially observed in 1934 and primarily described in 1963.<sup>22,23,32</sup> It occurs only in the nanoworld with a scarce natural abundance. The synthesis of  $\varepsilon\text{-Fe}_2\text{O}_3$  as an individual nanosized object is challenging in view of the essential requirement of the maintenance of spatial restriction of NPs growth. Thus, synthetic protocols towards  $\varepsilon\text{-Fe}_2\text{O}_3$  must involve some extent of agglomeration in either the precursor and/or the silica matrix used as support.  $\varepsilon\text{-Fe}_2\text{O}_3$  crystallizes embracing an orthorhombic unit cell which falls within the  $Pna2_1$  space group. Three octahedral and one tetrahedral sites

are authorized in the  $\varepsilon\text{-Fe}_2\text{O}_3$  crystalline arrangement differing significantly in the degree of polyhedral distortion (see Fig. 2f).  $\varepsilon\text{-Fe}_2\text{O}_3$  is a 4-sublattice Néel P-type ferrimagnet. Generally,  $\varepsilon\text{-Fe}_2\text{O}_3$  shows complex magnetic features which drastically changes at two distinct temperatures, *i.e.*, at  $\sim 490$  K (Curie temperature) and  $\sim 110$  K. At RT,  $\varepsilon\text{-Fe}_2\text{O}_3$  display the characteristics of a collinear ferrimagnet<sup>33</sup> with an enormous coercivity of  $\sim 2$  T and a net magnetic moment of  $1.3\mu_B$ .<sup>34</sup> At  $\sim 110$  K, another magnetic transition is noticed with drastic drop in the coercive field of  $\varepsilon\text{-Fe}_2\text{O}_3$  and a notable decrease in the orbital component of the magnetic moment associated with  $\text{Fe}^{3+}$ .<sup>32</sup> Nonetheless, the magnetic state of  $\varepsilon\text{-Fe}_2\text{O}_3$  at lower temperature remains unresolved and lacks a satisfactory explanation in current research. In addition, the magnetic transition at  $\sim 110$  K is attended by lattice distortions and a numerous morphological transformations.<sup>32</sup> Upon thermal treatment,  $\varepsilon\text{-Fe}_2\text{O}_3$  transforms to  $\alpha\text{-Fe}_2\text{O}_3$ ; the temperature of polymorphous transformation intensely depends on the restriction of size growth during structural change and varies from  $\sim 600$  to  $1300$  K.<sup>32</sup>  $\varepsilon\text{-Fe}_2\text{O}_3$  is considered as an extraordinary nanomaterial that exhibit a high coercive field at RT,<sup>34</sup> millimeter-wave ferromagnetic resonance,<sup>35</sup> and coupled magnetoelectric characteristics.<sup>36</sup> It is important to note that these unique properties not observed in another iron oxide phase. A combination of these nanomaterial properties renders  $\varepsilon\text{-Fe}_2\text{O}_3$  as an ideal matter for deployment in various applications that requires materials with high coercivity<sup>34</sup> and/or necessitates the coupling of electrical and magnetic material features (*e.g.*, memory elements with multiple state)<sup>36</sup> and/or involving electromagnetic waves absorption.<sup>35</sup>

$\zeta\text{-Fe}_2\text{O}_3$ , the youngest iron(III) oxide polymorph unearthed in 2015 as a product of pressure transformation of  $\beta\text{-Fe}_2\text{O}_3$ ,<sup>24</sup> is the first example of a monoclinic phase in the iron(III) oxide family. Its crystal structure falls into the  $I2/a$  space group with  $a = 9.683$  Å,  $b = 10.00$  Å, and  $c = 8.949$  Å;  $\text{Fe}^{3+}$  ions occupy six non-equivalent octahedral sites. At RT,  $\zeta\text{-Fe}_2\text{O}_3$  is paramagnetic with a transition to the antiferromagnetic state at the Néel temperature of  $\sim 69$  K. It has been suggested that  $\zeta\text{-Fe}_2\text{O}_3$  could have other interesting features such as electronic, optical, and transport that would enable its usage for empirical applications. However, more studies are needed to address its electronic structure and, therefore, physical properties.

FeO is often observed as an intermediate phase in the phase transformations of iron oxides and is frequently deficient with iron (*i.e.*,  $\text{Fe}_x\text{O}$  with  $x$  ranging from 0.83 to 0.96); if stoichiometric, it shows a cubic crystal morphology within the  $Fm3m$  space group and  $a = 4.296$  Å (see Fig. 2a). For non-stoichiometric  $\text{Fe}_x\text{O}$ , defects in its crystal structure cause an ordered distribution of vacancies in the cation sites.  $\text{Fe}_x\text{O}$  can be readily oxidized to  $\text{Fe}_3\text{O}_4$  and ultimately into  $\gamma\text{-Fe}_2\text{O}_3$ . FeO is an antiferromagnet with the Néel temperature of around 200 K; below the Néel temperature, the magnetocrystalline distortion establishes a rhombohedral crystal structure. FeO has been described in mineralogical and petrological studies as it a part of the solid solution with periclase (MgO) and its oxidation may form goethite-limonite systems.



$\text{Fe}_3\text{O}_4$ , the oldest magnetic material ever studied, has an identical crystal structure to  $\gamma\text{-Fe}_2\text{O}_3$ , *i.e.*, the cubic crystal structure of inverse spinel type with the two distinct cation sites, the T and O positions ( $a = 8.397 \text{ \AA}$ ,  $Fd3m$  space group) (see Fig. 2b). Contrary to  $\gamma\text{-Fe}_2\text{O}_3$ , the O sites are occupied by  $\text{Fe}^{2+}$  ions and  $\text{Fe}^{3+}$  ions in equal ratio. Thus,  $\text{Fe}_3\text{O}_4$  is described as  $(\text{Fe}^{3+})^{\text{T}}(\text{Fe}^{2+}\text{Fe}^{3+})^{\text{O}}\text{O}_4$ .  $\text{Fe}_3\text{O}_4$  behaves as a ferrimagnetic material with a net magnetic moment of  $4\mu_{\text{B}}$  per unit formula and a Curie temperature of about 980 K; moreover, above 120 K (the Verwey transition temperature),  $\text{Fe}_3\text{O}_4$  is a conductor. At RT,  $\text{Fe}_3\text{O}_4$  is believed to show a half-metallic behavior, a feature required for spintronics materials. At very high temperatures ( $>1300 \text{ K}$ ),  $\text{Fe}_3\text{O}_4$  transforms to  $\alpha\text{-Fe}_2\text{O}_3$  with an occasional occurrence of  $\gamma\text{-Fe}_2\text{O}_3$  as an intermediate phase. When synthesized as nanoparticles or core/shell structures, non-stoichiometric phases of  $\text{Fe}_3\text{O}_4$  are often observed, *i.e.*,  $\text{Fe}_{3-\delta}\text{O}_4$  with  $\delta$  in the range from 0 ( $\text{Fe}_3\text{O}_4$ ) to  $1/3$  ( $\gamma\text{-Fe}_2\text{O}_3$ ). There have been several discussions in the literature reporting different threshold value of  $\delta$  determining the transition between non-stoichiometric  $\text{Fe}_3\text{O}_4$  and non-stoichiometric  $\gamma\text{-Fe}_2\text{O}_3$ . Due to its robust magnetic reactivity in the presence of small external magnetic fields and superparamagnetic properties at nanoscale,  $\text{Fe}_3\text{O}_4$  has been found to be effective in many biomedical applications such as contrast agents, carriers of drugs, and heating elements in magnetically-assisted hyperthermia for cancer treatment, and catalytical processes such as magnetically-separable catalysts.<sup>6,7,21,37,38</sup>

It is widely acknowledged that the physical and chemical features and applicability of nanocrystalline iron oxides can be altered by their size and morphology, surface functionalization, particle arrangement and texture, and cation substitution.<sup>6–8,10,13,15–17</sup> In this review, the selected and vitally important applications of iron oxide nanomaterials are deliberated in the domain of catalysis and environmental remediation (see Fig. 3). Importantly, the emphasis has been mainly on challenging aspects in specific applications with the introductory aspects being briefly outlined under each section comprising recent review references.

The review is structured into three main sections with section 2 being focused on applications of iron oxides in the

field of catalysis with an emphasis on their roles in diverse reactions such as reduction-, oxidation-, coupling-, and alkylation reactions, Fischer–Tropsch synthesis, and multicomponent reactions (Fig. 3). Section 3 deliberates the use of iron oxides in the most recent environmental applications; accentuating the role of iron oxides as nanosorbents for toxic heavy metals and organic contaminants, their significance in photocatalysis processes deployed for environmental treatment while promoting  $\text{H}_2\text{O}_2$  decomposition, and their immobilization capability (Fig. 3). The concluding section summarizes the current state of applicability of nanocrystalline iron oxides in the aforementioned fields and delineates challenges that may motivate future research in the chemistry of nanocrystalline iron oxides.

## 2. Catalytic applications of nanosized iron oxides

Heterogeneous catalysis mostly deals with various metal nanoparticles, supported catalysts, hybrid catalysts, and metal oxides,<sup>39–41</sup> which includes  $\text{Al}_2\text{O}_3$ ,  $\text{MgO}$ ,  $\text{CeO}_2$ ,  $\text{Fe}_3\text{O}_4$ ,  $\alpha\text{-Fe}_2\text{O}_3$ , and  $\gamma\text{-Fe}_2\text{O}_3$  among other iron oxides; often deployed themselves or as supports for important catalytic transformations.<sup>42–44</sup> To date, various magnetic catalysts or magnetic supported catalysts, predominantly based on iron oxides have been employed in numerous organic transformations besides other applications.<sup>45–47</sup>

In the case of iron oxides, up to now, four distinct crystalline polymorphic forms of ferric oxides namely  $\alpha$ -,  $\beta$ -,  $\gamma$ -, and  $\epsilon\text{-Fe}_2\text{O}_3$  have been thoroughly characterized and their applications described.<sup>23</sup> Because of their unique structural arrangements, each of the nanoscale polymorphic variants of  $\text{Fe}_2\text{O}_3$  exhibits distinctive magnetic, biochemical, and catalytic features;<sup>48–52</sup>  $\alpha\text{-Fe}_2\text{O}_3$  and related hybrid nanomaterials have been examined as heterogeneous catalysts.<sup>53–57</sup> The catalytic applications of various forms of iron oxides and related hybrid catalysts are deliberated with emphasis on the non-magnetic supported or/iron oxides, especially hematite. The magnetically recyclable catalysts,<sup>58–65</sup> electrocatalysts,<sup>66–70</sup> and assorted

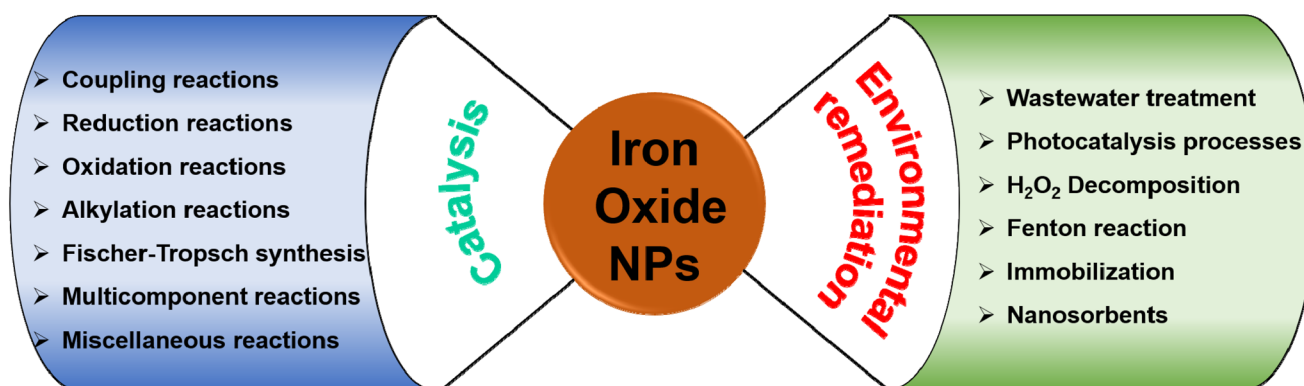


Fig. 3 Applications of iron oxide nanoparticles in catalysis and environmental technologies.

Fenton-type reactions<sup>71–74</sup> associated with iron oxides are not included here as they have been well discussed in the literature and being beyond the scope of this review, with the exception of environmental applications.<sup>75–82</sup>

Iron oxides are ideal oxide supports, as they are straightforward to synthesize, presence of highly reactive surface hydroxyl groups, facilitating effective adsorption and immobilization of metals and ligands. Additionally, they can be isolated through simple filtration post-reaction, rendering them relatively benign and greener heterogeneous catalysts.<sup>83,84</sup> In this section, nanoiron oxides (*e.g.*, hematite, goethite and their hybrid forms, like Au/ $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>,  $\beta$ -FeOOH@poly(dopamine)-Au-poly(dopamine), *etc.* and their catalytic applications are highlighted with few representative cases of their synthesis. A variety of catalytic transformations encompassing reduction-, oxidation-, coupling-, and alkylation reactions, Fischer Tropsch synthesis, multicomponent reactions, and other miscellaneous reactions are discussed (see Fig. 4).

## 2.1. Coupling reactions

Noble metal NPs, such as Pd, Pt, Au, and Ru, have garnered immense interest over the last decade because of their special features and promising applications in diverse fields like surface enhanced Raman scattering (SERS),<sup>85–87</sup> surface plasmon resonance (SPR),<sup>88,89</sup> and biomedicine<sup>90,91</sup> and especially in catalysis<sup>82,92–95</sup> encompassing C–C coupling reactions;<sup>96–98</sup> Heck and Suzuki reactions being the most

important examples.<sup>99–102</sup> These reactions are generally catalyzed by palladium-based catalysts and are widely deployed in the synthesis of various pharmaceuticals.<sup>103–106</sup> As it relates to catalysis, Pd is the widespread noble metal employed for its outstanding activity and selectivity in various coupling reactions under rather mild conditions.<sup>107–110</sup> However, there are still lingering limitations associated with such processes often stemming from the recovery of the catalyst and challenges pertaining to cumbersome isolation of the products. To overcome these problems, dispersion of Pd nanocatalysts on solid supports have been explored.<sup>111–115</sup>

**2.1.1. Suzuki–Miyaura cross-coupling reaction.** The Suzuki coupling reaction, which involves the cross-coupling of organoborons and organohalides, has emerged as a highly effective synthetic strategy for synthesizing a diverse array of biaryl compounds essential for various applications in natural products synthesis, pharmaceuticals, and polymers.<sup>108,116,117</sup> The Suzuki–Miyaura reaction stands out as the second most commonly utilized reaction in the realm of drug discovery and development.<sup>116</sup> Traditionally, these reactions are catalyzed by homogeneous Pd-complexed catalysts along with ligands like phosphorous and N-heterocyclic carbene.<sup>118</sup> While numerous homogeneous catalytic systems have been documented in the literature for efficiently driving Suzuki reactions, they encounter significant challenges pertaining to their recyclability and reusability.<sup>119</sup> The escalating demand and cost of Pd have prompted researchers to innovate and devise novel catalysts

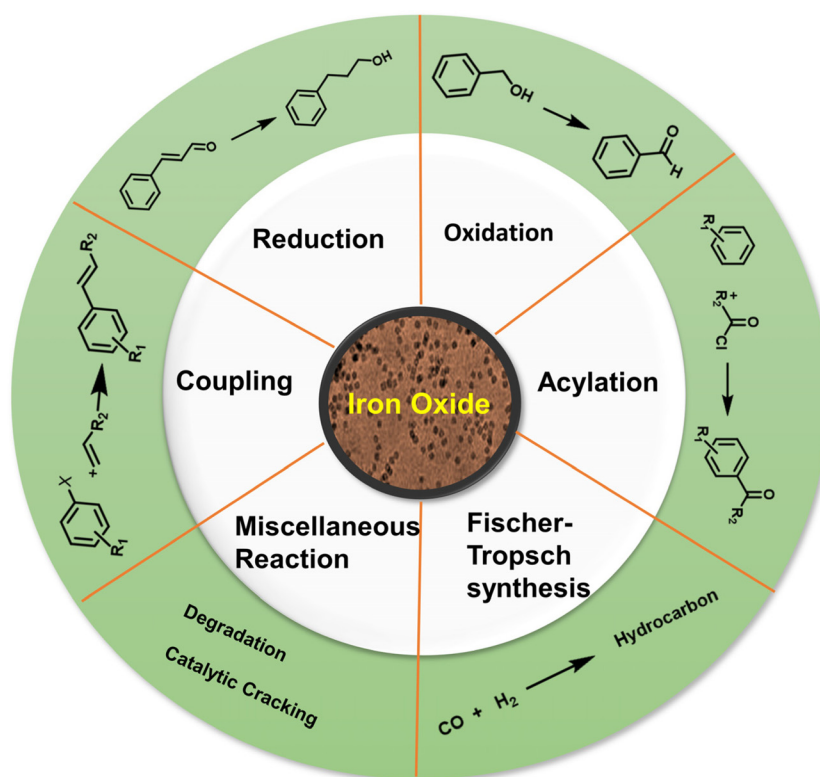


Fig. 4 Selected catalytic applications of nanocrystalline iron oxides.

that either eliminate the need for Pd or incorporate minimal amounts of this precious metal.<sup>120,121</sup>

The field of catalysis science has seen a notable development with the emergence of single-atom catalysts (SACs), where individual metal atoms are distributed on solid supports.<sup>122–124</sup> This novel approach has garnered significant research interest.<sup>43,125</sup> Recently, a highly efficient and scalable method for the synthesis of iron oxide-supported Pd SACs using a facile, eco-friendly ball milling process was reported for the Suzuki–Miyaura cross-coupling reaction.<sup>126</sup> In a typical gram-scale synthesis of Pd<sub>1</sub>/FeO<sub>x</sub>-10 SACs, the metal oxide, and Pd nitrate precursors are directly milled together in a planetary ball mill for a given time and then calcinated at 400 °C under aerobic conditions for 2 h (see Fig. 5a). Using this approach, a kilogram scale synthesis (up to 1.002 kg) of Pd<sub>1</sub>/FeO<sub>x</sub>-1000 SACs in one batch is also achieved, which holds considerable potential for application in industrial scale-up. The transmission electron microscopy (TEM) images of Pd<sub>1</sub>/FeO<sub>x</sub>-10 catalyst revealed that the absence of visible Pd nanoparticles or clusters, which indicated the uniform dispersion of Pd isolated atoms on iron oxide support (Fig. 5b). This homogeneous distribution of Pd, Fe, and O atoms is further confirmed by the elemental mapping images, suggesting a well-dispersed atomic structure (Fig. 5c). Additionally, the aberration-corrected high-angle annular dark-field scanning transmission electron microscopy (AC HAADF-STEM) images (Fig. 5d) demonstrated that the atomic dispersion of Pd species on the iron oxide support, as highlighted by the yellow circles. This well characterized Pd<sub>1</sub>/FeO<sub>x</sub>-10 catalyst exhibited remarkable catalytic activity, achieving a high turnover frequency (TOF) of 7844 h<sup>−1</sup> for the Suzuki–Miyaura cross-coupling reaction between bromobenzene and phenylboronic acid at 40 °C. Various aryl bromides containing electron-donating and withdrawing functional groups were efficiently converted into biphenyl products with high product yields (>95%) without the need for an inert atmosphere (Fig. 5e). This exceptional performance significantly surpassed other catalysts, including PdO, Pd/C, and Pd nanoparticles, highlighting the superior catalytic activity of the Pd<sub>1</sub>/FeO<sub>x</sub>-10 SACs. Furthermore, the catalyst displayed greater stability and recyclability, indicating its potential for practical applications in catalyzing cross-coupling reactions.

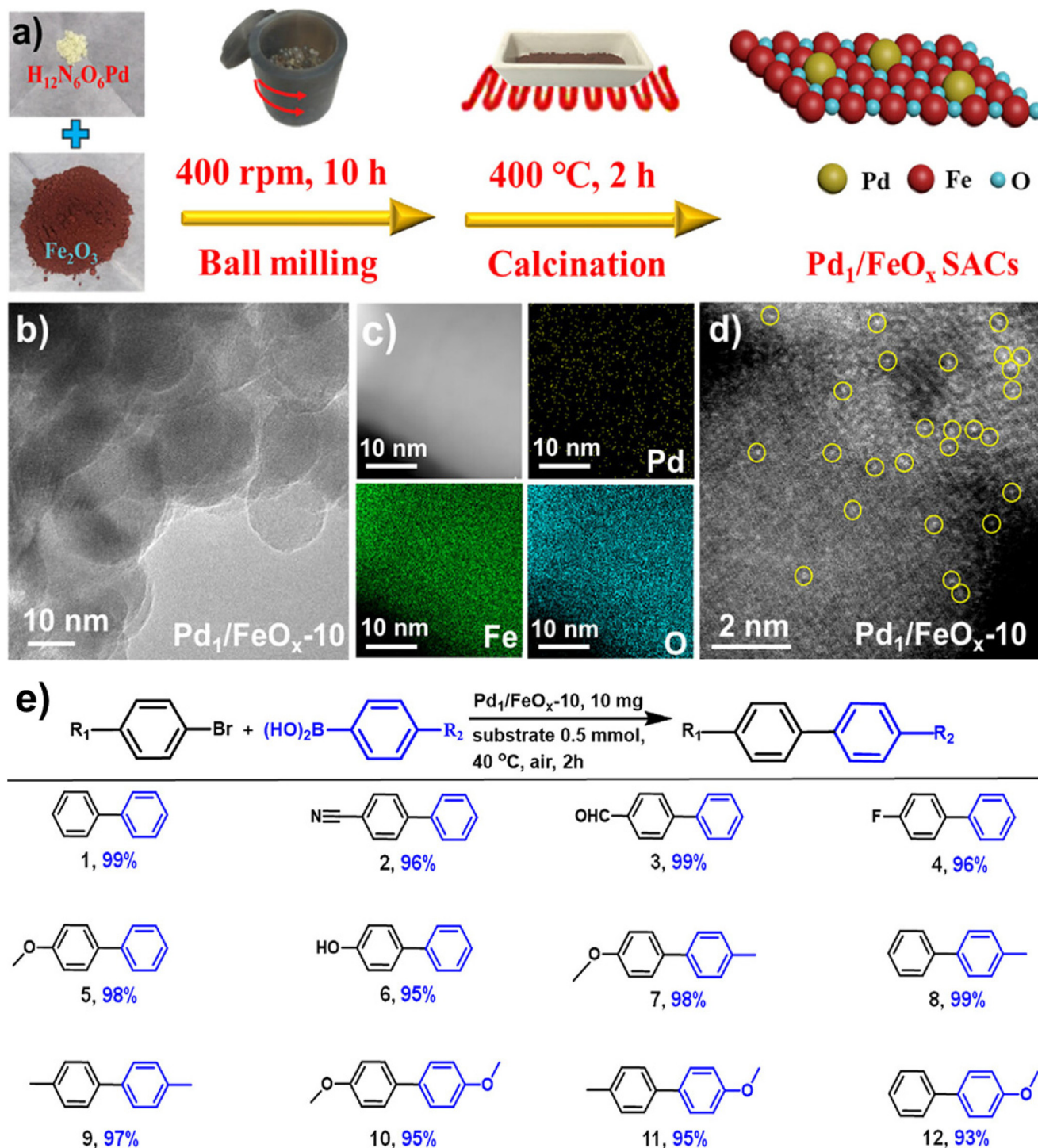
Iron oxide nanoparticles proved their high potential to act as a template for the production of advanced nanocatalyst.<sup>127–129</sup> Fe<sub>2</sub>O<sub>3</sub> containing zeolite-NaY (Fe<sub>2</sub>O<sub>3</sub>-Y) support have been developed for the fabrication of heterogeneous Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y nanocatalyst and deployed for the Suzuki–Miyaura cross-coupling reaction.<sup>130</sup> The support was prepared by employing coprecipitation method (Fig. 6a). The SEM images of the supported Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y nanocatalyst on zeolite-NaY revealed that the presence of foreign particles (Fig. 6c), whereas untreated zeolite-NaY displayed clear crystal indicating absence of additional particles (Fig. 6b). TEM analysis further confirmed the deposition of ultrafine Pd/PdO NPs on Fe<sub>2</sub>O<sub>3</sub>-Y support (Fig. 6d and e). This Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y catalyst demonstrated remarkable efficiency in activating the

robust C–Cl bond of aryl chlorides in the Suzuki–Miyaura cross-coupling reaction under mild conditions (Fig. 6f). Despite having an extremely low metal (Pd) loading of 0.0037 mol%, this catalyst exhibited higher reactivity, selectivity, and recyclability; ensued biaryl product yield of up to 92% with a good turnover number (249) was discerned. Particularly, biaryl product yield significantly improved when a small amount of water with methanol was used as a solvent system for the reaction. The presence of basic sites, together with zeolite-NaY and the transfer of charge from Fe to Pd, played a pivotal role in the activation of the C–Cl bond.

Diao and co-workers<sup>131</sup> synthesized hollow carbon nanonets (HCN) by combining hydrothermal carbonization of glucose with  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs acting as a hard template; Pd NPs were immobilized onto the exterior of the hollow HCN *via in situ* precipitation-reduction method (Fig. 7). HCN have been attractive candidates for the catalyst support as they could be fabricated employing the pre-synthesized hematite NPs as the hard template. Carbon supported porous nanostructures have demonstrated significant efficacy as catalyst support, particularly for noble metal nanocatalysts.<sup>132–134</sup> TEM images of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>@C, HCN, and Pd/HCN are depicted in Fig. 7b–e. The  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs with 50 nm diameter (Fig. 7a) have been prepared by hydrothermal precipitation, whereas the Pd nanoparticles with diameter  $\sim$ 8 nm was formed when the reduction/precipitation method was employed to graft Pd NPs on HCN. Following their synthesis and comprehensive characterization, the Pd/HCN catalysts were then investigated for the Suzuki and Heck–Miyaura reaction under mild reaction parameters. Notably, outstanding yields of the respective products were achieved in an aqueous medium (irrespective of the halides counterparts) with good Turnover frequency (TOF) for Suzuki cross-coupling reaction. The reaction scope was further explored for Heck–Miyaura reaction of haloarenes with alkenes at 120 °C, in DMF (dimethyl formamide) using a base, K<sub>2</sub>CO<sub>3</sub>. Comparatively, iodobenzene gave excellent yields of products, while bromobenzene and chlorobenzene gave rather low yields of the coupling products. Furthermore, when compared with some reported Pd-supported catalysts, the catalytic performance of Pd/HCN in facilitating the Suzuki reaction, between phenyl boronic acid and iodobenzene, displayed notable efficiency in terms of both product yields and reaction time.<sup>131</sup>

A heterogeneous iron oxide catalyst on graphene oxide (GO) support ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanocluster/GO) was synthesized for the Suzuki–Miyaura coupling reaction and hydrogenation of 4-hydroxynitrobenzene in an aqueous medium.<sup>135</sup> For the assembly of the catalyst, the tris-trz-PEG ligand was employed to promote the fabrication and deposition of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> on GO by supramolecular interactions (Fig. 8a). The TEM images revealed that the uniform deposition of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>, with a size of 1.8 nm, on the GO (Fig. 8b). The hexagonal morphology and a lattice fringe space (0.25 nm) correspond to the crystallographic plane (110) of the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystal, which was affirmed by HR-TEM analysis (Fig. 8c). In context of the Suzuki–Miyaura coupling in aqueous medium, Handa *et al.* developed a novel Fe/ppm Pd nanoparticle catalyst.<sup>136</sup> The highly active needle-



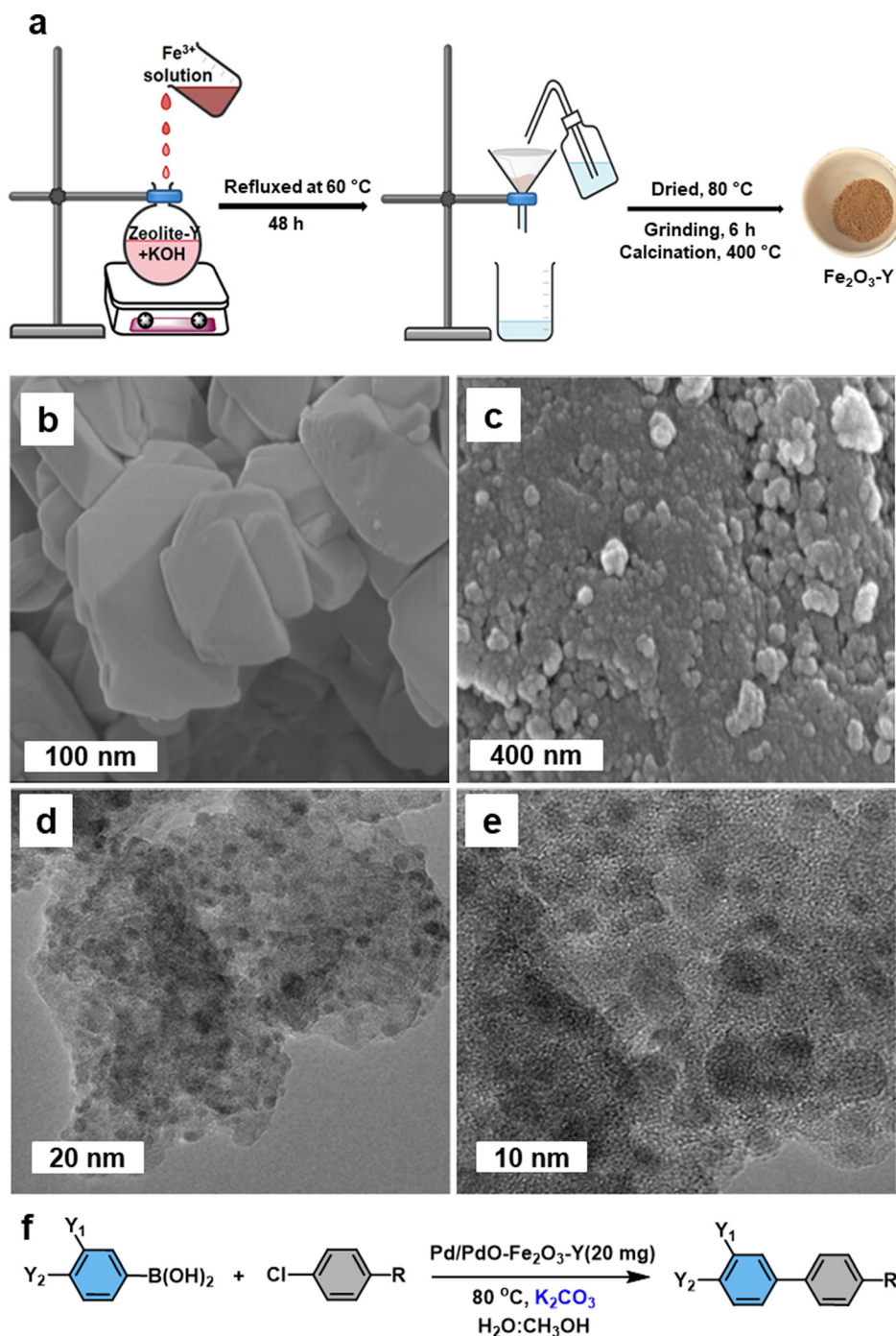


**Fig. 5** (a) Schematic representation of the synthesis of  $\text{Pd}_1/\text{FeO}_x\text{-10}$  catalysts; TEM (b), elemental mapping (c) and AC HAADF-STEM (d) images of  $\text{Pd}_1/\text{FeO}_x\text{-10}$ ; (e)  $\text{Pd}_1/\text{FeO}_x\text{-10}$  catalyzed Suzuki-Miyaura cross-coupling. Reproduced with permission from ref. 126 Copyright 2022, American Chemical Society.

shaped NPs of Fe/ppm Pd catalysts facilitated the Suzuki-Miyaura couplings across a broad range of electrophiles and nucleophiles. This innovative approach enabled the first ppm-level Pd catalysis under micellar conditions, offering signifi-

cant value to the pharmaceutical industry by reducing the residual palladium in the final product.

**2.1.2. C-N coupling.** Compounds with nitrogen atoms play a crucial role in the production of heterocyclic compounds,

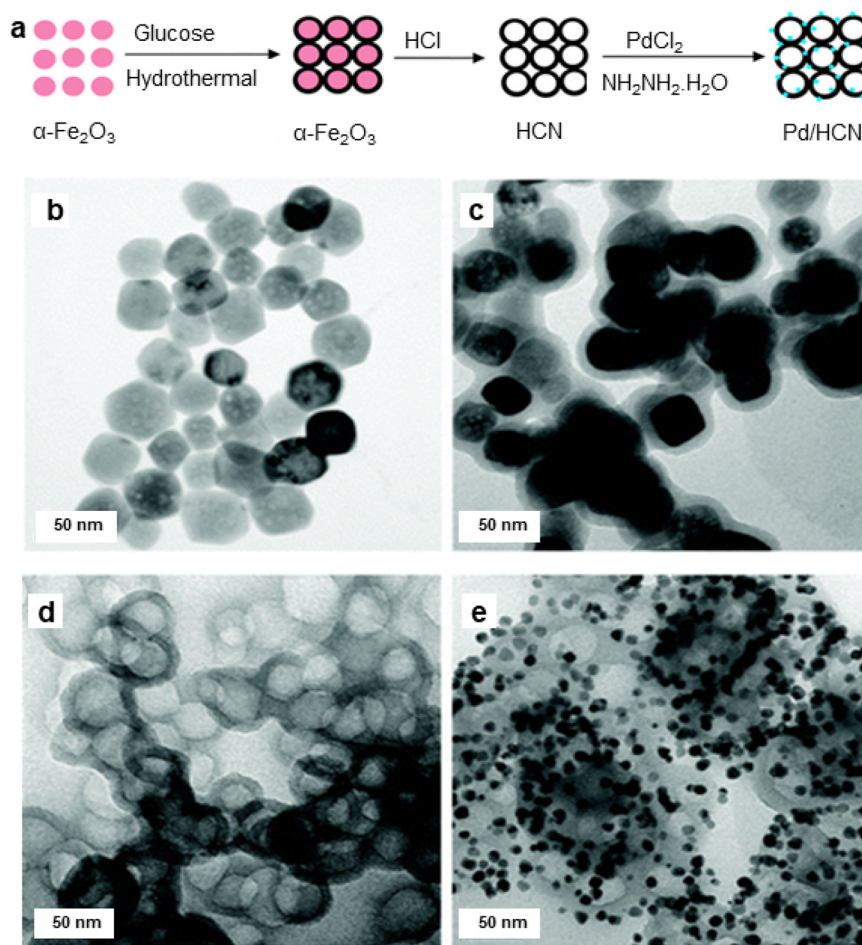


**Fig. 6** (a) Schematic illustration of the preparation of Fe<sub>2</sub>O<sub>3</sub>-Y; (b, c) SEM images of untreated zeolite-NaY and Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y respectively; (d, e) TEM images of Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y; (f) Pd/PdO-Fe<sub>2</sub>O<sub>3</sub>-Y mediated Suzuki-Miyaura cross-coupling reaction. Reused with permission from ref. 130 Copyright 2023, American Chemical Society.

pharmaceutical intermediates, various organic substances, ligands, and the development of catalysts due to their significant impact and versatility in assorted chemical applications.<sup>137</sup> Therefore, the advancement of cross-coupling reactions that form C-N bonds using substrates containing -NH groups has become highly significant in both the industrial and academic sectors.<sup>138,139</sup> In a recent study, iron oxide NPs

exhibiting oxygen vacancies (Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>) with variable Fe sites were used as a catalyst for the carbonylation reaction of aryl halides and amines/alcohols in presence of CO.<sup>140</sup> The study involves a C-N/C-O coupling reaction as part of the carbonylation process. Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalysts with varying oxygen vacancies were synthesized by hydrothermal reduction of Fe<sub>2</sub>O<sub>3</sub> using NaBH<sub>4</sub> (Fig. 9a). These catalysts were labelled as





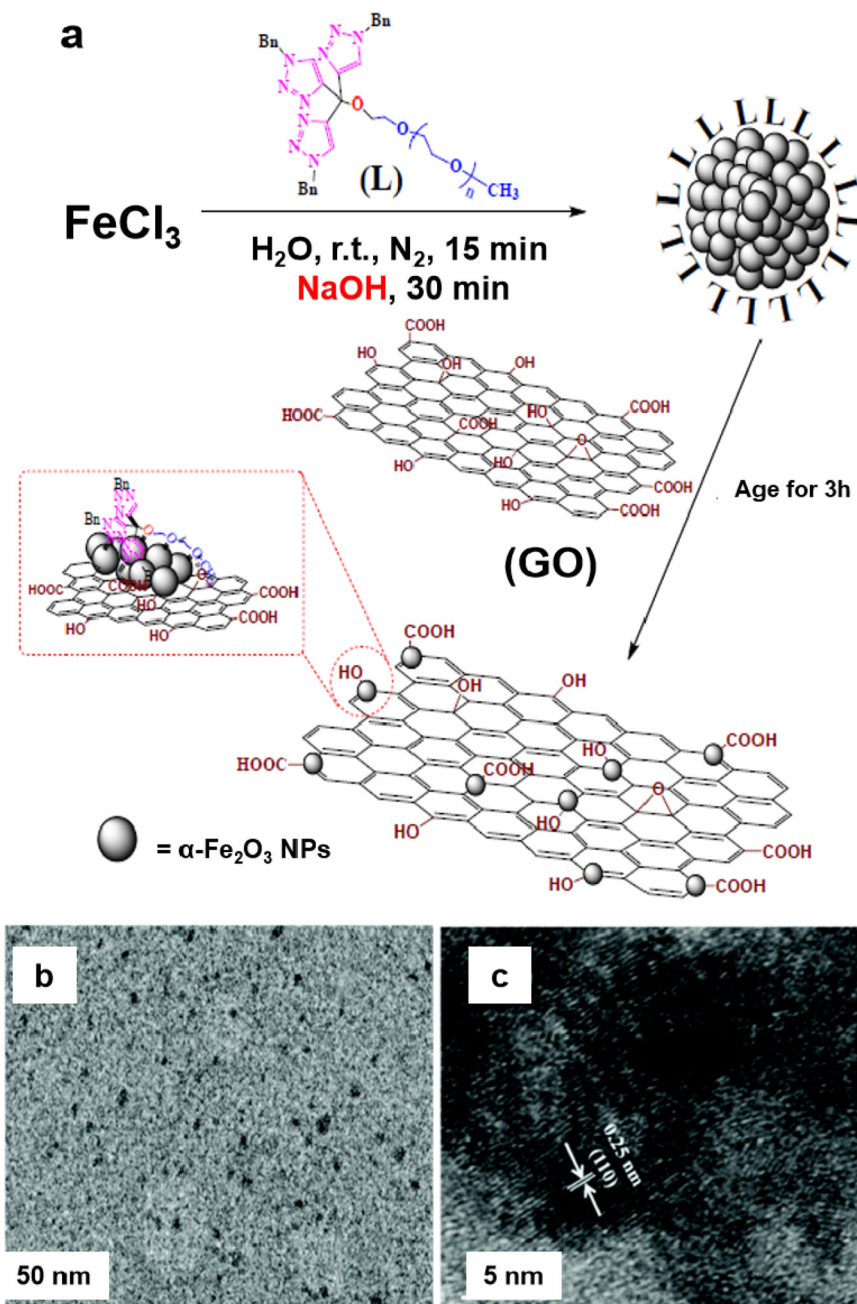
**Fig. 7** (a) Schematic illustration of synthesis of the Pd/HCN catalysts; (b–e) TEM images of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>@C, HCN, and Pd/HCN catalysts respectively. Reproduced with permission from ref. 131 Copyright 2013, The Royal Society of Chemistry.

0.5 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, and 2.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, with the numbers indicating the molar ratio of NaBH<sub>4</sub> to Fe<sub>2</sub>O<sub>3</sub> used in the synthesis process (0.5, 1.0, and 2.0, respectively). The morphology and structural features of the catalyst were investigated using TEM and HR-TEM analysis. TEM images showed that the catalysts had a cube-like structure with a diameter of approximately 400 nm (Fig. 9b–d). The HR-TEM images demonstrated a consistent lattice fringe spacing of 0.280 nm, which was in agreement with the (104) lattice of Fe<sub>2</sub>O<sub>3</sub> (Fig. 9e–g). The (104) lattice was observed for all the Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalysts, including 0.5 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, and 2.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub>, indicating that the morphology and structure of the catalysts were not affected by the NaBH<sub>4</sub> reduction treatment. Furthermore, the existence of oxygen vacancies and different Fe sites of the Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst was confirmed by O 1s XPS and XANES spectra, respectively (Fig. 9h and i).

The catalytic performance of the synthesized 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst was examined under the optimized condition *via* aminocarbonylation and alkoxycarbonylation (Fig. 10a and b).<sup>140</sup> The ideal 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst demonstrated conversion of aryl halides and amines/alcohols into the corresponding amides/esters with excellent yields (75–99%). Additionally, the

catalytically active 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst was also explored for the synthesis of important drugs such as Moclobemide, CX-546, Nikethamide, and chiral compounds *via* carbonylation reactions (Fig. 10c), highlighting their potential for pharmaceutical applications. The catalytic activity of the 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalysts was found to be critically dependent on the presence and density of oxygen vacancies, directly impacting their performance. Furthermore, the different Fe sites on the Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> surface emerged as a crucial factor in enhancing catalytic efficiency. The 1.0 Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst showed excellent recyclability, indicating its suitability for sustainable catalytic applications. The catalytic mechanism of the carbonylation reaction has been studied using DFT calculations. The Fe<sub>2</sub>O<sub>3</sub>-O<sub>vac</sub> catalyst facilitated the elementary steps of PhI activation, CO insertion, and C–N/C–O coupling efficiently, leading to improved catalytic performance (Fig. 10d).

The strategy of borrowing hydrogen is one of the benign approaches for the C–N coupling reaction as it circumvents the necessity for an external hydrogen source for the reduction reactions.<sup>141–144</sup> The heterogeneous iron oxide nanocatalyst<sup>145</sup> for the C–N/C–C bond formation reactions *via* borrowing hydrogen approach were reported to obtain quinoline and its



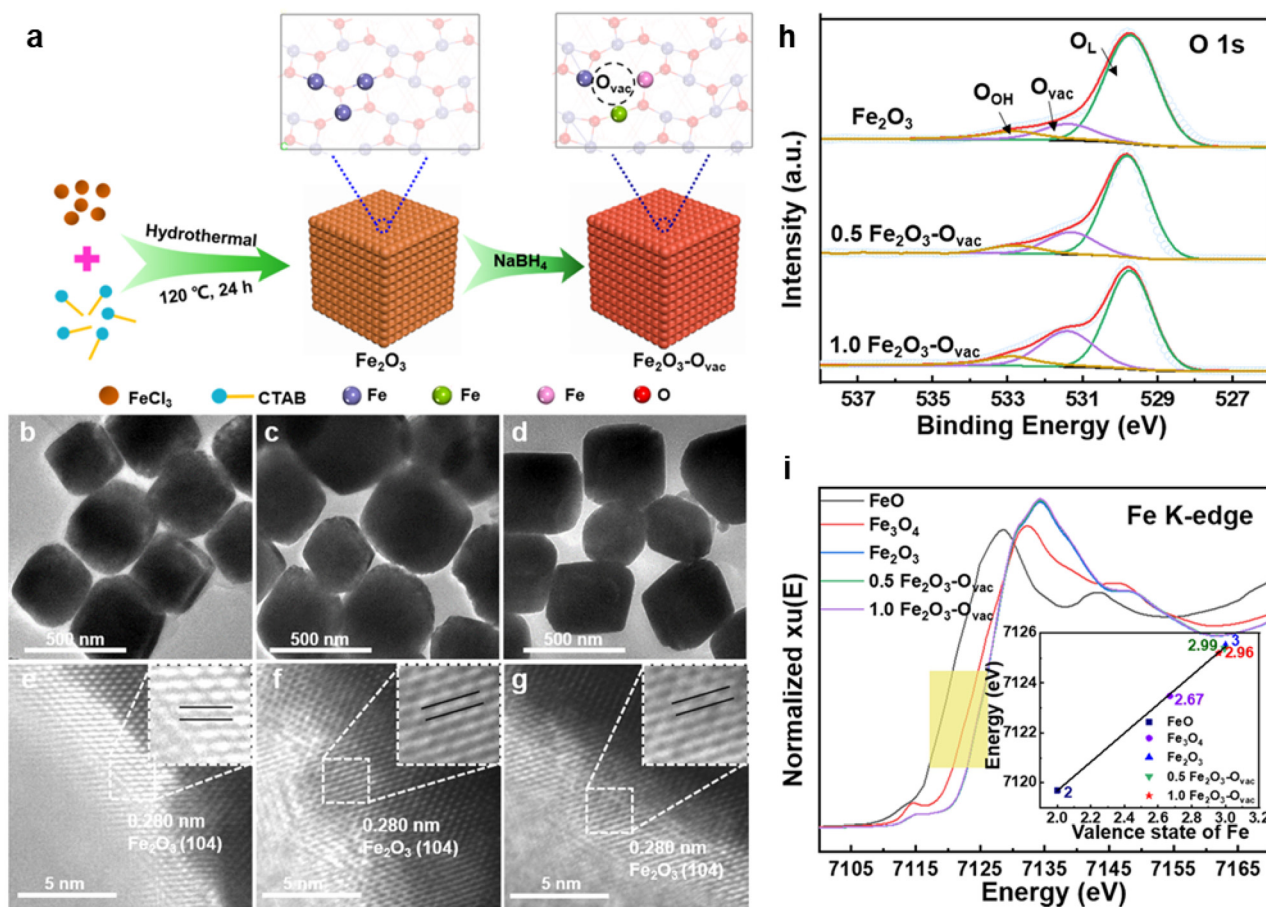
**Fig. 8** (a) Schematic representation for the synthesis of the  $\alpha\text{-Fe}_2\text{O}_3/\text{GO}$  catalyst; (b, c) TEM and HR-TEM images of  $\alpha\text{-Fe}_2\text{O}_3$  nanocluster/GO catalyst. Reproduced with permission from ref. 135 Copyright 2017, The Royal Society of Chemistry.

derivatives (Fig. 11); hydrogen auto-transfer mechanism was confirmed by the deuterium labelling study. In the similar context, Sarno *et al.* prepared core-shell  $\text{Fe}_3\text{O}_4/\text{Au}$  nanocatalyst and deployed it for the *N*-alkylation reactions.<sup>146</sup>

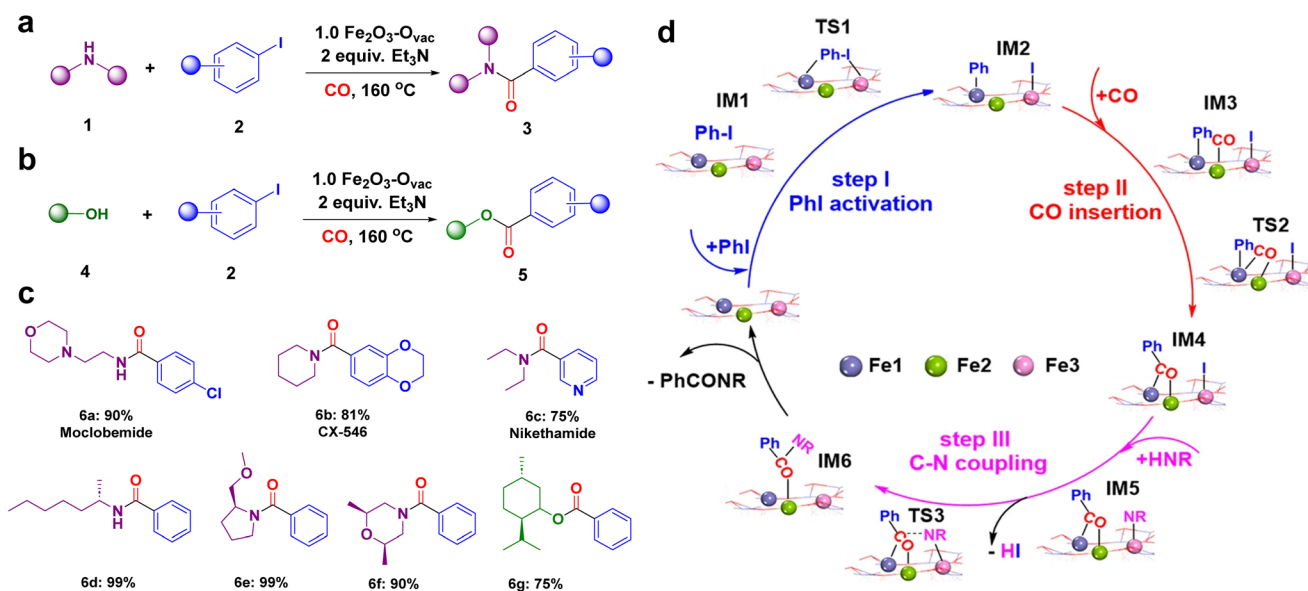
**2.1.3. Sonogashira coupling.** Sonogashira coupling is a highly effective method utilized in organic chemistry for the synthesis of conjugated compounds by linking aryl halides and alkynes to form C–C bonds. This method is widely documented and recognized for its efficiency in constructing C–C bonds.<sup>147–149</sup> Iron oxide-based NPs were also explored for

Sonogashira coupling reaction.<sup>150</sup> In this regard iron oxide based nanocatalyst,  $\text{PdCu@GQD@Fe}_3\text{O}_4$ , have been synthesized for the Sonogashira coupling reaction<sup>151</sup> which had been prepared by the modification of  $\text{Fe}_3\text{O}_4$  nanoparticles with graphene quantum dots (GQD) to stabilize the PdCu NPs (Fig. 12a). The small NPs with particle sizes in the ranges of 3–4 nm and 9–25 nm were present in the structure (Fig. 12b and c). The TEM images affirm the existence of  $\text{Fe}_3\text{O}_4$  NPs and thin layered GQD (Fig. 12c). The  $\text{PdCu@GQD@Fe}_3\text{O}_4$  exhibits high catalytic activity and recyclability for Sonogashira coup-

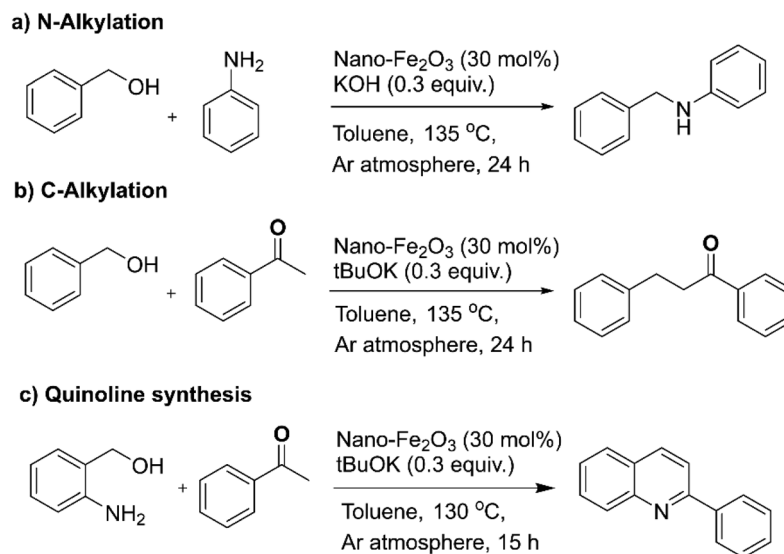




**Fig. 9** (a) Schematic illustration of the synthesis of  $\text{Fe}_2\text{O}_3\text{-O}_{\text{vac}}$ ; TEM and HR-TEM images of  $\text{Fe}_2\text{O}_3$  (b, e),  $0.5 \text{ Fe}_2\text{O}_3\text{-O}_{\text{vac}}$  (c, f),  $1.0 \text{ Fe}_2\text{O}_3\text{-O}_{\text{vac}}$  (d, g); (h) O 1s XPS spectra; (i) X-ray absorption near-edge structure (XANES) spectra of Fe K-edge. Reused with permission from ref. 140 Copyright 2023, Springer Nature.



**Fig. 10** Catalytic applications of  $1.0 \text{ Fe}_2\text{O}_3\text{-O}_{\text{vac}}$  catalyst (a) the aminocarbonylation; (b) alkoxycarbonylation reaction; (c) synthesized important drugs and chiral compounds; (d) mechanism for the aminocarbonylation. Reused with permission from ref. 140 Copyright 2023, Springer Nature.



**Fig. 11** (a–c) The *N*-alkylation, *C*-alkylation and quinoline synthesis over nano-Fe<sub>2</sub>O<sub>3</sub> catalyst. Reproduced with permission from ref. 145 Copyright 2019, The Royal Society of Chemistry.

ling reaction of different aryl iodides, bromides, and chlorides with various terminal alkynes, achieving excellent yield of product with only 0.3 and 0.35 mol% loading of Pd and Cu, respectively (Fig. 12d). The existence of copper in PdCu@GQD@Fe<sub>3</sub>O<sub>4</sub> catalyst was proven to be essential for achieving optimal yields. In the similar context, Handa *et al.* reported recyclable Cu free iron-based NPs with ppm level of Pd as an active catalyst for the Sonogashira reaction under mild conditions.<sup>152</sup>

## 2.2. Reduction reactions

Reduction reactions are indispensable in various industries, for the syntheses of pharmaceuticals, dyes and rubber, and agricultural chemicals<sup>153–155</sup> among others. Nanosized iron oxides have garnered attention among researchers for the catalytic hydrogenation of aromatic nitro groups,  $\alpha,\beta$ -unsaturated aldehydes, nitric oxide (NO) in view of their inexpensive nature, ease of preparation and environmentally benign attributes.

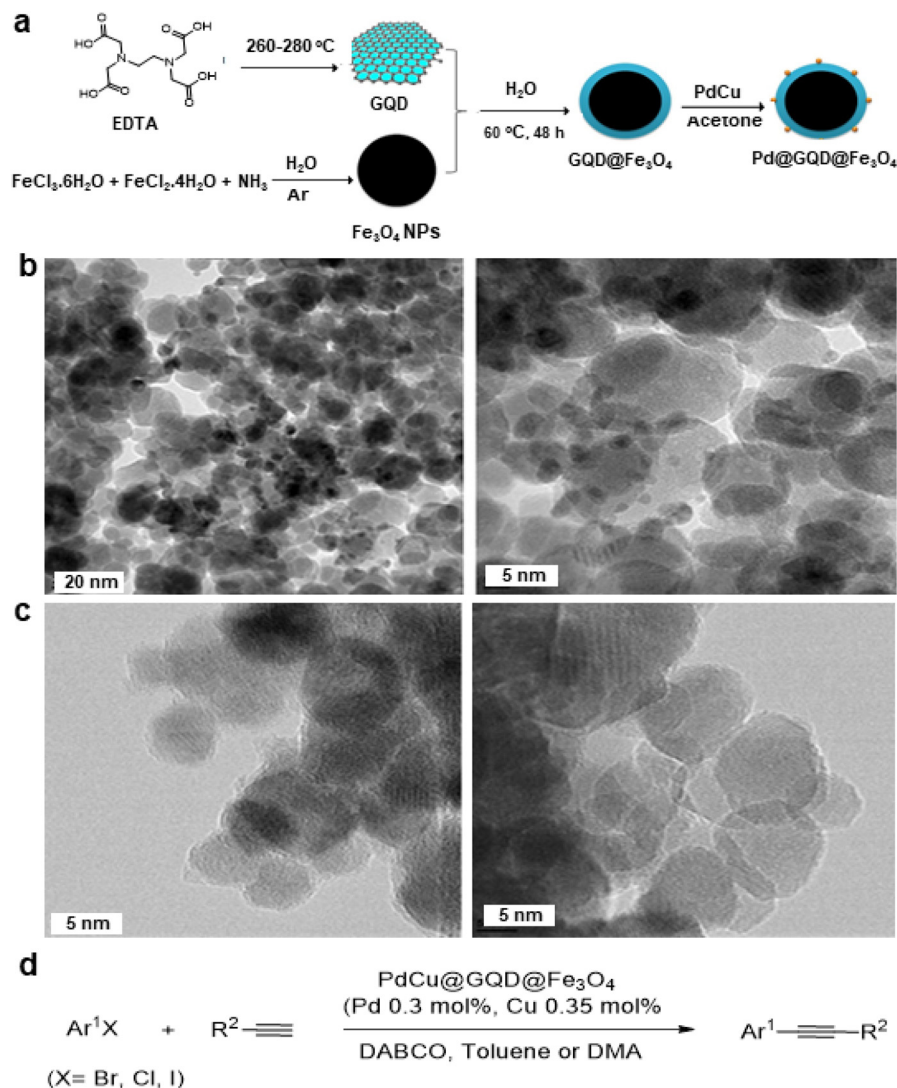
Goethite (FeOOH), maghemite ( $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>) and hematite ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>) supported gold catalysts have been used for reduction of cinnamaldehyde and *trans*-benzalacetone.<sup>156</sup> Among these studied catalysts, Au anchored on FeOOH (AF35G) presented excellent performance and selectivity for unsaturated alcohols to generate the corresponding unsaturated carbonyl compounds, while Au anchored on  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> (AF35H) and  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub> (AF35M) displayed inferior performances. It is crucial to emphasize that the catalytic performance for unsaturated alcohols in the reduction of cinnamaldehyde and benzalacetone are completely dependent on the characteristics of supporting material wherein both the performance and selectivity to unsaturated alcohols is enhanced due to the reducibility of the catalysts. Finally, it has been concluded that the

active and selective sites are generated *via* transfer of electron from the reduced support to the metal nanoparticles.<sup>156</sup>

Iron oxide supported Au catalyst for the liquid phase hydrogenation of  $\alpha,\beta$ -unsaturated aldehydes was reported.<sup>157</sup> Various supports including hematite, goethite, and iron oxide modified alumina have been used for the immobilization of gold and the corresponding catalysts investigated for the reduction of crotonaldehyde and cinnamaldehyde at 100 °C and at 1 MPa of H<sub>2</sub> in 2-propanol (Fig. 13). It is observed that iron oxides immobilized gold particles are more selective relative to  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> supported gold particles; hematite supported gold exhibits the high selectivity for unsaturated alcohols like cinnamyl alcohol (48%) and hydrocinnamyl alcohol (88%). Furthermore, no dependence of selectivity on substrates such as crotyl alcohol and cinnamyl alcohol has been discerned on gold particles.

The noble metal Pt was adorned on iron oxide *via* the atomic layer deposition and deployed for the selective hydrogenation of cinnamaldehyde to cinnamyl alcohol;<sup>158</sup> Pt NPs with 2.7 nm size were evenly dispersed over the alumina support (Fig. 14a and b) wherein the Pt30Fe30 catalyst exhibited higher selectivity (84%) as compared to the pure Pt catalyst (45%) for cinnamyl alcohol (Fig. 14c).

The chemoselective hydrogenation of cinnamaldehyde to cinnamyl alcohol were also carried out by employing an iron oxide decorated catalyst (Pt-3FeO<sub>x</sub>/MoO<sub>3-y</sub>).<sup>159</sup> The observed lattice fringes of 0.226 and 0.196 nm refers to Pt (111) and Pt (200), respectively. The size of Pt NPs was 3 nm which were well dispersed on FeO<sub>x</sub> (Fig. 15a and b). The Pt-3FeO<sub>x</sub>/MoO<sub>3-y</sub> catalyst showed a higher conversion and selectivity for cinnamyl alcohol due to the Pt-FeO<sub>x</sub> interfaces (Fig. 15c). The acidic Pt-FeO<sub>x</sub> interface had direct impact on the chemisorption and activation of the carbonyl group (C=O), leading to the selec-



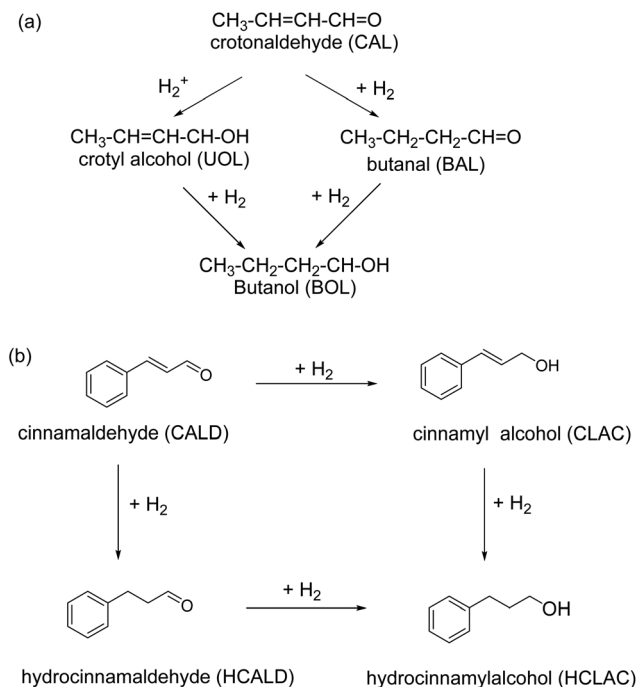
**Fig. 12** (a) Schematic representation for synthesis of PdCu@GQD@Fe<sub>3</sub>O<sub>4</sub> nanocatalyst; (b) TEM images PdCu@GQD@Fe<sub>3</sub>O<sub>4</sub>; (c) TEM images of GQD@Fe<sub>3</sub>O<sub>4</sub> NPs and (d) Application of Sonogashira–Hagihara reaction over the catalyst PdCu@GQD@Fe<sub>3</sub>O<sub>4</sub>. Reproduced with permission from ref. 151 Copyright 2017, Wiley-VCH GmbH & Co. KGaA, Weinheim.

tive cinnamaldehyde hydrogenation to cinnamyl alcohol (Fig. 15d).

The hydrogenation of nitroarenes by heterogeneous catalysis has been an imperative chemical transformation. The selective hydrogenation of nitro compounds containing additional reducible groups such as alkene, carbonyl, and/or halide to produce functionalized amines poses a significant and challenging task in both contemporary chemical and pharmaceutical industry.<sup>160–163</sup> In this context, Ma *et al.*<sup>164</sup> fabricated TiO<sub>2</sub> based iron oxide (Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub>) heterogeneous photocatalyst for the selective hydrogenation of nitroarenes into amine derivatives. The Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst was synthesized by the sol-gel approach followed by the pyrolysis process (Fig. 16a). The catalyst structure comprises Fe<sub>3</sub>O<sub>4</sub> NPs supported on TiO<sub>2</sub>, forming a composite with a well-defined morphology evident by TEM and HRTEM analysis (see Fig. 16b and c). The lattice

fringes observed in the HRTEM image (Fig. 16c) correspond to specific crystal planes within the iron oxide phase, with measurements of 2.5 Å and 2.9 Å corresponding to the (311) and (220) planes, respectively. Additionally, a lattice fringe of 3.5 Å was attributed to the TiO<sub>2</sub> (100) plane. The prepared Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> photocatalyst demonstrated remarkable efficiency in the selective hydrogenation of nitroaromatics to amines in the presence of other reducible groups under photothermal conditions (Fig. 16d). The exceptional performance of the Fe<sub>3</sub>O<sub>4</sub>@TiO<sub>2</sub> catalyst was attributed to the robust interaction between Fe<sub>3</sub>O<sub>4</sub> and the reducible TiO<sub>2</sub> support, boosting the photothermal effect and enhancing the adsorption of reactants. Moreover, this catalyst was also utilized for gram-scale reactions, showcasing its viability for diverse applications in organic synthesis, offering a sustainable and efficient alternative for the conversion of nitro compounds to valuable amines.





**Fig. 13** Hydrogenation of (a) crotonaldehyde, and (b) cinnamaldehyde using gold NPs supported on iron oxides. Reproduced with permission from ref. 157 Copyright 2009, Elsevier.

The oxygen defective nanocrystalline iron oxide catalysts ( $\text{Fe}_3\text{O}_4$ ) were used for the reduction of several nitroarenes to respective anilines with excellent yield and selectivity. Among as-prepared catalysts,  $\text{Fe}_3\text{O}_4$  showed high activity, excellent recycling stability, and 100% selectivity.<sup>165</sup> Moreover, Pt SACs and pseudo SACs supported on iron oxide were developed by Zhang and coworkers and deployed for the selective hydrogenation of nitroarenes.<sup>166</sup> The 0.08%Pt/ $\text{FeO}_x$ -R250 catalysts exhibited broad compatibility with a diverse range of substituted nitroarenes containing various functional groups, showcasing their versatility and applicability. In addition, micro-mesoporous iron oxide also employed for the base free transfer hydrogenation of nitroarenes.<sup>167</sup>

The hydrogenation of N-heterocycles in aqueous media was studied using the  $\text{Rh@Fe}_3\text{O}_4$  nanocatalyst,<sup>168</sup> where the Rh particles were uniformly distributed on the  $\text{Fe}_3\text{O}_4$  particles (7–9 nm) as scrutinized by TEM image analysis (Fig. 17a and b). The identification of Rh was confirmed by STEM (Fig. 17e) and <1 nm size of the Rh NPs (denoted by red circles) was affirmed by HR-TEM image of  $\text{Rh@Fe}_3\text{O}_4$  (Fig. 17f). The heterogeneous  $\text{Rh@Fe}_3\text{O}_4$  catalyst proved to be highly effective in the hydrogenation of N-heterocyclic compounds in water using tetrahydroxydiboron (THDB) as a reductant, demonstrating high selectivity for 1,2,3,4-tetrahydroquinoline (py-THQ) with an impressive turnover frequency of  $1632 \text{ h}^{-1}$  (Fig. 17h).

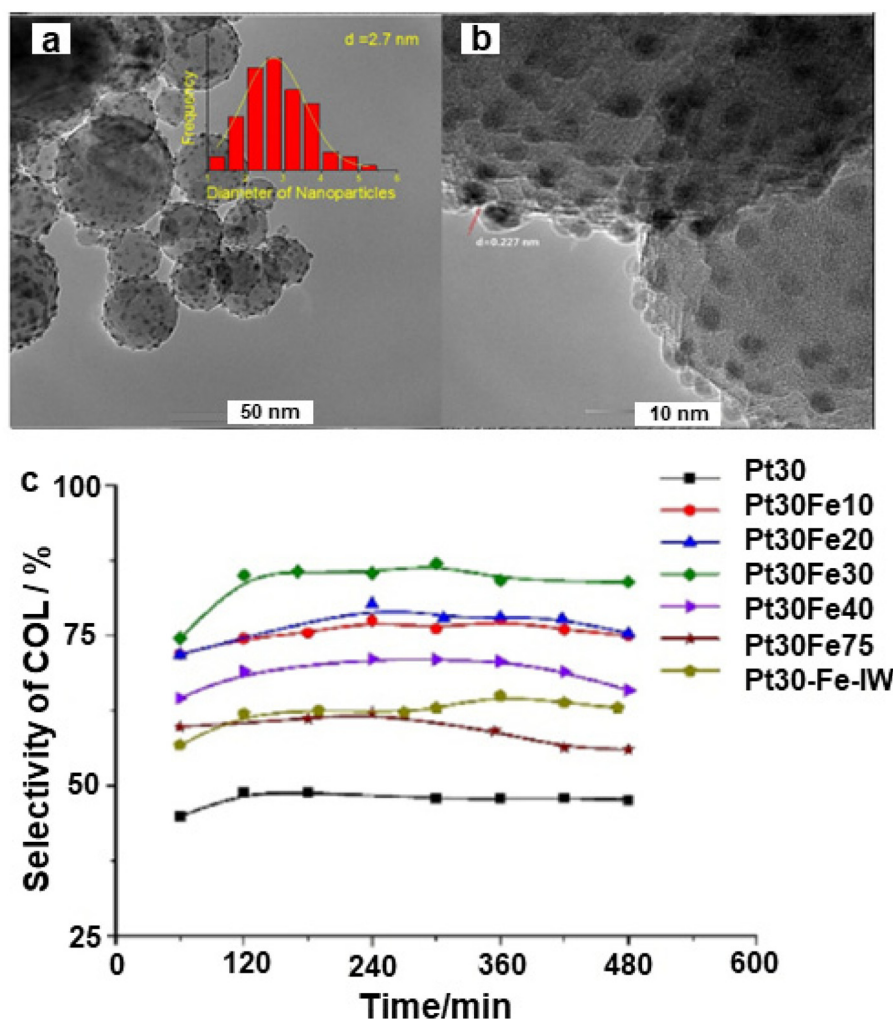
Afterwards, the  $\text{Rh@Fe}_3\text{O}_4$  nanocatalyst was modified by incorporation of  $\text{Co}_3\text{O}_4$  nanoparticles wrapped in N-doped g- $\text{C}_3\text{N}_4$  on  $\text{Fe}_3\text{O}_4$  support.<sup>169</sup> The synthesis of  $\text{Co}_3\text{O}_4/\text{N-Gr}/\text{Fe}_3\text{O}_4$  nanocomposites is depicted in Fig. 18a wherein the

$\text{Co}_3\text{O}_4$  NPs (15–20 nm) were wrapped in N-doped graphitic carbon on the surface of  $\text{Fe}_3\text{O}_4$  (Fig. 18b and c). The lattice spacing  $d$ -value (2.43 Å) is associated with (111) plane of crystalline  $\text{Co}_3\text{O}_4$  NPs as analyzed by HR-TEM (Fig. 18d). The core-shell morphology of this nanocomposite was confirmed by the HAADF-STEM imaging (Fig. 18e). This nanocomposite was deployed for the hydrogenation of nitroarenes, cinnamaldehyde, and quinoline (Fig. 18f). Notably, more than 99% hydrocinnamaldehyde (HCAL) chemoselectivity was obtained in toluene at 30 bar  $\text{H}_2$  (Fig. 18g).

Recently, silica-supported Fe/Fe-O NPs ( $\text{Fe/Fe-O@SiO}_2$ ) were utilized for the reduction of nitriles to amines.<sup>170</sup> The catalyst was synthesized through the impregnation and thermal treatment of Fe salt over the silica (Fig. 19a). The globular and rod-shape structure (Fig. 19b and c) and Fe core NPs resulting from  $\text{SiO}_2$  matrix covered by ultrathin iron oxide (Fig. 19d and e) comprising the catalyst,  $\text{Fe(OAc)}_2\text{-SiO}_2\text{-800}$ , was investigated by the TEM, HR-TEM imaging, and elemental analysis, respectively. The as-prepared catalyst with the catalytic amount of aluminium additives was employed for the reduction of various nitriles (aromatic, aliphatic, and heterocyclic) to important primary amines (Fig. 19f). Moreover, this catalyst was investigated for its utility in the reduction of fatty nitriles to respective fatty amines which are valuable oleochemicals (Fig. 19g). Apart from the cinnamaldehyde, nitroarenes and quinoline reduction, iron oxide was also instrumental in the reduction of 5-hydroxymethylfurfural (HMF) to 2,bis(hydroxymethyl)furan (BHMF).<sup>171</sup>

Selective catalytic reduction (SCR) of NO with ammonia at lower temperature has been reported *via* the deployment of  $\text{Fe}_2\text{O}_3$  catalysts<sup>172</sup> and various reaction parameters were inspected including temperature, oxygen concentration, and  $[\text{NH}_3]/[\text{NO}]$  molar ratio for SCR activity. Notably,  $\text{Fe}_2\text{O}_3$  catalysts displayed excellent catalytic performance for the SCR of NO with ammonia in a wide range of temperature from 150–270 °C; more than 95% NO conversion was achieved at 180 °C (molar ratio  $[\text{NH}_3]/[\text{NO}] = 1$ ). When the addition of  $\text{SO}_2$  on SCR catalytic performance were examined at 180 °C, the NO conversion was lowered from 99% to 58% in 240 min. Thermogravimetric and Fourier transform infrared spectroscopy analysis revealed<sup>172</sup> that  $\text{SO}_2$  was responsible for the deactivation of  $\text{Fe}_2\text{O}_3$  catalysts because the development of metal and ammonium sulfates at the surface of the catalyst during the de-NO reaction, leading to pore clogging and catalytic activity inhibition.

Similarly,  $\text{FeW}_{(x)}$  (hematite supported tungsten) catalysts with diverse Fe/W molar ratios obtainable through co-precipitation procedure were introduced for the SCR of  $\text{NO}_x$  with  $\text{NH}_3$ .<sup>173</sup> Among the catalysts subjected to testing, namely ( $\text{FeW}_{(1)}$ ,  $\text{FeW}_{(2)}$ ,  $\text{FeW}_{(3)}$ ,  $\text{FeW}_{(4)}$ ,  $\text{FeW}_{(5)}$ ), the catalyst  $\text{FeW}_{(5)}$  demonstrated an excellent activity, achieving nearly quantitative conversion of NO,  $\text{N}_2$  selectivity from 250 to 450 °C, and robust  $\text{H}_2\text{O}/\text{SO}_2$  strength at temperature more than 300 °C. It was observed that the insertion of  $\text{WO}_x$  moiety enabled the lattice structure to alter to the hematite form and high distribution of  $\text{WO}_x$  on the catalysts surface were noticed for the



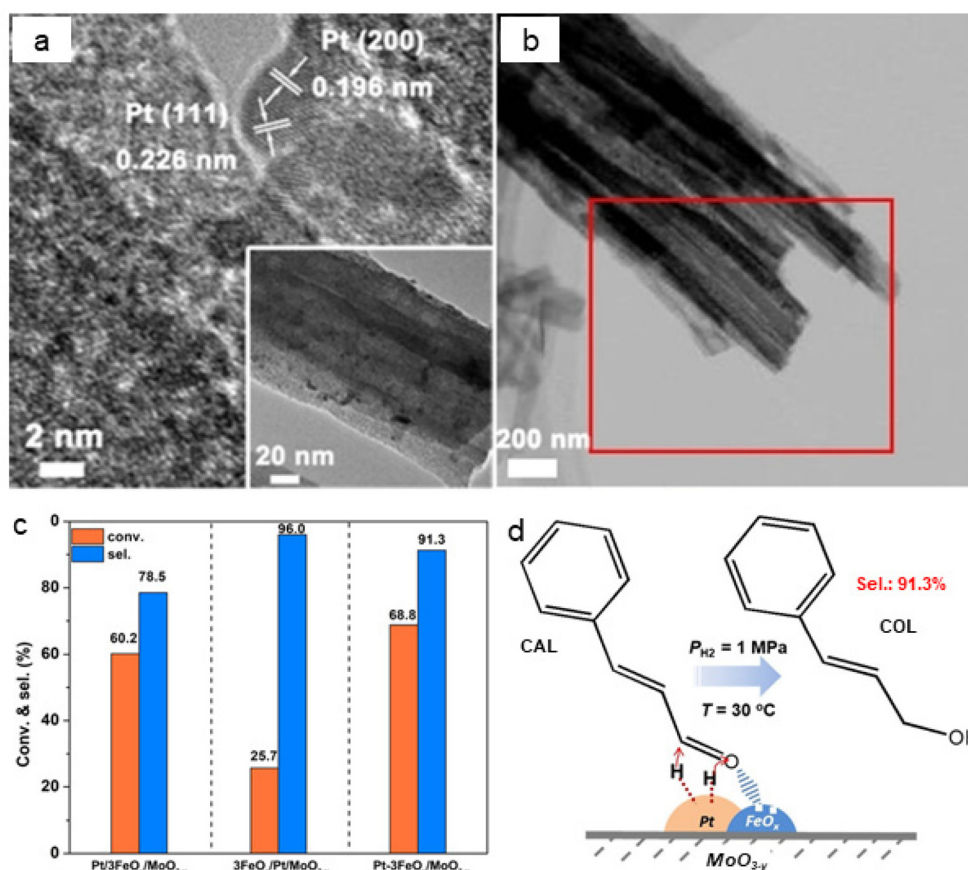
**Fig. 14** (a) TEM image of Pt30Fe30; (b) HR-TEM image of Pt30Fe30, and (c) Selectivity of cinnamyl alcohol. Reproduced with permission from ref. 158 Copyright 2017, Elsevier.

FeW<sub>(x)</sub>. Though redundant WO<sub>x</sub> addition was contrary to the reaction performance and presumably shields the acid sites due to big quantity of tungsten oxide moiety, the best performance of FeW<sub>(5)</sub> catalysts were ascribed to its largest BET surface area, amount of surface adsorbed oxygen molecules, Brønsted acidity and quantity of weak acid sites thus enabling the SCR reaction. Overall, the study offers promising alternatives to substitute the conventional vanadium related catalysts by FeW<sub>(x)</sub> type catalysts for the control of NO<sub>x</sub> emission.<sup>173</sup>

Iron oxide/silver (Fe<sub>x</sub>O<sub>y</sub>/Ag) nanocomposite was synthesized by a single step process using goethite ( $\alpha$ -FeOOH) rods as support.<sup>174</sup> First, FeOOH was treated with sodium citrate followed by attachment of Ag *via* electrostatic interaction. Afterwards, Ag ions were reduced by NaBH<sub>4</sub> to generate Ag NPs on the goethite rods surface (Fig. 20a).<sup>174</sup> The structural configuration of the composite material was characterized by SEM and TEM images as depicted in Fig. 20; Ag NPs with size of 10–50 nm appears to be well-coated over surface of FeOOH nanorod indicating the high quality Fe<sub>x</sub>O<sub>y</sub>/Ag nanocomposite

(Fig. 20b and c). The SAED pattern confirms the presence of spots because of Ag, Fe<sub>21.333</sub>O<sub>32</sub> and FeOOH (see inset in Fig. 20d). The FeOOH layers Fe<sub>21.333</sub>O<sub>32</sub> and crystalline lattices can be seen in HRTEM attributed to (111) phase ( $d = 0.235$  nm) of Ag (Fig. 20e).<sup>174</sup>

The as-synthesized and well characterized Fe<sub>x</sub>O<sub>y</sub>/Ag nanocomposite bearing varying contents of Ag were then studied for hydrogenation of nitroaromatic molecules and decomposition of organic dyes utilizing NaBH<sub>4</sub> as a reductant; two nitroaromatic molecules, namely *p*-nitro aniline and *p*-nitrophenol were reduced completely in few minutes as illustrated by instant decolorization of yellowish green solution. The good catalytic activities of Fe<sub>x</sub>O<sub>y</sub>/Ag nanocomposite were attributed to the incorporated Fe<sub>x</sub>O<sub>y</sub> components wherein rapid electron transfer between BH<sub>4</sub><sup>−</sup> ions and *p*-nitrophenol compound occurred not only on the surface of AgNPs but also on the interface between AgNPs and Fe<sub>x</sub>O<sub>y</sub>. Accordingly, Fe<sub>x</sub>O<sub>y</sub> can play important role in catalysis through a synergistic effect, resulting in better catalytic performance.<sup>174</sup>



**Fig. 15** (a) TEM images of Pt-3FeO<sub>x</sub>/MoO<sub>3-y</sub>; (b) HAADF-STEM image of Pt-3FeO<sub>x</sub>/MoO<sub>3-y</sub>; (c) Performance of catalysts for conversion and selectivity, and (d) Mechanism for the hydrogenation of cinnamaldehyde over Pt-3FeO<sub>x</sub>/MoO<sub>3-y</sub> catalyst. Reproduced with permission from ref. 159 Copyright 2018, Wiley-VCH GmbH & Co. KGaA, Weinheim.

### 2.3. Oxidation reactions

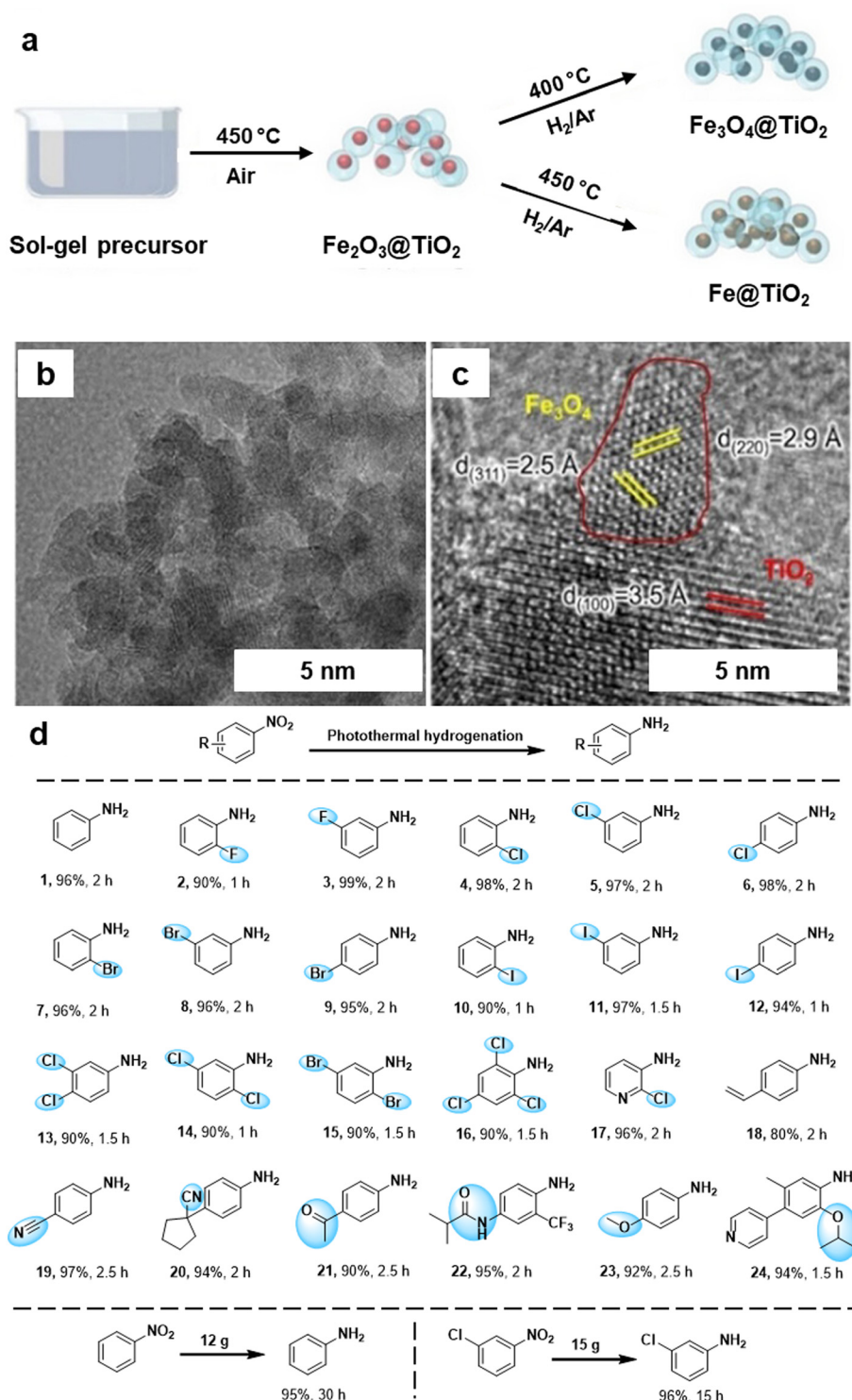
In the context of sustainable chemistry, catalytic oxidation of alcohols, carbonyls, CO, and other oxidizable entities including carbohydrates with molecular oxygen as an environmentally friendly oxidizing agent has garnered immense focus.<sup>175–179</sup> Generally, these protocols are mainly performed on supported noble metal catalysts like Au, Pd, Rh and Ru.<sup>180–186</sup> Since these metal-supported catalysts are expensive, the relatively non-toxic and abundant iron has been considered as a viable alternative as it is inexpensive and the second most easily available metal in the earth's crust.

For the fabrication of ultrafine iron oxides (FeO<sub>x</sub>/MC), mesoporous carbon (MC) support was developed *via* a hard-template route with abundant surface functional groups.<sup>187</sup> First, MC was synthesized through the modulated hard-template technique that encompasses carbonizing an organic-inorganic composite including sugar, citric acid, Al and P ions, and then the removal of on-site formed aluminophosphate template (Fig. 21a). Three different types of MC (pore sizes 6.5, 3.8, and 2.9 nm) were attained by adjusting the amount of citric acid and sugar in composite (abbreviated as MC-1, MC-2 and MC-3) and were deployed as support for the immobiliz-

ation of iron oxides (Fe<sub>2</sub>O<sub>3</sub>). The as-synthesized catalysts were investigated for the selective oxidation of benzyl alcohols to their respective aldehydes (Fig. 21b). Notably, the individual components, Fe<sub>2</sub>O<sub>3</sub> and MC supports, under the same preparative protocols were not active for the oxidation reaction. Under similar reaction parameters, all 5 wt% FeO<sub>x</sub>/MC catalysts with porous structure accomplished the conversions of more than 92% with a wide substrate scope as exemplified by the oxidation of an array of benzyl alcohols to the respective aldehydes with satisfactory yields.

Iron oxide nanoparticles showed their high potential also as the catalyst support for CO oxidation.<sup>188–190</sup> The hydrothermal approach to well-ordered α-Fe<sub>2</sub>O<sub>3</sub> nanoparticles using amino acids as additives were reported,<sup>191</sup> wherein the nature of amino acids regulates the size and shape of the α-Fe<sub>2</sub>O<sub>3</sub> NPs. The spindle shape α-Fe<sub>2</sub>O<sub>3</sub> NPs were obtained, when acidic amino acid was used, whereas basic amino acid afforded rhombohedrally shaped α-Fe<sub>2</sub>O<sub>3</sub> nanoparticles (see Fig. 22). Additionally, gold NPs were immobilized on the surfaces of α-Fe<sub>2</sub>O<sub>3</sub> NPs to assess their catalytic activity for CO oxidation; spindle shaped Au/α-Fe<sub>2</sub>O<sub>3</sub> displayed superior performance relative to the rhombohedral Fe<sub>2</sub>O<sub>3</sub>. Along with the morphological impact, particle size of α-Fe<sub>2</sub>O<sub>3</sub> play an integral role in CO oxidation; larger

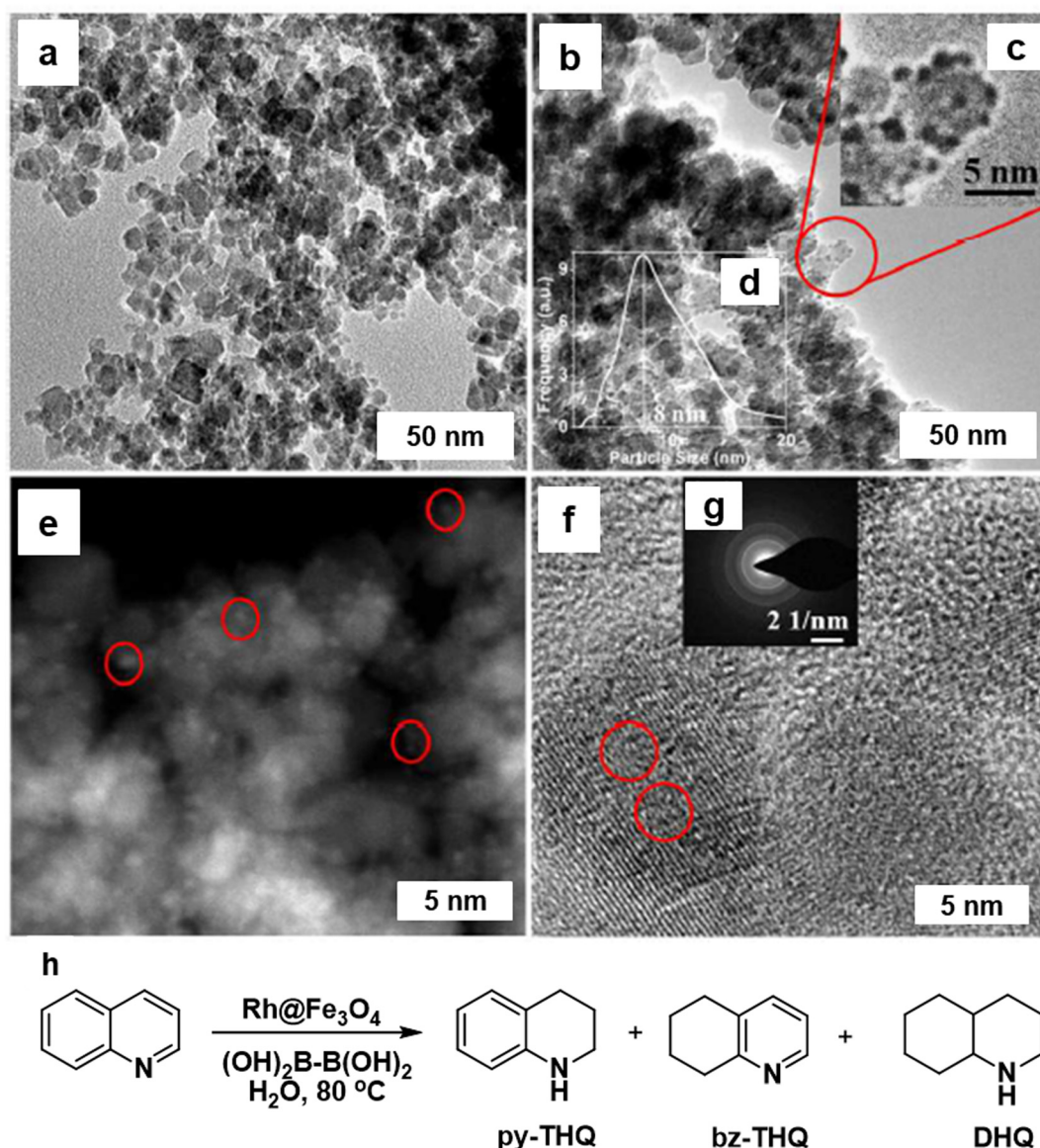




**Fig. 16** (a) Synthetic scheme for  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  and  $\text{Fe@TiO}_2$ ; (b, c) TEM and HR-TEM images of the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  catalyst; (d) Application of the  $\text{Fe}_3\text{O}_4@\text{TiO}_2$  catalyst for photothermal hydrogenation of various nitroaromatics. Reused with permission from ref. 164 Copyright 2024, American Chemical Society.

spindle  $\alpha\text{-Fe}_2\text{O}_3$  support caused excellent performance compared to smaller counterparts whereas in case of rhombohedral  $\text{Au}/\alpha\text{-Fe}_2\text{O}_3$ , medium-sized  $\alpha\text{-Fe}_2\text{O}_3$  nanocrystals displayed the maximum catalytic performance for CO oxidation.

The catalytic performance of hematite concave nanocubes for low temperature CO oxidation was also explored.<sup>192</sup> These nanocubes with high index and facets were fabricated by hydrothermal process employing kinetically controlled growth



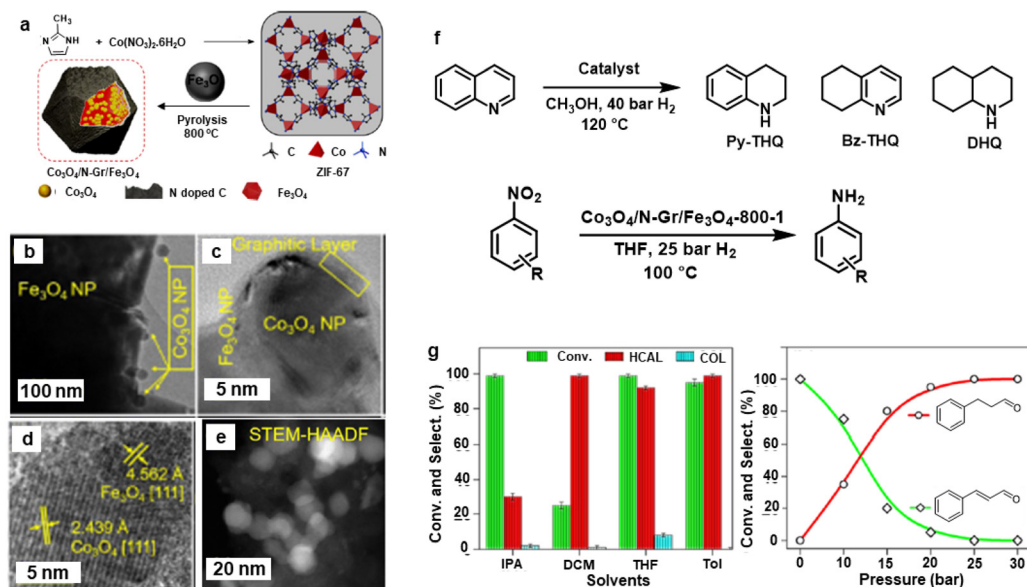
**Fig. 17** TEM images of (a) Fe<sub>3</sub>O<sub>4</sub>; and (b) Rh@Fe<sub>3</sub>O<sub>4</sub>; (e) STEM image of Rh@Fe<sub>3</sub>O<sub>4</sub> particles; (f) HRTEM image of Rh@Fe<sub>3</sub>O<sub>4</sub>; (h) Rh@Fe<sub>3</sub>O<sub>4</sub>-mediated hydrogenation of quinoline using THDB. Reproduced with permission from ref. 168 Copyright 2018, The Royal Society of Chemistry.

approach. To investigate the details of morphological development of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> concave nanocubes, time-dependent experiments were performed (see Fig. 23). Among the different catalysts, highly stable  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanocubes unveiled superior catalytic performance for CO oxidation.

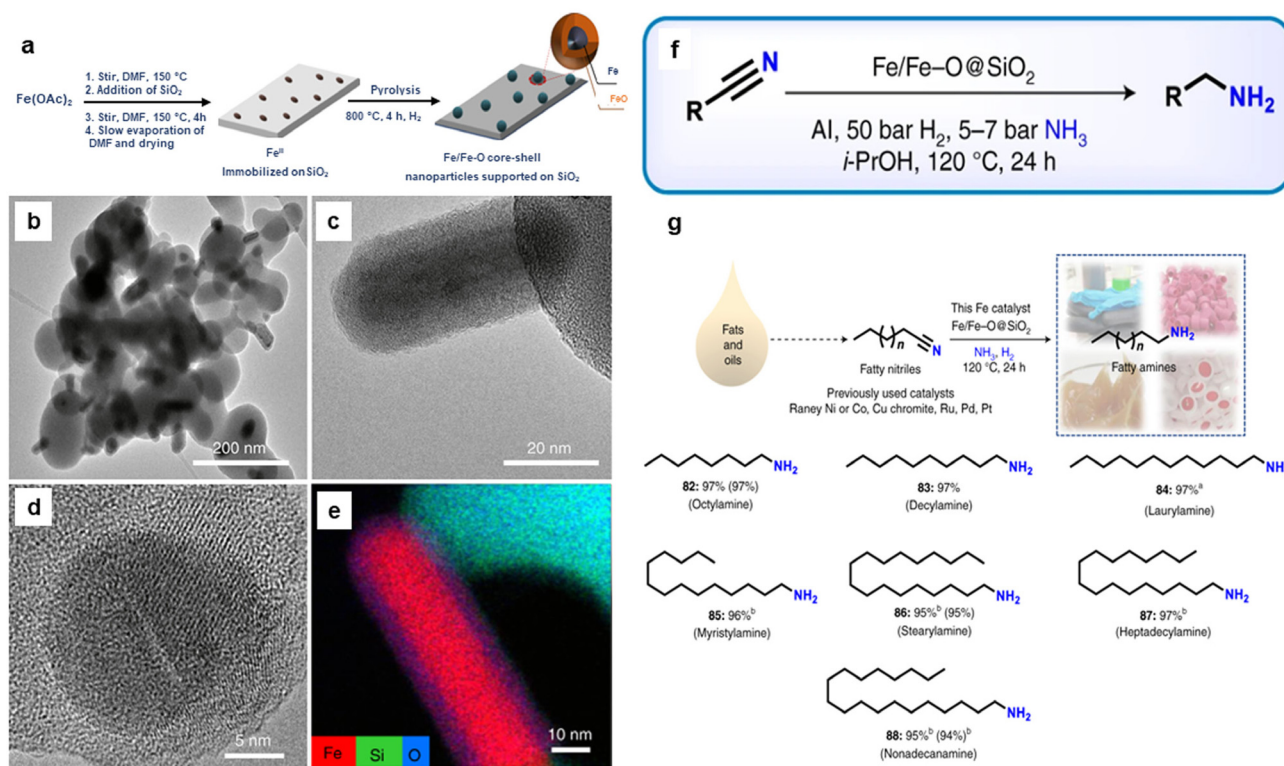
The synthesis of hematite ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>) and Pd-doped  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs *via* a surfactant-free hydrolysis approach has been reported.<sup>193</sup> Rod-like iron oxide NPs were yielded through hydrolysis of iron(III) chloride with diluted hydrochloric acid at 100 °C; further addition of citric acid in the mixture containing iron oxide NPs and (Pd (CH<sub>3</sub>CN)<sub>2</sub>Cl<sub>2</sub>), afforded Pd/iron oxide nanocomposites (see Fig. 24). This attractive protocol avoided the use of surfactant, template and higher temperatures culminating in good shape/size selectivity as well. A rod-like iron oxide/Pd nanocomposite displayed high catalytic per-

formance at low-temperature for CO oxidation as compared to usage of sole  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>.<sup>193</sup> Pd NPs displayed an important role in low-temperature catalytic CO oxidation and catalytic performance was associated with the facile absorption of (i) oxygen on the reduced sites of the support (Fe<sup>2+</sup>) and (ii) CO adsorbed on Pd@Fe<sub>2</sub>O<sub>3</sub> interface.

Oxidation of alcohol using heterogeneous catalyst is a crucial process in the production of high-value fine chemicals.<sup>194–196</sup> Iron oxide NPs were successfully used also for catalytic oxidation of alcohol.<sup>197,198</sup> Platinum nanowires (NWs) decorated on iron oxide (Pt@Fe<sub>2</sub>O<sub>3</sub>) were synthesized *via* the oxidation of FePt NWs in oleylamine and the resulting catalyst were examined for the oxidation of alcohols and alkenes.<sup>199</sup> For the styrene derivatives, molecular oxygen was employed as an oxidizing agent to obtain benzaldehyde in an



**Fig. 18** (a) Schematic for the synthesis of Co<sub>3</sub>O<sub>4</sub>/N-Gr/Fe<sub>3</sub>O<sub>4</sub> nanocomposite; (b, c) TEM; (d) HR-TEM; (e) HAADF-STEM images of Co<sub>3</sub>O<sub>4</sub>/N-Gr/Fe<sub>3</sub>O<sub>4</sub>-800-1 nanocomposite; (f) Schemes for hydrogenation of quinoline and nitroarenes, and (g) Effect of solvents and pressure on hydrogenation of cinnamaldehyde. Reproduced with permission from ref. 169 Copyright 2021, American Chemical Society.

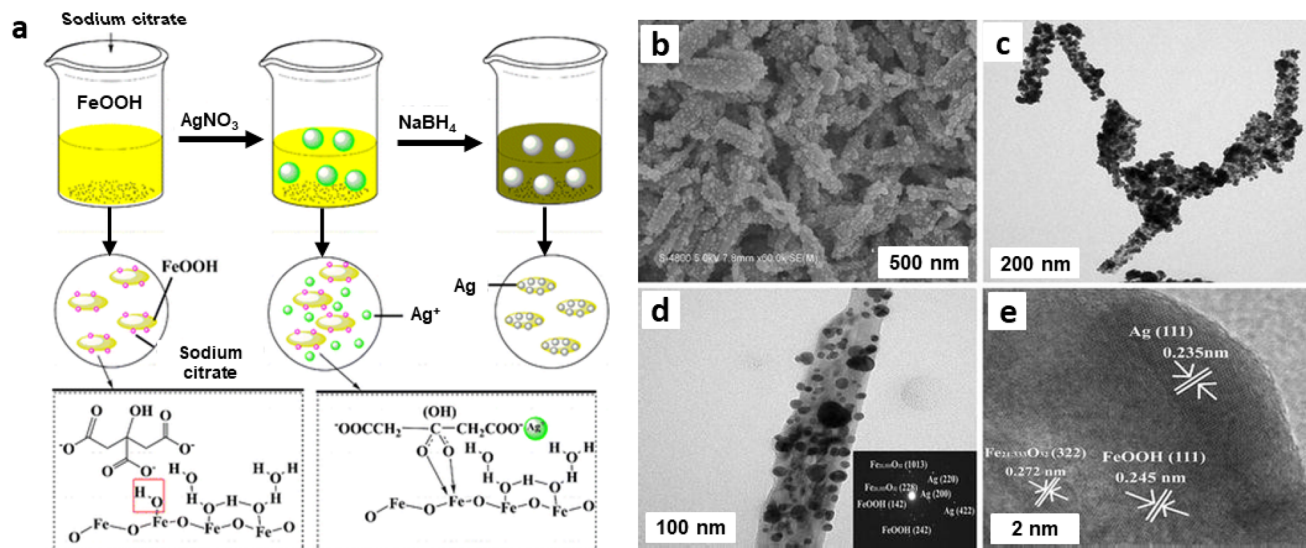


**Fig. 19** (a) Schematic representation for the preparation of Fe/Fe-O core-shell NPs; (b, c) TEM; (d) HR-TEM images of Fe(OAc)<sub>2</sub>-SiO<sub>2</sub>-800; (e) Elemental mapping image of Fe, Si and O; (f) Application of the catalyst for the various nitrile hydrogenation; and (g) Reduction of fatty nitriles. Reproduced with permission from ref. 170 Copyright 2021, Springer Nature.

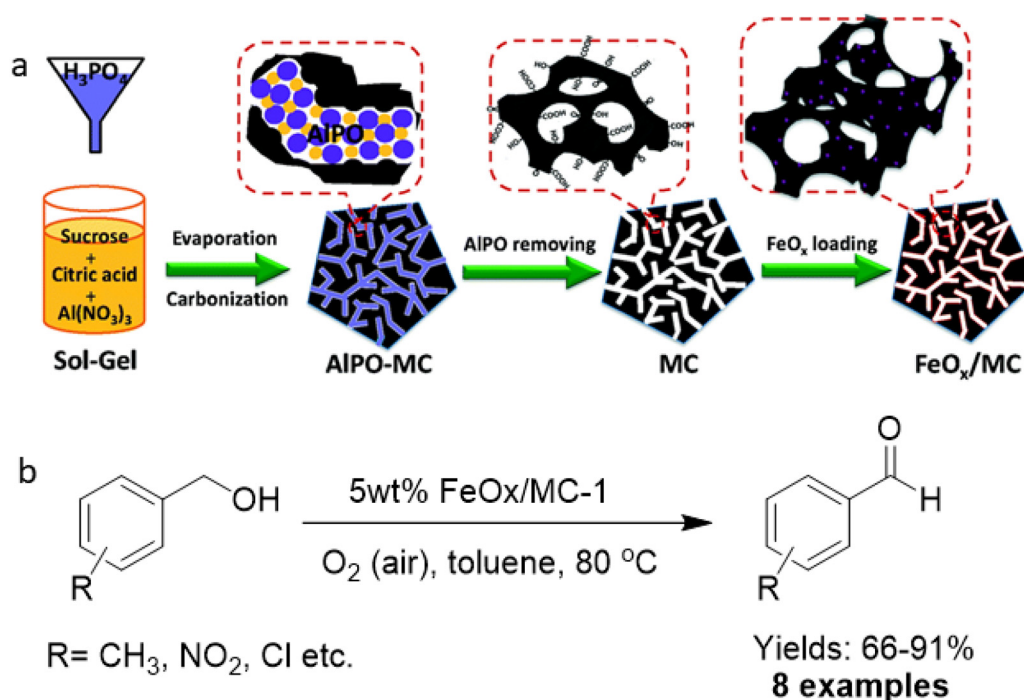
absolute yield of 31%; however, when tBuOOH was used as the sole oxidant for alcohol oxidation, higher yields (more than 80%) of carbonyl compounds could be obtained (Fig. 25).

The lengths of PtFe<sub>x</sub> NWs were several micrometers with diameters of ~1.9 nm (see Fig. 26a and b). After the catalytic oxidation reaction, the diameters got enlarged to ~2.8 nm (see





**Fig. 20** (a) Schematic diagram of the preparation of  $\text{Fe}_x\text{O}_y/\text{Ag}$  nanocomposite;  $\text{Fe}_x\text{O}_y/\text{Ag}$  nanocomposite: SEM image (b), TEM images (c, d) (inset: SAED), (e) HRTEM image. Reproduced with permission from ref. 174 Copyright 2016, Springer Nature.



**Fig. 21** (a) Schematic diagram for the preparation of MC and  $\text{FeO}_x/\text{MC}$  catalysts; (b) Oxidation of alcohols with 5 wt%  $\text{FeO}_x/\text{MC}$ -1. Reproduced with permission from ref. 187 Copyright 2015, The Royal Society of Chemistry.

Fig. 26c and d) and the Fe in the catalyst was oxidized to  $\text{Fe}_2\text{O}_3$  via the Kirkendall effect. This unsupported PtFe NWs catalyst was identified as more efficient catalyst relative to other reported  $\text{Fe}_2\text{O}_3$  NPs and was reusable many times with negligible loss of catalytic performance.

The application of iron oxide NPs has been also investigated for the oxidative dehydrogenation reaction (ODR).<sup>200,201</sup>

ODR is an important transformation in the chemicals reactions to produce olefins which are vital raw materials for variety of industrially important compounds, including polymers, fibers and their analogues.<sup>202,203</sup> In this context, Ondruschka and co-workers<sup>204</sup> performed oxidative dehydrogenation of ethylbenzene on iron oxide containing multi-walled carbon nanotubes (MWCNTs) in an integral fixed-bed

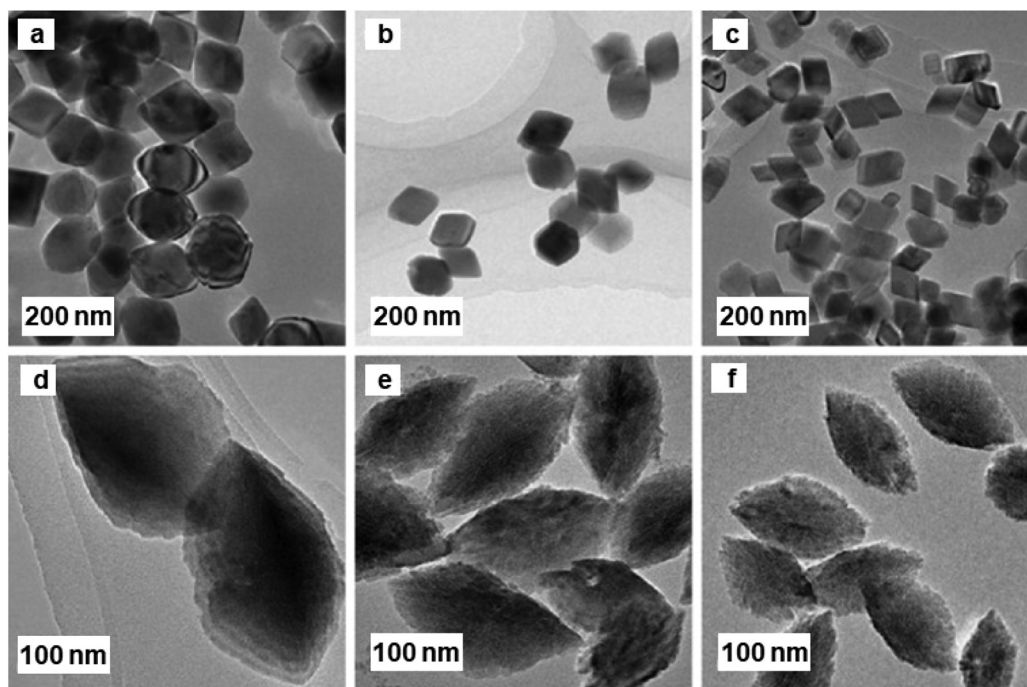


Fig. 22 TEM images of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs. Samples (a–c) prepared with [Fe<sup>3+</sup>]/[L-lysine] molar ratios; samples (d–f), prepared with [Fe<sup>3+</sup>]/[D-asparagine] molar ratios. Reproduced with permission from ref. 191 Copyright 2009, Elsevier.

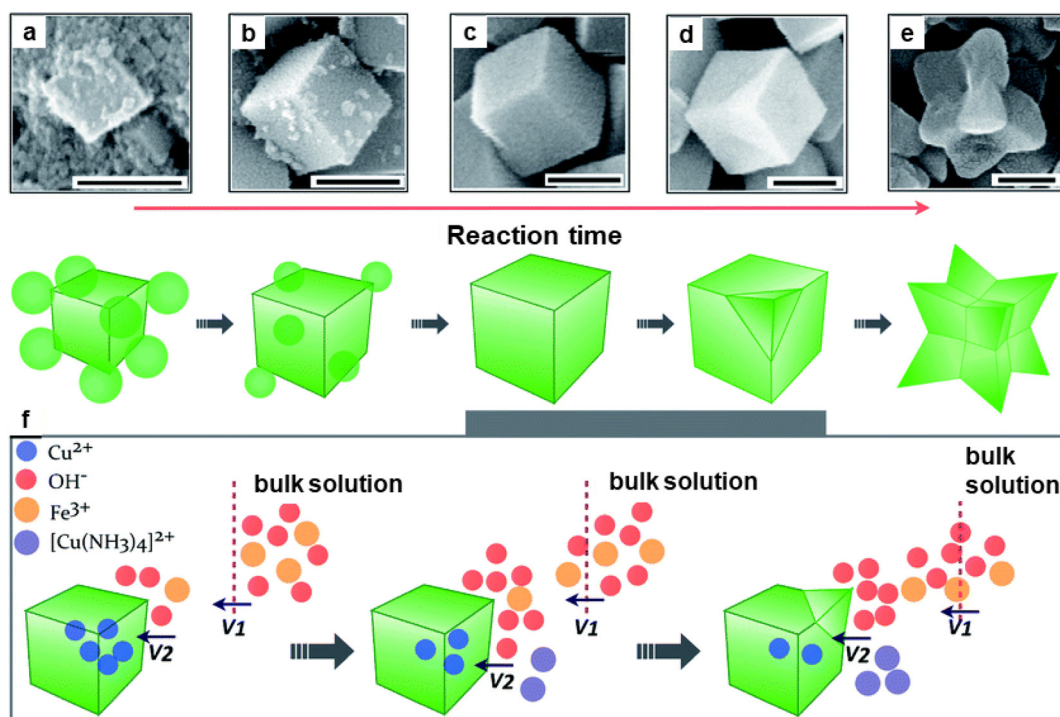
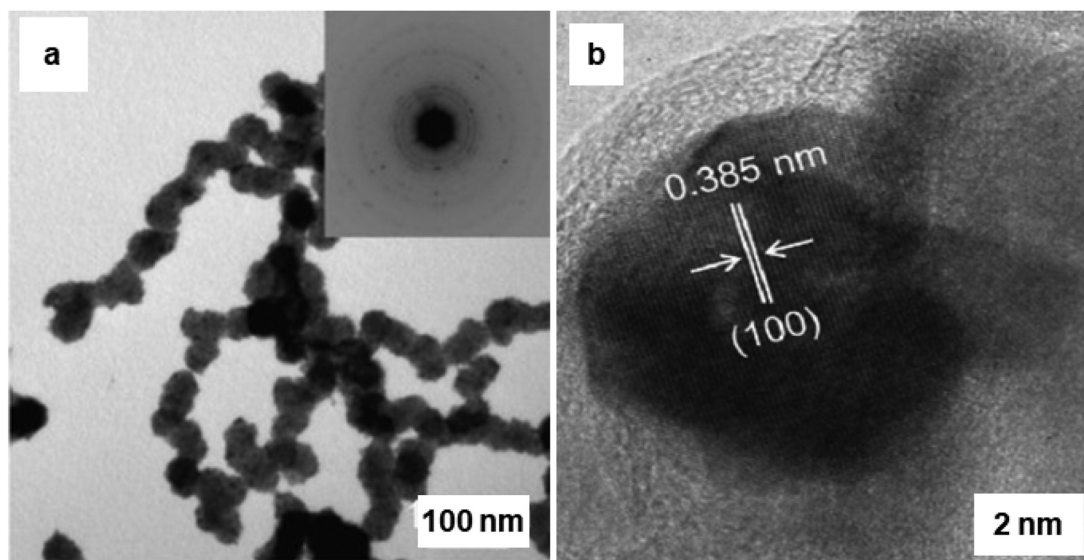
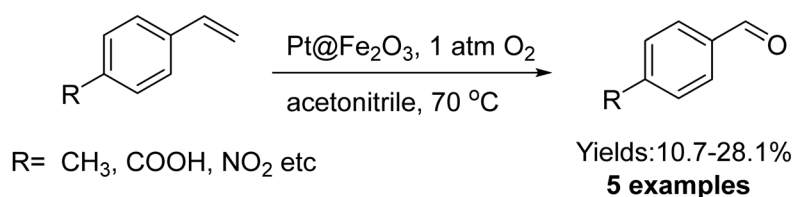


Fig. 23 SEM images (a–e) of the nanocrystals collected at different reaction times at 200 nm; (f) Schematic illustration of the kinetically controlled overgrowth of concave nanocubes developed from pseudonanocubes. Reproduced with permission from ref. 192 Copyright 2014, The Royal Society of Chemistry.

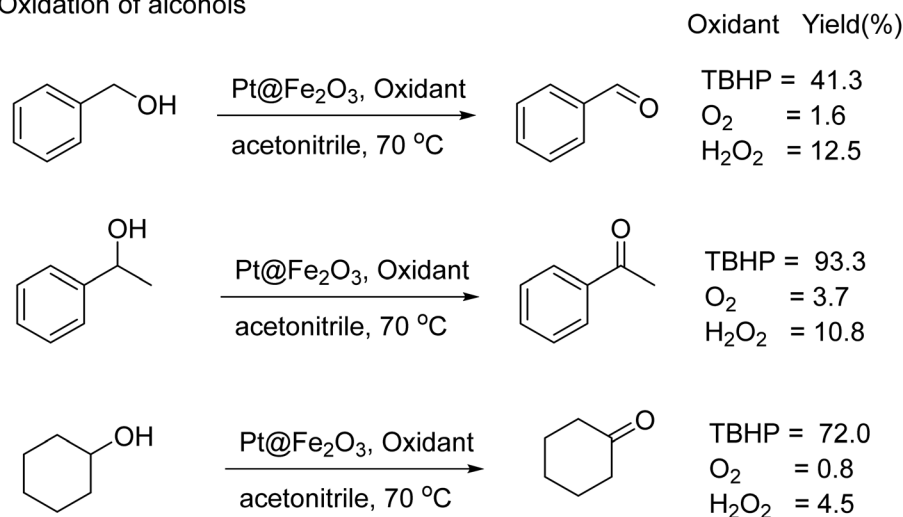


**Fig. 24** (a) TEM images and the corresponding SAED patterns of Pd doped  $\alpha$ - $\text{Fe}_2\text{O}_3$  rod-like particles; (b) HRTEM image of Pd@ $\text{Fe}_2\text{O}_3$ , where the lattice spacing  $\sim 0.385$  nm, which corresponds to Pd planes. Reproduced with permission from ref. 193 Copyright 2009, Elsevier.

(a) Oxidation of styrene



(b) Oxidation of alcohols

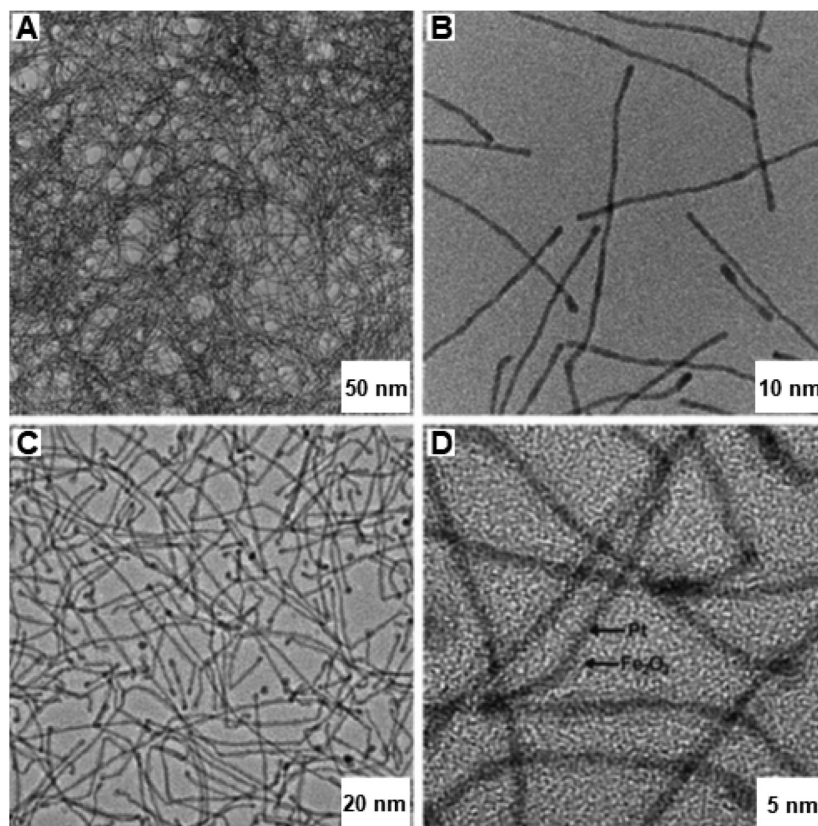


**Fig. 25** (a) Oxidation of styrene and (b) alcohols catalyzed by Pt@ $\text{Fe}_2\text{O}_3$ . Reproduced with permission from ref. 199 Copyright 2011, Wiley-VCH GmbH & Co. KGaA, Weinheim.

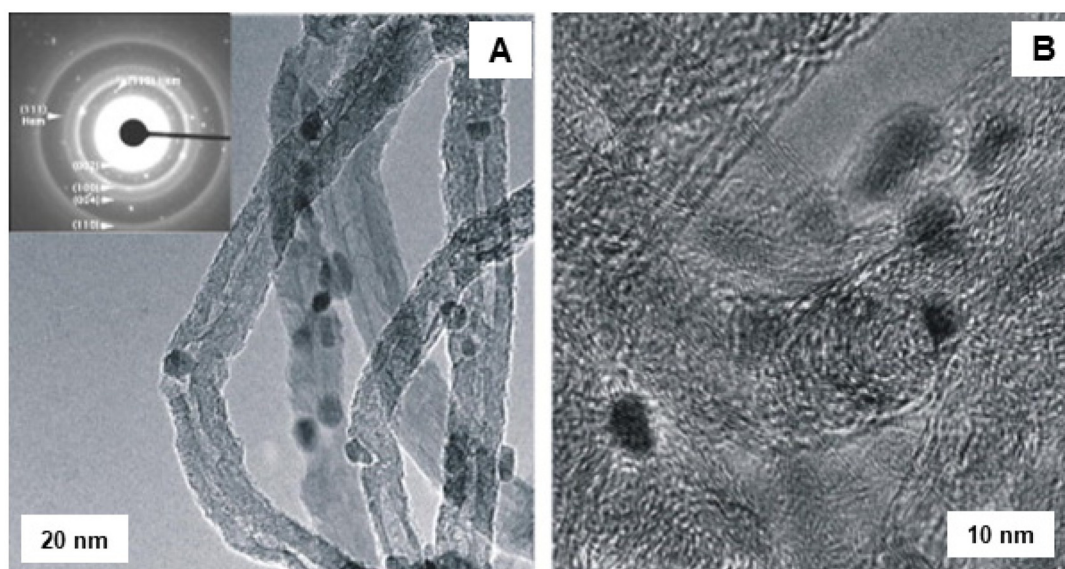
container using conventional heating and microwave (MW)-assisted methods. The SAED pattern confirmed the presence of hematite nanoparticles, which were arbitrarily found on the external surface of the MWCNTs (see Fig. 27). It has been

observed that 3 wt% of iron oxide-MWCNTs was found to be the ideal catalyst for ethylbenzene conversion and selectivity of styrene, while all others were found to be more selective at 380–450 °C under operation in a MW field. The sample dis-





**Fig. 26** TEM and HR-TEM images of (A, B) PtFe NWs and after catalysis (C, D) Pt@Fe<sub>2</sub>O<sub>3</sub> NWs. Reproduced with permission from ref. 199 Copyright 2011, Wiley-VCH GmbH & Co. KGaA, Weinheim.



**Fig. 27** TEM images of fresh Fe<sub>2</sub>O<sub>3</sub> modified MWCNTs: (A) LR image with SAED pattern; (B) HR-TEM image. Reproduced with permission from ref. 204 Copyright 2008, Elsevier.

played excellent styrene selectivity under MW irradiation than the ones achieved by traditional heating under the identical reaction parameters.

However, the influence of lanthanum (La), neodymium (Nd), zirconium (Zr), and aluminium (Al) on the structural properties of hematite and on its catalytic performance for the

dehydrogenation of ethylbenzene has been studied;<sup>205</sup> all dopants helped to enhance the specific surface area of the fresh and recycled catalysts thus rendering them more resistant against reduction. As the specific surface area rises, the area-dependent catalytic activity of hematite also increases except in the case of aluminum which essentially performed only as a textural agent. Notably, zirconium and lanthanum were the main dopants which decreased the selectivity of the catalytic processes, whereas other dopants did not affect the activity.

The iron-oxide NPs were synthesized within the macroporous resins through hydrolysis of  $\text{Fe}^{3+}$  ions, which were chemically adsorbed at the pore walls;<sup>206</sup> the phase of the ensuing spherical iron oxide particles (2–5 nm) inserted in resin was identified as  $\beta\text{-FeOOH}$ . They were employed for the hydroxylation of phenol with  $\text{H}_2\text{O}_2$  measured at 50% of conversion, when excellent catalytic activity for phenol hydroxylation was observed because of nanosized  $\beta\text{-FeOOH}$  particles within resins and exhibiting minimal aggregation.

The gold catalyst anchored on iron oxide nanoparticles were reported for the oxidation of formaldehyde and CO at low temperature.<sup>207</sup> The catalyst being prepared by the dispersion-precipitation method,<sup>208,209</sup> termed as FeA. For comparison, additional iron oxide support (denoted by FeB) was synthesized through precipitation technique. Both the samples were further decorated with gold nanoparticles and evaluated for the oxidation of formaldehyde and CO.<sup>207</sup> Oxidation of CO was accomplished in a U-tube the reactor cooled in an ice bath containing  $\text{NH}_4\text{Cl}$  and  $\text{NaNO}_3$  to obtain primary temperature of  $-25\text{ }^\circ\text{C}$ . Afterwards the temperature was increased up to  $25\text{--}80\text{ }^\circ\text{C}$  and the initial concentration of CO was maintained by introducing air to keep the concentration 10 000 ppm and the flow rate at  $50\text{ mL min}^{-1}$  with gas hourly velocity (GHSV) of *ca.*  $30\,000\text{ h}^{-1}$ . The HCHO oxidation was achieved by reactant containing 450 ppm HCHO in a 20.8 vol% (O)/79.2 vol% (N) mixture with a total flow rate was set at  $50\text{ mL min}^{-1}$  and product was analysed by GC. The catalytic activity of Au/FeA (2.5) and Au/FeB (2.5) in CO and HCHO oxidation were assessed (Fig. 28c and d). As depicted in Fig. 28c, the conversion of CO reached 89% at a temperature of  $-21\text{ }^\circ\text{C}$ , attaining 100% conversion at  $-3\text{ }^\circ\text{C}$  in case of Au/FeA (2.5), whereas value of only 22% was achieved at  $-21\text{ }^\circ\text{C}$  and the total transformation only accomplished at a temperature of  $23\text{ }^\circ\text{C}$  on Au/FeB (2.5). In the case of oxidation of HCHO, Au/FeA (2.5) also displayed greater performance as compared to Au/FeB (2.5) at ambient temperature where 33% and 23% conversions were achieved, respectively (Fig. 28d). However, the catalyst with 2.5–3.5% loading of Au exhibits greater activity for CO conversion compare to others (see Fig. 28e and f). The superior performance of Au/FeA (2.5) was rationalized by considering higher BET specific surface area of Au/FeA (2.5) ( $99\text{ m}^2\text{ g}^{-1}$ ) than that of Au/FeB (2.5) ( $67\text{ m}^2\text{ g}^{-1}$ ). Further, TEM images of Au/FeA (2.5) showed the existence of smaller particles assumed to be useful for its higher catalytic applicability (Fig. 28a and b).<sup>207</sup>

The iron oxide catalyst has been synthesized by the surface high-temperature synthesis (STS) approach<sup>210</sup> and the ensuing materials were deployed for oxidation of  $\text{H}_2\text{S}$ ; iron oxide was

also synthesized by the traditional method. The STS approach was well established for the generation of well-dispersed particles of active components which in turn showed high catalytic performance.<sup>211,212</sup> The TEM images of  $\text{FeO}_x/\text{GFC}$  glass-fiber catalysts (GFC) and traditionally synthesized  $\text{FeO}_x/\text{Al}_2\text{O}_3$  catalyst are shown in Fig. 29;  $\text{FeO}_x/\text{GFC}$  shows the localized silica through large porous particles, while iron oxide exists mainly as flattened  $\text{Fe}_2\text{O}_3$  islet with 1–2 nm long and a thickness of 0.5–1.0 nm. The conventional catalyst based on iron oxide in alumina is found with particle size (15–30 nm) over the surface of  $\alpha\text{-Al}_2\text{O}_3$  support. It has been affirmed that  $\text{FeO}_x$ -based GFC, synthesized from  $\text{Fe(III)}$  nitrate and glycine by the STS method is more active for selective  $\text{H}_2\text{S}$  oxidation with high conversion (55–60% at  $200\text{ }^\circ\text{C}$ ) than conventional  $\text{Fe}_2\text{O}_3/\text{Al}_2\text{O}_3$  granular catalyst.

The porous silicate supported iron oxide NPs were synthesized by the continuous flow methodology and applied it for the oxidation of benzyl alcohol;<sup>213</sup> synthesis of porous silicates supported iron oxide NPs being illustrated in Fig. 30a. The black stripes on gray silica grains of iron nanoparticles for FeAlSi and FeZrSi samples with 6–12 and 5–27 nm, respectively, were investigated by TEM analysis (Fig. 30b–e). The catalytic activity decreased with increasing iron content as depicted in Fig. 30f. The 51–66% conversion of benzyl alcohol and 69–85% selectivity to benzaldehyde for Fe/Al-SBA-15 catalyst was observed (Fig. 30g). Later, an ultra-small ( $<10\text{ nm}$ ) iron oxide hydroxide nanocatalyst have been synthesized and deployed it for various oxidation reactions like alcohol oxidation, epoxidation of alkenes and organic sulfide oxidation.<sup>214</sup>

Adipic acid plays a fundamental role in the synthesis of polymers, fertilizers, lubricants, and insecticides.<sup>215,216</sup> Recently Raja and coworkers<sup>217</sup> have fabricated the iron and tungsten oxide-incorporated MC sphere (Fe–W–MC) with diverse carbon origins *via in situ* hydrothermal method. The SEM images of 10Fe 90 W–MC FF (for fructose) and 10Fe 90 W–MC GF (for glucose) revealed sphere like morphology (Fig. 31a and b). Notably, 10Fe 90 W–MC FF demonstrated that the carbon spheres produced with fructose was consistently spherical and evenly distributed, exhibiting a homogeneous surface (Fig. 31a). The HR-TEM images of 10Fe 90 W–MC FF (Fig. 31c and d) revealed that the distinctive *d*-spacing values of 0.29 and 0.23 nm, signifying the presence of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_2\text{O}_3$  respectively. Additionally, lattice *d*-spacings of 0.31 nm were identified, corresponding to orthorhombic  $\text{WO}_3$ . This well characterized 10Fe 90 W–MC FF catalyst was employed for the synthesis of adipic acid from cyclohexanone using  $\text{H}_2\text{O}_2$  as an environmentally friendly oxidant under solvent-free conditions with the highest conversion of 93% in 12 h which is more than the traditional process of production of adipic acid from KA (ketone-alcohol) oil.<sup>218</sup>

Heterogeneous mesoporous Fenton nanocatalyst was synthesized using aluminum oxide anchored on iron-oxide as a support ( $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3$ )<sup>219</sup> *via* fabrication by self-assembly pathway (see Fig. 32a). TEM images of  $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3$ -2 core-shell nanoparticles displayed that the self-aggregation of tiny spherical nanocrystals with size of 15–20 nm (see Fig. 32b).

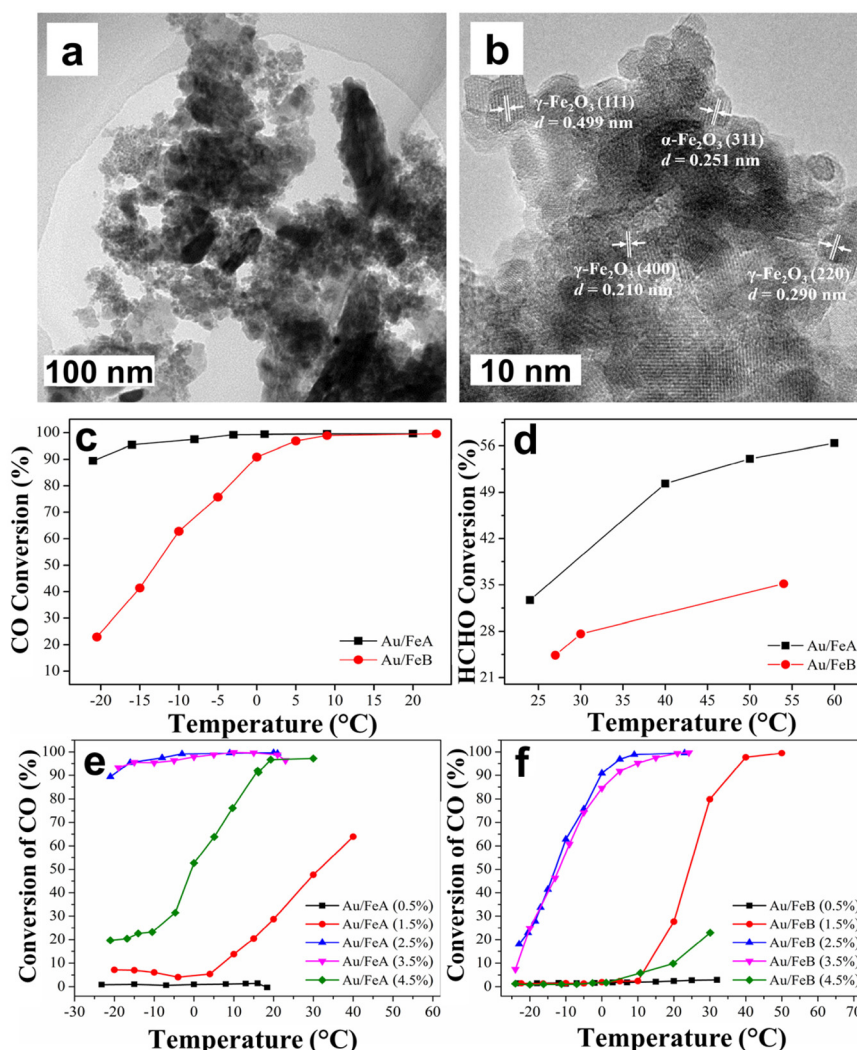


Fig. 28 (a, b) TEM images of Au/FeA; (c, d) CO and HCHO conversion curves over Au/FeA and Au/FeB; (e, f) Effect of Au loading on the conversion of CO. Reproduced with permission from ref. 207 Copyright 2015, Elsevier.

The exterior of the  $\alpha\text{-Fe}_2\text{O}_3$  layer can be distinctly visible with (012) lattice fringes (see Fig. 32c). Furthermore, the Fast Fourier Transformation (FFT) pattern of Fig. 32c was displayed in Fig. 32d, which demonstrated the existence of  $\gamma\text{-Al}_2\text{O}_3$  and  $\alpha\text{-Fe}_2\text{O}_3$ . The diffraction spots observed in the FFT pattern accurately matched and indexed with the crystal structures of  $\gamma\text{-Al}_2\text{O}_3$  (A) and  $\alpha\text{-Fe}_2\text{O}_3$  (F) (see Fig. 32e). The as prepared  $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3\text{-2}$  catalyst has a very high BET surface area of  $385\text{ m}^2\text{ g}^{-1}$  with an average pore size of 3.2 nm. This mesoporous  $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3\text{-2}$  nanocatalyst demonstrated significant catalytic activity in the one-pot transformation of cyclohexanone into adipic acid in a water-based system in presence of  $\text{H}_2\text{O}_2$  as a green oxidant. Recently,  $\text{TiO}_2@\text{Fe}_2\text{O}_3$  catalyst prepared *via* sol-gel method was employed for the cyclohexene oxidation using molecular oxygen achieved an impressive 97% selectivity for adipic acid.<sup>220</sup>

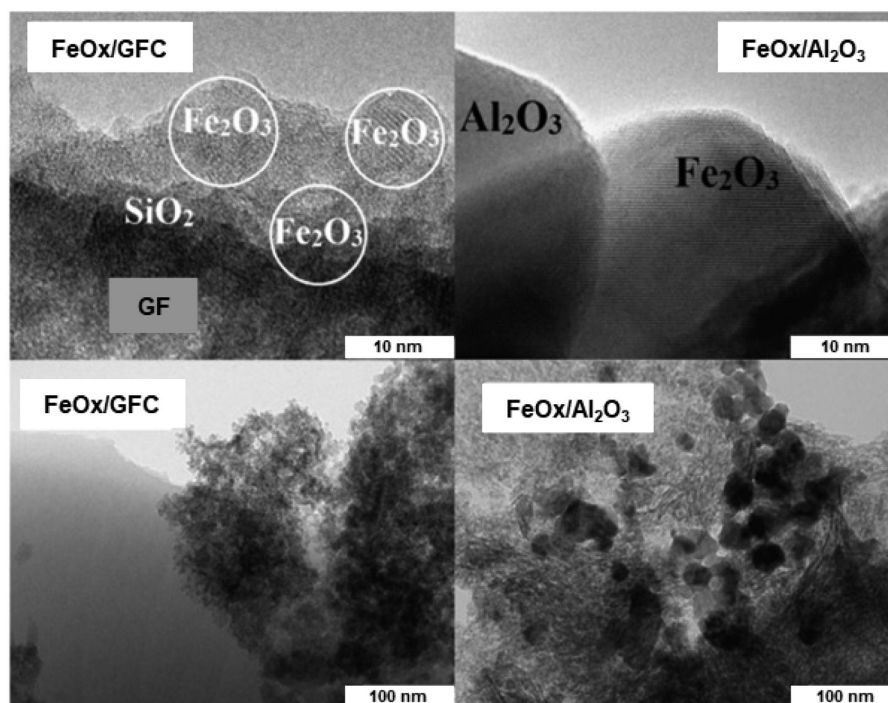
Although oxygen gas is the most cost-effective and easily accessible oxidant, its utilization is limited due to the safety

concerns associated in terms of its handling. Consequently, it is one of the least commonly employed reagents in chemical processes.<sup>221,222</sup> By considering up-to-date research findings on this issue, pure oxygen can be safely utilized on a large scale in continuous-flow reactors for liquid-phase aerobic oxidations. Moreover, this approach offers significant advantages in terms of synthetic outcomes and manufacturing efficiencies. The pharmaceutical industry can draw valuable insights from the established protocols in the bulk chemicals sector for handling aerobic oxidation processes. For successful implementation of large-scale molecular oxygen processes, it is imperative to foster collaboration among process chemists, chemical engineers, and process safety experts.<sup>223</sup>

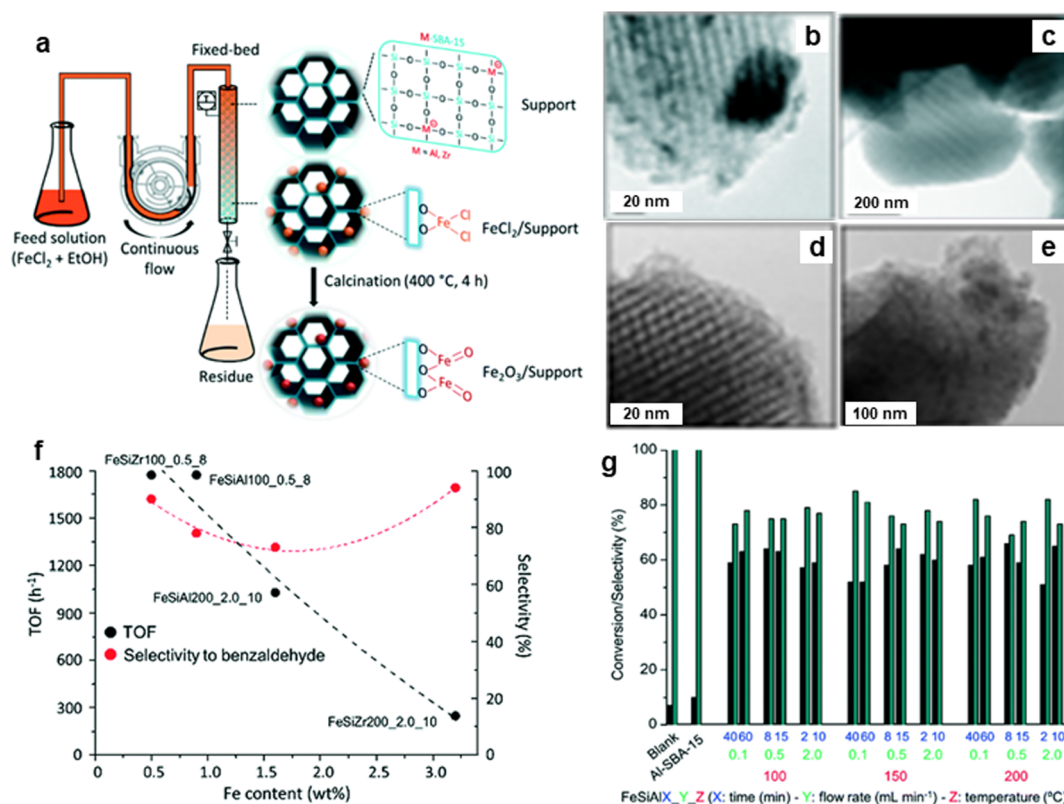
#### 2.4. Alkylation reactions

Friedel-Crafts alkylation reactions are universally known for the synthesis of the industrially significant organic compounds. *e.g.*, alkylation of benzene with benzyl chloride (BC)

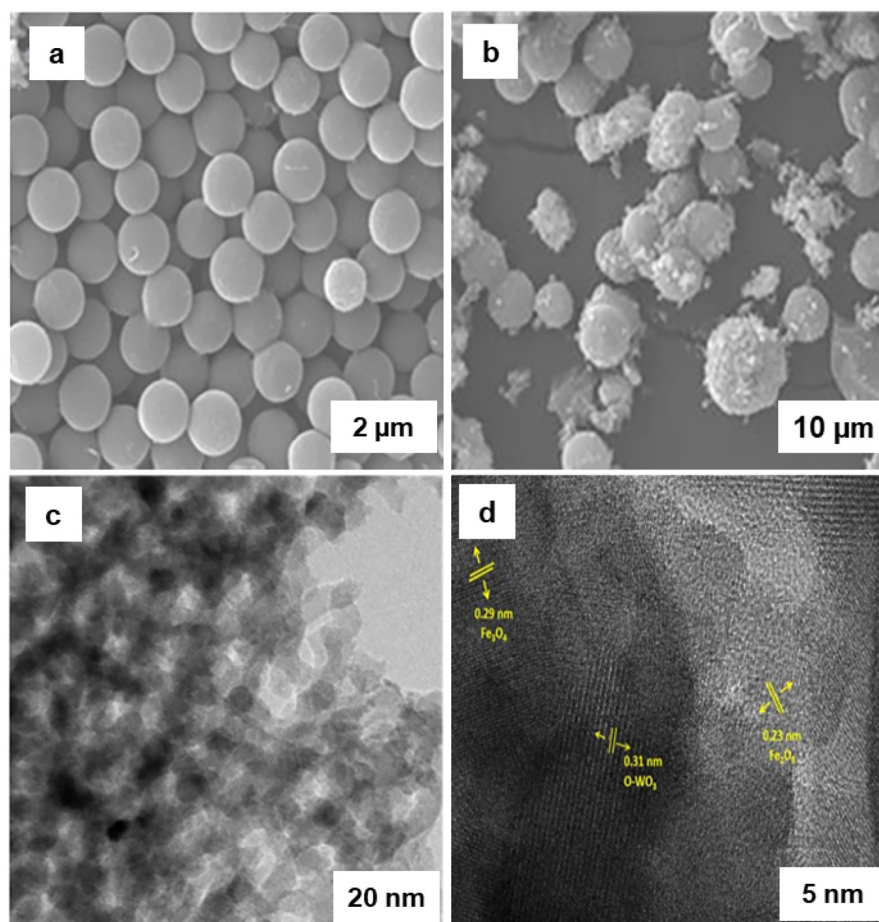




**Fig. 29** TEM images of the  $\text{FeO}_x/\text{GFC}$  (left) and conventional  $\text{FeO}_x/\text{Al}_2\text{O}_3$  catalyst (right). Reproduced with permission from ref. 210 Copyright 2016, Elsevier.



**Fig. 30** (a) Schematic for continuous flow synthesis of  $\text{Fe}_2\text{O}_3$  NPs; (b–e) TEM images of  $\text{FeAlSi150}_{0.1_{40}}$ ,  $\text{FeZrSi150}_{0.1_{40}}$ ,  $\text{FeSiAl200}_{0.1_{40}}$  and  $\text{FeZrSi200}_{0.1_{40}}$  catalysts respectively, (f) Effect of Fe loading on TOF and selectivity, and (g) Performance of catalysts on conversion and selectivity. Reproduced with permission from ref. 213 Copyright 2018, The Royal Society of Chemistry.



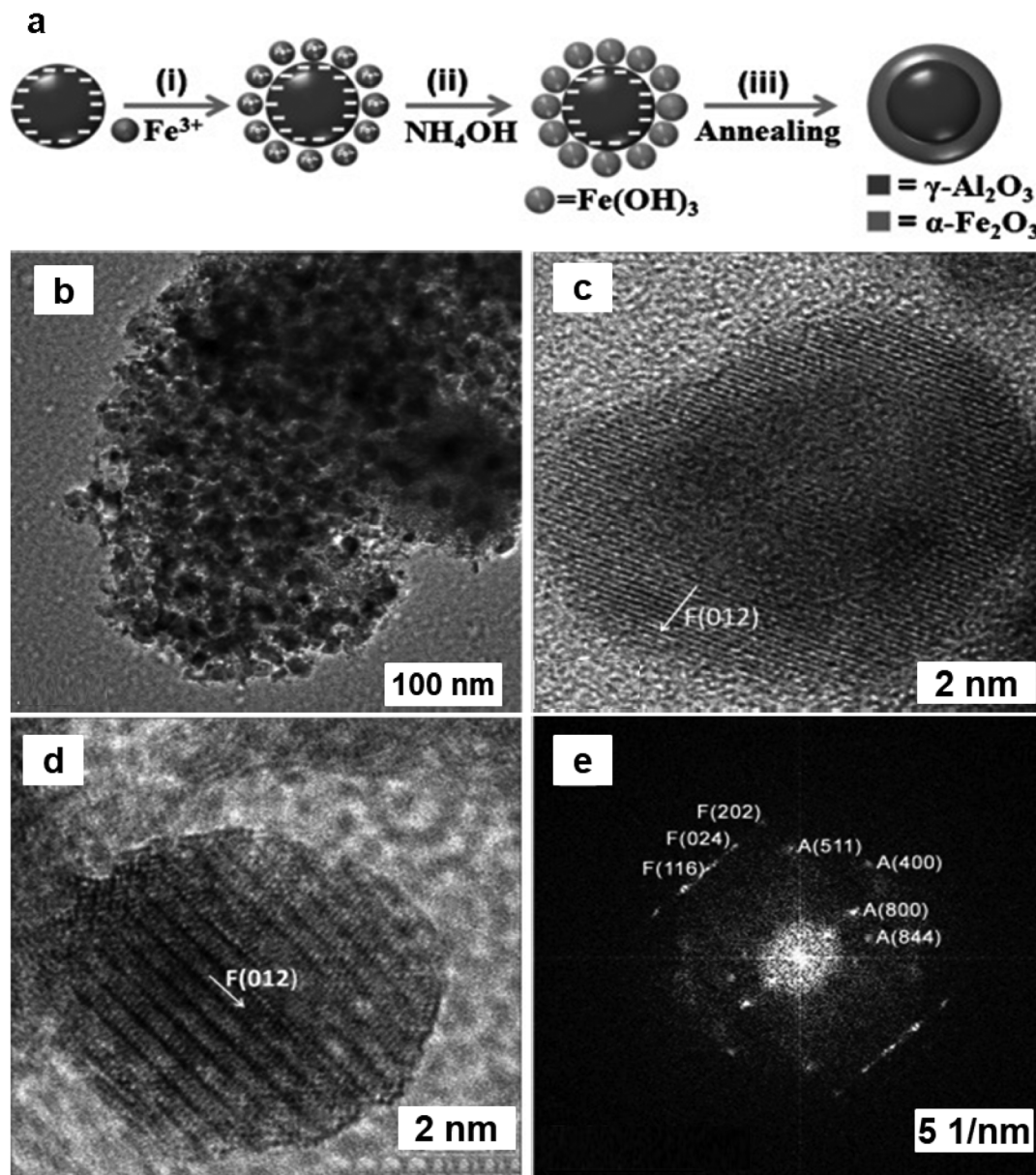
**Fig. 31** (a, b) SEM Images of 10Fe 90 W-FF and 10Fe 90 W-GF respectively; (c, d) HR-TEM images of 10Fe 90 W-FF. Reused with permission from ref. 217 Copyright 2022, Elsevier.

enables routes to benzylbenzene,<sup>224–226</sup> whose derivatives serve as essential scaffolds for pharmaceuticals and fine chemicals.<sup>227,228</sup> In this chemical reaction, iron oxide NPs exhibits an influential role.

In this regard, a Fe/SBA-15/carbon materials ( $\text{Fe}_2\text{O}_3$ -SBA-15 and Fe-carbon) prepared by chemical vapor infiltration (CVI) process utilizing ferrocene as source of Fe and carbon raw materials.<sup>229</sup> These  $\text{Fe}_2\text{O}_3$  NPs, anchored on SBA-15 silica or metallic Fe consistently introduced in MC, were prepared by selective oxidation of the carbon constituent in air or by eliminating the silica template, respectively. Two sets of catalysts were prepared namely  $\text{Fe}_2\text{O}_3$ /SBA-15-*t* and Fe/carbon-*t* (where *t* represents minute), *via* two different processes.  $\text{Fe}_2\text{O}_3$ /SBA-15-*t* catalyst were obtained *via* calcination of the Fe/SBA-15/carbon composites at 500 °C in an aerobic atmosphere for 3 h to eliminate the carbon precursor with concurrent formation of  $\text{Fe}_2\text{O}_3$  from Fe species. On the other hand, the Fe/carbon-*t* were prepared by calcination of the Fe/SBA-15/carbon materials at 800 °C in Ar for 2 h.<sup>229</sup> Fig. 33 depicts the TEM of different  $\text{Fe}_2\text{O}_3$ /SBA-15-*t* composites, where the catalyst synthesized at *t* = 20 min showed a fairly uniform distribution of  $\text{Fe}_2\text{O}_3$  NPs with ~2 nm (loading 21–22 wt%) in the mesoporous channels

of SBA-15.  $\text{Fe}_2\text{O}_3$ -15-40 form small aggregates and  $\text{Fe}_2\text{O}_3$  nanoparticles in  $\text{Fe}_2\text{O}_3$ /SBA-15-60 show lattice fringes of 0.275 nm (see Fig. 33b and c, inset), confirming the hexagonal hematite phase.  $\text{Fe}_2\text{O}_3$ -15-40 displayed excellent catalytic activity and selectivity for the benzene alkylation with BC. Importantly,  $\text{Fe}_2\text{O}_3$ /SBA-15 offered high selectivity and its catalytic performance was extremely sensitive to the reaction temperature. Both  $\text{Fe}_2\text{O}_3$ /SBA-15-20 and  $\text{Fe}_2\text{O}_3$ /SBA-15-40 catalysts exhibited good BC conversion (94%) within 5 and 10 min, respectively. The catalyst  $\text{Fe}_2\text{O}_3$ /SBA-15-40 synthesized by impregnation technique with the same  $\text{Fe}_2\text{O}_3$  loading (denoted a  $\text{Fe}_2\text{O}_3$ /SBA-15-40-im) showed a much less conversion compared to the  $\text{Fe}_2\text{O}_3$ /SBA-15-40 catalyst.

For the purposes of Friedel-Crafts acylation, the  $\alpha$ - $\text{Fe}_2\text{O}_3$  NPs (30 nm) were synthesized employing superabsorbent nanopolymer (SANP) *via* thermal treatment.<sup>230</sup> The salient feature of this approach has been to use salep-*g*-poly acrylic acid (salep-*g*-PAA) as a less expensive and easily accessible coating material which possesses -OH and -COOH functional groups to increase the binding affinity to metal ions as well as to manage the size and structure of  $\alpha$ - $\text{Fe}_2\text{O}_3$  excluding formation of clusters.<sup>231,232</sup> A variety of aromatic ketones were



**Fig. 32** (a) Schematic synthesis of  $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3$  mesoporous core-shell catalyst; (b–d) TEM images of  $\text{Al}_2\text{O}_3@\text{Fe}_2\text{O}_3$ -2; (e) Crystal structures of  $\gamma\text{-Al}_2\text{O}_3$  (A) and  $\alpha\text{-Fe}_2\text{O}_3$  (F). Reproduced with permission from ref. 219 Copyright 2013, Wiley-VCH GmbH & Co. KGaA, Weinheim.

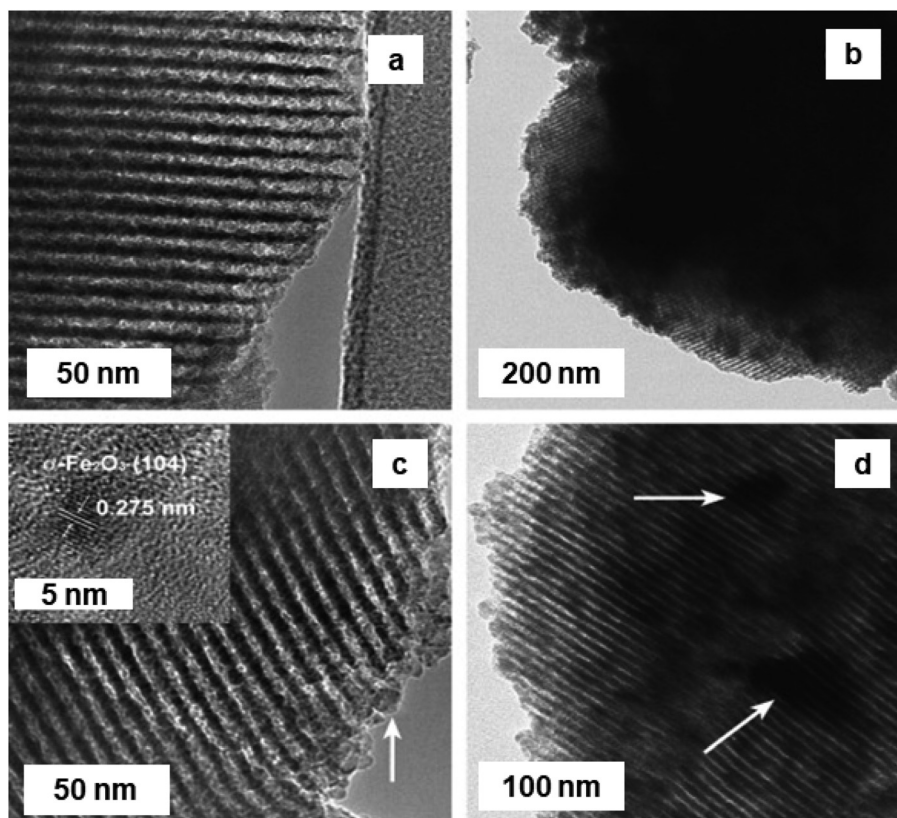
formed in moderate to good yields (71–94%) with low mol% of the catalyst (1 mol%) in 1 h (see Fig. 34). Further, catalytic performance of  $\alpha\text{-Fe}_2\text{O}_3$  NPs was explored for Friedel–Crafts acylation reaction with *p*-methyltoluene and benzyl bromide afforded product with good yield (87%).

Preparation of iron oxide NPs using a hydrothermal protocol has been reported for alkylation of benzene with BC to generate diphenylmethanes.<sup>233</sup> The benzylation of benzene with BC was performed using  $\alpha\text{-Fe}_2\text{O}_3$  nanoparticles, and the corresponding product was obtained in excellent activity and selectivity; benzylation reaction over  $\alpha\text{-Fe}_2\text{O}_3$  NPs were also explored for substituted aromatic compounds, *e.g.*, toluene

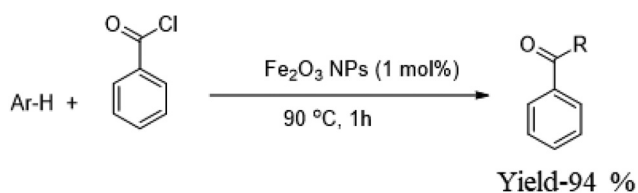
and *p*-xylene (see Table 1). It has been observed that 100% conversion of BC was obtained within 3 min.

Activated hematite catalyzed Friedel–Crafts acylation of benzene (*i.e.*, chlorobenzene and nitrobenzene) has been reported under benign conditions.<sup>234</sup> The activation of hematite was achieved *via* sonication under air atmosphere, followed by heating at 200 °C, which certainly helped improve the activity of the catalyst. A range of benzene derivatives were smoothly transformed to the desired acylated compounds with moderate to good yields (Fig. 35) and the activated  $\alpha\text{-Fe}_2\text{O}_3$  can be recovered with minor loss in catalytic performance. The benefits of employing this solvent-free methodology encom-





**Fig. 33** (a–d) TEM images of  $\text{Fe}_2\text{O}_3/\text{SBA}-15-20$ ;  $\text{Fe}_2\text{O}_3/\text{SBA}-15-40$ ;  $\text{Fe}_2\text{O}_3/\text{SBA}-15-60$ ; and  $\text{Fe}_2\text{O}_3/\text{SBA}-15-90$  catalysts respectively; inset in (c): high-resolution TEM image of (104) reflection of  $\alpha\text{-Fe}_2\text{O}_3$ . Reproduced from ref. 229 Copyright 2009, Elsevier.



**Fig. 34** Friedel–Crafts acylation using the hematite nanoparticles.<sup>230</sup>

pass easy reaction set-up, mild reaction parameters, greater efficacy, and selectivity, which bodes well for the future use of the catalyst for various other greener organic transformations.

Recently, Guo and colleagues<sup>235</sup> reported a blend of mechanically combined lipophilic  $\alpha\text{-Fe}_2\text{O}_3$  and  $\text{CaCO}_3$  NPs as a highly effective catalyst in the Friedel–Crafts acylation reaction. In this study,  $\alpha\text{-Fe}_2\text{O}_3$  nanoparticles were synthesized using a continuous precipitation method in a micro-mixer,

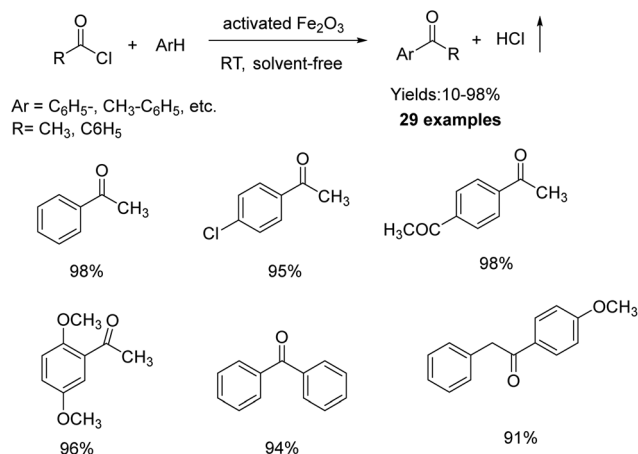
while  $\text{CaCO}_3$  NPs were prepared in a flow reactor (see Fig. 36). The modified NPs were then deployed as catalysts in the acylation process, leading to a high yield of 97.8% under optimized conditions. Interestingly, the addition of  $\text{CaCO}_3$  NPs enhanced the catalytic efficiency compared to using only modified  $\alpha\text{-Fe}_2\text{O}_3$  NPs. This novel acylation method demonstrated effectiveness across various substrates.

## 2.5. Fischer–Tropsch synthesis

The transformation of syngas into value-added linear hydrocarbons, popularly referred to as Fischer–Tropsch synthesis (FTS), is considered an important chemical transformation in heterogeneous catalysis.<sup>236–238</sup> However, creating FTS catalyst for the production of an array of compounds with greater performance and selectivity still remains a formidable task for chemists, the use of iron-based catalyst can potentially offer a viable solution because such inexpensive, earth-abundant

**Table 1** Effect of various electron donating groups for the alkylation of benzene over  $\alpha\text{-Fe}_2\text{O}_3$  NPs

| Substrate        | Time (min) | Temp. (K) | BC conversion (%) | Reaction products (selectivity (%))   |
|------------------|------------|-----------|-------------------|---------------------------------------|
| Benzene          | 3          | 358       | 100               | Diphenylmethane (97.76%)              |
| Toluene          | 3          | 368       | 100               | <i>o</i> -Benzyltoluene (52.36%)      |
|                  |            |           |                   | <i>p</i> -Benzyltoluene (47.64%)      |
| <i>p</i> -Xylene | 3          | 378       | 100               | 2-Benzyl-1,3-dimethylbenzene (99.93%) |



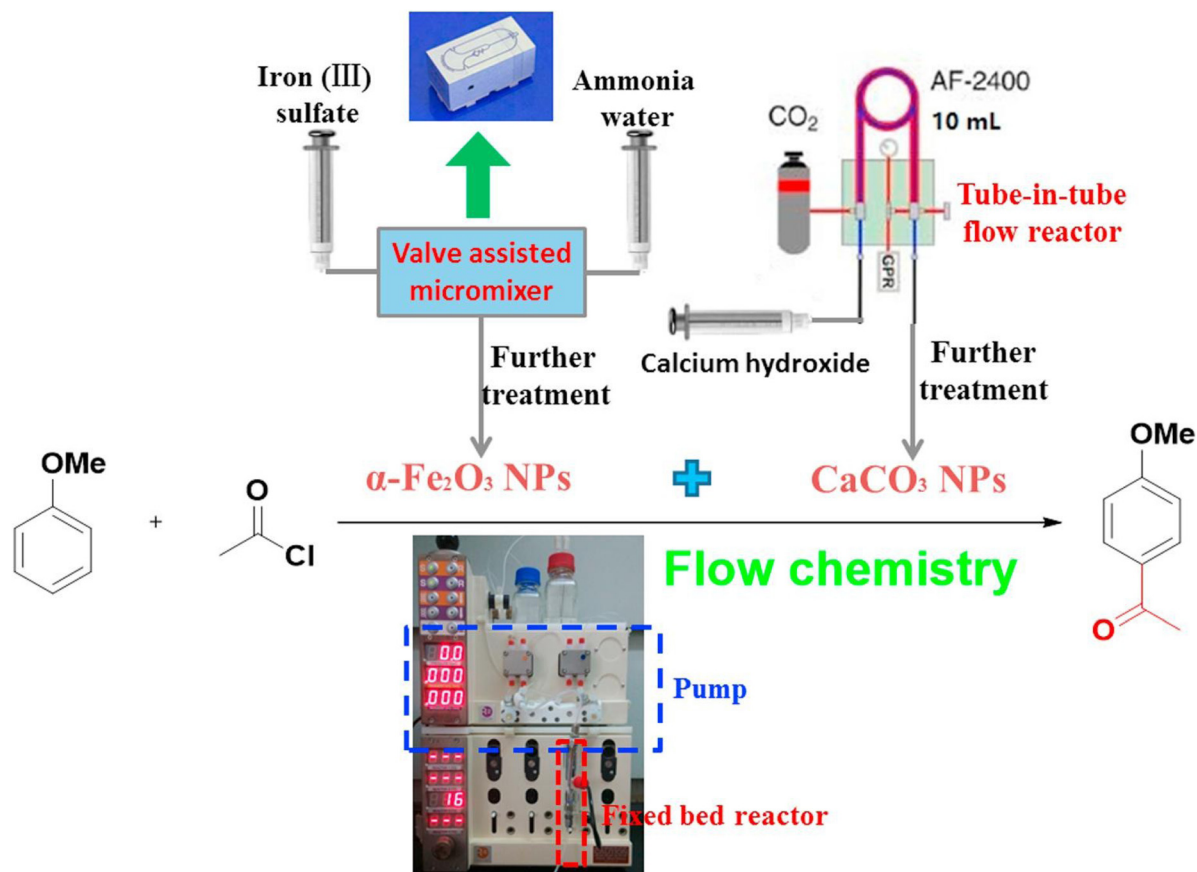
**Fig. 35** Friedel–Crafts acylation and benzoylation of aromatic compounds. Reproduced with permission from ref. 234 Copyright 2010, Wiley-VCH GmbH & Co. KGaA, Weinheim.

materials have displayed good performance and have capacity to produce various hydrocarbon compounds such as diesel, wax, gasoline to C<sub>2</sub>–C<sub>4</sub> olefins or paraffins.<sup>239–243</sup>

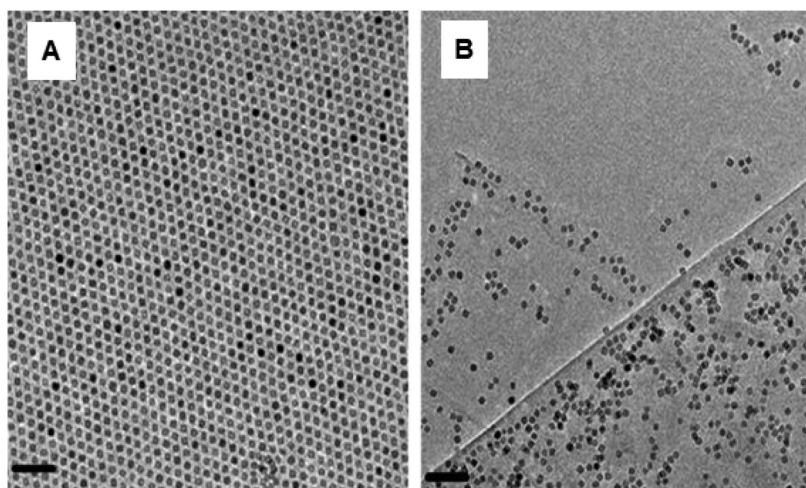
The graphene oxide incorporated monodispersed iron oxide NPs were employed as a catalysts for FTS.<sup>244</sup> In this

process, it was discovered that the thermal behavior of supporting materials was important for good catalytic performance and selectivity especially for C<sub>5</sub>+ hydrocarbons. The size and the structure of monodispersed iron oxide NPs and the final catalyst, Fe/PGO (pyrolytic graphene oxide), are depicted in Fig. 37. It was noted that the iron oxide nanoparticles were keeping the cubic morphology with a size of about 8 nm (see Fig. 37a) and can be accumulated into a “supper lattice” assembly because of their homogeneous distribution;<sup>245</sup> iron oxide NPs were very well-dispersed throughout the carbon support (see Fig. 37b). Because of the heat processing, the amount of “O” and “S” species decreased, and the degree of graphitization increased. It is noteworthy to highlight that oxygen groups onto the surface could change the surface features of the active iron form, which provides diverse catalytic performance.

The prepared catalyst has been employed for the CO conversions as time-on-stream function of FTS at 270 °C and their product selectivity's are depicted in Table 2. At the fixed iron loading for all catalysts (10%), when graphitization temperature was increased to 380 °C ((Fe/PGO-380), and 600 °C (Fe/PGO-600)), clearly an improved CO conversion was observed. As increasing treatment temperature up to 800 °C, only marginal increase in the activity was noticed when compared to



**Fig. 36** Schematic representation of continuous flow setup for Friedel–Crafts acylation reaction. Reproduced with permission from ref. 235 Copyright 2018, Elsevier.



**Fig. 37** (A and B) TEM images of iron oxide NPs and Fe/PGO respectively (scale bars: 50 nm). Reproduced with permission from ref. 244 Copyright 2013, Elsevier.

**Table 2** Optimization study of the FTS reaction over the catalysts<sup>a</sup>

| Catalysts                   | Conversion% | CO <sub>2</sub> yield (%) | Selectivity in hydrocarbon wt.% |          |                                |                  |                                                   |
|-----------------------------|-------------|---------------------------|---------------------------------|----------|--------------------------------|------------------|---------------------------------------------------|
|                             |             |                           | CH <sub>4</sub>                 | Methanol | C <sub>2</sub> –C <sub>4</sub> | C <sub>5</sub> + | Olefin/paraffin in C <sub>2</sub> –C <sub>4</sub> |
| Fe/PGO                      | 10.2        | 0.6                       | 21.4                            | 9.7      | 52.0                           | 16.9             | 0.24                                              |
| Fe/PGO-380                  | 30.4        | 5.1                       | 21.2                            | 8.6      | 46.6                           | 23.6             | 0.77                                              |
| Fe/PGO-600                  | 35.0        | 10.8                      | 12.7                            | 3.2      | 39.1                           | 45.0             | 1.57                                              |
| Fe/PGO-800                  | 36.7        | 10.1                      | 12.6                            | 3.2      | 36.8                           | 47.4             | 1.44                                              |
| Fe/AC-HNO <sub>3</sub>      | 7.8         | 0.7                       | 22.5                            | 6.7      | 47.1                           | 23.7             | 0.80                                              |
| Fe/AC-HNO <sub>3</sub> -800 | 13.6        | 1.7                       | 16.0                            | 4.1      | 40.8                           | 39.1             | 1.28                                              |

<sup>a</sup> Reaction parameters: 80 mg catalyst having 10% iron, 3 MPa syngas, <sup>1</sup> 270 °C. The C<sub>2</sub>–C<sub>4</sub> oxygenates were included in the C<sub>2</sub>–C<sub>4</sub> products.

Fe/PGO-600, signifying the similar physical properties of PGO-600 and PGO-800; comparable selectivity patterns were discerned for activated carbon containing catalysts, Fe/AC-HNO<sub>3</sub> and Fe/AC-HNO<sub>3</sub>-800, based on PGO resources.

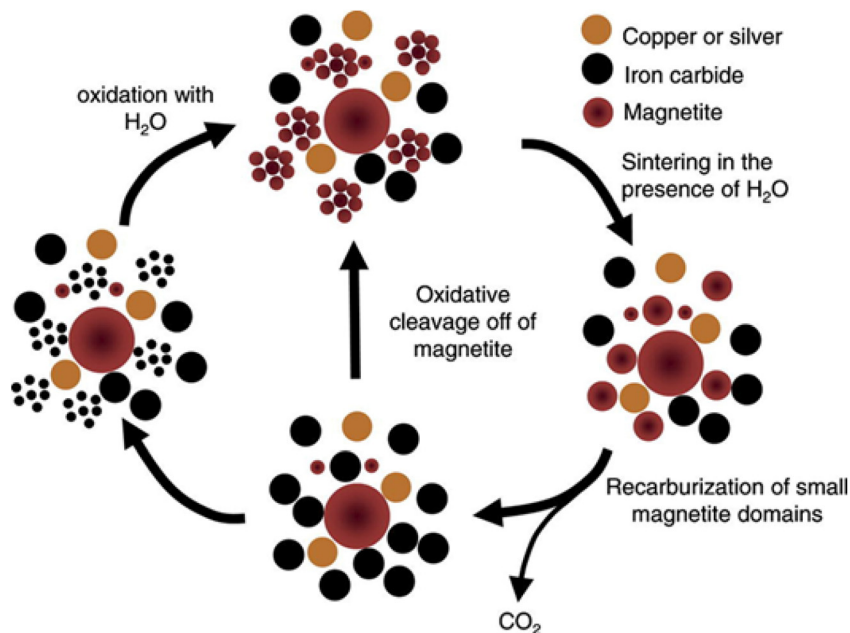
The dynamic behavior of the model iron-based Fischer-Tropsch catalysts has been demonstrated wherein Ag and Cu delafossite model systems were synthesized *via* co-precipitation method under basic conditions using metal nitrates as precursors, followed by calcination at elevated temperatures.<sup>246</sup> The catalysts were characterized using AAS, XRD, and Mössbauer spectroscopy and the catalytic activity was assessed in a slurry reactor. Upon activation of the catalysts under different conditions, *via* H<sub>2</sub> and CO-activations (commonly employed for FT catalysts), the evolution of the different phases was monitored using *in situ* XRD to understand the dynamic performance of such catalytic systems. The presence of either Ag or Cu assisted in the generation of magnetite during the H<sub>2</sub>-activation step, which ultimately resulted into conversion of magnetite into metallic iron, possibly *via* H<sub>2</sub>-spill-over. However, for CO-activation, the influence of as synthesized catalysts (Cu, and Ag catalyst) seems to be less prominent. Silver nanoparticles displayed higher catalytic activity generating not only the olefinic products but also relatively higher amount of undesired CO<sub>2</sub>

byproduct. The generation of CO<sub>2</sub> has been attributed to the existence of superparamagnetic iron species formed during the activation step and/or reaction conditions. Alternatively, hydrogen transfer from the group 11 metal surface could partly reduce the magnetite surface, aiding in the carburization process; Fig. 38 illustrates the changes in iron-based FT catalyst with group 11 metals presents.

The contribution of hematite in the precipitated iron-based reported for FT catalysts, by Duvenhage and co-workers,<sup>247</sup> where the co-precipitation method was used originally reported by the same group. By simply varying the hold time between the precipitation and the filtration steps, the content, and the crystallite size of hematite in the catalysts could be tuned. In their catalytic studies, the low amount of hematite content (1.5 to 25 wt%) did not improve the performance of the catalysts presumably due to lower surface area and pore volume. However, catalysts with hematite content between 25 to 45 wt% not only displayed better catalytic performance but higher reducibility and improved attrition resistance.

The influence of support for the iron-based FT catalysts were analyzed by preparing four supports namely SBA-1 (silica), activated carbon (carbon), CMK-3 (carbon) and CNTs (carbon) and incorporated Fe-species *via* incipient wetness

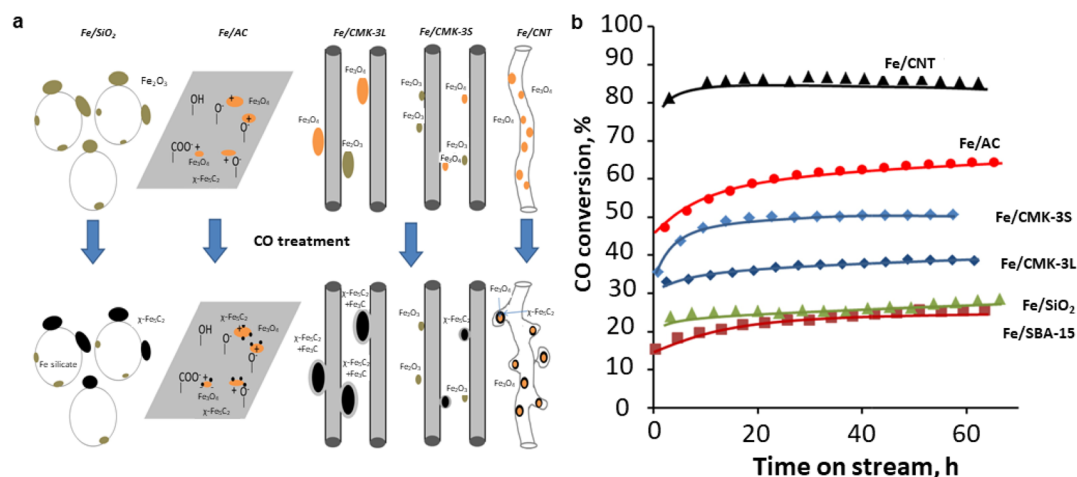




**Fig. 38** Schematic diagram for the transformations over the iron-based FT catalyst. Reproduced with permission from ref. 246 Copyright 2013, Elsevier.

impregnation method.<sup>248</sup> After a calcination step under nitrogen, these materials were treated with CO as a part of the activation step; finally, they were characterized and studied for the FT synthesis. During the calcination step, hematite was formed when silica was used as a support, while the decomposition of iron nitrate in carbon materials mostly formed  $\text{Fe}_3\text{O}_4$ , which cannot exclude the presence of maghemite phase. The CO activation step allowed the facile carbidisation process to yield Fe-carbide. Among these hybrid systems, silica-supported catalysts exhibited the lowest performance compared to carbon-supported catalysts presumably because of the vari-

ation in phase compositions. The greater catalytic performance was obtained with carbon-nanotube supported catalysts (Fig. 39b). The variation in performance was ascribed to the existence of the Fe-oxides as well as the formation of Fe-carbide during the CO-activation step (Fig. 39a). In case of CNTs, the highest activity was explained by the formation of Fe-carbide-magnetite core-shell nanoparticles, which act as “nodules” in a confined area exhibiting higher performance. It is crucial to emphasize that the catalysts without CO-activation did not catalyze the reaction, confirming that the iron-carbide-magnetite core-shell serve as efficient catalytic centers.



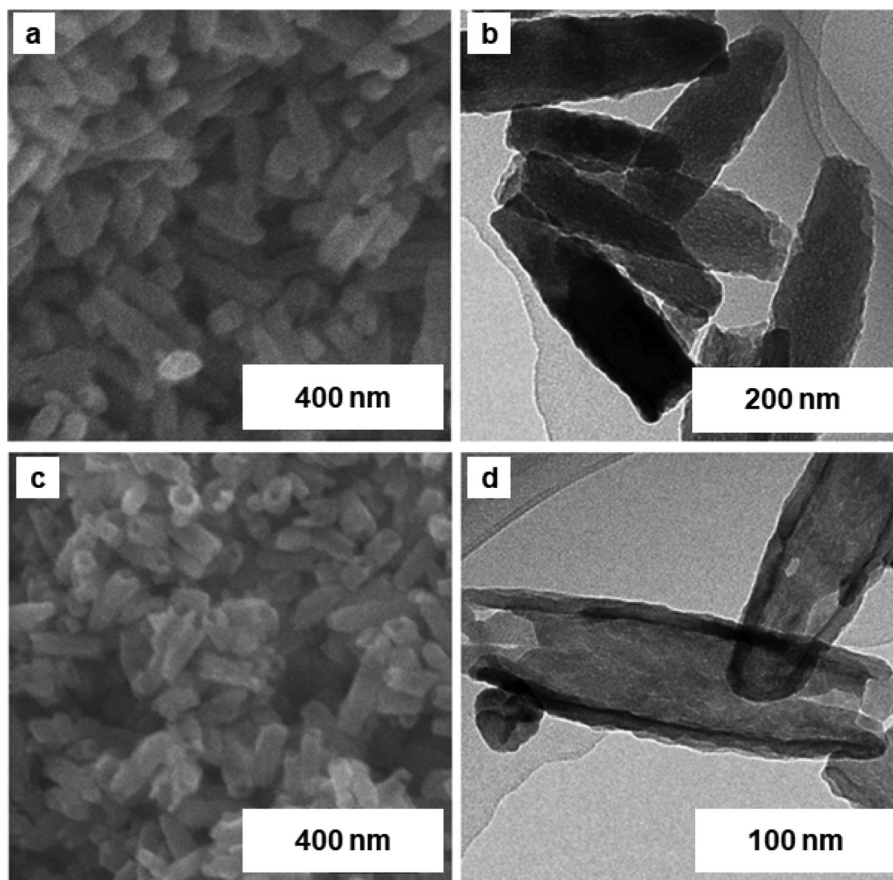
**Fig. 39** (a) Evolution of iron species over silica and carbon support for CO activation; (b) Catalytic performance of iron catalysts. Reproduced from ref. 248 Copyright 2014, Elsevier.

A relatively new and sophisticated inelastic neutron scattering (INS) technique was deployed to probe the mechanistic details of the hydrogen pre-treatment process for iron-based FTS catalysts used in CO hydrogenation.<sup>249</sup> The study was performed using hematite (prepared by co-precipitation method) as pre-catalysts, which were first activated using H<sub>2</sub>, at two different temperatures (623 and 723 K), and then subsequently investigated for CO hydrogenation using INS technique, coupled with TEM, XRD and other material characterization techniques. The INS spectra indicated the presence of carbonaceous layers with primarily saturated hydrocarbons for the samples heated at 623 K. However, this activation step for the high temperature sample exhibited larger quantity of amorphous carbons on the surface, thereby reducing the catalytic performance. The research showed that the activation step might be disadvantageous for such catalytic systems although a detailed mechanistic investigation is warranted.

The surface characteristics of 1D nanostructured iron oxides exhibit significant distinctions when compared to their counterparts with spherical shapes.<sup>250,251</sup> Among them, nanotubes are of particular importance due to its rolling, which imposes stress and allows the electron wave functions to be different within nanotubes interior and exterior walls. In FTS,

the selectivity of the product is the main issue because of Anderson–Schulz–Flory distribution of hydrocarbons.<sup>252</sup> Well-defined pore size, structure and surface properties have significant effect on the selectivity of FTS products.<sup>253,254</sup> Thus, nanotubes with unique properties such as mesoporous structure, uniform PSD, and surface properties are attractive for FTS. Recently, Sun and co-workers has synthesized Fe<sub>2</sub>O<sub>3</sub> nanorods and nanotubes by the hydrothermal process of ferric chloride in the existence of KH<sub>2</sub>PO<sub>4</sub> at 220 °C at certain reaction time.<sup>255</sup> TEM images of nanorods prepared after 6 h, show a diameter of around 80 nm and a length of 270 nm. The nanotubes synthesized after treatment for 48 h, show outer diameters, inner diameters, and lengths between 60–80, 40–60 and 260 nm respectively (Fig. 40).

The catalytic FTS reaction under simulated industrial conditions at 280 °C, 2.0 MPa, and a H<sub>2</sub>/CO ratio of 2 revealed that the activity of Fe<sub>2</sub>O<sub>3</sub> nanorods increases primarily for 16 h and reaches a maximum value of 39.5% and then falls slowly up to 12.9% at 120 h. On the other hand, for Fe<sub>2</sub>O<sub>3</sub> nanotubes the CO conversion values reached a maximum within 16 h, and remained constant during the 120 h period. The ratio of olefins to paraffin (O/P) for Fe<sub>2</sub>O<sub>3</sub> nanorods and nanotubes was found to be 1.85 and 3.0, respectively along with the



**Fig. 40** (a, b) SEM and TEM analysis of Fe<sub>2</sub>O<sub>3</sub> nanorods; (c, d) SEM and TEM images of Fe<sub>2</sub>O<sub>3</sub> nanotubes. Reproduced with permission from ref. 255 Copyright 2016, The Royal Society of Chemistry.

selectivity for  $C_{5+}$  products (63.4% and 72.1%, respectively). These findings clearly indicate superior selectivity's of nanotubes over nanorods. Reduction and carburization of Fe-based catalysts allegedly activate catalyst for FT synthesis due to carbide formation.<sup>256</sup>

Co- and Fe-based catalysts<sup>257</sup> were investigated for FT process wherein Fe-based catalyst were synthesized by reportedly similar method in which a Fe(100)/Zn(10) precursor (atomic ratios) mixture was obtained by semi-batch-co-precipitation of Fe and Zn nitrates at constant pH to produce porous Fe-Zn oxy/hydroxycarbonate powders. The obtained powders were heated at 350 °C for 1 h and further facilitated by potassium carbonate and copper nitrate by incipient wetness impregnation method, followed by calcinations at 400 °C for 4 h. Samples with a Cu/Fe a (0.01) and K/Fe with atomic ratios of 0.02, 0.04 and 0.1 were also synthesized; denoted as "Fe2K", "Fe4K" and "Fe10K" respectively.

All prepared catalysts were deployed in FT process under various reaction conditions. During the hydrogenation of  $CO_2$ , conversion of  $H_2$  and  $CO_2$  were found of 20% and 9%, respectively. The degree of the conversion remains constant over the entire period of the reaction (60–80 h). In fact, in addition to water, gaseous and liquid hydrocarbons, a significant amount of CO was observed in the product pool. Subsequent to subjecting the catalyst to testing in the presence of  $CO_2$ , the activity of the catalysts with  $H_2/CO$  mixtures were evaluated for comparative study analysis when CO and  $H_2$  conversions were identified as 12% and 22%, respectively, which are greater than with the similar H/C ratio of  $H_2/CO_2$  mixture. These findings suggest that  $CO_2$  has lesser performance than CO under similar conditions for an iron-based catalyst. Remarkably, it was found that in contrast to the  $CO_x$  conversion rates, the hydrocarbon distributions achieved from the hydrogenation of CO and  $CO_2$  were completely different. For CO, a direct Anderson-Schulz-Flory (ASF) distribution of hydrocarbons was accomplished, with probability of chain growth for the C3–C10 species of 0.71 and a small negative deviation from the linear trend of species C1 and C2. These results are completely consistent with the existing literature,<sup>258–260</sup> which suggests that the alkali-doped Fe-based catalysts show less selectivity for  $CH_4$  during the hydrogenation of CO.<sup>261</sup> In contrast, for  $CO_2$ , the yield of hydrocarbons (C1–C3) is substantially better and the chain growth probability of species C3–C10 decreased to a degree of 0.65. The other fractions of olefins, specifically C2–C10 products, are also found as a function of the carbon number. In this case, the olefin fractions decrease monotonically with C number, tending to an asymptote value close to 70% for C4–C10 species. It indicates that the distribution of product and the yield of olefin in the hydrocarbons are constant over the course of continuous CO hydrogenations and, after catalytic tests with  $CO_2$ , the mixture  $H_2/CO$  quickly reaches a steady state after switching back.

An *et al.*<sup>262</sup> synthesized  $Fe_3O_4$ @iron carbide NPs by pyrolysis of Fe-containing MOFs for FTS. The synthesis of the Fischer-Tropsch catalyst Fe-MIL-88B/C and Fe-MIL-88B-NH<sub>2</sub>/C is illustrated in Fig. 41a. The formation of surface carbonates

comes from the CO in the feed gas, as shown in Fig. 41b; core-shell Fe NPs were uniformly distributed on iron carbide. The lattice planes (311) and (111) correspond to the inner core  $Fe_3O_4$  and the outer shell  $\chi-Fe_5C_2$ , respectively (Fig. 41c). In the first 30 hours, the catalyst activity increased and then remains constant with no evidence of quenching even after 200 hours. The selectivity to olefins and long-chain hydrocarbons remains unchanged during test (Fig. 41d and e).

Recently, Wu *et al.*<sup>263</sup> reported boron carbon nitride supported iron oxide nanocatalyst (Fe@BCNNSs) through thermal decomposition for the FTS. The TEM images affirmed that the black iron oxide nanoparticles were evenly dispersed across boron carbon nitride sheet (BCNNs) with particle size of 2–18 nm (Fig. 42a and b). The lattice space of dark particle and the encapsulated layer was 0.21 nm and 0.34 nm, respectively (Fig. 42c and d). The conversion of CO enhanced remarkably with increasing reaction temperature at 320 °C and reached 95% at 340 °C over Fe@BCNNSs catalyst (Fig. 42f). The selectivity for different hydrocarbons is also illustrated (Fig. 42e). The increased stability of the catalyst is due to the special encapsulated structure even after 1000 hours of operation. The BCNNSs shell prevents catalyst deactivation under high temperature conditions.

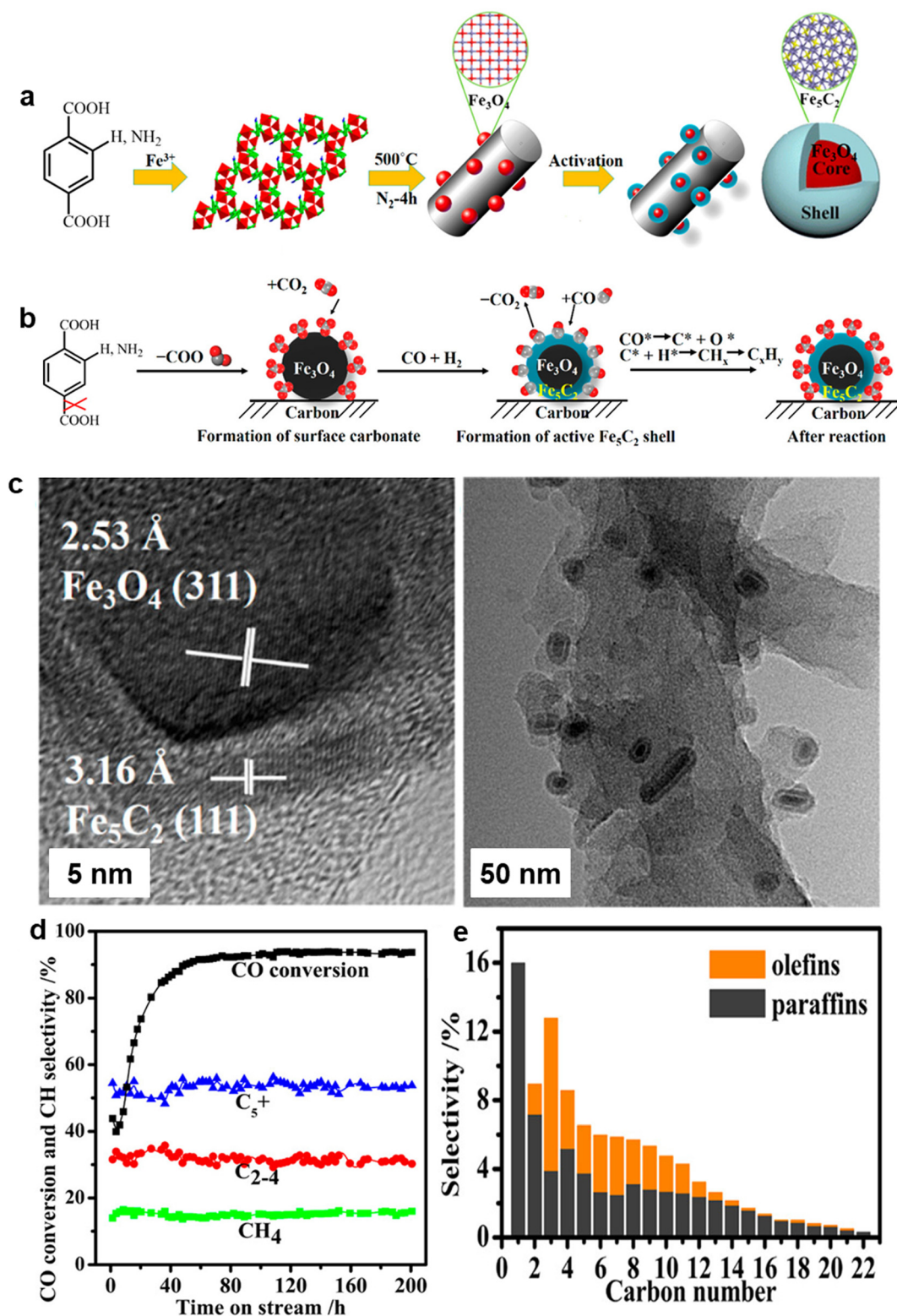
## 2.6. Multicomponent reactions

Multicomponent reactions (MCRs) involve the simultaneous reaction of three or more reactants within a single vessel to produce a final product that incorporates features from all the reactive components.<sup>264</sup> 3,4-Dihydropyrano[c]chromenes and its analogues are important building blocks in numerous areas including chemistry, biology and pharmacology;<sup>265–269</sup> representative compounds from this class display spasmolytic, diuretic, anti-cancer, anticoagulant, and anti-anaphylactic activities.<sup>270,271</sup> Additionally, they can be employed as a cognitive activator for the therapeutic interventions of neurodegenerative diseases, such as Alzheimer's disease, Huntington's disease, amyotrophic lateral sclerosis, *etc.*<sup>272,273</sup>

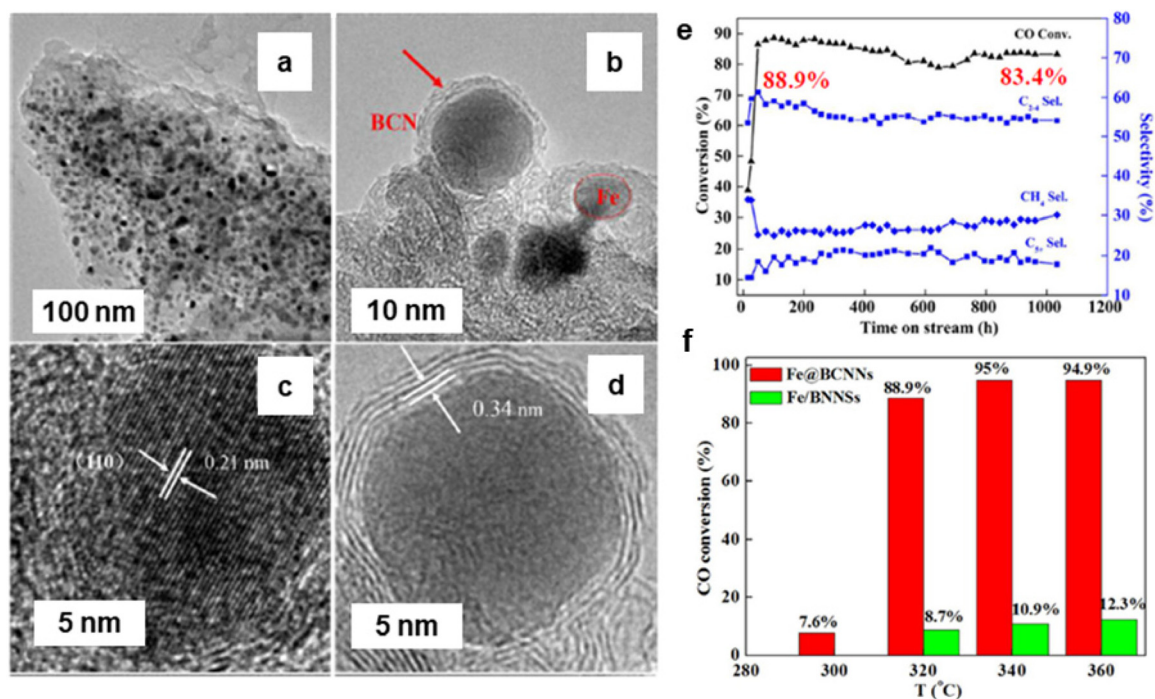
In this context, the combustion-based preparation of  $\alpha-Fe_2O_3$  nanopowder were developed<sup>274</sup> and their catalytic performance was studied for single step preparation of 3,4-dihydropyrano[c]chromenes under mild and benign reaction conditions. The  $\alpha-Fe_2O_3$  nanopowder was found to be very effective for the three-component condensation of aldehyde, malononitrile and 4-hydroxycoumarin at RT (Fig. 43). This appears to be an ideal alternative for the preparation of 3,4-dihydropyrano[c]chromenes as the reactions are rapid, clean, and the target compounds are obtained with satisfactory yields. The recyclability of  $\alpha-Fe_2O_3$  catalyst was also inspected wherein the catalyst can be recovered readily and they are reusable till five tested cycles.

Afterwards, iron oxide nanocatalyst was used for benzimidazoles synthesis.<sup>275</sup> The acidic nature of the prepared iron oxide catalyst activates aldehyde which participates in the nucleophilic addition of amine. In the next steps, Michael addition and air oxidation lead to the benzimidazole product. Recently, a benign nanocatalyst (NiFe<sub>2</sub>O<sub>4</sub>/geopolymer) were prepared for

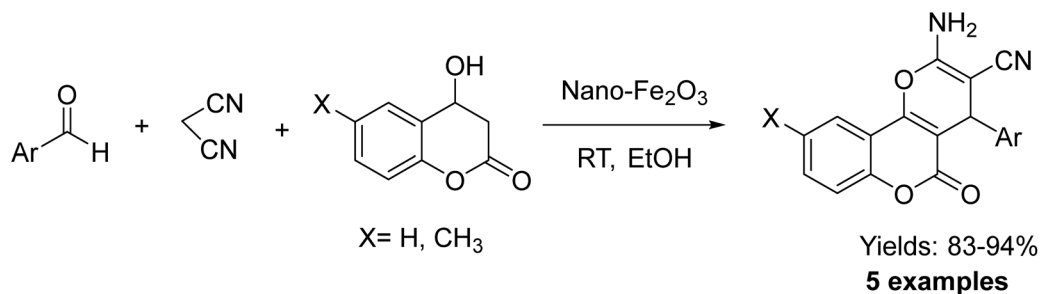




**Fig. 41** (a) Schematic representation for the synthesis of  $\text{Fe}_3\text{O}_4@\text{Fe}_5\text{C}_2$  nanocatalyst; (b) Schematic diagram for production of  $\text{Fe}_3\text{O}_4@\text{Fe}_5\text{C}_2$  catalysts and Fischer Tropsch surface chemistry; (c) HR-TEM images of Fe-MIL-88B- $\text{NH}_2/\text{C}$ ; (d, e) The catalytic activity of Fe-MIL-88B- $\text{NH}_2/\text{C}$  nanocatalyst. Reproduced with permission from ref. 262 Copyright 2016, American Chemical Society.



**Fig. 42** (a, b) TEM images of Fe@BCNNs nanocatalyst; (c, d) HR-TEM images Fe@BCNNs of nanocatalyst; (e, f) Activity of the Fe@BCNNs of nanocatalyst. Reproduced with permission from ref. 263 Copyright 2017, American Chemical Society.



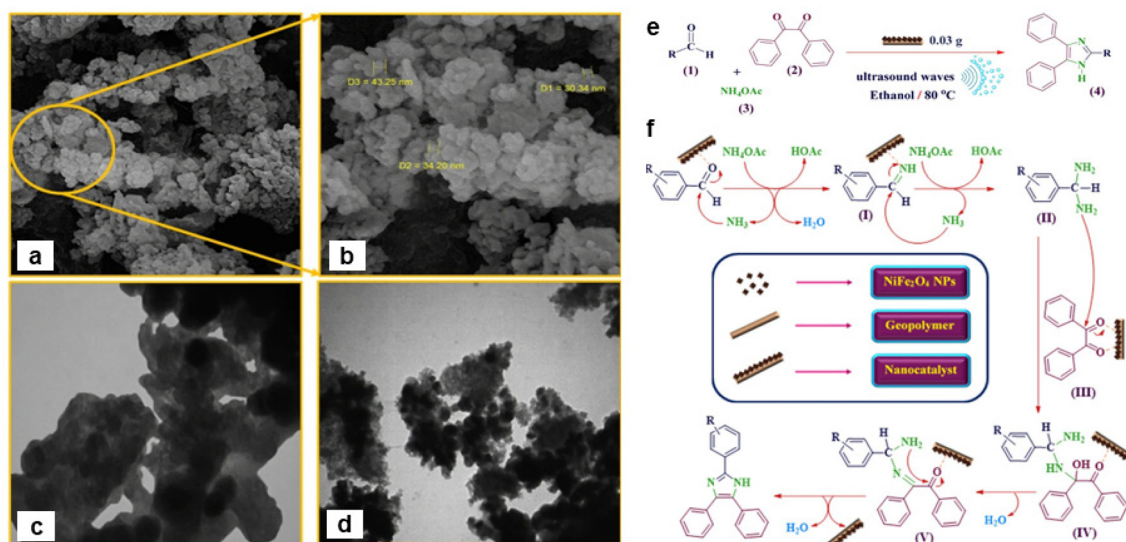
**Fig. 43** One-pot preparation of 3,4-dihydropyrano[c]chromenes catalyzed by  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>. Reproduced with permission from ref. 274 Copyright 2010, Elsevier.

the synthesis of imidazole derivatives *via* ultrasonication.<sup>276</sup> The nanocomposite was prepared by two steps including (i) synthesis of NiFe<sub>2</sub>O<sub>4</sub> NPs by coprecipitation method, and (ii) synthesis of bentonite-based geopolymer and the addition of NiFe<sub>2</sub>O<sub>4</sub> NPs to geopolymer (Fig. 44a). The cubic shape and particle size (30 nm) of NiFe<sub>2</sub>O<sub>4</sub> NPs were studied by FE-SEM analysis (Fig. 44b and c). Fig. 44d and e shows the presence and dispersion of NiFe<sub>2</sub>O<sub>4</sub> NPs on geopolymer. The stepwise mechanism is depicted in Fig. 44f. The Lewis acid sites of the nanocomposite activates the aldehyde while ammonium chloride was used as a nitrogen source for the synthesis of imidazole derivatives.

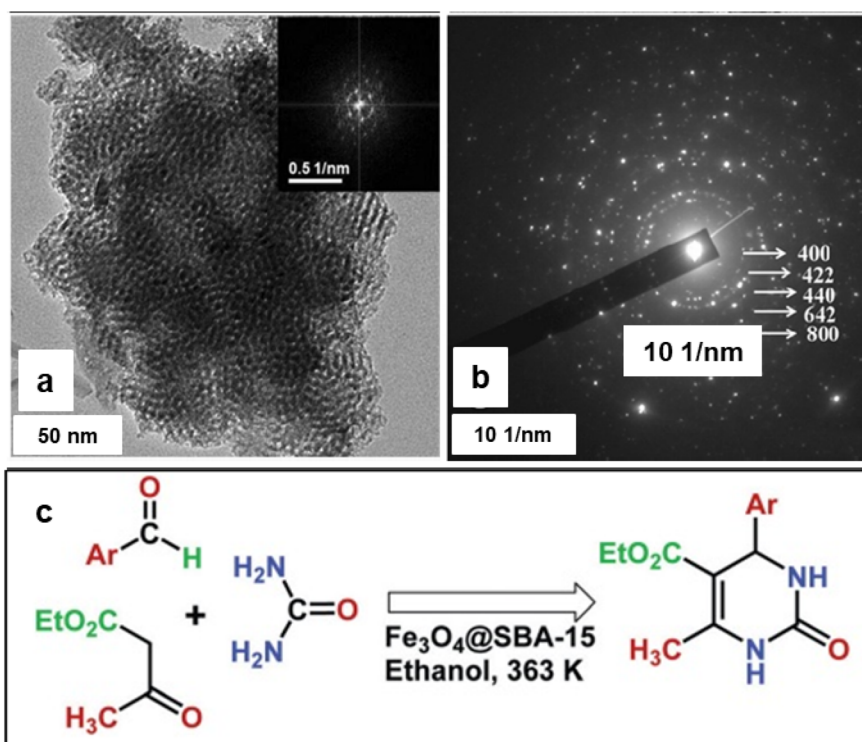
The Biginelli reaction is notably acknowledged for its role in the syntheses of dihydropyrimidones/thiones and essential compounds with biological significance.<sup>264</sup> Bhaumik and co-

workers<sup>277</sup> developed chemically conjugated catalyst that has been engineered through the thio-ene click reaction, incorporating Fe<sub>3</sub>O<sub>4</sub> NPs into mesoporous SBA-15 (Fe<sub>3</sub>O<sub>4</sub>@SBA-15). The HR-TEM image confirms honey-comb like hexagonal pattern (see Fig. 45a) with a pore size ranging from 6–7 nm and selected area electron diffraction (SAED) pattern affirms the existence of crystalline Fe<sub>3</sub>O<sub>4</sub> (see Fig. 45b). This as prepared Fe<sub>3</sub>O<sub>4</sub>@SBA-15 heterogeneous catalyst was utilized in the one-pot Biginelli condensation process (Fig. 45c) enabling the synthesis of diverse and valuable 3,4-dihydropyrimidin-2(1H)-ones.

Additionally, highly innovative and efficient green catalyst *i.e.* Fe<sub>3</sub>O<sub>4</sub>@[Ni(bpy)<sub>2</sub>(py-tmos)] was developed for the Biginelli condensation reaction<sup>278</sup> and this well characterized nano-catalyst was employed for the synthesis of a broad spectrum of



**Fig. 44** (a, b) Field emission SEM images; (c, d) TEM images; (e) Application; (f) The mechanism for the preparation of imidazole derivatives. Reproduced with permission from ref. 276 Copyright 2020, Springer Nature.



**Fig. 45** (a) TEM images of  $\text{Fe}_3\text{O}_4@\text{SBA-15}$  (FFT pattern is shown in the inset); (b) SAED Pattern of  $\text{Fe}_3\text{O}_4@\text{SBA-15}$ . (c) Biginelli condensation reaction over  $\text{Fe}_3\text{O}_4@\text{SBA-15}$ . Reproduced with permission from ref. 277 Copyright 2012, The Royal Society of Chemistry.

3,4-dihydropyrimidin-2(1H)-ones from the mixture of urea, aromatic-aldehyde and ethyl-acetoacetate. The synthesis of  $\alpha$ -aminonitriles, critical intermediates for  $\alpha$ -amino acid derivatives, amides, diamines, peptides, proteins, and heterocycles, was accomplished through the Strecker reaction, using methyl-arene oxidation. This reaction, considered one of the oldest

and most cost-effective methods, involves the nucleophilic addition of cyanide ions to imines. Similarly, wet impregnation method was deployed for the fabrication of nanocrystalline spinel ferrites *i.e.*  $\text{ZnFe}_2\text{O}_4$ .<sup>279</sup> It is represented by  $\text{MFe}_2\text{O}_4$  ( $\text{M} = \text{Ni}, \text{Zn}, \text{Mn}, \text{Co}, \text{Mg}, \text{etc.}$ ), and these heterogeneous Lewis acid catalysts are attracting significant attention for their unique



structures, superior selectivity, and catalytic activities compared to monometallic counterparts.<sup>280</sup> The most favorable outcome has been achieved when using  $\text{ZnFe}_2\text{O}_4$  as a dual catalyst, among these metal oxides ( $\text{ZnFe}_2\text{O}_4 > \text{NiFe}_2\text{O}_4 > \text{Fe}_3\text{O}_4$ ). Due to high Lewis acidity of as prepared  $\text{ZnFe}_2\text{O}_4$  catalyst further utilized for the Strecker reaction in presence of KI. Additionally, KI could serve as a scavenger for any elemental iodine that might be produced during the reaction, preventing side reactions and improving the yield of the desired product. This as prepared KI/ $\text{ZnFe}_2\text{O}_4$  catalytic system utilized for oxidation of methyl arenes using aqueous *tert*-butyl hydroperoxide (TBHP) as the oxidizing agent and trimethylsilyl cyanide (TMSCN) as a nitrile source, achieving a yield of up to 88% within 2 h.

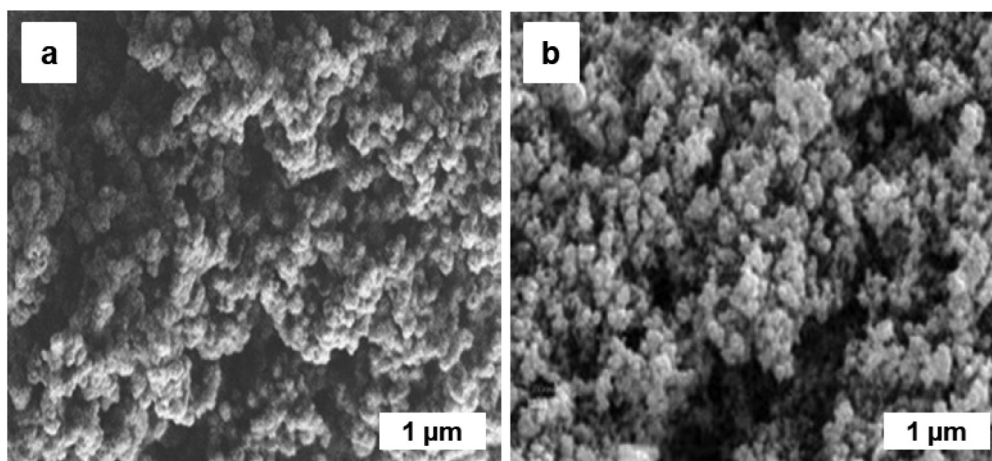
## 2.7. Miscellaneous reactions

In this section, a variety of miscellaneous catalytic reactions, exploring iron oxide NPs are described. Nanomaterials with a core/shell assembly can be developed with various elements/components to prepare multifunctional materials to fine tune their catalytic performances.<sup>92,281,282</sup> Besides composition, the size,<sup>283</sup> shape,<sup>284</sup> and assemblies also affect the catalytic activity. The anisotropic nanocomposites display versatile fundamental properties and considerable efforts are being made for the synthesis of novel functional 1D core/shell nanomaterials.<sup>285,286</sup>

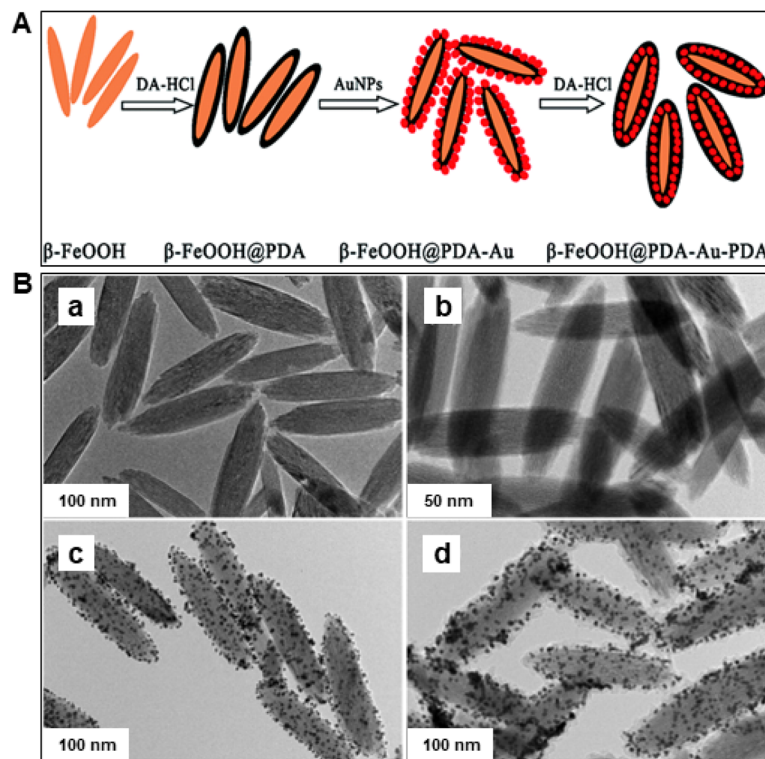
A reusable rod-like  $\beta\text{-FeOOH}@poly(\text{dopamine})\text{-Au-poly}(\text{dopamine})$  nanomaterials were prepared for reduction of Rhodamine B (RhB).<sup>287</sup> Initially,  $\beta\text{-FeOOH}$  was coated with poly(dopamine)(PDA) to generate a core/shell nanomaterial, followed by the decoration of Au nanoparticles on  $\beta\text{-FeOOH}@PDA$  nanorods. Another layer of PDA then coated onto the ensuing particles to avoid the leaching of Au nanoparticles (see Fig. 47A). TEM images of the nanomaterials during various steps are depicted in Fig. 47B, which shows an average size of the  $\beta\text{-FeOOH}$  nanorods amounting to 260 nm. The obtained  $\beta\text{-FeOOH}@PDA$  core/shell nanoparticles were

properly distributed on to Cu grid leaving out agglomeration. Next, the catalytic applicability of  $\beta\text{-FeOOH}@PDA\text{-Au}$  was examined for the reduction of Rhodamine B (RhB) where the amount of catalyst used seemingly played a pivotal role as the catalytic activity strongly improved with the increasing quantity of the catalyst. Due to the thin shell layer of PDA, the reusability of  $\beta\text{-FeOOH}@PDA\text{-Au-PDA}$  radically increased; excellent yield of 98% was obtained even after five cycles when using  $\beta\text{-FeOOH}@PDA\text{-Au-PDA}$  as catalysts, whereas the  $\beta\text{-FeOOH}@PDA\text{-Au}$  demonstrated that it was maintained at only 73%.

Earth surface contains its fair share of toxic conditions, which renders iron prevailing in the form of Fe(III) (oxyhydr) oxide minerals. Nonetheless, because of the microbial respiration, this subsurface environment become anoxic which could turn to reduction of iron species, including aq. Fe(II) and aq. Fe(III). The co-occurrence of aq. Fe(II) and Fe(III) (oxyhydr) oxides is normal at redox interfaces within the enduring of Fe (II)-containing primary rocks, the upsurge of anoxic spring water, and microbial iron species reduction. The chemical reaction of aqueous Fe(II) with iron oxides occurs macroscopically *via* cation sorption at principally passive oxide surfaces.<sup>288–291</sup> Scherer and co-workers<sup>292</sup> reported Fe atom switch within hematite and aq. Fe(II) under mild reaction conditions, where aqueous Fe(II) has been exchanged with Fe(III) of goethite devoid of any substantial phase alteration although it not clear that the aqueous Fe(II) endures related interchange reactions with hematite Fe(III). In this study, an enriched <sup>57</sup>Fe tracer was used to confirm that aqueous Fe(II) exchange with structural Fe(III) hematite at RT, and it was found that the quantity of interchange was affected by size of the particle, pH, and the concentration of Fe(II). In their experimental studies, hematite (80 nm, 27 m<sup>2</sup> g<sup>−1</sup>) in an aqueous medium of Fe(II) at pH = 7.0, was kept for thirty days, which resulted in ~5% of its structural Fe(III) atoms interchanging within Fe(II) in solution phase; being comparable to nearly one surface iron coating. Notably, hematite nanoparticles (50 nm, 54 m<sup>2</sup> g<sup>−1</sup>) displayed



**Fig. 46** (a, b) SEM images of  $\text{Fe}_3\text{O}_4\text{-bpy-Ni(II)}$ . Reproduced with permission from ref. 278 Copyright 2018, Wiley-VCH GmbH & Co. KGaA, Weinheim.



**Fig. 47** (A) Synthesis route of  $\beta$ -FeOOH@PDA-Au-PDA nanostructure; (B) TEM images of prepared catalysts: (a)  $\beta$ -FeOOH, (b)  $\beta$ -FeOOH@PDA, (c)  $\beta$ -FeOOH@PDA-Au, and; (d)  $\beta$ -FeOOH@PDA-Au-PDA. Reproduced with permission from ref. 287 Copyright 2015, The Royal Society of Chemistry.

roughly 25% exchange ( $\sim 3\times$  surface Fe) in aqueous Fe(II), indicating that structural hematite Fe(III) was convenient for liquid at existence of Fe(II). Importantly, the magnitude of exchange in hematite rises up with pH up to 7.5 and then starts to drop, presumably due to saturation of surface site sorbed by Fe(II). However, exchange levels decreased when aq. Fe(II) was enhanced above surface saturation limit. Overall, it can be concluded that even though hematite being the supreme thermodynamically stable iron oxide, Fe(II) can catalyze Fe atom interchange among aq. Fe(II) and bulk hematite. Remarkably, HR-TEM images of the hematite NPs before and after the reaction remained unchanged (see Fig. 48) and the absence of any new phases were affirmed by XRD analyses.<sup>292</sup>

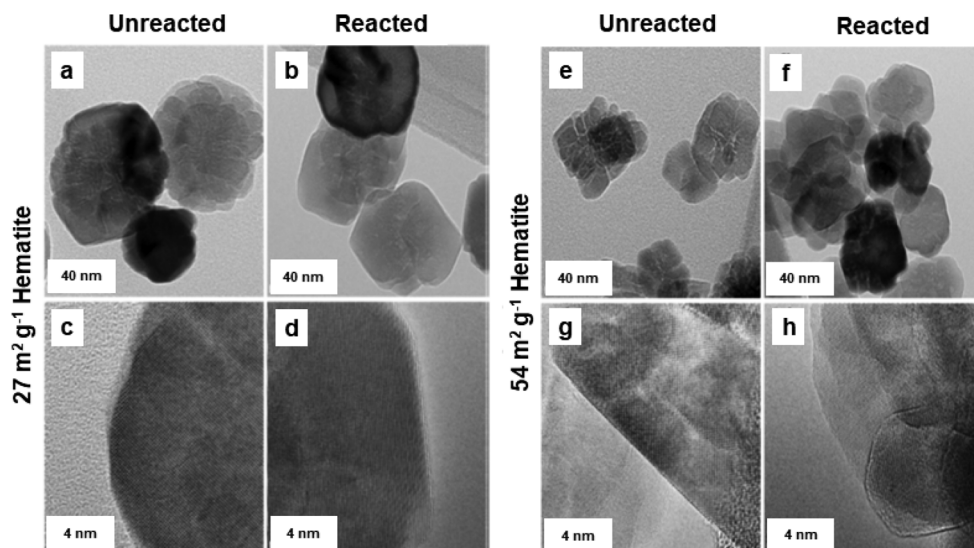
The strategy exploiting the graphene-based materials with designer features entails better knowledge of the interfacial interaction amidst iron oxide particles and graphene sheets.<sup>293,294</sup> Therefore, it is essential to know how the oxidation-reduction reactions of Fe NPs are influenced by the graphene support. This acquaintance is necessary in consideration of the activity of the nanocomposites depending crucially on a specific phase of the iron oxides (*i.e.*, oxidation state of the iron and the crystal structure of the oxides).

The spectroscopic investigation<sup>295</sup> was carried out as to how the specific surface sites influence the reducibility of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>/graphene nanomaterials with H<sub>2</sub>; the steadiness of the Fe<sub>2</sub>O<sub>3</sub> nanoparticles concerning reduction was enriched by the interaction of graphene nanosheets than the bulk Fe<sub>2</sub>O<sub>3</sub>. Post annealing TEM images, disclose the presence of both core/shell

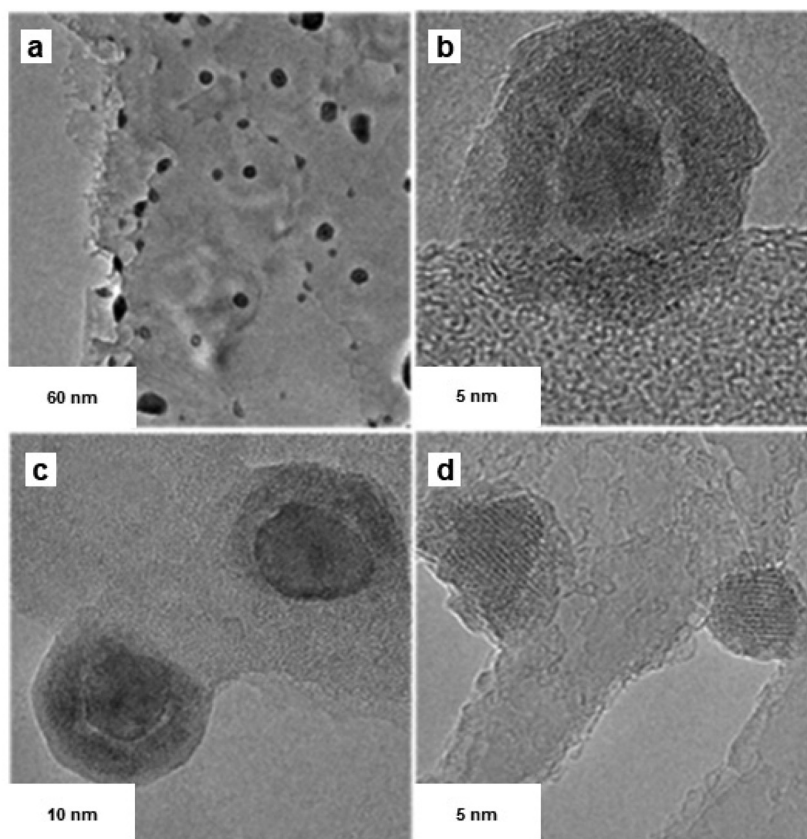
and homogeneous Fe<sub>2</sub>O<sub>3</sub> nanoparticles with the final development of unusual channels into the graphene sheets (see Fig. 49). Because of heat treatment under Fe<sub>2</sub>O<sub>3</sub> and H<sub>2</sub>, it was partly reduced to FeO and to some extent the Fe nanoparticles drill the few layers thick graphite (FLGs) and were grafted on the graphene surface. Overall, in this work, empirical evidence for the function of FeO<sub>x</sub> during the construction of trenches in the FLGs was established comparatively at lower temperature.

In petroleum refineries, valuable light fuels are obtained from bulk volume of atmospheric residue and vacuum-distilled residual oil.<sup>293</sup> In general, to produce the lighter fuels from the residual oil, various conventional processes are used including thermal cracking,<sup>296,297</sup> catalytic cracking<sup>298,299</sup> and hydrocracking.<sup>300,301</sup>

Iron oxide nanocatalysts (as free  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> NPs) as well as SiO<sub>2</sub>-supported  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> crystals were reported<sup>302</sup> for the catalytic cracking of bottom product from the vacuum distillation unit, *i.e.*, vacuum residue (VR) in supercritical water (SCW). Various reaction parameters such as reaction period, temperature, catalyst to oil weight ratio, and water to oil weight ratio were investigated on the yield of coke and maltene obtained from VR cracking including asphaltene conversion. It was found that the  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>@SiO<sub>2</sub> catalyst was more durable and efficient when compared to free NPs in case of VR cracking. In a plausible reaction mechanism, a cycle starting with oxidative cracking of hydrocarbons with lattice oxygen (obtained from reduction of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> to Fe<sub>3</sub>O<sub>4</sub>), followed by liberation of the active H<sub>2</sub> *via* SCW gas shift reaction into VR hydrocracking and



**Fig. 48** HRTEM images at two length scales for  $27 \text{ m}^2 \text{ g}^{-1}$  (a–d) and  $54 \text{ m}^2 \text{ g}^{-1}$  (e–h) hematite. Reproduced with permission from ref. 292 Copyright 2015, American Chemical Society.

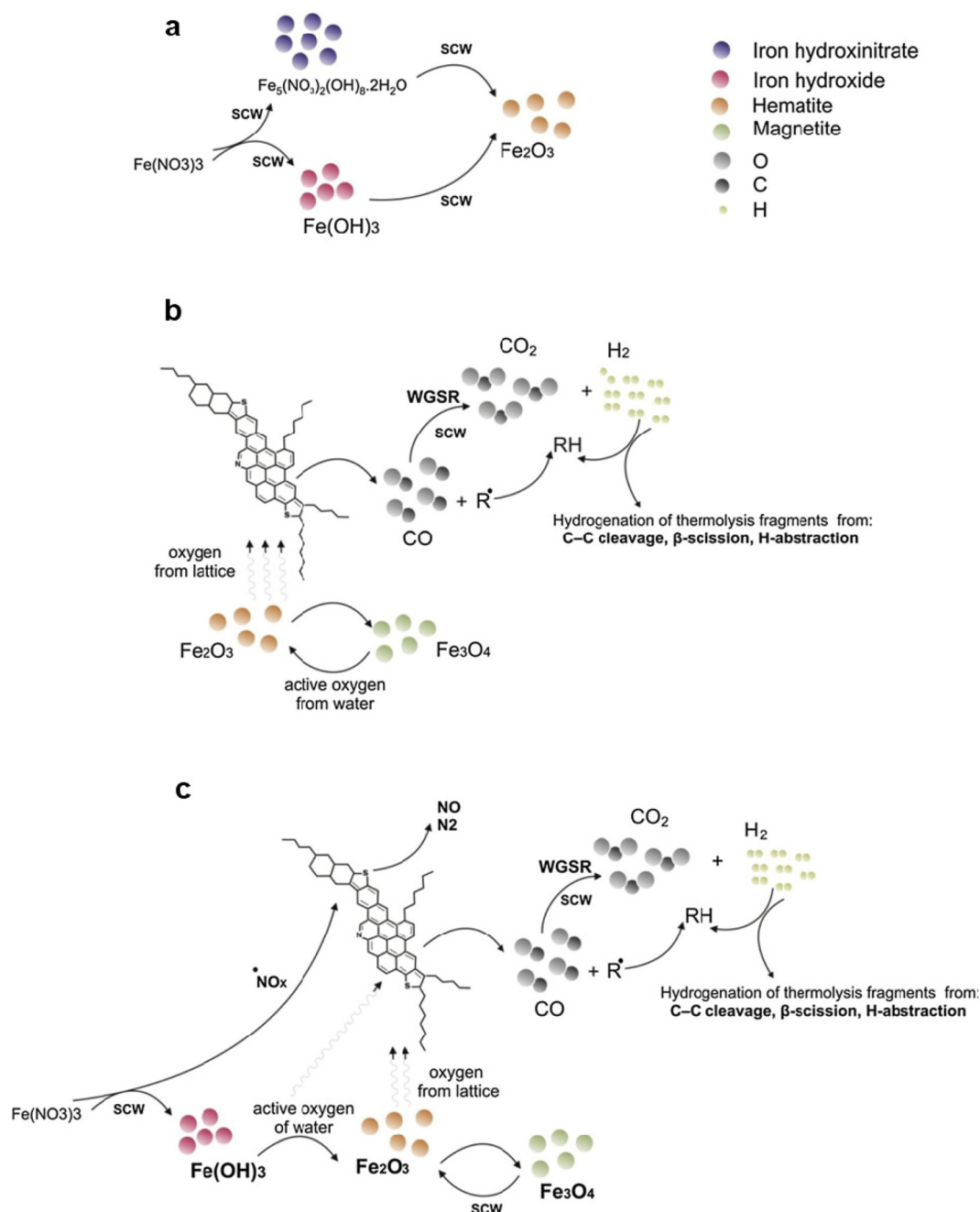


**Fig. 49** Post-annealing TEM image of Fe/FLGs (a) large-scale image; (b) core-shell iron NPs; (c) early stage of trenching and; (d) nanotrench creation in FLGs (few-layer thick graphite). Reproduced with permission from ref. 295 Copyright 2013, American Chemical Society.

manufacture of aliphatic compounds, was reported; the reduced species of the  $\text{Fe}_3\text{O}_4$  catalyst were converted back into  $\alpha\text{-Fe}_2\text{O}_3$  by the liberated “O” atom from SCW (see Fig. 50).

Recently, iron containing nitrogen-functionalized graphene nanoflakes (N-GNFs) were prepared<sup>303</sup> following a procedure by Pristavita *et al.*<sup>304</sup> for producing an active oxygen reduction





**Fig. 50** Schematic representation of catalytic cracking in the SCW: (a) generation of hematite from iron nitrate in SCW; (b) cracking of VR in the presence of hematite and; (c) cracking of VR in the presence of iron nitrate in SCW. Reproduced with permission from ref. 302 Copyright 2015, Elsevier.

reaction catalyst. By taking benefit of the exceptional performance of the plasma atmosphere in the GNFs preparation step, they produced iron-based catalyst in a one pot method. The methane was employed as a carbon source which upon decomposition with argon (Ar) thermal plasma produced GNFs *via* homogeneous nucleation. An inconsequential quantity of N is added at the time of the growth resulting in N content up to 2%. The Fe is added in two distinct phases, one in oxide and other in iron acetate. It is assumed that the vel-

ocity variation and the residence time of the excited species in the plasma recombination zone would affect the Fe functionalization of the GNFs. Further, iron functionalization is predicted to be governed by the duration of exposure of the GNFs to iron vapour; shorter exposure time leads to the generation of an inadequate number of catalytic sites, whereas longer duration of exposure results into the Fe overload of the samples (considering the restricted number of the N-based host sites).

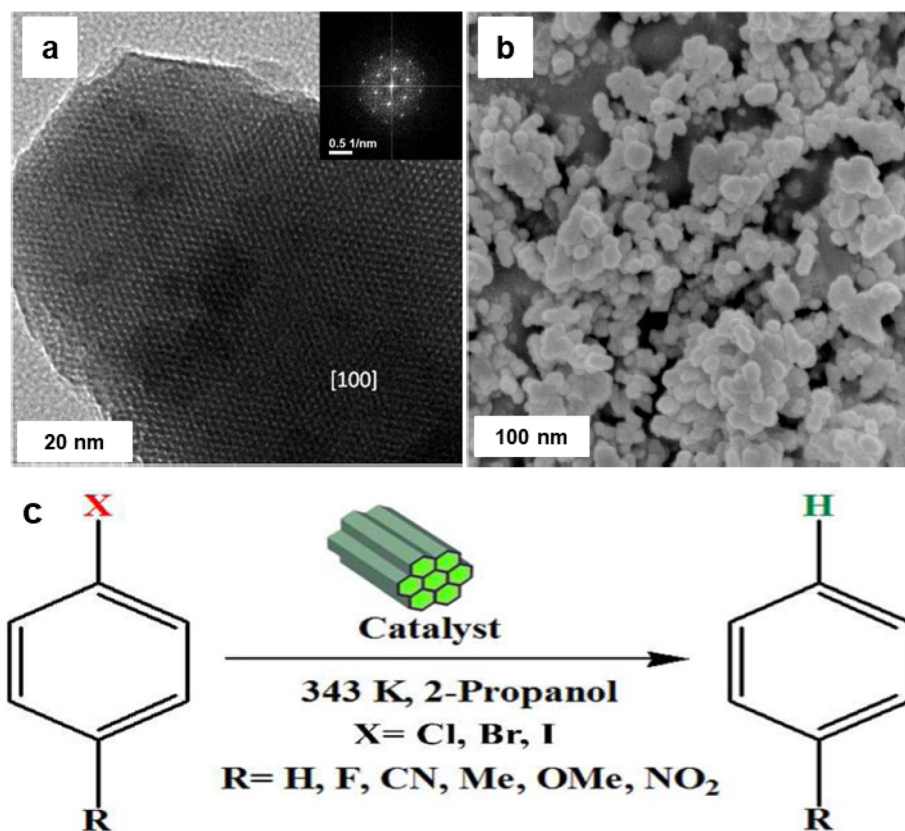
Aromatic and aliphatic halogenated chemicals are essential to the pharmaceutical industry and fine chemical synthesis, but because of their potential harm to the environment and human health, they must be used responsibly and disposed of appropriately. Regulatory frameworks and industry practices are adapting for more sustainable chemical and pharmaceutical production. Metal NPs play a key role in removing halogenated disinfection byproducts, aiding environmental remediation.<sup>305</sup> In this context, a precisely structured mesoporous metal oxide material named MFT-1 consisting of  $\text{TiO}_2$ - $\text{Fe}_2\text{O}_3$  was prepared using sodium dodecyl sulfate as a structured-directing agent by sol-gel method.<sup>306</sup> The HRTEM and FFT image of mesoporous  $\text{TiO}_2$ - $\text{Fe}_2\text{O}_3$  (MFT-1) catalyst revealed a highly ordered two-dimensional (2D) hexagonal mesophase with a 6-fold symmetry (Fig. 51a). The FESEM image showed that the sample consists of small spherical NPs around 40 nm in diameter (see Fig. 51b). This mesoporous MFT-1 catalyst exhibited good catalytic performance in dehalogenation of aryl iodides, bromides, and chlorides, even in the presence of functional groups like -F, -CN, -CH<sub>3</sub>, -OCH<sub>3</sub>, and -NO<sub>2</sub> (see Fig. 51c). This material offers a promising avenue for the development of sustainable technologies in the treatment and remediation of halogenated organic compounds.

In a similar context, a new approach was deployed for the hydro-dehalogenation of haloaromatic compounds, utilizing

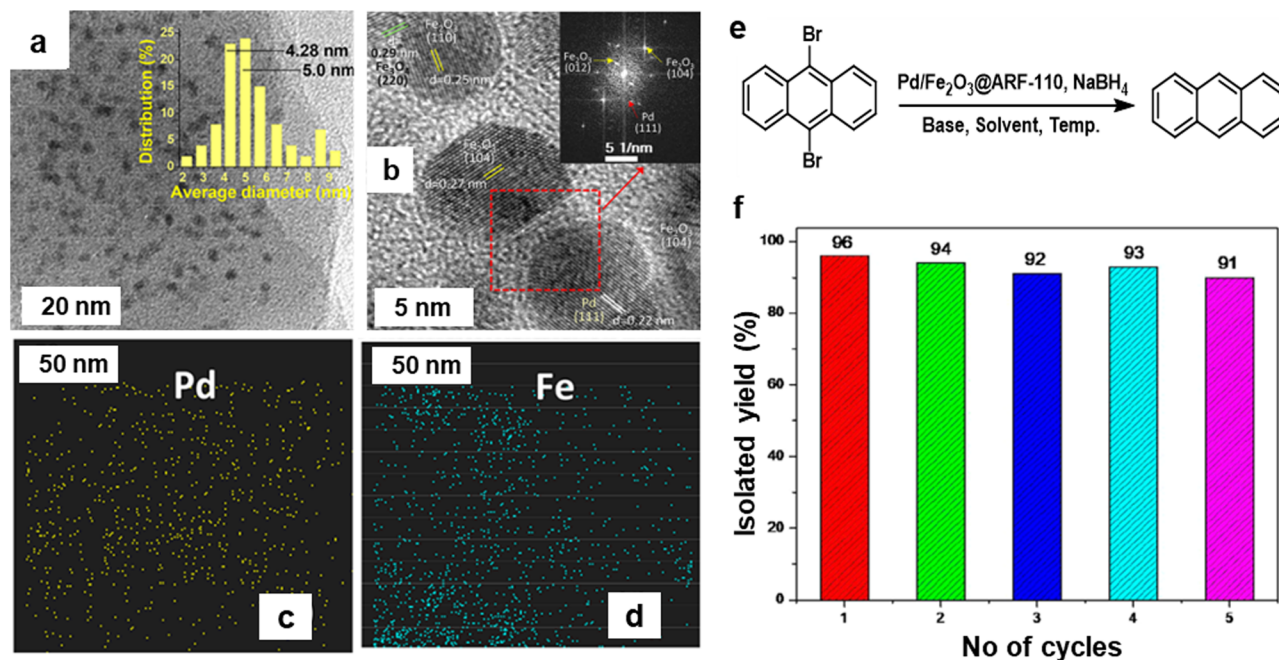
$\text{Pd}/\text{Fe}_2\text{O}_3$  nanohybrids anchored on Amberlite resin ( $\text{Pd}/\text{Fe}_2\text{O}_3@\text{ARF-110}$ ).<sup>129</sup> The HRTEM image and energy-dispersive X-ray spectroscopy (EDS) analysis confirmed that the crystalline Pd and  $\text{Fe}_2\text{O}_3$  NPs, with an average dimension of about 4–5 nm, coexisting within the resin matrix with a molar ratio approximately equal to 1 : 1 (see Fig. 52a–d). The arrangement of Pd and  $\text{Fe}_2\text{O}_3$  NPs on the polymer surface was optimized to boost the catalytic activity, showing potential for addressing persistent organic pollutants (POPs). Effective electron exchange between the iron oxide and palladium NPs aids in breaking B–H bonds of  $\text{NaBH}_4$ , resulting in the generation of active hydrogen and impressive catalytic efficiency. Particularly, the  $\text{Pd}/\text{Fe}_2\text{O}_3@\text{ARF-110}$  nanocomposites showed outstanding performance in dehalogenating various haloaromatic compounds (see Fig. 52e). Moreover, the heterogeneous  $\text{Pd}/\text{Fe}_2\text{O}_3@\text{ARF-110}$  catalyst attests to be conveniently separable and recyclable, exhibiting nearly identical efficiency over five consecutive runs (see Fig. 52f).

### 3. Nanosized iron oxides in environmental applications

Starting with the industrial revolution in the late 18<sup>th</sup> century and beginning of 19<sup>th</sup> century, a boom in the anthropogenic



**Fig. 51** (a) HRTEM image of MFT-1, FFT image is shown in the inset; (b) FESEM image of MFT-1 (c) Dehalogenation reaction using MFT-1 nanocatalyst. Reproduced with permission from ref. 306 Copyright 2012, American Chemical Society.



**Fig. 52** (a, b) HRTEM images of Pd and Fe-oxide NPs; (c, d) EDS elemental mapping of Pd and Fe respectively; (e) Hydrodebromination of 9,10-dibromoanthracene employing Pd/Fe<sub>2</sub>O<sub>3</sub>@ARF-110 nanohybrids (f) Recycle study of Pd/Fe<sub>2</sub>O<sub>3</sub>@ARF-110 catalyst. Reproduced with permission from ref. 129 Copyright 2019, American Chemical Society.

activities including mining, heavy industry, metallurgy, textile manufacture, production of chemicals, agriculture, steam power, *etc.* had a severe impact on environment. Air, water, and soil were contaminated with toxic inorganic and organic compounds with a little effort to decrease pollution and/or treat the affected environment. During 19<sup>th</sup> century, several laws have been introduced in big cities such as London and Paris to inflict companies polluting air and water; however, these laws and regulations were not strictly obeyed. In the 20<sup>th</sup> century, the human race witnessed increase in automobile industry, armament industry, industrial chemistry, pharmaceutical industry, plastic industry, electronics, energy production, transportation, and nuclear science, representing additional sources of pollution. The issue of atmospheric pollution was firstly brought to public attention after the World War II with worries caused by information about radioactive fallout from atomic testing and conflict. In the 1970s, several ecological movements were established to force governments of developed countries to limit pollution of the environment. Currently, the problem of pollution is addressed worldwide by international and local advisory and executive boards introducing regulations and laws in the area of pollution limits and protection of the environment with law suits and penalties. The protection of the environment constitutes a topic of utmost importance and is heavily discussed within the scientific community over the broad spectrum of fields.

Over the past five decades, substantial emphasis has been placed on the issue of water pollution which is frequently identified as prominent worldwide contributor to fatalities and diseases. The water contaminants include a broad portfolio of in-

organic, organic, and biological compounds/entities such as heavy metals, nitrates, phosphates, arsenates, ammonia, pharmaceutical drugs, surfactants, endocrine disrupting chemicals, antibiotics, hormones, perchlorate, chlorinated solvents, volatile organic substances, detergents, and pathogens, to name a few. Diverse methodologies have been introduced for water treatment including physical, chemical, and biological processes and their combinations. Currently, nanotechnology strategies are regarded as promising alternatives to complement or substitute traditional water treatment technologies as they often offer enhancement in the effectiveness of the treatment process, are environmentally friendly and, to some extent, low-cost.

Many efforts have focused on treatment of outer and underground water which are the source of potable water through which toxic pollutants enter the human body. Various techniques have been suggested for treatment of surface and underground water such as adsorption, exchange of ion, reverse osmosis, membrane filtration, photo-oxidation and Fe/Mn removal processes and their combinations. Among a long list of traditionally used materials and specifically designed nanostructures, iron oxides, especially in the form of NPs, hold a paramount position due to relatively high abundance, availability in nanosized forms *via* a diversity of sophisticatedly controlled chemical pathways, high surface area, robustness, eco-friendly attributes, and cost-effectiveness. Herein, the focus has been on environmental uses of iron oxide nanomaterials in sewage treatment, magnetic separation, photocatalytic applications, and activation of hydrogen peroxide and their use as supports *via* immobilization of biomaterials and enzymes (see Fig. 53).<sup>13,71,307–313</sup>



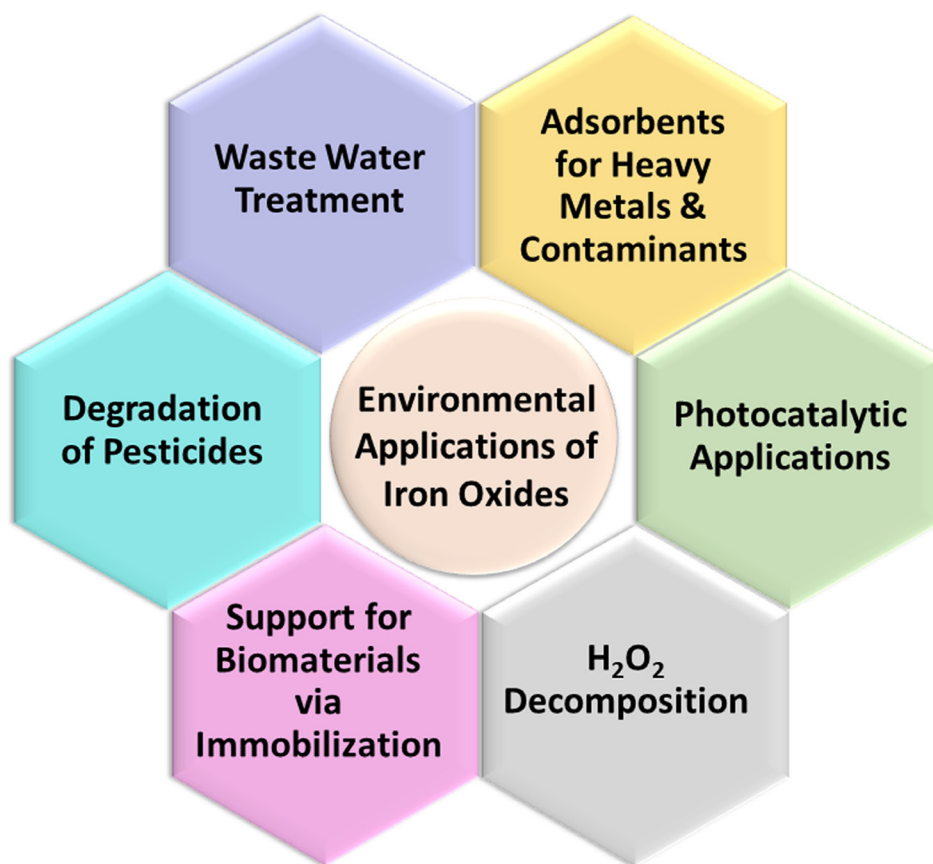


Fig. 53 Examples of environmental applications of iron oxide nanomaterials.

### 3.1. Iron oxide nanomaterials for wastewater treatment

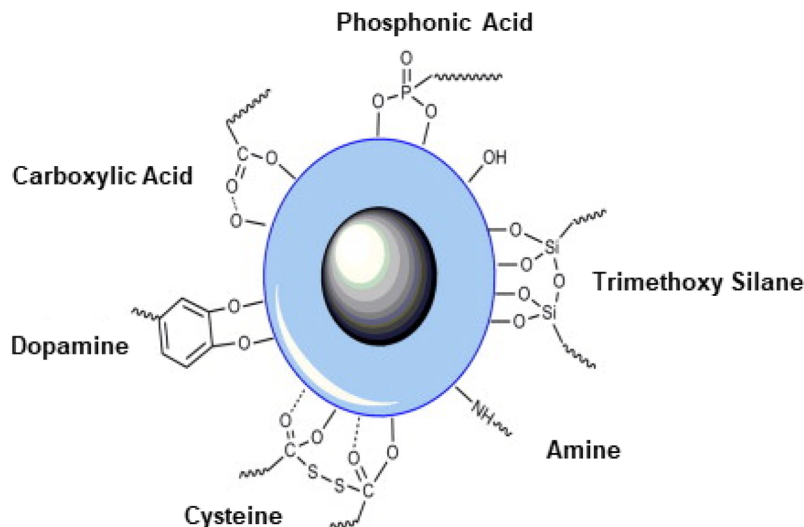
Due to worrying prognosis of the chronic shortage of drinking water around the globe in near future, an eminent scientific interest is devoted to the development and advancement of wastewater treatment technologies, especially using iron oxide nanoparticles.<sup>71,311,314,315</sup> Their distinct features such as greater surface area, excellent magnetic behavior and response to external magnetic fields, non-toxicity, biocompatibility, and biodegradability, rank them among most promising materials employed for waste water treatment. Numerous environmental and sustainable purification methods have been developed for sewage processing, which commonly exploit iron oxide nanoparticles as nanosorbents. The most recent applications in sewage processing and the knowledge gaps that restricts their extensive applications are delineated here.

The steadiness of iron oxide nanomaterials can be significantly enriched through modifying the surface with appropriate functional units, such as amine, cysteine, carboxylic and phosphonic acid (see Fig. 54).<sup>316,317</sup> Several options exist for adornment of various functional groups onto iron oxide NPs surface, still search for a robust protocol is continually being explored. It is important to highlight that the usage of iron oxide nanoparticles is strongly linked with their natural pro-

perties, which are dictated by immobilized entities on their surface.

**3.1.1. Iron oxide nanosorbents for heavy metal contaminants.** Contamination of a heavy metal is a chronic problem because of its toxic effects on human beings, plants, and animals; therefore, successful remediation protocols for the heavy metals are urgently sought. In recent years, the utilization of nanomaterials for sewage processing involves carbon nanotubes,<sup>318,319</sup> activated carbon,<sup>320</sup> mixed aluminum/iron hydroxides,<sup>321</sup> graphene-based macrostructures,<sup>322</sup> supported magnetic nanomaterials,<sup>323–325</sup> and zero-valent iron.<sup>326–328</sup> Although all these (nano)materials exhibit their own advantages/disadvantages; magnetic iron oxide NPs are viewed as the most potential tools for heavy metal treatment with an additional value of magnetic separation.<sup>329,330</sup>

The numerous techniques have been adopted for the elimination of heavy metal ions from industrial wastewater includes adsorption, nanofiltration, exchange of ion, electro-dialysis, and chemical precipitation.<sup>331</sup> Among these approaches, adsorption is the elegant because of its greatest effectiveness, ease of use and minimal costs.<sup>332</sup> Here, iron oxide NPs are broadly used owing to their great performance and sustainable properties.<sup>333</sup> A variety of iron oxide NPs varying in particle size, PSD, morphology, structure, and aggregation degree have been successfully designed *via* diverse pro-



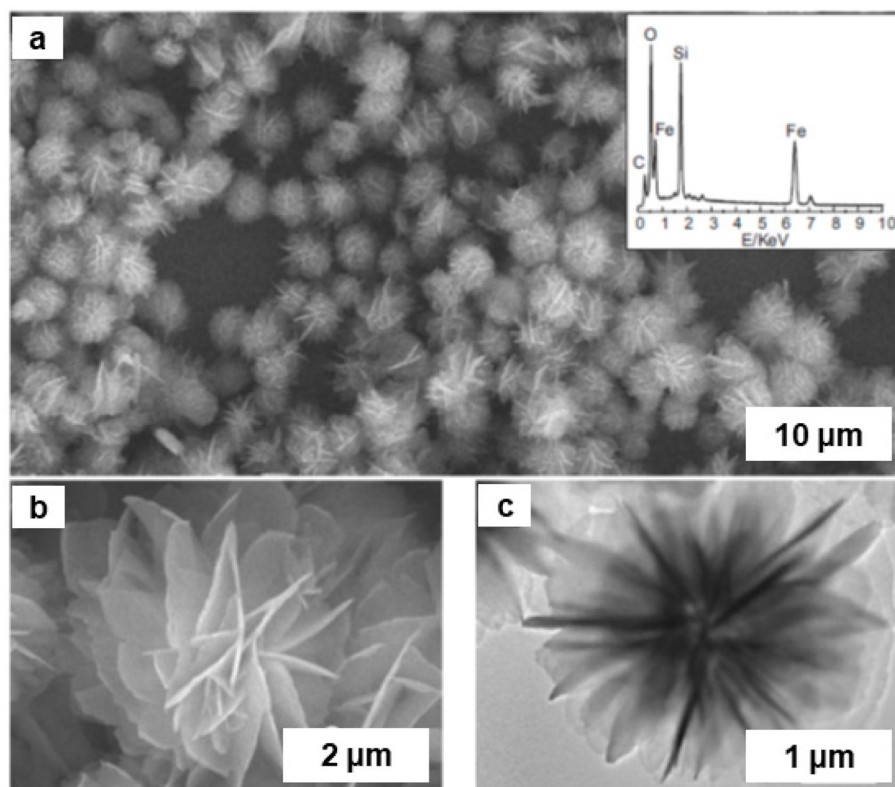
**Fig. 54** Immobilization of polymers and functional groups on the iron oxide NPs surface. Reproduced with permission from ref. 317 Copyright 2010, Elsevier.

protocols to improve their adsorption performances.<sup>334–338</sup> In general, heavy metal ions withdrawal by sorption relies on the degree of oxidation of the heavy metal, adsorption capability of the sorbent against these species, pH of the solution, sorbent-to-heavy metal ratio, and salts and molecules present in the aqueous phase that can compete for adsorption sites. Therefore, an effective approach to improve the removal efficacy is to adjust the size, structure, and physiochemical properties of the sorbent or the degree of oxidation of heavy metal species at the time of their withdrawal.

For heavy metal ions, these unique characteristics of iron oxide nanoparticles with diverse morphologies and three-dimensional (3D) structures show greater adsorption ability as compared to the bulk counterparts (see Fig. 55).<sup>339,340</sup> Although several types of 3D iron oxides nanoparticles comprising  $\text{Fe}_3\text{O}_4$ ,  $\alpha\text{-Fe}_2\text{O}_3$ ,  $\alpha\text{-FeOOH}$ , and  $\gamma\text{-Fe}_2\text{O}_3$  have been successfully synthesized by various methods,<sup>339–343</sup> the assembly of 3D iron oxides with higher adsorption potential for heavy metal ions remains a substantial challenge. Cui *et al.*<sup>344</sup> have documented the fabrication of 3D Mn doped  $\alpha\text{-Fe}_2\text{O}_3$  porous nano-system engineered by calcination of carbon spheres including  $\text{Fe(II)}$  and  $\text{Mn(II)}$  ions. This synthesis was achieved by hydrothermally treating the mixture of glucose,  $\text{Fe(II)}$ , and  $\text{Mn(II)}$  ions. The prepared and well-characterized iron oxide nanostructures show greater capabilities for elimination of  $\text{Pb(II)}$ , As (III), and  $\text{Cr(VI)}$ , ions from wastewater. Nassar and co-workers<sup>345</sup> have observed maximum adsorption performance ( $36.0 \text{ mg g}^{-1}$ ) for  $\text{Pb(II)}$  ions with  $\text{Fe}_3\text{O}_4$  nanoparticles. It was proposed that the smaller sized  $\text{Fe}_3\text{O}_4$  nanosorbents were promising for distribution of metal ions onto the adsorbent's surface, thus rendering them useful for extraction and retrieval of metal ions from wastewater. Despite that the extremely significant surface-forced phenomena in water medium, aggregation, induced by high surface area to volume ratios of nanoparticles, may impede various imperative environmental processes,

along with ion uptake.<sup>346</sup> Besides aggregation, numerous other interactions with ions could be invoked in wastewater, which could influence the adsorption of metals. In particular, the high concentration of phosphates in the wastewater can make it good adsorbent and even surpass metals for adsorption sites.<sup>347</sup> These causes along with the nature of the pollutants can confine the efficiency of nanosorbents, and consequently the investigation of considerably selective transformation protocols for nanomaterials is becoming a hot bed of research activity for enhancing the efficacy of nanosorbents.

Several interesting findings have been reported on heavy metal decontamination by iron oxide NPs and 3D type iron oxide nanostructures.<sup>339,340</sup> Arsenic (As) is classified as a carcinogen for humans and is viewed as one of the most toxic elements. The rising levels of arsenic in nature is an escalating problem that several nations currently face. Because of extreme health impacts on the population (irritation of the digestive tract, nausea, diarrhea, skin cancer, increased risk of cancers of the lung, kidneys, and liver), the influence on the health of humans significantly relies on the oxidized state of arsenic. Beside processes of natural origin such as weathering of rocks, artificial interferences like mining, utilization of arsenic containing toxicants, factory wastes, and inappropriate discarding chemical effluents heavily contribute to the increased levels of arsenic in nature.<sup>348</sup> Thus, to increase the performance of As extraction from the environment, engineered iron-oxide-based environmentally friendly materials<sup>349–351</sup> have been developed and examined. These materials comprise monodispersed  $\text{Fe}_3\text{O}_4$  nanocrystals,<sup>352</sup> hybrids of  $\text{Fe}_3\text{O}_4$  and rGO sheets,<sup>353</sup> thiol-functionalized iron oxide NPs,<sup>354</sup> (GO)/ $\text{Fe(OH)}_3$  composites,<sup>355</sup> high-surface area superparamagnetic  $\text{Fe}_3\text{O}_4$  NPs,<sup>356</sup> and superparamagnetic  $\gamma\text{-Fe}_2\text{O}_3$  nanoparticles with mesoporous nature of particle arrangement promoted by strong magnetic interparticle interactions.<sup>357</sup> Recently, a hypothesis has emerged suggesting that



**Fig. 55** (a) SEM image of the iron oxide NPs. Inset: EDX analysis; (b, c) SEM and TEM images of flowerlike iron oxide NPs respectively. Reproduced with permission from ref. 339 Copyright 2006, Wiley-VCH GmbH & Co. KGaA, Weinheim.

if the surface of Fe(III) oxide nanoparticles is functionalized with NaOH in liquid phase, new hydroxide reactive functional groups are generated which promotes increase in the ion exchange process, resulting in the enhancement of removal capacity towards arsenic species.<sup>358</sup>

A magnetic hybrid material fabricated by incorporating iron oxide NPs into a chitosan matrix with the assistance of eucalyptus extract as a reductant and utilized it for arsenic removal.<sup>359</sup> Bangari *et al.* synthesized magnetite-coated boron nitride nanocomposite for As(v) ion extraction from aqueous medium.<sup>360</sup> The diameter of the BNNS-Fe<sub>3</sub>O<sub>4</sub> nanocomposite (10–22 nm) was analyzed by HR-TEM analysis (Fig. 56a). The HAADF image display the uniform distribution of boron nitride on Fe<sub>3</sub>O<sub>4</sub> (Fig. 56b). The adsorption ability of BNNS-Fe<sub>3</sub>O<sub>4</sub> nanocomposite were higher relative to those of BNNS nanocomposites for As(v) ion removal (Fig. 56c). The several active sites in the BNNS-Fe<sub>3</sub>O<sub>4</sub> nanocomposite enhanced the percent removal than BNNSs nanocomposites; highest adsorption ability of both adsorbents being 0.2 g L<sup>-1</sup> (Fig. 56d). Recently, magnetite iron oxide NPs nanodevice coated with meglumine ligand by co-precipitation method were developed for the adsorption of heavy metals (As, Cr and B).<sup>361</sup>

If γ-Fe<sub>2</sub>O<sub>3</sub> nanoparticles are distributed on the CMK-3 surface, such a hybrid shows eminent capability to extract Cr(vi) from the aquatic medium<sup>362</sup> (Fig. 57). The synthesis method involves two steps: AcOH fumes react with an immobi-

lized Fe cation in the carbon matrix to generate an iron acetate intermediate, following by its pyrolysis to produce iron(III) oxide nanoparticles. Iron-oxide/carbon hybrids, combining organized forms of interlinked carbon rods, were reportedly displayed high specific surface areas ~1043 m<sup>2</sup> g<sup>-1</sup>, evenly immobilized γ-Fe<sub>2</sub>O<sub>3</sub> NPs with equal sizes (~20 nm) and superparamagnetic characteristics at RT. Because of the explicit surface characteristics of magnetic carbon hybrids and synergistic impact of both equivalents, these hybrids exhibited greater Cr(vi) extraction ability, which was significantly better compared to pure CMK-3 carbon.

Tuning the morphology and degree of porosity is frequently adopted as another approach to enhance the sorption capabilities of iron oxides as exemplified by the synthesis of α-Fe<sub>2</sub>O<sub>3</sub> in the form of very thin and porous nanofibers and its assessment for extraction of Cr(vi) from the aquatic environment.<sup>363</sup> Such α-Fe<sub>2</sub>O<sub>3</sub> nanofibers displayed greater adsorption efficiency (16.17 mg g<sup>-1</sup>), extraction rate, and excellent recovery without loss of performance; they can be recycled after centrifugation and treatment with diluted NaOH. The Cr(vi) species could be removed by a monolayer adsorption on the surface of porous α-Fe<sub>2</sub>O<sub>3</sub> nanofibers.

A single-step preparation of magnetic-silica nanoparticles by using alkaline sodium silicate solution has been reported by Gole and co-workers.<sup>364</sup> This methodology not only created iron oxide but simultaneously decorated Fe<sub>3</sub>O<sub>4</sub> nanoparticles



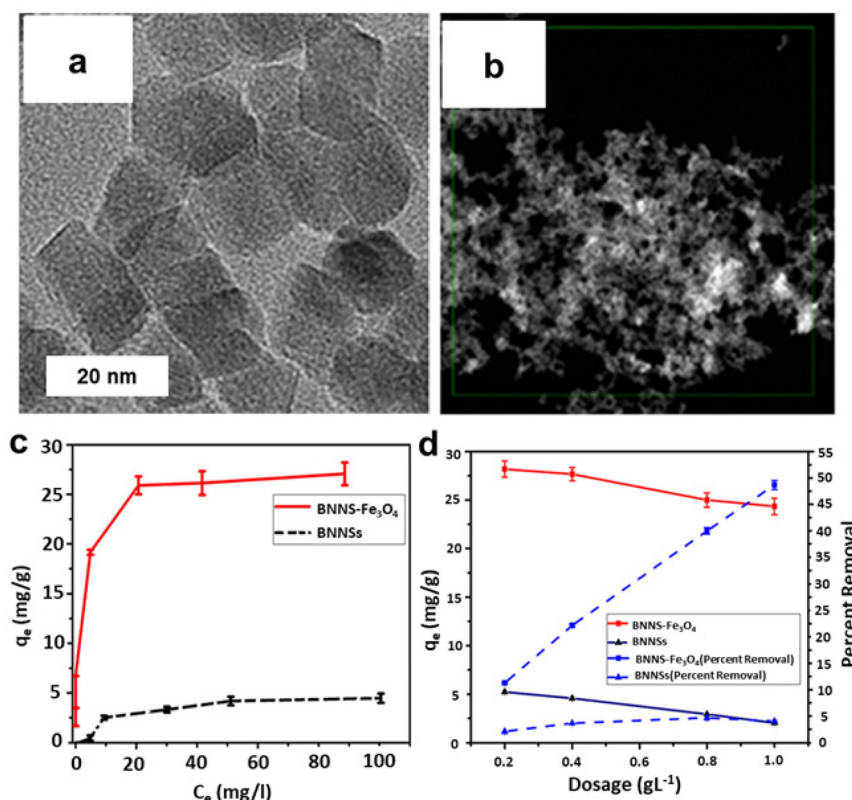


Fig. 56 (a, b) HR-TEM and HAADF image of BNNS-Fe<sub>3</sub>O<sub>4</sub> nanocomposite; (c) Adsorption isotherm of BNNSs and BNNS-Fe<sub>3</sub>O<sub>4</sub> nanocomposite; (d) Effect of adsorbent dose on As(v) ions removal. Reproduced with permission from ref. 360 Copyright 2019, American Chemical society.

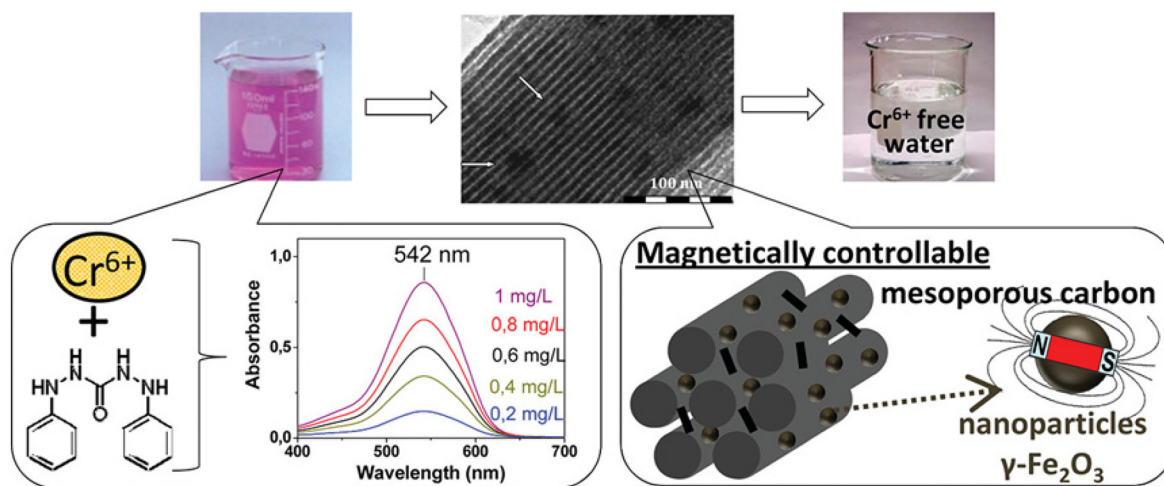


Fig. 57  $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>/CMK-3 hybrid for Cr(vi) extractions from aquatic solutions. Reproduced with permission from ref. 362 Copyright 2012, American Chemical Society.

with silica coating. The biocompatible and stable silica-shell magnetic nanoparticles serve as anchors for various functional groups; iron oxide-silica surface modified with 3-amino propyl triethoxy silane (APTES) are employed for tagging of Rhodamine B (Rh B) dye molecules (fluorophore tagging). The bare magnetic and silica-coated nanoparticles have been used

for the zinc loading and the utility of such nanocomposites have been explored for water purification by arsenic removal in the form of arsenate.<sup>364</sup>

Iron ferrite NPs<sup>365</sup> were synthesized *via* a biogenic strategy and utilized for the Pb(II) and Cr(III) heavy metal removal. The particle size (20–45 nm) of the magnetic inverse spinel iron

oxide nanoparticles (MISFNPs) was confirmed by TEM analysis (Fig. 58a) and the adsorption and desorption study suggested that the MISFNPs was stable and reusable up to four cycles (Fig. 58b). The adsorption percentage of the MISFNPs was higher relative to bulk  $\text{Fe}_3\text{O}_4$  because of the nano size and high surface area of the MISFNPs (Fig. 46d). The highest adsorption of  $\text{Pb(II)}$  and  $\text{Cr(III)}$  reached up to  $0.5 \text{ g L}^{-1}$  with increased NPs dosage and then decreased due to lower active sites (Fig. 58c). Pan *et al.*<sup>366</sup> reported iron oxide nanoparticles coated with organics and utilized them for the elimination of  $\text{Cr(VI)}$  from water. The DNA modified  $\text{Fe}_3\text{O}_4\text{@Au}$  magnetic NPs has been employed for the electrochemical detection of  $\text{Ag}^+$  and  $\text{Hg}^{2+}$ .<sup>367</sup>

A nanocomposite ( $\text{mPCS@Fe}_2\text{O}_3$ ) was prepared by combining mesoporous carbon sphere with  $\text{Fe}_2\text{O}_3$  and employed the catalyst to remove antimony (Sb) from wastewater.<sup>368</sup> The SEM images of mPCS and  $\text{mPCS@Fe}_2\text{O}_3$  revealed spherical morphology (Fig. 59a and b) and they were well dispersed on mPCS with particle size  $<6 \text{ nm}$ , as confirmed by HR-TEM studies (Fig. 59c and d). The adsorption kinetics suggested that the adsorption of Sb increased during its initial 40 min and afterwards, the adsorption attains equilibrium within 120 min (Fig. 59e). The co-existing anions contained in the Sb solution did not affect the removal of Sb metal. The  $\text{PO}_4^{3-}$  ion

slightly effected the Sb removal because of its similar structure to  $\text{Sb(III)}$  (Fig. 59f). Xiang *et al.*<sup>369</sup> reported carbon-supported zero valent Fe NPs for the photocatalytic extraction of  $\text{U(VI)}$  from sewage.

A magnetic  $\text{Fe}_2\text{O}_3/\text{AlO(OH)}$  nanocomposite was synthesized using a template-free route by utilizing ferrous sulphate and magnesium acetate. Initially, urchin-like lepidocrocite  $\gamma\text{-FeOOH}$  was prepared in single step, then  $\alpha,\gamma\text{-Fe}_2\text{O}_3$  was obtained *via* high temperature calcination and finally, the target compound was formed by immobilizing  $\alpha,\gamma\text{-Fe}_2\text{O}_3$  and  $\text{Al(NO}_3)_3 \cdot 9\text{H}_2\text{O}$  utilizing ultrasound-assisted chemical precipitation method<sup>370</sup> (Fig. 60a). The composite material comprising  $\text{Fe}_2\text{O}_3$  and  $\text{AlO(OH)}$  displayed admirable efficiency to extract heavy metal ions from drinking or wastewater.<sup>371,372</sup> The obtained hierarchical material exhibited superfast adsorption rates and greater adsorption performance for the extraction of  $\text{As(V)}$ ,  $\text{Cr(VI)}$  and  $\text{Pb(II)}$  ions from aquatic medium in 30 min; highest adsorption extents being  $37.45 \text{ mg g}^{-1}$ ,  $21.6 \text{ mg g}^{-1}$ , and  $29.55 \text{ mg g}^{-1}$ , respectively. Notably,  $\text{Fe}_2\text{O}_3/\text{AlO(OH)}$  materials displayed excellent recyclability for  $\text{As(V)}$  removal, even after three cycles 75% adsorption rate was retained. The high activity and recyclability could be because of the extensive surface area of the materials and special morphology of  $\text{Fe}_2\text{O}_3\text{@AlO(OH)}$ <sup>370</sup> (Fig. 60b). It is speculated that

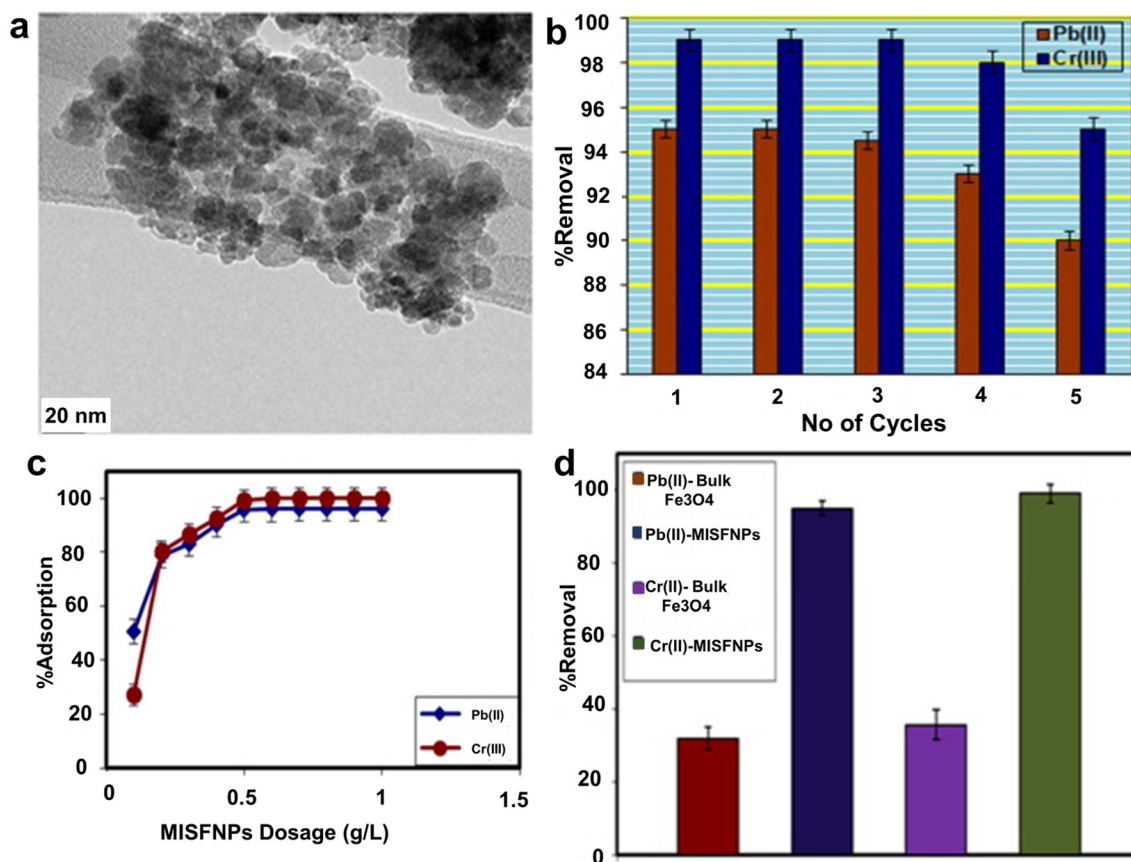
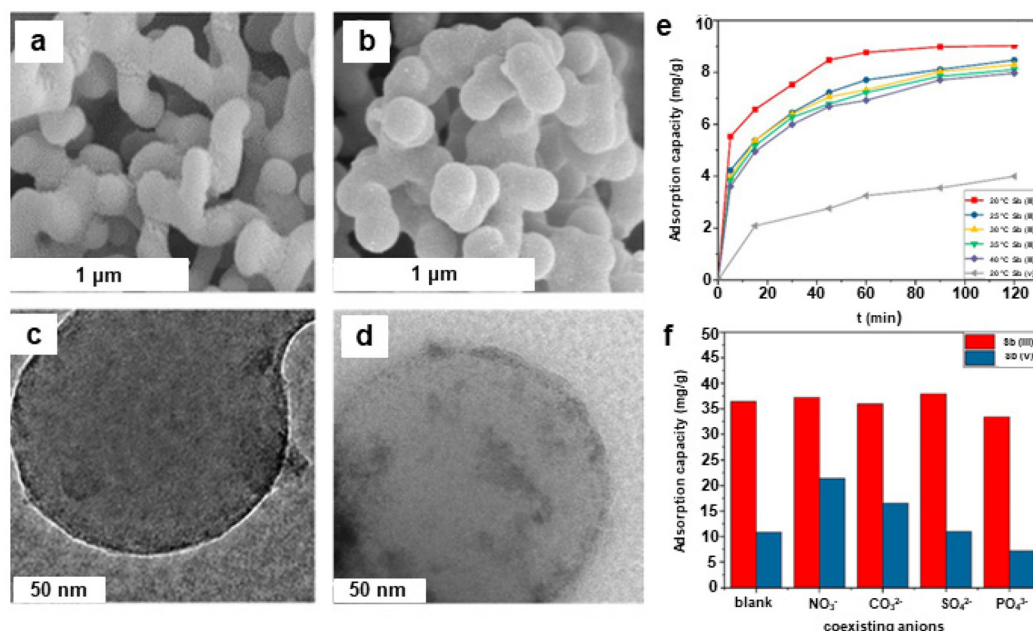


Fig. 58 (a) HR-TEM images of MISFNPs; (b) Study of the stability and reusability of the MISFNPs; (c) Adsorption activity; (d) Effect of MISFNPs dosage on  $\text{Pb(II)}$  and  $\text{Cr(III)}$  adsorption. Reproduced with permission from ref. 365 Copyright 2016, Elsevier.



**Fig. 59** (a, b) SEM images of mPCS and mPCS@ Fe<sub>2</sub>O<sub>3</sub>; (c, d) HR-TEM images of mPCS@ Fe<sub>2</sub>O<sub>3</sub> and mPCS@ Fe<sub>2</sub>O<sub>3</sub>/Sb(III) catalysts respectively; (e) Kinetic curves for the extraction of Sb; (f) Impact of present anions on adsorption of Sb. Reproduced with permission from ref. 368 Copyright 2018, American Chemical Society.

this inexpensive and benign synthetic approach for Fe<sub>2</sub>O<sub>3</sub>@AlO(OH) nanomaterial might be useful for other types of environmental applications.

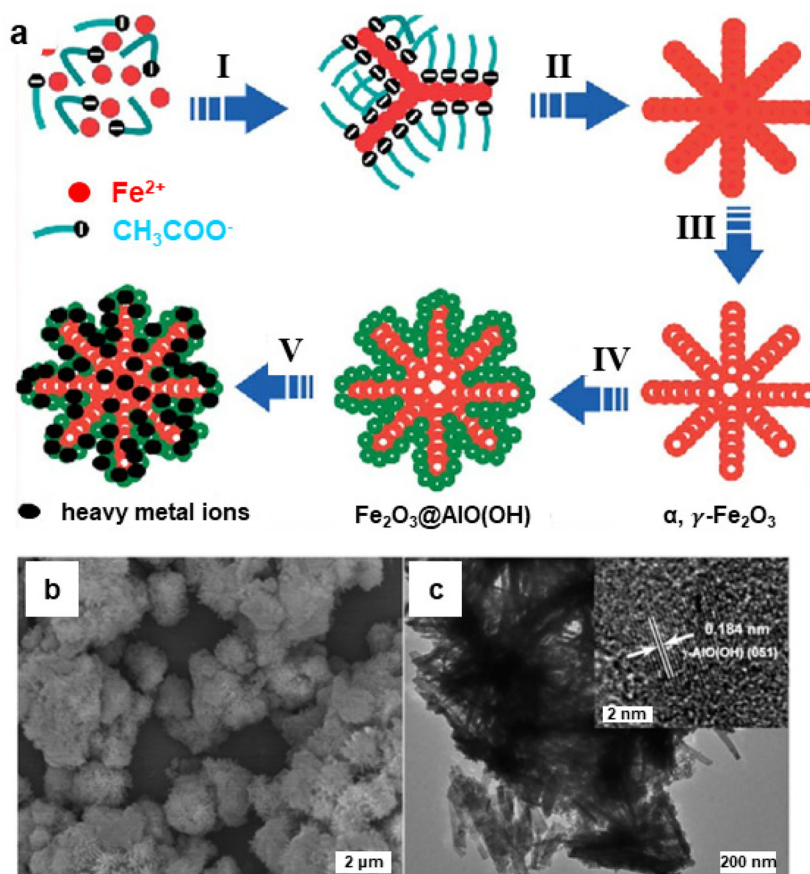
The growing universal need for pure and clean water coerces the research experts to discover functional processes for drinking water production.<sup>373,374</sup> Among these, membrane filtration is one of the most efficient and simple pathways to deliver high-quality of safe drinking water. Nevertheless, membrane fouling is the greatest drawback that inhibits the widespread utilization of membrane process. A new type of membrane, created from interwoven Fe<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub> nanowires (FeTi-NWM) has been reported<sup>375</sup> with anti-fouling ability for humic acid (HA) removal from water. TiO<sub>2</sub> and iron oxide nanowires were employed to make TiO<sub>2</sub> nanowires by a filtration and hot-pressing technique (Fig. 61). HA is a primary contaminant responsible for the fouling of membranes in water treatment processes.<sup>376</sup> A stainless-steel reactor housing nanowire-membrane based circulating water filtration technique was introduced.<sup>376</sup> The ensuing results revealed that under solar illumination the FeTi-NWM accomplished nearly complete HA extraction within 2 h short-term trial at a starting HA concentration of 200 mg L<sup>-1</sup>, which is comparable with HA extraction by Ti-NWM (89%). After long-term trial of 12 h, the FeTi-NWM displayed 98% HA abstraction, though the Ti-NWM could show only 55% extraction at the end. The enhanced HA removal provided by FeTi-NWM relative to Ti-NWM and its exceptional anti-fouling potential under solar light illumination can be ascribed to: (i) an improved absorption of HA by iron oxide nanowires and (ii) the created Fe<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> heterojunctions that enhances the photo-induced charge transfer

and enhance visible light performance. Outstandingly, in comparison to Ti-NWM without Fe<sub>2</sub>O<sub>3</sub> nanowires, FeTi-NWM displayed greater HA extraction.

**3.1.2. Carbon-supported iron oxide nanoparticles for water purification.** Recently, graphene/iron oxide nanocomposites explored as efficient nanosorbents in water purification technologies.<sup>377</sup> Magnetite-reduced graphene oxide (M-RGO) composites containing low concentration of magnetite (M1-RGO) and high concentration of magnetite (M2-RGO) were effectively deployed to extract As(III) and As(V) from contaminated water.<sup>353</sup> M-RGO superparamagnetic composites were synthesized through a chemical reaction and the TEM image of M-RGO (Fig. 62a) showed properly distributed magnetic nanoparticles in the RGO matrix having the average particle size of 11 nm, and the graphene sheets displayed the folding environment. The HRTEM image (Fig. 62b) depicts the lattice fringes from Fe<sub>3</sub>O<sub>4</sub> NPs in the nearby of the RGO matrix. Different concentrations of As, ranging from 3 to 7 ppm, were employed for the experiments (Fig. 62c) and maximum adsorption capacity for As ions was established (Fig. 62d). It was observed that the extraction of As by using M2-RGO is superior when compared to M1-RGO; the fact confirming the principal effect of magnetite nanoparticles in arsenic removal.

The surface area, temperature, and pH of the contaminated solution determine the ultimate adsorption capacity.<sup>378</sup> Certain supplementary additives boost the adsorption as shown by Luo *et al.*<sup>379</sup> for As(III) and As(V) ions, where the inclusion of MnO<sub>2</sub> with the magnetite/graphene material helps for the oxidation of As(III) to As(V) without any additives. As(V) was firmly absorbed at pH ranging from 2 to 10 which





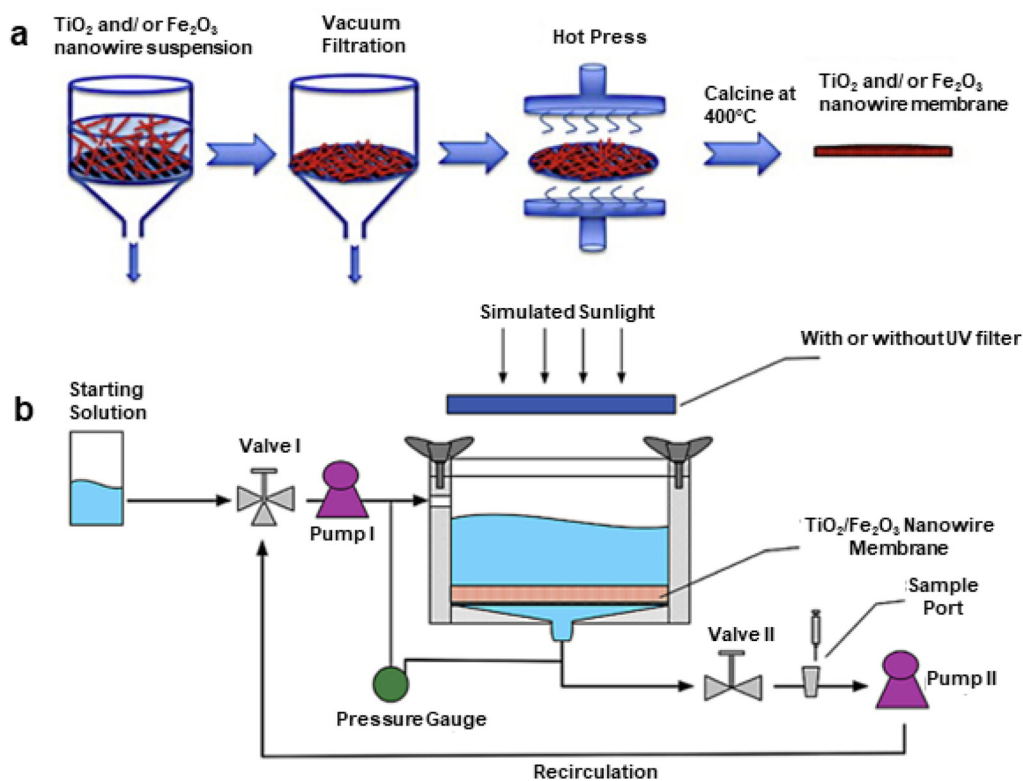
**Fig. 60** (a) Schematic illustration of the preparation of  $\text{Fe}_2\text{O}_3@\text{AlO}(\text{OH})$  hierarchical porous structure; (I) generation of nucleation centers; (II) nano-crystal development and directed linking to 3D urchin-like  $\gamma\text{-FeOOH}$  superstructure; (III) calcination and generation of porous magnetic  $\alpha, \gamma\text{-Fe}_2\text{O}_3$ ; (IV) formation of mesoporous  $\gamma\text{-AlO}(\text{OH})$  from  $\alpha, \gamma\text{-Fe}_2\text{O}_3$ ; (V) adsorption of heavy metal ions from aquatic media; (b, c) SEM images of  $\text{Fe}_2\text{O}_3@\text{AlO}(\text{OH})$ . Reproduced with permission from ref. 370 Copyright 2013, The Royal Society of Chemistry.

was not the case for the basic magnetite/graphene which afforded stable adsorption at lower pH range. Similarly, the addition of ZnO in maghemite/graphene composite, enhanced the decomposition of methylene blue (MB) with a high efficacy (95%) and was consistently effective after 5 cycles as shown by Kumar and co-workers.<sup>380</sup> The endocrine disruptors like dibutyl phthalate, bisphenol A, atrazine, and 1-naphthol, could be actively eliminated (85–100%) from contaminated aqueous streams by using graphene/ $\text{Fe}_2\text{O}_3$  based nanocomposites prepared by simple method.<sup>381</sup> These materials are well suited for the adsorption of endocrine disruptors from water due to the large surface area and an exposed graphene surface. Although synthetic steps for the hybrids containing graphene sheets and core/double shell NPs of  $\text{Fe}/\text{Fe}_2\text{O}_3/\text{Si-S-O}$  type were involved but they were found to be active in the extraction of  $\text{Cr}(\text{VI})$ .<sup>382</sup> The  $\text{Fe}/\text{Fe}_2\text{O}_3/\text{Si-S-O}$  material was prepared by thermo-decomposition procedure having a core@double-shell arrangement of the NPs with Fe as the core,  $\text{Fe}_2\text{O}_3$  as the first shell and amorphous Si-S-O material as the second shell (Fig. 63). This iron oxide based graphene nanomaterial displayed extremely quick extraction of  $\text{Cr}(\text{VI})$  from the sewage. Importantly, the material was retrievable for several

runs and it can be employed to treat solutions with lower pH levels which make it ideal material to eliminate the heavy metals from wastewater.

The size and morphology of modified NPs can contribute to the design of the magnetic graphene nanocomposites with unique characteristics, such as electroconductivity, flexibility, higher magnetic resistance, negative permittivity, and superparamagnetism.<sup>383–385</sup> The propensity of these materials to organic compounds and ions has also been used in sensing applications. More importantly, it offers suitable conditions for the immobilization of biomolecules like hemoglobin,<sup>386</sup> horseradish peroxidase<sup>387</sup> and such materials could be used for the detection of  $\text{H}_2\text{O}_2$  at low sensing limits of  $\sim 0.5 \mu\text{M}$ . These type of materials have also been employed for the extractions of numerous heavy metal ions such as  $\text{Cr}(\text{VI})$ ,<sup>388,389</sup>  $\text{U}(\text{VI})$ <sup>390</sup> and  $\text{Co}(\text{II})$ <sup>391</sup> and organic constituents including tetracycline,<sup>392</sup> 1-naphthol, 1-aminonaphthalene, methylene blue,<sup>393</sup> polychlorinated biphenyls, polyaromatic hydrocarbons, phthalates,<sup>394</sup> ciprofloxacin, and norfloxacin.<sup>395,396</sup>

**3.1.3. Iron oxide nanosorbents for organic contaminants.** Various studies have been performed to remove organic contaminants by using iron oxide nanomaterials.<sup>397–402</sup>  $\text{Fe}_3\text{O}_4$



**Fig. 61** (a) Schematic representation of process of synthesis of Ti-NWM and FeTi-NWM; (b) Schematic representation for water filtration process for HA extraction through nanowire membranes under sunlight irradiation. Reproduced with permission from ref. 375 Copyright 2015, Elsevier.

hollow nanospheres have been documented as a potent sorbent for red dye extraction.<sup>323</sup> The saturation magnetization of magnetite nanospheres was detected to be  $42 \text{ emu g}^{-1}$ , satisfactory enough for separation with magnet, thus demonstrating its viability. Similar to the adsorption of heavy metals, the adsorption of organic pollutants occurs *via* interchanging of surface until the functional surface sites are entirely filled, after which pollutants could disperse into the adsorbent for functional group interactions.<sup>403</sup>

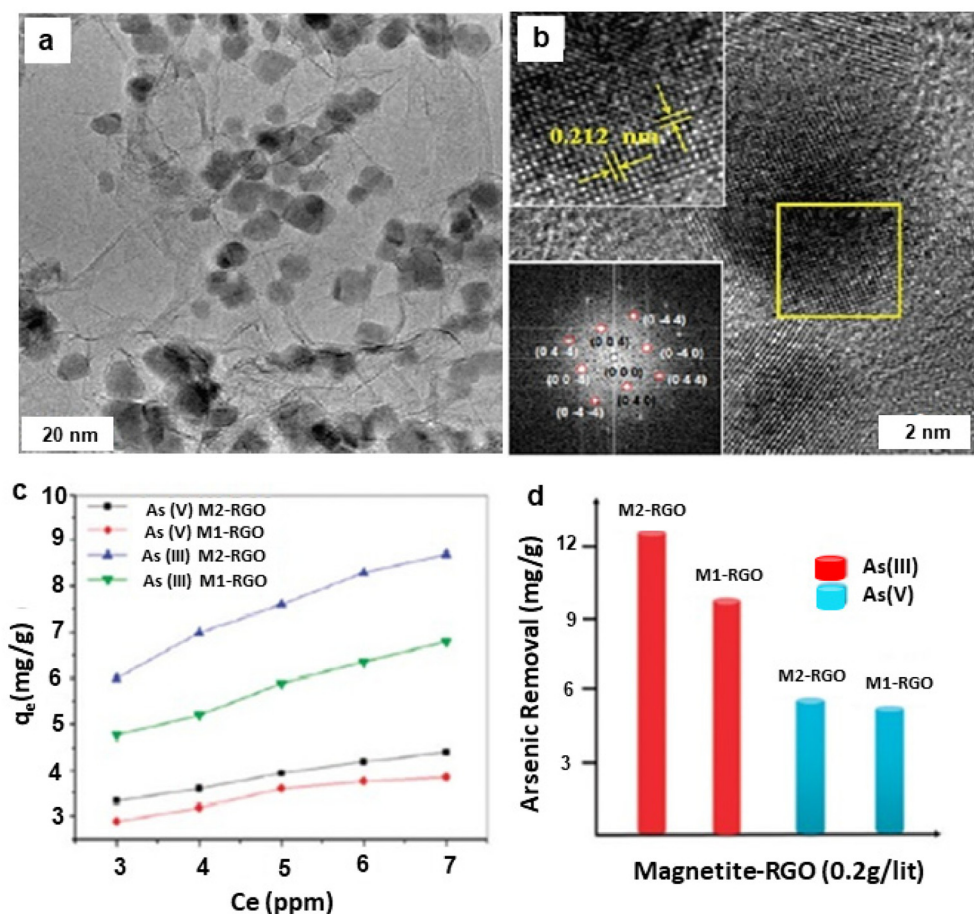
Mixed composite of nanocrystalline  $\gamma\text{-Fe}_2\text{O}_3$  and cerium oxide ( $\text{CeO}_2/\gamma\text{-Fe}_2\text{O}_3$ ) was developed for the decomposition of organophosphorus pesticides, parathion methyl, and the chemical fighting agent, soman, and nerve agents, VX.<sup>404</sup> The composite was prepared by simple reverse co-precipitation process in which  $\text{Fe(III)/Fe(II)}$  salts with aq.  $\text{NH}_3$  was employed for the preparation of  $\text{Fe}_3\text{O}_4$  core, with further precipitation of  $\text{Ce}_2(\text{CO}_3)_3$  on the surfaces of  $\text{Fe}_3\text{O}_4$  (again in the reversed mode); calcination finally delivered cerium oxide while  $\text{Fe}_3\text{O}_4$  got converted to  $\gamma\text{-Fe}_2\text{O}_3$  (Fig. 64).<sup>404</sup>

HR-TEM confirmed the existence of  $\text{CeO}_2$  nanoparticles decorating the  $\gamma\text{-Fe}_2\text{O}_3$  surface (Fig. 64a). The phase combination of the reactive sorbents produced at distinct temperatures is depicted in Fig. 64b. Increase in calcination temperature decreased the SSA and pore volume, and significant modifications occurred at 500 and 700 °C temperature range (see Fig. 64c). Degradation efficiencies were assessed by a test in 2 h using all types of sorbents; correlation of the degradation

efficacy on the calcination temperature was discerned at 300 °C (see Fig. 64d). The highest efficacy was obtained using sorbents annealed at temperatures  $<500$  °C, and the phosphatase-like performance lowered with rise in annealing temperature (see Fig. 64e). In general,  $\text{CeO}_2/\gamma\text{-Fe}_2\text{O}_3$  nanomaterials synthesized at temperatures of 300–400 °C displayed the higher decomposition performance without any change in its magnetic properties.<sup>404</sup>

Xiong *et al.*<sup>405</sup> described the preparation of nanocomposites comprising cellulose and iron oxide NPs by co-precipitation employing ionic liquid (IL) as co-solvent; as-synthesized  $\gamma\text{-Fe}_2\text{O}_3$  NPs exhibited uniform particle size distribution. The individual adsorption capacities of cellulose@ $\gamma\text{-Fe}_2\text{O}_3$ , pure  $\gamma\text{-Fe}_2\text{O}_3$  and IL processed cellulose were investigated, and cellulose@ $\gamma\text{-Fe}_2\text{O}_3$  was found to be the best candidate.<sup>405</sup> The adsorption ability of nanospheres for the withdrawal of  $\text{Pb(II)}$  and Methylene Blue (MB) were 21.5 and  $40.5 \text{ mg g}^{-1}$ , respectively which is comparable to the other reported magnetic materials. Additionally, utilizing an external magnet, magnetic nano-adsorbent could be easily recycled. The excellent removal capacities render the cellulose@ $\gamma\text{-Fe}_2\text{O}_3$  as extremely capable nano-adsorbent for water treatment. In a similar context, magnetic iron oxide nanosorbent, and polymer functionalized nanoparticles were utilized for MB adsorption.<sup>406–408</sup>

Water bodies confront pollution from iodinated contrast media (ICM), primarily released by pharmaceutical companies.<sup>409</sup> The microbial processes involved in organohalide res-



**Fig. 62** (a, b) TEM and HR-TEM images of M-RGO (inset: SAED pattern); (c) adsorption isotherms over the  $\text{Fe}_3\text{O}_4$ -RGO composite; (d) maximal adsorption ability of M-RGO composites for the extraction of As from water. Reproduced with permission from ref. 353 Copyright 2010, American Chemical Society.

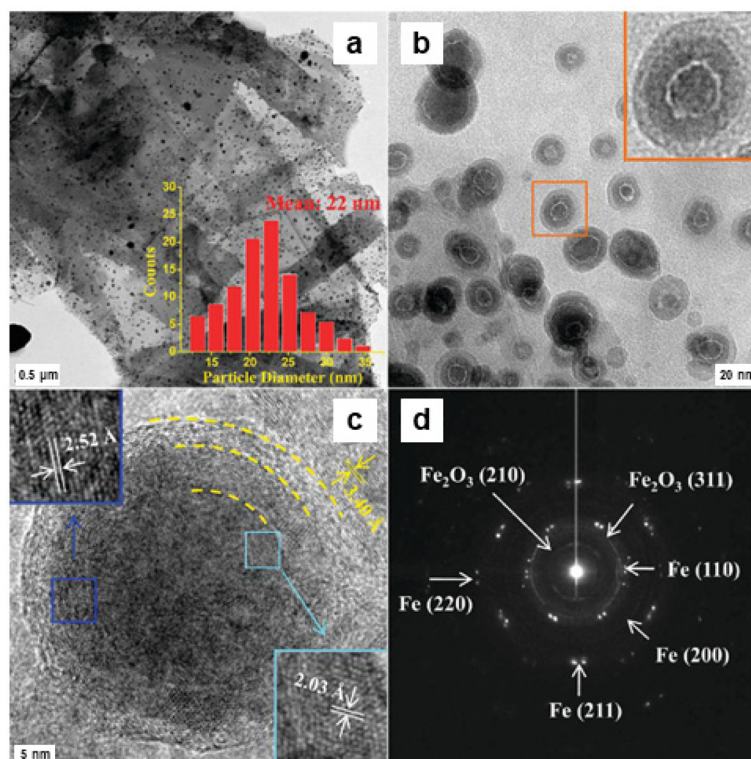
piration are essential for developing effective bioremediation strategies and promoting the sustainable cleanup of sites contaminated with chloroethene.<sup>410</sup> To tackle this problem, the reductive dehalogenation of trichloroethene (TCE) has been scrutinized using aquifer material rich in iron oxides in a continuous flow column.<sup>411</sup> The study observed sustained dehalogenation effectiveness over a period of 1000 days of column operation. In a similar context, recent research employed nanoscale zero-valent iron (nZVI) for the reduction-based removal of halogens, specifically focusing on the iodinated contrast medium diatrizoate (DTA).<sup>412</sup> The study reported a 100% removal efficiency of diatrizoate (DTA) within a 24-hour timeframe.

The iron oxide NPs (17 nm) prepared by Chang *et al.*<sup>413</sup> was employed for the extraction of Reactive Black 5 (RB5, Azo dye) from polluted water in the textile industry. The adsorption of RB5 to iron oxide NPs was ascribed to electrostatic attraction and the highest withdrawal capacity was  $18 \text{ mg g}^{-1}$  at  $45^\circ\text{C}$ ; withdrawal capability of NPs being 90% after 10 cycles. Mazarío and co-workers<sup>314</sup> reported superparamagnetic nanosorbents for the adsorptive elimination of methyl orange and

lead (Pb) from water. The physio-chemical interactions of the pollutant with the nanosorbent were demonstrated by a pseudo-second order kinetic model. The highest adsorption ability for methyl orange was found to be  $240 \text{ mg g}_{\text{NS}}^{-1}$ . In a similar line, iron oxide was also utilized for the degradation of organic matters.<sup>414</sup> Recently, core-shell magnetic NPs were synthesized and deployed them for binding of the organic pollutant such as polychlorinated biphenyls.<sup>415</sup>

**3.1.4. Iron oxide-based metal-organic frameworks (MOFs) for waste water treatment.** Metal-organic frameworks (MOFs) also known as porous co-ordination polymers (PCPs), have garnered significant attention in the modern world of chemistry. These compounds are distinctive in that they comprise metal ions or clusters connected by organic ligands, resulting in a three-dimensional porous structure. Due to exceptionally high surface area and 3-D structure, rendering them valuable in diverse applications such as gas adsorption, catalysis, sensing, plasmonic, pollutant-immobilization, separation, fuel production, and bio-medical, *etc.*<sup>416</sup> Nowadays ionic liquids (ILs) and their composites are considered promising substrates as an adsorbent for adsorption separation due to their versatile





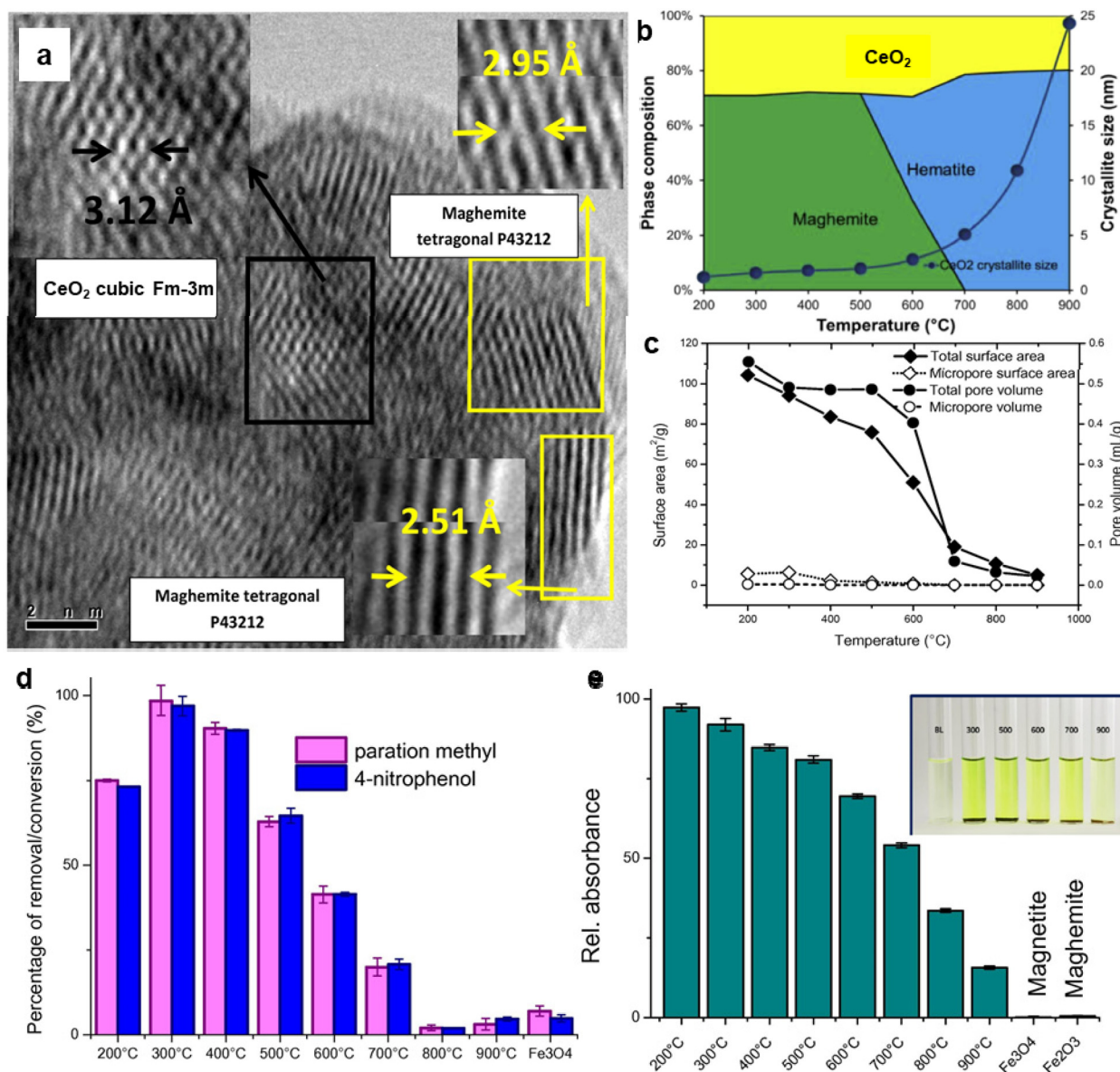
**Fig. 63** TEM images of the MGNCs (a) The nanoparticles are equally spread on the graphene sheet; (b) magnified image of (a) shows core@shell structure of the NPs; (c) HR-TEM of a single particle displaying an Fe core covered by a double shell structure; (d) SAED pattern of the core@shell nanoparticles. Reproduced with permission from ref. 337 Copyright 2011, American Chemical Society.

functionality present on the surface and multiple interaction forces.<sup>417</sup> Recently, layer by layer modification method was employed for the engineering of IL-COOH/Fe<sub>3</sub>O<sub>4</sub>@Zr water stable MOF nanocomposites aimed at selectively adsorbing and detecting fluoroquinolone antibiotics (FQs).<sup>418</sup> TEM images of IL-COOH/Fe<sub>3</sub>O<sub>4</sub>@Zr water stable MOF nanocomposites confirmed that the Fe<sub>3</sub>O<sub>4</sub> exhibits a uniform particle size, measuring approximately 280–300 nm (see Fig. 65a). The Fe<sub>3</sub>O<sub>4</sub>@PDA (polydopamine) nanocomposites displayed a well-defined core-shell structure, with a shell thickness of around 24 nm (see Fig. 65b). Zr-MOF particles, such as UiO-67-bpydc, exhibited a regular octahedral crystal structure (see Fig. 65c). Fe<sub>3</sub>O<sub>4</sub>@UiO-67-bpydc revealed that the uneven thickness ranged from 42 to 75 nm (see Fig. 65d). Among these different IL MOFs, IL-COOH/Fe<sub>3</sub>O<sub>4</sub>@UiO-67-bpydc exhibited superior adsorption capabilities compared to other MOFs, with an impressive maximum adsorption capacity of 438.5 mg g<sup>-1</sup> for ofloxacin.

In recent years, the utilization of hydrogen as a renewable substitute for fossil-based energy has been gaining momentum, and photoelectrochemical (PEC) water splitting stands out as an appealing and promising method for converting sunlight into hydrogen without the direct emission of greenhouse gases. However, achieving economic viability in PEC necessitates the enhancement of electrode efficiency and durability as the primary challenge.<sup>419</sup> Mondal and colleagues<sup>420</sup> have

developed a cost-effective bifunctional Fe<sub>2</sub>O<sub>3</sub>@C and FeP@C electrocatalyst for solar-driven water splitting (see Fig. 66a). As Fe<sub>2</sub>O<sub>3</sub>@C was synthesized through a straightforward one-step pyrolysis process at different temperatures 600, 700, and 800 °C under inert conditions. The resulting brown colored powders synthesized at different temperature were identified by various shades and labeled as Fe-A, Fe-B, and Fe-C. TEM images of the Fe<sub>2</sub>O<sub>3</sub>@C nanohybrid revealed that the densely packed arrangement of Fe<sub>2</sub>O<sub>3</sub> in Fe<sub>2</sub>O<sub>3</sub>@C (see Fig. 66b–d). The HRTEM images confirmed that the distinct lattice fringes, with a measured *d*-spacing of ~0.252 nm (see Fig. 66e–g). Additionally, selected area electron diffraction (SAED) patterns, as shown in the insets of Fig. 66(e–g), indicated that the polycrystalline nature of Fe<sub>2</sub>O<sub>3</sub> in all the nanostructures. The Fe<sub>2</sub>O<sub>3</sub>@C/Si composite has demonstrated significant activity in catalyzing the oxygen evolution reaction (OER), achieving a photoanodic current density of 2.5 mA cm<sup>-2</sup> at 1.65 V vs. RHE (*versus* the reversible hydrogen electrode).

Oxytetracycline (OTC) is a frequently utilized antibiotic for addressing infectious diseases in animals in intensive farming systems and aquaculture due to its broad-spectrum antibiotic properties but it became a major problem when OTC release was encountered in soil and groundwater.<sup>421,422</sup> Traditional methods for detecting oxytetracycline (OTC) primarily rely on liquid chromatography, capillary electrophoresis, enzyme-linked immunosorbent assay, and high-performance liquid



**Fig. 64** (a) HRTEM image of  $\text{CeO}_2/\gamma\text{-Fe}_2\text{O}_3$  nanocatalyst; (b) phase combinations of annealed composite sorbents and; (c)  $\text{N}_2$  isotherm and BJH plot; (d) Impact of calcination temperature on the degradation performance for parathion methyl in 2 h; (e) The phosphatase-like performance of the sorbents inset: images of chosen samples. Reproduced with permission from ref. 404 Copyright 2014, Elsevier.

chromatography (HPLC). While these conventional techniques are known for their reliability, sensitivity, and stability, their widespread application is hindered by certain drawbacks, including the need for expensive equipment, high costs, and lengthy sample preparation times. Limited research has been conducted on MOF-derived materials in the context of electrochemical sensing and aptasensors applications.<sup>423</sup> A chain of  $\text{Fe}_3\text{O}_4@\text{mC}$  nanocomposites derived through the pyrolysis of Fe-MOF (525-MOF) was successfully explored for detection of OTC.<sup>424</sup> The as-synthesized catalyst was analyzed by TEM to examine the morphological transformations of the  $\text{Fe}_3\text{O}_4@\text{mC}$  nanocomposites under different calcination temperatures. In the initial temperature range ( $350\text{ }^{\circ}\text{C}$ ) (see Fig. 67a and b), the

majority of the  $\text{Fe}_2\text{O}_3$  exhibits a uniform distribution, resembling sphere-like structures with an average size of 5–8 nm. Moving to the second stage ( $550\text{ }^{\circ}\text{C}$ ) (see Fig. 67c and d), larger spherical particles are observed, forming, and embedding into porous carbon nanosheets, with most particles ranging in size between 10 and 12 nm. Further elevation of the calcination temperature to 700 and  $900\text{ }^{\circ}\text{C}$  results in the enlargement of iron oxide particle sizes due to crystal aggregation (see Fig. 67e–h), as evidenced by TEM images. Red arrows indicated that the  $\text{Fe}_2\text{O}_3$  or  $\text{Fe}_3\text{O}_4$  NPs; yellow arrows indicated the mesopores within the amorphous carbon sheet (see Fig. 67a, c, e and g). As reported  $\text{Fe}_3\text{O}_4@\text{mC}_{900}$  stands out as the optimal candidate for achieving highly sensitive and selective detection of OTC.

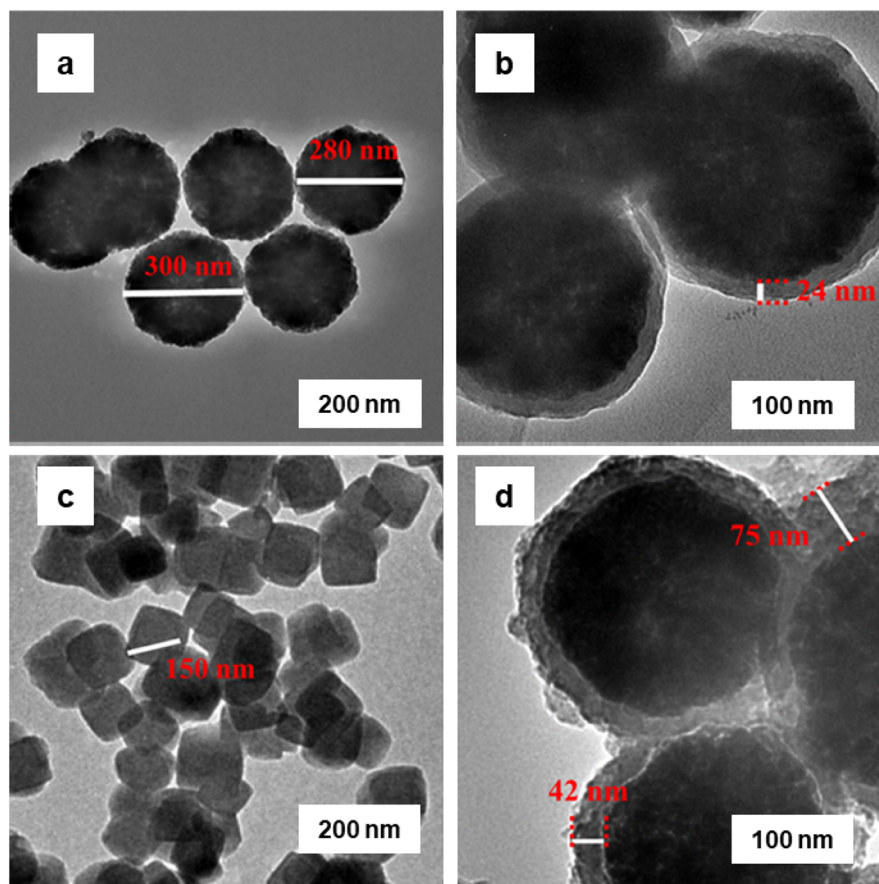


Fig. 65 TEM images of (a)  $\text{Fe}_3\text{O}_4$ ; (b)  $\text{Fe}_3\text{O}_4$ @PDA; (c) UiO-67-bpydc; and (d)  $\text{Fe}_3\text{O}_4$ @UiO-67-bpydc. Reproduced with permission from ref. 418 Copyright 2021, American Chemical Society.

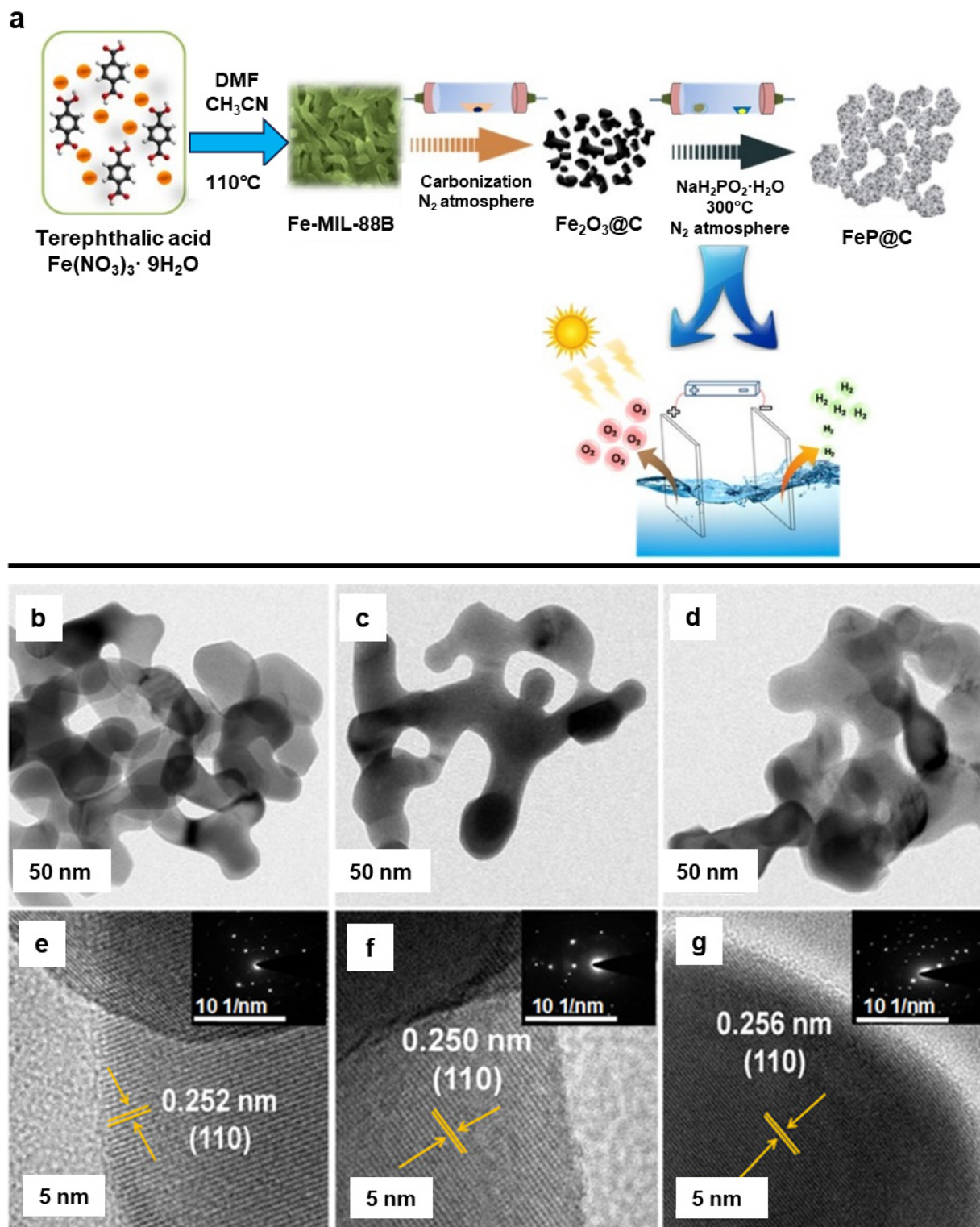
Hydrogen sulfide ( $\text{H}_2\text{S}$ ) is a malodorous gas emitted from various natural and human activities. Gupta *et al.*<sup>425</sup> have developed an innovative method to convert  $\text{H}_2\text{S}$  waste into value-added products by utilizing FeBDC and FeBTC derived iron oxide MOF's, labelled as IO-D and IO-T. They have detailed a process for synthesizing iron-based MOFs by sonication of organic linkers with freshly prepared iron hydroxide. The removal of  $\text{H}_2\text{S}$  using iron oxide adsorbents primarily involves oxidizing  $\text{H}_2\text{S}$  into sulfur and sulfates. Notably, the adsorption capacity of iron oxide adsorbents surpassed that of the corresponding MOF. Among them, FeBDC (IO-D) exhibited the highest adsorption capacity, reaching  $36.2 \text{ mg g}^{-1}$  under moist conditions.

### 3.2. Photocatalytic applications of iron oxides in environmental technologies

Photocatalysis, a cutting-edge technology employed in photocatalytic decomposition of organic pollutants, has garnered attention in view of its sustainability attributes.<sup>426–429</sup> By definition, photocatalysis entails speeding up the reaction by the light in the existence of catalyst. In catalyzed photolysis, a substrate absorbs light, whereas in the photogenerated catalysis, the catalyst performance depends on the capacity to form electron–hole pairs, which undergo secondary reactions.

However, some difficulties restrict the extensive implementation of iron oxide NPs for the photodegradation of hazardous chemicals due to difficulty in partition of compounds after completion of the action. The operational procedure is usually costly due to labor, time and raw materials intended for precipitation, further decantation or centrifugation at the termination of process, and the low quantum-yield of treatment that limits the rate and efficacy of the process.<sup>430</sup> Great strides, however, have been made to increase the photocatalytic performance by reducing the size of the photocatalyst, thereby increasing the surface area, thus merging photocatalyst with some new and efficient metal nanoparticles;<sup>431–433</sup> a variety of iron oxide nanoparticles have been employed for photocatalytic reactions with varied applications.<sup>434</sup> As an example, Zhou *et al.*<sup>435</sup> have reported 1D nanorods of goethite ( $\alpha\text{-FeOOH}$ ) and hematite ( $\alpha\text{-Fe}_2\text{O}_3$ ) for photocatalytic decomposition of Rhodamine B (RhB) by visible light under the existence of  $\text{H}_2\text{O}_2$ . Nanometer-scale  $\alpha\text{-FeOOH}$  and  $\alpha\text{-Fe}_2\text{O}_3$  particles were found to be more effective compare to microscale counterparts in respect of surface area normalized reaction rate. Furthermore,  $\alpha\text{-Fe}_2\text{O}_3$  nanorods displayed the highest catalytic performance compared to other samples. The perceived photocatalytic

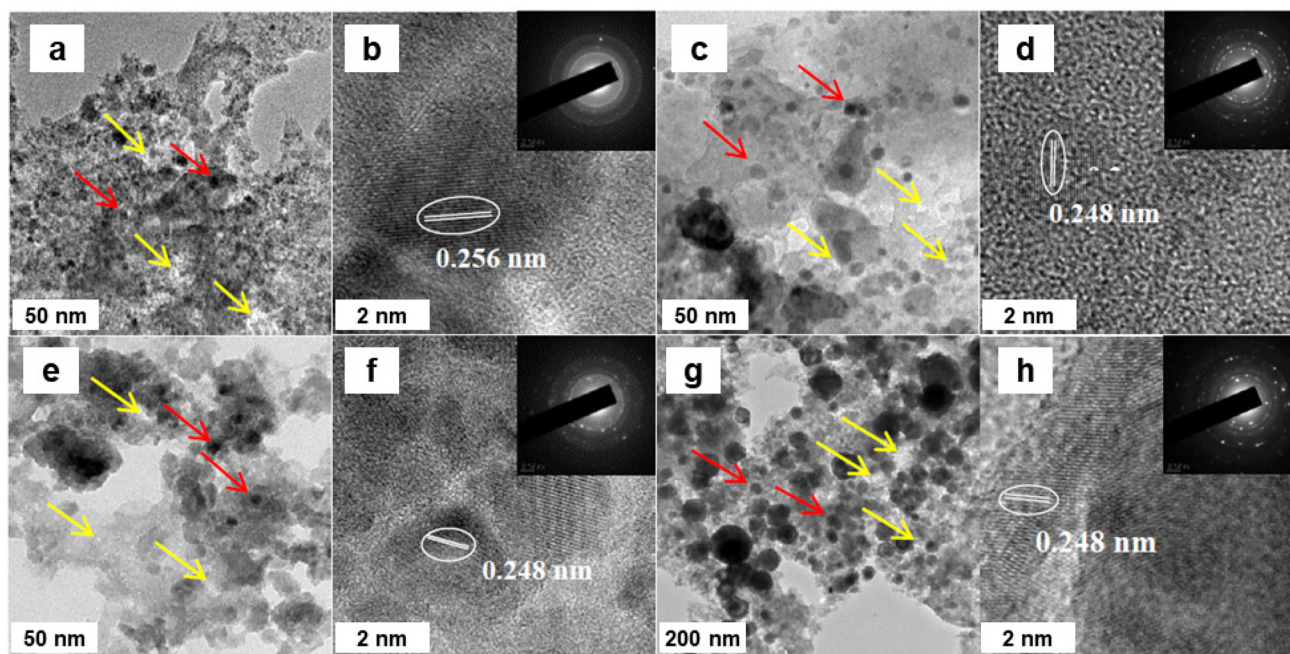




**Fig. 66** (a) Synthesis of bifunctional photoelectrodes, namely  $\text{Fe}_2\text{O}_3@\text{C}$  and  $\text{FeP}@\text{C}$ , intended for neutral water splitting; (b–d) TEM images of the Fe-A, Fe-B, and Fe-C respectively; (e–g) HRTEM images of the Fe-A, Fe-B, and Fe-C respectively, inset SAED patterns of the Fe-A, Fe-B, and Fe-C respectively; reproduced with permission from ref. 420 Copyright 2018, Wiley-VCH GmbH & Co. KGaA, Weinheim.

efficiency of iron oxide NPs was ascribed to the combined impact of particle composition, porosity, size, and deviations in morphology.

The  $\text{Fe}_2\text{O}_3/\text{CQDs}$  (Carbon Quantum Dots) composites for photodegradation of toxic gas under visible light have been reported by Liu and Kang.<sup>436</sup> Fig. 68a shows three photographs



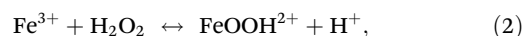
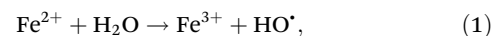
**Fig. 67** TEM images of (a, b)  $\text{Fe}_3\text{O}_4@\text{mC}_{350}$ , (c, d)  $\text{Fe}_3\text{O}_4@\text{mC}_{550}$ , (e, f)  $\text{Fe}_3\text{O}_4@\text{mC}_{700}$ , and (g, h)  $\text{Fe}_3\text{O}_4@\text{mC}_{900}$  nanocomposites (insets: corresponding SAED patterns). Reproduced with permission from ref. 424 Copyright 2013, The Royal Society of Chemistry.

of distinct colors of (i) CQDs aq. solution, (ii) reaction mixture including CQDs,  $\text{FeCl}_3$  and  $(\text{NH}_2)_2\text{CO}$  and (iii) product solution. The complete disappearance of the dust color of CQDs is indicative of the formation of  $\text{Fe}_2\text{O}_3/\text{CQDs}$ . The deployment of  $\text{Fe}_2\text{O}_3/\text{CQDs}$  composites for photocatalytic toxic gas decomposition has been described in this report for the first time. The synthesized  $\text{Fe}_2\text{O}_3/\text{CQDs}$  nanomaterials displayed improved photocatalytic performance for decomposition of toxic gas under visible light when compared to  $\text{Fe}_2\text{O}_3$ ; photoexcited electrons from iron oxide particles could be transferred without restraint in the conducting network of CQDs (Fig. 68b).<sup>436</sup> Moreover, it was proposed that an improvement in the photoactivity of iron oxide is encouraged by the presence of CQDs as they support for active segregation of photogenerated electrons and holes. The electron-hole pairs can then react with adsorbed oxidants/reductants, generating plentiful active oxygen radicals with strong oxidizing ability for the degradation of toxic gases. In addition, CQDs display up conversion photoluminescence by lower wavelength of light than absorbed light, thereby exciting  $\text{Fe}_2\text{O}_3$  to form electron-hole pairs. There have been other reports on grafting iron oxide NPs in the mesoporous carbon matrix for such potential applications.<sup>362,437–440</sup>

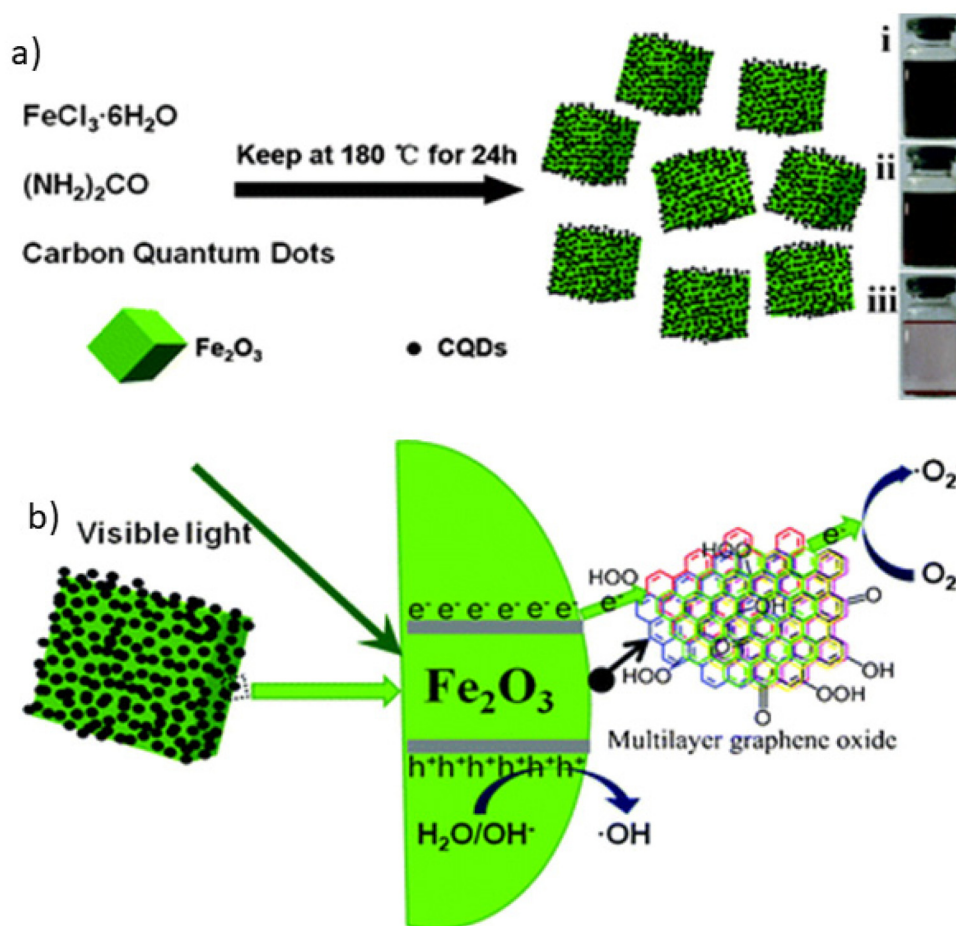
Among iron oxides, hematite ( $\alpha\text{-Fe}_2\text{O}_3$ , with a bandgap of  $\sim 2.1$  eV) is one of most widely explored oxides for photocatalysis;<sup>441–443</sup> various protocols have been applied for the synthesis of controlled films of hematite with considerable photocatalytic activity although some of them have drawbacks including formation of less amount of the product. Diab and Mokari<sup>434</sup> reported the scaled-up general synthesis of meso-

porous  $\alpha\text{-Fe}_2\text{O}_3$  to exploit their photoelectrochemical (PEC) properties. The presented methodology has been established on direct thermal degradation of iron acetate on a substrate to form a mesoporous film of  $\alpha\text{-Fe}_2\text{O}_3$  with excellent pore size regulation. An improvement of the PEC features of iron oxide was attained by using CoO areas, which were developed by thermolysis of the Co salt on the hematite surface to get  $\alpha\text{-Fe}_2\text{O}_3/\text{CoO}$  nanomaterials. The cobalt material was deposited by two methods: (a) by thermal decomposition and (b) by adsorption of Co salt. The photoconductivity of pristine hematite was  $0.25 \text{ mA cm}^{-2}$  at  $1.23 \text{ V}$  versus reversible hydrogen electrode (RHE), whereas alteration of hematite surface employing thermolysis protocol displayed 180% enhancement by the adsorption process. Furthermore, the beginning potential was changed by 130 and 70 mV when hematite surface was amended by the thermolysis and adsorption process, respectively.

Fenton and photo-Fenton processes have been proposed as potent methods for treating organic pollutants in wastewater. Hydroxyl ( $\text{HO}^\bullet$ ) and superoxide ( $\text{O}_2^{\bullet-}$ ) radical are formed in the Fenton reactions (eqn (1)–(3)), which then significantly decompose and mineralize the organic contaminants to  $\text{H}_2\text{O}$ ,  $\text{CO}_2$ , and other inorganic compounds. In particular,



Despite exhibiting powerful oxidation capability, Fenton reagents face several drawbacks like very low pH range for

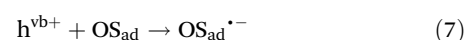
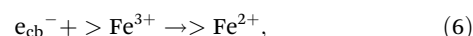
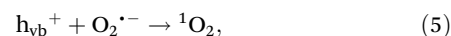
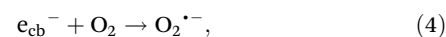


**Fig. 68** (a) Preparation of  $\text{Fe}_2\text{O}_3/\text{CQDs}$  composites by the hydrothermal treatment; (b) Schematic of the photocatalytic process of  $\text{Fe}/\text{CQDs}$  composites in the presence of visible light. Reproduced with permission from ref. 436 Copyright 2011, The Royal Society of Chemistry.

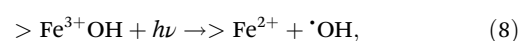
efficient reactions (2.5–4.0), formation of ferric hydroxide sludge at values of pH higher than 4.0, difficulty in recovery of the catalyst, and higher costs for iron ions removal from the process after the termination of the reaction.<sup>444</sup> Moreover, an impulsive oxidation of  $\text{Fe}^{2+}$  to  $\text{Fe}^{3+}$  ions frequently occur by dissolved oxygen in water *via* diverse partially oxidized metastable  $\text{Fe}^{2+}/\text{Fe}^{3+}$  intermediates which eventually transforms into stable iron oxides like hematite, maghemite, and magnetite. Thus, an idea has been proposed to replace the dissolved iron with solid catalysts.

Photo-Fenton reaction is a fusion of the Fenton reagents and ultraviolet and/or visible light that promotes formation of an extra  $\cdot\text{OH}$  radicals through photo-reduction of  $\text{Fe}^{3+}$  to  $\text{Fe}^{2+}$  ions and  $\text{H}_2\text{O}_2$  photolysis. Iron oxides have been identified as promising candidates for photocatalysts as they, among others, show semiconductor properties. However, hole–electron recombination process in iron oxides can be very fast, impairing the photocatalyst performance. In iron oxides, semi-conducting mechanisms involves two steps. Firstly, a photon with an energy equal of higher than the energy band gap between the valence and conduction band is adsorbed by iron oxides, generating an electron–hole pair, *i.e.*,  $\text{Fe}_2\text{O}_3 + h\nu \rightarrow$

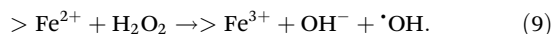
$\text{Fe}_2\text{O}_3 (e^- + h^+)$ . Even though the excited electron–hole pair can recombine with a heat dissipated, few of the excited electron and holes can promote the redox reactions occurring on the surface of iron oxide semiconducting particle. Several redox processes may then occur in an aqueous environment, containing iron oxide particles with generated electron–hole pairs and organic substance (OS) such as (eqn (4)–(7)).<sup>445</sup>



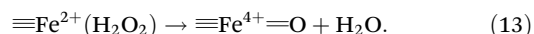
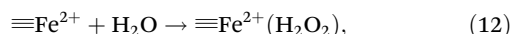
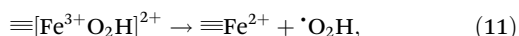
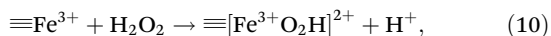
It is well known that irradiation may also trigger the heterogeneous Fenton process on Fe-containing nanoparticles, encouraging occurrence of the photo-reduction of  $>\text{Fe}^{3+}\text{OH}$  to  $>\text{Fe}^{2+}$ ;  $>\text{Fe}^{2+}$  can then react with  $\text{H}_2\text{O}_2$  to produce  $\cdot\text{OH}$  radicals at the surface of the nanoparticle, *i.e.*<sup>446</sup>



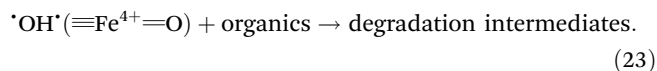
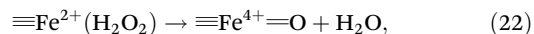
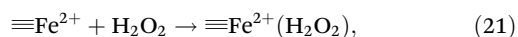
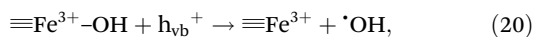
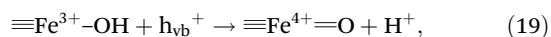
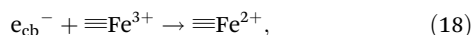
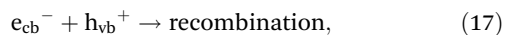
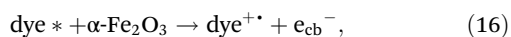
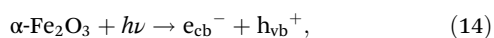




However,  $\alpha\text{-Fe}_2\text{O}_3$  shows a poor Fenton reaction performance. Thus, there have been several attempts to increase the reaction activity of  $\alpha\text{-Fe}_2\text{O}_3$ . One of the approaches is to dope  $\alpha\text{-Fe}_2\text{O}_3$  structure with sulfur (in the form of  $\text{FeS}$  or  $\text{FeS}_2$ ) as has been described by Guo *et al.*<sup>447</sup> sulfur in the  $\alpha\text{-Fe}_2\text{O}_3$  structure promotes photo-Fenton reaction. Firstly, S-doping alters the interfacial reaction process of Fe ions with  $\text{H}_2\text{O}_2$ , *i.e.*



It confirms that electron transfer among the peroxide species ( $\cdot\text{O}-\text{O}$ ) and Fe ions is increased at the interface which results in a higher Fenton reactivity. Secondly, doping sulfur of  $\alpha\text{-Fe}_2\text{O}_3$  promotes formation of trap states within the band gap of  $\alpha\text{-Fe}_2\text{O}_3$ . When illuminated under UV or visible light,  $\alpha\text{-Fe}_2\text{O}_3$  photocatalytic processes occur.<sup>447</sup>



The formed trap states act as defect state with a tendency to catch the charge carriers immediately after they are formed, thus retarding their recombination process. The photo-Fenton reactivity of S-doped  $\alpha\text{-Fe}_2\text{O}_3$  has been then assessed for the decomposition of phenol and acid orange, showing much higher performance compared to undoped  $\alpha\text{-Fe}_2\text{O}_3$ .<sup>447</sup>

A nanocomposite comprising  $\text{TiO}_2$  nanowires,  $\text{Fe}_2\text{O}_3$  NPs, and GO sheets has been synthesized to address the problem of membrane fouling in membrane water treatment technologies, produced by humic acid.<sup>448</sup> The removal of humic acid involves two steps, *i.e.*, adsorption and photo-degradation (see Fig. 69). Humic acid is first adsorbed on the  $\text{Fe}_2\text{O}_3$  nanoparticle sites. Then, under irradiation, electron-hole pairs are formed on the surface layers of the  $\text{TiO}_2$  nanowires. The holes oxidize water and generate  $\cdot\text{OH}$  radicals which oxidize nearby adsorbed HA. The electrons are preferentially carried to graphene oxide sheets (as a result of strong electric conductivity of graphene oxide) and upon reaction with oxygen, they promote formation of superoxide anion radicals ( $\text{O}_2^{\cdot-}$ ). Thus, membrane photocatalytic activity is enhanced due to splitting of electrons and holes. The 12 h test confirmed a higher removal of humic acid (92%) and a decrease in pressure across membrane were observed under irradiation compared to dark conditions, implying an anti-fouling ability of the novel membrane. Very recently, Qiu and co-workers<sup>449</sup> employed iron for the photocatalytic remediation of heavy metals. The combination of iron oxide and graphene also increased the adsorption for the decomposition of ammonium perchlorate.<sup>450</sup>

### 3.3. $\text{H}_2\text{O}_2$ decomposition promoted by iron oxides for environmental applications

In general, the Fenton process was initiated with the invention of short-lived, enormously reactive hydroxyl radical ( $\cdot\text{OH}$ ) with a potential of 2.8 V (ref. 451) from the interaction between  $\text{Fe}^{2+}$  and  $\text{H}_2\text{O}_2$ ; hydroxyl radical then helps for the material decomposition as discussed above.<sup>452-454</sup> Over the last few

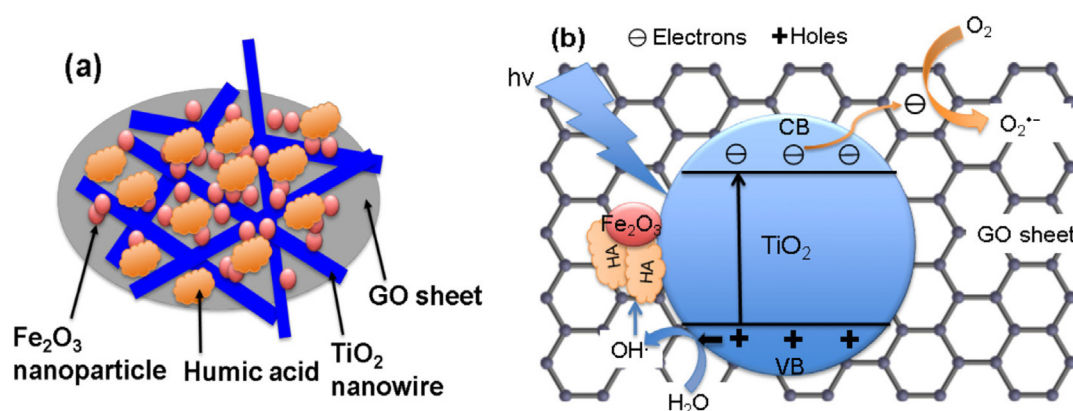


Fig. 69 (a, b) Schematic representations of membrane surface with humic acid adsorption and plausible mechanism for humic acid photo-degradation over the membrane surface. Reproduced with permission from ref. 448 Copyright 2016, Elsevier.

**Table 3** Iron oxides in the Fenton reactions<sup>452,455</sup>

| Sr. no. | Fenton's reaction types            | Reagents                                                    | Iron loss | pH                | Light |
|---------|------------------------------------|-------------------------------------------------------------|-----------|-------------------|-------|
| 1       | Photo Fentons                      | Complex free iron ions                                      | Yes       | Acidic to neutral | Yes   |
| 2       | Classic Fentons                    | Fe <sup>2+</sup> , H <sub>2</sub> O <sub>2</sub>            | Yes       | 2–4               | No    |
| 3       | Fenton like                        | Fe <sup>3+</sup> , H <sub>2</sub> O <sub>2</sub>            | Yes       | 2–4               | No    |
| 4       | Electro-Fentons                    | Electrogenerated Fe <sup>2+</sup>                           | Yes       | 2–4               | No    |
| 5       | Heterogeneous Fentons              | H <sub>2</sub> O <sub>2</sub> , solid iron oxide, free iron | No        | Broad range       | No    |
| 6       | Heterogeneous Photo-Fenton         | H <sub>2</sub> O <sub>2</sub> , solid iron oxide            | No        | Broad Range       | Yes   |
| 7       | Heterogeneous Photoelectron-Fenton | H <sub>2</sub> O <sub>2</sub> , solid iron oxide            | No        | Broad Range       | Yes   |

years, tremendous emphasis has been directed towards the progress of Fenton reactions specially focused on role of pH increase, *in situ* delivery of H<sub>2</sub>O<sub>2</sub> through oxygen reduction, *in situ* offering of Fe<sup>2+</sup> through the electrochemical oxidation of Fe, prevention loss of Fe and regeneration of Fe(II) by enlightening the sludge of iron origins (see Table 3).<sup>455</sup>

The catalytic decomposition of H<sub>2</sub>O<sub>2</sub> has been widely examined because of its major application in water treatment technologies. Hydrogen peroxide along with iron oxides has the capability to decompose organic pollutants in wastewater and contaminated soils; thus, it is viewed as a challenge for chemists to design unique and inexpensive catalyst materials/nanomaterials.<sup>75,456</sup> The rate of the H<sub>2</sub>O<sub>2</sub> decomposition primarily depends on several experimental factors like concentration of H<sub>2</sub>O<sub>2</sub>, pH, and the nature of catalyst.<sup>457,458</sup> The reactions of Fe(II) with O<sub>2</sub> and H<sub>2</sub>O<sub>2</sub> are essential as they directly produce the highly reactive oxidants *i.e.* hydroxyl radical (<sup>•</sup>OH) which is the key reactive species in various advanced oxidation processes.<sup>458–460</sup>

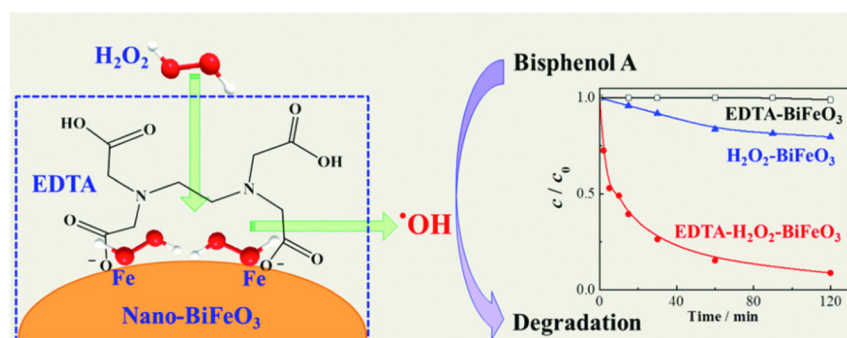
There are numerous scientific literatures detailing the exploitation of various iron oxide nanoparticles for the heterogeneous Fenton reaction including mainly hematite, magnetite, goethite, and maghemite NPs.<sup>77,461–463</sup> Tang and co-workers<sup>462</sup> reported BiFeO<sub>3</sub> NPs for the oxidation of bisphenol A (BPA) with benign oxidant. To initiate the catalytic efficacy of BiFeO<sub>3</sub> nanoparticles, *in situ* surface tempering of ligands was employed and BPA removal was enhanced through incorporating chelates including formic acid, tartaric acid, glycine, nitrilotriacetic acid (NTA) and EDTA. The catalytic efficiency order was found to be, blank < tartaric acid < formic acid < glycine < NTA < EDTA. Among these ligands, EDTA serve as the highly

active complexing agent, and 0.25 mmol L<sup>−1</sup> of EDTA removes 91% BPA. The degradation of BPA was reliant on the quantity of additional EDTA, the starting conc. of H<sub>2</sub>O, pH, and temperature. Furthermore, EDTA strongly induced the performance of BPA decomposition, resulting from the three different reaction sites on the BiFeO<sub>2</sub> surface, such as bare BiFeO<sub>3</sub> sites, EDTA-adsorbed sites, and intermediate blocked sites (see Fig. 70).<sup>462</sup>

The mechanism of hydrogen peroxide decomposition utilizing iron oxide as a catalyst has been clearly delineated<sup>459,464</sup> where degree of H<sub>2</sub>O<sub>2</sub> decomposition is in direct proportion to the iron oxide concentration.<sup>465</sup> However, salient feature responsible for the enhanced catalytic efficacy in heterogeneous catalysis involves greater surface area, obtained with the help of NPs. Hydrogen peroxide with iron oxide nanoparticles have been especially found attractive for wastewater treatment; H<sub>2</sub>O<sub>2</sub> decomposes catalytically by means of Fe<sup>2+</sup> at acidic pH to generate hydroxyl radicals.<sup>466</sup>

Fe/H<sub>2</sub>O<sub>2</sub> oxidations have been prominent because of the fact that Fe is an earth-abundant and relatively nontoxic metal, combined with the ease of handling of H<sub>2</sub>O<sub>2</sub>, which additionally degrades into environmentally benign byproducts when present in excess safe products. It has been referred to as the most economical alternative when compared to other oxidation methods; the process uses simple equipment and mild operational conditions (atmospheric pressure and room temperature).<sup>467</sup> H<sub>2</sub>O<sub>2</sub> decomposition on iron oxide nanoparticles is a well-established platform for environmental applications in wastewater treatment, organic compounds, and dyes degradation.<sup>468–471</sup>

Mesoporous iron oxides are important and versatile materials as they possess high surface area, equal pore size

**Fig. 70** Degradation of BPA showing distinct reaction sites. Reproduced with permission from ref. 462 Copyright 2011, American Chemical Society.

distributions, nanosized walls, substantial pore volume, and surface functionality.<sup>472</sup> An organized mesoporous Mg-modified hematite with an ultra-high surface area was synthesized by hard templating techniques in mesoporous silica KIT-6 and was employed for the methylene blue degradation.<sup>473</sup> The concentration of methylene blue in the supernatant was obtained at an absorbance peak of 664 nm and the concentration of  $\cdot\text{OH}$  was determined by the terephthalic acid by a fluorescence method.<sup>474</sup> Further, these results confirmed that approximately 2/3 of the Mg cations were detached at the time of leaching, and as a result produces more structural defects (Fig. 71). The activated mesoporous  $\text{Fe}_2\text{O}_3$  displays outstanding catalytic efficiency for MB degradation, achieving over 95% extraction of  $60 \text{ mg L}^{-1}$  MB after 3 h. The rate constant of employed *meso*-Mg/ $\text{Fe}_2\text{O}_3$  catalyst is  $1.972 \text{ h}^{-1}$  which is 1.22, 3.02 and 4.53 times higher compared to *meso*- $\text{Fe}_2\text{O}_3$ , *con*-Mg/ $\text{Fe}_2\text{O}_3$ ,<sup>473</sup> and  $\gamma\text{-Fe}_2\text{O}_3$  respectively. The leaching concentration of Mg and the catalytic activity increased with the reuse of *meso*-Mg/ $\text{Fe}_2\text{O}_3$  catalyst, which is fully disparate with the multi-component catalytic mechanism in typical heterogeneous Fenton-like processes, like Fe–Cu and Fe–Zn composites.<sup>473</sup>

The heterogeneous catalyst ( $\text{Fe}_3\text{O}_4/\text{usGO}$ ) for Fenton-like degradation of MB as dye pollutant was reported by Song *et al.*<sup>475</sup> Various iron oxide NPs have been employed for the removal of methylene blue,<sup>476</sup> antibiotics degradation<sup>477</sup> and also for safeguarding of human health by Fenton reaction.<sup>478</sup>

To increase the reactivity of the system, a strategy was suggested to enhance the contact of Fe(0) with  $\text{Fe}_3\text{O}_4$  nanoparticles by grinding;<sup>479</sup> it was found that assembling such architectures promote electron transfer from the metal to the reaction center. In particular, at the Fe(0)/ $\text{Fe}_3\text{O}_4$  interface, the metal transfers electrons to iron oxide which serves as an inter-

mediary with the reaction center. Iron oxide is a semiconductor showing a high electric conductivity, thus promoting the movement of electrons; moreover, its octahedral sites can readily adapt  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$  species in the redox equilibrium. The development of the reactive species is schematically depicted in Fig. 72. Reactive networks are also synthesized by mechanical milling and thermal treatment leading to Fe(0)/ $\alpha\text{-Fe}_2\text{O}_3$  and Fe(0)/ $\gamma\text{-Fe}_2\text{O}_3$  interface mixtures, but with an inferior efficiency for  $\text{H}_2\text{O}_2$  in comparison with Fe(0)/ $\text{Fe}_3\text{O}_4$ . This implies that  $\text{Fe}^{2+}$  species are accountable for the activity and thus, are more effective in the oxidation of organic pollutants in wastewaters. Recently, Qin *et al.*<sup>480</sup> studied the degradation of pollutant such as *p*-nitrophenol by regulating the concentration of  $\text{Fe}^{2+}$  and ligand as a tripolyphosphate.

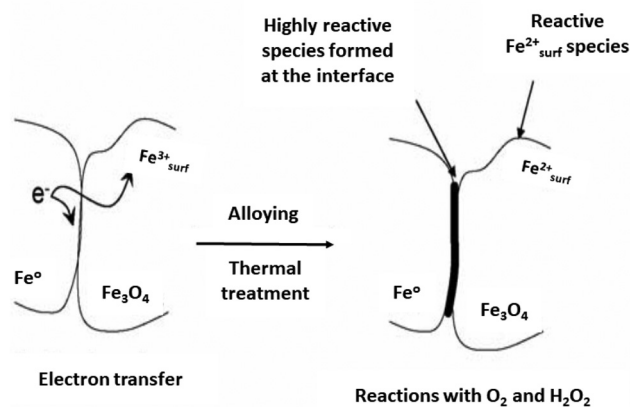


Fig. 72 The formation of the reactive species at the Fe(0)/ $\text{Fe}_3\text{O}_4$  interface. Reproduced with permission from ref. 479 Copyright 2006, Elsevier.

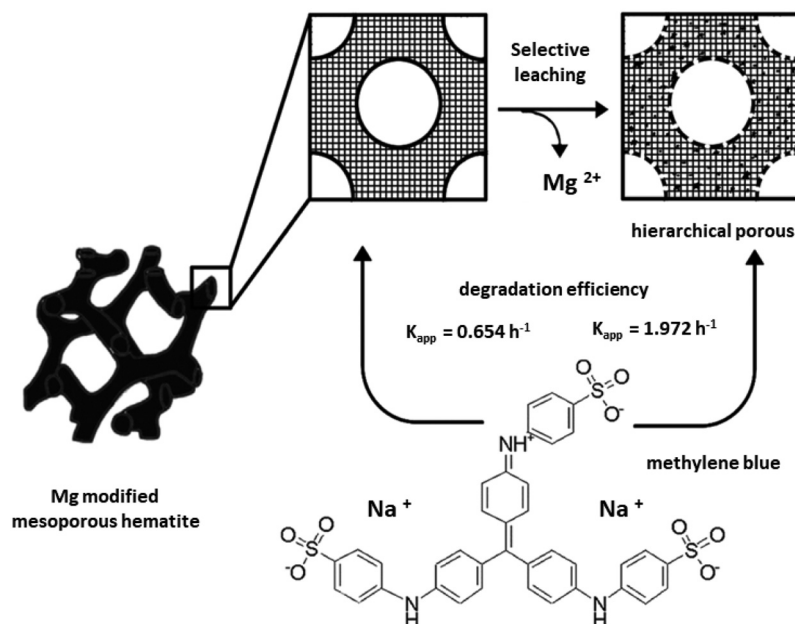


Fig. 71 Schematic representation of mesoporous Mg– $\text{Fe}_2\text{O}_3$  by leaching of Mg ions; arrows indicate the Mg leaching sites. Reproduced with permission from ref. 473 Copyright 2015, The Royal Society of Chemistry.



### 3.4. Biomolecule immobilization on iron oxide nanoparticles towards advanced environmental applications

Iron oxide nanoparticles have displayed a substantial potential for immobilizing the biomaterials, enzymes, *etc.*<sup>481,482</sup> The bio-sorption capability of diverse macro- and microbial enzymes or biomolecules has extensively employed to eliminate many contaminants; assorted types of iron oxide nanomaterials offer higher surface areas and number of active sites for synergy.<sup>483–485</sup>

The research on biofuels is advancing at a fast pace as an emerging field of study to offer substitute sources of renewable energy. Nanotechnology advancements have aimed to increase the efficacy of biofuel production, thereby increasing energy security.<sup>486</sup> Recently, magnetic single walled carbon nanotubes (mSWCNTs) have developed<sup>487</sup> by introducing an iron oxide NPs into SWCNTs. In this protocol, the enzyme amyloglucosidase (AMG) was immobilized onto mSWCNTs utilizing to combine the two technologies *i.e.*, nanotechnology and biofuel generation. Up on immobilization on mSWCNTs, enzyme preserves its catalytic performance in the ideal enzymatic hydrolysis of starch over repeated applications, subsequently, the material can be removed from the reacting environment by using an external magnet. These ensuing results, open the path for higher efficacy and lower principal expense of carbon nanotube enzyme bioreactors in industrial enzyme protocols, together with the special features of carbon nanotubes. There are several other innovative examples of post-synthetic modifications of iron oxides nanoparticles. Carbon-coated cobalt NPs that are chemically functionalized were employed for the immobilization of enzyme.<sup>488</sup> Li and co-workers<sup>489</sup> have investigated Ni-NTA (2,2',2''-nitrilotriacetic acid) functionalized iron oxide NPs that were deployed for the selective immobilization of histidine-tagged enzyme; other promising examples of immobilization of enzymes and their applications have been documented.<sup>490–492</sup>

Another crucial arena is the immobilization of biomaterials onto a sturdier and porous support that has been significantly investigated for varied applications; examples can be found for fungi and microalgae and exploitation for hydrogen production.<sup>493–497</sup> Indeed, immobilized cells have garnered a huge attention since the 1970s, because of their clear merits over dispersed cells.<sup>498</sup> First, the immobilization of native biomaterial improves the physical properties and proposes advanced degree of action.<sup>499</sup> In addition, opposition to environmental influences like pH, temperature, and toxicity can be improved.<sup>500</sup> Moreover, immobilization promotes the use cyclic biomaterials, offering simplified liquid–solid separation, and reducing the blocking in continuous-flow systems. These benefits could meet the technical requirements for the utilization of such supports, where it is crucial to use economical, simple, easy, and suitable methods for immobilization.

Peng and co-workers<sup>501</sup> have reported that *Saccharomyces cerevisiae* supported on chitosan-coated magnetic NPs (SICCM) can be deployed as an adsorbent for Cu(II) ions from aqueous media. The removal efficacy of over 90% is achievable within

20 min, with the highest adsorption capability being 134 mg g<sup>−1</sup>. It can therefore be assumed that the dispersion of biomaterials on appropriate support is important for the application of bio adsorbents in bulk-scale technologies. Additional research, however, is needed to improve the adsorbent, primarily by choosing suitable strains that have great adsorption capability for specific heavy metals and organic compounds.

In a similar context, recently the modified iron oxide nanoparticles have been used for the environmental application such as the immobilization of cadmium from contaminated soil,<sup>502</sup> arsenic removal from wastewater,<sup>503</sup> nano-remediation of contaminated aquifers<sup>504,505</sup> and also, for the immobilization of phosphorous from soil.<sup>506,507</sup>

Although an array of immobilization media and protocols have been examined, relatively scant information is available on combination of nanotechnology-based iron oxides with other biological matrices for environmental use. An ideal fusion could result in the development of innovative applications by using the inherent advantages of both the nanomaterial and biomaterials. Consequently, it is crucial to investigate not only the mass scale applications of adsorption technique but also ideal immobilization methods with a greater potential and constancy. Further research ought to exploit the potential of magnetic nanomaterials in combination with biological components for novel biotechnology applications like biosensors, immobilization of proteins for magnetic separation and environmental enhancement.

## 4. Conclusions and future directions

In this review, we have strived to comprehensively describe the usage of non-hydrated iron oxides in catalytic and environmental applications. It is amply demonstrated that the position of non-hydrated iron oxide phases in these areas is paramount and superior compared to other materials. The review deals with the identification of various parameters that can be synthetically controlled and, hence, they can be finely tuned in a way to be targeted for specific catalytic and environmental technologies.

Iron oxide nanoparticles have been extensively deployed as highly efficient catalysts and/or catalytic supports for diverse organic transformations like reduction, oxidation, coupling, and alkylation reactions, Fischer Tropsch synthesis, or multi-component reactions. A remarkable impact has also been made by iron oxide nanoparticles to promote the production of crucial organic compounds. Nonetheless, there are still several challenges associated with iron oxide NPs and their applications in catalysis that need to be circumvented in the future. Despite of having diverse physical, chemical, and biological procedures to prepare various iron oxide NPs, there is still an obstacle to regulate their surface properties and immobilization of surface fractions in the framework of organic/inorganic composites, thus tuning their stability and the composite's strength. Therefore, future research ought to be undertaken on computational design including artificial intelligence

approaches and optimizing routes for the controllable and scalable synthesis of iron oxide nanoparticles. There is also a significant challenge in exploring the reaction mechanisms and identifying individual reaction steps. Here, the computational approaches and advanced *in situ* techniques should be largely applied. Finally, the possible use of magnetic iron oxides as advanced supports for single atom embedding need to be more intensively studied thus opening the doors towards scalable and readily separable iron oxide based single atom catalysts.

One of the foremost societal and scientific challenge is the generation of large amounts of wastewater, which needs routine wastewater treatment operations to prevent harm to people, animals, soils, and plants as well as the spread of numerous illnesses. Thus, the substantial portion of this review article is dedicated to the use of iron oxide NPs in advanced environmental and water treatment technologies including *e.g.*, sorption technologies, photocatalytic applications, hydrogen peroxide assisted degradation of pollutants and other techniques. When compared to traditional adsorbents, iron-oxide nanoparticles operate more effectively and efficiently in wastewater treatment in terms of their abundance, low toxicity, and low costs. However, the future research should examine and assess the possibility of sorbent regeneration, and reusability potential to exploit the use of iron oxide nanoparticles for wastewater treatment. Similarly, the tailored surface modification of iron oxide NPs towards selective removal of particular contaminants represents another important challenge. There is a paucity of information on the interaction of iron oxides with biological matrices, which would affect their efficiency in environmental applications. Behind the successful progress of the heterogeneous nanocrystalline iron oxides for the use in photo-Fenton process, skillful coupling of this technology with traditional techniques including filtration, coagulation, and membrane technology is needed. In addition, further pilot-scale studies are required to investigate the full-scale application of iron oxide NPs in remediation and photocatalytic technologies.

## Author contributions

MBG, RV, and RZ conceptualized the idea, supervised, and edited the complete manuscript. DSC and RPU wrote the draft, edited the manuscript, and compiled the review. GYS and JF co-wrote the manuscript part.

## Conflicts of interest

The authors declare no conflict of interest.

## Acknowledgements

DSC and RPU express special thanks to the Institute of Chemical Technology, Mumbai-Marathwada Campus, Jalna,

for providing facilities for pursuing a doctoral degree. M. B. G. gratefully acknowledge the funding support from Department of Science and Technology, SERB, Core Research Grant (CRG/2021/001738). This article has been produced with the financial support of the European Union under the REFRESH – Research Excellence for Region Sustainability and High-tech Industries project number CZ.10.03.01/00/22\_003/0000048 via the Operational Programme Just Transition. Furthermore, the work was supported by ERDF/ESF project TECHSCALE (No. CZ.02.01.01/00/22\_008/0004587).

## References

- 1 D. Liu, W. Wu, J. Ling, S. Wen, N. Gu and X. Zhang, *Adv. Funct. Mater.*, 2011, **21**, 1498–1504.
- 2 W. Mekseriwattana, W. Phanchai, T. Thiangtrongjit, O. Reamtong, T. Puangmali, P. Wongtrakoongate, A. Roig and K. P. Katewongsa, *ACS Appl. Nano Mater.*, 2023, **6**, 13952–13964.
- 3 M. Ognjanović, M. Radović, M. Mirković, Ž. Prijović, M. del Puerto Morales, M. Čeh, S. Vranješ-Durić and B. Antić, *ACS Appl. Mater. Interfaces*, 2019, **11**, 41109–41117.
- 4 K. X. Vazquez-Prada, S. S. Moonshi, Y. Wu, F. Akther, B. W. C. Tse, K. A. Sokolowski, K. Peter, X. Wang, G. Xu and H. T. Ta, *Small*, 2023, **19**, 2205744.
- 5 T. Vangijzegem, V. Lecomte, I. Ternad, L. Van Leuven, R. N. Muller, D. Stanicki and S. Laurent, *Pharmaceutics*, 2023, **15**, 236.
- 6 A. K. Gupta and M. Gupta, *Biomaterials*, 2005, **26**, 3995–4021.
- 7 S. Laurent, D. Forge, M. Port, A. Roch, C. Robic, L. Vander Elst and R. N. Muller, *Chem. Rev.*, 2008, **108**, 2064–2110.
- 8 Q. A. Pankhurst, J. Connolly, S. K. Jones and J. Dobson, *J. Phys. D: Appl. Phys.*, 2003, **36**, R167.
- 9 T. Vangijzegem, D. Stanicki and S. Laurent, *Expert Opin. Drug Delivery*, 2019, **16**, 69–78.
- 10 K. Sivula, F. Le Formal and M. Grätzel, *ChemSusChem*, 2011, **4**, 432–449.
- 11 Z. Zhang, L. Weng, Q. Rao, S. Yang, J. Hu, J. Cai and Y. Min, *J. Power Sources*, 2019, **439**, 227107.
- 12 M. Chen, F.-M. Liu, H. Zhao, S.-S. Chen, X. Qian, Z.-Y. Yuan and R. Wan, *Phys. Chem. Chem. Phys.*, 2022, **24**, 27114–27120.
- 13 D. Mohan and C. U. Pittman, *J. Hazard. Mater.*, 2007, **142**, 1–53.
- 14 A. M. H. Shadi, M. A. Kamaruddin, N. M. Niza, F. M. Omar and M. S. Hossain, *J. Environ. Chem. Eng.*, 2022, **10**, 107753.
- 15 A.-H. Lu, E. L. Salabas and F. Schüth, *Angew. Chem., Int. Ed.*, 2007, **46**, 1222–1244.
- 16 S. Shylesh, V. Schünemann and W. R. Thiel, *Angew. Chem., Int. Ed.*, 2010, **49**, 3428–3459.
- 17 V. Polshettiwar, R. Luque, A. Fihri, H. Zhu, M. Bouhrara and J.-M. Basset, *Chem. Rev.*, 2011, **111**, 3036–3075.

- 18 N. Lewinski, V. Colvin and R. Drezek, *Small*, 2008, **4**, 26–49.
- 19 M. I. Idris, J. Zaloga, R. Detsch, J. A. Roether, H. Unterweger, C. Alexiou and A. R. Boccaccini, *Sci. Rep.*, 2018, **8**, 7286.
- 20 H. Cai, X. An, J. Cui, J. Li, S. Wen, K. Li, M. Shen, L. Zheng, G. Zhang and X. Shi, *ACS Appl. Mater. Interfaces*, 2013, **5**, 1722–1731.
- 21 H. Guo and A. S. Barnard, *J. Mater. Chem. A*, 2013, **1**, 27–42.
- 22 R. Zboril, M. Mashlan and D. Petridis, *Chem. Mater.*, 2002, **14**, 969–982.
- 23 L. Machala, J. Tuček and R. Zbořil, *Chem. Mater.*, 2011, **23**, 3255–3272.
- 24 J. Tuček, L. Machala, S. Ono, A. Namai, M. Yoshikiyo, K. Imoto, H. Tokoro, S.-i. Ohkoshi and R. Zbořil, *Sci. Rep.*, 2015, **5**, 15091.
- 25 C. Wu, P. Yin, X. Zhu, C. OuYang and Y. Xie, *J. Phys. Chem. B*, 2006, **110**, 17806–17812.
- 26 P. Robinson, R. J. Harrison, S. A. McEnroe and R. B. Hargraves, *Nature*, 2002, **418**, 517–520.
- 27 O. Malina, J. Tuček, P. Jakubec, J. Kašlík, I. Medřík, H. Tokoro, M. Yoshikiyo, A. Namai, S.-i. Ohkoshi and R. Zbořil, *RSC Adv.*, 2015, **5**, 49719–49727.
- 28 C.-W. Lee, K.-W. Lee and J.-S. Lee, *Mater. Lett.*, 2008, **62**, 2664–2666.
- 29 M. M. Rahman, A. Jamal, S. B. Khan and M. Faisal, *Superlattices Microstruct.*, 2011, **50**, 369–376.
- 30 G. Carraro, D. Barreca, M. Cruz-Yusta, A. Gasparotto, C. Maccato, J. Morales, C. Sada and L. Sánchez, *ChemPhysChem*, 2012, **13**, 3798–3801.
- 31 G. Carraro, C. Maccato, A. Gasparotto, T. Montini, S. Turner, O. I. Lebedev, V. Gombac, G. Adami, G. Van Tendeloo, D. Barreca and P. Fornasiero, *Adv. Funct. Mater.*, 2014, **24**, 372–378.
- 32 J. Tuček, R. Zbořil, A. Namai and S.-i. Ohkoshi, *Chem. Mater.*, 2010, **22**, 6483–6505.
- 33 J. Tuček, S.-i. Ohkoshi and R. Zboril, *Appl. Phys. Lett.*, 2011, **99**, 253108.
- 34 J. Jin, S. Ohkoshi and K. Hashimoto, *Adv. Mater.*, 2004, **16**, 48–51.
- 35 A. Namai, S. Sakurai, M. Nakajima, T. Suemoto, K. Matsumoto, M. Goto, S. Sasaki and S.-i. Ohkoshi, *J. Am. Chem. Soc.*, 2009, **131**, 1170–1173.
- 36 M. Gich, C. Frontera, A. Roig, J. Fontcuberta, E. Molins, N. Bellido, C. Simon and C. Fleta, *Nanotechnology*, 2006, **17**, 687–691.
- 37 A. Espinosa, R. Di Corato, J. Kolosnjaj-Tabi, P. Flaud, T. Pellegrino and C. Wilhelm, *ACS Nano*, 2016, **10**, 2436–2446.
- 38 O. K. Arriortua, M. Insausti, L. Lezama, I. Gil de Muro, E. Garaio, J. M. de la Fuente, R. M. Fratila, M. P. Morales, R. Costa, M. Eceiza, M. Sagartzazu-Aizpurua and J. M. Aizpurua, *Colloids Surf., B*, 2018, **165**, 315–324.
- 39 M. B. Gawande, R. K. Pandey and R. V. Jayaram, *Catal. Sci. Technol.*, 2012, **2**, 1113–1125.
- 40 J. Pal and T. Pal, *Nanoscale*, 2015, **7**, 14159–14190.
- 41 Y. Liu, W. Wang, X. Xu, J.-P. Marcel Veder and Z. Shao, *J. Mater. Chem. A*, 2019, **7**, 7280–7300.
- 42 S. Jung, S. Bae and W. Lee, *Environ. Sci. Technol.*, 2014, **48**, 9651–9658.
- 43 R. Lang, X. Du, Y. Huang, X. Jiang, Q. Zhang, Y. Guo, K. Liu, B. Qiao, A. Wang and T. Zhang, *Chem. Rev.*, 2020, **120**, 11986–12043.
- 44 A. Aitbekova, E. D. Goodman, L. Wu, A. Boubnov, A. S. Hoffman, A. Genc, H. Cheng, L. Casalena, S. R. Bare and M. Cargnello, *Angew. Chem., Int. Ed.*, 2019, **58**, 17451–17457.
- 45 D. Toulemon, B. P. Pichon, C. Leuvrey, S. Zafeiratos, V. Papaefthimiou, X. Cattoën and S. Bégin-Colin, *Chem. Mater.*, 2013, **25**, 2849–2854.
- 46 Q. Wang, Z. Shang, H. Wang and A. Wei, *Nanoscale*, 2023, **15**, 5074–5082.
- 47 F. Zareh, M. Gholinejad, H. Sheibani and J. M. Sansano, *Environ. Sci. Pollut. Res.*, 2023, **30**, 69362–69378.
- 48 A. Navrotsky, L. Mazeina and J. Majzlan, *Science*, 2008, **319**, 1635–1638.
- 49 A. A. Herzing, C. J. Kiely, A. F. Carley, P. Landon and G. J. Hutchings, *Science*, 2008, **321**, 1331–1335.
- 50 M. Afrouz, F. A. Nouraldinwand, S. G. Elias, M. T. Alebrahim, T. M. Tseng and H. Zahedian, *Sci. Rep.*, 2023, **13**, 775.
- 51 Z. Sun, J. Ma, Y. Liu, H. Wang, W. Cao, N. Zhu and Z. Lou, *Sep. Purif. Technol.*, 2021, **277**, 119506.
- 52 M. Tang, L. Wang, H. Li, X. Huang, C. Du and S. Lu, *J. Environ. Sci.*, 2024, **137**, 478–487.
- 53 S. Dong, X. Yan, W. Li, Y. Liu, X. Han, X. Liu, J. Feng, C. Yu, C. Zhang and J. Sun, *J. Ind. Eng. Chem.*, 2022, **108**, 254–262.
- 54 J. Li, J. You, Z. Wang, Y. Zhao, J. Xu, X. Li and H. Zhang, *J. Environ. Chem. Eng.*, 2022, **10**, 108329.
- 55 A. A. Marciniak, E. C. S. Santos, R. J. Caraballo-Vivas, O. C. Alves, M. E. H. Maia da Costa, F. Garcia and C. J. A. Mota, *Energy Fuels*, 2024, **38**, 628–636.
- 56 L. Chen, M. Arshad, Y. Chuang, T.-B. Nguyen, C.-H. Wu, C.-W. Chen and C.-D. Dong, *J. Alloys Compd.*, 2023, **947**, 169577.
- 57 R. K. Sahoo, A. K. Manna, A. Das, A. Mitra, M. Mohapatra, S. Nath Sarangi, P. Garg, U. Deshpande and S. Varma, *Appl. Surf. Sci.*, 2022, **577**, 151954.
- 58 M. B. Gawande, P. S. Branco and R. S. Varma, *Chem. Soc. Rev.*, 2013, **42**, 3371–3393.
- 59 M. B. Gawande, Y. Monga, R. Zboril and R. K. Sharma, *Coord. Chem. Rev.*, 2015, **288**, 118–143.
- 60 M. B. Gawande, R. Luque and R. Zboril, *ChemCatChem*, 2014, **6**, 3312–3313.
- 61 R. Hudson, Y. Feng, R. S. Varma and A. Moores, *Green Chem.*, 2014, **16**, 4493–4505.
- 62 R. B. N. Baig and R. S. Varma, *Chem. Commun.*, 2013, **49**, 752–770.
- 63 J. Rahimi, M. Naderi, M. T. Ijdani, M. Heidari, M. Azizi and A. Maleki, *Mater. Today Chem.*, 2023, **28**, 101375.



- 64 X. Xiao, S. Lee, H. Ma, J. Yang, W.-S. Han and T. Yu, *Dalton Trans.*, 2022, **51**, 11485–11490.
- 65 A. Marandi and N. Koukabi, *Colloids Surf., A*, 2021, **621**, 126597.
- 66 M. Gong and H. Dai, *Nano Res.*, 2015, **8**, 23–39.
- 67 J. Qi, W. Zhang, R. Xiang, K. Liu, H.-Y. Wang, M. Chen, Y. Han and R. Cao, *Adv. Sci.*, 2015, **2**, 1500199.
- 68 J. Gautam, K. Kannan, M. M. Meshesha, B. Dahal, S. Subedi, L. Ni, Y. Wei and B. L. Yang, *J. Colloid Interface Sci.*, 2022, **618**, 419–430.
- 69 N.-U.-A. Babar, Y. F. Joya, H. Khalil, F. Hussain and K. S. Joya, *Int. J. Hydrogen Energy*, 2021, **46**, 7885–7902.
- 70 S. Yuan, Y. Xue, R. Ma, Q. Ma, Y. Chen and J. Fan, *Sci. Total Environ.*, 2023, **866**, 161444.
- 71 S. Rahim Pouran, A. A. Abdul Raman and W. M. A. Wan Daud, *J. Cleaner Prod.*, 2014, **64**, 24–35.
- 72 Y. Cheng, S. Zhang, Z. Wang, B. Wang, J. You, R. Guo and H. Zhang, *Sep. Purif. Technol.*, 2023, **318**, 123971.
- 73 S. Xin, S. Huo, Y. Xin, M. Gao, Y. Wang, W. Liu, C. Zhang and X. Ma, *Appl. Catal.*, 2022, **312**, 121442.
- 74 C. Lai, F. Huang, G. Zeng, D. Huang, L. Qin, M. Cheng, C. Zhang, B. Li, H. Yi, S. Liu, L. Li and L. Chen, *Chemosphere*, 2019, **224**, 910–921.
- 75 M. C. Pereira, L. C. A. Oliveira and E. Murad, *Clay Miner.*, 2012, **47**, 285–302.
- 76 P. V. Nidheesh, *RSC Adv.*, 2015, **5**, 40552–40577.
- 77 K. Rusevova, F.-D. Kopinke and A. Georgi, *J. Hazard. Mater.*, 2012, **241–242**, 433–440.
- 78 S. Lian, H. Li, X. He, Z. Kang, Y. Liu and S. Tong Lee, *J. Solid State Chem.*, 2012, **185**, 117–123.
- 79 D. Saberi, M. Sheykhan, K. Niknam and A. Heydari, *Catal. Sci. Technol.*, 2013, **3**, 2025–2031.
- 80 M. B. Gawande, V. D. B. Bonifácio, R. S. Varma, I. D. Nogueira, N. Bundaleski, C. A. A. Ghumman, O. M. N. D. Teodoro and P. S. Branco, *Green Chem.*, 2013, **15**, 1226–1231.
- 81 M. B. Gawande, A. K. Rath, I. D. Nogueira, R. S. Varma and P. S. Branco, *Green Chem.*, 2013, **15**, 1895–1899.
- 82 M. B. Gawande, A. K. Rath, J. Tucek, K. Safarova, N. Bundaleski, O. M. N. D. Teodoro, L. Kvitek, R. S. Varma and R. Zboril, *Green Chem.*, 2014, **16**, 4137–4143.
- 83 Y. Gao, D. Ma, G. Hu, P. Zhai, X. Bao, B. Zhu, B. Zhang and D. S. Su, *Angew. Chem., Int. Ed.*, 2011, **50**, 10236–10240.
- 84 K. J. Datta, M. B. Gawande, K. K. R. Datta, V. Ranc, J. Pechousek, M. Krizek, J. Tucek, R. Kale, P. Pospisil, R. S. Varma, T. Asefa, G. Zoppellaro and R. Zboril, *J. Mater. Chem. A*, 2016, **4**, 596–604.
- 85 X. Qian, X.-H. Peng, D. O. Ansari, Q. Yin-Goen, G. Z. Chen, D. M. Shin, L. Yang, A. N. Young, M. D. Wang and S. Nie, *Nat. Biotechnol.*, 2008, **26**, 83–90.
- 86 H. Yilmaz, D. Yilmaz, I. C. Taskin and M. Culha, *Adv. Drug Delivery Rev.*, 2022, **184**, 114184.
- 87 C.-Y. Zhang, B.-C. Zhao, R. Hao, Z. Wang, Y.-W. Hao, B. Zhao and Y.-Q. Liu, *J. Hazard. Mater.*, 2020, **385**, 121510.
- 88 S. Liu, G. Chen, P. N. Prasad and M. T. Swihart, *Chem. Mater.*, 2011, **23**, 4098–4101.
- 89 J.-H. Choi, J.-H. Lee, J. Son and J.-W. Choi, *Sensors*, 2020, **20**, 1003.
- 90 P. K. Jain, X. Huang, I. H. El-Sayed and M. A. El-Sayed, *Acc. Chem. Res.*, 2008, **41**, 1578–1586.
- 91 J. Zhu and R. B. Lennox, *ACS Appl. Nano Mater.*, 2021, **4**, 3790–3798.
- 92 K. J. Datta, K. K. R. Datta, M. B. Gawande, V. Ranc, K. Čepe, V. Malgras, Y. Yamauchi, R. S. Varma and R. Zboril, *Chem. – Eur. J.*, 2016, **22**, 1577–1581.
- 93 M. Sankar, Q. He, R. V. Engel, M. A. Sainna, A. J. Logsdail, A. Roldan, D. J. Willock, N. Agarwal, C. J. Kiely and G. J. Hutchings, *Chem. Rev.*, 2020, **120**, 3890–3938.
- 94 K. Sakamoto, S. Masuda, S. Takano and T. Tsukuda, *ACS Catal.*, 2023, **13**, 3263–3271.
- 95 T.-H. Yang, J. Ahn, S. Shi, P. Wang, R. Gao and D. Qin, *Chem. Rev.*, 2021, **121**, 796–833.
- 96 A. K. Rath, M. B. Gawande, J. Pechousek, J. Tucek, C. Aparicio, M. Petr, O. Tomanec, R. Krikavova, Z. Travnicek, R. S. Varma and R. Zboril, *Green Chem.*, 2016, **18**, 2363–2373.
- 97 S. Lapointe, A. Sarbajna and V. H. Gessner, *Acc. Chem. Res.*, 2022, **55**, 770–782.
- 98 K. Hasan, I. A. Shehadi, K. Ahmed Bagudu, N. Osama Mohamed Elmabrouk, A. Elgamouz, S. P. Patole and R. A. Al-Qawasmeh, *Appl. Surf. Sci.*, 2022, **571**, 151369.
- 99 K. C. Nicolaou, P. G. Bulger and D. Sarlah, *Angew. Chem., Int. Ed.*, 2005, **44**, 4442–4489.
- 100 A. Fihri, M. Bouhrara, B. Nekoueishahraki, J.-M. Basset and V. Polshettiwar, *Chem. Soc. Rev.*, 2011, **40**, 5181–5203.
- 101 G. S. Lee, D. Kim and S. H. Hong, *Nat. Commun.*, 2021, **12**, 991.
- 102 K. Hong, M. Sajjadi, J. M. Suh, K. Zhang, M. Nasrollahzadeh, H. W. Jang, R. S. Varma and M. Shokouhimehr, *ACS Appl. Nano Mater.*, 2020, **3**, 2070–2103.
- 103 K. Sakoda, J. Mihara and J. Ichikawa, *Chem. Commun.*, 2005, 4684–4686.
- 104 N. Miyaura and A. Suzuki, *Chem. Rev.*, 1995, **95**, 2457–2483.
- 105 W. Yao, G. Zhao, Y. Wu, L. Zhou, U. Mukherjee, P. Liu and M.-Y. Ngai, *J. Am. Chem. Soc.*, 2022, **144**, 3353–3359.
- 106 M. J. Buskes and M.-J. Blanco, *Molecules*, 2020, **25**, 3493.
- 107 S. Sá, M. B. Gawande, A. Velhinho, J. P. Veiga, N. Bundaleski, J. Trigueiro, A. Tolstogousov, O. M. N. D. Teodoro, R. Zboril, R. S. Varma and P. S. Branco, *Green Chem.*, 2014, **16**, 3494–3500.
- 108 A. Biffis, P. Centomo, A. Del Zotto and M. Zecca, *Chem. Rev.*, 2018, **118**, 2249–2295.
- 109 J. Colavida, J. A. Lleberia, A. Salom-Català, A. Gual, A. Collado, E. Zangrando, J. M. Ricart, C. Godard, C. Claver, J. J. Carbó and S. Castillon, *ACS Catal.*, 2020, **10**, 11458–11465.
- 110 D. Wang, C. A. Salazar and S. S. Stahl, *Organometallics*, 2021, **40**, 2198–2203.

- 111 A. K. Rath, M. B. Gawande, V. Ranc, J. Pechousek, M. Petr, K. Cepe, R. S. Varma and R. Zboril, *Catal. Sci. Technol.*, 2016, **6**, 152–160.
- 112 L. Sun, Q. Li, M. Zheng, S. Lin, C. Guo, L. Luo, S. Guo, Y. Li, C. Wang and B. Jiang, *J. Colloid Interface Sci.*, 2022, **608**, 2463–2471.
- 113 Á. Mastalir and Á. Molnár, *ChemCatChem*, 2023, e202300643.
- 114 N. Y. Baran, T. Baran and M. Nasrollahzadeh, *Sci. Rep.*, 2023, **13**, 12008.
- 115 X. Pei, Y. Li, L. Lu, H. Jiao, W. Gong and L. Zhang, *ACS Appl. Mater. Interfaces*, 2021, **13**, 44418–44426.
- 116 J. Boström, D. G. Brown, R. J. Young and G. M. Keserü, *Nat. Rev. Drug Discovery*, 2018, **17**, 709–727.
- 117 A. Taheri Kal Koshvandi, M. M. Heravi and T. Momeni, *Appl. Organomet. Chem.*, 2018, **32**, e4210.
- 118 I. P. Beletskaya, F. Alonso and V. Tyurin, *Coord. Chem. Rev.*, 2019, **385**, 137–173.
- 119 V. S. Shende, V. B. Saptal and B. M. Bhanage, *Chem. Rec.*, 2019, **19**, 2022–2043.
- 120 G. Wang, P. Hao, Y. Chang, Q. Zhang, W. Liu, B. Duan, H. Zhan and S. Bi, *Nanoscale*, 2022, **14**, 2256–2265.
- 121 X. Chen, D. Qian, G. Xu, H. Xu, J. Dai and Y. Du, *Colloids Surf., A*, 2019, **573**, 67–72.
- 122 B. Singh, M. B. Gawande, A. D. Kute, R. S. Varma, P. Fornasiero, P. McNeice, R. V. Jagadeesh, M. Beller and R. Zboril, *Chem. Rev.*, 2021, **121**, 13620–13697.
- 123 M. B. Gawande, P. Fornasiero and R. Zboril, *ACS Catal.*, 2020, **10**, 2231–2259.
- 124 B. Singh, V. Sharma, R. P. Gaikwad, P. Fornasiero, R. Zboril and M. B. Gawande, *Small*, 2021, **17**, 2006473.
- 125 H. B. Kale, A. D. Kute, R. P. Gaikwad, P. Fornasiero, R. Zboril and M. B. Gawande, *Coord. Chem. Rev.*, 2024, **502**, 215602.
- 126 H. Zhang, X. Zhang, S. Shi, Q. He, X. He, T. Gan and H. Ji, *ACS Appl. Mater. Interfaces*, 2022, **14**, 53755–53760.
- 127 X. Wang, J. Li, Q. Xue, X. Han, C. Xing, Z. Liang, P. Guardia, Y. Zuo, R. Du, L. Balcells, J. Arbiol, J. Llorca, X. Qi and A. Cabot, *ACS Nano*, 2023, **17**, 825–836.
- 128 M. J. Baruah, A. Dutta, S. Biswas, G. Gogoi, N. Hoque, P. K. Bhattacharyya and K. K. Bania, *ACS Appl. Nano Mater.*, 2022, **5**, 1446–1459.
- 129 K. Biswas, S. Chattopadhyay, Y. Jing, R. Che, G. De, B. Basu and D. Zhao, *Ind. Eng. Chem. Res.*, 2019, **58**, 2159–2169.
- 130 T. J. Bora, N. Hazarika, N. K. Gour, S. Lee, Y.-B. Park, S. Biswas, A. Devi and K. K. Bania, *ACS Appl. Nano Mater.*, 2023, **6**, 17972–17985.
- 131 M. Zhu, Y. Wang, C. Wang, W. Li and G. Diao, *Catal. Sci. Technol.*, 2013, **3**, 952–961.
- 132 J. Lee, J. Kim and T. Hyeon, *Adv. Mater.*, 2006, **18**, 2073–2094.
- 133 B. Hu, L. Warczynski, X. Li, M. Lu, J. Bitzer, M. Heidelmann, T. Eckhard, Q. Fu, J. Schulwitz, M. Merko, M. Li, W. Kleist, C. Hättig, M. Muhler and B. Peng, *Angew. Chem., Int. Ed.*, 2021, **60**, 6807–6815.
- 134 D. Hu, H. Xu, Z. Yi, Z. Chen, C. Ye, Z. Wu, H. F. Garces and K. Yan, *ACS Sustainable Chem. Eng.*, 2019, **7**, 15339–15345.
- 135 C. Wang, L. Salmon, R. Ciganda, L. Yate, S. Moya, J. Ruiz and D. Astruc, *Chem. Commun.*, 2017, **53**, 644–646.
- 136 S. Handa, Y. Wang, F. Gallou and B. H. Lipshutz, *Science*, 2015, **349**, 1087–1091.
- 137 P. Arora, P. Kumar, V. Tomar, M. Sillanpää, R. Kumar Joshi and M. Nemiwal, *Inorg. Chem. Commun.*, 2022, **145**, 109982.
- 138 M. Shahabi Nejad, N. Seyedi, H. Sheibani and S. Behzadi, *Mol. Divers.*, 2019, **23**, 527–539.
- 139 G. Li, L. Yang, J.-J. Liu, W. Zhang, R. Cao, C. Wang, Z. Zhang, J. Xiao and D. Xue, *Angew. Chem., Int. Ed.*, 2021, **60**, 5230–5234.
- 140 S. Liu, T. Li, F. Shi, H. Ma, B. Wang, X. Dai and X. Cui, *Nat. Commun.*, 2023, **14**, 4973.
- 141 C. Gonzalez-Arellano, K. Yoshida, R. Luque and P. L. Gai, *Green Chem.*, 2010, **12**, 1281–1287.
- 142 E. Podyacheva, O. I. Afanasyev, D. V. Vasilyev and D. Chusov, *ACS Catal.*, 2022, **12**, 7142–7198.
- 143 T. Irrgang and R. Kempe, *Chem. Rev.*, 2019, **119**, 2524–2549.
- 144 X. Q. Ng, Y. Zhao and V. Isoni, *ACS Sustainable Chem. Eng.*, 2023, **11**, 12389–12396.
- 145 M. Nallagangula, C. Sujatha, V. T. Bhat and K. Namitharan, *Chem. Commun.*, 2019, **55**, 8490–8493.
- 146 M. Sarno, C. Cirillo and M. Iuliano, *ChemistryOpen*, 2019, **8**, 520–531.
- 147 W. Pickhardt, E. Siegfried, S. Fabig, M. F. Rappen, M. Etter, M. Wohlgemuth, S. Grätz and L. Borchardt, *Angew. Chem., Int. Ed.*, 2023, **62**, e202301490.
- 148 P. Singh and A. C. Shaikh, *Chem. Commun.*, 2023, **59**, 11615–11630.
- 149 X. Zeng, C. Wang, W. Yan, J. Rong, Y. Song, Z. Xiao, A. Cai, S. H. Liang and W. Liu, *ACS Catal.*, 2023, **13**, 2761–2770.
- 150 M. Tarahomi, H. Alinezhad and B. Maleki, *Appl. Organomet. Chem.*, 2019, **33**, e5203.
- 151 M. Gholinejad, J. Ahmadi, C. Nájera, M. Seyedhamzeh, F. Zareh and M. Kompany-Zareh, *ChemCatChem*, 2017, **9**, 1442–1449.
- 152 S. Handa, B. Jin, P. P. Bora, Y. Wang, X. Zhang, F. Gallou, J. Reilly and B. H. Lipshutz, *ACS Catal.*, 2019, **9**, 2423–2431.
- 153 M. B. Gawande, A. K. Rath, P. S. Branco, I. D. Nogueira, A. Velhinho, J. J. Shrikhande, U. U. Indulkar, R. V. Jayaram, C. A. A. Ghumman, N. Bundaleski and O. M. N. D. Teodoro, *Chem. – Eur. J.*, 2012, **18**, 12628–12632.
- 154 M. B. Gawande, A. K. Rath, P. S. Branco, T. M. Potewar, A. Velhinho, I. D. Nogueira, A. Tolstogousov, C. A. A. Ghumman and O. M. N. D. Teodoro, *RSC Adv.*, 2013, **3**, 3611–3617.
- 155 Y. Li, N. Li, W. Jiang, G. Ma and M. M. Zangeneh, *Int. J. Biol. Macromol.*, 2020, **163**, 2162–2171.

- 156 C. Milone, C. Crisafulli, R. Ingoglia, L. Schipilliti and S. Galvagno, *Catal. Today*, 2007, **122**, 341–351.
- 157 J. Lenz, B. C. Campo, M. Alvarez and M. A. Volpe, *J. Catal.*, 2009, **267**, 50–56.
- 158 Q. Hu, S. Wang, Z. Gao, Y. Li, Q. Zhang, Q. Xiang and Y. Qin, *Appl. Catal., B*, 2017, **218**, 591–599.
- 159 Y. Shu, T. Chen, H. C. Chan, L. Xie and Q. Gao, *Chem. – Asian J.*, 2018, **13**, 3737–3744.
- 160 Y. Wang, R. Qin, Y. Wang, J. Ren, W. Zhou, L. Li, J. Ming, W. Zhang, G. Fu and N. Zheng, *Angew. Chem., Int. Ed.*, 2020, **59**, 12736–12740.
- 161 Y. Zhong, P. Liao, J. Kang, Q. Liu, S. Wang, S. Li, X. Liu and G. Li, *J. Am. Chem. Soc.*, 2023, **145**, 4659–4666.
- 162 J. Feng, S. Handa, F. Gallou and B. H. Lipshutz, *Angew. Chem., Int. Ed.*, 2016, **55**, 8979–8983.
- 163 W. Liu, H. Feng, Y. Yang, Y. Niu, L. Wang, P. Yin, S. Hong, B. Zhang, X. Zhang and M. Wei, *Nat. Commun.*, 2022, **13**, 3188.
- 164 J. Ma, X. Mao, C. Hu, X. Wang, W. Gong, D. Liu, R. Long, A. Du, H. Zhao and Y. Xiong, *J. Am. Chem. Soc.*, 2024, **146**, 970–978.
- 165 H. Niu, J. Lu, J. Song, L. Pan, X. Zhang, L. Wang and J.-J. Zou, *Ind. Eng. Chem. Res.*, 2016, **55**, 8527–8533.
- 166 H. Wei, X. Liu, A. Wang, L. Zhang, B. Qiao, X. Yang, Y. Huang, S. Miao, J. Liu and T. Zhang, *Nat. Commun.*, 2014, **5**, 5634.
- 167 K. J. Datta, A. K. Rath, M. B. Gawande, V. Ranc, G. Zoppellaro, R. S. Varma and R. Zboril, *ChemCatChem*, 2016, **8**, 2351–2355.
- 168 M. N. Shaikh, M. A. Aziz, A. N. Kalanthoden, A. Helal, A. S. Hakeem and M. Bououdina, *Catal. Sci. Technol.*, 2018, **8**, 4709–4717.
- 169 M. N. Shaikh, M. M. Abdelnaby, A. S. Hakeem, G. A. Nasser and Z. H. Yamani, *ACS Appl. Nano Mater.*, 2021, **4**, 3508–3518.
- 170 V. G. Chandrashekhara, T. Senthamarai, R. G. Kadam, O. Malina, J. Kašlík, R. Zboril, M. B. Gawande, R. V. Jagadeesh and M. Beller, *Nat. Catal.*, 2022, **5**, 20–29.
- 171 I. Elsayed, M. A. Jackson and E. B. Hassan, *ACS Sustainable Chem. Eng.*, 2020, **8**, 1774–1785.
- 172 X. Wang and K. Gui, *J. Environ. Sci.*, 2013, **25**, 2469–2475.
- 173 X. Li, J. Li, Y. Peng, T. Zhang, S. Liu and J. Hao, *Catal. Sci. Technol.*, 2015, **5**, 4556–4564.
- 174 L. Zhang, J. Li, X. Chu and G.-c. Zhao, *J. Cluster Sci.*, 2016, **27**, 227–239.
- 175 A. N. Campbell and S. S. Stahl, *Acc. Chem. Res.*, 2012, **45**, 851–863.
- 176 K. Schröder, B. Join, A. J. Amali, K. Junge, X. Ribas, M. Costas and M. Beller, *Angew. Chem., Int. Ed.*, 2011, **50**, 1425–1429.
- 177 Y. Hou, M. Niu and W. Wu, *Ind. Eng. Chem. Res.*, 2020, **59**, 16899–16910.
- 178 Z. He, Y. Hou, H. Li, J. Wei, S. Ren and W. Wu, *Chem. Eng. Sci.*, 2023, **280**, 119055.
- 179 Z. He, Y. Hou, H. Li, Y. Wang, S. Ren and W. Wu, *Renewable Energy*, 2023, **211**, 403–411.
- 180 R. Weingarten, A. Rodriguez-Beuerman, F. Cao, J. S. Luterbacher, D. M. Alonso, J. A. Dumesic and G. W. Huber, *ChemCatChem*, 2014, **6**, 2229–2234.
- 181 A. Villa, G. M. Veith, D. Ferri, A. Weidenkaff, K. A. Perry, S. Campisi and L. Prati, *Catal. Sci. Technol.*, 2013, **3**, 394–399.
- 182 D. Wang, A. B. Weinstein, P. B. White and S. S. Stahl, *Chem. Rev.*, 2018, **118**, 2636–2679.
- 183 Y. Liu, H.-Y. Ma, D. Lei, L.-L. Lou, S. Liu, W. Zhou, G.-C. Wang and K. Yu, *ACS Catal.*, 2019, **9**, 8306–8315.
- 184 Z. Wang and H. Wang, *ACS Appl. Mater. Interfaces*, 2023, **15**, 36676–36687.
- 185 G. Qi, T. E. Davies, A. Nasrallah, M. A. Sainna, A. G. R. Howe, R. J. Lewis, M. Quesne, C. R. A. Catlow, D. J. Willock, Q. He, D. Bethell, M. J. Howard, B. A. Murrer, B. Harrison, C. J. Kiely, X. Zhao, F. Deng, J. Xu and G. J. Hutchings, *Nat. Catal.*, 2022, **5**, 45–54.
- 186 F. Gu, X. Qin, M. Li, Y. Xu, S. Hong, M. Ouyang, G. Giannakakis, S. Cao, M. Peng, J. Xie, M. Wang, D. Han, D. Xiao, X. Wang, Z. Wang and D. Ma, *Angew. Chem., Int. Ed.*, 2022, **61**, e202201540.
- 187 L. Geng, M. Zhang, W. Zhang, M. Jia, W. Yan and G. Liu, *Catal. Sci. Technol.*, 2015, **5**, 3097–3102.
- 188 S. Dey, S. Sun and N. S. Mehta, *Carbon Capture Sci. Technol.*, 2021, **1**, 100013.
- 189 B. Zheng, T. Gan, S. Shi, J. Wang, W. Zhang, X. Zhou, Y. Zou, W. Yan and G. Liu, *ACS Appl. Mater. Interfaces*, 2021, **13**, 27029–27040.
- 190 S. Neumann, H. H. Doebl, S. Keil, A. J. Erdt, C. Gutsche, H. Borchert, J. Kolny-Olesiak, J. Parisi, M. Bäumer and S. Kunz, *ACS Catal.*, 2020, **10**, 4136–4150.
- 191 G.-H. Wang, W.-C. Li, K.-M. Jia, B. Spliethoff, F. Schüth and A.-H. Lu, *Appl. Catal., A*, 2009, **364**, 42–47.
- 192 H. Liang, X. Jiang, Z. Qi, W. Chen, Z. Wu, B. Xu, Z. Wang, J. Mi and Q. Li, *Nanoscale*, 2014, **6**, 7199–7203.
- 193 X. C. Jiang and A. B. Yu, *J. Mater. Process. Technol.*, 2009, **209**, 4558–4562.
- 194 S. Najafshir, K. Friedel Ortega, M. Douthwaite, S. Pattison, G. J. Hutchings, C. J. Bondue, K. Tschulik, D. Waffel, B. Peng, M. Deitermann, G. W. Busser, M. Muhler and M. Behrens, *Chem. – Eur. J.*, 2021, **27**, 16809–16833.
- 195 H. Jiang, X. Chen, D. Cui, K. Lu, X. Kong and X. Zhang, *Materials*, 2023, **16**, 3139.
- 196 D. Xu, J. Li, B. Li, H. Zhao, H. Zhu, J. Kou, F. Zhang, Z. Dong and J. Ma, *Chem. Eng. J.*, 2022, **434**, 134545.
- 197 C. Zhou, W. Shi, X. Wan, Y. Meng, Y. Yao, Z. Guo, Y. Dai, C. Wang and Y. Yang, *Catal. Today*, 2019, **330**, 92–100.
- 198 K. Yang, Y. Liu, J. Deng, X. Zhao, J. Yang, Z. Han, Z. Hou and H. Dai, *Appl. Catal., B*, 2019, **244**, 650–659.
- 199 H. Hong, L. Hu, M. Li, J. Zheng, X. Sun, X. Lu, X. Cao, J. Lu and H. Gu, *Chem. – Eur. J.*, 2011, **17**, 8726–8730.
- 200 J. Sheng, W.-C. Li, W.-D. Lu, B. Yan, B. Qiu, X.-Q. Gao, R.-P. Zhang, S.-Z. Zhou and A.-H. Lu, *Appl. Catal., B*, 2022, **305**, 121070.



- 201 T. Ye, J. H. Carter, B. Chen, X. Li, Y. Ye, S. H. Taylor and G. J. Hutchings, *Catal. Commun.*, 2022, **162**, 106383.
- 202 S. Kumar, A. Lyalin, Z. Huang and T. Taketsugu, *ChemistrySelect*, 2022, **7**, e202103795.
- 203 J. H. Carter, T. Bere, J. R. Pitchers, D. G. Hewes, B. D. Vandegehuchte, C. J. Kiely, S. H. Taylor and G. J. Hutchings, *Green Chem.*, 2021, **23**, 9747–9799.
- 204 B. Nigrovski, U. Zavyalova, P. Scholz, K. Pollok, M. Müller and B. Ondruschka, *Carbon*, 2008, **46**, 1678–1686.
- 205 M. de S. Ramos, M. de S. Santos, L. P. Gomes, A. Albornoza and M. do C. Rangel, *Appl. Catal., A*, 2008, **341**, 12–17.
- 206 D. Wang, Z. Liu, F. Liu, X. Ai, X. Zhang, Y. Cao, J. Yu, T. Wu, Y. Bai, T. Li and X. Tang, *Appl. Catal., A*, 1998, **174**, 25–32.
- 207 Z. Tang, W. Zhang, Y. Li, Z. Huang, H. Guo, F. Wu and J. Li, *Appl. Surf. Sci.*, 2016, **364**, 75–80.
- 208 W. Cheng, J. Xu, Y. Wang, F. Wu, X. Xu and J. Li, *J. Colloid Interface Sci.*, 2015, **445**, 93–101.
- 209 W. Cheng, J. Xu, W. Ding, Y. Wang, W. Zheng, F. Wu and J. Li, *Mater. Chem. Phys.*, 2015, **153**, 187–194.
- 210 P. Mikenin, S. Zazhigalov, A. Elyshev, S. Lopatin, T. Larina, S. Cherepanova, D. Pisarev, D. Baranov and A. Zagoruiko, *Catal. Commun.*, 2016, **87**, 36–40.
- 211 P. E. Mikenin, P. G. Tsyrl'nikov, Y. S. Kotolevich and A. N. Zagoruiko, *Catal. Ind.*, 2015, **7**, 155–160.
- 212 I. V. Desyatykh, A. A. Vedyagin, Y. S. Kotolevich and P. G. Tsyrl'nikov, *Combust., Explos. Shock Waves*, 2011, **47**, 677–682.
- 213 A. Yopez, P. Prinsen, A. Pineda, A. M. Balu, A. Garcia, F. L. Y. Lam and R. Luque, *React. Chem. Eng.*, 2018, **3**, 757–768.
- 214 M. Amini, Y. Mousazade, Z. Zand, M. Bagherzadeh and M. M. Najafpour, *Sci. Rep.*, 2021, **11**, 6642.
- 215 M. Lang and H. Li, *ChemSusChem*, 2022, **15**, e202101531.
- 216 J. Rios, J. Lebeau, T. Yang, S. Li and M. D. Lynch, *Green Chem.*, 2021, **23**, 3172–3190.
- 217 S. P. Mekala, M. Prabhu, S. D. Gawali, K. Gopakumar, P. Gogoi, A. R. Bhatkar, G. Mohapatra, E. Unnikrishanan and T. Raja, *Catal. Commun.*, 2022, **168**, 106466.
- 218 A. Rahman, M. Mupa and C. Mahamadi, *Catal. Lett.*, 2016, **146**, 788–799.
- 219 A. K. Patra, A. Dutta and A. Bhaumik, *Chem. – Eur. J.*, 2013, **19**, 12388–12395.
- 220 N. Ameer, R. Bachir, S. Bedrane and A. Choukchou-Braham, *J. Chin. Chem. Soc.*, 2017, **64**, 1096–1103.
- 221 S. Caron, R. W. Dugger, S. G. Ruggeri, J. A. Ragan and D. H. B. Ripin, *Chem. Rev.*, 2006, **106**, 2943–2989.
- 222 Q. Cao, L. M. Dornan, L. Rogan, N. L. Hughes and M. J. Muldoon, *Chem. Commun.*, 2014, **50**, 4524–4543.
- 223 C. A. Hone, D. M. Roberge and C. O. Kappe, *ChemSusChem*, 2017, **10**, 32–41.
- 224 A. Vinu, D. P. Sawant, K. Ariga, K. Z. Hossain, S. B. Halligudi, M. Hartmann and M. Nomura, *Chem. Mater.*, 2005, **17**, 5339–5345.
- 225 A. Pineda, N. Lázaro, A. M. Balu, A. Garcia, A. A. Romero and R. Luque, *Mol. Catal.*, 2020, **493**, 111092.
- 226 B. Török, C. Schäfer and A. Kokel, *Heterogeneous Catalysis in Sustainable Synthesis*, 2022, 317–378.
- 227 C. Anand, P. Srinivasu, S. Alam, V. V. Balasubramanian, D. P. Sawant, M. Palanichamy, V. Murugesan and A. Vinu, *Microporous Mesoporous Mater.*, 2008, **111**, 72–79.
- 228 V. R. Choudhary, S. K. Jana and V. S. Narkhede, *Appl. Catal., A*, 2002, **235**, 207–215.
- 229 Z. Lei, S. Bai, L. Dang, H. Xia, Q. Xu, Y. Cao, L. An, M. Zhao, A.-Y. Lo and S.-B. Liu, *Microporous Mesoporous Mater.*, 2009, **123**, 306–313.
- 230 H. Saeidian, F. M. Moghaddam, A. Pourjavadi, S. Barzegar, R. Soleyman and A. Sohrabi, *J. Braz. Chem. Soc.*, 2009, **20**, 466–471.
- 231 A. Pourjavadi, R. Soleyman and G. R. Barajee, *Starch/Stärke*, 2008, **60**, 467–475.
- 232 G. R. Bardajee, A. Pourjavadi, R. Soleyman and N. Sheikh, *Nucl. Instrum. Methods Phys. Res., Sect. B*, 2008, **266**, 3932–3938.
- 233 N. D. Cuong, N. D. Hoa, T. T. Hoa, D. Q. Khieu, D. T. Quang, V. V. Quang and N. V. Hieu, *J. Alloys Compd.*, 2014, **582**, 83–87.
- 234 H. Sharghi, M. Jokar, M. M. Doroodmand and R. Khalifeh, *Adv. Synth. Catal.*, 2010, **352**, 3031–3044.
- 235 Z. Fang, W. He, T. Tu, N. Lv, C. Qiu, X. Li, N. Zhu, L. Wan and K. Guo, *J. Chem. Eng.*, 2018, **331**, 443–449.
- 236 Q. Zhang, J. Kang and Y. Wang, *ChemCatChem*, 2010, **2**, 1030–1058.
- 237 Y. Tang, Y. Liu, J. Chen, C. He, X. Lu, R. Zhang and X. Liu, *React. Chem. Eng.*, 2023, **8**, 1229–1249.
- 238 K. Wei, S. Yue, X. Hou, Y. Jiang, C. Jiang, Y. Yao, J. Yin and J. Ma, *Int. J. Energy Res.*, 2022, **46**, 10864–10874.
- 239 E. de Smit and B. M. Weckhuysen, *Chem. Soc. Rev.*, 2008, **37**, 2758–2781.
- 240 Y. Gao, L. Shao, S. Yang, J. Hu, S. Zhao, J. Dang, W. Wang, X. Yan and P. Yang, *Catal. Commun.*, 2023, **181**, 106720.
- 241 X. Liu, T. Lin, P. Liu and L. Zhong, *Appl. Catal., B*, 2023, **331**, 122697.
- 242 Y. Xu, X. Li, J. Gao, J. Wang, G. Ma, X. Wen, Y. Yang, Y. Li and M. Ding, *Science*, 2021, **371**, 610–613.
- 243 J. Weiß, Q. Yang, U. Bentrup, E. V. Kondratenko, A. Brückner and C. Kubis, *ChemCatChem*, 2022, **14**, e202200577.
- 244 H. Zhao, Q. Zhu, Y. Gao, P. Zhai and D. Ma, *Appl. Catal., A*, 2013, **456**, 233–239.
- 245 J. Park, K. An, Y. Hwang, J.-G. Park, H.-J. Noh, J.-Y. Kim, J.-H. Park, N.-M. Hwang and T. Hyeon, *Nat. Mater.*, 2004, **3**, 891–895.
- 246 Z. H. Chonco, A. Ferreira, L. Lodya, M. Claeys and E. van Steen, *J. Catal.*, 2013, **307**, 283–294.
- 247 D. J. Duvenhage, C. Schmidt and H. W. Wright, *J. Mater. Sci.*, 2014, **49**, 2810–2823.
- 248 K. Cheng, V. V. Ordonsky, M. Virginie, B. Legras, P. A. Chernavskii, V. O. Kazak, C. Cordier, S. Paul, Y. Wang and A. Y. Khodakov, *Appl. Catal., A*, 2014, **488**, 66–77.

- 249 R. Warringham, N. G. Hamilton, I. P. Silverwood, C. How, P. B. Webb, R. P. Tooze, W. Zhou, C. D. Frost, S. F. Parker and D. Lennon, *Appl. Catal., A*, 2015, **489**, 209–217.
- 250 G. R. Patzke, F. Krumeich and R. Nesper, *Angew. Chem., Int. Ed.*, 2002, **41**, 2446–2461.
- 251 S. K. Mohapatra, S. E. John, S. Banerjee and M. Misra, *Chem. Mater.*, 2009, **21**, 3048–3055.
- 252 R. A. Friedel and R. B. Anderson, *J. Am. Chem. Soc.*, 1950, **72**, 1212–1215.
- 253 H. Becker, R. Güttel and T. Turek, *Catal. Sci. Technol.*, 2016, **6**, 275–287.
- 254 H. Preising and D. Enke, *Colloids Surf., A*, 2007, **300**, 21–29.
- 255 J. Sun, Y. Chen and J. Chen, *Catal. Sci. Technol.*, 2016, **6**, 7505–7511.
- 256 S. Li, G. D. Meitzner and E. Iglesia, *J. Phys. Chem. B*, 2001, **105**, 5743–5750.
- 257 C. G. Visconti, M. Martinelli, L. Falbo, L. Fratalocchi and L. Lietti, *Catal. Today*, 2016, **277**, 161–170.
- 258 H. Ando, Y. Matsumura and Y. Souma, *J. Mol. Catal. A: Chem.*, 2000, **154**, 23–29.
- 259 M. K. Gnanamani, W. D. Shafer, D. E. Sparks and B. H. Davis, *Catal. Commun.*, 2011, **12**, 936–939.
- 260 Y. Yao, X. Liu, D. Hildebrandt and D. Glasser, *Ind. Eng. Chem. Res.*, 2011, **50**, 11002–11012.
- 261 S. Li, A. Li, S. Krishnamoorthy and E. Iglesia, *Catal. Lett.*, 2001, **77**, 197–205.
- 262 B. An, K. Cheng, C. Wang, Y. Wang and W. Lin, *ACS Catal.*, 2016, **6**, 3610–3618.
- 263 J. Wu, L. Wang, B. Lv and J. Chen, *ACS Appl. Mater. Interfaces*, 2017, **9**, 14319–14327.
- 264 R. Shakya, B. D. Kurmi and P. Patel, *Appl. Organomet. Chem.*, 2023, **37**, e7075.
- 265 R. Pratap and V. J. Ram, *Chem. Rev.*, 2014, **114**, 10476–10526.
- 266 D. Insuasty, J. Castillo, D. Becerra, H. Rojas and R. Abonia, *Molecules*, 2020, **25**, 505.
- 267 S. Agarwal, A. Sethiya, J. Soni, N. Sahiba and P. Teli, *Appl. Organomet. Chem.*, 2022, **36**, e6604.
- 268 E. Sheikhsosseini and M. Yahyazadehfar, *Front. Chem.*, 2023, **10**, 984502.
- 269 V. Raj and J. Lee, *Front. Chem.*, 2020, **8**, 623.
- 270 L. Bonsignore, G. Loy, D. Secci and A. Calignano, *Eur. J. Med. Chem.*, 1993, **28**, 517–520.
- 271 M. Costa, T. A. Dias, A. Brito and F. Proença, *Eur. J. Med. Chem.*, 2016, **123**, 487–507.
- 272 C. Konkoy, D. Fick, S. Cai, N. Lan and J. Keana, *PCT Int. Appl. WO0075123*, 2000; *Chem. Abstr.*, 2001, **134**, 29313a.
- 273 S. Luo, C. Ma, M.-Q. Zhu, W.-N. Ju, Y. Yang and X. Wang, *Front. Cell. Neurosci.*, 2020, **14**, 21.
- 274 H. Nagabhushana, S. S. Saundalkar, L. Muralidhar, B. M. Nagabhushana, C. R. Girija, D. Nagaraja, M. A. Pasha and V. P. Jayashankara, *Chin. Chem. Lett.*, 2011, **22**, 143–146.
- 275 S. A. Mirfarjood, M. Mamaghani and M. Sheykhani, *J. Nanostruct. Chem.*, 2017, **7**, 359–366.
- 276 Z. Hajizadeh, F. Radinekiyan, R. Eivazzadeh-keihan and A. Maleki, *Sci. Rep.*, 2020, **10**, 11671.
- 277 J. Mondal, T. Sen and A. Bhaumik, *Dalton Trans.*, 2012, **41**, 6173–6181.
- 278 D. Girija, H. S. Bhojya Naik, B. Vinay Kumar, C. N. Sudhamani and K. N. Harish, *Arabian J. Chem.*, 2019, **12**, 420–428.
- 279 L. Ghandi, M. Kazemi Miraki, M. Karimi, I. Radfar and A. Heydari, *Appl. Organomet. Chem.*, 2019, **33**, e4616.
- 280 E. Eidi, M. Z. Kassae and Z. Nasresfahani, *Appl. Organomet. Chem.*, 2016, **30**, 561–565.
- 281 K. S. Soppimath, D. C. W. Tan and Y. Y. Yang, *Adv. Mater.*, 2005, **17**, 318–323.
- 282 M. B. Gawande, A. Goswami, T. Asefa, H. Guo, A. V. Biradar, D.-L. Peng, R. Zboril and R. S. Varma, *Chem. Soc. Rev.*, 2015, **44**, 7540–7590.
- 283 S. Bashir, A. K. Wahab and H. Idriss, *Catal. Today*, 2015, **240**, 242–247.
- 284 Y. Wang, D. Wang, Q. Fu, D. Liu, Y. Ma, K. Racette, Z. He and F. Liu, *Mol. Pharm.*, 2014, **11**, 3766–3771.
- 285 S. Liu, N. Zhang, Z.-R. Tang and Y.-J. Xu, *ACS Appl. Mater. Interfaces*, 2012, **4**, 6378–6385.
- 286 G. Cotin, C. Kiefer, F. Pertion, D. Ihiawakrim, C. Blanco-Andujar, S. Moldovan, C. Lefevre, O. Ersen, B. Pichon, D. Mertz and S. Bégin-Colin, *Nanomaterials*, 2018, **8**, 881.
- 287 Y. Mao, W. Jiang, S. Xuan, Q. Fang, K. C.-F. Leung, B. S. Ong, S. Wang and X. Gong, *Dalton Trans.*, 2015, **44**, 9538–9544.
- 288 S. Dixit and J. G. Hering, *Chem. Geol.*, 2006, **228**, 6–15.
- 289 B.-H. Jeon, B. A. Dempsey and W. D. Burgos, *Environ. Sci. Technol.*, 2003, **37**, 3309–3315.
- 290 B.-H. Jeon, B. A. Dempsey, W. D. Burgos and R. A. Royer, *Colloids Surf., A*, 2001, **191**, 41–55.
- 291 R. Sitko, E. Turek, B. Zawisza, E. Malicka, E. Talik, J. Heimann, A. Gagor, B. Feist and R. Wrzalik, *Dalton Trans.*, 2013, **42**, 5682–5689.
- 292 A. J. Friedrich, M. Helgeson, C. Liu, C. Wang, K. M. Rosso and M. M. Scherer, *Environ. Sci. Technol.*, 2015, **49**, 8479–8486.
- 293 T. Yan, J. Xu, L. Wang, Y. Liu, C. Yang and T. Fang, *RSC Adv.*, 2015, **5**, 75129–75140.
- 294 M. Ding, Y. Tang and A. Star, *J. Phys. Chem. Lett.*, 2013, **4**, 147–160.
- 295 V. Papaefthimiou, I. Florea, W. Baaziz, I. Janowska, W. H. Doh, D. Begin, R. Blume, A. Knop-Gericke, O. Ersen, C. Pham-Huu and S. Zafeiratos, *J. Phys. Chem. C*, 2013, **117**, 20313–20319.
- 296 J. B. Joshi, A. B. Pandit, K. L. Kataria, R. P. Kulkarni, A. N. Sawarkar, D. Tandon, Y. Ram and M. M. Kumar, *Ind. Eng. Chem. Res.*, 2008, **47**, 8960–8988.
- 297 L. Carbognani, M. F. González, F. Lopez-Linares, C. S. Stull and P. Pereira-Almao, *Energy Fuels*, 2008, **22**, 1739–1746.
- 298 C. Xu, H. E and K. H. Chung, *Energy Fuels*, 2003, **17**, 631–636.

- 299 H. Gao, G. Wang, H. Wang, J. Chen, C. Xu and J. Gao, *Energy Fuels*, 2012, **26**, 1870–1879.
- 300 J. G. Speight, *Catal. Today*, 2004, **98**, 55–60.
- 301 N. Hallale and F. Liu, *Adv. Environ. Res.*, 2001, **6**, 81–98.
- 302 M. Hosseinpour, S. Fatemi and S. J. Ahmadi, *Fuel*, 2015, **159**, 538–549.
- 303 U. Legrand, J. L. Meunier and D. Berk, *Appl. Catal., A*, 2016, **528**, 36–43.
- 304 R. Pristavita, J.-L. Meunier and D. Berk, *Plasma Chem. Plasma Process.*, 2011, **31**, 393–403.
- 305 A. K. Ilunga, B. B. Mamba and T. T. I. Nkambule, *J. Water Process. Eng.*, 2021, **44**, 102402.
- 306 A. K. Patra, A. Dutta and A. Bhaumik, *ACS Appl. Mater. Interfaces*, 2012, **4**, 5022–5028.
- 307 M. Hua, S. Zhang, B. Pan, W. Zhang, L. Lv and Q. Zhang, *J. Hazard. Mater.*, 2012, **211–212**, 317–331.
- 308 S. Yang, Y. Guo, N. Yan, D. Wu, H. He, Z. Qu, C. Yang, Q. Zhou and J. Jia, *ACS Appl. Mater. Interfaces*, 2011, **3**, 209–217.
- 309 A. D. Bokare and W. Choi, *J. Hazard. Mater.*, 2014, **275**, 121–135.
- 310 W. Li, D. Liu, J. Wu, C. Kim and J. D. Fortner, *Environ. Sci. Technol.*, 2014, **48**, 11892–11900.
- 311 O. V. Kharissova, H. V. R. Dias and B. I. Kharisov, *RSC Adv.*, 2015, **5**, 6695–6719.
- 312 D. S. Monje, O. S. Ruiz, G. C. Valencia and D. F. Mercado, *Environ. Sci. Pollut. Res.*, 2022, **29**, 57127–57146.
- 313 L. Jia, Y. Yu, Z.-p. Li, S.-n. Qin, J.-r. Guo, Y.-q. Zhang, J.-c. Wang, J.-c. Zhang, B.-g. Fan and Y. Jin, *Bioresour. Technol.*, 2021, **332**, 125086.
- 314 A. Gallo-Cordova, J. Lemus, F. J. Palomares, M. P. Morales and E. Mazario, *Sci. Total Environ.*, 2020, **711**, 134644.
- 315 K. Q. Jabbar, A. A. Barzinjy and S. M. Hamad, *Environ. Nanotechnol., Monit. Manage.*, 2022, **17**, 100661.
- 316 C. Fang and M. Zhang, *J. Mater. Chem.*, 2009, **19**, 6258–6266.
- 317 A. M. G. C. Dias, A. Hussain, A. S. Marcos and A. C. A. Roque, *Biotechnol. Adv.*, 2011, **29**, 142–155.
- 318 S. Navalon, A. Dhakshinamoorthy, M. Alvaro and H. Garcia, *ChemSusChem*, 2011, **4**, 1712–1730.
- 319 Y. Fan, J. Su, L. Xu, S. Liu, C. Hou, Y. Liu and S. Cao, *Environ. Res.*, 2023, **231**, 116307.
- 320 S. M. Korotta-Gamage and A. Sathasivan, *Chemosphere*, 2017, **167**, 120–138.
- 321 Y. Masue, R. H. Loeppert and T. A. Kramer, *Environ. Sci. Technol.*, 2007, **41**, 837–842.
- 322 S. Daer, J. Kharraz, A. Giwa and S. W. Hasan, *Desalination*, 2015, **367**, 37–48.
- 323 M. Iram, C. Guo, Y. Guan, A. Ishfaq and H. Liu, *J. Hazard. Mater.*, 2010, **181**, 1039–1050.
- 324 R. D. Ambashta and M. Sillanpää, *J. Hazard. Mater.*, 2010, **180**, 38–49.
- 325 M. E. Mahmoud, M. S. Abdelwahab and E. M. Fathallah, *Chem. Eng. J.*, 2013, **223**, 318–327.
- 326 Y. H. Huang, P. K. Peddi, C. Tang, H. Zeng and X. Teng, *Sep. Purif. Technol.*, 2013, **118**, 690–698.
- 327 L.-n. Shi, X. Zhang and Z.-l. Chen, *Water Res.*, 2011, **45**, 886–892.
- 328 H. Liu, Q. Wang, C. Wang and X.-z. Li, *Chem. Eng. J.*, 2013, **215–216**, 90–95.
- 329 H. Hu, Z. Wang and L. Pan, *J. Alloys Compd.*, 2010, **492**, 656–661.
- 330 F. Almomani, R. Bhosale, M. Khraisheh, A. Kumar and T. Almomani, *Appl. Surf. Sci.*, 2020, **506**, 144924.
- 331 F. Fu and Q. Wang, *J. Environ. Manage.*, 2011, **92**, 407–418.
- 332 I. Ali, *Chem. Rev.*, 2012, **112**, 5073–5091.
- 333 P. Xu, G. M. Zeng, D. L. Huang, C. L. Feng, S. Hu, M. H. Zhao, C. Lai, Z. Wei, C. Huang, G. X. Xie and Z. F. Liu, *Sci. Total Environ.*, 2012, **424**, 1–10.
- 334 Z. Wei, R. Xing, X. Zhang, S. Liu, H. Yu and P. Li, *ACS Appl. Mater. Interfaces*, 2013, **5**, 598–604.
- 335 B. Wang, H. Wu, L. Yu, R. Xu, T.-T. Lim and X. W. Lou, *Adv. Mater.*, 2012, **24**, 1111–1116.
- 336 H. Li, W. Li, Y. Zhang, T. Wang, B. Wang, W. Xu, L. Jiang, W. Song, C. Shu and C. Wang, *J. Mater. Chem.*, 2011, **21**, 7878–7881.
- 337 C.-Y. Cao, J. Qu, W.-S. Yan, J.-F. Zhu, Z.-Y. Wu and W.-G. Song, *Langmuir*, 2012, **28**, 4573–4579.
- 338 M. E. Mahmoud, A. A. Yakout, K. H. Hamza and M. M. Osman, *J. Ind. Eng. Chem.*, 2015, **25**, 207–215.
- 339 L.-S. Zhong, J.-S. Hu, H.-P. Liang, A.-M. Cao, W.-G. Song and L.-J. Wan, *Adv. Mater.*, 2006, **18**, 2426–2431.
- 340 J.-S. Hu, L.-S. Zhong, W.-G. Song and L.-J. Wan, *Adv. Mater.*, 2008, **20**, 2977–2982.
- 341 M. B. Gawande, S. N. Shelke, R. Zboril and R. S. Varma, *Acc. Chem. Res.*, 2014, **47**, 1338–1348.
- 342 B. Kong, J. Tang, Z. Wu, J. Wei, H. Wu, Y. Wang, G. Zheng and D. Zhao, *Angew. Chem., Int. Ed.*, 2014, **53**, 2888–2892.
- 343 G. Ali, Y. J. Park, A. Hussain and S. O. Cho, *Nanotechnology*, 2019, **30**, 095601.
- 344 H.-J. Cui, J.-K. Cai, J.-W. Shi, B. Yuan, C.-L. Ai and M.-L. Fu, *RSC Adv.*, 2014, **4**, 10176–10179.
- 345 N. N. Nassar, *J. Hazard. Mater.*, 2010, **184**, 538–546.
- 346 M. Baalousha, *Sci. Total Environ.*, 2009, **407**, 2093–2101.
- 347 Y. Feng, J.-L. Gong, G.-M. Zeng, Q.-Y. Niu, H.-Y. Zhang, C.-G. Niu, J.-H. Deng and M. Yan, *Chem. Eng. J.*, 2010, **162**, 487–494.
- 348 S. R. Kanel, T. K. Das, R. S. Varma, S. Kurwadkar, S. Chakraborty, T. P. Joshi, A. N. Bezbaruah and M. N. Nadagouda, *ACS Environ. Au*, 2023, **3**, 135–152.
- 349 T. A. Kurniawan, M. E. T. Sillanpää and M. Sillanpää, *Crit. Rev. Environ. Sci. Technol.*, 2012, **42**, 1233–1295.
- 350 J. Tuček, K. C. Kemp, K. S. Kim and R. Zbořil, *ACS Nano*, 2014, **8**, 7571–7612.
- 351 T. Mishra and D. K. Mahato, *J. Environ. Chem. Eng.*, 2016, **4**, 1224–1230.
- 352 C. T. Yavuz, J. T. Mayo, W. W. Yu, A. Prakash, J. C. Falkner, S. Yean, L. Cong, H. J. Shipley, A. Kan, M. Tomson, D. Natelson and V. L. Colvin, *Science*, 2006, **314**, 964–967.
- 353 V. Chandra, J. Park, Y. Chun, J. W. Lee, I.-C. Hwang and K. S. Kim, *ACS Nano*, 2010, **4**, 3979–3986.



- 354 W. Yantasee, C. L. Warner, T. Sangvanich, R. S. Addleman, T. G. Carter, R. J. Wiacek, G. E. Fryxell, C. Timchalk and M. G. Warner, *Environ. Sci. Technol.*, 2007, **41**, 5114–5119.
- 355 K. Zhang, V. Dwivedi, C. Chi and J. Wu, *J. Hazard. Mater.*, 2010, **182**, 162–168.
- 356 L. Feng, M. Cao, X. Ma, Y. Zhu and C. Hu, *J. Hazard. Mater.*, 2012, **217–218**, 439–446.
- 357 M. Kilianová, R. Prucek, J. Filip, J. Kolařík, L. Kvítek, A. Panáček, J. Tuček and R. Zbořil, *Chemosphere*, 2013, **93**, 2690–2697.
- 358 E. Iakovleva, P. Maydannik, T. V. Ivanova, M. Sillanpää, W. Z. Tang, E. Mäkilä, J. Salonen, A. Gubal, A. A. Ganeev, K. Kamwilaisak and S. Wang, *J. Cleaner Prod.*, 2016, **133**, 1095–1104.
- 359 M. Martínez-Cabanas, M. López-García, J. L. Barriada, R. Herrero and M. E. Sastre de Vicente, *Chem. Eng. J.*, 2016, **301**, 83–91.
- 360 R. S. Bangari, A. K. Singh, S. Namsani, J. K. Singh and N. Sinha, *ACS Appl. Mater. Interfaces*, 2019, **11**, 19017–19028.
- 361 S. Scurti, S. Dattilo, D. Gintsburg, L. Vigliotti, A. Winkler, S. C. Carroccio and D. Caretti, *ACS Omega*, 2022, **7**, 10775–10788.
- 362 M. Baikousi, A. B. Bourlinos, A. Douvalis, T. Bakas, D. F. Anagnostopoulos, J. Tuček, K. Šafářová, R. Zboril and M. A. Karakassides, *Langmuir*, 2012, **28**, 3918–3930.
- 363 T. Ren, P. He, W. Niu, Y. Wu, L. Ai and X. Gou, *Environ. Sci. Pollut. Res.*, 2013, **20**, 155–162.
- 364 M. Kokate, K. Garadkar and A. Gole, *J. Mater. Chem. A*, 2013, **1**, 2022–2029.
- 365 L. P. Lingamdinne, Y.-Y. Chang, J.-K. Yang, J. Singh, E.-H. Choi, M. Shiratani, J. R. Koduru and P. Attri, *Chem. Eng. J.*, 2017, **307**, 74–84.
- 366 Z. Pan, X. Zhu, A. Satpathy, W. Li, J. D. Fortner and D. E. Giammar, *Environ. Sci. Technol.*, 2019, **53**, 11913–11921.
- 367 P. Miao, Y. Tang and L. Wang, *ACS Appl. Mater. Interfaces*, 2017, **9**, 3940–3947.
- 368 J. Wang, Y. Chen, Z. Zhang, Y. Ai, L. Liu, L. Qi, J. Zhou, Z. Hu, R. Jiang, H. Bao, S. Ren, J. Liang, H. Sun, D. Niu and Q. Liang, *ACS Sustainable Chem. Eng.*, 2018, **6**, 12925–12934.
- 369 S. Xiang, W. Cheng, F. Chi, X. Nie, T. Hayat and N. S. Alharbi, *ACS Appl. Nano Mater.*, 2020, **3**, 1131–1138.
- 370 X. Yang, X. Wang, Y. Feng, G. Zhang, T. Wang, W. Song, C. Shu, L. Jiang and C. Wang, *J. Mater. Chem. A*, 2013, **1**, 473–477.
- 371 Y. Zhu, H. Hou, G. Tang and Q. Hu, *Eur. J. Inorg. Chem.*, 2010, **2010**, 872–878.
- 372 Y. Lin, W. Cai, H. He, X. Wang and G. Wang, *RSC Adv.*, 2012, **2**, 1769–1773.
- 373 T. Josephine, Drinking Water Treatment and Challenges in Developing Countries, in *The Relevance of Hygiene to Health in Developing Countries*, ed. P. Natasha and H. Afsatou Ndama Traore, IntechOpen, Rijeka, 2019, ch. 5.
- 374 S. H. Teo, C. H. Ng, A. Islam, G. Abdulkareem-Alsultan, C. G. Joseph, J. Janaun, Y. H. Taufiq-Yap, S. Khandaker, G. J. Islam, H. Znad and M. R. Awual, *J. Cleaner Prod.*, 2022, **332**, 130039.
- 375 Q. Zhang, G. Rao, J. Rogers, C. Zhao, L. Liu and Y. Li, *Chem. Eng. J.*, 2015, **271**, 180–187.
- 376 W. Yuan and A. L. Zydney, *J. Membr. Sci.*, 1999, **157**, 1–12.
- 377 T. Peik-See, A. Pandikumar, L. H. Ngee, H. N. Ming and C. C. Hua, *Catal. Sci. Technol.*, 2014, **4**, 4396–4405.
- 378 G. Sheng, Y. Li, X. Yang, X. Ren, S. Yang, J. Hu and X. Wang, *RSC Adv.*, 2012, **2**, 12400–12407.
- 379 X. Luo, C. Wang, S. Luo, R. Dong, X. Tu and G. Zeng, *Chem. Eng. J.*, 2012, **187**, 45–52.
- 380 S. V. Kumar, N. M. Huang, N. Yusoff and H. N. Lim, *Mater. Lett.*, 2013, **93**, 411–414.
- 381 A. Sinha and N. R. Jana, *Chem. – Asian J.*, 2013, **8**, 786–791.
- 382 J. Zhu, S. Wei, H. Gu, S. B. Rapole, Q. Wang, Z. Luo, N. Haldolaarachchige, D. P. Young and Z. Guo, *Environ. Sci. Technol.*, 2012, **46**, 977–985.
- 383 V. Georgakilas, M. Otyepka, A. B. Bourlinos, V. Chandra, N. Kim, K. C. Kemp, P. Hobza, R. Zboril and K. S. Kim, *Chem. Rev.*, 2012, **112**, 6156–6214.
- 384 H. Y. Koo, H.-J. Lee, H.-A. Go, Y. B. Lee, T. S. Bae, J. K. Kim and W. S. Choi, *Chem. – Eur. J.*, 2011, **17**, 1214–1219.
- 385 J. Zhu, Z. Luo, S. Wu, N. Haldolaarachchige, D. P. Young, S. Wei and Z. Guo, *J. Mater. Chem.*, 2012, **22**, 835–844.
- 386 Y. He, Q. Sheng, J. Zheng, M. Wang and B. Liu, *Electrochim. Acta*, 2011, **56**, 2471–2476.
- 387 K. Zhou, Y. Zhu, X. Yang and C. Li, *Electroanalysis*, 2011, **23**, 862–869.
- 388 K. Yang, L. Feng, X. Shi and Z. Liu, *Chem. Soc. Rev.*, 2013, **42**, 530–547.
- 389 H. Jabeen, K. C. Kemp and V. Chandra, *J. Environ. Manage.*, 2013, **130**, 429–435.
- 390 P. Zong, S. Wang, Y. Zhao, H. Wang, H. Pan and C. He, *Chem. Eng. J.*, 2013, **220**, 45–52.
- 391 M. Liu, C. Chen, J. Hu, X. Wu and X. Wang, *J. Phys. Chem. C*, 2011, **115**, 25234–25240.
- 392 Y. Zhang, B. Chen, L. Zhang, J. Huang, F. Chen, Z. Yang, J. Yao and Z. Zhang, *Nanoscale*, 2011, **3**, 1446–1450.
- 393 J. Guo, R. Wang, W. W. Tjiu, J. Pan and T. Liu, *J. Hazard. Mater.*, 2012, **225–226**, 63–73.
- 394 A. A. Karamani, A. P. Douvalis and C. D. Stalikas, *J. Chromatogr. A*, 2013, **1271**, 1–9.
- 395 Y. Tang, H. Guo, L. Xiao, S. Yu, N. Gao and Y. Wang, *Colloids Surf., A*, 2013, **424**, 74–80.
- 396 K. C. Kemp, H. Seema, M. Saleh, N. H. Le, K. Mahesh, V. Chandra and K. S. Kim, *Nanoscale*, 2013, **5**, 3149–3171.
- 397 H. Li, Y. Jia, A. Wang, W. Cui, H. Ma, X. Feng and J. Li, *Chem. – Eur. J.*, 2014, **20**, 499–504.
- 398 J. K. Biswas, A. Mitra, M. P. Shah and S. Rodriguez-Couto, in *Development in Wastewater Treatment Research and Processes*, ed. M. Shah, S. Rodriguez-Couto and J. Biswas, Elsevier, 2022, pp. 1–22.
- 399 A. M. Gutierrez, T. D. Dziubla and J. Z. Hilt, *Rev. Environ. Health*, 2017, **32**, 111–117.

- 400 S. Nizamuddin, M. T. H. Siddiqui, N. M. Mubarak, H. A. Baloch, E. C. Abdullah, S. A. Mazari, G. J. Griffin, M. P. Srinivasan and A. Tanksale, in *Nanoscale Materials in Water Purification*, 2019, pp. 447–472.
- 401 N. Nassar, *Iron Oxide Nanoadsorbents for Removal of Various Pollutants from Wastewater: An Overview*, 2012, pp. 81–118.
- 402 M. Li, C. Liu, Z. Zhang, S. Cao, H. Liu, S. Shen and W. Wang, *Sep. Purif. Technol.*, 2022, **281**, 119978.
- 403 Z.-Y. Ma, Y.-P. Guan, X.-Q. Liu and H.-Z. Liu, *J. Appl. Polym. Sci.*, 2005, **96**, 2174–2180.
- 404 P. Janoš, P. Kuráň, V. Pilařová, J. Trögl, M. Šťastný, O. Pelant, J. Henych, S. Bakardjieva, O. Životný, M. Kormunda, K. Mazanec and M. Skoumal, *Chem. Eng. J.*, 2015, **262**, 747–755.
- 405 R. Xiong, Y. Wang, X. Zhang and C. Lu, *RSC Adv.*, 2014, **4**, 22632–22641.
- 406 C. Păcurariu, O. Pașka, R. Ianoș and S. G. Muntean, *Clean Technol. Environ. Policy*, 2016, **18**, 705–715.
- 407 X. Zheng, H. Zheng, R. Zhao, Y. Sun, Q. Sun, S. Zhang and Y. Liu, *Materials*, 2018, **11**, 1312.
- 408 S. Sharma, A. Hasan, N. Kumar and L. M. Pandey, *Environ. Sci. Pollut. Res.*, 2018, **25**, 21605–21615.
- 409 H. Yan, T. Zhang, Y. Yang, J. Li, Y. Liu, D. Qu, L. Feng and L. Zhang, *J. Environ. Manage. Today*, 2024, **351**, 119931.
- 410 I. Dolinová, M. Štrojsová, M. Černík, J. Němeček, J. Macháčková and A. Ševců, *Environ. Sci. Pollut. Res. Int.*, 2017, **24**, 13262–13283.
- 411 M. F. Azizian, I. P. G. Marshall, S. Behrens, A. M. Spormann and L. Semprini, *J. Contam. Hydrol.*, 2010, **113**, 77–92.
- 412 P. P. He, C. S. He, Q. Liu and Y. Mu, *RSC Adv.*, 2017, **7**, 27214–27223.
- 413 M. Chang and Y. H. Shih, *J. Environ. Manage.*, 2018, **224**, 235–242.
- 414 L. Zhang, Y. Zhu, J. Zhang, G. Zeng, H. Dong, W. Cao, W. Fang, Y. Cheng, Y. Wang and Q. Ning, *Waste Manage.*, 2019, **95**, 289–297.
- 415 A. M. Gutierrez, F. C. Leniz, X. Wang, T. D. Dziubla and J. Z. Hilt, *Mat. Sci. Eng., B*, 2022, **277**, 115577.
- 416 P. Falcaro, R. Ricco, A. Yazdi, I. Imaz, S. Furukawa, D. Maspocho, R. Ameloot, J. D. Evans and C. J. Doonan, *Coord. Chem. Rev.*, 2016, **307**, 237–254.
- 417 X. Li, K. Chen, R. Guo and Z. Wei, *Chem. Rev.*, 2023, **123**, 10432–10467.
- 418 D. Lu, M. Qin, C. Liu, J. Deng, G. Shi and T. Zhou, *ACS Appl. Mater. Interfaces*, 2021, **13**, 5357–5367.
- 419 J. R. McKone, N. S. Lewis and H. B. Gray, *Chem. Mater.*, 2014, **26**, 407–414.
- 420 S. C. Shit, I. Mondal, S. Pendem, L. Bai, J. Y. Park and J. Mondal, *ChemElectroChem*, 2018, **5**, 2842–2849.
- 421 T. Ma, L. Zhou, L. k. Chen, Z. Li, L. Wu, P. Christie and Y. Luo, *J. Agric. Food Chem.*, 2016, **64**, 8045–8053.
- 422 S. Santaefemia, E. Torres, R. Mera and J. Abalde, *J. Hazard. Mater.*, 2016, **320**, 315–325.
- 423 A. Vasilescu and J.-L. Marty, *TrAC, Trends Anal. Chem.*, 2016, **79**, 60–70.
- 424 Y. Song, F. Duan, S. Zhang, J.-Y. Tian, Z. Zhang, Z.-W. Wang, C.-S. Liu, W.-M. Xu and M. Du, *J. Mater. Chem. A*, 2017, **5**, 19378–19389.
- 425 N. K. Gupta, J. Bae and K. S. Kim, *J. Environ. Chem. Eng.*, 2021, **9**, 106195.
- 426 X. Wang, C. Liu, X. Li, F. Li and S. Zhou, *J. Hazard. Mater.*, 2008, **153**, 426–433.
- 427 F. Li, X. Wang, Y. Li, C. Liu, F. Zeng, L. Zhang, M. Hao and H. Ruan, *J. Colloid Interface Sci.*, 2008, **321**, 332–341.
- 428 F. B. Li, X. Z. Li, C. S. Liu and T. X. Liu, *J. Hazard. Mater.*, 2007, **149**, 199–207.
- 429 W. Feng and D. Nansheng, *Chemosphere*, 2000, **41**, 1137–1147.
- 430 J. Bandara, U. Klehm and J. Kiwi, *Appl. Catal., B*, 2007, **76**, 73–81.
- 431 S. Linley, Y. Liu, C. J. Ptacek, D. W. Blowes and F. X. Gu, *ACS Appl. Mater. Interfaces*, 2014, **6**, 4658–4668.
- 432 S. Vasantharaj, S. Sathiyavimal, P. Senthilkumar, F. LewisOscar and A. Pugazhendhi, *J. Photochem. Photobiol., B*, 2019, **192**, 74–82.
- 433 S. Qasim, A. Zafar, M. S. Saif, Z. Ali, M. Nazar, M. Waqas, A. U. Haq, T. Tariq, S. G. Hassan, F. Iqbal, X.-G. Shu and M. Hasan, *J. Photochem. Photobiol., B*, 2020, **204**, 111784.
- 434 M. Diab and T. Mokari, *Inorg. Chem.*, 2014, **53**, 2304–2309.
- 435 X. Zhou, H. Yang, C. Wang, X. Mao, Y. Wang, Y. Yang and G. Liu, *J. Phys. Chem. C*, 2010, **114**, 17051–17061.
- 436 H. Zhang, H. Ming, S. Lian, H. Huang, H. Li, L. Zhang, Y. Liu, Z. Kang and S.-T. Lee, *Dalton Trans.*, 2011, **40**, 10822–10825.
- 437 Y. Zhai, Y. Dou, X. Liu, B. Tu and D. Zhao, *J. Mater. Chem.*, 2009, **19**, 3292–3300.
- 438 X. Dong, H. Chen, W. Zhao, X. Li and J. Shi, *Chem. Mater.*, 2007, **19**, 3484–3490.
- 439 Z. Wu, W. Li, P. A. Webley and D. Zhao, *Adv. Mater.*, 2012, **24**, 485–491.
- 440 A.-H. Lu, J.-J. Nitz, M. Comotti, C. Weidenthaler, K. Schlichte, C. W. Lehmann, O. Terasaki and F. Schüth, *J. Am. Chem. Soc.*, 2010, **132**, 14152–14162.
- 441 H. G. Cha, H. S. Noh, M. J. Kang and Y. S. Kang, *New J. Chem.*, 2013, **37**, 4004–4009.
- 442 C. Baumanis, J. Z. Bloh, R. Dillert and D. W. Bahnemann, *J. Phys. Chem. C*, 2011, **115**, 25442–25450.
- 443 W. Zhou, L. Lin, W. Wang, L. Zhang, Q. Wu, J. Li and L. Guo, *J. Phys. Chem. C*, 2011, **115**, 7126–7133.
- 444 M. I. Pariente, F. Martínez, J. A. Melero, J. Á. Botas, T. Velegraki, N. P. Xekoukoulotakis and D. Mantzavinos, *Appl. Catal., B*, 2008, **85**, 24–32.
- 445 J. R. Chueca, R. M. Abad, M. Melero, N. Miguel and J. Narviñ, *Water Technol.*, 2012, **337**, 72–77 <https://dialnet.unirioja.es/servlet/articulo?codigo=3896468>.
- 446 C. Ruales-Lonfat, J. F. Barona, A. Sienkiewicz, M. Bensimon, J. Vélez-Colmenares, N. Benítez and C. Pulgarín, *Appl. Catal., B*, 2015, **166–167**, 497–508.
- 447 L. Guo, F. Chen, X. Fan, W. Cai and J. Zhang, *Appl. Catal., B*, 2010, **96**, 162–168.

- 448 G. Rao, Q. Zhang, H. Zhao, J. Chen and Y. Li, *Chem. Eng. J.*, 2016, **302**, 633–640.
- 449 L. Liu, A. Li, M. Cao, J. Ma, W. Tan, S. L. Suib and G. Qiu, *ACS EST Eng.*, 2022, **2**, 1376–1385.
- 450 F. Yang, J. Pei and H. Zhao, *Langmuir*, 2022, **38**, 3844–3851.
- 451 E. Neyens and J. Baeyens, *J. Hazard. Mater.*, 2003, **98**, 33–50.
- 452 E. Brillas, I. Sirés and M. A. Oturan, *Chem. Rev.*, 2009, **109**, 6570–6631.
- 453 H. Vafaei Molamahmood, W. Geng, Y. Wei, J. Miao, S. Yu, A. Shahi, C. Chen and M. Long, *Chemosphere*, 2022, **291**, 133037.
- 454 T. Tatarchuk, N. Danyliuk, I. Lapchuk, W. Macyk, A. Shyichuk, R. Kutsyk, V. Kotsyubynsky and V. Boichuk, *J. Mol. Liq.*, 2022, **366**, 120267.
- 455 A. Bozzi, T. Yuranova, J. Mielczarski and J. Kiwi, *New J. Chem.*, 2004, **28**, 519–526.
- 456 S.-S. Lin and M. D. Gurol, *Environ. Sci. Technol.*, 1998, **32**, 1417–1423.
- 457 C.-P. Huang and Y.-H. Huang, *Appl. Catal., A*, 2008, **346**, 140–148.
- 458 W. P. Kwan and B. M. Voelker, *Environ. Sci. Technol.*, 2002, **36**, 1467–1476.
- 459 A. L.-T. Pham, F. M. Doyle and D. L. Sedlak, *Environ. Sci. Technol.*, 2012, **46**, 1055–1062.
- 460 M. Hartmann, S. Kullmann and H. Keller, *J. Mater. Chem.*, 2010, **20**, 9002–9017.
- 461 S.-P. Sun and A. T. Lemley, *J. Mol. Catal. A: Chem.*, 2011, **349**, 71–79.
- 462 N. Wang, L. Zhu, M. Lei, Y. She, M. Cao and H. Tang, *ACS Catal.*, 2011, **1**, 1193–1202.
- 463 T. Jiang, A. S. Poyraz, A. Iyer, Y. Zhang, Z. Luo, W. Zhong, R. Miao, A. M. El-Sawy, C. J. Guild, Y. Sun, D. A. Kriz and S. L. Suib, *J. Phys. Chem. C*, 2015, **119**, 10454–10468.
- 464 M. Yang and M. Jonsson, *J. Phys. Chem. C*, 2014, **118**, 7971–7979.
- 465 M. D. Gurol and S.-S. Lin, *J. Adv. Oxid. Technol.*, 2002, **5**, 147–154.
- 466 C. Walling and A. Goosen, *J. Am. Chem. Soc.*, 1973, **95**, 2987–2991.
- 467 C. Gregor, M. Hermanek, D. Jancik, J. Pechousek, J. Filip, J. Hrbac and R. Zboril, *Eur. J. Inorg. Chem.*, 2010, **16**, 2343–2351.
- 468 K. C. Park, F. Wang, S. Morimoto, M. Fujishige, A. Morisako, X. Liu, Y. J. Kim, Y. C. Jung, I. Y. Jang and M. Endo, *Mater. Res. Bull.*, 2009, **44**, 1443–1450.
- 469 H. Lim, J. Lee, S. Jin, J. Kim, J. Yoon and T. Hyeon, *Chem. Commun.*, 2006, 463–465.
- 470 M. Gui, V. Smuleac, L. E. Ormsbee, D. L. Sedlak and D. Bhattacharyya, *J. Nanopart. Res.*, 2012, **14**, 861.
- 471 S. Hsieh and P.-Y. Lin, *J. Nanopart. Res.*, 2012, **14**, 956.
- 472 S. Navalon, M. Alvaro and H. Garcia, *Appl. Catal., B*, 2010, **99**, 1–26.
- 473 C. Zheng, X. Cheng, P. Chen, C. Yang, S. Bao, J. Xia, M. Guo and X. Sun, *RSC Adv.*, 2015, **5**, 40872–40883.
- 474 K.-i. Ishibashi, A. Fujishima, T. Watanabe and K. Hashimoto, *J. Photochem. Photobiol., A*, 2000, **134**, 139–142.
- 475 S. Song, Y. Wang, H. Shen, J. Zhang, H. Mo, J. Xie, N. Zhou and J. Shen, *ACS Appl. Nano Mater.*, 2019, **2**, 7074–7084.
- 476 N. Singh, S. Riyajuddin, K. Ghosh, S. K. Mehta and A. Dan, *ACS Appl. Nano Mater.*, 2019, **2**, 7379–7392.
- 477 S. Liu, L. Mei, X. Liang, L. Liao, G. Lv, S. Ma, S. Lu, A. Abdelkader and K. Xi, *ACS Appl. Mater. Interfaces*, 2018, **10**, 29467–29475.
- 478 P. A. O'Day, A. Pattammattel, P. Aronstein, V. J. Leppert and H. J. Forman, *Environ. Sci. Technol.*, 2022, **56**, 7006–7016.
- 479 F. C. C. Moura, G. C. Oliveira, M. H. Araujo, J. D. Ardisson, W. A. A. Macedo and R. M. Lago, *Appl. Catal., A*, 2006, **307**, 195–204.
- 480 C. Zhang, C. Kong, P. G. Tratnyek and C. Qin, *Environ. Sci. Technol.*, 2022, **56**, 4367–4376.
- 481 N. Shakeel, R. Perveen, M. Imran Ahamed, A. Ahmad and Inamuddin, *Fuel*, 2023, **341**, 127579.
- 482 S. Rawat, N. Misra, S. S. Meena, S. S. Shelkar, N. Kumar N, N. K. Goel and V. Kumar, *Environ. Sci. Pollut. Res.*, 2022, **29**, 82524–82540.
- 483 M. Paljevac, M. Primožič, M. Habulin, Z. Novak and Ž. Knez, *J. Supercrit. Fluids*, 2007, **43**, 74–80.
- 484 L. Cai, L. Chen, L. Zhang, G. Lu, X. He, S. Zhang, H. Sun, Z. Liu and B. Zhao, *ChemPlusChem*, 2013, **78**, 1437–1439.
- 485 J. Virkutyte and R. S. Varma, *Chem. Sci.*, 2011, **2**, 837–846.
- 486 S. K. Lee, H. Chou, T. S. Ham, T. S. Lee and J. D. Keasling, *Curr. Opin. Biotechnol.*, 2008, **19**, 556–563.
- 487 W. J. Goh, V. S. Makam, J. Hu, L. Kang, M. Zheng, S. L. Yoong, C. N. B. Udalagama and G. Pastorin, *Langmuir*, 2012, **28**, 16864–16873.
- 488 V. Zlateski, R. Fuhrer, F. M. Koehler, S. Wharry, M. Zeltner, W. J. Stark, T. S. Moody and R. N. Grass, *Bioconjugate Chem.*, 2014, **25**, 677–684.
- 489 W. Wang, D. I. C. Wang and Z. Li, *Chem. Commun.*, 2011, **47**, 8115–8117.
- 490 Y. Ren, J. G. Rivera, L. He, H. Kulkarni, D.-K. Lee and P. B. Messersmith, *BMC Biotechnol.*, 2011, **11**, 63.
- 491 R. F. H. Dekker, *Appl. Biochem. Biotechnol.*, 1990, **23**, 25–39.
- 492 A. R. Herdt, B.-S. Kim and T. A. Taton, *Bioconjugate Chem.*, 2007, **18**, 183–189.
- 493 X.-m. Li, Q. Yang, Y. Zhang, W. Zheng, X. Yue, D.-b. Wang and G.-m. Zeng, *Water Sci. Technol.*, 2010, **62**, 947–955.
- 494 B. S. Fernandes, N. K. Saavedra, S. I. Maintinguer, L. D. Sette, V. M. Oliveira, M. B. A. Varesche and M. Zaiat, *Appl. Biochem. Biotechnol.*, 2013, **170**, 1348–1366.
- 495 L. Lima de Oliveira, I. C. Silveira Duarte, I. K. Sakamoto and M. B. Amâncio Varesche, *J. Environ. Manage.*, 2009, **90**, 1261–1268.
- 496 C. Jolival, S. Brenon, E. Caminade, C. Mougin and M. Pontié, *J. Membr. Sci.*, 2000, **180**, 103–113.
- 497 X.-y. Jiang, G.-m. Zeng, D.-l. Huang, Y. Chen, F. Liu, G.-h. Huang, J.-b. Li, B.-d. Xi and H.-l. Liu, *World J. Microbiol. Biotechnol.*, 2006, **22**, 909–913.



- 498 A. P. McHale and S. McHale, *Biotechnol. Adv.*, 1994, **12**, 647–652.
- 499 S. R. Couto, *Biotechnol. Adv.*, 2009, **27**, 227–235.
- 500 M. Shin, T. Nguyen and J. Ramsay, *Appl. Microbiol. Biotechnol.*, 2002, **60**, 218–223.
- 501 L. Peng, T. Xie, Y. Lu, H. Fan and D. Wang, *Phys. Chem. Chem. Phys.*, 2010, **12**, 8033–8041.
- 502 J. Lin, M. Sun, B. Su, G. Owens and Z. Chen, *Sci. Total Environ.*, 2019, **659**, 491–498.
- 503 A. Sigdel, J. Lim, J. Park, H. Kwak, S. Min, K. Kim, H. Lee, C. H. Nahm and P.-K. Park, *Environ. Sci.: Water Res. Technol.*, 2018, **4**, 1114–1123.
- 504 C. Bianco, J. E. Patino Higuaita, T. Tosco, A. Tiraferri and R. Sethi, *Sci. Rep.*, 2017, **7**, 12992.
- 505 M. Sarcletti, H. Park, J. Wirth, S. Englisch, A. Eigen, D. Drobek, D. Vivod, B. Friedrich, R. Tietze, C. Alexiou, D. Zahn, B. A. Zubiri, E. Spiecker and M. Halik, *Mater. Today*, 2021, **48**, 38–46.
- 506 G. F. Koopmans, T. Hiemstra, C. Vaseur, W. J. Chardon, A. Voegelin and J. E. Groenenberg, *Sci. Total Environ.*, 2020, **711**, 135220.
- 507 H. Cui, B. Bao, Y. Cao, S. Zhang, J. Shi, J. Zhou and J. Zhou, *Environ. Pollut.*, 2022, **292**, 118323.