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1. Introduction

Growing levels of both natural and man-made contaminants in air and water systems have resulted in a wide range of toxicological hazards that have significant impacts on human health.¹⁻⁴ The public is particularly concerned about the largescale leakage of low-concentration radioactive iodine isotopes (¹²⁹I and ¹³¹I) from nuclear waste and accidents.⁵ ¹²⁹I is a radioactive isotope of iodine with an exceptionally long halflife of 15.7×10^6 years and long-lasting effects on the environment. Despite having a short half-life (about 8 days), ¹³¹I is harmful to the thyroid and interferes with human metabolism.^{6,7} To lessen the effects on the ecosystem and human health, it is imperative to develop techniques for capturing and storing iodine over the long term. The removal of inorganic contaminants from wastewater has been documented using a variety of techniques in recent studies, including filtration, membrane separation, ion exchange, electrochemistry, etc.^{8,9} The adsorption method is superior to the other methods because it can be used to treat a wide range of target pollutants in water and has fewer cost and energy requirements. It can also be utilized in a wide range of pH values. Activated carbon, zeolite, silica, and chalcogenide

Fabrication of bimetallic MOF-74 derived materials for high-efficiency adsorption of iodine[†]

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Owing to their high porosity, open metal sites, and huge surface area, metal–organic framework (MOF) materials are commonly employed in iodine adsorption processes. Bimetallic MOFs have drawn a lot of attention since mono-metal MOFs have been unable to keep up with the demand. Bimetallic MOF materials still have drawbacks, including limited adsorption capacity, extended adsorption time, poor stability, and poor selectivity, despite their positive performance in radioactive iodine capture. It has been therefore difficult to develop adsorbents with quick iodine adsorption rates and high iodine adsorption efficiency. This study investigated the adsorption properties of a series of bimetallic MOF-74 materials (Mn–Co-MOF-74, Mn–Zn-MOF-74, and Mn–Ni-MOF-74) for radioactive iodine, as well as their design and synthesis utilizing the reflux approach. It was discovered that the adsorption performance of Mn–Ni-MOF-74 for radioidine was superior to that of the other two bimetallic MOF-74 materials. Using the bimetallic Mn–Ni-MOF-74 as a precursor, a variety of bimetallic MOF-74 derived carbon compounds (Mn–Ni-CX) were prepared by high-temperature pyrolysis. Simultaneously, the structure of the material and the iodine adsorption characteristics have been thoroughly studied.

elements are currently the most prevalent adsorbents; nevertheless, their ability to adsorb iodine and organoiodides is limited.¹⁰⁻¹² In contrast to conventional commercial adsorbents, emerging porous materials such as covalent organic frameworks (COFs), porous organic polymers (POPs), and metal-organic frameworks (MOFs) have highly customizable pore topologies and abundant surface functionalities.¹³⁻²² Innovative adsorption methods can be used to collect molecular iodine and organic iodides, opening up new possibilities for the development of high-performing adsorbents.

The efficient structure of metal-organic framework (MOF) materials-for example, MOF-74, which is one of the best adsorption materials because of its large specific surface area, uniform pore size, permanent porosity, structural diversity, resistance to high-temperature decomposition, and open metal sites-allows for a variety of applications, including liquid purification, catalysis, gas storage and separation, and structural diversity. Sensing and electrochemical energy storage MOFs have demonstrated promising capabilities in wastewater purification by adsorption methods and have been widely utilized to adsorb heavy metals and other inorganic contaminants from water due to their high porosity, utility, flexibility, and superior crystallinity.²³⁻²⁷ An and co-workers prepared fractionally porous Mg-MOF-74 rich in flaws, which had a strong trapping effect and increased the adsorption capacity of CO₂.²⁸

But as scientists strive for ever-higher MOF performance, these mono-metal MOFs have been unable to keep up with the



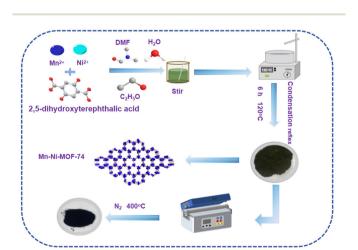
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demand, and thus bimetallic MOFs have drawn a lot of interest.^{29–32} In order for a single metal MOF to form a central bimetallic cluster and retain both the nature of the original MOF and the physical and chemical properties of the second metal, it is necessary to introduce a second metal into a single metal MOF. This allows the MOFs to modify their framework while also enhancing the performance diversity of each individual MOF. For example, Cu and Zn bimetallic embedded porous carbon (CuZn@C) was prepared by carbonizing ZIF-8 pre-grown on CuO nanosheets. It possessed a good porous structure, large specific surface area, uniform bimetallic active site distribution, and strong adsorption capacity (60 mg g^{-1}) for dibenzothiophene (DBT).33 Bimetallic FeCu-MOFs with chlorine-containing functional groups have been designed and synthesized by the hydrothermal method with the aid of ultrasound.³⁴ The prepared bimetallic FeCu-MOFs exhibited good crystallinity, high elemental dispersion, and high removal efficiency for gaseous element mercury (HgO). The mercury equilibrium adsorption capacity of FeCu-MOFs could reach 12.27 mg g^{-1} . Bimetallic MOF materials have demonstrated positive results in the capture of radioactive iodine; nonetheless, many drawbacks remain, including low adsorption capacity, poor stability, and extended adsorption time. It is therefore difficult to develop adsorbents with quick iodine adsorption rates and high iodine adsorption efficiency.

Based on the above considerations, a series of bimetallic MOF-74 materials (Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74) were designed and prepared by the reflux method using the Mn metal ion as the first metal ion and different second metal ions. The adsorption performance of Mn–Ni-MOF-74 for radioactive iodine was studied, and it was found that Mn–Ni-MOF-74 had better adsorption performance than the other two bimetallic MOF-74 materials (Scheme 1). A series of bimetallic MOF-74 derived carbon materials (Mn–Ni-CX) were prepared by pyrolysis at high temperature using the bimetallic Mn–Ni-MOF-74 as a precursor. Mn–Ni-C400 had a strong adsorption capacity of 219 mg g⁻¹ for radioactive iodine. As a result, the bimetallic material formed from Mn–



Scheme 1 Preparation of Mn–Ni-MOF-74 and Mn–Ni-C400.

Ni-MOF-74 proved to be a viable material for trapping radioactive iodine, and this study offered a workable technical method for doing so.

2. Experimental section

2.1 Synthesis of bimetallic MOF-74

2.1.1 Synthesis of Mn–Co-MOF-74. A solid mixture of Mn $(NO_3)_2 \cdot 6H_2O$ (0.8418 g), Co $(NO_3)_2 \cdot 6H_2O$ (0.9725 g) and 2,5dihydroxyterephthalic acid (0.3968 g) was dissolved in 160 mL of *N*,*N'*-dimethylformamide (DMF). After stirring for 10 min, ensuring thorough mixing, a solvent mixture of ethanol and deionized water (1:1, v/v) was added. The resulting solution was transferred to a spherical bottle for condensation reflux at 120 °C for 6 h, followed by standing for 12 h. Then, the product was collected by extraction and filtration, washed three times with DMF and ethanol respectively, and dried in a vacuum drying oven at 80 °C for 6 h.

2.1.2 Synthesis of Mn–Zn-MOF-74. The synthesis method was the same as that of Mn–Co-MOF-74 except that the reactants were changed to $Mn(NO_3)_2 \cdot 6H_2O$ (1.4308 g), Co $(NO_3)_2 \cdot 6H_2O$ (1.7025 g), 2,5-dihydroxyterylene (0.7528 g) and DMF (150 mL).

2.1.3 Synthesis of Mn–Ni-MOF-74. The synthesis method was the same as that of Mn–Co-MOF-74 except that the reactants were changed to $Mn(NO_3)_2 \cdot 6H_2O$ (1.4308 g), Ni $(NO_3)_2 \cdot 6H_2O$ (1.6615 g), 2,5-dihydroxyterylene (0.7528 g) and DMF (150 mL).

2.2 Synthesis of Mn–Ni-MOF-74 derivative materials (Mn–Ni-CX)

2.2.1 Mn–Ni-C200. First, the above prepared Mn–Ni-MOF-74 (100 mg) was placed in a quartz boat and kept in a tube furnace. Subsequently, the furnace temperature was raised to 200 °C within 20 min at a N_2 flow rate of 200 mL min⁻¹ (purity 99.999%). The carbon-based material Mn–Ni-C200 was then synthesized under nitrogen (200 mL min⁻¹) for 60 min. After the carbon-based material was synthesized, the reactor was cooled to room temperature under the protection of N_2 flow.

2.2.2 Mn–Ni-C400. The synthesis method is the same as that of Mn–Ni-C200 except that the heating rate is changed to 40 min and the calcination temperature is changed to 400 $^{\circ}$ C.

2.2.3 Mn–Ni-C600. The synthesis method is the same as that of Mn–Ni-C200 except that the heating rate is changed to 60 min and the calcination temperature is changed to 600 °C.

2.3 Synthesis of monometal MOF-74

2.3.1 Synthesis of Mn-MOF-74. A solid mixture of Mn $(NO_3)_2$ ·6H₂O (1.390 g) and 2,5-dihydroxyterephthalic acid (0.3968 g) was dissolved in 130 mL of DMF. After stirring for 10 min, ensuring thorough mixing, a solvent mixture of ethanol and deionized water (1:1, v/v) was added. The resulting solution was transferred to a spherical bottle for condensation reflux at 120 °C for 5 h, followed by standing for 4 h.

Then, the product was collected by extraction and filtration, washed three times with DMF and ethanol, respectively, and dried in a vacuum drying oven at 80 $^{\circ}$ C for 6 h.

2.3.2 Synthesis of Ni-MOF-74. The synthesis method was the same as that of Mn-MOF-74 except that the reactants were changed to Ni(NO₃)₂·6H₂O (1.6615 g), 2,5-dihydroxyterylene (0.67 g) and DMF (130 mL).

2.4 Synthesis of Mn/Ni-MOF-C400 derivative materials

2.4.1 Mn-MOF-C400. First, the above prepared Mn-MOF-74 (100 mg) was placed in a quartz boat and kept in a tube furnace. Subsequently, the furnace temperature was raised to 400 °C within 40 min at a N₂ flow rate of 400 mL min⁻¹ (purity 99.999%). The carbon-based material (Mn-MOF-C400) was then synthesized under nitrogen (200 mL min⁻¹) for 60 min. After the carbon-based material was synthesized, the reactor was cooled to room temperature under the protection of N₂ flow.

2.4.2 Ni-MOF-C400. The synthesis method is identical to that of Mn-MOF-C400, except that the material is substituted with Ni-MOF-74.

2.5 Characterization

Fourier transform infrared (FTIR) spectroscopy (potassium bromide compression method) was performed using a Varian 6400-400-IR spectrometer. Powder X-ray diffraction (PXRD) data were collected using a CuKa diffractometer. The morphology and structure of Mn-Co-MOF-74, Mn-Zn-MOF-74, Mn-Ni-MOF-74 and the derived Mn-Ni-CX materials were characterized using a scanning electron microscope (SEM, Nova Nano 430) and an energy dispersive X-ray (EDX) detector. The thermal stability of Mn-Co-MOF-74, Mn-Zn-MOF-74, Mn-Ni-MOF-74 and the derived material Mn-Ni-CX was determined using a thermogravimetric analyzer (NETZSCH STA 449C). The UV-vis absorption spectrum was recorded using an SP-1900 UV-vis spectrophotometer. X-ray photoelectron spectroscopy (XPS) measurements were performed using a Kratos Axis 165 photoelectron spectrometer to assess the elemental composition and bonding energy of fresh and negative iodine samples. The Raman spectra of Mn-Ni-C400 and I@Mn-Ni-C400 were recorded using a high-resolution confocal Raman spectrometer (Horiba LabRAM HR800) with a 532 nm laser. The metal contents of the materials were detected by ICP-AES (Thermo ICAP PRO).

2.6 Adsorption experiment

Iodine with a purity of 99.8% was employed as the iodine source in each of the experiment's iodine solutions. Cyclohexane was chosen as the non-polar solvent to prevent polar solvent interference with the host-guest interaction between the MOF and iodine. A predefined amount of iodine was added to cyclohexane, and the mixture was subjected to ultrasonic treatment for 30 min to prepare the iodine-cyclohexane solution.

Initially, a 0.001 mol L^{-1} iodine-cyclohexane solution was prepared at ambient temperature and atmospheric pressure. A

dry tiny glass bottle containing 5 mg of the sample was filled with 5 mL of the iodized cyclohexane solution mentioned above. The bottle was then placed on a stirring table and stirred. Samples were collected every 24 h, at intervals of 0.5, 1, 2, 3, 4, 8, 12 and 24 h. An ultraviolet spectrophotometer was used to detect the absorbance of iodine after samples were taken at predetermined intervals and the solution in the bottle was filtered. The adsorption capacity of the iodine solution was calculated using formula (1):

$$W = [(I_0 - I_t)/I_0 \times C \times V]/m \times 100 \tag{1}$$

where I_0 is the initial absorbance, I_t is the absorbance at time t, C is the concentration of iodine solution, V is the volume of iodine solution, and m is the weight of the sample.

3. Results and discussion

3.1 Structural characterization of Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74

The PXRD patterns of Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74 are shown in Fig. 1a–c. The characteristic peaks of the three bimetallic MOF-74 materials at $2\theta = 6.8^{\circ}$ and 11.7° were consistent with the characteristic diffraction peaks of the simulated PXRD pattern of MOF-74.^{35–37} According to the results, the produced bimetallic MOF-74 possessed the typical MOF-74 structure. It is known that the first metal is replaced by the second metal when the second metal is added to the crystal, keeping the first metal's position unchanged. This shows that the second metal atom now occupies the position previously occupied by the first metal in the lattice.³⁸

The FTIR spectra of Mn-Co-MOF-74, Mn-Zn-MOF-74 and Mn-Ni-MOF-74 were recorded in the frequency range of 4000–500 cm^{-1} (Fig. 1d). First, the peaks at 3500–3300 cm^{-1} of the three bimetallic MOF-74 materials were found to be wide and blunt, due to the stretching vibrations of the –OH group.³⁹ Second, the characteristic peaks of the three materials at 2930 cm^{-1} were caused by the stretching vibration and bending vibration of C-H groups.⁴⁰ Third, the characteristic peaks of the three materials at 1660 and 1550 cm⁻¹ were due to the stretching vibrations of -COOH and C=O.⁴¹ Fourth, the characteristic peaks of the three materials at 1400 cm^{-1} were caused by the C=C stretching vibration of mononuclear aromatics, corresponding to the benzene ring skeleton vibration, indicating that the organic ligand was retained in the target product.42 Fifth, the characteristic peaks of the three materials at 1200 cm⁻¹ were caused by the stretching vibration of the C-O group.43

The thermal stability of the three bimetallic Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74 materials was determined under a nitrogen atmosphere and in the temperature range of 20–800 °C (Fig. 1e). The TG curve made it evident that there were three significant mass loss stages and that the initial decomposition temperatures of the three bimetallic MOF-74 materials were nearly the same. Furthermore, all of

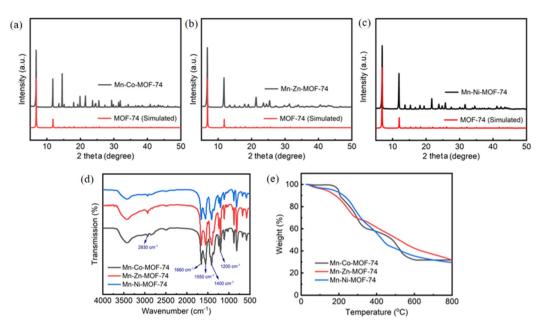


Fig. 1 The PXRD patterns of simulated and fresh samples of Mn–Co-MOF-74 (a), Mn–Zn-MOF-74 (b), and Mn–Ni-MOF-74 (c). (d) FTIR spectra of bimetallic MOF-74. (e) TG curves of bimetallic MOF-74.

the three materials lose weight at nearly the same rate in the end. During the initial phase, the mass loss resulting from the release of guest molecules in the sample channel caused the sample to gradually lose weight. Mn–Co-MOF-74, Mn–Zn-MOF-74, and Mn–Ni-MOF-74 exhibited weight loss rates of 11.10%, 9.50%, and 7.70%, respectively. Due to the release of bound guest molecules in the sample and the mass loss resulting from partial pore collapse, the sample clearly lost weight in the second stage. Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74 exhibited weight loss rates of 37.70%, 46.70%, and 47.40%, respectively. The collapse of the majority of the pores during the third stage caused mass loss and structural damage.

The morphology and elemental distribution of the three bimetallic materials, Mn-Co-MOF-74, Mn-Zn-MOF-74 and Mn-Ni-MOF-74, were characterized using SEM and EDX images. As shown in Fig. S1 and S2,† Mn-Co-MOF-74 and Mn-Zn-MOF-74 exhibited a rod-like structure, and the EDX images revealed that Mn and Co, and Mn and Zn elements were evenly distributed, indicating that the two metal elements were evenly distributed in the bimetallic MOF-74. Mn-Ni-MOF-74 had a petallike structure made up of agglomerated acicular crystals, as shown in Fig. 2. EDX images revealed that Mn and Ni elements were uniformly distributed, suggesting that the two metal elements were uniformly dispersed in Mn-Ni-MOF-74. Mn-Ni-MOF-74 had a distinct petal-like morphology because this material system generated a unique heterogeneous structure during phase transition. Macroscopic strain differences resulted from different volume changes in various phases during cooling. As a result of this strain differential, stress eventually concentrated on the material's surface, where it took the shape of a fracture with petals. The petal-like shape with a greater specific surface area and number of active sites

improved the material's adsorption capacity.^{44,45} According to the above characterization, it was found that the appearance of MOF-74 was affected by the introduction of second metal ions, and the differing morphologies of the three bimetallic MOF-74 materials might be one of the reasons for their different iodine adsorption properties.

3.2 Structural characterization of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600

In order to further investigate the structural changes of Mn–Ni-MOF-74 derived materials during carbonization, Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600 were analyzed by PXRD, as shown in Fig. 3a. When the calcination temperature reached 600 °C, the small-angle diffraction peaks of MOF-74 ($2\theta = 7.0^{\circ}$ and 12.0°) disappeared, and the skeleton of the material collapsed.⁴⁶ The diffraction peaks at $2\theta = 35.1^{\circ}$, 40.6° and 58.7° corresponded to the MnO structure,⁴⁷ the diffraction peaks at $2\theta = 44.4^{\circ}$, 51.8° and 76.3° corresponded to the metal Ni structure,⁴⁸ and the diffraction peak at $2\theta = 47.6^{\circ}$ corresponded to the Mn₃O₄ structure.⁴⁹

The FTIR spectra of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600 were recorded in the frequency range of 4000–500 cm⁻¹, as shown in Fig. 3b. The characteristic peak of Mn–Ni-C200 at 2930 cm⁻¹ was caused by the stretching vibration and bending vibration of the C–H group.⁴⁰ The characteristic peaks of Mn–Ni-C200 at 1656 and 1556 cm⁻¹ were due to the stretching vibrations of –COOH and C=O.⁴¹ The characteristic peaks of Mn–Ni-C400 and Mn–Ni-C600 at 1544 and 1630 cm⁻¹, respectively, were due to the stretching vibration of C=O.⁵⁰ The characteristic peaks of Mn–Ni-C200 at 1403 cm⁻¹, respectively, were caused by the C=C stretching vibration of mononuclear aromatic hydrocarbons, corres-

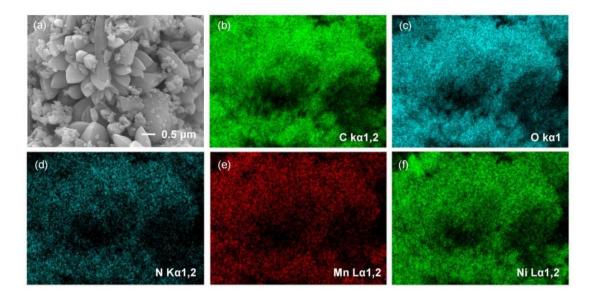


Fig. 2 (a) SEM image of Mn–Ni-MOF-74. (b–f) EDX elemental distribution mapping images of Mn–Ni-MOF-74.

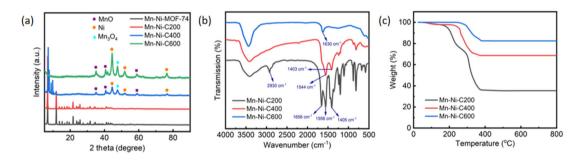


Fig. 3 (a) PXRD patterns of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600. (b) FTIR spectra of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600. (c) TG curves of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600.

ponding to the benzene ring skeleton vibration, indicating that the organic ligand was retained in the target product.⁴²

The thermal stability of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600 derived from Mn–Ni-MOF-74 was measured under a nitrogen atmosphere in the temperature range of 20–800 °C (Fig. 3c). It could be clearly seen that the three derived materials began to decompose after about 200 °C and reached a stable state after 400 °C. The final weight losses of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600 were 64.60%, 31.40% and 17.50%, respectively.

The morphology and elemental distribution of Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600 materials derived from Mn–Ni-MOF-74 were characterized using scanning electron microscopy and EDX images, as shown in Fig. 4, S3 and S4.† The EDX images of the three derived materials show that they are all made of agglomerated acicular crystals and exhibit petal-like shapes. The Mn and Ni elements are also uniformly distributed. With the increase of calcination temperature, the petal structure partially collapsed, and the petal size of Mn–Ni-C600 was the smallest. The findings demonstrated that pyrolysis at various temperatures had an impact on the morphology of the materials derived from Mn–Ni-MOF-74 and that variation in morphology could account for some of the observed differences in iodine adsorption characteristics.

The specific surface area and pore analysis results of Mn-Ni-C200, Mn-Ni-C400 and Mn-Ni-C600 are shown in Fig. 5. The specific surface areas of Mn-Ni-C200, Mn-Ni-C400 and Mn–Ni-C600 were 136, 229 and 262 $m^2 g^{-1}$, respectively, and the average pore radii were 1.2, 9.5 and 5.9 nm, respectively. It was clear that when the calcination temperature increased, the material made of Mn-Ni-MOF-74 had an increased specific surface area. As the temperature increased, Mn-Ni-C400 transformed into a macroporous structure. The material framework disintegrated at around 600 °C, converting Mn-Ni-C600 into a mesoporous structure. It was evident from our previous work⁵¹ that the original Mn-MOF-74 had a BET surface area of up to 386 m² g⁻¹, and the thermogravimetric study revealed that as the temperature increased, the framework of Mn-MOF-74 started to disintegrate. It could be observed from the FTIR spectrum (Fig. S5[†]) that the position of the characteristic peak

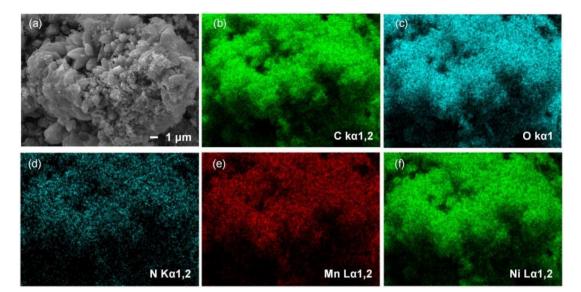


Fig. 4 (a) SEM image of Mn-Ni-C200. (b-f) EDX elemental distribution mapping images of Mn-Ni-C200.

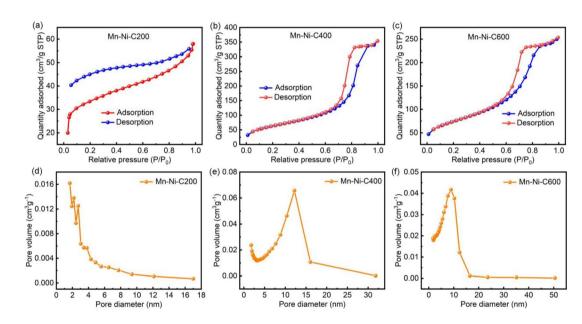


Fig. 5 Specific surface area and pore analysis of Mn-Ni-C200 (a and d), Mn-Ni-C400 (b and e) and Mn-Ni-C600 (c and f).

of monometallic Mn-MOF-74 was the same^{46–49} as that of bimetallic Mn-MOF-74, which indicated that bimetallic Mn-MOF-74 retained the structural characteristics of monometallic Mn-MOF-74. Through comparison, it could be seen that the surface area of the new material decreased during pyrolysis. This might be due to the collapse of the frameworks, which exposed more active sites, proving that the metals in the material played an important role.

3.4 Iodine adsorption performance test

3.4.1 Iodine adsorption performance test of Mn-Co-MOF-74, Mn-Zn-MOF-74 and Mn-Ni-MOF-74. Firstly, the adsorption properties of bimetallic Mn–Co-MOF-74, Mn–Zn-MOF-74 and Mn–Ni-MOF-74 for iodine were studied (Fig. 6). It could be observed that different secondary metal ions had different adsorption effects on iodine. Among the three materials, Mn–Ni-MOF-74 exhibited a strong adsorption capacity for iodine–cyclohexane solution, and the removal rate reached 65.36% (Table 1). Therefore, in this study, bimetallic Mn–Ni-MOF-74 was selected as the precursor, which was treated at a high temperature by the pyrolysis method, and a series of Mn–Ni-MOF-74 derived materials were obtained which were explored for their iodine adsorption properties.

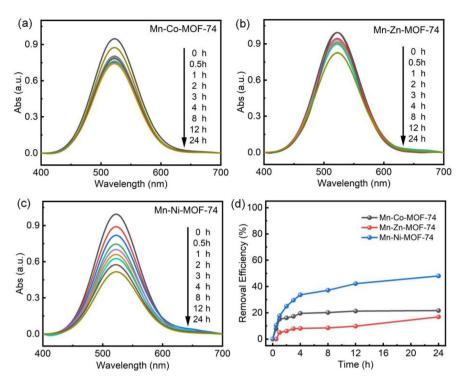


Fig. 6 UV-vis spectra of Mn–Co-MOF-74 (a), Mn–Zn-MOF-74 (b), and Mn–Ni-MOF-74 (c) in iodine–cyclohexane solution at 0.001 mol L^{-1} concentration at different times. (d) Removal rates of three bimetallic MOF-74 materials for iodine solutions at different times.

Table 1 Removal efficiencies of Mn–Co-MOF-74, Mn–Zn-MOF-74, Mn–Ni-MOF-74 and Mn–Ni-CX

Materials	Removal rate (%)
Mn-Co-MOF-74	21.69
Mn-Zn-MOF-74	16.89
Mn-Ni-MOF-74	65.36
Mn-Ni-C200	50.79
Mn-Ni-C400	86.56
Mn-Ni-C600	36.45

3.4.2 Test of the iodine adsorption properties of Mn–Ni-CX. By pyrolyzing bimetallic Mn–Ni-MOF-74 as a precursor at 200, 400 and 600 °C, a series of derivative materials, Mn–Ni-C200, Mn–Ni-C400 and Mn–Ni-C600, were produced. Their iodine adsorption characteristics were then examined. As shown in Fig. 7, different calcination temperatures change the adsorption properties of Mn–Ni-MOF-74 derived materials for iodine. Among them, Mn–Ni-C400 exhibited the best adsorption effect, possibly due to its larger porosity, which enhanced its ability to adsorb iodine solution. It is worth mentioning that after 24 h, the removal rate of Mn–Ni-C400 for iodinecyclohexane solution could reach 86.56%, and the iodinecyclohexane solution changed from purple to colorless (Table 1). Therefore, the high temperature pyrolysis method could improve the adsorption performance of MOFs.

Inductively coupled plasma atomic emission spectrometry (ICP-AES) was used to examine the metal components of the bimetallic MOF-74 and the pyrolyzed Mn–Ni-CX samples, which helped determine how the bimetallic system affected the iodine adsorption performance. The data shown in Table S1[†] indicate that there was a relatively high content of additional secondary metals, such as Zn, Co, and Ni, and that this content increased as the pyrolysis temperature increased. Based on these experimental findings, it was hypothesized that increasing the heat treatment temperature would enhance the iodine adsorption capacity. On the other hand, the iodine adsorption performance declined with excessive metal presence. Excessive metal accumulation might be the cause of this phenomenon as it reduces the dispersion and impairs the adsorption of iodine molecules.⁵²

The iodine adsorption experiment was conducted on single-metal Mn-MOF-74 and Ni-MOF-74 (Fig. S6†) in order to investigate the role played by each metal in Mn–Ni-C400. It could be seen that Mn-MOF-74 had a weaker adsorption capacity for iodine than Ni-MOF-74, and their iodine removal rates were 41.44% and 65.69%, respectively. The iodine adsorption experiment was conducted using the derivative materials of Mn-MOF-74 and Ni-MOF-74, which were developed at the optimal heat treatment temperature of 400 °C. As a result, Ni-MOF-C400 had a considerable adsorption capacity and a clearance rate of up to 79.69%. Therefore, it could be inferred that the second metal Ni played an important role in the iodine adsorption process.

3.4.3 Influence of reaction temperature on iodine removal efficiency. In order to explore how the reaction temperature affects the material's iodine removal efficiency, Mn–Ni-C400 was taken as an example, and a cyclohexane solution of

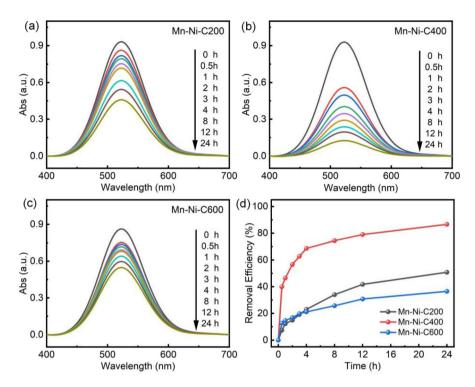


Fig. 7 UV-vis spectra of Mn-Ni-C200 (a), Mn-Ni-C400 (b), and Mn-Ni-C600 (c) in iodine-cyclohexane solution at 0.001 mol L⁻¹ concentration at different times. (d) Removal rate of Mn-Ni-CX for iodine solution at different times.

0.015 mol L⁻¹ iodine was selected at 25, 40 and 60 °C for batch experiments (Fig. S7a–S7c†). The adsorption capacity and adsorption rate of Mn–Ni-C400 for iodine increased on increasing the temperature. At 25, 40 and 60 °C, the removal efficiencies of iodine after 24 h were 86.56%, 97.45% and 87.26%, respectively (Fig. 8a). It was obvious that the material exhibited the best iodine removal efficiency at 40 °C.

3.4.4 Influence of iodine concentration on removal efficiency. In order to explore the effect of the iodine concentration on removal efficiency, three iodine-cyclohexane solutions with concentrations of 0.0010, 0.0015 and 0.0020 mol L^{-1} were tested using the Mn-Ni-C400 material as the sample at 40 °C. The result is shown in Fig. S8a–S8c.† The removal efficiencies of 0.0010, 0.0015 and 0.0020 mol L^{-1} iodine-cyclohexane solutions after 24 h were 97.45%, 59.16% and 37.26%,

respectively (Fig. 8b). Since the three concentrations of iodine solution were treated with the same grade adsorbent, Mn–Ni–C400, the occurrence might be explained by the fact that the quality of the iodine in the solution was higher than the adsorbent's saturation adsorption capacity, which led to a decrease in the effectiveness of iodine removal.

3.4.5 Influence of interfering ions in solution on iodine removal efficiency. Typically, other interfering ions are present in radioactive waste produced during nuclear fission. In order to explore the influence of interfering ions on iodine removal efficiency in solution, iodine adsorption tests were carried out, using Mn–Ni-C400 as an example, in iodine–cyclohexane solutions containing Cl⁻, CO₃²⁻ or a mixture of Cl⁻ + CO₃²⁻, and the results are shown in Fig. S9a–S9c.† The presence of interfering ions in the solution affected the iodine adsorption

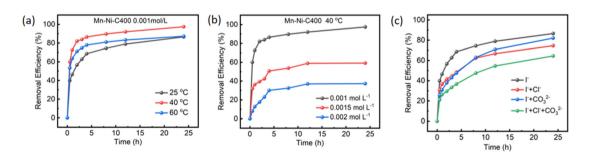


Fig. 8 (a) Removal rate of Mn–Ni-CX at 0.001 mol L^{-1} concentration for iodine–cyclohexane solution at different times. (b) Removal efficiency of Mn–Ni-CX at different adsorption temperatures. (c) Removal efficiency of Mn–Ni-C400 at 60 °C for iodine solutions with different concentrations.

capacity of the adsorbent Mn–Ni-C400. When Cl⁻, CO_3^{2-} and their mixture (Cl⁻ + CO₃²⁻) were added to the iodine solution, the iodine removal efficiencies after 24 h were 74.58%, 82.06% and 64.45%, respectively (Fig. 8c), which were obviously lower than that for the iodine solution (86.56%) without interfering ions. The order of electronegativity of the elements contained in the three anionic groups is I (1.85) < Cl (3.16) < O (3.44). When Cl⁻, CO_3^{2-} or a mixture of Cl⁻ + CO_3^{2-} was added to the iodine solution, the removal efficiency of the mixed solution followed the order I⁻ > (I⁻ + Cl⁻) > (I⁻ + CO_3^{2-}) > (I⁻ + Cl⁻ + CO_3^{2-}) because Cl and O are both more electronegative than I.

3.5 Kinetic analysis of iodine adsorption

The adsorption characteristics of Mn–Ni-C400 were investigated further using the Freundlich and Langmuir models.⁵³ The Langmuir model assumed that the adsorption process was homogeneous on the surface, while the Freundlich model assumed that the adsorption process was heterogeneous on the surface. The linear forms of the Langmuir model and the Freundlich isotherm are expressed by eqn (2) and (3), respectively:

$$\frac{C_e}{q_e} = \frac{1}{k_L q_{max}} + \frac{C_e}{q_{max}} \tag{2}$$

$$\ln q_{\rm e} = \ln K_{\rm F} + \frac{1}{n} \ln C_{\rm e} \tag{3}$$

where C_e is the equilibrium concentration (mg L⁻¹), q_e is the equilibrium adsorption capacity (mg g⁻¹), and q_{max} is the maximum theoretical adsorption capacity (mg g⁻¹). Meanwhile, K_{L} (L mg⁻¹) and K_{F} ((mg g⁻¹) (L mg⁻¹)^{1/n}) are the Langmuir constant and Freundlich constant, respectively, and 1/n is related to adsorption strength.

As shown in Fig. 9, the experimental trend described by the Langmuir model was found to be slightly better than that described by the Freundlich model, with R^2 values of 0.9769 and 0.9348, respectively. This suggested that the homogeneity of the MOF surface resulted in the adsorption of iodine ions in a monolayer manner.⁵⁴ It could be clearly seen from Table 2

Table 2 Dynamic model parameters of Mn-Ni-C400

326 0.0081
0.9769
$(1.69)^{1/n}$
2.83
0.9348

that for the Langmuir model, the q_{max} generated by the C_e/q_e to C_e curve was 326 mg g⁻¹ and the K_L value was 0.0081 L mg⁻¹. A graph of $\log(q_e)$ to $\log(C_e)$ yielded a K_F value of 1.69 (mg g⁻¹) (L mg⁻¹)^{1/n}.

3.6 Adsorption mechanism

3.6.1 Mn–Ni-C400@I characterization of samples after iodine adsorption. First, as seen in Fig. 10b, the FTIR spectra of Mn–Ni-C400 and Mn–Ni-C400@I were recorded in the $4000-500 \text{ cm}^{-1}$ frequency range. After iodine adsorption, it was evident that there was no additional diffraction peak for Mn–Ni-C400@I, and the peak remained very similar to that of Mn–Ni-C400. TG curves were used to test the thermal stability of Mn–Ni-C400 and Mn–Ni-C400@I in a nitrogen environment at 20–800 °C (Fig. 10c). It was clear that the two generated materials undergo degradation at a temperature of approximately 250 °C and stabilized at 400 °C. It could be inferred that the iodine carrying capacity of the Mn–Ni-C400@I material was 10%.

In order to explore whether iodine adsorption would affect the morphology of Mn–Ni-C400, the morphology and elemental distribution of Mn–Ni-C400 and Mn–Ni-C400@I were characterized using SEM and EDX images (Fig. 11). It could be clearly seen that the iodized sample Mn–Ni-C400@I still maintained the original petal-like structure composed of agglomerated acicular crystals, but particles were attached to the surface of the acicular crystals. The EDX image showed the presence of C, N, O, Mn, Ni and I, which were uniformly distributed on the surface of the material.

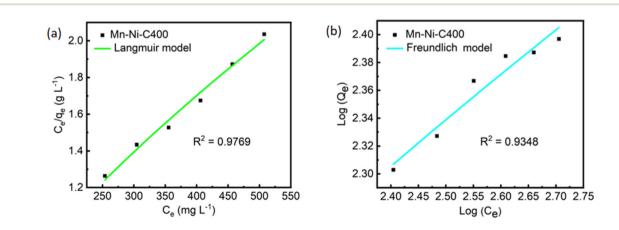


Fig. 9 Langmuir (a) and Freundlich (b) models of Mn–Ni-C400 at six different concentrations for Mn–Ni-C400.

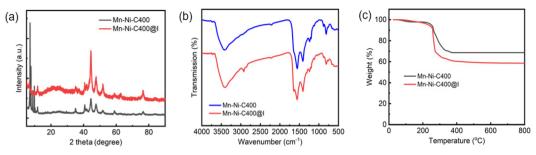


Fig. 10 (a) PXRD patterns of Mn–Ni-C400 and Mn–Ni-C400@I. (b) FTIR spectra of Mn–Ni-C400 and Mn–Ni-C400@I. (c) TG curves of Mn–Ni-C400 and Mn–Ni-C400@I.

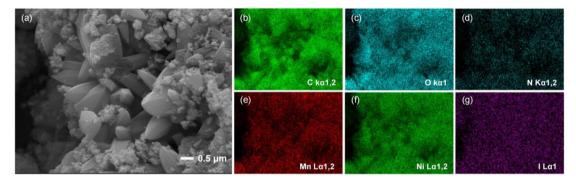


Fig. 11 SEM (a) and EDX elemental distribution mapping (b-g) images of Mn-Ni-C400@I.

The chemical state of iodine in Mn–Ni-C400@I after iodine adsorption was investigated. First, the Raman spectra of Mn–Ni-C400 and Mn–Ni-C400@I before and after iodine adsorption were recorded. As shown in Fig. 12, there is no obvious characteristic peak on the Raman spectra of Mn–Ni-C400, but there are characteristic peaks at 110 and 168 cm⁻¹ on the Raman curve of Mn–Ni-C400@I after iodine adsorption, corresponding to the peaks of I^{3–} and I^{5–}, respectively.⁵⁵ The

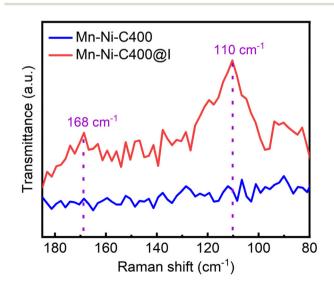


Fig. 12 Raman curves for Mn-Ni-C400 and Mn-Ni-C400@I.

above analysis results showed that the iodine in Mn–Ni-C400@I mainly existed in the form of polyiodide anions, and there was charge interaction with Mn–Ni-C400, which led to the formation of I^{3-} and I^{5-} complexes.⁵⁶

In order to further explore the iodine adsorption mechanism, XPS analysis was performed on Mn–Ni-C400 and Mn–Ni-C400@I. As shown in Fig. 13, the XPS spectrum of Mn–Ni-C400, together with the 3d spectrum, shows 0.005 M (for clear peak intensity) iodine adsorption. After adsorption, I 3d peaks appeared in the range of 610.0 to 640.0 eV, which were attributed to I $3d_{5/2}$ and I $3d_{3/2}$ and adsorbed on Mn–Ni-C400.^{57,58} According to the binding energies of $3d_{5/2}$ and $3d_{3/2}$, iodine was adsorbed on Mn–Ni-C400 in the form of I₂ molecules at 631.0 eV and 619.6 eV, respectively.⁵⁹

According to the above analysis, the adsorption performance of Mn–Ni-C400 for iodine might be related to the following factors (Scheme 2). The first is the macroporous structure of Mn–Ni-C400, whose pore size was 9.5 nm with a BET specific surface area of 229 m² g⁻¹. One theory was that the porosity of Mn–Ni-C400 contributed to its excellent iodine adsorption performance. Secondly, according to the analysis of XPS results, I was mainly adsorbed on Mn–Ni-C400 in the form of simple substances, and 3d peaks of I appeared in the range of 610.0 to 640.0 eV, which was due to the adsorption of I 3d to Mn–Ni-C400. The Raman spectrum study indicated that the iodine in Mn–Ni-C400@I was mostly present as polyiodide anions and that charge interactions with Mn–Ni-C400 led to



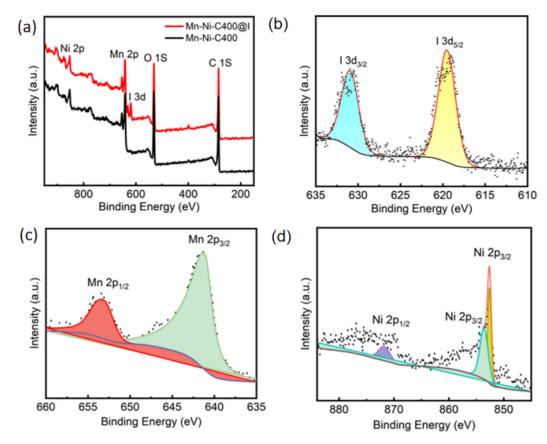
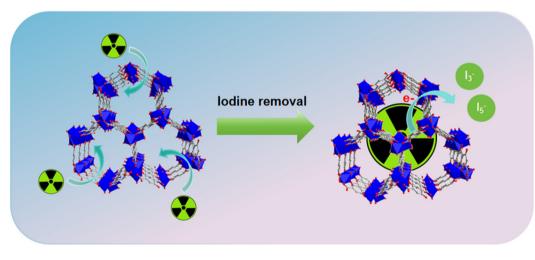


Fig. 13 (a) XPS spectra of Mn–Ni-C400 and Mn–Ni-C400@l. (b) I 3d of Mn–Ni-C400@l. (c) Mn 2p of Mn–Ni-C400@l. (d) Ni 2p of Mn–Ni-C400@l.



Scheme 2 Diagram depicting the iodine adsorption mechanism.

iodine adsorption by Mn–Ni-C400. The Mn 2p spectrum (Fig. 13c) showed the diffraction peaks of Mn $2p_{1/2}$ and Mn $2p_{3/2}$ corresponding to the binding energies of 653.4 eV and 641.3 eV, respectively,^{60–62} and the Ni 2p spectrum (Fig. 13d) showed the diffraction peak of Ni $2p_{1/2}$ corresponding to the binding energy of 871.8 eV.⁶³ Furthermore, the XPS analysis revealed no chemical link between the metal and iodine, and

the binding energies of 852.6 and 853.6 eV were ascribed to the diffraction peak of Ni $2p_{3/2}$.⁶⁴ As a result, Mn–Ni-C400 primarily relies on physical adsorption to adsorb iodine.

Iodine vapor was investigated in order to learn more about the adsorption characteristics of Mn–Ni-C400 (Fig. S10a†). Iodine and 10 mg of Mn–Ni-C400 were heated to 75 °C for 24 h in a closed container for these studies. The amount of iodine vapor adsorbed reached 720 mg g^{-1} once the adsorption approached saturation after 24 hours, as indicated by eqn (4):

$$W = [(M_t - M_0)/m_0] \times 100 \tag{4}$$

where M_t is the mass at time t and m_0 is the initial mass.

This was because, despite initially having a lot of free pores, the adsorption process proceeded more slowly as iodine was adsorbed because fewer free pores were accessible. Iodine vapor in cyclohexane solution exhibited a greater adsorption capacity than iodine itself, likely because the solvent molecules are co-encapsulated.65 The iodine adsorption capacity of Mn-Ni-C400 in cyclohexane was compared with that of other materials reported in the literature.⁶⁶⁻⁶⁸ The results showed that the iodine adsorption capacity of Mn-Ni-C400 in cyclohexane was higher than that of some other materials reported (Table S2[†]). Therefore, Mn-Ni-C400 is a promising material for radioiodine capture. Similarly, Mn-Ni-C400 that had adsorbed iodine solution was subjected to a desorption experiment (Fig. S10b[†]). The Mn-Ni-C400 (5 mg) loaded with iodine solution was added to 5 mL of ethanol. The absorption spectra of iodine released at different times were measured by the UV-vis spectra of the samples. The color of the solvent changed from colorless to dark brown due to the absorption bands of polyiodide ions and iodine molecules in ethanol, observed at 290 and 360 nm, respectively. A comparison of the PXRD patterns of Mn-Ni-C400 and Mn-Ni-C400@I (Fig. 10a) showed that the framework of the material did not collapse after iodine adsorption, indicating the good stability of the material, and the position of the diffraction peak of the material did not change significantly, indicating that the crystal structure of the two materials did not change. Moreover, no diffraction peak corresponding to iodine and metal coordination was observed, further indicating that the adsorption was physical adsorption. Recyclability is a prerequisite for developing iodine-capturing adsorbents that would meet practical production needs, achieve cost-effectiveness, and find useful applications. The adsorption properties of the regenerated adsorbent are shown in Fig. S10c.† After five cycles, the adsorption capacity did not decrease significantly, indicating that the synthetic material is reusable.

4. Conclusion

By using the reflux approach, a number of bimetallic MOF-74 materials were effectively synthesized for the iodine adsorption process. Mn–Ni-MOF-74 exhibited superior adsorption capability for radioiodine. By pyrolyzing a series of bimetallic materials at 400 °C, the Mn–Ni-C400 series exhibited strong iodine adsorption capabilities. Experiments were conducted consecutively in order to further investigate the effects of varying reaction temperature, iodine solution concentration, and interfering ions on removal efficiency. Ultimately, further examination of the process suggested that

the porosity of Mn-Ni-C400 contributes to its high iodine adsorption performance.

Author contributions

Wen-Ze Li: Writing – original draft; resources; and project administration. Fu-Yu Guo: Writing – original draft; visualization; and validation. Jing Li: Writing – original draft; investigation; and formal analysis. Xiao-Sa Zhang: Methodology and software. Yu Liu: Conceptualization; methodology; and project administration. Jian Luan: Writing – review & editing; investigation; and resources.

Data availability

The data supporting this article have been included as part of the ESI.†

Conflicts of interest

The authors declare no competing financial interest.

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References

- R. P. Schwarzenbach, B. I. Escher, K. Fenner, T. B. Hofstetter, C. A. Johnson, U. von Gunten and B. Wehrli, *Science*, 2006, 313, 1072–1077.
- 2 D. Luo, Y. He, J. Tian, J. L. Sessler and X. Chi, *J. Am. Chem. Soc.*, 2022, 144, 113–117.
- 3 J. E. T. Hoeve and M. Z. Jacobson, *Energy Environ. Sci.*, 2012, 5, 8743–8757.
- 4 M. R. Wiesner, G. V. Lowry, P. Alvarez, D. Dionysiou and P. Biswas, *Environ. Sci. Technol.*, 2006, **40**, 4336–4345.
- 5 A. Saiz-Lopez, J. M. C. Plane, A. R. Baker, L. J. Carpenter and R. von Glasow, *Chem. Rev.*, 2012, **112**, 1773–1804.
- 6 F. C. Kupper, M. C. Feiters, B. Olofsson, T. Kaiho, S. Yanagida, M. B. Zimmermann, L. J. Carpenter, G. W. Luther, Z. L. Lu, M. Jonsson and L. Kloo, *Angew. Chem., Int. Ed.*, 2011, 50, 11598–11620.
- 7 A. Saiz-Lopez, J. M. C. Plane, A. R. Baker, L. J. Carpenter, R. von Glasow, J. C. G. Martin, G. McFiggans and R. W. Saunders, *Chem. Rev.*, 2012, 112, 1773–1804.
- 8 F. Ahmadijokani, H. Molavi, M. Rezakazemi, T. M. Aminabhavi and M. Arjmand, *Chem. Rev.*, 2021, **445**, 214037.

- 9 M. Taseidifar, F. Makavipour, R. M. Pashley and A. F. M. M. Rahman, *Environ. Technol.*, 2017, **8**, 182–190.
- 10 R. Li, Y. Zhao, Y. Chen, Z. Liu, B. Han and Z. Li, *Commun. Chem.*, 2018, 1, 69.
- 11 Z. Fei, F. D. Bobbink, E. Paunescu, R. Scopelliti and P. J. Dyson, *Inorg. Chem.*, 2015, **54**, 10504–10512.
- 12 Z. Zhang, X. Dong, J. Yin, Z. G. Li, X. Li, D. Zhang, T. Pan, Q. Lei, X. Liu, Y. Xie, F. Shui, J. Li, M. Yi, J. Yuan, Z. You, L. Zhang, J. Chang, H. Zhang, W. Li, Q. Fang, B. Li, X. H. Bu and Y. Han, *J. Am. Chem. Soc.*, 2022, **144**, 6821– 6829.
- 13 X. Yang, X. Liu, Y. Liu, X. F. Wang, Z. Chen and X. Wang, Front. Chem. Sci. Eng., 2023, 17, 395–403.
- P. H. M. Andrade, M. Moreau, N. Henry, M. T. Bakouche, S. Duval, C. Volkringer, T. Loiseau, M. Hureau and A. Moissette, *J. Phys. Chem. C*, 2023, 127, 4618–4635.
- 15 M. Leloire, C. Walshe, P. Devaux, R. Giovine, S. Duval, T. Bousquet, S. Chibani, J. Paul, A. Moissette and H. Vezin, *Chem. – Eur. J.*, 2022, 28, 2021–4437.
- 16 S. Shetty, N. Baig, S. A. Wahed, A. Hassan, N. Das and B. Alameddine, *Polymers*, 2023, 15, 4153.
- 17 N. Baig, S. Shetty, S. S. Pasha, S. K. Pramanik and B. Alameddine, *Polymer*, 2022, 239, 124467.
- 18 S. Shetty, N. Baig and B. Alameddine, Polymers, 2022, 14, 4818.
- 19 N. Baig, S. Shetty, S. S. Habib, A. A. Husain, S. Al-Mousawi and B. Alameddine, *Polymers*, 2022, **14**, 3727.
- 20 C. Liu, Y. Jin, Z. Yu, L. Gong, H. Wang, B. Yu, W. Zhang and J. Jian, *J. Am. Chem. Soc.*, 2022, **144**, 12390–12399.
- 21 T. Liu, Y. Zhao, M. Song, X. Pang, X. Shi, J. Jia, L. Chi and G. Lu, J. Am. Chem. Soc., 2023, 145, 2544–2552.
- 22 Y. Xie, T. Pan, Q. Lei, C. Chen, X. Dong, Y. Yuan, W. Al Maksoud, L. Zhao, L. Cavallo, I. Pinnau and Y. Han, *Nat. Commun.*, 2022, **13**, 2878.
- 23 K. L. Lauren, E. Kreno, O. K. Farha, M. Allendorf, R. P. Van Duyne and J. T. Hupp, *Chem. Rev.*, 2012, **112**, 1105–1125.
- 24 K. Jayaramulu, D. P. Dubal, A. Schneemann, V. Ranc, C. Perez-Reyes, J. Stráská, T. Kment, M. Otyepka, R. A. Fischer and R. Zboil, *Adv. Funct. Mater.*, 2019, **29**, 1902539.
- 25 J. Yang and Y. W. Yang, Small, 2020, 16, 1906846.
- 26 T. Wang, L. Gao, J. Hou, S. J. A. Herou, J. T. Griffiths, W. Li, J. Dong, S. Gao, M. M. Titirici, R. V. Kumar, A. K. Cheetham, X. Bao, Q. Fu and S. K. Smoukov, *Nat. Commun.*, 2019, **10**, 1340.
- 27 Y. Wang, H. Jin, Q. Ma, K. Mo, H. Mao, A. Feldhoff, X. Cao, Y. Li, F. Pan and Z. Jiang, *Angew. Chem., Int. Ed.*, 2020, **59**, 4365–4369.
- 28 A. H. Fei, T. W. Jian, L. Xin, Y. H. Mei, Y. L. Yun, Z. Hao, S. H. Ming and B. Hao, *Chem. Eng. J.*, 2023, 469, 144052.
- 29 A. Wang, M. Luo, B. Luo, Y. Song, Z. Yang, M. Li and B. Shi, *Ind. Eng. Chem. Res.*, 2022, 61, 3941–3951.
- 30 X. Zhang, J. S. Luo, K. Wan, D. Plessers, B. Sels, J. X. Song, L. G. Chen, T. Zhang, P. Y. Tang, J. R. Morante, J. Arbiol and J. Fransaer, *J. Mater. Chem. A*, 2019, 7, 1616–1628.
- 31 S. M. El-Sheikh, D. I. Osman, O. I. Ali, W. G. Shousha, M. A. Shoeib, S. M. Shawky and S. M. Sheta, *Appl. Surf. Sci.*, 2021, **562**, 150202.

- 32 H. Y. Chen, Y. Q. Huo, K. Z. Cai and Y. Teng, *Synth. Met.*, 2021, **276**, 116761.
- 33 Q. Huo, J. S. Li, X. R. Qi, G. Q. Liu, X. B. Zhang, B. Y. Zhang, Y. Ning, Y. F. Fu, J. M. Liu and S. Y. Liu, *Chem. Eng. J.*, 2019, **378**, 122106.
- 34 Z. Zhang, J. Liu, Z. Wang and J. Y. Zhang, Ind. Eng. Chem. Res., 2021, 60, 781–789.
- R. N. Hu, H. Y. Huang, H. Chen, J. H. Zhang, Q. M. Zhong,
 X. Wu and S. T. Yang, *Environ. Sci.: Processes Impacts*, 2024,
 26, 710–720.
- 36 J. G. Flores, J. A. Pliego, N. M. Guaregua, I. A. Ibarra and M. S. Sanchez, *Catal. Today*, 2022, **394–396**, 295–303.
- 37 Y. Shi, Q. Chu, W. Xiong, J. S. Gao, L. Huang, Y. Q. Zhang and Y. Ding, *Chem. Eng. Process.*, 2021, **159**, 108232.
- 38 H. Kim and C. S. Hong, CrystEngComm, 2021, 23, 1377– 1387.
- 39 Z. Gao, L. Liang, X. Zhang, P. Xu and J. Sun, ACS Appl. Mater. Interfaces, 2021, 13, 61334–61345.
- 40 G. Dang, H. Lam, A. Nguyen, D. Le, T. Truong and N. Phan, J. Catal., 2016, 337, 167–176.
- 41 A. Vimont, J. M. Goupil, J. C. Lavalley, M. Daturi, S. Surble, C. Serre, F. Millange, G. Ferey and N. Audebrand, *J. Am. Chem. Soc.*, 2006, **128**, 3218–3227.
- 42 K. Tan, S. Zuluaga, Q. Gong, P. Canepa, H. Wang, J. Li, Y. J. Chabal and T. Thonhauser, *Chem. Mater.*, 2014, 26, 6886–6895.
- 43 C. R. Muniz, J. M. G. Vallejo, P. J. Merkling and S. Calero, ACS Appl. Mater. Interfaces, 2022, 12, 54980–54990.
- 44 J. Shi, H. B. Tai, D. W. Xu, X. M. Kang and Z. L. Liu, *Dalton Trans.*, 2024, **53**, 3167–3179.
- 45 C. F. Zhao, H. Y. Liu, J. W. Liu, Y. H. Shi, S. G. Wang, Q. W. Tang, X. B. Zhu, H. M. Zhang and Y. Zhao, *RSC Adv.*, 2023, **13**, 8706–8717.
- 46 K. Kim, J. Culp, P. Ohodnicki, P. Thallapally and J. Tao, ACS Appl. Mater. Interfaces, 2021, 13, 35223–35231.
- 47 B. Yang, H. J. Quan, J. Gao, S. H. Wang, N. Wang and C. L. Sun, *J. Alloys Compd.*, 2021, 889, 161680.
- 48 X. J. Hong, C. L. Song, Z. M. Wu, Z. H. Li, Y. P. Cai, C. X. Wang and H. Wang, *Chem. Eng. J.*, 2021, 404, 126566.
- 49 J. X. Feng, S. H. Ye, X. F. Lu, Y. X. Tong and G. R. Li, ACS Appl. Mater. Interfaces, 2015, 7, 11444–11451.
- 50 Q. Zhang, Y. Liu, Z. Wang, P. Wang, Z. Zheng, H. Cheng, X. Qin, X. Zhang, Y. Dai and B. Huang, J. Colloid Interface Sci., 2022, 617, 578–584.
- 51 W. Z. Li, J. Li, W. L. Ma, X. S. Zhang, Y. Liu and J. Luan, *Talanta*, 2024, **269**, 125496.
- 52 C. D. Agostino, G. Brett, G. Divitini, C. Ducati, G. J. Hutchings, M. D. Mantle and L. F. Gladden, ACS Catal., 2017, 7, 4235–4241.
- 53 T. Alghamdi, P. O. Aina, A. A. Rownaghi and F. Rezaei, ACS Appl. Mater. Interfaces, 2023, 15, 33621–33632.
- 54 D. Chen, T. Ma, X. Zhao, X. Jing, R. Zhao and G. Zhu, *ACS Appl. Mater. Interfaces*, 2022, **14**, 47126–47135.
- 55 M. Colovi'c, M. Hajzeri, M. Tramšek, B. Orel and A. K. Surca, Sol. Energy Mater. Sol. Cells, 2021, 220, 110863.

- 56 Y. Z. Tang, Z. J. He, W. J. Xue, H. l. Huang and G. L. Zhang, *Chem. Eng. J.*, 2023, **470**, 144211.
- 57 G. Li, Y. Huang, J. Lin, C. Yu, Z. Liu, Y. Fang, Y. Xue and C. Tang, *Chem. Eng. J.*, 2020, **382**, 122833.
- 58 X. Li, H. Xiong and Q. Jia, ACS Appl. Mater. Interfaces, 2019, 11, 46205-46211.
- 59 J. Chen, A. Gu, E. D. Miensah, Y. Liu, P. Wang, P. Mao, C. Gong, Y. Jiao, K. Chen and Y. Yang, *J. Hazard. Mater.*, 2021, **416**, 126097.
- 60 G. C. Allen, S. J. Harris, J. A. Jutson and J. M. Dyke, *Appl. Surf. Sci.*, 1989, 37, 111–134.
- 61 B. J. Tan, K. J. Klabunde and P. M. A. Sherwood, J. Am. Chem. Soc., 1991, 113, 855–861.
- 62 V. DiCastro and G. Polzonetti, J. Electron Spectrosc. Relat. Phemon., 1989, 48, 117–123.

- 63 A. M. Venezia, R. Bertoncello and G. Deganello, *Surf. Interface Anal.*, 1995, 23, 239–247.
- 64 E. E. Khawaja, M. A. Salim, M. A. Khan, F. F. Al-Adel, G. D. Khattak and Z. Hussain, *J. Non-Cryst. Solids*, 1989, 110, 44–52.
- 65 T. M. Geng, G. F. Chen, L. Z. Ma, C. Zhang, W. Y. Zhang and H. Xu, *Eur. Polym. J.*, 2019, **115**, 37–44.
- 66 R. L. Yu, Q. F. Li, T. Zhang, Z. L. Li and L. Z. Xia, Process Saf. Environ. Prot., 2023, 174, 770–777.
- 67 M. Li, G. Y. Yuan, Y. Zeng, Y. Y. Yang, J. L. Liao, J. J. Yang and N. Liu, *J. Radioanal. Nucl. Chem.*, 2020, **324**, 1167– 1177.
- 68 J. Y. Xian, Z. Y. Huang, X. X. Xie, C. J. Lin, X. J. Zhang, H. Y. Song and S. R. Zheng, *Chin. J. Struct. Chem.*, 2023, 42, 100005.