

## REVIEW

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[rsc.li/materials-advances](https://rsc.li/materials-advances)Recent progress and prospect of  
electrodeposition-type catalysts  
in carbon dioxide reduction utilizations

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In recent years, electrocatalytic reduction of CO<sub>2</sub> has been a focus in the research field. There are also various methods for synthesizing catalysts, such as the hydrothermal method, the arc method, electrospinning, etc. Here, we introduce the electrochemical deposition method. Compared with ordinary synthesis methods, electrodeposition has the advantages of simple processing, controllable conditions, high safety, and environmental friendliness. It is also a promising method for industrialized catalyst synthesis. In this review, we give a detailed introduction to electrodeposition, summarize the research progress of electrodeposition in the synthesis of catalysts, and discuss the key conditions in the preparation process, which are provided as a reference to synthesize next-generation electrodeposited electrocatalysts.

## 1. Introduction

With the intensification of human activities, the emission of CO<sub>2</sub> has gradually become one of the dilemmas faced by human beings. The massive emission of CO<sub>2</sub> leads to serious climate and environmental crises, such as the greenhouse effect and sea level rise.<sup>1</sup> Recently, the conversion of CO<sub>2</sub> into high value-added chemicals, thus alleviating energy problems and solving environmental problems, has been of wide concern. Various energy conversion and storage methods have been proposed, such as photocatalysis,<sup>2</sup> electrocatalysis,<sup>3</sup>

metal-CO<sub>2</sub> batteries,<sup>4</sup> etc. Among them, electrocatalysis is attracting more and more attention due to its high selectivity and energy utilization. Under the combined action of electricity and a catalyst, CO<sub>2</sub> can be converted into a series of high value-added products, such as CO,<sup>5–7</sup> formic acid,<sup>8,9</sup> methane,<sup>10</sup> ethylene,<sup>11</sup> and ethanol.<sup>12</sup> Researchers are also working on reducing CO<sub>2</sub> to C<sub>3</sub>–C<sub>4</sub> products.<sup>13</sup> Therefore, the selection of catalysts is particularly important for the carbon dioxide reduction reactions (CDRRs).

In order to improve the conversion efficiency of catalysts, the synthesis method plays a crucial role in controlling the structure and performance of electrocatalysts. Recently, various methods for synthesizing catalysts have also been developed by researchers, such as the hydrothermal method,<sup>14</sup> the

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impregnation method,<sup>15</sup> *etc.* Although the catalysts synthesized by these synthetic methods have the advantages of large specific surface area and less agglomeration, there are also many limitations. These synthetic methods often require harsh environments, additional surfactants or capping agents, and high temperature conditions. The morphology and microstructure of nanomaterials cannot be easily and finely controlled. Moreover, the generated waste is highly toxic, and the mixture of pollutants and catalysts affects their long-term catalytic activity. In this context, electrodeposition is a promising alternative method for catalyst preparation. Electrodeposition has the following advantages: (1) fine control of electrodeposition can yield catalysts strongly bonded to the substrate with good homogeneity. For example, electrodes, current density, voltage, electrolyte composition, *etc.* can be easily regulated. (2) Morphologically controlled nanostructures can be prepared. (3) The deposition conditions are convenient and the operation is simple. However, electrodeposition also presents significant challenges, namely, the large experimental parameter space and the influence of the substrate on the morphology and chemical composition of the catalyst.

In this review, we introduce the recent progress of electrodeposition in the synthesis of catalysts in the CDRRs. Fig. 1 shows the main topics of this review. Various electrodeposition methods, including potentiostatic deposition, galvanostatic deposition and co-deposition, are discussed. And their advantages and challenges in CDRR applications are also discussed. In addition, we also discussed the influence of experimental parameters on the synthesis of the catalyst, including the deposition time, pH, additives and other factors. Finally, the research, challenges and future prospects of electrodeposition methods in the CDRRs are described.

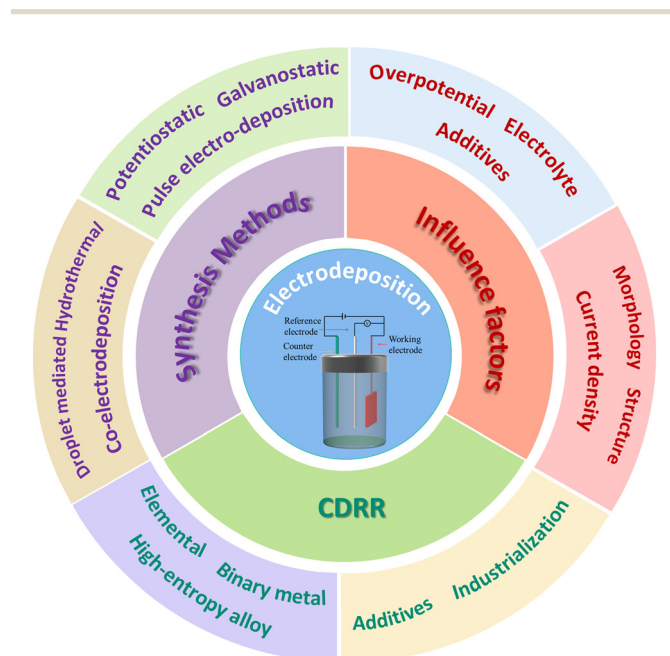


Fig. 1 An overview of the electrodeposition topics of this review.

## 2. Brief description of electrodeposition

### 2.1 Principle of electrodeposition

Electrodeposition typically occurs in a three-electrode system in which a metal electrode is immersed in a specific electrolyte solution and an electric field is applied to deposit the desired substance. Specifically, the first step is to reduce cations on the substrate surface to form adsorption atoms, which migrate to energy-favorable sites. Atoms deposited at other sites then cluster on the previous particles, forming the nucleus of the new phase. These nuclei will grow in different dimensions finally, and it is clear that many nuclei will form on the surface of the matrix. When a monolayer is formed on the surface of the substrate, electrodeposition takes place on this monolayer instead of the original substrate. It can be expected that the first layer of deposition formed will have a decisive influence on the morphology and structure of the following electrodeposition. Electrodeposition technology has many applications in the field of catalysis, ranging from deposition of single metals to alloys,<sup>16,17</sup> metal oxides<sup>18,19</sup> and even high entropy alloys.<sup>20</sup>

### 2.2 Apparatus for electrodeposition

Electrodeposition is generally carried out in a three-electrode system. A reference electrode is introduced into the conventional two-electrode system (working electrode and opposite electrode) to stabilize the working electrode. Therefore, the control and measurement of current and potential can be realized simultaneously in the three-electrode system. The device mainly includes the following three parts: the working electrode, counter electrode, and reference electrode. To be specific, the electrodeposition process and the subsequent electrocatalytic reaction take place at the working electrode, which possesses excellent electrical conductivity and chemical inertness. A polarization circuit is formed between the counter electrode and the working electrode to make the current on the working electrode unblocked. The potential of the counter electrode will change with the change of current. Therefore, a reference electrode is needed to ensure the accuracy of the test. The ideal reference electrode has some characteristics:<sup>21</sup> (1) electrode reaction is reversible and conforms to the Nernst equation; (2) electric potential does not change with time; and (3) it is able to remain stable when a tiny current is passed, and is insensitive to temperature and other factors.

## 3. Electrodeposition method

Electrochemical reduction of carbon dioxide is a promising method, which depends on the morphology, surface composition and structural characteristics of the catalyst. In recent years, researchers have made many explorations to design catalysts with high selectivity, high activity and excellent stability. Catalysts with various morphologies have also been reported, such as foam, thin film, dendrite, plate, crystal, *etc.*



In this chapter, we will discuss in detail the method of preparing the catalyst by electrodeposition.

### 3.1 Galvanostatic electrodeposition

In galvanostatic deposition the current is kept constant and the thickness and morphology of catalyst deposition is controlled by controlling the current density and deposition time. Fig. 2a shows a schematic diagram of one-step deposition of a nanocrystalline bismuth electrode with a constant current in a two-electrode system.<sup>22</sup> Chen *et al.* used stainless steel as the counter electrode, polycrystalline copper foil as the working electrode, and a bath of 10 mM  $\text{Bi}^{3+}$  in 0.2 M  $\text{NO}_3^-$ . At 15  $\text{mA cm}^{-2}$ , the morphology and deposition thickness of the catalyst were optimized by controlling the deposition time. Nano-Bi branches were initially formed on the surface of the matrix after deposition for 500 s, and sharp spiniform secondary structures were formed at 800 s and 1200 s. When the deposition time was extended to 1500 s, the branches formed into grains, and Bi-agglomerated films were obtained. The Bi

film electrode deposited at 1200 s exhibits high formate selectivity at  $-1.5$  V (vs. Ag/AgCl), with a faradaic efficiency (FE) of 97.5%, and remains above 90% after 108 h of operation. Its excellent selectivity and stability are closely related to its spiny structure.

In galvanostatic deposition, time and current are the two most important variables. Wang *et al.* deposited Sn on copper foil by controlling for a change in current density over the same deposition time (Fig. 2b).<sup>23</sup> The catalyst was deposited at current densities of 5, 10, 15 and 20  $\text{mA cm}^{-2}$  at a controlled deposition time of 10 min. At a current density of 5  $\text{mA cm}^{-2}$ , the small current density is not enough to deposit enough Sn to cover the matrix. For current densities of 10 and 15  $\text{mA cm}^{-2}$ , this system is suitable to create fine and compact particles. As for the current density of 20  $\text{mA cm}^{-2}$ , due to the serious hydrogen evolution reaction, the structure of the prepared catalyst is relatively loose and forms a columnar shape. It can be seen that the electrodeposition parameters can significantly control the morphology of the catalyst, resulting in the

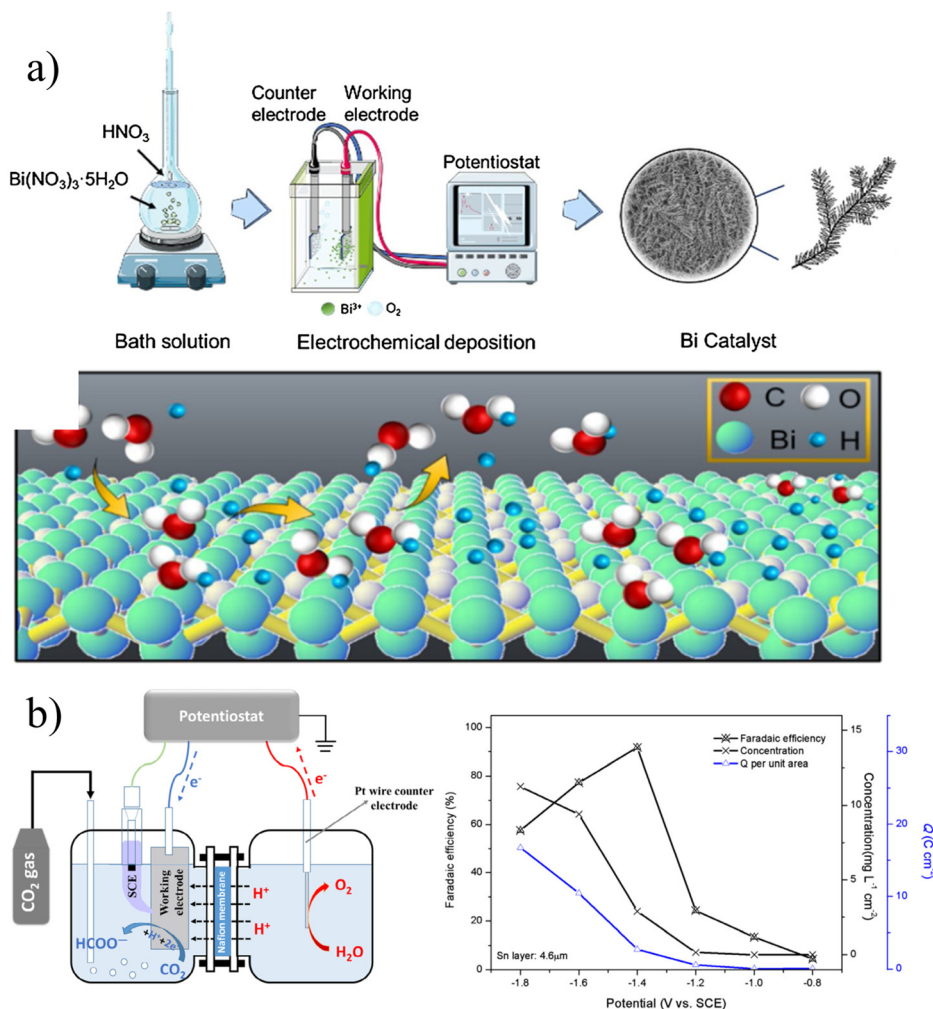


Fig. 2 (a) Schematic diagram of the two-electrode system for constant current deposition of bismuth electrodes. Reproduced with permission.<sup>22</sup> Copyright 2021, Elsevier. (b) Schematic diagram of electrocatalytic reduction of carbon dioxide in a three-electrode system and a summary of its performance. Reproduced with permission.<sup>23</sup> Copyright 2016, Elsevier.



formation of dendritic, granular, columnar and other morphologies.

### 3.2 Potentiostatic electrodeposition

Potentiostatic deposition is a method of applying a constant potential deposition for a certain period of time during the electrodeposition process. Scholten *et al.* deposited nano-dendrite copper on Ag foil and Pt foil, respectively.<sup>24</sup> Electrodeposition was completed by applying a voltage of  $-1.25$  V (*vs.* reversible hydrogen electrode, RHE) in  $0.05$  M  $\text{CuSO}_4$ . What is more interesting is that they treated the substrate with oxygen plasma for different periods of time, which increased the surface roughness. The substrate treatment not only affects the morphology of the deposition, but also inhibits the hydrogen evolution reaction.

In the three-electrode system, the potential can be better controlled to adjust the morphology, surface structure and other properties of the catalyst, so as to obtain the most ideal catalyst. He *et al.* reported the synthesis of  $\text{Cu}_x\text{Au}_y$  NWAs (nanowire arrays) in different proportions (*i.e.*,  $\text{CuAu}$ ,  $\text{Cu}_3\text{Au}$ , and  $\text{CuAu}_3$ ) by the potentiostatic pulse electrodeposition method.<sup>25</sup> The optimized  $\text{Cu}_x\text{Au}_y$  NWAs showed high ethanol selectivity, with the FE of ethanol up to 45% at  $-0.7$  V<sub>RHE</sub>. They controlled the atomic ratio by electrodeposition potential and further regulated the surface electronic structure of the catalyst. They found that during the CDRR process, due to the dense nanoarrays, the diffusion of  $\text{OH}^-$  and  $^*\text{CO}$  was restricted, resulting in higher local pH and  $^*\text{CO}$  concentration on the nanowire surface, thus facilitating ethanol production.

The morphology and catalytic performance of the materials prepared using different electrodeposition methods are also divergent. Zhao *et al.* prepared hexagonal Bi sheets on copper foil by electrodeposition.<sup>26</sup> The Bi film was deposited on a Cu substrate by the potentiostatic method, direct current electrodeposition method and pulse electrodeposition method, respectively. When the total charge passed is 20C, the deposition terminates. As shown in Fig. 3b, they prepared hexagonal, cubic and dendritic catalysts by different electrodeposition methods, respectively. The study showed that Bi slices prepared at a constant potential contained a large number of sharp edges and corners, which could improve the local electric field intensity and promote the rapid transfer of electrons. When the overpotential is  $-0.65$  V, the FE of formate is close to 100%, and the yield is  $96.37 \mu\text{mol h}^{-1} \text{cm}^{-2}$ .

### 3.3 Co-electrodeposition method

Co-electrodeposition is generally used to deposit two or more metals for porous nanomaterials. By controlling the composition of precursors, deposition potential and other conditions, it is easy to control the deposition thickness and composition. Fontecave *et al.* report on a porous dendritic Ag–Zn alloy catalyst with an ultra-high specific surface area prepared by co-deposition (Fig. 4a).<sup>27</sup> The combination of Ag and Zn produces a highly CO biased catalytic environment, showing a faradaic efficiency of more than 91% and no significant loss of selectivity at 40 h ( $\text{FE}_{\text{CO}} > 90\%$ ). As shown in Fig. 4b,

Wang *et al.* prepared Cu–Sn alloys by co-electrodeposition in a three-electrode system.<sup>28</sup> The electrodeposition solution contained  $0.2 \text{ mol L}^{-1} \text{SnSO}_4$  and  $1.5 \text{ mol L}^{-1} \text{H}_2\text{SO}_4$ . Before electrodeposition, the pretreated foam Cu was immersed in the electrolyte to obtain its own source of  $\text{Cu}^{2+}$  ions. The catalyst was obtained by applying a constant current of  $4.0 \text{ mA cm}^{-2}$  at 0.01–60 s on the electrode. The catalyst has a large active surface area, which is one of the reasons for its superior selectivity to formate.

### 3.4 Pulse electrodeposition method

Pulse electrodeposition has pulse conduction time and pulse off time. During pulsed electrodeposition, the deposition ions consumed at the cathode–solution interface can be replenished within the pulse interval. Therefore, a higher peak of current density can be used to obtain smaller nanomaterials. Lee *et al.* deposited Bi catalyst with a nanosheet structure on copper foil by the pulse electrodeposition method.<sup>29</sup> Bi nanosheet has more edges and corners, which is conducive to the generation of a local strong electric field and the highly selective production of  $\text{HCOOH}$ . Fig. 5 shows the Bi catalyst deposited under DC and pulse conditions, respectively. Some Bi particles were formed on the Cu substrate by DC deposition for 60 s, while the nanostructure changed to the dendritic form by DC deposition for 120 s. On the other hand, the nanosheet structure was formed by 6 times repeated pulse electrodeposition. A series of catalysts with different morphologies can be synthesized by pulse electrodeposition with different pulse periods and current densities.

Pulse electrodeposition can yield catalysts with special structures by controlling the parameters. For example, Yu *et al.* designed a Cu–Pd heterostructure,<sup>30</sup> and they synthesized the  $\text{CuCl-PdO}_x$  precursor by double-potential pulsed electrodeposition. The treated electrode was reduced at  $-1.6$  V (*vs.* Ag/AgCl) for 100 s to obtain Cu–Pd heterojunction. The catalyst has a unique selectivity for  $\text{CH}_4$  with an FE of 32%. Furthermore, Zhang *et al.* provided a new strategy for the preparation of highly (111) textured nanotwinned copper (nt-Cu) by medium-frequency pulse electrodeposition.<sup>31</sup> The effect of  $\text{Cu}^{2+}$  concentration on the structure was discussed in detail. A simple and robust method for the future large-scale preparation of (111) nt-Cu is also proposed.

### 3.5 Hydrothermal deposition and droplet mediated control of microstructure

There are also some more stringent conditions in the electrodeposition methods to meet special requirements. Researchers have done a lot of work to control the size and morphology of nanoparticles. Dick *et al.* first demonstrated a method for depositing platinum nanoparticles onto a graphite substrate.<sup>32</sup> By adjusting the experimental parameters, including the concentration of the metal precursor in the droplet, deposition time, deposition potential and other factors, the ability to control the size, roughness and overall morphology of nanoparticles was demonstrated. By introducing glycerol into water droplets,



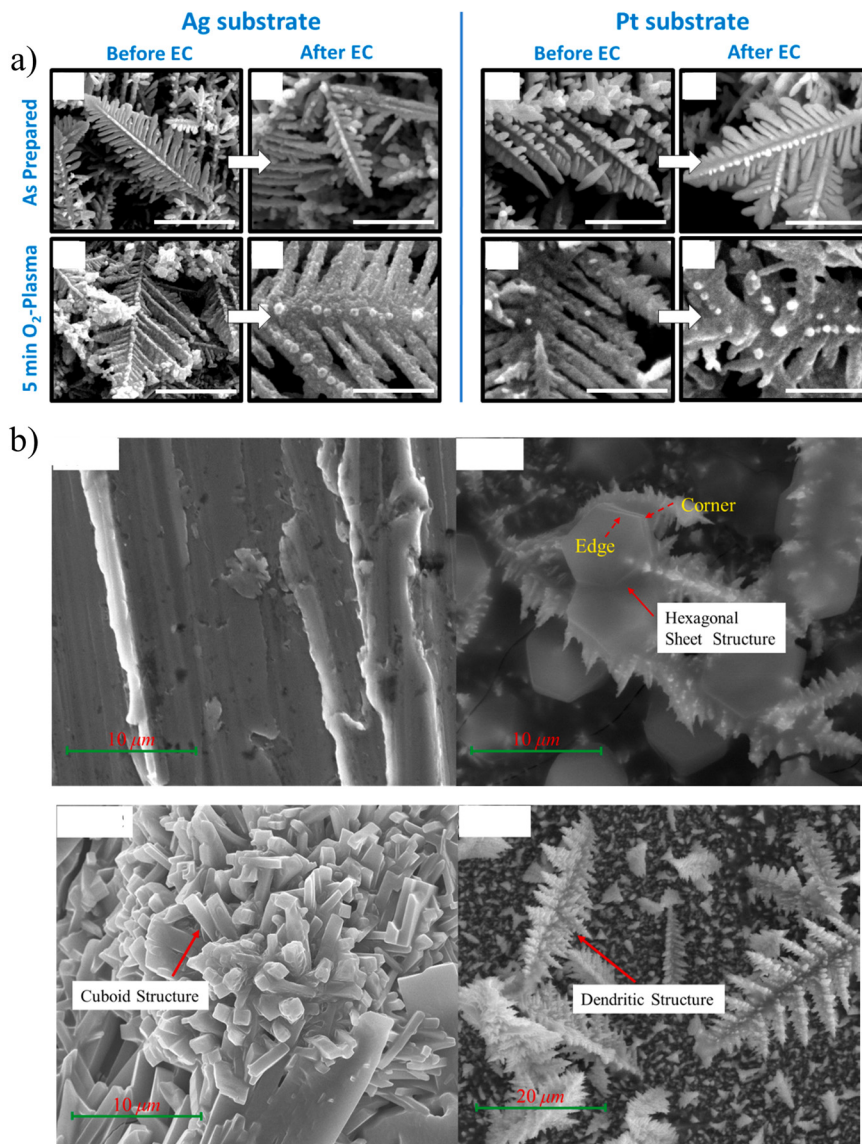


Fig. 3 (a) Scanning electron microscopy (SEM) images of catalysts prepared under different conditions before and after the CDRR reaction. Reproduced with permission.<sup>24</sup> Copyright 2019, American Chemical Society. (b) SEM images of copper and deposits of Bi obtained by different electrodeposition methods: constant potential, CP; direct current, DC; and pulse current, PC. Reproduced with permission.<sup>26</sup> Copyright 2021, Elsevier.

Dick's research group demonstrated the control of droplet mediated electrodeposition on the porosity of nanomaterials.<sup>33</sup>

Non-self-supported catalysts usually exist in the powder form and are supported on the carrier by a binder. Inevitably, the use of a binder reduces the conductivity of the electrode, and prolonged catalysis also strips the bonded catalyst from the carrier. Yao *et al.* first reported the preparation of mesoporous Ni<sub>0.8</sub>Fe<sub>0.2</sub> films by hydrothermal deposition as an OER catalyst.<sup>34</sup> They show that hydrothermal deposition accelerates H<sub>2</sub> overflow due to high temperature, and high pressure and rapid gas overflow facilitate the formation of more active sites compared to conventional electrodeposition methods.

The catalyst and matrix prepared by this method have a stronger binding force. Although hydrothermal deposition and droplet mediated electrodeposition are a little more

complicated than traditional electrodeposition methods, they also have many references for the synthesis of catalysts. It is believed that the application of these methods to CDRRs will have a good prospect.

In this section, we introduce different electrodeposition methods. The main controllable parameter of chronopotentiometry electrodeposition is current density, which is simple to analyze and easy to deposit alloys. However, the electrode potential is easily fluctuated by external influences, and it is difficult to accurately control the current density. Therefore, it is more suitable for the three-electrode system. Due to the different reduction potentials of different metal ions, the chronoamperometry method is more suitable for the deposition of single metal or multi-layer metal. Pulse electrodeposition has three independent parameters, and the ion concentration on the



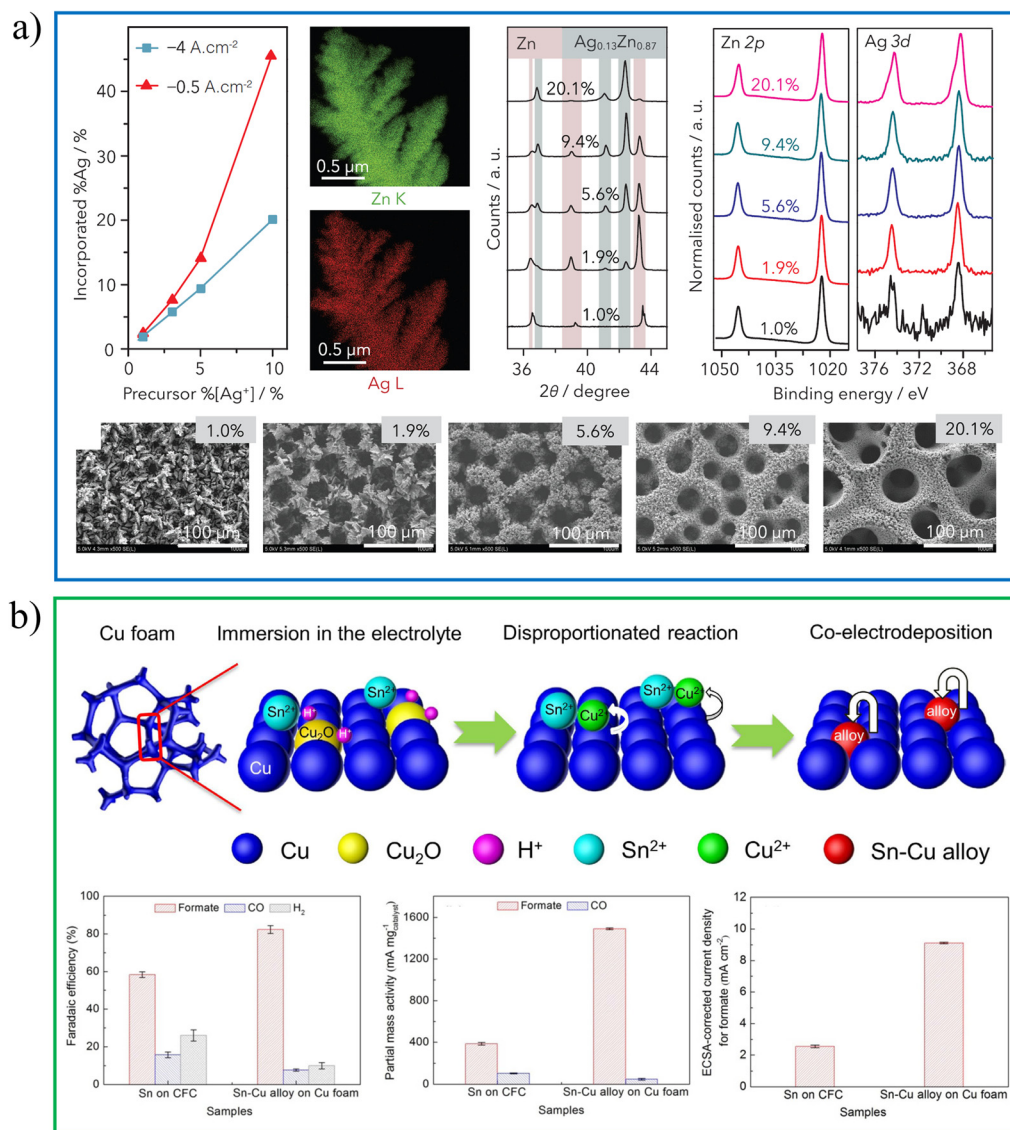


Fig. 4 (a) Ag-Zn alloy growth and characterization. Reproduced with permission.<sup>27</sup> Copyright 2020, Elsevier Inc. (b) Schematic diagram of SnCu alloy preparation and catalytic performance. Reproduced with permission.<sup>28</sup> Copyright 2020, Elsevier.

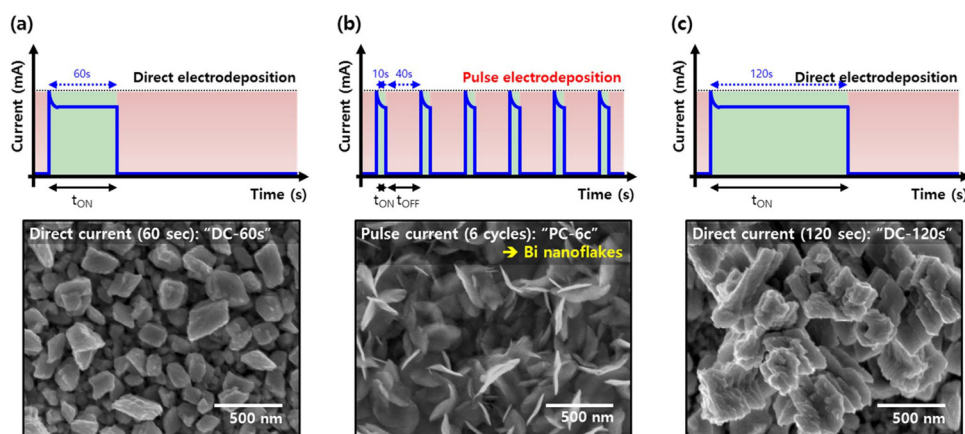


Fig. 5 Current curves and the corresponding SEM images of direct electrodeposition and pulse electrodeposition. Reproduced with permission.<sup>29</sup> Copyright 2017, Elsevier.

electrode surface is more stable during the deposition process, so the phenomenon of concentration polarization becomes weaker. The resulting grains are smaller and the deposition is more uniform and denser. Electrodeposition also has its limitations. First, the controllable parameters of electrodeposition have a wide range of adjustment with many influencing factors, such as the deposition method, potential, current density, pH, additives, and electrolyte. Second, the lack of effective theoretical models to describe the relationship between parameters and properties of different systems limits the large-scale application of electrodeposition. Therefore, building a complete database and corresponding theories should be the direction of future development.

## 4. Influence factors and characterization methods

### 4.1 Influence factors

The morphology and structure of the catalyst determine its catalytic performance, and the experimental parameters determine the morphology and structure of the catalyst. Therefore, the synergistic effect of various experimental parameters in the electrodeposition process is very important. In general, the electrodeposition process depends mainly on several factors, including overpotential,<sup>35</sup> electrolyte concentration,<sup>36</sup> current density,<sup>35</sup> additives,<sup>37,38</sup> etc.

Overpotential has a substantial influence on the morphology of deposition.<sup>39</sup> For example, Branco *et al.* studied the catalytic activity of copper with different morphologies and the effects of cathode potential.<sup>36</sup> They deposited predominantly dendritic deposits in the plateau region of the limiting diffusion current density. As shown in Fig. 6a, the strength of dendritic growth was dependent on the applied potential. In the region within the current density plateau, copper dendrites are strengthened as the deposition potential increases. In the region beyond the current density plateau, due to the further evolution of HER, the length and number of dendrites will gradually decrease when the potential is increased. Interestingly, copper catalysts with honeycomb and foam-like structures can produce C<sub>2</sub> products, suppressing the production of methane. This may provide a direction for electrochemical CO<sub>2</sub> conversion applications.

In addition, the effect of electrolyte concentration on the deposition morphology is studied in Branco's work.<sup>36</sup> They obtained the honeycomb-like structure by changing the concentration of H<sub>2</sub>SO<sub>4</sub> to promote the attachment of hydrogen bubbles. With the increase of CuSO<sub>4</sub> concentration, the reduction of copper ions is stronger than that of the HER, and the pore size and wall thickness are enhanced. This structure is beneficial to the rapid transport of gas and liquid, and the higher specific surface area is beneficial to CDRRs. The results show that the methane current efficiency decreases and the ethylene selectivity is enhanced for the catalyst deposited at higher overpotentials.

In the electrodeposition process, additives are often added into the bath to control the fine transform of the morphology

and surface structure of the catalyst. As shown in Fig. 6b, Gewirth *et al.* used 3,5-diamino-1,2,4-triazole (DAT) as an electrodeposition inhibitor to control the morphology of copper alloys, and obtained catalyst with a high specific surface area and porous structure.<sup>37</sup> Some studies have found that additives can form complexes with metals to participate in the catalytic process while regulating the morphology of the catalysts. Xu *et al.* investigated the electrodeposition of copper phosphate complex by modifying the electrode with phosphate ligands.<sup>41</sup> Phosphate anions form complexes with free Cu(II), which compete with the electrodeposition process, resulting in dendrites replacing aggregates. Moreover, Lin *et al.* used EDTA as an additive for both structural induction and ligand effect, and then creatively generated ligand-modified porous hollow copper through the electrodeposition process.<sup>42</sup> The charge and space interaction between EDTA and OCCO adsorbent is helpful to stabilize the lower activation barrier and facilitate the formation of ethylene.

The choice of substrate also has a great influence on the performance of the catalyst; the most commonly used substrates are carbon paper-based gas diffusion layer<sup>40,55</sup> and metal.<sup>24,52–54</sup> Different substrates can result in different growth orientations of catalysts. As shown in Fig. 3a, the dendrite morphology of Cu is formed on both Ag and Pt substrates, but its properties are quite different. When the substrate was Pt, the HER was severe due to the exposure of the substrate. On the contrary, the exposure of Ag increased the production of CO, and the special acicular structure enhanced the selectivity of the C<sub>2</sub>–C<sub>3</sub> products.

It is undeniable that additives have a non-negligible effect on the morphology and performance of catalysts. However, a reserve system that integrates theoretical guidance may allow us to make better use of them. Recently, Wang *et al.* provided a new path for additive selection and optimization by combining experiment and theory with efficient data analysis through machine guidance (Fig. 6c).<sup>43</sup> They indicate that the Sn salt can be used as an important additive for the production of CO and HCOOH, while aliphatic alcohols can promote the formation of Cu<sub>2</sub>O cubes in the electrodeposition process, which tends to produce C<sub>2+</sub> products.

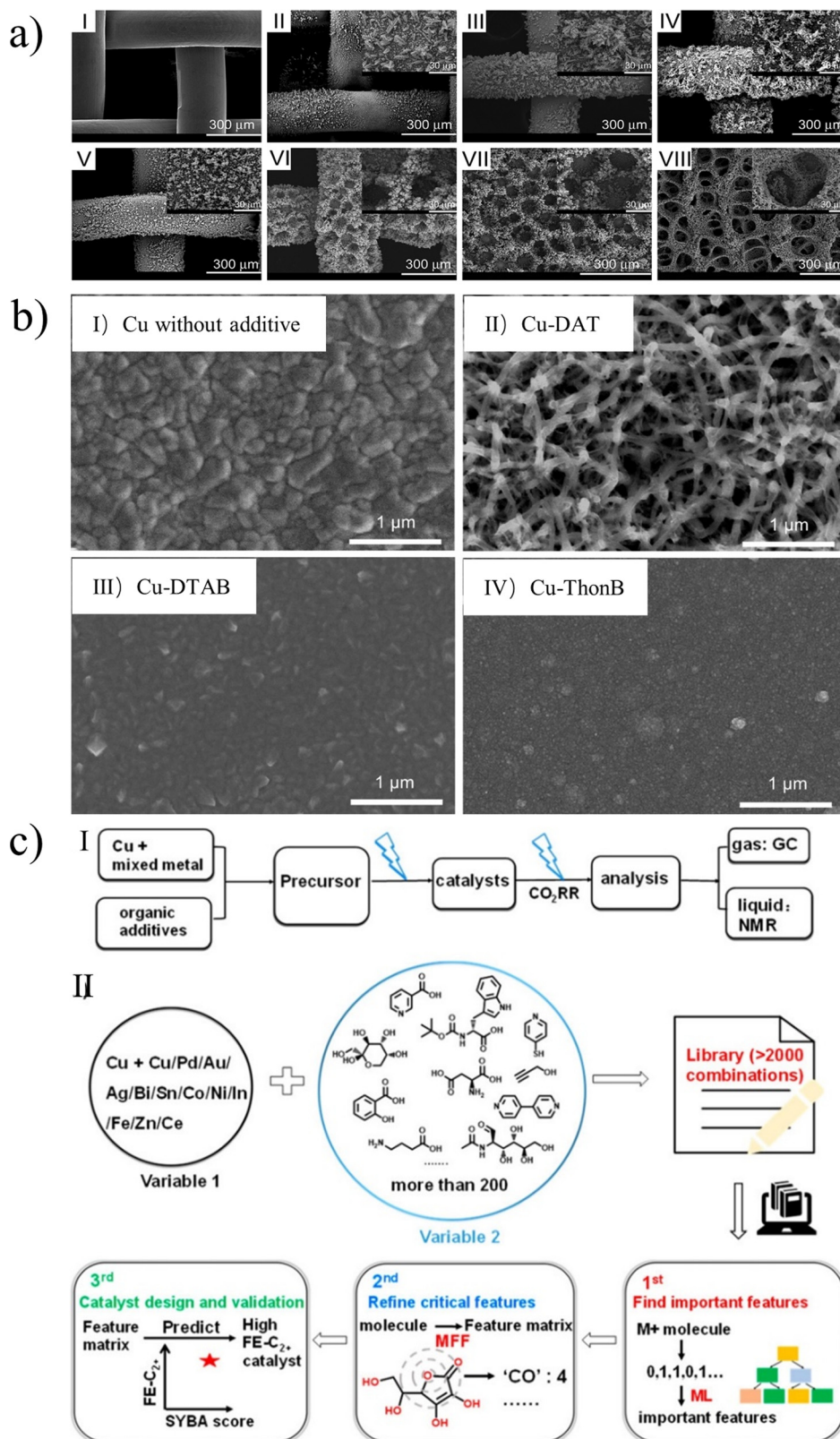
There are many influencing factors of electrodeposition, due to its huge technical parameter space. In addition to the above-mentioned factors, deposition time,<sup>44</sup> pH<sup>45</sup> and other factors also have a non-negligible influence. The huge parameter space means infinite possibilities, but also one of the biggest challenges.

### 4.2 Characterization methods

There are many sophisticated characterization instruments currently available for the detailed characterization of electrocatalysts. Here, we introduce some conventional methods for characterizing electrodeposited catalysts and their functions, so that we can better understand the morphology, internal structure and other properties of catalysts.

SEM can be used to observe the microscopic morphology of substances, and at the same time, it can also be used to analyze





**Fig. 6** (a) SEM images of copper electrodes prepared by electrodeposition at different potentials. Reproduced with permission.<sup>36</sup> Copyright 2013, Elsevier. (b) SEM images of Cu electrodeposited (I) without additive, (II) with DAT, (III) with dodecyltrimethylammonium bromide (DTAB), and (IV) with thonzonium bromide (ThonB). Reproduced with permission.<sup>37</sup> Copyright 2017, American Chemical Society. (c) (I) Preparation of Cu electrocatalysts via electrochemical deposition followed by evaluation of catalytic performance. (II) Schematic illustration of machine-learning-guided optimization of additives for copper catalyst preparation. Reproduced with permission.<sup>43</sup> Copyright 2021, American Chemical Society.



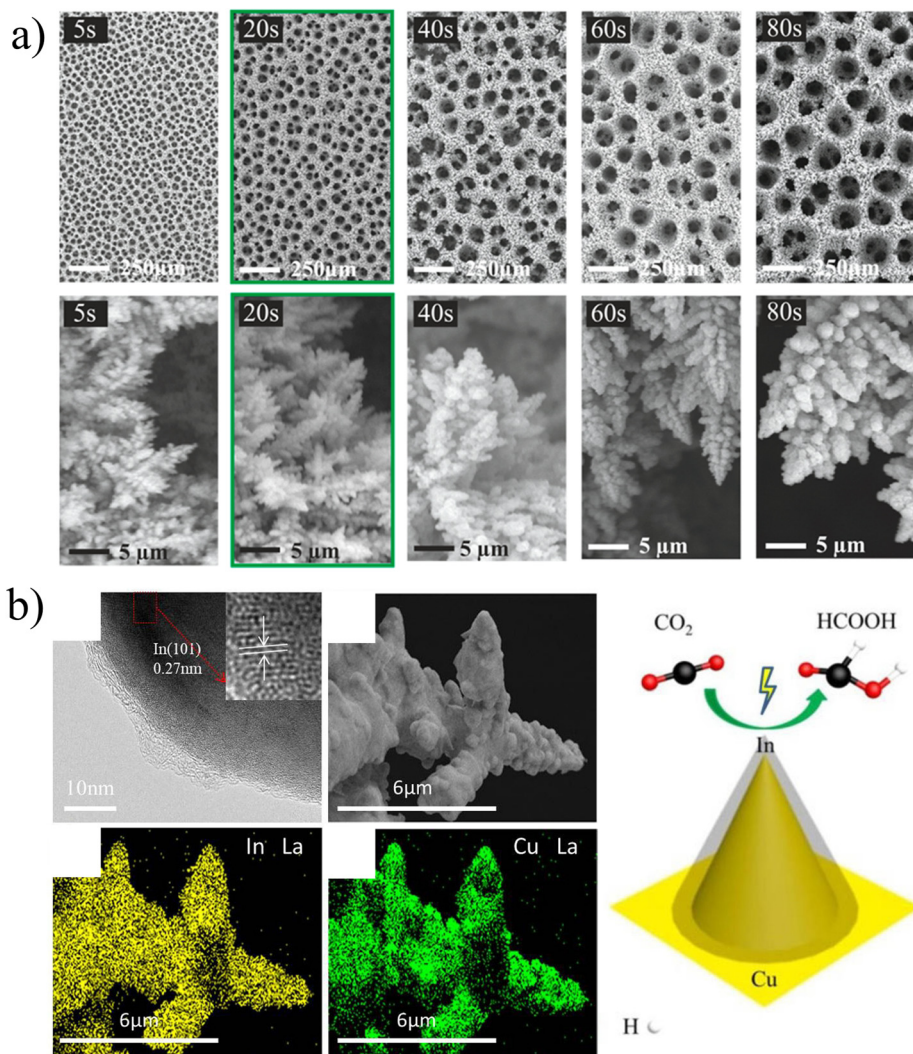


Fig. 7 (a) SEM micrographs showing the changes of surface pore size and dendrite size with deposition time. Reproduced with permission.<sup>46</sup> Copyright 2021, American Chemical Society. (b) HRTEM images of the Cu–In–30 catalyst, SEM image of the Cu–In–30 catalyst, and the corresponding EDX elemental maps. Reproduced with permission.<sup>47</sup> Copyright 2021, American Chemical Society.

the composition of micro-areas of substances. Fig. 7a shows the SEM images of mesoporous copper foam deposited on the Cu substrate at different deposition times.<sup>46</sup> The deposition rate is limited by the mass transport of metal ions and the mobility of adsorbed atoms on the electrode surface.

A HR-TEM (high resolution transmission electron microscope) can be employed to observe the crystal plane, so as to calibrate the crystal plane orientation or the growth direction of the material. Fig. 7b shows the TEM image of the Cu–In catalyst.<sup>47</sup> In the enlarged local region, the characteristic space of the lattice is observed, which is 0.27 nm and fits well with the indium(101) plane. The morphology and element distribution are closely related to the electrodeposition conditions, and the properties of the catalyst have a huge impact on the performance.

X-Ray diffraction (XRD) is one of the most basic structural characterization methods, mainly used for phase analysis. Fig. 8a-I shows the XRD patterns of the electrodeposited CuAg

catalyst in different states, and the transformation of metal and oxide was analyzed, providing direct evidence of the activation of the catalyst under thermal annealing.<sup>59</sup> Fig. 8b shows the XRD result of AgCu-10 and AgCu-50 at different deposition times.<sup>48</sup> The main phases of the catalyst are Cu<sub>2</sub>O and Ag. The peaks with different diffraction angles represent different crystal planes, and the intensity of crystallization peaks increases with the increase of the deposition time.

Since XRD is only sensitive to reveal the bulk phase of the long-range translation order, the complementary X-ray photoelectron spectroscopy (XPS) analysis is more sensitive to the chemical state of the catalyst surface. Fig. 8a-II and III describe the Cu 2p and Ag 3d nuclear level emissions of bimetallic catalyst materials at different stages of preparation and use.<sup>59</sup> XPS spectra of silver foil and copper foil samples are also provided as reference. Apparently, Cu(II) species already existed on the deposited foam. As shown in Fig. 8c, dicopper chloride trihydroxide is used as a precursor for



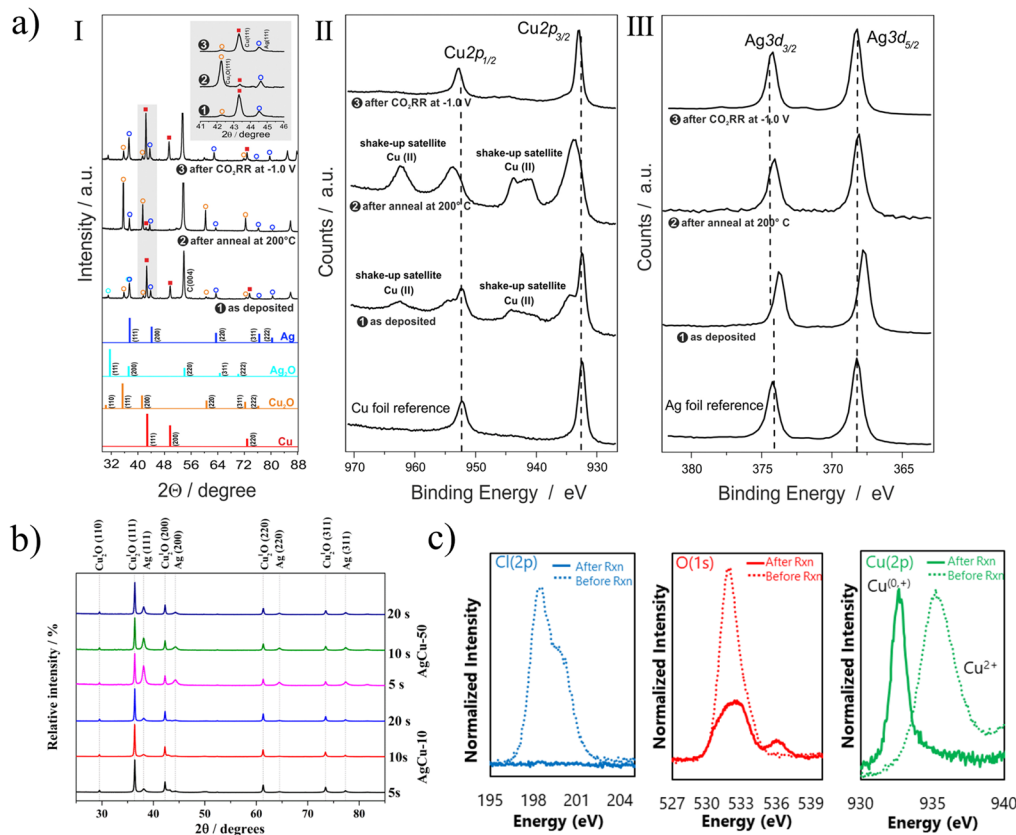


Fig. 8 (a) (I) XRD patterns of the as deposited Ag<sub>15</sub>Cu<sub>85</sub> foam, the annealed foam (12 h at 200 °C), and OD-Ag<sub>15</sub>Cu<sub>85</sub> (after 1 h CO<sub>2</sub>RR at -1.0 V vs. RHE); (II and III) corresponding XPS of the bimetallic foam. Reproduced with permission.<sup>59</sup> Copyright 2020, Elsevier. (b) XRD patterns of AgCu film electrodeposited. Reproduced with permission.<sup>48</sup> Copyright 2019, American Chemical Society. (c) XPS spectra of electro-redeposited (ERD) copper before and after the reaction. Reproduced with permission.<sup>49</sup> Copyright 2018, Macmillan Publishers Limited.

carbon dioxide reduction.<sup>49</sup> It can be seen that there is almost no Residual Cl ion after the reaction, and the strength of oxygen after the reaction is also significantly reduced, indicating that CuO has been reduced. However, it is difficult to distinguish Cu<sub>2</sub>O from Cu on XPS after reaction. Further analysis of X ray absorption spectrum (sXAS) can prove the existence of Cu<sup>+</sup>. The effective combination of various characterization methods can make us better obtain the properties and changes of catalyst, so as to further study its catalytic mechanism. It can better guide researchers to synthesize catalysts.

With the development of CDRRs, traditional characterization techniques are unable to meet the increasing needs. *In situ* testing technology has gradually entered the core area of scientific research. For example, operando hard X-ray absorption spectroscopy (hXAS) can be used to monitor the formation and transformation of catalysts in real time during the test, and even observe the exposure of crystal planes.<sup>50</sup> To monitor the specific process of CDRRs, *in situ* surface-enhanced Raman spectroscopy (SERS) can be used to capture the appearance of important intermediates, such as the peaks of Cu-CO.<sup>75</sup> With the progress and popularization of *in situ* characterization technology, it is believed that this will greatly promote the research of CDRRs.

## 5. Application of electrodeposition in CDRRs

The development of catalytic CO<sub>2</sub> towards the production of high value-added fuels has a positive impact on the world's energy and environment. Electrodeposition has been widely studied and promoted in CDRRs owing to its advantages of cost effectiveness and environmental friendliness. The latest progress in the synthesis of catalytic CO<sub>2</sub> reduction catalysts by electrodeposition is summarized below. Table 1 presents data for some CDRR catalysts prepared by electrodeposition.

### 5.1 Electrodeposited elemental materials

Transition metals are mostly reported as active materials for CDRRs, but low activity and small specific surface area are also problems that need to be solved urgently in this field. Electrodeposition, as one of the most active fields of current material preparation, can yield nanomaterials of various sizes and morphologies. Moreover, the method is not only relatively simple, but also the obtained materials often exhibit high catalytic activity. Cu,<sup>50,51</sup> Ag,<sup>52–54,57</sup> Sn,<sup>55</sup> Zn,<sup>56</sup> Bi,<sup>16</sup> etc. have been effectively used in electrodeposition catalysts. For example, Sargent *et al.* synthesized copper with abundant (100) facets by *in situ* electrodeposition, as shown in Fig. 9a.<sup>50</sup>

Table 1 Summary of electrodeposition-type catalysts for CDRRs in recent years

| Electrocatalyst                   | Preparation method               | Electrolyte              | Potential (vs. RHE) | Product                                                                         | FE (%)  | $J$ (mA cm <sup>-2</sup> ) | Stability | Ref. |
|-----------------------------------|----------------------------------|--------------------------|---------------------|---------------------------------------------------------------------------------|---------|----------------------------|-----------|------|
| Cu (100)-rich copper              | <i>In situ</i> electrodeposition | 1 M KOH                  | −0.38 V to −0.74 V  | C <sub>2+</sub>                                                                 | 90      | 520                        | 65 h      | 50   |
| Porous 3D Cu skeletons            | Electrodeposition                | 0.5 M KHCO <sub>3</sub>  | −1.1 V              | C <sub>2</sub> (C <sub>2</sub> H <sub>4</sub> , C <sub>2</sub> H <sub>6</sub> ) | 29.1    | —                          | —         | 51   |
| Nanoscale Ag grains (40–100 nm)   | Galvanostatic electrodeposition  | 0.5 M KHCO <sub>3</sub>  | —                   | CO                                                                              | Over 90 | 14                         | —         | 52   |
| Ag foam                           | Galvanostatic electrodeposition  | 0.5 M KHCO <sub>3</sub>  | −1.5 V              | CH <sub>4</sub>                                                                 | 51      | —                          | 5 h       | 53   |
|                                   |                                  | 0.5 M KHCO <sub>3</sub>  | −0.8 V              | CO                                                                              | 90      | —                          | 70 h      |      |
| Sn-DT GDE                         | Potentiostatic electrodeposition | 1 M KHCO <sub>3</sub>    | −0.76 V             | HCOOH + CO                                                                      | 91      | 14                         | 72 h      | 55   |
| Zn dendrite                       | Galvanostatic electrodeposition  | 0.5 M KHCO <sub>3</sub>  | −0.9 V              | CO                                                                              | 80      | 4                          | —         | 56   |
| Bi-CMEC                           | Potentiostatic electrodeposition | Ionic liquid             | —                   | CO                                                                              | ≈ 95    | 5.51                       | —         | 16   |
| Cu <sub>2</sub> Zn                | Galvanostatic electrodeposition  | 0.1 M KHCO <sub>3</sub>  | −1.05 V             | C <sub>2</sub> H <sub>6</sub> O                                                 | 29.1    | 8.2                        | 5 h       | 58   |
| Cu@Sn                             | Galvanostatic electrodeposition  | 0.5 M KHCO <sub>3</sub>  | −0.93 V             | HCOOH                                                                           | ≈ 100   | 16.52                      | 15 h      | 60   |
| Cu–Sn                             | Electrodeposition–calcination    | 0.1 M KHCO <sub>3</sub>  | −1.0 V              | HCOOH                                                                           | 82      | 18.9                       | 42 h      | 62   |
| SnCu                              | Potentiostatic electrodeposition | 0.5 M KHCO <sub>3</sub>  | −1.2 V              | HCOOH                                                                           | 78      | 88                         | 250 min   | 63   |
| In <sub>55</sub> Cu <sub>45</sub> | Electrodeposition                | 0.5 M KHCO <sub>3</sub>  | −1.0 V              | HCOOH                                                                           | 96.8    | 8.9                        | 30 h      | 65   |
| Cu–Pd                             | Pulse electrodeposition          | 0.1 M KHCO <sub>3</sub>  | −1.2 V              | CH <sub>4</sub>                                                                 | 32      | —                          | —         | 30   |
| Cu–Pd                             | Galvanostatic electrodeposition  | 0.1 M KCl                | −1.2 V              | C <sub>2</sub> H <sub>4</sub>                                                   | 45.2    | 17.4                       | —         | 67   |
| CuBi                              | Co-electrodeposition             | 0.5 M KHCO <sub>3</sub>  | −1.07 V             | HCOOH                                                                           | 98.3    | 56.6                       | —         | 68   |
| GB–Cu                             | Potentiostatic electrodeposition | —                        | −1.0 V              | C <sub>2</sub>                                                                  | 70      | 52                         | 180 min   | 72   |
| Cu                                | Electrodeposition                | 0.1 M KHCO <sub>3</sub>  | −1.1 V              | C <sub>2</sub> H <sub>4</sub>                                                   | 27.8    | 11.8                       | 12 h      | 73   |
| Cu foam                           | Galvanostatic electrodeposition  | 0.1 M NaHCO <sub>3</sub> | −0.98 V             | C <sub>2</sub> H <sub>4</sub>                                                   | 26      | 60                         | —         | 74   |
| Cu–P1                             | Co-electrodeposition             | 10 M KOH                 | −0.47 V             | C <sub>2</sub> H <sub>4</sub>                                                   | 87      | —                          | —         | 75   |

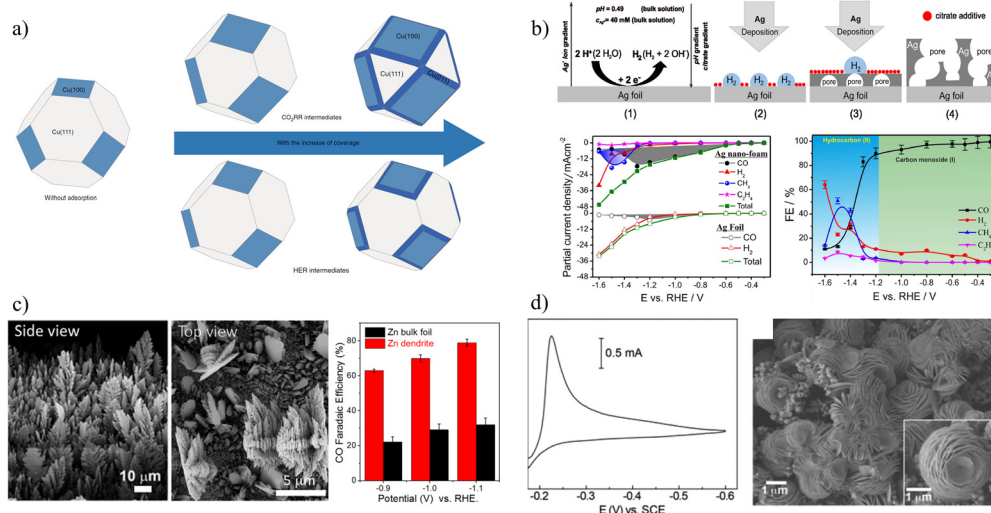


Fig. 9 (a) Schematic diagram of crystal plane distribution when covered by different intermediates. Reproduced with permission.<sup>50</sup> Copyright 2020, Springer Nature. (b) Preparation and catalytic performance of silver nanofoam. Reproduced with permission.<sup>53</sup> Copyright 2018, American Chemical Society. (c) SEM image and performance distribution diagrams of zinc catalysts. Reproduced with permission.<sup>56</sup> Copyright 2015, American Chemical Society. (d) Cyclic voltammogram (CV) in 1.0 M HCl (aq.) and 0.5 M KBr (aq.) containing 20 mM Bi<sup>3+</sup> and SEM image of a Bi-modified glassy carbon electrode (GCE). Reproduced with permission.<sup>16</sup> Copyright 2013, American Chemical Society.

During the electrodeposition of Cu, the ratio of Cu(100) facets was increased by 70%, and C<sub>2+</sub> products with an FE of 90% were achieved at 520 mA m<sup>-2</sup>. The adsorption of CDRR intermediates reduced the surface energy of high-energy copper surfaces, such as Cu(100) facets. This capping effect was similar to colloidal crystal synthesis, regulating the growth of copper and increasing the proportion of (100) planes. Ag has been shown to be effective in converting CO<sub>2</sub> to CO.<sup>54</sup> Broekmann *et al.* obtained a foamed mesoporous silver catalyst by

controlling silver growth with citrate additives.<sup>53</sup> The CO efficiency does not fall below 90% in the range of −0.3 V<sub>RHE</sub> to −1.2 V<sub>RHE</sub> (Fig. 9b). Most interesting is the ability of this foamed Ag catalyst to generate hydrocarbons, reaching 51% and 8.6% for FE<sub>CH<sub>4</sub></sub> and FE<sub>C<sub>2</sub>H<sub>4</sub></sub> at −1.5 V<sub>RHE</sub>, respectively. This is attributed to the significant increase in the binding energy of the novel silver foam to \*CO.

Despite the high activity of noble metals, low-cost metals have gained more attention to implement applications on a

large scale driven by cost-effectiveness. For example, Jiao *et al.* reported a nanostructured Zn dendrite electrocatalyst by the electrodeposition method (Fig. 9c), which not only reduces the formation of surface oxide layer, but also creates a highly active catalyst with dendritic.<sup>56</sup> At an electrodeposition rate of  $1.0 \text{ A cm}^{-2}$ , Zn dendrites with highly branched nanostructures can be formed. Under environmental conditions, dendrite Zn catalyst has significant electrochemical  $\text{CO}_2$  reduction performance, and its activity is about 3 times higher than that of Zn foil, which is attributed to its higher active surface area. Rosenthal and his team electrodeposited cheap Bi material onto glassy carbon electrodes (Fig. 9d).<sup>16</sup> The catalyst can be used with ionic liquids to effectively convert  $\text{CO}_2$  to CO at an overpotential of less than 0.2 V, and the FE is about 95%. The interface between  $\text{Bi}^0$  and  $\text{Bi}^{3+}$  sites may play a role in stabilizing  $\text{CO}_2^{\bullet-}$  intermediates.

Consequently, as a simple and effective method for preparing catalysts, electrodeposition has been successfully applied to the CDRRs of metals and has become one of the preferred methods for the preparation of catalysts by researchers. As the method matures, the combination with other technologies gradually expands its application.<sup>5</sup> It is foreseeable that electrodeposition will gradually develop towards refinement and industrialization.

## 5.2 Electrodeposition of binary alloys

Compared with single metal, bimetallic component catalysts often exhibit synergistic effects, geometric effects or coupling effects, and are expected to greatly reduce the cost, which is one of the important directions in the field of electrocatalysis.

At present, most research studies focus on the combination of Cu with another metal to improve the CDRR performance, such as CuZn,<sup>58</sup> CuAg,<sup>17,59</sup> CuSn,<sup>28,60–63</sup> CuPb,<sup>64</sup> CuIn,<sup>47,65,66</sup> CuPd,<sup>67</sup> CuBi,<sup>68</sup> *etc.* In Fig. 10a, Yeo *et al.* proposed a strategy to compensate for the insufficient CO solubility by introducing  $\text{Cu}_x\text{Zn}$  alloys to catalyze the *in situ* generation of CO during the  $\text{CO}_2$ RR process.<sup>58</sup> CO is weakly adsorbed on the Zn site and

easily diffuses into the Cu matrix, increasing the concentration of  $\text{*CO}$  intermediate, and the intermediate bonds with  $\text{*CH}_2$  to form  $\text{*COCH}_2$  to further generate ethanol. At  $-1.05 \text{ V}_{\text{RHE}}$ ,  $\text{Cu}_4\text{Zn}$  can reach the FE of ethanol (29.1%) and the current density ( $-8.2 \text{ mA m}^{-2}$ ). Moreover, Gewirth fabricated a catalyst with a high specific surface area by electrodepositing CuAg alloy films in an additive bath.<sup>17</sup> The faradaic efficiencies of  $\text{C}_2\text{H}_4$  and  $\text{C}_2\text{H}_5\text{OH}$  are close to 60 and 25% (Fig. 10b), respectively. Ag promotes the formation of  $\text{Cu}_2\text{O}$ , which is beneficial to improve the production efficiency of CO and  $\text{C}_2\text{H}_4$ . Moreover, Strasser *et al.* tuned the selectivity and efficiency of electrochemical  $\text{CO}_2$  reduction by controlling the inhibition of the hydrogen evolution reaction channel.<sup>64</sup> They demonstrate an unusually high selectivity for formate ( $\text{HCOO}^-$ ) over a wide range of overpotentials when a small amount of submonolayer Pb atoms is deposited on the Cu surface. In short, although there have been many studies on binary alloys of Cu with enhanced selectivity, the research on commercialization is relatively lacking and relevant research is urgently needed.

Compared with the binary alloys of copper, combination studies of other metals are rare. One of the reasons is that it lacks the ability to produce hydrocarbons and the main research is on CO<sup>27,70</sup> and  $\text{HCOOH}$ .<sup>69</sup> The extremely high selectivity may give it a huge potential to industrialize earlier. Fontecave *et al.* optimized the Ag content, porosity, thickness and specific surface area by adjusting the electrodeposition parameters to prepare a AgZn dendritic electrode.<sup>27</sup> The selectivity of  $\text{CO}_2$  to CO conversion was higher than 91%, and remained above 90% on an average within 40 h. As shown in Fig. 10c, after increasing the pressure of CO to 9.5 bar, the current density of  $\text{CO}_2$  to CO can reach  $286 \text{ mA cm}^{-2}$ . For cost consideration, Li *et al.* used electrodeposition technology to deposit cheap Bi and Sn on the copper mesh to obtain similar pine needle-shaped dendritic structured BiSn metal electrodes.<sup>69</sup> The  $\text{Bi}_5\text{Sn}_{60}$  electrode has good catalytic activity for  $\text{CO}_2$  reduction at  $-1.0 \text{ V}_{\text{RHE}}$ , the FE of formic acid is as high as 94.8%, the partial current density is  $34 \text{ mA m}^{-2}$ , and the

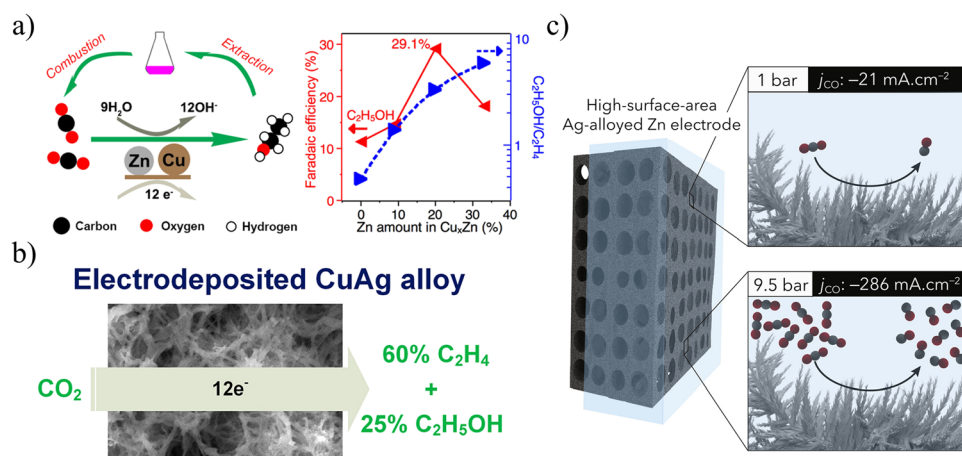


Fig. 10 (a) Schematic diagram of ethanol production from CuZn alloy. Reproduced with permission.<sup>58</sup> Copyright 2016, American Chemical Society. (b) Schematic diagram of the production of C2 products from CuAg alloys. Reproduced with permission.<sup>17</sup> Copyright 2018, American Chemical Society. (c) Schematic diagram of efficient CO production from AgZn alloy. Reproduced with permission.<sup>27</sup> Copyright 2019, Elsevier Inc.

yield is  $636.3 \mu\text{mol cm}^{-2} \text{h}^{-1}$ . At a constant potential of  $-1.0 \text{ V}$ , the alloy was stable for 20 h while maintaining a high FE. The good performance is attributed to the large active surface area and abundant active sites of the catalyst, as well as the fast charge transfer brought by the optimized structure.

The combination of binary alloys has greatly improved the performance and stability of catalysts. However, there have been many research studies on binary alloys, but most of them are attributed to the synergistic effect of alloys. The effect of the distance between different metal active sites in bimetallic component catalysts on the catalytic activity is not yet clear,<sup>71</sup> and deep research at the atomic level may provide further understanding of binary alloys, and also help us obtain better theoretical guidance to prepare alloys.

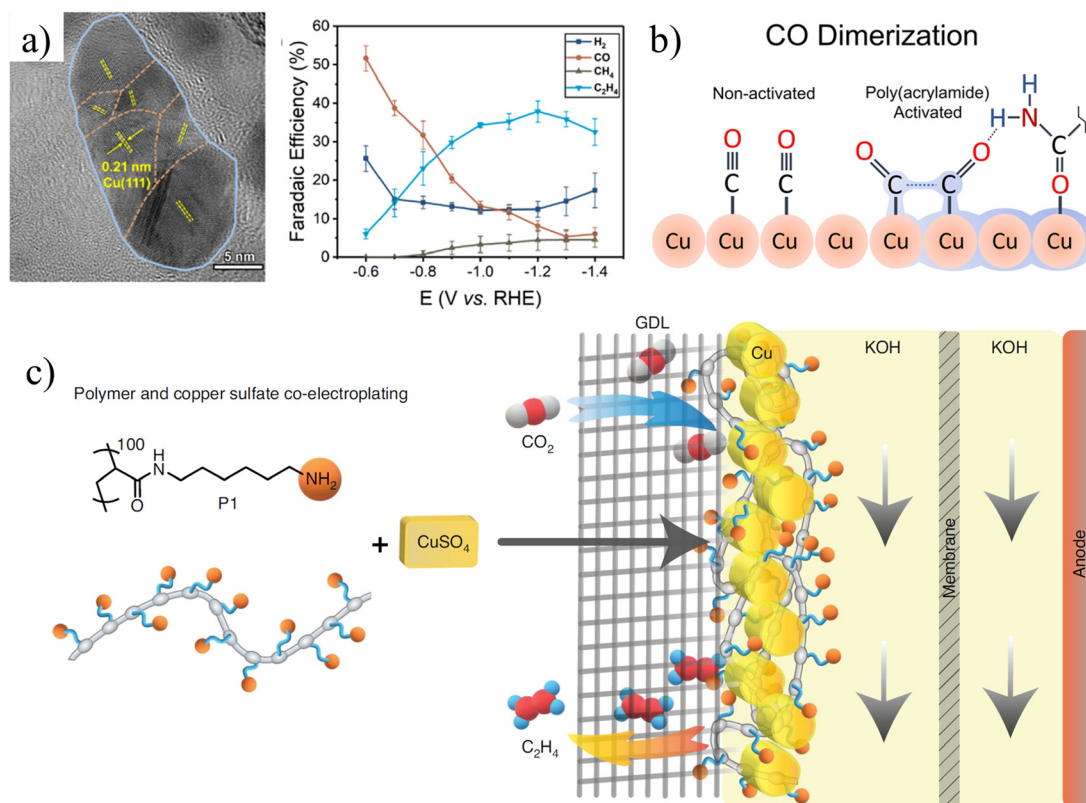
### 5.3 Combination of additives and metals

(1) Additives are mostly used as inhibitors and corrosion inhibitors to control the morphology and improve the performance and selectivity of catalysts. Gong *et al.* introduced a method for controlled grain growth of copper electrodeposition with polyvinylpyrrolidone (PVP) as an additive (Fig. 11a).<sup>72</sup> In terms of kinetics, PVP is an inert polymer that can be reversibly adsorbed on the copper surface to kinetically increase the nucleation rate and decrease the crystal size. Compared with Cu electrocatalysts, grain boundary-rich Cu

exhibits higher selectivity ( $\text{FE} = 70\%$ ) for  $\text{C}_2$  products in the range of  $-1.0$  to  $-1.3 \text{ V}_{\text{RHE}}$ . Cuenya *et al.* prepared prismatic Cu electrocatalysts using crystal-modifying additives.<sup>73</sup> The change of the additive concentration (Janus Green B) can make the prism width more uniform and narrower, the surface rougher, and the defect site concentration higher. The large number of defects on the surface of the catalyst plays an important role in improving the production of  $\text{C}_2\text{H}_4$ .

(2) Some additives can also be adsorbed on metals through bonding during the deposition process, or form complexes with metals to participate in catalysis. For example, Andreoli *et al.* obtained a polyacrylamide-modified Cu electrode by electrodepositing copper in an additive-added bath (Fig. 11b).<sup>74</sup> DFT calculations indicated that polyacrylamide was adsorbed on copper through oxygen on the carbonyl group. The additive also promotes the adsorption of CO molecules, thereby enhancing the generation of  $\text{C}_2\text{H}_4$ . Appropriate additives can promote the progress of the CDRR reaction.

(3) Adding additives that alter the stability of the intermediates on the electrode surface can increase the CDRR activity. Unfortunately, small molecules decorated on the catalyst surface are usually desorbed and removed in the flow cell. Therefore, the co-deposition of polymer and copper on the electrode surface can maintain the required entrainment function. To understand the effect of polymers on the electrocatalytic



**Fig. 11** (a) HRTEM image of grain boundary-rich copper catalyst (GB-Cu) and its catalytic performance. Reproduced with permission.<sup>72</sup> Copyright 2020, American Chemical Society. (b) Schematic diagram of poly-amide modified copper foam electrodes. Reproduced with permission.<sup>74</sup> Copyright 2018, American Chemical Society. (c) Schematic illustration of poly-N-(6-aminohexyl)acrylamide (P1) and Cu co-electroplating on the gas diffusion layer (GDL). Reproduced with permission.<sup>75</sup> Copyright 2021, Springer Nature.



activity, Gewirth *et al.* co-deposited poly-*n*-(6-aminohexyl)acrylamide and copper to make Cu-polymer electrodes (Fig. 11c).<sup>75</sup> In 1 M KOH, the FE of ethylene reaches 72% at  $-0.97 V_{\text{RHE}}$ , and the partial current density of ethylene can reach  $-312 \text{ mA cm}^{-2}$ . Amino groups on the electrode surface can change the reactivity and surface pH to capture  $\text{CO}_2$ , resulting in a higher local concentration of  $\text{CO}_2$  on the surface.

The use of additives affects the electrodeposition process and even the catalyst performance to a great extent, but its limitations are rarely mentioned in the literature. First, the excessive use of catalysts deviates from green electrochemistry. Second, the position of the additive attached to the catalyst is random and easy to fall off, resulting in its general stability. Therefore, a green, easy-to-recycle, and stable additive may provide a reference for the selection of additives.

#### 5.4 Electrodeposition synthesis of high-entropy alloys

One of the earliest papers defined HEAs as “an element consisting of five or more principal elements in equal molar ratios”.<sup>76</sup> The requirement for equal molarity is limited, and the definition is expanded to include “concentrations of each element between 5% and 35%”. The HEA field introduces new ideas and deliberately explores the vast field of hyper-dimensional complex component space. For example, Nellaippan *et al.* used nano-AuAgPtPdCu to convert  $\text{CO}_2$  into hydrocarbons.<sup>77</sup> At a low applied potential ( $-0.3 V_{\text{RHE}}$ ), the FE for gaseous products is approximately 100%. Electrocatalytic activity is mainly attributed to the presence of redox-active copper metal ( $\text{Cu}^{2+}/\text{Cu}^0$ ), while other metals provide only synergistic effects. This is one of the few examples of high-entropy alloys used in CDRRs, although it is not synthesized by electrodeposition.

The concept of entropy was also introduced into binary alloys, Takeguchi *et al.* proposed an entropy-based adsorption theory that alloys with random distributions can weaken the adsorption of  $\ast\text{CO}$ .<sup>78</sup> Therefore, high-entropy state CuSn alloys ( $\text{Cu}_6\text{Sn}_5$ ) may not be suitable for  $\ast\text{CO}$  adsorption, while low-entropy state CuSn alloys may provide enhanced  $\ast\text{CO}$  adsorption capacity and subsequent enhanced  $\text{C}_2$  product selectivity. Based on this, Zheng *et al.* developed a bimetallic low-entropy  $\text{Cu}_3\text{Sn}$  catalyst with high efficiency for  $\text{CO}_2$  reduction to ethanol, with an FE of 64%.<sup>79</sup> At an industrial current density of  $-900 \text{ mA cm}^{-2}$ , the  $\text{Cu}_3\text{Sn}$  catalyst exhibits excellent stability over 48 h.

As a brand-new alloy system, high-entropy alloys have great advantages in material stability, strength, and electrochemical properties. At present, the preparation of high-entropy alloys by electrodeposition for CDRRs is extremely rare. Reasonable design and preparation of ideal high-entropy alloys have broad application prospects in CDRRs.

#### 5.5 Exploration of industrialization

With the gradual maturity of traditional electrodeposition technology, its application is becoming more and more extensive. However, most research studies have focused on developing novel catalysts with excellent performance and good stability.

Perhaps our focus should turn to the path of industrialization, and Fig. 12 expresses some of our prospects for industrialization. Operation in the laboratory with H-cells is far from being scaled up for commercialization. For large-scale conversion of  $\text{CO}_2$ , the main impediment is the solubility of  $\text{CO}_2$  in water ( $\sim 0.03 \text{ mol kg}^{-1}$  at  $\sim 300 \text{ K}$  and 1 atm).<sup>80</sup> Currently, electrolyzers with flow have been used in CDRRs, and flow reaction cells can transport more reagents, thereby reducing the mass transport problems inherent in H cells. Second,  $\text{CO}_2$  can be delivered to the cathode in the gas phase, providing a new way to generate higher current densities. Here we mainly introduce some studies and suggestions that are close to industrialization.

As we know, the market for methane, ethane, methanol, formic acid and ethylene is huge and in short supply (Fig. 13a). The advancement of carbon neutrality is also imperative. However, we lack a system of business models to integrate which products are our identified goals, and second, the huge cost of electrocatalytic  $\text{CO}_2$  reduction has also become a hindrance to commercialization. Electrolyzers with high power, high selectivity and stability are what we must explore. For example, Gewirth *et al.* electrodeposited CuSn-DAT catalyst on a carbon paper-based gas diffusion layer (GDL) with 3,5-diamino-1,2,4-triazole (DAT) as the buffer.<sup>40</sup> The CuSn-DAT electrode exhibits the highest FE for CO ( $\sim 90\%$  at  $-0.4 V_{\text{RHE}}$ ) and  $\text{C}_2\text{H}_4$  ( $\sim 60\%$  at  $-0.8 V_{\text{RHE}}$ ) production and high current density ( $-225 \text{ mA cm}^{-2}$  at  $-0.8 \text{ V}$ ) in a flow cell. As shown in Fig. 13b, the flow cell consists of anode, cathode and electrolyte flow channels. When the reaction takes place,  $\text{CO}_2(\text{g})$  is supplied to the cathode side, where it diffuses to the electrocatalyst to be reduced; OER occurs at the anode, and is released into the air. As shown in Fig. 13c, Sargent *et al.* deposited copper using carbon-based GDL and polymer-based GDL as substrates, respectively.<sup>81</sup> In strongly basic media, the abrupt interface formed on the catalyst enables ethylene incorporation to progress. The bias current density of ethylene at  $-0.67 V_{\text{RHE}}$  reached  $473 \text{ mA cm}^{-2}$ . GDL is a porous material, and catalysts are immobilized on these layered materials to make gas diffusion electrodes (GDEs). The current density is highly important for industrialization (Fig. 13a).<sup>82</sup> Laboratory-scale flow cells provide an opportunity for further efficient CDRRs and are gaining increasing attention. This is a critical step towards carbon neutrality and one of CDRR's paths towards industrialization. It is believed that with the continuous in-depth research on flow cells, industrial-scale CDRRs will be realized in the near future.

In addition to the attempts on electrolyzers, the researchers also considered various factors conducive to industrialization, such as the production of CO under high pressure,<sup>27</sup> the large-area electrodes,<sup>83</sup> the recovery of electrodeposition waste liquid,<sup>84</sup> and the use of low-sink metals to efficiently prepare CO.<sup>85,86</sup> For example, large-area gas diffusion electrodes are of great significance. Kim *et al.* fabricated large-area ( $25.5$  and  $136 \text{ cm}^2$ ) Ag gas diffusion electrodes by electrodeposition. And it was successfully combined with MEA-type  $\text{CO}_2$  electrolyzer.<sup>83</sup> The preparation of large-area electrodes has more stringent technical requirements, and it is necessary to accurately control



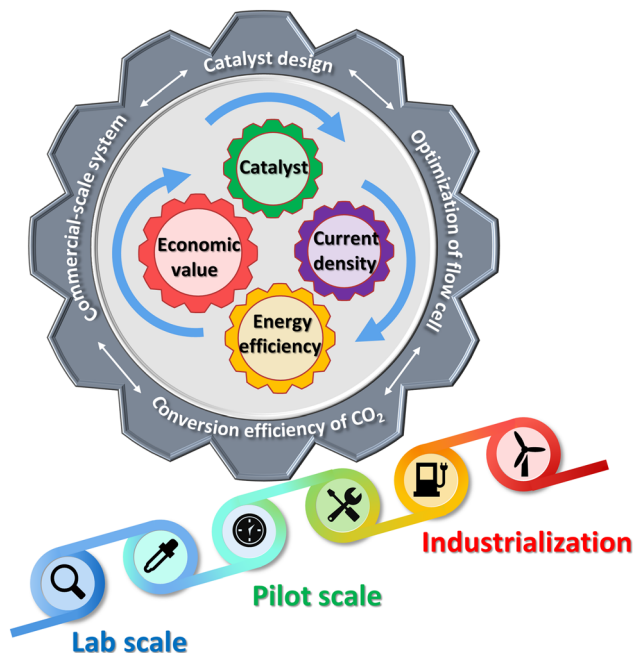


Fig. 12 Schematic diagram of electrodeposition technology for CDRR industrialization.

and compare factors such as electrode system, electrode arrangement, deposition current and deposition time. In this

way, a catalyst with uniform deposition and good morphology can be obtained to ensure that its catalytic activity reaches a high level. The 136 cm<sup>2</sup> Ag GDE fabricated under optimal conditions has an effective geometric area of 107.44 cm<sup>2</sup> in an MEA-type CO<sub>2</sub> electrolyzer, giving potential-dependent CO conversion efficiencies of 41.99–57.75% at  $V_{\text{cell}} = 2.2$ –2.6 V. Although the performance of the catalyst has not reached the high level of laboratory research, and it also faces many technical problems, it is undoubtedly an effective attempt for commercialization. The next development direction should be focused on solving key technical challenges, such as the optimization and update of electrolyzers.<sup>87,88</sup> Excellent technologies from various fields need to be reasonably combined to overcome difficulties in the industrialization of CDRRs.

## 6. Summary and outlook

In this review, we discuss in detail the progress of electrodeposition technology as a promising alternative for preparing highly active and stable CDRR catalysts. We introduce several general electrodeposition methods such as galvanostatic deposition, potentiostatic deposition, and pulsed deposition. The catalysts synthesized by different electrodeposition methods also have different characteristics, morphologies, and the corresponding performance differences.

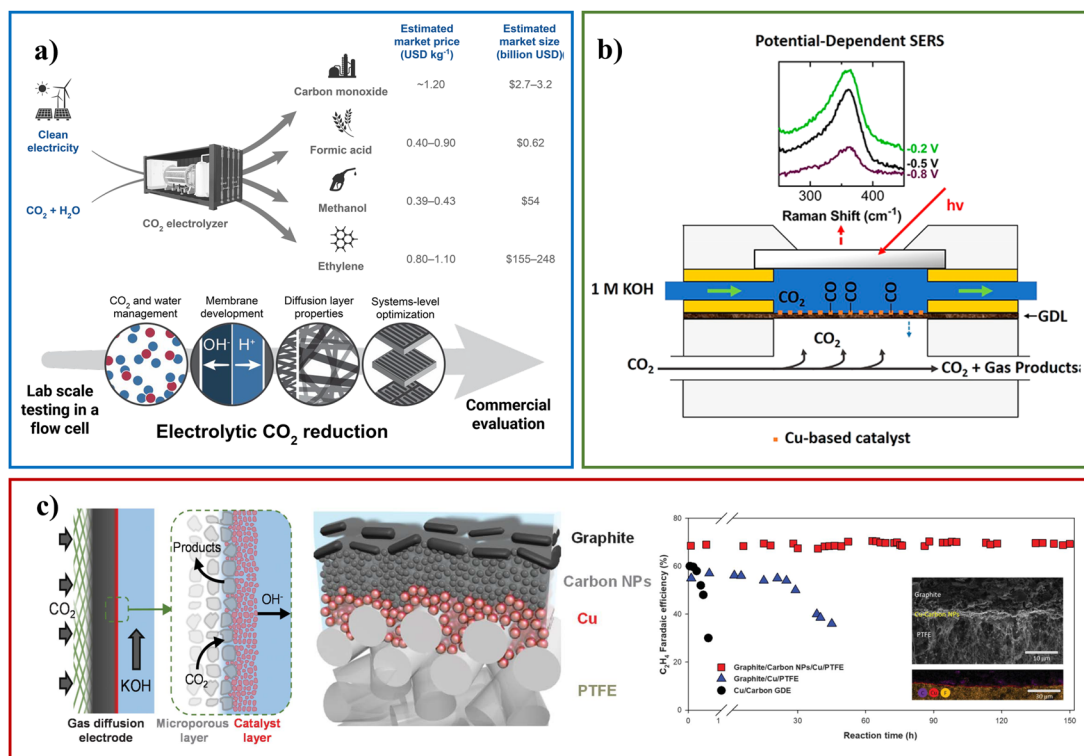


Fig. 13 (a) An overview of the market for CDRR products and the application of flow cell. Reproduced with permission.<sup>82</sup> Copyright 2018, American Chemical Society. (b) Schematic diagram of the flow tank structure. Reproduced with permission.<sup>40</sup> Copyright 2019, American Chemical Society. (c) Schematic diagrams of flow cell cathode and the catalytic performance. Reproduced with permission.<sup>81</sup> Copyright 2018, American Association for the Advancement of Science.



Undoubtedly, the preparation of catalysts by electrodeposition has many advantages. Simultaneously, different experimental parameters can create different catalysts in electrodeposition technology. Experimental parameters such as current density, electrolyte, pH, and additives have their own influence and play a crucial role in obtaining an ideal catalyst, which is also one of the biggest challenges posed by electrodeposition technology.

We also outline the application of electrodeposition in CDRRs. The exploration of additives, units, and binary metals has gradually deepened, while multi-element and even high-entropy still need a long way to be explored. According to the current research progress and some gaps in the field, we give the following suggestions:

(1) Given the low cost and easy scalability of electrodeposition, it is attractive for the preparation of electrochemical CO<sub>2</sub> reduction catalysts. In order to achieve industrialization, it is necessary to overcome the shortcomings of traditional electrodeposition lacking metering control, establish a complete database, accurately adjust electrochemical methods and experimental parameters, and expand the relatively mature technology in the laboratory to large-scale experiments.

(2) Surface modification is an important strategy to modulate the selectivity, and it is also a complex engineering process. Modifications of amines, halogens, and polymers have been reported one after another. By combining theoretical calculation simulations and experiments, the number of effective modified molecules can be expanded faster and more accurately, providing a feasible and effective strategy for improving the C<sub>2+</sub> product efficiency of CDRRs.

(3) The limitations of traditional electrodeposition technology need to be overcome and a new catalyst system should be developed, for example, the preparation of high-entropy alloys mentioned in this article, the preparation of single-atom catalysts, *etc.* Wang *et al.* introduced the synthesis and application of high-entropy alloys in detail.<sup>89</sup> Zeng *et al.* successfully obtained a variety of single-atom HER catalysts using electrodeposition through different metal precursors and supports.<sup>90</sup> Sun *et al.* summarized the applications and preparations of single-atom catalysts in CDRRs, and introduced the relationship between their structures and properties.<sup>91</sup> In addition, 2D nanosheets have abundant low-coordination atoms and a large specific surface area, which is one of the candidates for electrochemical catalysis.<sup>92</sup> It is believed that combining electrodeposition technology with new materials holds promise for CDRRs.

(4) There are many factors that affect the selectivity and efficiency of electrodeposition catalysts, including material composition, crystal structure, microscopic morphology, electronic state, *etc.* Making full use of advanced characterization and measurement techniques (*in situ* optics, X-ray) and theoretical calculations to detect the actual deposition operation and even the process of CDRRs is of great help in further understanding the relationship between materials and reaction mechanisms. In particular, in the face of the complex reaction process, the catalyst itself undergoes a large structural evolution, and we need to reveal the key influencing factors.

Advanced technology will undoubtedly help our research in depth.

(5) In the face of increasingly high industry requirements, the reference and cooperation between different technologies may bring electrodeposition technology to a new level, for example, in terms of technology, plasma treatment of the substrate before deposition to further increase the surface roughness of the substrate or to obtain a substrate with doped properties. The electrodeposited material is further calcined to obtain a more stable material. In terms of theory, in the age of information data, machine learning has become an inevitable path. Combining the guidance of machine learning with the effective screening and preparation of catalysts will be an effective way to develop high-performance catalysts.

(6) In the carbon neutrality, there is no doubt that CDRRs are one of the promising areas to settle energy and environmental problems. With the in-depth study, current density, energy efficiency, CO<sub>2</sub> utilization and even economic benefits<sup>93</sup> have gradually become the focus for scientific researchers. Electrodeposition technology is one of the most cost-effective synthesis methods, so it has become an excellent choice for catalysts. In order to adapt to new demands, electrodeposition technology needs to be integrated with GDEs and applied in the state-of-the-art device systems. Only this way can make it one of the best choices for future industrialization.

## Conflicts of interest

The authors declare no conflict of interest.

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