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# Single-phase $\text{Ni}_5\text{P}_4$ –copper foam superhydrophilic and aerophobic core–shell nanostructures for efficient hydrogen evolution reaction†

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The facile synthesis of a highly durable, low-cost and robust electrocatalyst for hydrogen generation from water is vital to address the existing environmental issues, as well as to provide an environmentally-friendly clean and green energy supply. Electrochemical deposition of single-phase nickel phosphide on galvanostatically deposited copper foam ( $\text{Cu}@\text{Ni}_5\text{P}_4$ ) core–shell nanostructure offers an innovation in the structural design of a new platform for novel electrocatalysts. The  $\text{Cu}@\text{Ni}_5\text{P}_4$  provides a superior three-dimensional conductive channel for ion transport during the catalytic process. The catalyst exhibits an excellent electrocatalytic activity towards the hydrogen evolution reaction (HER) in acidic media. The superhydrophilic and aerophobic properties of the porous electrode help the  $\text{H}_2$  gas bubbles to quickly leave the surface. Interestingly, it requires a very low overpotential of 90 mV for HER at a current density of  $10 \text{ mA cm}^{-2}$ . The very small Tafel slope of  $49 \text{ mV dec}^{-1}$  and the very high exchange current density ( $\sim 0.76 \text{ mA cm}^{-2}$ ) originate from the large electrochemically active surface area and the fast mass and electron transfer efficiency of the  $\text{Cu}@\text{Ni}_5\text{P}_4$  catalyst. A theoretical study was performed to investigate the mechanism underlying the HER activity in Cu-supported  $\text{Ni}_5\text{P}_4$  at an atomic scale. Density functional theory (DFT) calculations suggest a very high negative Gibbs free energy change ( $\Delta G_{\text{H}^+}$ ) in  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) upon hydrogen adsorption, which is actually responsible for the excellent HER activity of the catalyst. Furthermore, it shows remarkable durability for hydrogen generation under low ( $10 \text{ mA cm}^{-2}$ ) and high current densities ( $160 \text{ mA cm}^{-2}$ ) for >84 h with  $\sim 96\%$  retention of the overpotential, establishing a low-cost and efficient catalyst for sustainable, future energy generation strategies.

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## Introduction

The electrochemical generation of  $\text{H}_2$  from water has attracted considerable attention, as it is one of the promising approaches used for the production of renewable fuels aimed at future energy supply. Hydrogen generation is economically favorable and environmentally friendly as it generally gives pure products, which are free from  $\text{CO}$ .<sup>1,2</sup> In addition, not only is  $\text{H}_2$  required as the starting material for fuel cells, several industries also have a demand for it as a precursor material for the production of ammonia and the refining of petroleum. To date, several catalysts for the hydrogen evolution reaction (HER) have been developed, among them, noble metal catalysts such as platinum for HER are recognized as benchmark catalysts owing to their high efficiency and low overpotential towards electrocatalytic reactions.<sup>2,3</sup> However, due to limited resources and the expense

of noble metal catalysts, transition metal (Ni, Co, Fe and Mn)-based catalysts have drawn attention owing to their performance and their abundant sources.

Transition metal sulfides, phosphides and selenides are the most studied catalysts and have drawn enormous attention in recent years.<sup>4</sup> Typically phosphorous-based transition metal pnictide with the earth abundant element nickel, and nickel phosphides have gained considerable attention as HER catalysts owing to their high activity and stability.<sup>5–8</sup> Nickel phosphide exists in several phases in nanostructures such as  $\text{Ni}_3\text{P}$ ,  $\text{Ni}_2\text{P}$ ,  $\text{Ni}_5\text{P}_2$ ,  $\text{Ni}_5\text{P}_4$ ,  $\text{NiP}_2$  and  $\text{Ni}_{12}\text{P}_5$ .<sup>9</sup>  $\text{Ni}_2\text{P}$  was theoretically predicted to be an efficient HER electrocatalyst, even better than Pt,<sup>10</sup> and experimental validation has been carried out by several researchers.<sup>11–15</sup> Recently,  $\text{Ni}_5\text{P}_4$  crystalline nanoparticles have been explored to produce  $\text{H}_2$  in acidic media.<sup>6,16,17</sup> Although most of the mixed phased nickel phosphides are reported to have a good electrocatalytic activity towards HER, they also have some disadvantages such as uncontrolled agglomeration, less hydrophilicity and poor contact resistance which stop them from being used in commercial applications.<sup>18</sup> Single-phase  $\text{Ni}_5\text{P}_4$  has been proven to show better electrode kinetics than

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the multiphase nickel phosphides during catalysis. Pan *et al.* successfully synthesized single phase  $\text{NiP}_2$ ,  $\text{Ni}_{12}\text{P}_5$  and  $\text{Ni}_5\text{P}_4$ , and showed that the single phase  $\text{Ni}_5\text{P}_4$  was the best electrode material in terms of the HER among the other nickel phosphide based catalysts.<sup>5</sup> This is owed to the amount of positive charge on the Ni ( $\text{Ni}^{6+}$ ) in  $\text{Ni}_5\text{P}_4$ , which is greater than the other nickel phosphides, this helps to achieve better catalytic performances. However, the synthesis of single-phase  $\text{Ni}_5\text{P}_4$  is still a challenge to researchers in this field.

Strategic synthetic approaches and stepwise routes have been employed to create rational active sites to achieve the superior catalytic activity of nickel phosphide.<sup>13</sup> Several procedures have recently been explored such as hydrothermal, high temperature reactions and wet chemical routes/hydrothermal in combination with a high temperature reaction and an electrochemical method for the synthesis of nanostructured nickel phosphide catalysts.<sup>4</sup> However, to the best of our knowledge, to date an electrochemical synthesis of a single-phase nickel phosphide has not been reported, for instance crystalline  $\text{Ni}_5\text{P}_4$ , for the HER. Electrochemical synthesis has several advantages over other methods, such as: (i) the electrochemical reaction is usually a one-step process; (ii) it does not involve a high temperature for the phosphorization reaction; (iii) the reaction time is reduced; and (iv) self-supported catalyst loading is possible on the electrode surface. It has been established that a rough electrode surface is known to favor the electrodeposition of the desired material.<sup>19</sup> Furthermore, an electrodeposited core-shell material offers a synergistic effect between the core and shell that results in the high efficiency of the nanostructures.<sup>20,21</sup> Electrodeposited porous architectures have the advantages of creating a hydrophilic as well as a aerophobic surface, which helps to decrease the ohmic resistance of the electrode with electrolyte and the fast removal of gas bubbles from the surface.<sup>22</sup> Herein, taking advantage of these effects, for the

first time, we have explored the single-phase electrochemical synthesis of nickel phosphide ( $\text{Ni}_5\text{P}_4$ ) on a galvanostatically deposited copper foam (Cuf) electrode. The dendritic nanostructure of Cuf offers a rough surface and acts as template for the deposition of  $\text{Ni}_5\text{P}_4$ . The core-shell morphology of  $\text{Cuf}@\text{Ni}_5\text{P}_4$  further shows an excellent catalytic activity towards the HER in acidic medium.

## Experimental

### Preparation of copper foam electrode

The Cuf thin film was grown on Cu foil using the galvanostatic electrodeposition method following our previous report with a few modifications.<sup>23</sup> First, a copper foil ( $0.5 \times 0.5 \text{ cm}^2$ ) was cleaned with dilute nitric acid followed by deionized (DI) water repeatedly and finally with ethanol. The Cu foil was kept in an argon atmosphere when not in use to avoid atmospheric oxidation. The deposition of Cuf was carried out using a two-electrode deposition process, in which the copper foil was used as both the cathode and anode with a fixed distance of 1.5 cm. A constant current density of  $1 \text{ A cm}^{-2}$  was applied between the electrodes placed in an electrochemical cell containing 0.4 M  $\text{CuSO}_4$  in 1.5 M  $\text{H}_2\text{SO}_4$  for a duration of 45 s. The as-deposited Cuf was washed in DI water 3–4 times to remove any acidic residue and kept in an argon atmosphere for further use.

### Electrodeposition of $\text{Ni}_5\text{P}_4$ on copper foam

Electrodeposition of  $\text{Ni}_5\text{P}_4$  on the Cuf was carried out under a constant potential of  $-0.8 \text{ V}$  in a three-electrode system. Typically, electrodeposition was carried out in an aqueous solution of  $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$  (60 mM),  $\text{NaH}_2\text{PO}_2 \cdot \text{H}_2\text{O}$  (50 mM), and  $\text{NaH}_2\text{PO}_4$  (0.5 M) for different periods of time (30, 60, 90 and 120 min). Previously deposited Cuf was used as a working electrode, platinum wire as the counter electrode, and  $\text{Ag}/\text{AgCl}$  (3 M KCl) as the reference electrode for all of the depositions. The as-deposited black layer of nickel phosphide (Fig. S1†) on Cuf thin film was washed thoroughly with Millipore water and stored under a vacuum when not in use.

**Electrodeposition of  $\text{Ni}_5\text{P}_4$  on different substrates.** For comparison of the catalytic activity, the electrodeposition of  $\text{Ni}_5\text{P}_4$  on different substrates such as copper foil ( $\text{Ni}_5\text{P}_4/\text{Cu}$  foil), graphite plate ( $\text{Ni}_5\text{P}_4/\text{GP}$ ) and nickel foam ( $\text{Ni}_5\text{P}_4/\text{Nif}$ ) were carried out in a three-electrode system at a constant potential of  $-0.8 \text{ V}$ . Prior to the electrodeposition, the substrates were cleaned using their required method. All other conditions were kept the same as the previous section for the electrodeposition of  $\text{Ni}_5\text{P}_4$  on different substrates.

### Electrode fabrication with Pt/C

A glassy carbon (GC) (2 mm diameter) electrode was cleaned with alumina powder as mentioned earlier for the preparation of Pt/C. Homogeneous ink was prepared using commercially available Pt/C (20 wt%) and was dispersed in a mixed solution of water and ethanol (1 : 1, v/v) and followed by sonication for



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30 min. The ink was further drop casted onto the GC electrode for Pt/C to obtain a mass loading of  $0.5 \text{ mg cm}^{-2}$ .

### Electrochemical measurements

All of the electrochemical characterization measurements for the HER were conducted at room temperature ( $25^\circ\text{C}$ ) with  $\text{Cuf@Ni}_5\text{P}_4$  ( $0.5 \times 0.5 \text{ cm}^2$ ) as the working electrode,  $\text{Ag/AgCl}$  (3 M KCl) and the graphite rod were used as the reference and counter electrode, respectively. All of the linear sweep voltammetry (LSV) and cyclic voltammetry (CV) experiments were carried out to check the HER activity with 0.5 M  $\text{H}_2\text{SO}_4$  as the electrolyte. All of the potentials used in this study were calibrated to a reversible hydrogen electrode (RHE) based on the formula

$$E_{\text{RHE}} = (E_{\text{Ag/AgCl(3 M KCl)}} + 0.210 + 0.0591 \text{ pH})\text{V}$$

The chronopotentiometric (CP) measurements were conducted to evaluate the durability of the as-prepared electrocatalyst under the same experimental conditions without compensating the  $iR$  drop. Commercial Pt/C catalysts were employed for hydrogen evolution, respectively, as the baseline catalysts for comparison. Electrochemical impedance spectroscopy (EIS) measurements were carried out at a potential of  $-0.2 \text{ V}$  (vs. RHE) in the frequency range of  $10^5$ – $10^{-2} \text{ Hz}$ . The polarization curves for all of the catalysts were  $iR$  corrected (unless mentioned otherwise) to minimize the effect of the ohmic resistance present at the electrode electrolyte interface and the current was normalized with the geometrical surface area. The  $iR$ -correction was performed according to the following equation:

$$E_{\text{corr}} = E_{\text{mea}} - iR_s$$

in which  $E_{\text{corr}}$  is the  $iR$ -corrected potential, the  $E_{\text{mea}}$  is the experimentally measured potential, and  $R_s$  is the equivalent series resistance extracted from the Nyquist plots at the open circuit potential.

### Computational methodology

Density functional theory (DFT) calculations were performed within the Vienna *ab initio* simulation package (VASP).<sup>24</sup> The ion-electron exchange correlation functionals were treated with the projector augmented wave (PAW)<sup>25,26</sup> pseudopotentials by considering the Perdew–Burke–Ernzerhof (PBE)<sup>27</sup> parametrization form of the generalized gradient approximation (GGA) with a kinetic energy cutoff of 500 eV to expand the electronic wave functions in a plane wave basis-set. A  $\Gamma$ -centered  $5 \times 5 \times 1 \text{ k}$ -mesh was used for the Brillouin zone (BZ) sampling with an energy threshold of  $1 \times 10^{-5} \text{ eV}$  for the total energy convergence and a force tolerance of  $0.01 \text{ eV \AA}^{-1}$  for the ionic and electronic relaxation. The periodic replicas of the slab geometry were decoupled by considering a large vacuum spacing of more than  $20 \text{ \AA}$  along the  $z$ -axis. In addition, the van der Waals (vdW) corrections to the dispersive forces were explicitly treated using

the Grimme DFT-D2 method for the surface adsorbed geometries.

## Results and discussion

### Characterization of the electrode materials

The core-shell  $\text{Cuf@Ni}_5\text{P}_4$  thin film electrode (Fig. S1, ESI†) was synthesized by the electrodeposition method in a three-electrode system at a constant potential of  $-0.8 \text{ V}$ , which is schematically shown in Fig. 1 (details are given in the experimental section). The growth of  $\text{Ni}_5\text{P}_4$  at different deposition times (30, 60, 90 and 120 min) was performed with the aim of achieving the best electrocatalytic activity of  $\text{Cuf@Ni}_5\text{P}_4$  and the optimized time was found to be 90 min. All of the characterizations were conducted using  $\text{Cuf@Ni}_5\text{P}_4$  prepared under the optimal conditions (*i.e.* a deposition time of 90 min). The structural analysis was investigated using X-ray powder diffraction (XRD) analysis. Fig. 2a and b displays the XRD pattern of  $\text{Cuf@Ni}_5\text{P}_4$ , in which all of the diffraction peaks are in good agreement with the hexagonal structure of  $\text{Ni}_5\text{P}_4$  (JCPDS PDF 01-089-2588). The diffraction peaks at the  $2\theta$  values of  $28.69^\circ$ ,  $32.57^\circ$ ,  $36.06^\circ$ ,  $41.42^\circ$ ,  $47.06^\circ$ ,  $47.84^\circ$ ,  $52.96^\circ$ ,  $53.98^\circ$ ,  $57.74^\circ$ ,  $61.06^\circ$ ,  $69.66^\circ$ ,  $76.46^\circ$  and  $79.01^\circ$  were attributed to the planes of (103), (004), (104), (211), (300), (301), (214), (220), (304), (107), (320), (226) and (413), respectively for  $\text{Ni}_5\text{P}_4$ . However, the diffraction peaks for bare Cuf at a  $2\theta$  of  $43.19^\circ$ ,  $50.30^\circ$  and  $73.89^\circ$  correspond to the (111), (200) and (220) planes, respectively, for the cubic lattice (JCPDS PDF 01-070-3038), which were also observed as expected in the diffraction pattern of  $\text{Cuf@Ni}_5\text{P}_4$ . However, the peaks of  $\text{Cuf@Ni}_5\text{P}_4$  were observed to be shifted by an angle of approximately  $0.3^\circ$  with respect to the peak for bare Cuf towards a lower angle of  $2\theta$  owing to the uniform interfacial strain induced in the geometry of the core and shell which originated from the strong size mismatch between them.<sup>28,29</sup> This confirms the interfacial interaction of the hybrid core-shell nanostructure formed during electrochemical synthesis.<sup>30</sup> The two small peaks are observed at a  $2\theta$  of  $37.24^\circ$  and  $38.95^\circ$ , which corresponds to the (111) plane of NiO (PDF 00-047-1049) and the (111) plane of CuO (PDF 00-001-1117), respectively. The peak arising for CuO may be due to the exposure of the sample to the air atmosphere and the appearance of a small oxide peak of nickel (NiO) may be due to its formation in the working electrolyte conditions during the electrodeposition process.<sup>31,32</sup> The selected area electron diffraction (SAED) pattern obtained during the transmission electron microscopic (TEM) measurement (Fig. 2c), again reveals the single-phase  $\text{Ni}_5\text{P}_4$  formation on Cuf, which is well correlated with the XRD pattern.

The surface morphological information for the as-deposited Cuf and  $\text{Cuf@Ni}_5\text{P}_4$  was systematically investigated using scanning electron microscopy (SEM) and TEM. The SEM images of Cuf (Fig. 3a and S2, ESI†) show the honeycomb porous structure resulting from the generation and dissipation of  $\text{H}_2$  bubbles during the electrodeposition process.<sup>33</sup> The SEM images of  $\text{Cuf@Ni}_5\text{P}_4$  at different deposition durations demonstrate the growth of  $\text{Ni}_5\text{P}_4$  with time (Fig. S3, ESI†).  $\text{Cuf@Ni}_5\text{P}_4$  shows a similar structure to Cuf with uniformly





Fig. 1 Schematic illustration of the electrochemical synthesis of the copper foam-nickel phosphide active material and the HER activity.



Fig. 2 (a) XRD pattern for Cuf (blue) and Cuf@Ni<sub>5</sub>P<sub>4</sub> (red); (b) scaled image of XRD of Cuf@Ni<sub>5</sub>P<sub>4</sub>; and (c) SAED pattern for Cuf@Ni<sub>5</sub>P<sub>4</sub>.

distributed continuous macropores across the surface (Fig. 3b and S4, ESI†). Unlike Cuf@Ni<sub>5</sub>P<sub>4</sub>, the SEM images of the electrodeposited Ni<sub>5</sub>P<sub>4</sub>/GP, Ni<sub>5</sub>P<sub>4</sub>/Cu foil and the Ni<sub>5</sub>P<sub>4</sub>/Nif samples are particulate in nature (Fig. S5, ESI†). Although they have different morphologies, all of the materials exhibit aggregated particles throughout the surface. The pore size distribution (Fig. S6, ESI†) reveals that the average pore size of the bare Cuf was approximately 110 μm, which was reduced to an average pore size of approximately 85 μm in the Cuf@Ni<sub>5</sub>P<sub>4</sub>, which indicates the deposition of Ni<sub>5</sub>P<sub>4</sub> is *via* the electrodeposition technique. The high-resolution SEM images at different

magnifications, (Fig. 3c and d) further suggests the formation of a dendritic Ni<sub>5</sub>P<sub>4</sub> film onto the copper foam.

The TEM images of the Cuf@Ni<sub>5</sub>P<sub>4</sub> (Fig. 3e and S7a and b, ESI†) show the dendritic structure of the material. A close look at Fig. 3e and f shows the different intensities of the layer, which arise from the transmission dependency of the different atomic layers as schematically represented in Fig. 3g. The thickness of the deposited layer calculated from the high-resolution TEM (HRTEM) image was 30–40 nm (Fig. 3f) with a core diameter of 0.4–0.8 μm which proves the formation of a core shell nanostructure with copper as the core and Ni<sub>5</sub>P<sub>4</sub> as the shell. This hierarchically structured electrode with a core-shell configuration is known to show excellent electrocatalytic activity towards hydrogen generation.<sup>21</sup> The HRTEM study was performed with the Ni<sub>5</sub>P<sub>4</sub> material as the shell (Fig. 3h). Well-resolved lattice fringes were observed with *d*-spacing values of 0.222, 0.248 and 0.217 nm, which correspond to the (210), (104) and (211) planes of Ni<sub>5</sub>P<sub>4</sub>, respectively. The junction of the core-shell heterostructures, as revealed from the HRTEM images shown in Fig. 3i and j, indicate the presence of the (001) plane of Ni<sub>5</sub>P<sub>4</sub>, grown on the copper (111) plane. The energy dispersive X-ray spectra (EDX) suggests the presence of Ni, Cu and P elements in the sample (Fig. S8, ESI†). The EDX mapping study was accomplished over a branched structure of Cuf@Ni<sub>5</sub>P<sub>4</sub> (Fig. 3k–n). The EDX elemental mapping study proves the homogeneous distribution of the nickel, phosphorous and copper elements on the branched structure. It is noteworthy from the mapping analysis that the more intense red (for Ni) and blue (for P) color at the branched structure and the green color (for Cu) throughout the scanned area further confirm that the Ni<sub>5</sub>P<sub>4</sub> thin film fully covered the Cuf nanostructure. The surface area, pore volume and pore size were analysed using the Brunauer–Emmett–Teller (BET) method using N<sub>2</sub> adsorption–desorption



**Fig. 3** (a) SEM image of bare Cuf; (b–d) SEM images of Cuf@Ni<sub>5</sub>P<sub>4</sub> at different magnifications; (e) and (f) TEM images of Cuf@Ni<sub>5</sub>P<sub>4</sub> reflecting the core shell nanostructure of the catalyst; (g) schematic illustration showing the core–shell nanostructure of Cuf@Ni<sub>5</sub>P<sub>4</sub>; (h) high resolution TEM image of Cuf@Ni<sub>5</sub>P<sub>4</sub> (inset shows an enlarged version of the selected area from the HRTEM image); (i) and (j) HRTEM images of the interface of Cuf@Ni<sub>5</sub>P<sub>4</sub> showing the (001) plane of Ni<sub>5</sub>P<sub>4</sub> present at the interface; and (k–n) elemental mapping of Cuf@Ni<sub>5</sub>P<sub>4</sub>.

isotherms (Fig. S9a, ESI†). The specific surface area of our material, Cuf@Ni<sub>5</sub>P<sub>4</sub>, was found to be 6.944 m<sup>2</sup> g<sup>−1</sup>. The isotherms were type IV, which are usually identified for mesoporous materials. The average pore size was found to be 9.29 nm (Fig. S9b, ESI†), which plays a part in the efficient catalytic activity of the catalyst.

X-ray photoelectron spectroscopy (XPS) is an important tool to ascertain the chemical states of the elements present in a sample. As shown in Fig. 4a, the XPS survey scan confirms the presence of Ni, Cu, P, C as well as O elements. The presence of C and O can be attributed to the surface adsorbed electrolyte ion or surface oxidation of the material.<sup>11</sup> The high-resolution XPS spectra of Ni 2P were employed to detect the metallic and oxidized peak corresponding to Ni 2P<sub>3/2</sub> and Ni 2P<sub>1/2</sub> (Fig. 4b). Interestingly, two metallic peaks for Ni (Ni<sup>δ+</sup>) corresponding to 853.4 and 870.3 eV were identified.<sup>34,35</sup> The spectrum of Ni 2P also indicates the presence of peaks at 856.8 (oxidized Ni) and 862.3 eV (satellite) for Ni 2P<sub>3/2</sub> and at 875.6 (oxidized Ni) and 880.2 eV (satellite) for the Ni 2P<sub>1/2</sub> energy level.<sup>5</sup> The high-



**Fig. 4** (a) XPS survey spectra of Cuf@Ni<sub>5</sub>P<sub>4</sub>, and high-resolution deconvoluted XPS spectra for: (b) Ni 2p; (c) P 2p; and (d) Cu 2p.



resolution spectrum of P 2p for the  $\text{Cu@Ni}_5\text{P}_4$ , in which the peak at 129.9 eV was assigned to the  $\text{P } 2p_{3/2}$  and  $\text{P } 2p_{1/2}$ , whereas the peak at 133.4 eV was attributed to the oxidized P species (Fig. 4c). The XPS spectra of copper present as a core in  $\text{Cu@Ni}_5\text{P}_4$  (Fig. 4d), indicates three main peaks at 932.1, 934.5, and 953.7 eV, which are attributed to metallic Cu ( $\text{Cu}^{0+}$ ),  $\text{Cu } 2p_{3/2}$  (oxidized Cu) and  $\text{Cu } 2p_{1/2}$  (oxidized Cu), respectively. The three peaks which appeared at a binding energy of 939.1, 942.4, and 962.4 eV were attributed to the satellite peaks of the  $\text{Cu } 2p_{3/2}$  and  $2p_{1/2}$ , respectively.<sup>36,37</sup>

### Electrochemical characterization

The electrocatalytic activity of the as-prepared catalyst was evaluated by means of the HER in 0.5 M  $\text{H}_2\text{SO}_4$ . There are only a few reports in the literature of a single-phase synthesis of  $\text{Ni}_5\text{P}_4$  used for the generation of  $\text{H}_2$ .<sup>16,18</sup> However, all of the reports either failed to achieve a high exchange current density or did not perform for a long time in acidic medium. In order to assess the electrocatalytic activity of the as-prepared  $\text{Cu@Ni}_5\text{P}_4$ , a systematic electrochemical characterization for HER was performed. All of the potential used here was converted to the RHE unless mentioned otherwise. The polarization curve of the electrodeposited nickel phosphide on Cu at different deposition durations (Fig. S10, ESI†), clearly shows that a 90 min deposition time gives the best HER activity in terms of the overpotential and chemical kinetics. As observed from the SEM images (Fig. S3, ESI†), more coverage of electrodeposited  $\text{Ni}_5\text{P}_4$  films is obtained with a deposition time of up to 90 min. Further deposition (120 min) inhibits the charge transfer between the

Cu and  $\text{Ni}_5\text{P}_4$ , which weakens the catalytic performances of the electrode. Fig. 5a displays the obtained polarization curve for Pt/C,  $\text{Cu@Ni}_5\text{P}_4$ ,  $\text{Ni}_5\text{P}_4/\text{GP}$ ,  $\text{Ni}_5\text{P}_4/\text{Cu}$  foil,  $\text{Ni}_5\text{P}_4/\text{Nif}$  and bare Cu at a scan rate of  $10 \text{ mV s}^{-1}$ . The  $\text{Cu@Ni}_5\text{P}_4$  catalyst attained an overpotential ( $\eta$ ) of 90 mV at a current density of  $10 \text{ mA cm}^{-2}$ , which is 239 mV more positive than bare Cu, 148 mV more positive than  $\text{Ni}_5\text{P}_4/\text{GP}$ , 113 mV more positive than  $\text{Ni}_5\text{P}_4/\text{Cu}$  foil, 36 mV more positive than  $\text{Ni}_5\text{P}_4/\text{Nif}$  and 63 mV more negative in comparison to Pt/C. Interestingly, the  $\text{Cu@Ni}_5\text{P}_4$  catalyst displays a  $\eta$  of only 164 mV even at a very high current density of  $100 \text{ mA cm}^{-2}$ . It is noteworthy to mention here that the achieved overpotential of  $\text{Cu@Ni}_5\text{P}_4$  is very low compared to the previously reported data on nickel phosphide based electrocatalysts (Fig. 5b and Table S1, ESI†).<sup>1,18,38</sup> The excellent electrocatalytic activity of  $\text{Cu@Ni}_5\text{P}_4$  reveals the important role of the core shell nanostructures of the catalyst and confirms that the surface nickel phosphide (shell) exploited the copper (core) in terms of the porosity and surface area, resulting in a superior catalytic performance of these a core/shell nanostructures. The HER electrocatalytic activity crucially depends on the uneven electrode surface.<sup>39</sup>

The corresponding Tafel plots were employed to determine the kinetics of the HER rate for the different catalysts (Fig. 5c). The Tafel slope for  $\text{Cu@Ni}_5\text{P}_4$  derived from the Tafel plot was found to be  $49 \text{ mV dec}^{-1}$ , which is less than that of the  $\text{Ni}_5\text{P}_4/\text{Cu}$  foil (slope =  $93 \text{ mV dec}^{-1}$ ),  $\text{Ni}_5\text{P}_4/\text{GP}$  ( $110 \text{ mV dec}^{-1}$ ),  $\text{Ni}_5\text{P}_4/\text{Nif}$  ( $87 \text{ mV dec}^{-1}$ ) and bare Cu ( $150 \text{ mV dec}^{-1}$ ), which determines the better kinetic rate of  $\text{Cu@Ni}_5\text{P}_4$  for hydrogen generation. However, the Tafel slope of Pt/C was found to be  $27 \text{ mV dec}^{-1}$ .



Fig. 5 (a) HER polarization curves for bare Cu,  $\text{Ni}_5\text{P}_4/\text{Cu}$  foil,  $\text{Ni}_5\text{P}_4/\text{GP}$ ,  $\text{Ni}_5\text{P}_4/\text{Nif}$ ,  $\text{Cu@Ni}_5\text{P}_4$  and Pt/C catalysts recorded at a scan rate of  $10 \text{ mV s}^{-1}$ . (b) Bar diagram depicting the comparison of the overpotential and the exchange current density of the previously reported nickel phosphide based electrocatalyst. (c) Tafel plots of bare Cu,  $\text{Ni}_5\text{P}_4/\text{Cu}$  foil,  $\text{Ni}_5\text{P}_4/\text{GP}$ ,  $\text{Ni}_5\text{P}_4/\text{Nif}$ ,  $\text{Cu@Ni}_5\text{P}_4$  and Pt/C. (d) CV response of bare Cu and  $\text{Cu@Ni}_5\text{P}_4$  at a scan rate of  $100 \text{ mV s}^{-1}$ . (e) Nyquist plot of bare Cu and  $\text{Cu@Ni}_5\text{P}_4$  recorded at  $-0.2 \text{ V}$  (vs. RHE), the inset shows the equivalent circuit used to fit the EIS data. All of the experiments were performed in 0.5 M  $\text{H}_2\text{SO}_4$  solution.

An electrode with a larger exchange current density needs less driving force (smaller current density) to conduct the HER.<sup>40</sup> The exchange current density of Cuf@Ni<sub>5</sub>P<sub>4</sub> was calculated to be 0.76 mA cm<sup>-2</sup> by extrapolating the linear part of the Tafel plot to the X-axis and it was found to be very close to that of the exchange current density of Pt/C (1.00 mA cm<sup>-2</sup>) in 0.5 M H<sub>2</sub>SO<sub>4</sub> (Fig. S11, ESI†). The exchange current density achieved by Cuf@Ni<sub>5</sub>P<sub>4</sub> was the highest in comparison with the recently reported nickel phosphide based electrocatalysts<sup>38,41–43</sup> (Table S2, ESI†). The exchange current density is usually expressed in terms of the projected or geometric surface area and depends on the surface roughness or roughness factor (RF) of the catalyst.<sup>37</sup> The porous nature of the nanostructure offers a high electrochemically active surface area (ECSA) and leads to more electrochemically active sites that undoubtedly help to improve the electrocatalytic activity.<sup>44</sup> A comparative CV scan was performed to calculate the ECSA and RF of Cuf@Ni<sub>5</sub>P<sub>4</sub> (Fig. 5d). The CV response obtained from Cuf@Ni<sub>5</sub>P<sub>4</sub> at different scan rates in a non-faradic region (0 to 0.1 V) and the corresponding scan rate *versus* the anodic and cathodic peak current for the calculation of the value of the double layer capacitance (*C*<sub>dl</sub>) are shown Fig. S12 (ESI†). The ECSA was calculated and found to be 423.5 cm<sup>2</sup> by considering the *C*<sub>dl</sub> of 33.9 mF cm<sup>-2</sup> and the specific capacitance (*C*<sub>sp</sub> = 0.02 mF cm<sup>-2</sup>) of the Ni surface in the 0.5 M H<sub>2</sub>SO<sub>4</sub> electrolyte.<sup>45</sup> The RF was calculated to be 1694 (see ESI† for details), which is very high and outperforms the state-of-the-art catalysts reported to date.<sup>46–50</sup>

To study the electrode kinetics (charge transfer behavior), EIS of the bare Cuf and Cuf@Ni<sub>5</sub>P<sub>4</sub> (Fig. 5e) were recorded at -0.2 V (vs. RHE). An equivalent circuit model was employed to fit the Nyquist plot as shown in the inset of Fig. 5e. Interestingly, Cuf@Ni<sub>5</sub>P<sub>4</sub> possesses a very small solution resistance (*R*<sub>s</sub> = 2.59 Ω) which indicates a reduced interfacial resistance and the superior catalytic activity of the as-prepared catalyst. The charge transfer resistance (*R*<sub>ct</sub>) of Cuf@Ni<sub>5</sub>P<sub>4</sub> was only 3.62 Ω (giving rise to the rapid charge transfer kinetics), which is much lower than that of bare Cuf (*R*<sub>ct</sub> = 20 Ω). The EIS of the nickel phosphide deposited on Cuf for different periods of time (Fig. S13, ESI†), clearly indicates that the minimum *R*<sub>ct</sub> of Cuf@Ni<sub>5</sub>P<sub>4</sub> with a 90 min deposition time was obtained as compared to the other catalyst. The low *R*<sub>s</sub> and *R*<sub>ct</sub> value of Cuf@Ni<sub>5</sub>P<sub>4</sub> ensures the fast charge transfer kinetics between the catalyst and the electrolyte, as well as the catalyst to the electrode, which facilitates the faster reaction rate. It is generally accepted that small values of *R*<sub>s</sub> correspond to close contact between the current collector and catalysts.

During the catalytic process, plenty of bubbles are generated from the surface of the electrode which blocks electrolyte diffusion and increases the ohmic resistance between the electrode and the electrolyte interfaces, which decreases the ECSA and eventually leads to degradation of the catalytic performance. To overcome this challenge, it is necessary to design a fine surface catalyst which is hydrophilic as well as aerophobic in nature.<sup>51</sup> To understand the hydrophilicity of the as-synthesized catalyst, wettability analysis on the surface of the Cuf@Ni<sub>5</sub>P<sub>4</sub> electrode was performed by measuring the contact angle of the water drop on the surface of the catalyst. Fig. 6a



Fig. 6 Wettability test of the Cuf@Ni<sub>5</sub>P<sub>4</sub> surface: (a) before; and (b) after placing a liquid drop with a contact angle of 0°. (c–e) Optical images with a schematic diagram in the bottom panel showing the bubble formation behavior on the Cuf@Ni<sub>5</sub>P<sub>4</sub> surface at different overpotentials and at the end of LSV.

shows that the droplet imposes no contact with the surface of Cuf@Ni<sub>5</sub>P<sub>4</sub> and when the drop falls on the surface, the Cuf@Ni<sub>5</sub>P<sub>4</sub> catalyst absorbed the liquid drop instantly (Fig. 6b) with a contact angle of 0°, indicating that the material is superhydrophilic in nature. An aerophobic study of the catalyst was also performed by analysing the bubble formation during and after the LSV run, demonstrated in Fig. 6c–e. The aerophobic nature of the foam-like Cuf@Ni<sub>5</sub>P<sub>4</sub> core-shell nanostructure provides an abrupt renewal of the gas bubbles (as schematically shown in the bottom panel of Fig. 6),<sup>52</sup> which helps to increase the efficiency of the catalyst towards hydrogen evolution. When the HER process has just started the average size of the bubbles formed on the surface were approximately 200 μm at an overpotential of approximately 60 mV and the size starts to increase and is observed to be approximately 300 μm at an overpotential of approximately 130 mV, which is due to the rapid renewal of the minor gas bubbles. Interestingly, when the LSV was stopped it was observed that only a few bubbles, which were trapped in the pores, were seen resembling the superior aerophobic behavior of the catalyst. The superhydrophilic and aerophobic nature of the sample originated from the fine nanostructures and selection of an appropriate material is crucial for HER electrocatalysis.

To ascertain the origin of the high electrocatalytic activity in the as-synthesized materials and to deepen the understanding of the HER mechanism, DFT calculations were performed. As established, the electrochemical reduction of ionic hydrogen on a metal-catalyst surface is a combination of a hydrogen adsorption process called the Volmer reaction step followed by either the Tafel or Heyrovsky reaction mechanism for H<sub>2</sub> desorption (see ESI† for details). The H\* (in which \* refers to atomic hydrogen over the surface of the catalyst) is the rate determining step for proton adsorption in an acidic medium. To estimate the hydrogen adsorption energy (*E*<sub>Ads.</sub>) and the

$\Delta G_{H^*}$  of the reaction intermediate,  $H^*$ , different metal-catalyst surfaces were explored using the computational hydrogen electrode model proposed by Nørskov *et al.*<sup>53</sup> as follows:

$$\Delta G_{H^*} = E_{\text{Ads.}} + \Delta E_{\text{ZPE}} - T\Delta S$$

$$E_{\text{Ads.}} = E_{\text{surface+H}} - E_{\text{surface}} - 1/2E_{H_2}$$

in which  $E_{\text{Ads.}}$  is the hydrogen adsorption energy on the surface of the metal catalyst,  $E_{\text{surface+H}}$  and  $E_{\text{surface}}$  are the total ground state energy of H adsorbed surface and the pure metal catalyst surface, whereas  $E_{H_2}$  is the energy of the  $H_2$  molecule in the vacuum gas-phase state.  $\Delta E_{\text{ZPE}}$  and  $\Delta S$  are the zero-point energy and entropy difference between the adsorbed state ( $H^*$ ) and

molecular gas-phase state of hydrogen ( $H_2$ ), and  $T$  is the absolute temperature ( $T = 298.15$  K in our calculation). The zero-point energy ( $E_{\text{ZPE}}$ ) of the H exposed surfaces was evaluated from the harmonic vibrational frequencies at 0 K. The entropy of the H adsorbed surfaces was found to be very small in our calculation (Table S3, ESI†) and hence, can be safely ignored by assuming the entropy of the  $H_2$  molecule is  $\Delta S = -1/2\Delta S(H_2) = -64.915$  J mol<sup>-1</sup> K<sup>-1</sup> in the standard gas phase state at a pressure of 1 bar, temperature 300 K and pH = 0.

In order to explore the HER activity of the pure  $Ni_5P_4$  (0001) and  $Ni_5P_4$  (0001)/Cu (111) hybrid catalyst surface, several hydrogen adsorption sites around the surface Ni and P atoms in the optimized geometry of the  $Ni_5P_4$  (0001) surface (Fig. S14, ESI†) have been considered to rule out the most probable ones.



Fig. 7 (a and b) A top and side view of  $H^*$  adsorption over the three-fold Ni site of the  $Ni_5P_4$  (0001)/Cu (111) (site I). (c and d)  $H^*$  over the on-top P site of the  $Ni_5P_4$  (0001)/Cu (111) surface (site II). The differential ground state charge density distribution around the adsorbate ( $H^*$ ) is at an isolevel of  $0.59 \times 10^{-2}$  e Å<sup>-3</sup>. (e) The  $\Delta G_{H^*}$  of the reaction intermediate ( $H^*$ ) on different metal-catalyst surfaces (f) Charge density difference and charge transfer at the interface between Cu (111) and  $Ni_5P_4$  (001) surface.



As demonstrated in Fig. 3i and j, the (001) plane of  $\text{Ni}_5\text{P}_4$  is present at the  $\text{Cuf@Ni}_5\text{P}_4$  interface. Fig. S15 in ESI† describes how the three-fold Ni hollow site (site I) and the on-top P site (site II) turn out to be the two most favorable hydrogen adsorption sites with binding energies of  $-0.54$  eV and  $0.21$  eV, respectively. These adsorption sites have been used for further studies on the  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) hybrid interface structure with the Cu (111) surface underneath the  $\text{Ni}_5\text{P}_4$  (0001) surface. Fig. 7a and b shows the adsorption geometry of  $\text{H}^*$  on the three-fold Ni site (site I) of  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) with a binding energy of  $-0.79$  eV, which is the highest among all of the surfaces explored in this study, indicating the importance of Cuf support in facilitating the HER activity in the  $\text{Ni}_5\text{P}_4$  nanostructures. Similar to the hydrogen adsorption over the on-top P site (site II) of  $\text{Ni}_5\text{P}_4$  (0001), the interface structure of  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) also exhibits a positive H binding energy of  $0.16$  eV with a strong delocalization of the valence charge density around the P atom, as shown in Fig. 7c and d. Details of the  $\text{H}^*$  adsorption on various metal-catalyst surfaces and computational details have been provided in the ESI (Fig. S15, S16, and Table S3, ESI†).

The change in the Gibbs free energy ( $\Delta G_{\text{H}^*}$ ) of the reaction intermediate, for example  $\text{H}^*$ , is a well-known descriptor of the HER activity of any adsorbate ( $1/2\text{H}_2$  in this case) over a metal-catalyst surface. According to the Sabatier principle, a good catalyst should have a  $\Delta G_{\text{H}^*}$  value as close as possible to  $0$  eV. The  $\Delta G_{\text{H}^*}$  of the reaction intermediate  $\text{H}^*$  on different metal-catalyst surfaces was measured. The  $\text{Ni}_5\text{P}_4$  (0001) and  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) surface with  $\text{H}^*$  adsorbed over the three-fold Ni site (site I) exhibited a negative value of  $\Delta G_{\text{H}^*}$ , favoring the HER activity (Fig. 7e). In addition, the negative value of  $\Delta G_{\text{H}^*}$  was found to be much higher ( $-0.52$  eV) for the  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) surface as compared to the value of  $-0.18$  eV for the  $\text{Ni}_5\text{P}_4$  (0001) surface. This is attributable to a very high negative adsorption energy,  $E_{\text{Ads.}} = -0.79$  eV of  $\text{H}^*$  over the  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) surface and a localized charge density distribution around the three-fold Ni site of the adsorbate, which strongly binds the atomic hydrogen to its surface (Fig. 7a and b). While for  $\text{H}^*$  at the on-top P site of  $\text{Ni}_5\text{P}_4$  (0001) and the  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) surface, a very high positive value of  $\Delta G_{\text{H}^*}$  indicates a much weaker binding of  $\text{H}^*$  or a reduction in the desorption of hydrogen, resulting in a much lower HER activity. The adsorption geometry of  $\text{H}^*$  on the three-fold Ni site (site I) of  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) with a binding energy of  $-0.79$  eV, which is the highest among all of the surfaces explored in this study, indicates the importance of Cuf for the deposition of  $\text{Ni}_5\text{P}_4$  nanostructures towards HER activity. The high value of the H-binding energy results from the charge transfer between Cu (111) and  $\text{Ni}_5\text{P}_4$  (0001), as the interface is chemical in nature. The interfacial study of the  $\text{Cuf@Ni}_5\text{P}_4$  was validated by the interfacial charge density distribution. The interface between Cu and  $\text{Ni}_5\text{P}_4$  was found to be chemical in nature as shown in Fig. 7f. The charges accumulating at the  $\text{Cuf@Ni}_5\text{P}_4$  interface are transferred from the portion of the Cu (111) surface, which in turn, becomes depleted. The difference in the charge density distribution was calculated *via*  $\Delta\rho = \rho[\text{interface system}] - \rho[\text{Cu (111)}] - \rho[\text{Ni}_5\text{P}_4 (001)]$ . This calculation is based on the explicit inclusion of the vDW-D3 dispersive interactive forces, which

accounts for the long range electronic interactions in the surface geometries.

The electrochemical stability or durability of the catalyst in the working electrolyte is an important parameter that one should look for in a catalyst. The chronopotentiometry test was performed to check the durability of the  $\text{Cuf@Ni}_5\text{P}_4$  catalyst at a low ( $10 \text{ mA cm}^{-2}$ ) as well as high current density ( $160 \text{ mA cm}^{-2}$ ) in  $0.5 \text{ M H}_2\text{SO}_4$  for  $84 \text{ h}$ . As demonstrated in Fig. 8a, the electrocatalyst showed an excellent stability performance with approximately 96% retention of the overpotential even at a high current density of  $160 \text{ mA cm}^{-2}$ . The LSV pattern of the  $\text{Cuf@Ni}_5\text{P}_4$  catalyst was recorded before and after the chronoamperometry study and found a minute change in the overpotential as shown in Fig. 8b, which indicates the excellent durability of the catalyst. In order to check the structural integrity of the catalyst during the stability test, SEM (Fig. 8a, inset) as well as elemental mapping analysis (Fig. S17, ESI†) were performed before and after the chronoamperometry test. The SEM study confirmed the morphology of the catalyst is not altered upon continuous evolution ( $84 \text{ h}$ ) of hydrogen gas. Elemental mapping further revealed the presence of Ni, Cu and P even after  $84 \text{ h}$  of the chronoamperometry test, which proved the structural integrity and superior durability of the  $\text{Cuf@Ni}_5\text{P}_4$  catalyst. The ultrathin deposited layer ( $30 \text{ nm}$ ) of the catalyst on the Cuf could increase the contact area between them and thus decrease the average stress suffered by the hosts upon  $\text{H}_2$  generation ensuring excellent structural integrity



Fig. 8 (a) Chronopotentiometric curve of  $\text{Cuf@Ni}_5\text{P}_4$  at a current density of  $10$  and  $160 \text{ mA cm}^{-2}$ , inset shows the SEM images obtained before and after the test. (b) LSV of  $\text{Cuf@Ni}_5\text{P}_4$  before and after the chronopotentiometric test.

during continuous gas evolution by the as-prepared catalyst. The excellent durability, along with the outstanding catalytic activity of the catalyst, opens up a new method for the electrochemical generation of hydrogen.

## Conclusions

In summary, we present here a simple electrochemical approach to design a single-phase  $\text{Ni}_5\text{P}_4$  catalyst deposited on a galvanostatically-grown Cu nanoarchitecture. The core-shell  $\text{Cu}@\text{Ni}_5\text{P}_4$  catalyst showed a high catalytic activity towards HER in acidic medium with a significantly reduced overpotential and a superior exchange current density. The high ECSA and excessive RF that originates from the foam-like surface of Cu is essentially responsible for the high electrocatalytic activity of the catalyst. DFT calculations elucidated the origin of a very high negative  $\Delta G_{\text{H}^*}$  in  $\text{Ni}_5\text{P}_4$  (0001)/Cu (111) upon hydrogen adsorption. This arises owing to a localized charge density distribution around the three-fold Ni site of the adsorbate, which is favorable for the HER activity of the catalyst. The superhydrophilic and aerophobic nanostructured surface actually helps by reducing the contact resistance and the fast release of air bubbles during the catalysis process. Moreover, the  $\text{Cu}@\text{Ni}_5\text{P}_4$  catalyst shows a long-term durability of 84 h measured using a chronopotentiometry test at a low and high current density with approximately 96% retention of the initial overpotential and preserving the structural consistency, which strongly indicates the superiority of the catalyst. This study opens up a new route for the synthesis of efficient and robust catalysts for the generation of  $\text{H}_2$  in a cost-effective and less time-consuming pathway, which will have encouraging future applications in the field of renewable energy.

## Conflicts of interest

There are no conflicts to declare.

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